

Biased and flow driven Brownian motion in confined geometries

S. Martens¹, A. Straube¹, G. Schmid², P. Hänggi²,
and L. Schimansky-Geier¹

¹Department of Physics, Humboldt-Universität zu Berlin

²Department of Physics, Universität Augsburg

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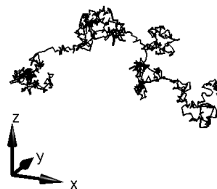


Free Brownian particle

- free Brownian particle subjected to external force $\mathbf{F} = (F, 0, 0)^T$ in x -direction

$$\cancel{m\ddot{\mathbf{q}}(t)} + \eta\dot{\mathbf{q}}(t) = \mathbf{F} + \sqrt{2\eta k_B T}\boldsymbol{\xi}(t)$$

- viscosity η , thermal energy $k_B T$, and Gaussian white noise $\boldsymbol{\xi}(t)$: $\langle\boldsymbol{\xi}(t)\rangle$ and $\langle\xi_i(t)\xi_j(s)\rangle = \delta_{i,j}\delta(t-s)$



- transport quantities of interest

- averaged velocity in the long time limit

$$\langle\dot{x}\rangle = \lim_{t\rightarrow\infty} \frac{\langle x(t) \rangle}{t}$$

- respectively, the mobility

$$\mu(F) = \langle\dot{x}\rangle / F$$

- effective diffusion coefficient D_{eff}

$$D_{\text{eff}} = \lim_{t\rightarrow\infty} \frac{\langle x(t)^2 \rangle - \langle x(t) \rangle^2}{2t}$$



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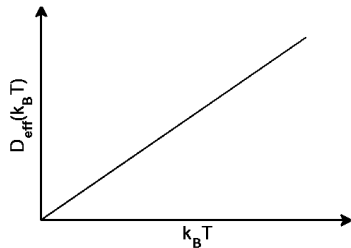
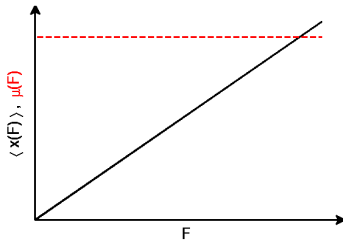
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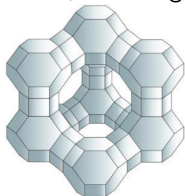
- averaged velocity $\langle \dot{x} \rangle = F/\eta$ is **independent** of thermal energy $k_B T$
- free mobility is given by $\mu_0 = 1/\eta$
- effective diffusion coefficient $D_{\text{eff}} = k_B T/\eta$ is **independent** of external force magnitude F

Sutherland-Einstein-relation $D_{\text{eff}} = \mu_0 k_B T$

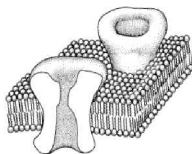


Brownian particle in confined geometries

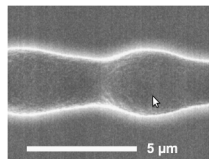
- interest in mass transport through confined structures such as porous media, zeolites, and irregular pores



<http://www.explainthatstuff.com/zeolites.html>



B. Hille, *Ion Channels of Excitable Membranes* (Sinauer, Sunderland, 2001)



C. Kettner et al., PRE **61**,312 (2000)

- *until now*: within the Fick-Jacobs approach ¹ effective description of biased Brownian particles suspended in an **unmovable fluid** is possible ^{2 3 4}

¹ R. Zwanzig, J. Chem. Phys., **96**, p. 3926-3930 (1992)

² D. Reguera et al., PRL, **96**, 130603 (2006)

³ P. S. Burada et al., BioSystems, **93**, 16 (2008)

⁴ P.S. Burada et al., Phil. Trans. R. Soc. A, **367**, 3157 (2009)

Reminder: FJ approach ⁵

- dimensionless Langevin equation for $V(x, y) = -f x$

$$\dot{x} = f + \sqrt{2}\xi_x(t), \quad \dot{y} = \sqrt{2}\xi_y(t)$$

where $f = FL/k_B T$

- assumption of fast equilibration in y
 \hookrightarrow reduction to an effective 1D description

$$\dot{x} = -\partial_x A(x) + \sqrt{2}\xi_x(t)$$

„entropic“ potential

$$A(x) = -f x - \ln(W(x))$$

⁵R. Zwanzig, J. Chem. Phys., **96**, p. 3926-3930 (1992)

Reminder: FJ approach ⁶

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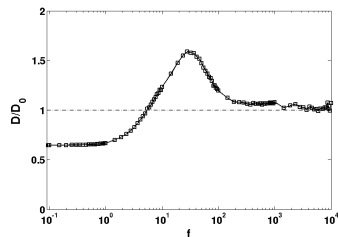
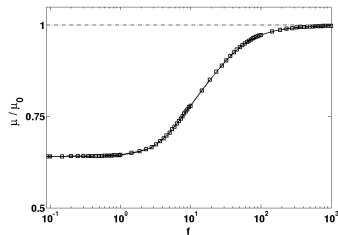
$$A(x) = -f x - \ln(W(x))$$

$$\lim_{f \rightarrow 0} \mu/\mu_0 \leq 1 \approx \frac{1}{\langle W(x) \rangle \langle 1/W(x) \rangle}$$

$$\lim_{f \rightarrow \infty} \mu/\mu_0 = 1$$

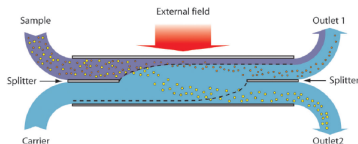
$$\lim_{f \rightarrow 0} D_{\text{eff}}/D_0 = \lim_{f \rightarrow 0} \mu/\mu_0$$

$$\lim_{f \rightarrow \infty} D_{\text{eff}}/D_0 = 1$$

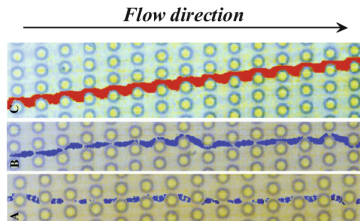


⁶R. Zwanzig, J. Chem. Phys., **96**, p. 3926-3930 (1992)

- experimentally relevant situation: **flow driven** separation of macro-molecules⁷, colloids⁸, and DNA⁹



A. Lenshof and T. Laurell, Chem. Soc. Rev. **39**, 1203 (2010),



⁷Lenshof et al., ChemSocRev **39**, 1203 (2010)

⁸M. Balvin et al., PRL **103**, 078301 (2009)

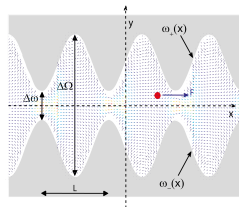
⁹M. P. MacDonald et al., Nature **426**, 421 (2003)

The model

- particle dynamics described by

$$\cancel{m\ddot{\mathbf{q}}(t)} + \eta (\dot{\mathbf{q}}(t) - \mathbf{u}(\mathbf{q}, t)) = -\vec{\nabla} V(\mathbf{q}) + \sqrt{2\eta k_B T} \xi(t)$$

- solvent flow field $\mathbf{u}(\mathbf{q}, t)$, external potential $V(\mathbf{q})$, viscosity η , thermal energy $k_B T$



- passing to dimensionless quantities and set $m = L = \eta = k_B T = 1$

$$\mathbf{q}' \rightarrow \mathbf{q}/L, t' \rightarrow t k_B T / \eta L^2, \mathbf{u}' \rightarrow \mathbf{u} \eta L / k_B T, V' \rightarrow V / k_B T$$

- yielding

$$\dot{\mathbf{q}} = \mathbf{u}(\mathbf{q}, t) - \vec{\nabla} V(\mathbf{q}) + \sqrt{2} \xi(t)$$



Fokker-Planck equation

- evolution of $P(\mathbf{q}, t)$ of finding the particle at $\mathbf{q} = (x, y)^T$ at time t

$$\partial_t P(\mathbf{q}, t) + \nabla_{\mathbf{q}} \cdot \mathbf{J}(\mathbf{q}, t) = 0,$$

with no-flux boundary conditions

$$\mathbf{J}(\mathbf{q}, t) \cdot \mathbf{n} = 0, \quad \forall \mathbf{q} \in \text{channel wall}.$$

and probability flux

$$\mathbf{J}(\mathbf{q}, t) = \left(\mathbf{u}(\mathbf{q}, t) - \vec{\nabla} V(\mathbf{q}) \right) P(\mathbf{q}, t) - \vec{\nabla} P(\mathbf{q}, t)$$

- obeys periodicity condition $P(x + m, y, t) = P(x, y, t)$, $\forall m \in \mathbb{Z}$ and is normalized
- focus on stationary probability density $P^{\text{st}}(\mathbf{q})$



Navier-Stokes equation

- evolution of volume element with flow velocity $\mathbf{u} = (v(\mathbf{q}, t), w(\mathbf{q}, t))^T$

$$R_e [\underbrace{\partial_t \mathbf{u}(\mathbf{q}, t) + (\mathbf{u}(\mathbf{q}, t) \cdot \vec{\nabla}) \mathbf{u}(\mathbf{q}, t)}_{\text{convection acceleration}}] = - \underbrace{\vec{\nabla} p(\mathbf{q}, t)}_{\text{pressure drop}} + \underbrace{\Delta \mathbf{u}(\mathbf{q}, t)}_{\text{viscosity}}$$

with dimensionless quantities $R_e = \rho_f k_B T / \eta^2$ and $p \rightarrow p k_B T / L^3$

- continuity equation for an incompressible flow

$$\vec{\nabla} \cdot \mathbf{u}(\mathbf{q}, t) = 0$$

- no-slip boundary condition

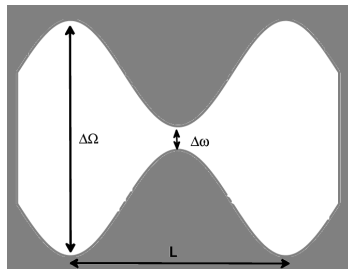
$$\mathbf{u}(\mathbf{q}, t) = 0 \quad , \quad \forall \mathbf{q} \in \text{wall}.$$



Long-wave analysis

- series expansion in the geometric parameter ε

$$\varepsilon = \frac{\Delta\Omega - \Delta\omega}{L}$$



- new scaling $y \rightarrow y/\varepsilon$, $w \rightarrow w/\varepsilon$, and $\omega_{\pm}(x) \rightarrow \varepsilon h_{\pm}(x)$
- perturbation series in the geometric parameter ε

$$v = v_0 + \varepsilon v_1 + \dots,$$

$$w = w_0 + \varepsilon w_1 + \dots,$$

$$\text{pressure : } p = \frac{1}{\varepsilon^2} p_0 + \frac{1}{\varepsilon} p_1 + \dots,$$

$$\text{prob.density : } P^{\text{st}} = P_0^{\text{st}} + \varepsilon^2 P_1^{\text{st}} + \dots,$$



Navier-Stokes equation: Zeroth order

- time derivative and convection acceleration are proportional to $\mathbf{Re}\epsilon^2$

leading order

$$p_0(x, y) = p_0(0, y) + \Delta p \int_0^x dx 1/W(x)^3 / \int_0^1 dx 1/W(x)^3 ,$$

$$v_0(x, y) = - \frac{p'_0(x)}{2} (h_+(x) - y) (y - h_-(x)) ,$$

$$w_0(x, y) = - \frac{1}{12} \partial_x \left[p'_0(x) (y - h_-(x))^2 (3h_+(x) - h_-(x) - 2y) \right]$$

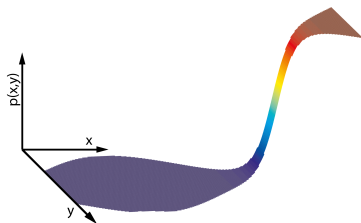
- pressure drop over period $\Delta p = p(x+1, y) - p(x, y)$
- local channel width $W(x) = h_+(x) - h_-(x)$



- exemplarily taken boundary function

$$h_{\pm}(x) = \pm h(x) = \pm \frac{1}{4} \left(\frac{1+\delta}{1-\delta} + \sin(2\pi x) \right)$$

with $\delta = \Delta\omega/\Delta\Omega$



Pressure profile $p(x, y)$ for $\Delta p > 0$.

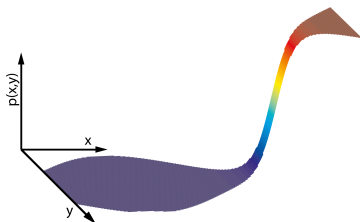
$\Delta\Omega = 1, \Delta\omega = 0.1$, and $Re = 0.1$



- exemplarily taken boundary function

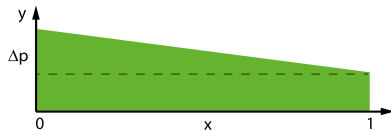
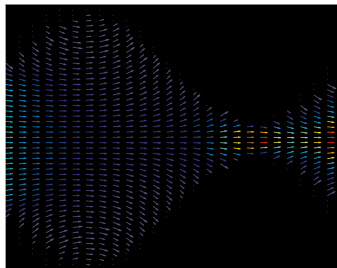
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Pressure profile $p(x, y)$ for $\Delta p > 0$.

$\Delta\Omega = 1, \Delta\omega = 0.1$, and $Re = 0.1$



Solvent velocity $u(q)$.

$\Delta\Omega = 1, \Delta\omega = 0.1, \Delta p = -10^3$, and $Re = 0.1$



Extension of FJ-approach to solvent flows

- zero-th order: $0 = \partial_y [e^{-V} \partial_y (e^V p_0(x, y))] \hookrightarrow p_0(x, y) = g(x) e^{-V(x, y)}$

"generalized" Fick-Jacobs equation

$$0 = \partial_x \left\{ e^{-\Psi(x)} \partial_x \left(e^{\Psi(x)} p_0(x) \right) \right\}$$

"generalized" effective potential

$$\Psi(x) = A(x) - \int_0^x dx' \left[\frac{\int_{h_-(x')}^{h_+(x')} v_0(x', y) e^{-V(x', y)} dy}{\int_{h_-(x')}^{h_+(x')} e^{-V(x', y)} dy} \right]$$



"generalized" effective potential

- concept of mean force

$$\frac{d \Psi(x)}{d x} = -\partial_x \ln \left[\int_{h_-(x)}^{h_+(x)} e^{-V(q)} dy \right] - \int_{h_-(x)}^{h_+(x)} v_0(x, y) \frac{e^{-V(q)}}{\int_{h_-(x)}^{h_+(x)} e^{-V(q)} dy} dy$$



"generalized" effective potential

- concept of mean force

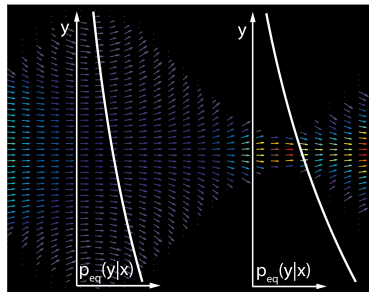
$$\frac{d\Psi(x)}{dx} = -\partial_x \ln \left[\int_{h_-(x)}^{h_+(x)} e^{-V(q)} dy \right] - \int_{h_-(x)}^{h_+(x)} dy v_0(x, y) \underbrace{\frac{e^{-V(q)}}{\int_{h_-(x)}^{h_+(x)} e^{-V(q)} dy}}_{p_{\text{eq}}(y|x)} dy$$



"generalized" effective potential

- concept of mean force

$$-\frac{d\Psi(x)}{dx} = - \int_{h_-(x)}^{h_+(x)} \partial_x V(\mathbf{q}) p_{\text{eq}}(y|x) dy \\ + \int_{h_-(x)}^{h_+(x)} v_0(x, y) p_{\text{eq}}(y|x) dy$$



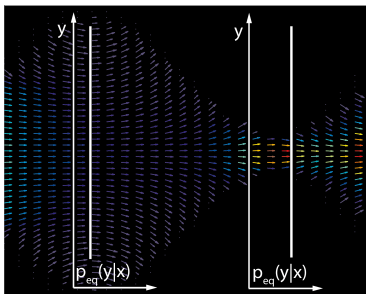
$p_{\text{eq}}(y|x)$ for $V(\mathbf{q}) = -f x - g y$.



"generalized" effective potential

- for only longitudinal forcing $V(\mathbf{q}) = -f x$

$$-\frac{d\psi(x)}{dx} = \underbrace{f + \frac{W'(x)}{W(x)}}_{\text{mean force originated by bias}} - \underbrace{\frac{\Delta p}{12 \int_0^1 dx 1/W^3(x)}}_{\text{mean force originated by solvent flow}} \frac{1}{W(x)}$$



$p_{eq}(y|x)$ for $V(\mathbf{q}) = -f x$.



- solution of "generalized" Fick-Jacobs equation

$$p_0(x) = e^{-\Psi(x)} \int_x^{x+1} e^{\Psi(x')} dx' / \left[\int_0^1 dx e^{-\Psi(x)} \int_x^{x+1} e^{\Psi(x')} dx' \right]$$

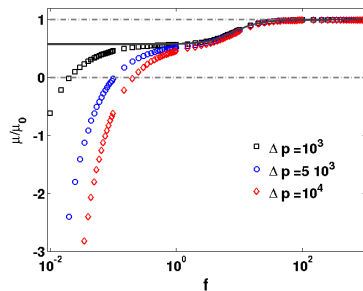
- Stratonovich formula ¹⁰

$$\frac{\mu(f)}{\mu_0} = \frac{\langle \dot{x}(f) \rangle_0}{f} = \frac{1 - e^{\Delta\Psi}}{f \int_0^1 dx e^{-\Psi(x)} \int_x^{x+1} e^{\Psi(x')} dx'}$$

with $\Delta\Psi = \Psi(1) - \Psi(0)$

¹⁰R. L. Stratonovich, Radiotekh. Elektron. (Moscow),3, 497 (1958)

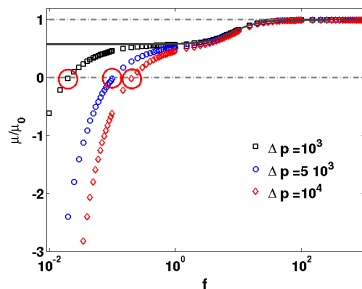
Particle mobility μ



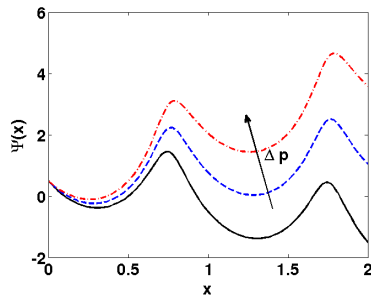
Particle mobility versus f . $\Delta\Omega = 0.1$, $\Delta\omega = 0.01$, and $Re = 0.1$



Particle mobility μ



Particle mobility versus f . $\Delta\Omega = 0.1$, $\Delta\omega = 0.01$, and $Re = 0.1$.

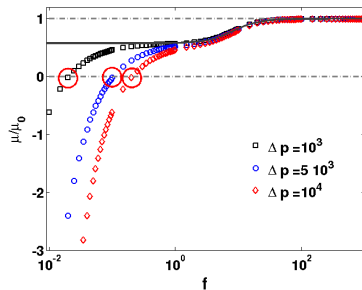


Effective potential $\Psi(x)$ for $f = 0.1$ and $\Delta p = 0, 5 \cdot 10^3, 10^4$ (from bottom to top).

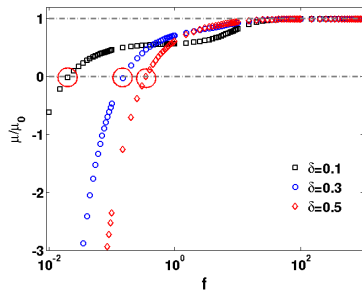
$\Delta\Omega = 1$, $\Delta\omega = 0.1$, and $Re = 0.1$



Particle mobility μ



Particle mobility versus f . $\Delta\Omega = 0.1$, $\Delta\omega = 0.01$, and $Re = 0.1$.



Particle mobility versus f . $\Delta\Omega = 0.1$, $\Delta p = 10^3$, and $Re = 0.1$.

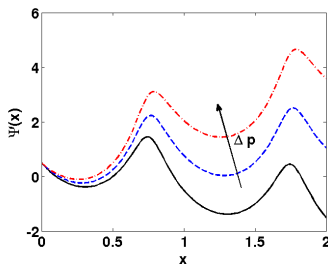


Competition between external bias and solvent flow

- mean particle current vanishes if

$$0 = \Delta\Psi = -f - \frac{\Delta p \int_0^1 1/W(x) dx}{12 \int_0^1 1/W(x)^3 dx}$$

$$\hookrightarrow \left(\frac{f}{\Delta p}\right)_{\text{crit}} = - \frac{\int_0^1 1/W(x) dx}{12 \int_0^1 1/W(x)^3 dx}$$

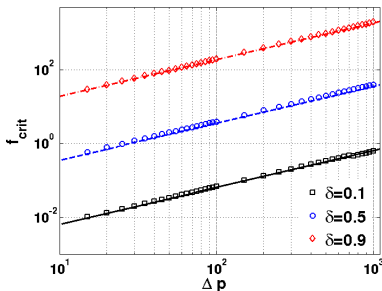


Potential of mean force $\Psi(x)$



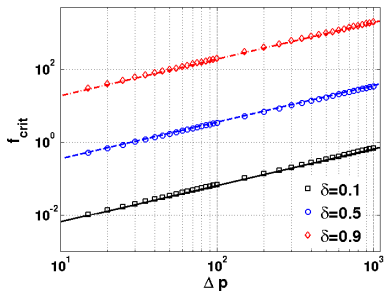
- for sinusoidal channel $h(x)$

$$\left(\frac{f}{\Delta p}\right)_{\text{crit}} = \frac{\delta^2}{6(1-\delta)^2(3+2\delta+3\delta^2)}$$



Critical force magnitude versus pressure drop Δp .

$\Delta\Omega = 0.1$ and $Re = 0.1$.



Critical force magnitude versus pressure drop Δp .

$\Delta\Omega = 1$ and $Re = 0.1$.



Summary

- present expansion of NSE and FPE in geometric parameter ε
 \hookrightarrow calculate leading order of $\mathbf{u}(\mathbf{q})$ and $P(\mathbf{q})$
- ① purely flow driven transport
 - obtain $P(\mathbf{q}) = 1/A_{\text{unit-cell}}$ and analytic expression for $\langle \dot{x} \rangle_0$ and D_{eff}/D_0
- ② combined biased and flow driven transport
 - present extension of Fick-Jacobs approach to experimentally relevant situation of moving solvent
 - effective description where particle evolve in potential of mean force

$$\Psi(x) = A(x) - \int_0^x \left[\int_{h_-(x)}^{h_+(x)} v_0(x, y) p_{\text{eq}}(y|x) \right]$$

- it exist critical ratio $(f/\Delta p)_{\text{crit}}$ where both drag forces anihilate each other
- numerics show that results are also **valid for $\varepsilon \simeq 1$**

