6.3
$$pH = 10.5$$

$$10_{3}^{2} = 39 \text{ mg/L}$$

$$Hl0_{3}^{-} = 24.5 \text{ mg/L}$$
a) Alkalining as lally (ignore H^{+} OH)
$$Alkalining = (Hl0_{3}^{-}) + (l0_{3}^{2}^{-})$$

$$24.5 \text{ mg/L} Hl0_{3}^{-} \cdot \frac{50 \cos 20 \cos 200}{61.0 \text{ mg/meg}} = 20.08 \text{ mg/L} \text{ as lally}$$

$$39 \text{ mg/L} l0_{3}^{2} - \frac{50 \cos 20 \cos 200}{61.0 \text{ mg/meg}} = 65 \text{ mg/L} \text{ as lally}$$

$$Alk = 85 \text{ mg/L} \text{ as lally}$$

$$Alk = 85 \text{ mg/L} \text{ as lally}$$

$$4lk = 85 \text{ mg/L} \text{ as lally}$$

$$10 \text{ mol/L} \cdot \frac{1000 \text{ mg/meg}}{1 \text{ mol}} = 1.58.10 \text{ mg/L} \text{ as lally}$$

$$1.58.10 \text{ mg/L} \text{ as lally}$$

$$1.58.10 \text{ mg/L} \text{ as lally}$$

$$1.58.10 \text{ mg/L} \text{ as lally}$$

041 = 10 -3.5 mol/ - 17000mg - 50 Calos = 15.81 mg/L as la Co3

Total Alk = 85.08 + 15.81+ 1.58.10-6 = 100.89 mg/L aslaCo.

 Ca^{2+} 90 | 224.1 | C1 - 120 | 169.2 | 156.24 | 169.2 | 156.24 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.2 | 169.26.4 Chemical Analysis of Water myle myle-lates PH = 7.5 OH 0.0158 H+ 0.00158 Xmg/L as lally = Xmy/L 50. M Conv. factors e/-: 50(1) = 1.41 $l_{a}^{2+}: \frac{50(2)}{40.1} = 2.49$ So_{4}^{2} : $\frac{50(2)}{96} = 1.04$ $m_g^{2+}: \frac{50(2)}{24.3} = 4.11$

 $\begin{array}{lll} \ell_{a}^{2+} : & \frac{50(2)}{40.1} = 2.49 & \ell / & \frac{50(2)}{35.5} = 1.11 \\ M_{g}^{2+} : & \frac{50(2)}{24.3} = 4.11 & So_{g}^{2-} : & \frac{50(2)}{96} = 1.04 \\ N_{a}^{+} : & \frac{50(1)}{23} = 2.17 & So_{g}^{(1)} = 0.82 \\ K^{+} : & \frac{50(1)}{39.1} = 1.28 & HCO_{3}^{-} : & \frac{50(1)}{61} = 0.82 \end{array}$

a) A/kalini5 = 135.3+0+0.0158-0.00158=/35.314

135-3 = 135-3 =

b) Hardress = 224.1 + 123.3 = 347.4 $347 \text{ as } laCO_3 = 347.4$

c) TDS = 708 mg/L

$$Ca^{2+}40.0$$
 | 99.6 $H603^{-}$ | 110 mg/L | 90.2 $Mg^{2+}10.0$ | 41.1 $S0g^{2-}$ | 67.2 | 69.88 Na^{+} ? | $C1^{-}$ | 11.0 | 15.57 K^{+} | 7.0 | 8.96

Elations = 99.6 + 41.1 + 8.96 + ? = 149.66 my/L as la CO3 Etnicus = 90.2 + 69.88 + 15.51 = 175.59 mg/L as la 203 .. Net = 25.93 my/L as lalo3

(a)
$$Ne^{+}*2.17 = 25.93$$

 $Na^{+} = \frac{25.93}{2.17} = 11.95 \text{ mg/L}$

b)
$$TH = Ca^{+} + Mg^{+} = 99.6 + 41.1 = 140.7 \text{ mg/L as } Ca^{+}C03$$

$$99.6 \qquad 140.7 \qquad 166.63 \qquad 175.59 \qquad mg/L$$

$$Ca^{+} \qquad mg^{+} + Na^{+} \qquad K^{+} \qquad as \ Ca^{+}C03$$

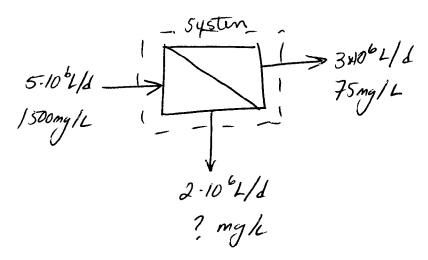
$$HCO_{3}^{-} \qquad 504^{2} - \qquad C1^{-}$$

$$90.2 \qquad 160.88 \qquad 175.59$$

RO plant heats 5-106L/day heednate 1500mg/L TDS.

Produces 3.106L/d product water at 75 mg/L TDS

What is concentrate in reject stream?



Simple muss balance $\int_{1.1}^{0} c$ intow - outflow = accomplation

(5-10kg)(1500my/L) - (3-106/L)(75my/L) - (2.106/L)(x my/L) = 0

(5olve for x

 $\frac{(5.10^6)(1500) - (3.10^6)(75)}{(2.10^6)} = x = 367 3637.5 \text{ my/L}$

Settling tank 2MOD plant. Overflow rate 800g/d-ft2 Minimum HRT 2.0 hrs. Min depth = 11tt.

Size He circular trak.

$$HRT = \frac{V}{Q}$$

A
$$Q_{OU}$$

A Q_{OU}
 $A = \pi D^2$
 $A = \pi D^2$

$$A = \pi D^{2}$$

$$H = Ah = \frac{\pi D^{2}h}{4}$$

Convert Q into 43/1

2.10 6 gal.
$$\frac{1}{7.48 \text{ gal}} = 267,379.7 \text{ ft}^3/\text{day}$$

Also in ft3/hr

trequired to meet HPT criterion

MRT criterian.

A regured to meet onether rate

$$800 \text{gal} = \frac{Q}{A} : A = \frac{Q}{800}$$
$$= \frac{2.10^{6}}{800} = 2500 \text{ ft}^{2}$$

Solve for D
$$\sqrt{\frac{4A}{17}} = D = \sqrt{\frac{4(2500)}{17}} = 56.4ft$$

Now check if morph

+= (2500ft2)(11ft) = 27,500 ft3 which is larger than trequied.

Design tank as

11 ft tall; 56.4 ft diameter for this problem.