

**ChE 101 – Final Exam
Winter 2008**Instructor: Sumit Kundu
2.5 hours (12:30 – 3:00)Thursday April 10, 2008
Location: RCH 301

Chemical Periodic Table is allowed. 2 page cheat sheet is allowed.

YOU CAN NOT USE A GRAPHING CALCULATOR TO SIMULTANEOUSLY SOLVE MULTIPLE EQUATIONS (but feel free to check your work with them)

PLAGIARISM/CHEATING: A zero-tolerance policy will be adhered to. No talking or sharing of Notes during the mid-term. All of the University of Waterloo mid-term and exam regulations do apply.

The question pages must be returned with the answer booklet. **NUMBER ANY ADDITION PAGES ADDED** and indicate the total number of pages.

HINT –NOT all questions are of equal difficulty, complexity or length. Marks for each question are not representative of the question difficulty.

Data:

Pressure:	1.0 atm = 101.3 kPa = 760 mmHg = 760 torr = 14.696 psia
Temperature:	Water freezes at 0°C = 273.15 K = 32°F = 492°R; boils at 100°C = 212°F
Quantities:	Molar volume of ideal gas = 22.414 L mol ⁻¹ at 273.15 K and 1.0 atm. (STP)
	Molecular weight of air = 29 g mol ⁻¹
	1 m = 3.28 ft; 2.54 cm = 1 in; 1 acre = 43,560 ft ²
	28.32 L = 1.0 ft ³ 1 L = 1000 cm ³
	1.0 pound = 454 grams 1 cal = 4.184 J
	1 erg = 1 g cm ² s ⁻² 1 J = 1 N m 1 W = J s ⁻¹ 1 A = C s ⁻¹
Gas constants:	R = 8.314 (10 ⁷) erg mol ⁻¹ K ⁻¹ = 8.314 L kPa mol ⁻¹ K ⁻¹
	= 0.08206 L atm mol ⁻¹ K ⁻¹ = 8.314 J mol ⁻¹ K ⁻¹
	= 1.987 cal mol ⁻¹ K ⁻¹ = 8.314 kg m ² s ⁻² mol ⁻¹ K ⁻¹
Planck's Constant	= 6.626218*10 ⁻³⁴ J sec Speed of light = 2.997925*10 ⁸ m sec ⁻¹
Avogadro's Number	= 6.022*10 ²³
Boltzmann constant:	k _B = 1.381 (10 ⁻¹⁶) erg molecule ⁻¹ K ⁻¹
Faraday	F = 96,485 coulombs mol ⁻¹

MARKS WILL BE DEDUCTED FOR:

- incorrect answers,
- simple math errors,
- synthesis flaws,
- poorly presented solutions,
- hard to follow solutions,
- lack of a clearly stated Basis;
- lack of a clearly outlined flow diagram or sketch of the process;
- incorrect units, or
- improper use of significant figures.

Do all FIVE of the following Questions

NAME: _____

Problem 1 (10 Marks)

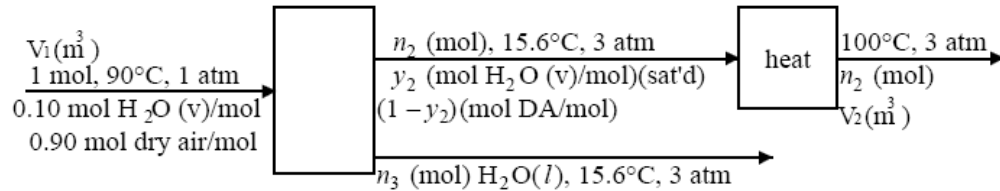
Water flows from an elevated reservoir, through a pipe, to a turbine at a lower level, then out of the turbine through a similar pipe. At a point 100 m above the turbine the pressure is 207 kPa, and at a point 3 m below the turbine the pressure is 124 kPa. Use a mechanical energy balance to determine what the water flow rate must be if the turbine output is 1×10^5 W? Assume no friction losses.

Data: Density of water is 1000 kg/m^3

Problem 2 (10 Marks)

Air at 90°C and 1 atm (absolute) contains 10 mole% water. A continuous stream of this air enters a condenser, in which the temperature is lowered to 15.6°C and the pressure is raised to 3 atm. The air leaving the condenser is then heated at constant pressure to 100°C. Calculate the fraction of water that is condensed from the air and the relative humidity of the air at 100°C.

6.18 Basis: 1 mol feed



$$\text{Saturation: } y_2 = \frac{P_{\text{H}_2\text{O}}^*(15.6^\circ\text{C})}{P} \xrightarrow{\text{Table B.3}} y_2 = \frac{13.29 \text{ mm Hg}}{3 \text{ atm}} \left| \frac{\text{atm}}{760 \text{ mm Hg}} \right| = 0.00583$$

$$\text{Dry air balance: } 0.90(1) = n_2(1 - 0.00583) \Rightarrow n_2 = 0.9053 \text{ mol}$$

$$\text{H}_2\text{O mol balance: } 0.10(1) = 0.00583(0.9053) + n_3 \Rightarrow n_3 = 0.0947 \text{ mol}$$

$$\text{Fraction H}_2\text{O condensed: } \frac{0.0947 \text{ mol condensed}}{0.100 \text{ mol fed}} = \underline{\underline{0.947 \text{ mol condense/mol fed}}}$$

$$h_r = \frac{y_2 P \times 100\%}{p^*(100^\circ\text{C})} = \frac{0.00583(3 \text{ atm})}{1 \text{ atm}} \times 100\% = \underline{\underline{1.75\%}}$$

Problem 3 (12 Marks)

8.28

On a warm winter day the temperature is 2°C and the relative humidity is 15%. You inhale air at an average rate of 5500 mL/min and exhale a gas saturated with water at body temperature, 37°C. If the mass flow rates of the inhaled and exhaled air (excluding water) are the same, the heat capacity of dry air is 1.05 J/g °C, and water exists in your body as a liquid at 22°C, at what rate in J/day do you lose energy by breathing? Treat breathing as a continuous process and neglect work done by the lungs.

Heat capacity of liquid water = , Cp Water Vapour = , Heat of vapourization of water(22°C)

ANTOINE'S CONSTANTS:

A

B

C

Water:

7.96681

1668.21

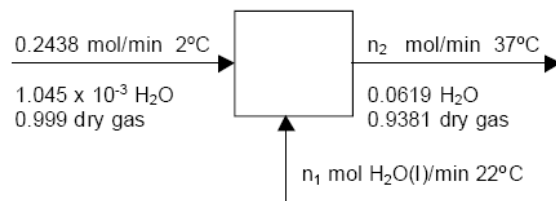
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$$8.28 \quad 2^\circ\text{C}, 15\% \text{ rel. humidity} \Rightarrow p_{\text{H}_2\text{O}} = (0.15)(5.294 \text{ mm Hg}) = 0.7941 \text{ mm Hg}$$

$$(y_{\text{H}_2\text{O}})_{\text{inhaled}} = (0.7941)/(760) = 1.045 \times 10^{-3} \text{ mol H}_2\text{O/mol inhaled air}$$

$$\dot{n}_{\text{inhaled}} = \frac{5500 \text{ ml}}{\text{min}} \left| \frac{273 \text{ K}}{275 \text{ K}} \right| \left| \frac{1 \text{ liter}}{10^3 \text{ ml}} \right| \left| \frac{1 \text{ mol}}{22.4 \text{ liters(STP)}} \right| = 0.2438 \text{ mol air inhaled/min}$$

$$\text{Saturation at } 37^\circ\text{C} \Rightarrow y_{\text{H}_2\text{O}} = \frac{p^*(37^\circ\text{C})}{760 \text{ mm Hg}} = \frac{47.067}{760} = 0.0619 \text{ mol H}_2\text{O/mol exhaled dry gas}$$



$$\text{Mass of dry gas inhaled (and exhaled)} = \frac{(0.2438)(0.999) \text{ mol dry gas}}{\text{min}} \left| \frac{29.0 \text{ g}}{\text{mol}} \right| = 7.063 \text{ g/min}$$

$$\text{Dry gas balance: } (0.999)(0.2438) = 0.9381 \dot{n}_2 \Rightarrow \dot{n}_2 = 0.2596 \text{ mols exhaled/min}$$

$$\text{H}_2\text{O balance: } (0.2438)(1.045 \times 10^{-3}) + \dot{n}_1 = (0.2596)(0.0619) \Rightarrow \dot{n}_1 = 0.0158 \text{ mol H}_2\text{O/min}$$

References for enthalpy calculations: $\text{H}_2\text{O}(l)$ at triple point, dry gas at 2 °C

substance	\dot{m}_{in}	\hat{H}_{in}	\dot{m}_{out}	\hat{H}_{out}
Dry gas	7.063	0	7.063	36.75
$\text{H}_2\text{O}(v)$	0.00459	2505	0.290	2569
$\text{H}_2\text{O}(l)$	0.285	92.2	—	—

$$\begin{aligned} \dot{m} \text{ in g/min} & \quad \dot{m}_{\text{H}_2\text{O}} = 18.02 \dot{n}_{\text{H}_2\text{O}} \\ \hat{H} \text{ in J/g} & \quad \hat{H}_{\text{H}_2\text{O}} \text{ from Table 8.4} \\ & \quad \hat{H}_{\text{dry gas}} = 1.05(T - 2) \end{aligned}$$

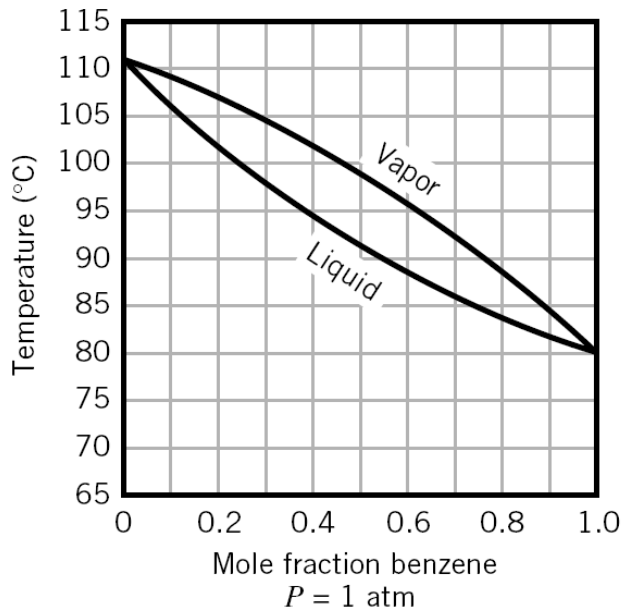
$$Q = \Delta H = \sum_{\text{out}} \dot{m}_i \hat{H}_i - \sum_{\text{in}} \dot{m}_i \hat{H}_i = \frac{966.8 \text{ J}}{\text{min}} \left| \frac{60 \text{ min}}{1 \text{ hr}} \right| \left| \frac{24 \text{ hr}}{1 \text{ day}} \right| = 1.39 \times 10^6 \text{ J/day}$$

Problem 4 (14 Marks)

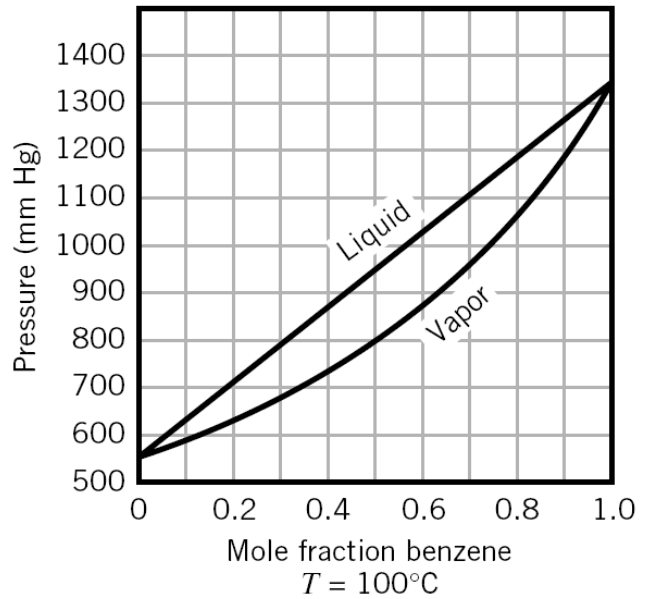
Eg.

100 mols of an equimolar liquid mixture of benzene and toluene at 10°C and 760 mm Hg is fed continuously to a vessel in which the mixture is heated to 50°C. What is the heating requirement of the heater?

Data: $C_{p, \text{Benzene}, l} =$, $C_{p, \text{Benzene}, v}$, $C_{p, \text{Toluene}, l}$, $C_{p, \text{Toluene}, v}$, $\Delta\hat{H}_{vap, \text{Benzene}}(80.1^\circ\text{C}) =$, $\Delta\hat{H}_{vap, \text{Toluene}}(110^\circ\text{C}) =$



(a) Txy diagram

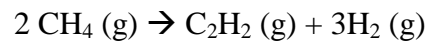


(b) Pxy diagram

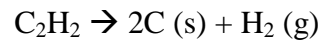
Problem 5 (14 Marks)

9.36

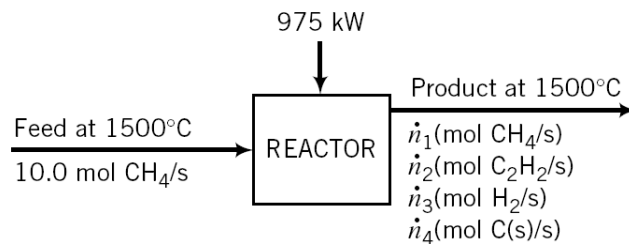
You are checking the performance of a reactor in which acetylene is produced from methane in the reaction



An undesired side reaction is the decomposition of acetylene:



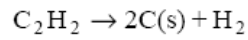
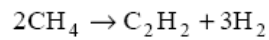
Methane is fed to the reactor at 1500 °C at a rate of 10.0 mol CH₄/s. Heat is transferred to the reactor at a rate of 975 kW. The product temperature is 1500 °C and the fractional conversion of methane is 0.600.



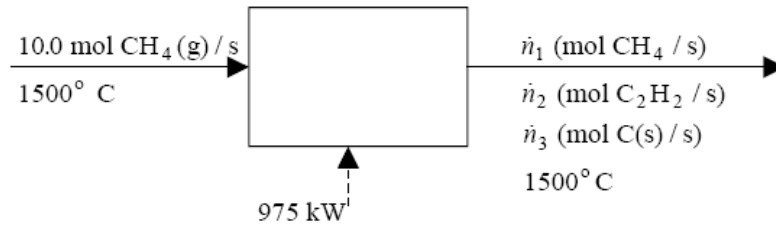
Determine the molar flow rates of the product components and the yield of acetylene (mol C₂H₂ produced/mol CH₄ consumed).

DATA: Cp, heat of formations

9.36



Basis: 10 mol $\text{CH}_4(\text{g})$ fed/s



a.

60% conversion $\Rightarrow \dot{n}_1 = 10(1 - 0.600) = \underline{\underline{4.00 \text{ mol CH}_4/\text{s}}}$

C balance: $10(1) = 4(1) + 2\dot{n}_2 + \dot{n}_4 \Rightarrow 2\dot{n}_2 + \dot{n}_4 = 6 \quad (1)$

H balance: $10(4) = 4(4) + 2\dot{n}_2 + 2\dot{n}_3 \Rightarrow 2\dot{n}_2 + 2\dot{n}_3 = 24 \quad (2)$

References for enthalpy calculations : C(s) , $\text{H}_2(\text{g})$ at 25°C

$$H_i = \left(\Delta \hat{H}_f^\circ \right)_i + C_{pi}(1500 - 25), \quad i = \text{CH}_4, \text{C}_2\text{H}_2, \text{C}, \text{H}_2$$

Substance	\dot{n}_{in} (mol/s)	\hat{H}_{in} (kJ/mol)	\dot{n}_{out} (mol/s)	\hat{H}_{out} (kJ/mol)
$\text{CH}_4(\text{g})$	10	41.68	4	41.68
$\text{C}_2\text{H}_2(\text{g})$	—	—	\dot{n}_2	303.45
$\text{H}_2(\text{g})$	—	—	\dot{n}_3	45.72
C(s)	—	—	\dot{n}_4	32.45

Energy Balance: $Q = \Delta H \Rightarrow 975 \text{ kJ/s} = \sum_{\text{out}} \dot{n}_i \hat{H}_i - \sum_{\text{in}} \dot{n}_i \hat{H}_i \quad (3)$

Solve (1) - (3) simultaneously $\Rightarrow \begin{cases} \dot{n}_2 = \underline{\underline{2.50 \text{ mol C}_2\text{H}_2/\text{s}}} \\ \dot{n}_3 = \underline{\underline{9.50 \text{ mol H}_2/\text{s}}} \\ \dot{n}_4 = \underline{\underline{1.00 \text{ mol C/s}}} \end{cases}$

Yield of acetylene $= \frac{2.50 \text{ mol C}_2\text{H}_2/\text{s}}{6.00 \text{ mol CH}_4 \text{ consumed/s}} = \underline{\underline{0.417 \text{ mol C}_2\text{H}_2/\text{mol CH}_4 \text{ consumed}}}$