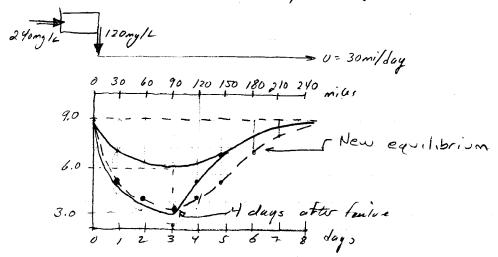
Raw sewage BOD = 240 mg/L sent to plant that achieves 50% removal. Effluent produces Dxygen say curve shown.



a) Assume plant fails, draw new DO say curve after long time (equilibrium)

Only change in equation is value of Lo, He ultimate BOD. It essentially doubles. Therefore D(x) is doubled.

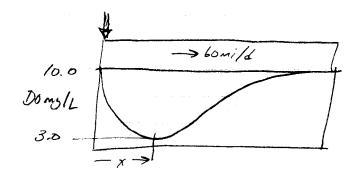
b) shelp ID say come ofter only 4 days.

- day 5 & beyond no change lupset has not arrived yet)

-days I -3 are probably near new equilibrium.

-day 4 is between dat new equilibrium.

Lood processing plant. Do sage 3mg/L occurs downstream of plant as stown



kr = 0.8/1 k = 0.2/1

a) by what % should BOD of wastes be reduced to achieve D=5.0 mg/L everywhere?

from sketch we observe that Do = 0

$$D = \frac{k_0 L_0}{k_r - k_d} \left(e^{-k_0 x/U} - e^{-k_r x/U} \right)$$

$$\frac{\chi_{e}}{U} = \frac{1}{k_{e} - k_{e}} l_{n} \left\{ \frac{k_{r}}{k_{a}} \left(1 - \frac{D_{o}(k_{r} - k_{a})}{k_{a} L_{o}} \right) = \frac{1}{0.8 - 0.2} l_{n} \left(\frac{b.8}{0.2} \right) = 2.3 l day.$$

$$D(\chi_c) = 7.0 mg/L = \frac{(0.2)(L_0)}{(0.6)} \left(e^{-0.2(2.31)} - e^{-0.8(2.31)}\right)$$

Goal is to reduce D(xe) from 7.0 mg/L to 5.0 mg/L

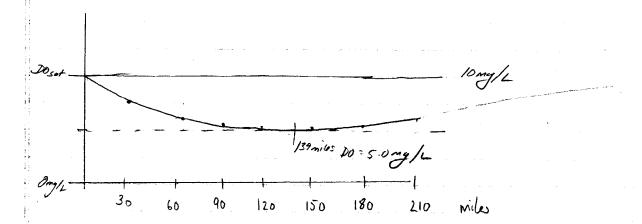
4/2

Will a primary plant achieve this reducken? Cannot answer based on information in text.

- b) Whene does longst DO occur?

 Le = 2.31 days Ke = V. 2.31 day = 60 mily 2.31 day = 138.6 miles
- e) Already calculated to = 31.7 mg/L for 5.0 mg/L DO.

d) Shetch the Do curve



	Waste	River	
2	0.3	0,9	m3/5
40	6.4	7.0	ng/L
Do.	1.0	6.0	mg/L
kd		6.2	day-1
kr		0.37	day -1
U		0.65	m/5
Dosat	8.0	8.0	

$$D = \frac{k_a h_0}{k_r - k_a} \left(e^{-k_a \times l_0} - e^{-k_r \times l_0} \right) + D_0 e^{-k_r \times l_0}$$

Do (initial deficit) of mixture

Now find
$$\frac{\chi_e}{U} = \frac{1}{k_r - k_z} \ln \left(\frac{k_r}{k_d} \left(1 - \frac{D_o(k_r - k_d)}{k_z + o} \right) \right)$$

$$= \frac{1}{(0.37 - 0.2)} \ln \left(\frac{0.37}{0.2} \left(1 - \frac{3.25(0.37 - 0.2)}{0.2(6.95)} \right) \right) = 0.581 \, days$$

Now find
$$D(\chi_c) = \frac{(0.2)(6.85)}{(0.17)} \left[e^{-0.2(0.581d)} - e^{-0.37(0.581d_{eq})} \right] + 3.25 e^{-(0.32)(0.581)}$$

= 3.29mg/L

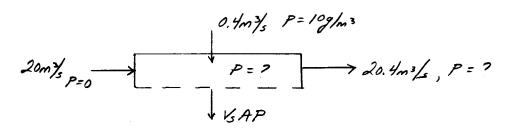
LAKE S.A. = $100.10^{6}m^{2}$.

PSOURCE 15 $0.4m^{3}/s$ @ 10mg/L ($10g/m^{3}$)

CTREAM FLOW $N = 20m^{3}/s$, P = 0.

Vs $\times 10m/yr$.

ESTIMATE P CONC.



$$\frac{1NFLON}{20(0)+0.4(10)} \frac{0UPRON}{-(10)(100\cdot10^6)P} = 0$$

$$(20.1)P$$

$$4g/\sec - (lon/yr)(\frac{1}{3656})(\frac{1}{86400sec})(loo.106m^{2})P - 20.4P = 0$$

$$4g/\sec - 31.7 \frac{m^{3}}{5ec}P - 20.4\frac{m^{3}}{5ec}P = 0$$

Solve for
$$P = \frac{49/\text{sec}}{52.1\text{m}^3/\text{sec}} = 0.07679/\text{m}^3$$

$$0.076.79/m^3 = \frac{76.7mg}{m^3} \cdot \frac{1m^3}{1000L} = \frac{0.0767mg/L}{1000L}$$

How much TREATMENT TO GET P = 0.0/mg/L? $\frac{\chi}{52.1} = 0.01 - \chi = 0.521$ $0.4(y) = 0.521 \quad y = 1.302 g/m^{3}$ % removal: $\frac{10-1.302}{100} \times 100 = 87\%$