PROBLEM 8.44

Miren - A smooth pipe designed to carry chile oil (D=47 in)
p= 1.75 sing/ft = and u= 4x10-4 lbf. 5/ft 2 is to be modeled with a smooth pipe 4 in in deameter carrying water (T=60°F). If the mean velocity in the putotype is 2 ft/s, what should be the mean velocity of the lake in the model to sensure dynamically similar conditions?

Cruce oil 7 D= 47in Vp= 2 At/5 P= 1.75 Slugs/B+3 U= 4x.10-4 lbf.5/8+2 water T= GOF P= 1.94 slugs/8+ 5 D= 4 in. n= 2.73*10-5 lbf.5/8+2

Find > mean relocity of the water in the model, Vm

Dynamically Miniliar model and prototype

Reynolds number equation

Re=Vdp

Rem = Rep -) Vndmpm = Vpdppp um up

=) Vm = Vp (dp) (Pp) (um)

= Units in ft = Dp= 47-in/18t = 3.92 ft

Dm = 4 in / 1ft = , 333 ft

=) Vm = 2 ft | 3.92 ft | 1.75 slags | ft 3 | 2.73 e-5 lbfs | ft 2 5 | .353 ft | ft 3 | 1.94 slags | ft = | 4e-4 16f-5

3/Vm = 1.45 #

Discussion -> The model and the prototype have different finds so they have different third properties. To calculate the velocity In the matel the Reynold's humbers have to match. Setting the Reynolds number for the model equal to the Reynolds number for the purtotype 1ets us put the given traid properties into the equation to solve for the velocity in the model. PROBLEM 8. Cece

Mirer & Flow around a bridge pier is studied using a model 1/12 scale, when the velocity in the model is .9 m/s, the strating wave at the pier hose is observed to be 2.5 cm in height.

what are the corresponding values of Lebour and wave height in the prototype?

model-8 Vm=.9 m/s Em= 2.5 cm 1/12 scale

Find = velocity of the putotype - wave height of the putotype.

Solution > Unny France number matching >> Frp = Frm

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=> Vp = Vm [[Lp]

Since soule is in Im= in Lp => 12 Lm= Lp

put into equation > Vp = Vm [\[\sqrt{12Lm}] = Vm \sqrt{12}

Vp= .9 m | Via => [Vp=5.12 m/s]

12 Lm = Lp =) 12(2,5 cm) = Lp

=) [Lp = 30 cm

Discussion - Open channel from almost always uses Fronce number watching. By setting Fro equal to Frm, we can input the given midel and scale factor data to solve for both the velocity and were height of the prototype.

PROBLEM 8.77

Miver > Experiments ove performed to measure pressure clop

IN apple with autor at 20°C and could oil cut the

Same temperature bata was gathered with pipes of a diameters

5 cm and 10 cm. The data obtained is shown on the

tubles on the next page.

Preciure chop per unit length is assumed to be a function

of pipe diameter, lequid density, viscosity, and velocity.

PC = f(p, u, V, D)

Find > Diminstral analysis to Obtain IT groups, plot the results using

Solution Dimensional analysis

$$J = \frac{kq}{ms} \qquad W = \frac{N \cdot s}{m^2} = \frac{kq \cdot m}{s^2} \frac{|s|}{|s|} = \frac{kq}{s \cdot m}$$

$$V = \frac{m}{s} \qquad D = m.$$

$$\frac{\Delta P}{L} = \frac{Kg}{m^3} = \frac{Kg}{S^2 m^2} = \frac{Kg}{S^2 m^2}$$

$$\frac{\Delta P}{L} = \frac{Kg}{S^2 m^2} = \frac{Kg}{M} = \frac{Kg}{M}$$

=) Ap = chwerrin less.

70 VD = chressintess - regional number

a) plot death using excellent data tobles given.

Diviension less pressure drap

Reynolas #

Fixed tubles of Calculated and given Values on next page.

Piscussion of When the data is reduced to dimensionless parameters, the function of 15 obtained by passing a curve through the data. This curve eventually populates design publications

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|----------|---------------------------------------|----------------------------|---------------|----------------|--|-------------|-------------------------------|--|-------------------|--------------|----------|
| - | Α | В | С | | D | | E | T | F | | G |
| 1 | | r Fluid Propertie | | | <u> </u> | | | _ | | | |
| 2 | density= | 998.2 | _ | /m3 | <u> </u> | | | | | | |
| 3 | viscosity= | 1.00E-03 | P | a s | ļ | | | \perp | | | |
| 5 | | | <u> </u> | | <u> </u> | | | 4 | | | |
| _ | | | <u> </u> | | | | | \perp | _ | | |
| 6 | | Crude Oil Fluid Properties | | | | | ļ <u></u> | | | | |
| 7 | density= | 900 | _ | m3 | | | | \perp | | | |
| 8 | viscosity= | 2.00E-02 | Pa | 3 5 | | | | 1 | | | |
| 9 | 144-4 | | ┼ | | <u> </u> | | | \perp | | | |
| 10 | Water | | | | <u> </u> | | | | | | |
| 11 | | Given | | | | | | Calculated | | | |
| 12 | Pipe Diameter | Pipe Diameter | Velo | city | Pressure Drop | | Dimensionless | , | | | |
| 14 | | | <u> </u> | _ | | | Pressure Drop | 1 | Vumbe | er_ | |
| 15 | cm | m | $\frac{m}{s}$ | - | $\frac{N}{m}$ | <u>'</u> | $\frac{\Delta pD}{L\rho V^2}$ | | PVD | | |
| 16 | r | 0.05 | | | | | | ╄ | μ | _ | |
| 17 | 5 | 0.05 0.05 | | <u>1</u> | | 210 | | - | 4.98E | | |
| 18 | 5 | 0.05 | | <u>_</u> 2 | | 730 3750 | | +- | 9.96E | _ | |
| 19 | 10 | 0.03 | - | $-\frac{3}{1}$ | | 3/30 | | | 2.49E- | _ | |
| 20 | 10 | 0.1 | | 2 | | 320 | | - | 1.99E- | | |
| 21 | 10 | 0.1 | | 5 | | 1650 | | _ | 4.98E- | _ | |
| 22 | | | | | | | | | | | |
| 23 | Crude Oil | | | | | | | \top | | \dashv | |
| 24 | | Given | | | | | Calcul | Calculated | | - | |
| 25 | 0: | | | | | | Dimensionless | | Reynolds | | |
| 26 | Pipe Diameter | Pipe Diameter | Velo | city | Pressur | e Drop | Pressure Drop | | lumbe | | |
| 27 | | | m | | N | | | | ρVD | 一 | |
| 28 | cm | m | _ _ | | m^3 | 1 | $\frac{\Delta pD}{L\rho V^2}$ | | $\frac{\mu}{\mu}$ | ŀ | |
| 29 | 5 | 0.05 | | 1 | | 310 | | | 2.25E+ | -03 | |
| 30 | 5 | 0.05 | | 2 | | 1040 | | _ | 4.50E+ | _ | <u> </u> |
| 31 | 5 | 0.05 | | 5 | | 5300 | 0.0118 | | 1.13E+ | _ | |
| 32 | 10 | 0.1 | | 1 | | 130 | | | 4.50E+ | -03 | |
| 33 | 10 | 0.1 | | _2 | | 450 | | _ | 9.00E+ | _ | |
| 34 | 10 | 0.1 | | 5 | | 2210 | 0.0098 | | 2.25E+ | 04 | |
| 35 36 | | | | | | | l | <u></u> | | -↓ | |
| 3b 37 | 0.0180 | | | | | | | | | \parallel | |
| 38 | | | | | | | | | | \parallel | |
| 39 | 0.0160 | | | | | | | | | \mathbb{H} | |
| 40 | 0.0180 | | | | | 1-1-1 | | | | \mathbb{H} | |
| 41 | | | | | | | | | | \parallel | |
| 42 | 0.0140 Pressure Drop of 0.0100 | | | | | | | | | \parallel | |
| 43 | | | | | | | | | | | - |
| 44 | 1 👸 👖 | | | | | | + | - | | | |
| 45 | ်င္က 0.0120 🖥 | | | | | | | | | | |
| 46 | 를 를 | | - | | | | | | | 1 | |
| 47 48 | l sk | | | 11 | | | | 1 1 | | \parallel | |
| 48 | E 0.0100 | | | | | | | | | \parallel | |
| 50 | - | | | | | | | | | # | |
| 51 | | | | | | | | | | \mathbb{H} | |
| 52 | 0.0080 | | - | | | | | | | \mathbb{H} | |
| 53 | | | | | | | | | | \mathbb{H} | |
| 54 | 0.0050 | | | | | | | | П | \mathbb{H} | |
| 55 | 0.0060 +- 0.E+0 | 0 1.E+05 | 2.E+0 |)5 | 3.E+05 | 4 | E+05 5.E+05 | | 6.E+05 | \parallel | |
| 56 | 3.2.0 | | | | وريخي.د پnoids Nu | | 3.6705 | | u.E+U3 | | |
| 57 | E 201 | | | | , | | | | | | |
| 58 | All Expe | eriments 📮 Wate | r 🛮 | Crud | le Oil | Power | Law Model All Exi | oerim | ents | * | |
| 59 | | | | 1 | | | | | | _[| |
| 60 | | | | 1 | | | | | | ĺ | |