$$RO \bullet +O_2 \to HO_2 \bullet +R'CHO \tag{7.19}$$

for R'CHO to be HCHO, R' must be H so that

$$RO \bullet +O_2 \rightarrow HO_2 \bullet +HCHO$$

for the reaction to balance, $R = CH_3$

which says RH in (7.16) must be CH₄ (methane)

7.10 RH = propene = CH_2 = CH_3 = C_3H_6 so, R = C_3H_5

so the sequence of reactions (7.16) to (7.19) are:

$$C_3H_6 + OH \bullet \rightarrow C_3H_5 \bullet + H_2O$$

$$C_3H_5 \bullet + O_2 \rightarrow C_3H_5O_2 \bullet$$

$$C_3H_5O_2 \bullet +NO \rightarrow C_3H_5O \bullet +NO_2$$

$$C_3H_5O \bullet +O_2 \rightarrow HO_2 \bullet +C_2H_3CHO$$

The end product is acrolein, CH2CHCHO.

7.11 U. S. Power plants:

heat input =
$$685 \times 10^6 \text{ tons } \times 2000 \frac{\text{lb}}{\text{ton}} \times 10,000 \frac{\text{Btu}}{\text{lb}} = 1.37 \times 10^{16} \text{Btu}$$

efficiency =
$$\frac{\text{output}}{\text{input}} = \frac{1400 \times 10^9 \text{ kWh x } 3412 \text{Btu/kWh}}{1.37 \times 10^{16} \text{Btu}} = 0.349 \approx 35\%$$

At NSPS of 0.03 lb particulates per 10⁶ Btu input, emissions would have been:

emissions =
$$\frac{0.03 \text{ lb}}{10^6 \text{Btu heat input}} \times 1.37 \times 10^{16} \text{Btu in } \times \frac{1000 \text{g}}{2.2 \text{ lb}} = 1.87 \times 10^{11} \text{g}$$

For comparison,
$$\frac{\text{emissions at NSPS}}{\text{actual emissions}} = \frac{1.87 \times 10^{11} \text{g}}{0.39 \times 10^{12}} = 0.48 = 48\%$$

7.12 Derivation for the dry adiabatic lapse rate:

$$dQ = dU + dW$$
 where $dU = C_v dt$ and $dW = PdV$

$$dQ = C_v dt + PdV \qquad (1)$$

ideal gas law says PV = nRT

so,
$$d(PV) = PdV + VdP = nRT$$

or,
$$PdV = nRT - VdP$$

plugged into (1) gives: