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# Multiphase and Multicomponent Nickel-Iron Oxide Heterostructure as an Efficient Separator Modification Layer for Advanced Lithium Sulfur Batteries

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Lithium sulfur batteries (LSBs) have been seen as of considerable potential candidate for lithium-ion batteries (LIBs) to satisfy high energy density demand. However, the application of LSBs until now has been stubbornly dragged by the “shuttle effect” of lithium polysulfides (LiPSs) due to dissolution of LiPSs in electrolyte and reaction with the lithium anode, incurring a severe capacity decay. Herein, the straightforward separator modification method that multiphase and multicomponent nickel-iron oxide heterostructure grown on oxidized carbon

nanotube (NiFe<sub>2</sub>O<sub>4</sub>–NiO/OCNT) composites directly coated on the polypropylene (PP) separator, has been implemented, which effectively inhibits the migration of LiPSs, enhances the electron and lithium-ion transfer, and promotes the redox kinetics by virtue of the heterostructure interfaces between NiFe<sub>2</sub>O<sub>4</sub>, NiO, and OCNT. In conclusion, the synthesized NiFe<sub>2</sub>O<sub>4</sub>–NiO/OCNT/PP separator delivers good rate capacities and high stability up to 1000 cycles at 2 C with a low-capacity decay rate of approximately 0.065 % per cycle.

## 1. Introduction

Lithium sulfur battery (LSB) is considered as the most promising energy storage device to replace existing lithium ion battery owing to high theoretical energy density (2600 Wh kg<sup>−1</sup>) and low cost.<sup>[1–3]</sup> Nevertheless, the practical implementation of LSB is hindered by the technical issues of sulfur cathode, such as the insulating property of S and the shuttle effect of the intermediate lithium polysulfides (LiPSs).<sup>[4–6]</sup> Different methodologies have been studied to resolve these problems.<sup>[7,8]</sup> Among them, the chemical design of sulfur hosting materials, such as carbon-based materials<sup>[9]</sup> and metal oxides/carbides/nitrides/sulfides,<sup>[10–12]</sup> has been intensively investigated. Although the cathode design can enhance the sulfur utilization and suppress the LiPSs shuttle effect to the certain extent, the overall energy

density is unsatisfactory due to the portion of inactive species and the low density of porous hosting materials.<sup>[13–15]</sup> Moreover, the complicated fabrication process of cathodes also limits the industrial application.

Another promising strategy is the introduction of multifunctional coating layer onto the pristine separator, which acts as a barrier to withstand the direct penetration of soluble LiPSs. In particular, this separator modification is a facile and straightforward methodology to obstruct the overall shuttling effect in the LSB system and to minimize the addition of inactive species.<sup>[16–18]</sup> Various functional materials, such as sulfide,<sup>[19]</sup> oxide,<sup>[20]</sup> hydroxide,<sup>[21,22]</sup> carbon material,<sup>[23]</sup> and polymer,<sup>[24]</sup> have been employed as the coating layer to develop multifunctional separator. Along with the passivation of LiPS crossover, the conversion reaction of LiPS also needs to be promoted, where the heterostructured materials with multiphase and multicomponent are expected to greatly improve the LiPSs capture and sulfur utilization. It notes that the heterostructured materials possess abundant interfacial active sites and high electrical conductivity, which ensure the smooth trapping-diffusion-conversion of LiPSs and the fast electron transfer.<sup>[25–27]</sup> In this regard, various of metal compound-based heterostructures, such as nitrides,<sup>[28,29]</sup> sulfides,<sup>[30]</sup> and oxides,<sup>[31,32]</sup> have been extensively exploited as the sulfur hosts, while rarely employed as coating layer for separator modification. Moreover, the heterostructured materials composed of multicomponent and multiphase bimetallic oxides have yet to be explored.

Herein, we demonstrate a multiphase and multicomponent nickel-iron oxide heterostructure tightly attached with oxidized carbon nanotube (NiFe<sub>2</sub>O<sub>4</sub>–NiO/OCNT) for the design of multifunctional modified separator. The NiFe<sub>2</sub>O<sub>4</sub>–NiO/OCNT-modified functional separator could efficiently adsorb LiPSs and promote the redox kinetics of the conversion reactions as confirmed by spectroscopic, electrochemical, and operando

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analyses. Consequently, LSB with  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT}$ -modified separator could deliver a high specific capacity of  $1350.16 \text{ mAh g}^{-1}$  at 0.1 C and a low capacity decay rate of 0.065 % per cycle over 1000 cycles at 2 C.

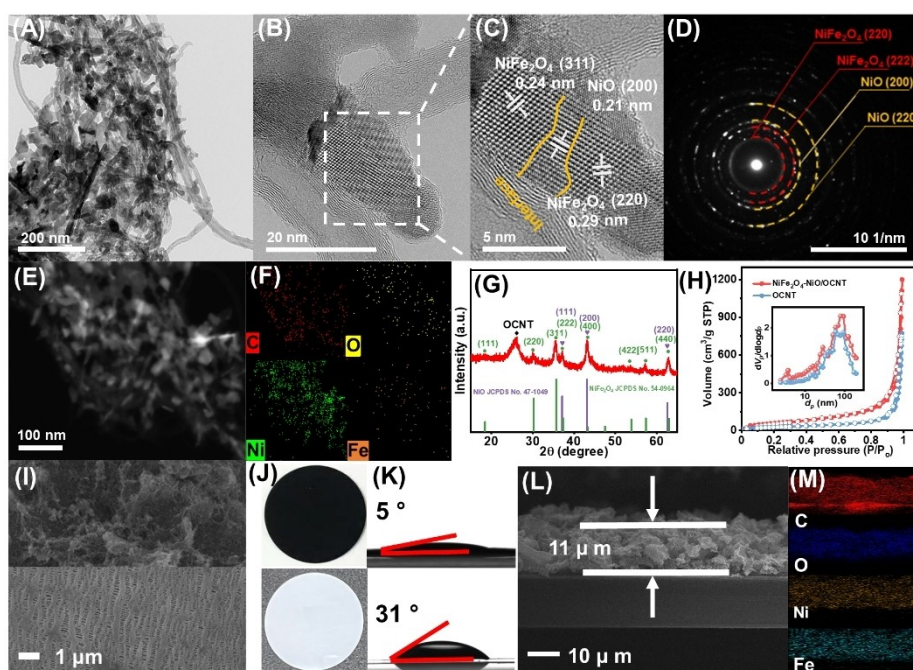
## 2. Results and Discussion

The  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT}$  nanocomposites were synthesized via a flexible calcination of NiFe-layered double hydroxide/OCNT ( $\text{NiFe-LDH/OCNT}$ ) prepared by single-step hydrothermal method (see Experimental Section). As shown in Figures 1(A) and S1,  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT}$  nanocomposites presented a reticulation structure incorporated with numerous discrete tiny-slices and grains with the size of 20–40 nm, which was observed through transmission electron microscopy (TEM). The magnified TEM image (Figure 1B) showed clear crystal lattices of  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT}$  nanocomposites. Furthermore, the lattice fringes of 0.24, 0.29, and 0.21 nm, corresponding to the (311), (220) planes of  $\text{NiFe}_2\text{O}_4$  and (200) plane of NiO, could be seen in the high-resolution TEM (HR-TEM) image (Figure 1C), expounding the characteristic crystalline and interfaces of the  $\text{NiFe}_2\text{O}_4\text{--NiO}$ . The interlaced dots and ring patterns, representing the (220), (311), (400) facets of  $\text{NiFe}_2\text{O}_4$  and (111), (200) facets of NiO, respectively, were shown in the selected area electron diffraction (SAED) pattern (Figure 1D). Energy dispersive X-ray (EDX) mapping indicated the constituent of  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT}$  heterostructures, proving a homogenous distribution of C, O, Ni, and Fe elements tightly combined with OCNT walls all over the entire detected area (Figure 1E and F). In contrast, aimed at interphase influence study, the composites prepared by

$\text{NiFe}_2\text{O}_4$ , NiO (see Supporting Information), and OCNT in a physical blend method showed a non-uniform distribution of  $\text{NiFe}_2\text{O}_4$  and NiO particles (Figures S2–S4).

The X-ray diffraction (XRD) pattern analysis further confirmed the crystallographic and microstructure for the  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT}$  composites. In Figure 1(G), a typical diffraction peak of OCNT was captured at  $26.3^\circ$ . In addition, very strong peaks located at  $18.2^\circ$ ,  $30.2^\circ$ ,  $35.6^\circ$ ,  $37.0^\circ$ ,  $43.1^\circ$ ,  $53.7^\circ$ ,  $57.3^\circ$ , and  $62.8^\circ$ , corresponding to the (111), (200), (311), (222), (400), (422), (511), and (440) lattice planes of  $\text{NiFe}_2\text{O}_4$  spinel phase (JCPDS 54-0964), respectively, were observed. Moreover, the peaks were at  $37.25^\circ$ ,  $43.28^\circ$ , and  $62.88^\circ$ , ascribed to (111), (200), and (220) plane of cubic phase NiO (JCPDS 47-1049), as verified by the HR-TEM and SAED results. The  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT}$  composites featured a large specific surface area of  $219.21 \text{ m}^2 \text{ g}^{-1}$  with multi-porous adsorption, as analyzed by the  $\text{N}_2$  sorption/desorption isotherm with a type IV performance (Figure 1H and Table S1). The mesoporous structure, which was attributed to the hysteresis of the isotherm, provided abundant active sites and transporting channels to accelerate the redox kinetics of the LiPSs.

The  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT}$  composites were well coated onto the PP surface through a vacuum filtration process, forming the modified  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT/PP}$  separator (Figure S5). Compared with bare PP surface, the modified separator was uniformly and fully coated by  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT}$  composites, as revealed by the top-view SEM image and optical photographs (Figure 1I and J). It was worth mentioning that the hydrophilicity of PP surface can be improved via the  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT}$  coating layers (Figure 1K). A thickness of  $\sim 11 \mu\text{m}$  of the homogeneous  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT}$  composites



**Figure 1.** A, B) TEM images, C) HR-TEM image, D) SAED pattern, E) STEM image and F) EDX mapping images, and G) XRD pattern of  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT}$ . H)  $\text{N}_2$  adsorption-desorption curves of  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT}$  and OCNT. I) SEM images, J) optical photographs, and K) contact angle images of  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT/PP}$  separator (top) and OCNT/PP separator (down). L) Cross-sectional SEM image and M) EDX mapping images of  $\text{NiFe}_2\text{O}_4\text{--NiO/OCNT/PP}$  separator.

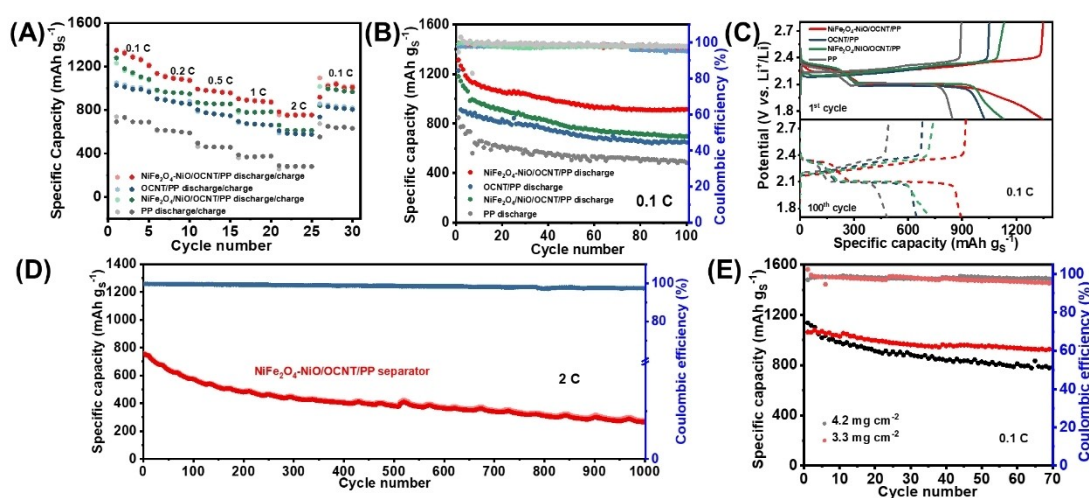
layer was further measured by means of cross-sectional SEM image (Figure 1L). EDX mapping of the cross-sectional  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  image further proved homogeneous coverage of the modified layer around the PP surface (Figure 1M). Taken together, the features of mesoporous structure and high wettability of  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  are beneficial for the penetration and transportation of Li ions across the as-modified separator and the contact with active sites during the redox reaction, further improving the electrochemical performance of the LSB cells.

The electrochemical performance of the LSB cells with different separators were evaluated by assembling the 2032-type coin cells with Li foil as anodes and MWCNT/S composites (76 wt% sulfur content, Figure S6) as cathodes. According to different separators involved, the as-assembled coin cells were denoted as  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$ , OCNT/PP,  $\text{NiFe}_2\text{O}_4\text{/NiO/OCNT/PP}$ , and PP cells, respectively. In view of the rate performance evaluated in Figure 2(A),  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cell showed much higher discharging capacities than that of the OCNT/PP and PP cells.  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cell delivered the specific discharging capacities of 1350.2, 1136.1, 991.8, 902.6, and 781.7  $\text{mAh g}^{-1}$  at 0.1, 0.2, 0.5, 1.0, and 2.0 C, respectively. In obvious comparison, the specific capacities of the OCNT/PP cell were rapidly dropped from 1026.5  $\text{mAh g}^{-1}$  (0.1 C) to 608.5  $\text{mAh g}^{-1}$  (2.0 C). The  $\text{NiFe}_2\text{O}_4\text{/NiO/OCNT/PP}$  cell was situated between OCNT/PP cell and  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cell in electrochemical performance due to interphase absence between  $\text{NiFe}_2\text{O}_4$ , NiO, and OCNT. Let alone PP cell, the capacities are changed from 691.4  $\text{mAh g}^{-1}$  (0.1 C) to 287.0  $\text{mAh g}^{-1}$  (2.0 C). Notably, the reversible capacity could be retained at 1007.0  $\text{mAh g}^{-1}$  after resting of current density to 0.1 C. The ratios of the low plateau region discharge capacity ( $Q_L$ ) and the high plateau region discharge capacity ( $Q_H$ ) were further estimated according to the discharge-charge profiles (Figure S7).<sup>[33]</sup> As displayed in Figure S8, the values of the  $Q_L/Q_H$  ratios for the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cell were much higher

than those of the contrast samples at different C rate from 0.1 to 2.0 C, disclosing the reversible redox kinetics and the limited diffusion of LiPSs with  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  modified layer. In addition, in Figure 2(B and C), the cycling performance of  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cell at 0.1 C showed a higher initial discharge capacity of 1312  $\text{mAh g}^{-1}$  and a better cyclic stability of 915  $\text{mAh g}^{-1}$  after 100 cycles. By contrast, the reference samples of OCNT/PP,  $\text{NiFe}_2\text{O}_4\text{/NiO/OCNT/PP}$ , and PP cells showed relatively inferior specific capacities of 648, 697, and 482  $\text{mAh g}^{-1}$ , respectively. Meanwhile, the lowest overpotential was delivered for  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cell and no big difference between initial cycle (200 mV) and 100<sup>th</sup> cycle (201 mV) with a higher Coulombic efficiency of 97.79%, profiting from good conductivity, fast electron transfer, and facile redox conversion reaction.

The long-term durability test was also carried out to reflect the reversible redox kinetics. As shown in Figure 2(D),  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cell delivered initial discharge capacities of 755  $\text{mAh g}^{-1}$  at 2 C and retained 292  $\text{mAh g}^{-1}$  after 1000 cycles with a low capacity fading rate of 0.065% per cycle and a Coulombic efficiency of 99.32%. Notably, to satisfy the practical application, the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cells were further fabricated at higher sulfur loading of 3.3 and 4.2  $\text{mg cm}^{-2}$  with a lean electrolyte of 9.8  $\mu\text{L mg}^{-1}$ , which still delivered high reversible specific capacities of 935 and 783  $\text{mAh g}^{-1}$  after 70 cycles (Figure 2E). The lean electrolyte for LSB cells was also tested (Figure S9). These results indirectly provided proof for using  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  heterostructure to highly promote the redox conversion and effectively capture polysulfide in LSB system.

To further explore the absorption ability and principle of  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  to LiPSs, polysulfide adsorption experiment, UV-vis absorption measurement, and XPS test were carried out under identical conditions. As indicated in Figure S10, the stronger absorptivity of  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  was apparently observed from the color change (brown yellow to colorless).



**Figure 2.** A) The specific capacities of LSBs with  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$ , OCNT/PP,  $\text{NiFe}_2\text{O}_4\text{/NiO/OCNT/PP}$ , and PP separators at various C-rates. B) Cycling performance and C) charge-discharge curves of LSBs with  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$ , OCNT/PP,  $\text{NiFe}_2\text{O}_4\text{/NiO/OCNT/PP}$ , and PP separators at 0.1 C; D) long cycle performance of LSB with  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  separator over 1000 cycles at 2 C. E) High sulfur loading LSBs with  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  separator at 0.1 C.



The UV-vis adsorption experiments revealed that the concentration decay degree of  $\text{Li}_2\text{S}_6$  for  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  was much lower than those of OCNT and  $\text{NiFe}_2\text{O}_4\text{/NiO/OCNT}$ , as demonstrated by a peak intensity change of characteristic peak at 420 nm for  $\text{S}_6^{2-}$  species,<sup>[34,35]</sup> suggesting the strong interaction between  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  and LiPSs. Figure 3(A) showed the Fe  $2p_{3/2}$  XPS spectra of the pristine and adsorbed  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$ . The Fe  $2p_{3/2}$  spectra of the pristine  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  exhibited the two peaks at 711.27 and 723.62 eV, accorded with characteristic peaks of  $\text{Fe}^{3+}$  and shakeup satellites (designed as "sat.").<sup>[36–40]</sup> After adsorption of  $\text{Li}_2\text{S}_6$  for  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$ , the peaks of  $\text{Fe}^{3+}$  shifted to 711.56 eV. Figure 3(B) exhibited the Ni  $2p_{3/2}$  spectra of the pristine  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  with three peaks at 855.23, 857.12, and 861.81 eV, corresponding to  $\text{Ni}^{2+}$ ,  $\text{Ni}^{3+}$  and sat., respectively.<sup>[41–43]</sup> After adsorption, the peaks of  $\text{Ni}^{2+}$  and  $\text{Ni}^{3+}$  shifted to 855.44 and 857.39 eV, respectively. To further study the interaction between LiPSs and  $\text{NiFe}_2\text{O}_4\text{-NiO}$ , the separator was checked by XPS disassembled from  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cell after 100 cycles at 0.1 C. As shown in Figure 3(C and D), after cycling, the peak of  $\text{Fe}^{3+}$  shifted from 711.27 to 711.73 eV, while the  $\text{Ni}^{2+}$  and  $\text{Ni}^{3+}$  peaks shifted from 855.23 and 857.12 eV to 855.44 and 857.56 eV, respectively, which was in good agreement with the XPS results of the adsorbed experiments. The peak location variation of Fe  $2p_{3/2}$  and Ni  $2p_{3/2}$  spectra could be ascribed to the electron transfer between  $\text{Li}_2\text{S}_x$  and Fe/Ni atoms, exposing the strong polar-polar interaction between LiPSs and  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$ , thus leading to a high capacity performance of LSB.<sup>[30,44]</sup>

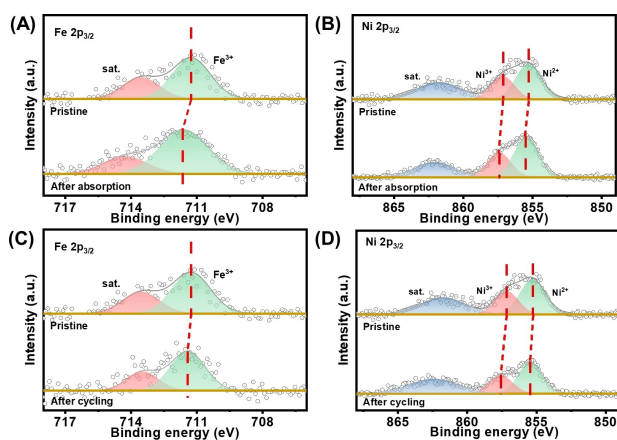
To further verify the superiority of conversion for LiPSs on the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  heterostructure surface, a simple  $\text{Li}_2\text{S}$  nucleation and precipitation experiments were conducted via potentiostatic discharge method.<sup>[45]</sup> In the experiments, Li foil,  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  pasted on aluminum foil, and  $\text{Li}_2\text{S}_8$  were used as anode, cathode, and electrolyte, respectively (see Supporting Information). As shown in Figure 4(A–C), a high  $\text{Li}_2\text{S}$  precipitation specific capacity of  $133.2 \text{ mAh g}^{-1}$  was obtained for  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  cell compared to that of OCNT

( $97.2 \text{ mAh g}^{-1}$ ) and  $\text{NiFe}_2\text{O}_4\text{/NiO/OCNT}$  ( $119.6 \text{ mAh g}^{-1}$ ) cells. The response time of peak current for  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$ ,  $\text{NiFe}_2\text{O}_4\text{/NiO/OCNT}$ , and OCNT reached 2536, 2366, and 6602 sec, respectively. However, the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  cell exhibited the highest precipitation current (0.235 mA) compared to  $\text{NiFe}_2\text{O}_4\text{/NiO/OCNT}$  (0.105 mA) and OCNT (0.0859 mA) cells, implying an enhanced conversion kinetics for  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  heterostructures toward LiPSs.

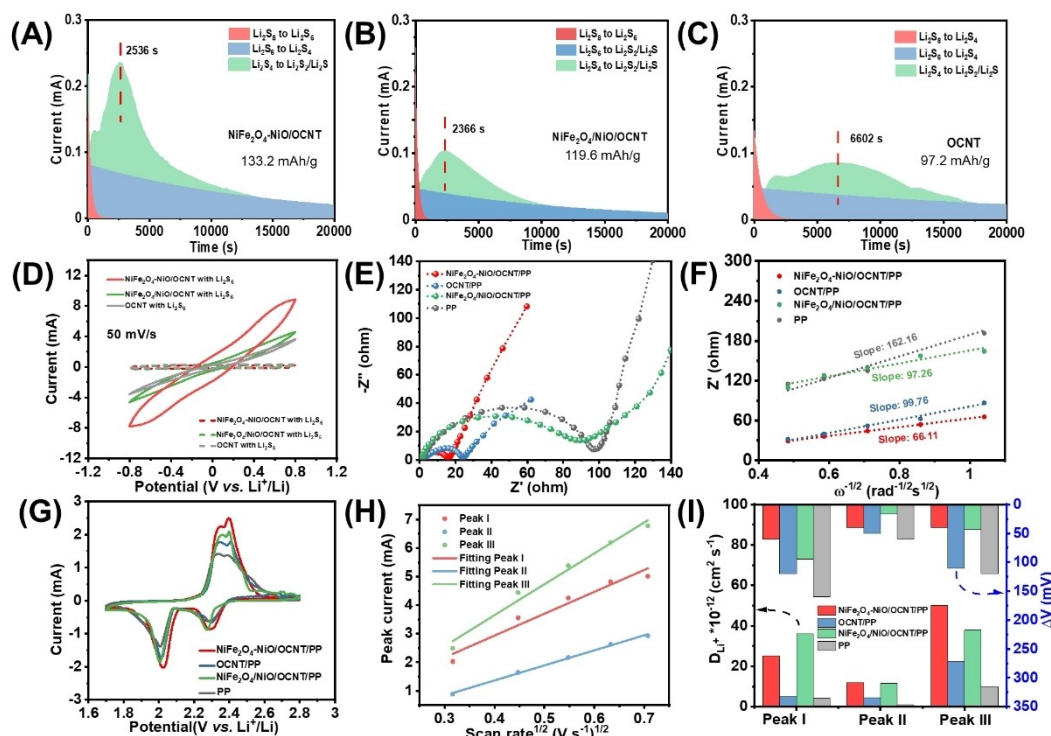
The symmetric cells were further assembled to confirm the LiPSs conversion on the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  surface (see Supporting Information). As shown in Figure 4(D), CV curves of the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  symmetric cell evidently harvested a higher current variation than OCNT and  $\text{NiFe}_2\text{O}_4\text{/NiO/OCNT}$  at scan rate of  $50 \text{ mV s}^{-1}$ , indicating the boosted redox kinetics of  $\text{Li}_2\text{S}_x$  conversion towards short-chain LiPSs.

To investigate charge and ion diffusion ability of  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  in LSB system, Nyquist curves were measured within  $10^6\text{--}10^{-1} \text{ Hz}$  range (see Supporting Information). Apparently, Figure 4(E) exhibited that the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$ , OCNT/PP, and  $\text{NiFe}_2\text{O}_4\text{/NiO/OCNT/PP}$  cells possessed suppressed semicircles in contrast with PP cell, indicative of decreased charge transfer impedance and promoted reaction kinetics. It was clear that the smaller equivalent series impedance of the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cell further stated higher electrical conductivity and faster charge transfer over the interface between heterostructure composites and LiPSs. Moreover, Figure 4(F) showed the linear relationship between the real resistance ( $Z'$ ) and frequency ( $\omega^{-1/2}$ ) for  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$ , OCNT/PP,  $\text{NiFe}_2\text{O}_4\text{/NiO/OCNT/PP}$ , and PP cells in the low-frequency range. The slope of the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cell profile was smaller than that of OCNT/PP,  $\text{NiFe}_2\text{O}_4\text{/NiO/OCNT/PP}$ , and PP cells, implying the faster  $\text{Li}^+$  ions and charge diffusion in the internal electrode,<sup>[46]</sup> which agreed with the foregoing conclusion. To prove the enhanced effect of redox kinetic with  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  heterostructures, the CV plots of three kind of LSB cells were investigated under a scan rate of  $0.1 \text{ mV s}^{-1}$ . Figure 4(G) displayed CV plots with two cathodic peaks during the discharge process, located at around 2.0 V (denoted as "peak I") and 2.3 V (denoted as "peak II"), assigned to the reduction of  $\text{S}_8$  into long-chain  $\text{Li}_2\text{S}_4$  then to  $\text{Li}_2\text{S}_2/\text{Li}_2\text{S}$ . In view of charge process, an anodic peak was located at approximately 2.4 V (denoted as "peak III"), indicating the oxidation reaction of final product to  $\text{S}_8$ .<sup>[47,48]</sup> Notably, the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cell exhibited the highest current density and much narrower peak separation compared with that of the others, disclosing a higher sulfur utilization and better conversion efficiency. In the wake of the following cycles, all the peaks of  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cell still were stable (Figure S11).

To further demonstrate the superiority of  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  heterostructures, the  $\text{Li}^+$  ion coefficients ( $D_{\text{Li}^+}$ ) were calculated via the Randles-Sevick equation (see Supporting Information).<sup>[49]</sup> As shown in Figure 4(H), the linear relationship between peak current and the square root of the scan rates was displayed, deriving from CV profiles in Figure S12. The  $D_{\text{Li}^+}$  of peak I, II, and III for the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cell were  $2.52 \times 10^{-11}$ ,  $1.19 \times 10^{-11} \text{ cm}^2 \text{ s}^{-1}$ , and  $5.02 \times 10^{-11} \text{ cm}^2 \text{ s}^{-1}$ , respec-



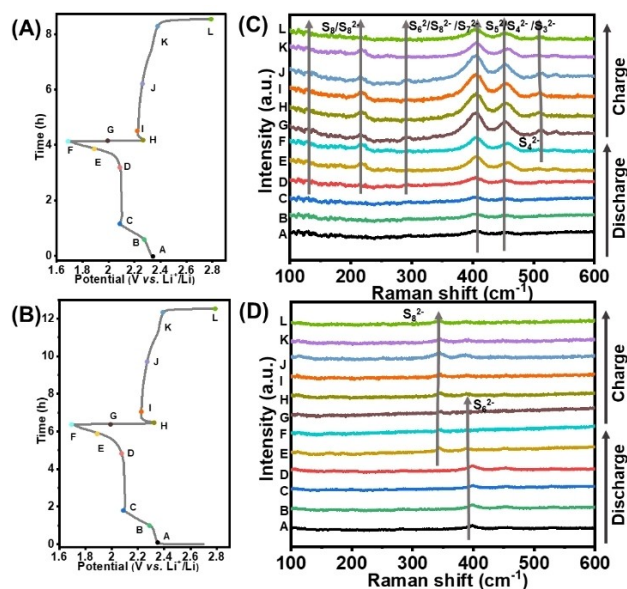
**Figure 3.** The XPS spectra of  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  hybrids A, B) with or without  $\text{Li}_2\text{S}_6$  addition: A) Fe  $2p_{3/2}$ , B) Ni  $2p_{3/2}$ , and C, D) before or after cycling: C) Fe  $2p_{3/2}$ , D) Ni  $2p_{3/2}$ .



**Figure 4.** A)  $\text{Li}_2\text{S}$  nucleation curves of cells with  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/Al}$  cathode, B)  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/Al}$ , and C)  $\text{OCNT/Al}$  cathode, and Li anode. D) CV curves of symmetric cells with  $\text{OCNT/Al}$ ,  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/Al}$ , and  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/Al}$  electrodes. E) Nyquist plots of the LSB cells with  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$ ,  $\text{OCNT/PP}$ ,  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$ , and  $\text{PP}$  separators. F) Relationship between the real part of impedance and low frequencies. G) CV curves of the LSB cells with  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$ ,  $\text{OCNT/PP}$ ,  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$ , and  $\text{PP}$  separators under scan rate of 0.1 mV/s. H) Relationship between scan rate<sup>1/2</sup> to peak current of LSB cell with  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  separator. I) Li ion diffusion coefficient (black axis) and polarized voltage (blue axis) comparison for the LSB cells with  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$ ,  $\text{OCNT/PP}$ ,  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$ , and  $\text{PP}$  separators.

tively, which relatively outperformed the others (Figures 4I and S13). Moreover, the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  cell also possessed relatively lower peak-to-peak separation ( $\Delta V$ ) for all peaks than the contrast samples, which were also calculated from the data in Figure S12. All the findings substantiate that  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  could facilitate and improve the redox kinetics due to the high conductivity, fast charge and  $\text{Li}^+$  ion diffusion.

To further demonstrate the blocking effect of the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  heterostructures for LiPSs diffusion during the actual work process of the LSB system, in-situ Raman spectroscopy was performed (Figure S14). Raman spectra were obtained from the anode side of separator at different discharge/charge potentials (Figure 5A, B). As shown in Figure 5(C), the spectra of the PP cell exhibited a faint peak at 402.3 (corresponding to  $\text{S}_6^{2-}$ ) and 451.7  $\text{cm}^{-1}$  (designed at  $\text{S}_4^{2-}$ ).<sup>[50]</sup> When the PP cell was discharged to 2.10 V, the  $\text{S}_6^{2-}$  and  $\text{S}_4^{2-}$  characteristic peak intensity became stronger, meanwhile the new peaks located at 511.85 (assigned at  $\text{S}_4^{2-}$ ) and 216.73  $\text{cm}^{-1}$  (assigned at  $\text{S}_8^{2-}$ ) were observed.<sup>[51]</sup> The intensity of polysulfides peaks further was enhanced until the discharge process ended. Following with charge process, the intensity of  $\text{S}_6^{2-}$ ,  $\text{S}_4^{2-}$ , and  $\text{S}_8^{2-}$  peaks slightly became weaker but these peaks still existed till the ending of all the charge process, demonstrating a serious LiPSs shuttle effect of PP cell. However, the polysulfides characteristic peaks were rarely observed on the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  separator surface towards anode



**Figure 5.** Voltage curves of the discharge/charge process of the LSB cells assembled with A) PP and B)  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  separators. The corresponding in-situ Raman spectra of the cells with C) PP and D)  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  separators.

side, confirming the good polysulfides adsorption ability of  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  composites, successfully inhibiting the LiPSs diffusion to anode part (Figure 5D).

### 3. Conclusions

In summary, the as-prepared multifunctional separator was composed of multiphase and multicomponent  $\text{NiFe}_2\text{O}_4\text{-NiO}$  nanocrystals tightly adhered to OCNT walls to form reticulation and cover the pristine separator. The heterostructure  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  could effectively suppress the “shuttle effect” of LiPSs, highly promote Li ion diffusion and electron transfer, and improve the conversion kinetics of LiPSs owing to unique heterostructure interfaces and good chemical/physical absorption ability. In virtue of the above structure superiority, the as-synthesized  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  separator delivered a good rate capacity up to  $1350\text{ mAh g}^{-1}$  at 0.1 C and a very low capacity decay rate of approximately 0.065% per cycle over 1000 cycles at 2 C, which offer a broad field in heterostructure application on separator modification with charming electrochemical performance for LSBs.

## Experimental Section

### Synthesis of OCNT

Commercial multiwall carbon nanotubes (MWCNTs) of 200 mg were firstly suspended into a glass flask filling with deionized water (100 mL, DI-water) to form a MWCNT dispersion. In succession, the above dispersion was sonicated for 1 h using tip sonication, then the mixture was flowed with continuous  $\text{O}_3$  gas originated from a PC-57 L model ozone generator and kept for 3 h. Next, the treated dispersion by  $\text{O}_3$  was sonicated again by means of tip sonication. The above treatment process was repeated again to get the final OCNT dispersion. To get OCNT powder, the final OCNT dispersion was washed till the pH of the filtrate shown 7 via vacuum filtration. Finally, the OCNT dispersion of 20 mL with DI-water was freeze-dried for 3 days to get OCNT powder.

### Synthesis of $\text{NiFe-LDH/OCNT}$

In a typical method, 40 mg of OCNT was added into 20 mL of N-methyl-2-pyrrolidone (NMP) solvent via sonication for 1 h to form a homogenous dispersion A. Meanwhile, 0.3 mmol of  $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ , 0.1 mmol of  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ , and 2 mmol of urea was dissolved into 20 mL of DI-water to form jade-green solution B. Then solution B was poured into dispersion A and stirred for 30 min to form mixture C. Finally, mixture C was transferred into 50-mL Teflon-line and put the line into the autoclave then heat for 6 h at  $120^\circ\text{C}$ . After heating and cooling down, the mixture was washed with DI-water for 5 times by centrifugal machine and lyophilized to get the  $\text{NiFe-LDH/OCNT}$  powder.

### Synthesis of $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$

The obtained powder of  $\text{NiFe-LDH/OCNT}$  was placed into a railboat and put into the quartz tube then heated to  $500^\circ\text{C}$  with a heating rate of  $2^\circ\text{C min}^{-1}$  for 2 h under argon atmosphere. Finally,  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  powder was achieved.

### Synthesis of $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$ modified PP separator

6 mg of  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  composites were added and dispersed into 15 mL of NMP solvent via a 1-h sonication. Moreover, polyvinylidene fluoride (PVDF) as a binder with a mass ratio of 10% was poured into the above mixture stirring for another 1 h. Next, the as-prepared  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  suspension was vacuum-filtered and covered over on PP surface (Celgard 2400). After that, the  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT}$  modified PP separator was dried for 12 h using vacuum oven at room temperature. A diameter of 19 mm of  $\text{NiFe}_2\text{O}_4\text{-NiO/OCNT/PP}$  was punched into disks with a weight loading of  $\sim 0.4\text{ mg cm}^{-2}$  for assembly of LSB cells.

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## Conflict of Interest

The authors declare no conflict of interest.

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