

Fugacity and activity coefficient for Van der Waals mixture

$\frac{1}{9}$

\underline{V} = molar volume, \bar{V} = partial molar volume
 V = extensive volume.

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By definition:

$$\ln \phi_i = \ln \frac{f_i}{x_i P} = \frac{1}{RT} \int_0^P (\bar{V}_i - \bar{V}_i^{IG}) dP \quad (1)$$

where ϕ_i is the mixture fugacity coefficient of component i , f_i is the fugacity of component i , \bar{V}_i is the partial molar volume of i and the superscript "IG" refers to an ideal gas.

we wish to integrate over V for most cubic EOS.

$$\bar{V}_i dP = \left(\frac{\partial V}{\partial N_i} \right)_{T,P,N_j} dP \quad (2)$$

where V is the total volume of the system.

Using the triple product rule

$$\left(\frac{\partial V}{\partial N_i} \right)_{T,P,N_j} \left(\frac{\partial P}{\partial V} \right)_{T,N_i,N_j} \left(\frac{\partial N_i}{\partial P} \right)_{T,V,N_j} = -1 \quad (3)$$

$$\therefore \left(\frac{\partial V}{\partial N_i} \right)_{T,P,N_j} dP = - \left(\frac{\partial V}{\partial P} \right)_{T,N_i,N_j} \left(\frac{\partial P}{\partial N_i} \right)_{T,V,N_j} dP \quad (4)$$
$$= \bar{V}_i dP$$

$$dV = \left(\frac{\partial V}{\partial P} \right)_{T, N_i, N_j} dP \quad (5)$$

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So eqn (4) can be written

$$\bar{V}_i dP = \left(\frac{\partial V}{\partial N_i} \right)_{T, P, N_j} dP = - \left(\frac{\partial P}{\partial N_i} \right)_{T, V, N_j} dV \quad (6)$$

$$dV = N d\bar{V} \quad \text{where } N = \text{total moles and } \bar{V} \text{ is molar volume.}$$

We need one more identity:

$$\frac{1}{\bar{V}} d(P\bar{V}) = \frac{P}{\bar{V}} d\bar{V} + dP \quad (7)$$

$$\therefore dP = \frac{1}{\bar{V}} d(P\bar{V}) - \frac{P}{\bar{V}} d\bar{V} \quad (8)$$

$$Z = \frac{P\bar{V}}{RT} \Rightarrow dP = \frac{RT}{\bar{V}} dZ - \frac{P}{\bar{V}} d\bar{V}$$

$$dP = \frac{P}{Z} dZ - \frac{P}{\bar{V}} d\bar{V} \quad (9)$$

Going back to eqn (1):

$$\ln \phi_i = \ln \frac{f_i}{x_i P} = \frac{1}{RT} \int_0^P (\bar{V}_i - \bar{V}_i^{\text{IG}}) dP$$

$$\bar{v}_i = \left(\frac{\partial v}{\partial N_i} \right)_{T, v, N_j} = - \left(\frac{\partial p}{\partial N_i} \right)_{T, v, N_j} \left(\frac{\partial v}{\partial p} \right)_{T, N_j} \quad (10)$$

$$\bar{v}_i^{IG} = \frac{RT}{p} \quad (11)$$

Substitute (10) and (11) into (1):

$$\ln \frac{f_i}{x_i p} = \frac{1}{RT} \int_0^p \left[- \left(\frac{\partial p}{\partial N_i} \right)_{T, v, N_j} \left(\frac{\partial v}{\partial p} \right)_{T, N_j} - \frac{RT}{p} \right] dp \quad (12)$$

↑ Eq'n (5)

$$dv = \left(\frac{\partial v}{\partial p} \right)_{T, N_j, N_j} dp$$

$$\ln \phi_i = - \frac{1}{RT} \int_{v=\infty}^v \left(\frac{\partial p}{\partial N_i} \right)_{T, v, N_j} N dv + \int_0^p - \frac{1}{p} dp \quad (13)$$

↑ Eq'n (9)

$$dp = \frac{p}{z} dz - \frac{p}{v} dv$$

$$\begin{aligned} \ln \phi_i &= - \frac{1}{RT} \int_{v=\infty}^v \left(\frac{\partial p}{\partial N_i} \right)_{T, v, N_j} N dv - \int \frac{1}{p} \left[\frac{p}{z} dz - \frac{p}{v} dv \right] \\ &= - \frac{1}{RT} \int_{v=\infty}^v \left(\frac{\partial p}{\partial N_i} \right)_{T, v, N_j} N dv + \int_{v=\infty}^v \frac{1}{v} dv - \int_{\substack{p=0 \\ z=1}}^z \frac{1}{z} dz \quad (14) \end{aligned}$$

$$\ln \phi_i = \frac{1}{RT} \int_{\underline{v}=\infty}^{\underline{v}} \left[\frac{RT}{\underline{v}} - N \left(\frac{\partial p}{\partial N_i} \right)_{T, \underline{v}, N_j} \right] d\underline{v} + \int_{\underline{v}=\infty}^{\underline{v}} \frac{1}{\underline{v}} d\underline{v} - \int_{z=1}^z \frac{1}{z} dz \quad \frac{4}{9}$$

$$\ln \phi_i = \ln \frac{f_i}{x_i p} = \frac{1}{RT} \int_{\underline{v}=\infty}^{\underline{v}} \left[\frac{RT}{\underline{v}} - N \left(\frac{\partial p}{\partial N_i} \right)_{T, \underline{v}, N_j} \right] d\underline{v} - \ln z \quad (15)$$

this form can now be used for vdw EOS.

$$p = \frac{RT}{\underline{v} - b} - \frac{a}{\underline{v}^2} \quad (16)$$

mixing rules

$$a = \sum_i \sum_j x_i x_j a_{ij} \quad (17)$$

$$b = \sum_i x_i b_i \quad (18)$$

write (16) using extensive volume and moles

$$p = \frac{NRT}{\underline{v} - Nb} - \frac{N^2 a}{\underline{v}^2} = \frac{NRT}{\underline{v} - \sum_i N_i b_i} - \frac{\sum_i \sum_j N_i N_j a_{ij}}{\underline{v}^2} \quad (19)$$

$$\left(\frac{\partial P}{\partial N_i}\right)_V = \frac{RT}{V - \sum N_i b_i} - \frac{NRT}{(V - \sum N_i b_i)^2} (-b_i) - 2 \frac{\sum N_j a_{ij}}{V^2} \quad (19)$$

$$\left(\frac{\partial P}{\partial N_i}\right)_V = \frac{RT}{V - Nb} + \frac{NRT b_i}{(V - Nb)^2} - 2 \frac{\sum N_j a_{ij}}{V^2} \quad (20)$$

Eq. (15) needs $N \left(\frac{\partial P}{\partial N_i}\right)_V$, so ...

$$N \left(\frac{\partial P}{\partial N_i}\right)_V = \frac{RT}{V - b} + \frac{RT b_i}{(V - b)^2} - 2 \frac{\sum x_j a_{ij}}{V^2} \quad (21)$$

Substitute into (15)

$$\ln \phi_i = \frac{1}{RT} \int_{V=\infty}^V \left[\frac{RT}{V} - \frac{RT}{(V-b)} - \frac{RT b_i}{(V-b)^2} + 2 \frac{\sum x_j a_{ij}}{V^2} \right] dV - \ln Z \quad (22)$$

integrate from $V=\infty \rightarrow V = \frac{2RT}{P}$

$$\ln \phi_i = \frac{1}{RT} \left[RT \ln \left(\frac{V}{V-b} \right) \right] \Big|_{V=\infty}^{\frac{2RT}{P}} + \frac{RT b_i}{(V-b)} \Big|_{V=\infty}^{\frac{2RT}{P}} - 2 \frac{\sum x_j a_{ij}}{V} \Big|_{V=\infty}^{\frac{2RT}{P}} - \ln Z \quad (23)$$

$$\ln \phi_i = \ln \left[\frac{\frac{z R T}{P}}{\frac{z R T}{P} - b} \cdot \left(\frac{P}{R T} \right) \right] + \frac{b_i}{\frac{z R T}{P} - b} \cdot \left(\frac{P}{R T} \right)^{\frac{6}{9}}$$

$$= \frac{z \sum x_j Q_{ij}}{R T \cdot \frac{z R T}{P}} - \ln z \quad (24)$$

define $B_i \equiv \frac{P b_i}{R T}$, $B \equiv \frac{P b}{R T}$ note: $\frac{z R T}{P} = \underline{V}$

$$\ln \phi_i = \ln \frac{z}{z-B} + \frac{B_i}{z-B} - z \frac{\sum x_j Q_{ij}}{R T \underline{V}} - \ln z \quad (25)$$

or finally...

$$\ln \phi_i = \ln \frac{f_i}{x_i P} = \frac{B_i}{z-B} - \ln(z-B) - z \frac{\sum_j x_j Q_{ij}}{R T \underline{V}} \quad (26)$$

To write each term wrt z :

$$A_{ij} \equiv Q_{ij} \frac{P}{(R T)^2}$$

$$\ln \phi_i = \frac{B_i}{z-B} - \ln(z-B) - \frac{z \sum_j A_{ij}}{z} \quad (27)$$

we can also compute the activity coefficient of species i in a mixture:

$$f_i = \gamma_i x_i f_i^0 \quad (27)$$

superscript 0 = pure fluid.

where γ_i is the activity coefficient and f_i^0 = pure i fugacity

From (26)

$$f_i = x_i P \exp \left[\frac{B_i}{Z-B} - \ln(Z-B) - \frac{2 \sum_j x_j A_{ij}}{Z} \right] \quad \text{mixture} \quad (28)$$

$f_i^0 = ?$ Derive in similar manner as for mixture.

Pure fluid: (Assume vapor, no phase change)

$$\ln \frac{f^0}{P} = \frac{1}{RT} \int_{\underline{v}=\infty}^{\underline{v}} \left(\frac{RT}{\underline{v}} - P \right) d\underline{v} - \ln Z^0 + (Z^0 - 1) \quad (29)$$

Integrate 1st term in (29)

$$\begin{aligned} \int_{\underline{v}=\infty}^{\underline{v}} \left(\frac{RT}{\underline{v}} - P \right) d\underline{v} &= \int_{\underline{v}=\infty}^{\underline{v}} \left(\frac{RT}{\underline{v}} - \frac{RT}{\underline{v}-b} + \frac{a}{\underline{v}^2} \right) d\underline{v} \\ &= RT \ln \left(\frac{\underline{v}}{\underline{v}-b} \right) - \frac{a}{\underline{v}} \quad \checkmark \quad (30) \end{aligned}$$

Substitute into (2a)

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$$\ln \frac{f^0}{P} = \ln \frac{\underline{V}}{\underline{V}-b} - \frac{a}{RT\underline{V}} + (z^0-1) - \ln z^0 \quad (31)$$

$$\ln \frac{f^0}{P} = \ln \left(\frac{z^0}{z^0 - \frac{Pb}{RT}} \right) - \frac{a}{RT\underline{V}} \cdot \left(\frac{RT}{P} \cdot \frac{P}{RT} \right) + (z^0-1) - \ln z^0 \quad (32)$$

multiply top
and bottom by P/RT

$$B \equiv \frac{Pb}{RT} \quad A \equiv \frac{aP}{(RT)^2}$$

$$\ln \frac{f^0}{P} = \ln z^0 - \ln(z^0 - B) - \frac{A}{z^0} + (z^0-1) - \ln z^0 \quad (33)$$

Note:

VdW EOS

$$P = \frac{RT}{\underline{V}-b} - \frac{a}{\underline{V}^2}$$

$$z^{VdW} = \frac{P\underline{V}}{RT} = \frac{\underline{V}}{\underline{V}-b} - \frac{a}{RT\underline{V}}$$

Finally

$$\ln \frac{f^0}{P} = (z^0-1) - \frac{A}{z^0} - \ln(z^0 - B) \quad (34)$$

From (34)

Pure i

$$f_i^0 = P \exp \left[(z^0 - 1) - \ln(z^0 - B_i) - \frac{A_{ii}}{z^0} \right]$$

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combine 27, 28, 35

(35)

$$\frac{f_i}{x_i f_i^0} = \gamma_i = \frac{\exp \left\{ \left[\frac{B_i}{(z - B)} \right] - \ln(z - B) - \left[\frac{\sum_j x_j A_{ij}}{z} \right] \right\}}{\exp \left\{ [z^0 - 1] - \ln[z^0 - B_i] - \frac{A_{ii}}{z^0} \right\}}$$

* This should give γ_i , but top term is for the mixture and bottom term is for pure. z in mixture not necessarily same as z^0 pure fluid. (36)