

POD 21

①

How to get K_L^0

$$K_L^0 a = \frac{1}{\frac{1}{K_L a} + \frac{1}{H K_g a}}$$

So we need H , K_L , K_g & a

a should be a_w - wetted area/vol

vs. a_t = total area/vol

Onda correlation:

$$\frac{a_w}{a_t} = 1 - \exp \left[-1.45 \left(\frac{\sigma_c}{\sigma_L} \right)^{0.75} \times (Re_L)^{0.1} (Fr)^{-0.05} (We_L)^{0.2} \right]$$

σ_c : critical packing tension

σ_L : liquid surface tension

$$Re_L = \left(\frac{\rho_L L}{a_t \mu_L} \right)$$

(2)

$$L = \text{liquid superficial } \cancel{\text{flow rate}} \left(\frac{\text{velocity} \times \text{length}}{\text{time}} \right)$$

$$= \frac{Q}{A} \leftarrow \text{vol flow rate}$$

$$= \frac{Q}{A} \leftarrow \text{column area}$$

ρ_L = density of liquid

a_t = total packing area/vol

μ_L = liquid viscosity

$$Fr = \frac{L^2 a_t}{g} \quad (\text{Froude } \cancel{\text{no}})$$

g = gravity

$$We = \text{Weber } \cancel{\text{no}} = \left(\frac{L^2 \rho_L}{\sigma_L a_t} \right)$$

Now for K_L :

$$K_L = 0.0051 \left(\frac{\mu_L g}{\rho_L} \right)^{1/3} Re^{2/3} Sc^{-1/2} (a_t d_p)^{0.4}$$

$$Sc = \text{Schmidt } \cancel{\text{no}} = \frac{\nu_L}{D_L}$$

$$D_L = \text{liquid diff}, \quad \nu_L = \frac{\mu_L}{\rho_L}$$

(3)

~~Re~~ $a_t d_p$ is a packing (shape) factor:

d_p = nominal packing size

Note that $\left(\frac{\rho_L g}{\rho_L}\right)^{1/3}$ has units of velocity, as is k_L

And for the gas phase:

$$k_{GG} = C a_t D_G \left(\frac{G \rho_{GG}}{a_t \mu_G}\right)^{0.7} \left(\frac{\mu_G}{\rho_G D_G}\right)^{1/3} (a_t d_p)^{-2}$$

$C = 2.0$ if $d_p < 15\text{mm}$, 5.3 if $d_p > 15\text{mm}$

D_G = gas phase diffusivity

G = Gas superficial velocity

ρ_G = Gas density

μ_G = Gas viscosity

So we need:

Packing prop. { Packing type/size:
 a_t , Q_p , σ_c (packing tension)

Liquid prop. { Liquid surface tension σ_L
 Liquid density ρ_L
 Liquid viscosity μ_L

Gas prop. { Gas density ρ_G
 Gas viscosity μ_G

Solute prop. { ~~Dif~~ Solute Dif in Gas D_G
 Solute Dif in Liquid D_L
 Henry's law Coef (vol basis) H

operating param. { Liquid superficial vel. L
 Gas superficial vel. G

5

Let's look at stripping chloroform out of water at 25°C

We propose to use 1" Pall rings
(~~plastic~~ ^{steel}).

From the manufacturer,

$$d_p = 25 \text{ mm} = 2.5 \text{ cm}$$

$$a_t = 209 \text{ m}^2/\text{m}^3 = 2.09 \text{ 1/cm}$$

$$\text{so } a_t d_p = 5.22$$

$$\text{For } ~~plastic~~ ^{steel} \quad \sigma_c = 0.075 \text{ N/m} = 75 \text{ dynes/cm}$$

~~and~~

Liquid properties: (water)

$$\sigma_L = 70 \text{ dynes/cm (clean water)}$$

$$\rho_L = 1 \text{ g/cm}^3$$

$$\mu_L = 0.01 \text{ poise } \left(\frac{\text{g}}{\text{cm s}} \right)$$

$$\nu_L = 0.01 \text{ cm}^2/\text{s}$$

(6)

Gas properties : air at 1 Atm, 25°C

$$\rho_G = 1.18 \times 10^{-3} \text{ g/cm}^3$$

$$\mu_G = 1.85 \times 10^{-4} \text{ poise}$$

$$\nu_G = 0.156 \text{ cm}^2/\text{s}$$

Solute Properties (chloroform)

$$D_G = 0.090 \text{ cm}^2/\text{s}$$

$$D_L = 1.0 \times 10^{-5} \text{ cm}^2/\text{s}$$

$$H = 10^{\left[4.673 - \frac{1627}{T}\right]} = 0.163$$

Operating Parameters

$$L = 1.53 \text{ cm/s} \quad (= 22.6 \text{ gpm/ft}^2)$$

$$G = 43 \text{ cm/s} \quad (= 84 \text{ cfm/ft}^2)$$

$$R = \frac{H \cdot G}{L} = 4.6$$

(7)

So:

$$\sigma_c / \sigma_L = \frac{75}{70} = \cancel{0.857} 1.07$$

$$Re_L = \frac{(1.53 \text{ cm/s})(1 \text{ g/cm}^3)}{(2.09 \text{ } \frac{1}{\text{cm}})(0.01 \text{ g/cm}^3)} = 73.2$$

$$Fr = \frac{(1.53 \text{ cm/s})^2 (2.09 \text{ } \frac{1}{\text{cm}})}{980 \text{ cm/s}^2} = 0.0050$$

$$We_L = \frac{(1.53 \text{ cm/s})^2 (1 \text{ g/cm}^3)}{(70 \text{ dyne/cm})(2.09 \text{ } \frac{1}{\text{cm}})} = 0.016$$

$$\begin{aligned} \frac{a_w}{a_f} &= 1 - \exp \left[-1.45 \left(\cancel{0.857} \right)^{0.75} \times (73.2)^{0.1} \right. \\ &\quad \left. \times (0.0050)^{-0.05} \times (0.016)^{0.2} \right] \\ &= 0. \cancel{85} 74 \end{aligned}$$

So for these conditions we're only ^{3/4} ~~100%~~ wetted! Note that if σ_L is lower then it changes a lot.

8

Now for k_L :

$$Re_L = 73.2 \quad a_t d_p = 5.22$$

$$Sc = \frac{0.01 \frac{\text{cm}^2}{\text{s}}}{1 \times 10^{-5} \frac{\text{cm}^2}{\text{s}}} = 1000$$

$$\frac{\mu_L g}{\rho_L} = \nu_L g = 0.01 \frac{\text{cm}^2}{\text{s}} \cdot 980 \frac{\text{cm}}{\text{s}^2} = 9.8 \frac{\text{cm}^3}{\text{s}^3}$$

$$\begin{aligned} \therefore k_L &= 0.0051 \times \left(9.8 \frac{\text{cm}^3}{\text{s}^3}\right)^{1/3} \times (73.2)^{2/3} \\ &\quad \times (1000)^{-1/2} \times (5.22)^{0.4} \\ &= 0.0117 \frac{\text{cm}}{\text{s}} \end{aligned}$$

And for k_G

$$\frac{G \rho_g}{a_t \mu_g} = \frac{43 \frac{\text{cm}}{\text{s}}}{(2.09 \frac{1}{\text{cm}})(0.156 \frac{\text{cm}^2}{\text{s}})} = 132$$

$$\frac{\mu_g}{\rho_g D_g} = \frac{0.156 \frac{\text{cm}^2}{\text{s}}}{0.090 \frac{\text{cm}^2}{\text{s}}} = 1.73$$

$$C = 5.3 \quad (d_p = 25 \mu\text{m} > 15 \mu\text{m})$$

(9)

So:

$$K_G = (5.3)(2.09 \text{ } ^1\text{/cm})(0.09 \text{ cm}^2\text{/s}) \\ \times (132)^{0.7} (1.73)^{1/3} (5.22)^{-2} \\ = 1.34 \text{ cm/s}$$

$$\text{so } K_L^0 = \frac{1}{\frac{1}{K_L} + \frac{1}{H K_G}} \\ = \frac{1}{\frac{1}{0.0117} + \frac{1}{(1.34)(0.163)}} = 0.0111 \text{ cm/s}$$

↑
Almost same
as K_L !

$$\text{and } K_L^0 a_w = 0.0172 \text{ s}^{-1}$$

$$w/ H_{ox} = \frac{L}{K_L^0 a_w} = \frac{1.53 \text{ cm/s}}{0.0172 \text{ } ^1\text{/s}} = 89 \text{ cm} \\ \approx 0.89 \text{ m}$$

This, coupled w/ N_{ox} , would give you the height of the tower!