

POD 293: Simulation of AF4 Separation Suppose we have the sample shear: ux = by and we have a species Which has diffusivity D. We have the convective of a egin: 3c +8y 8x - 40 8y = 0 32c scaling: y= //2 /c = U $t_c = \frac{\gamma_c^2}{D} = \frac{D}{U_0^2}, \quad x_c = \frac{8\gamma_c^3}{D} = \frac{3}{4}\frac{D^2}{U_0^3}$ Recall we had the dimensionless dispersively $\frac{17}{D} = 1 + 2 \frac{x_c}{\Delta t_c} = 1 + 2 \left(\frac{80^2}{40^3} \right)^2 \frac{u_0^2}{D^2} = 1 + 2 \frac{8^2 D^2}{40^3}$ obtained from method of moments.

In any event, we can simulate the Dispersion!



Our Dimensionless egin is: $\frac{\partial C}{\partial t} + \gamma \frac{\partial C}{\partial x} - \frac{\partial C}{\partial y} = \frac{\partial^2 C}{\partial y}$ Instially our distribution on the y direction is e We can get this by placing tracers s, t. y = - log (rand (n, 1)) At each time step we displace in the y direction - lt and a random step (22t") randn(n,1). We integrate the velocity in the x direction and the Dimensionless scaled Dispersivity is just for half the growth in the variance:

Where K = 1203 = 2

Thus or should increase as 4t at long times (e.g., in the Taylor lond). What if we have a second species sit. D2 = D2. We can smulate this by adding a random step (20 dt) tat each time. Our initial dist. should be y= - D= log (rand(n,1)) as well. The two peates should separate w/ velocity D2-1. If D2-1 is small then the variances should be smilar. doupte the separation would occur when (D2-1)t>4 (4t*)" or $t^{*/2} > \frac{8}{D_2^*-1}$. $t^* > \frac{64}{D_2^*-1}$ this is a pretty long tome . . . (actually like

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POD 23: MC Simulation of Taylor Dispersion in AF4

We construct a simple Monte Carlo simulation of dispersion in a asymmetric flow field flow fractionation device. The distribution is exponential in y, and there is a simple shear flow in the x direction. We add in a second species to see separation based on the diffusivity.

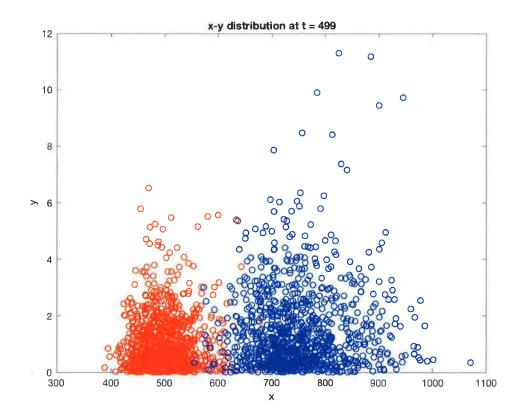
```
n = 1000;
Dastar = 1.5; % A second species with a different diffusivity.
% We distribute them randomly.
y = -log(rand(n,1));
x = zeros(n,1);
ya = -Dastar*log(rand(n,1));
xa = zeros(n,1);
dt = 0.001; %Our time step
tquit = 500;
t = [dt:dt:tquit]'; %Our times
ux = \theta(y) y; %our velocity profile
varx = zeros(1/dt,1); %we keep track of the variance.
varxa = zeros(1/dt,1); %we keep track of the variance.
for i=1:tquit/dt-1
    dx1 = ux(y);
    y = y - dt + randn(n,1)*(2*dt)^.5; %Updating y
    y = abs(y); %Reflection from the accumulating wall
    dx2 = ux(y);
    x = x + (dx1+dx2)/2*dt; %We update the velocity
    varx(i) = var(x);
    % Now we repeat for the second type of particle.
    dxal = ux(ya);
    ya = ya - dt + randn(n,1)*(2*Dastar*dt)^.5;
    ya = abs(ya);
    dxa2 = ux(ya);
    xa = xa + (dxa1+dxa2)/2*dt; %We update the velocity
   varxa(i) = var(xa);
    % We plot up the distributions every thousand iterations.
    if i/1000==round(i/1000)
      figure(1)
      plot(x,y,'or',xa,ya,'ob')
     xlabel('x')
      ylabel('y')
      title(['x-y distribution at t = ',num2str(t(i))])
```

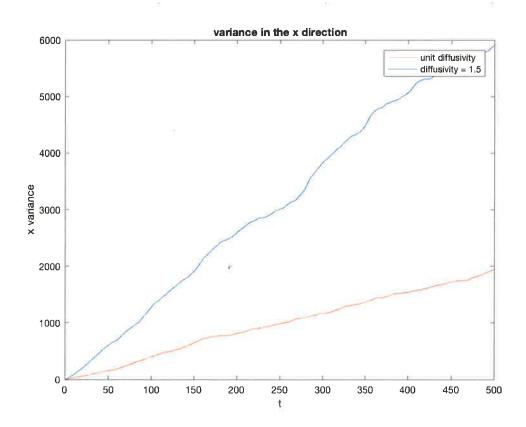
```
drawnow
end

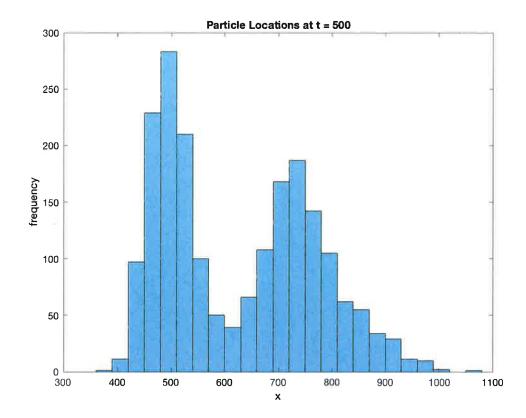
end

figure(2)
plot(t(1:i),varx(1:i),'r',t(1:i),varxa(1:i),'b')
xlabel('t')
ylabel('x variance')
title('variance in the x direction')
legend('unit diffusivity',['diffusivity = ',num2str(Dastar)])

figure(3)
histogram([x,xa])
xlabel('x')
ylabel('frequency')
title(['Particle Locations at t = ',num2str(tquit)])
```







Conclusion

As can be seen, the variance of the distribution with the higher diffusivity is much larger (going as D^3). This actually degrades the separation significantly requiring a greater simulation time for complete separation. The scalings are correct, however. There is also considerable skewness to the distributions resulting from the shear flow.

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