



**EMBRY-RIDDLE  
HYDROGEN**

# **Electrolysis and Material Storage of Hydrogen Gas**

# Team Members



Dylan Astrup  
Detail Team Lead



Hannah Spiller  
Lead Material Storage  
Engineer



Grant Carrabine  
Lead Electrolysis  
Engineer



Tesla Alford III  
Lead Extraction Engineer

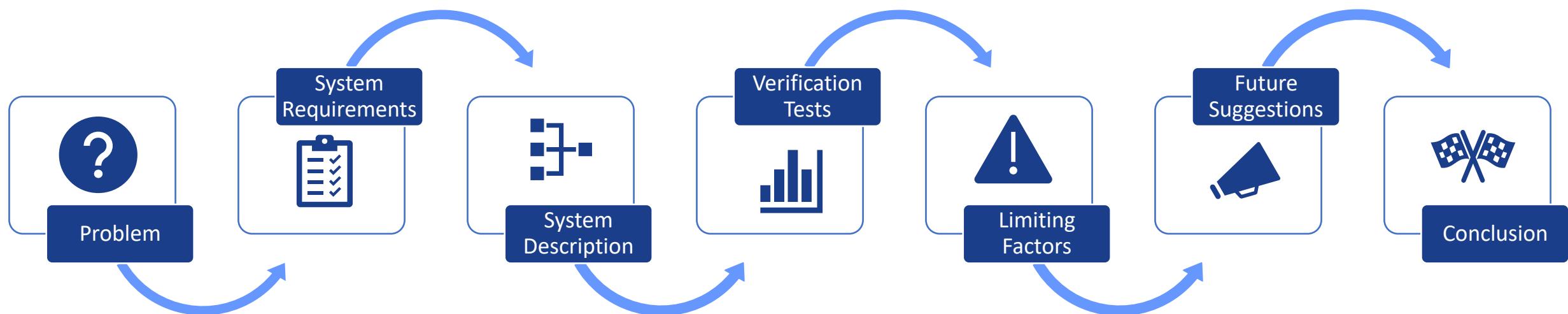


Titan Berson  
Lead Interface Engineer



Jacob Wolf  
Lead Piping Engineer

# Agenda

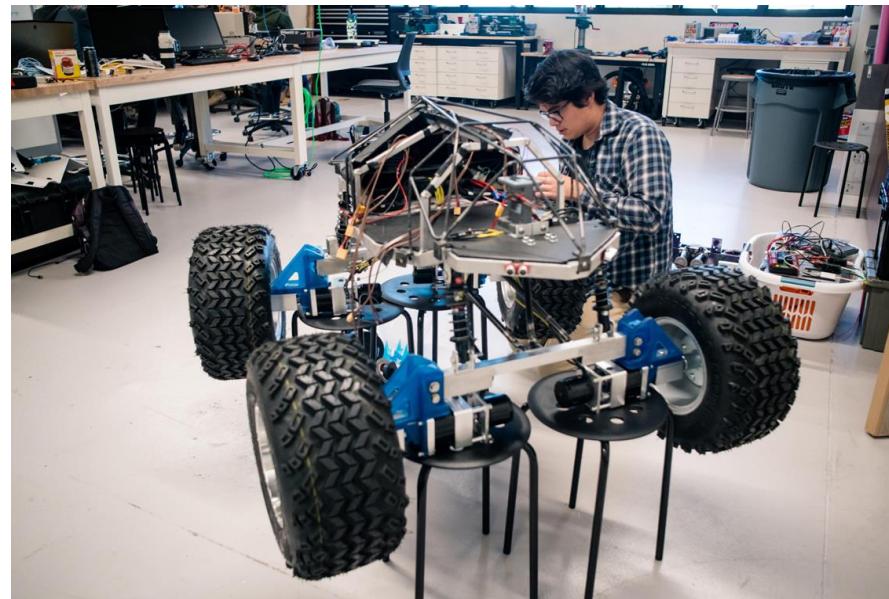




# What Embry-Riddle Has



**Wind Tunnel**



**Robotics Lab**



**Propulsion Lab**



# What Embry-Riddle Needs

Energy Labs

Viewable Demonstrations

Create Interest in the Energy Track



# Hydrogen Storage Applications

Personal Vehicles



Commercial Vehicles



Aircraft

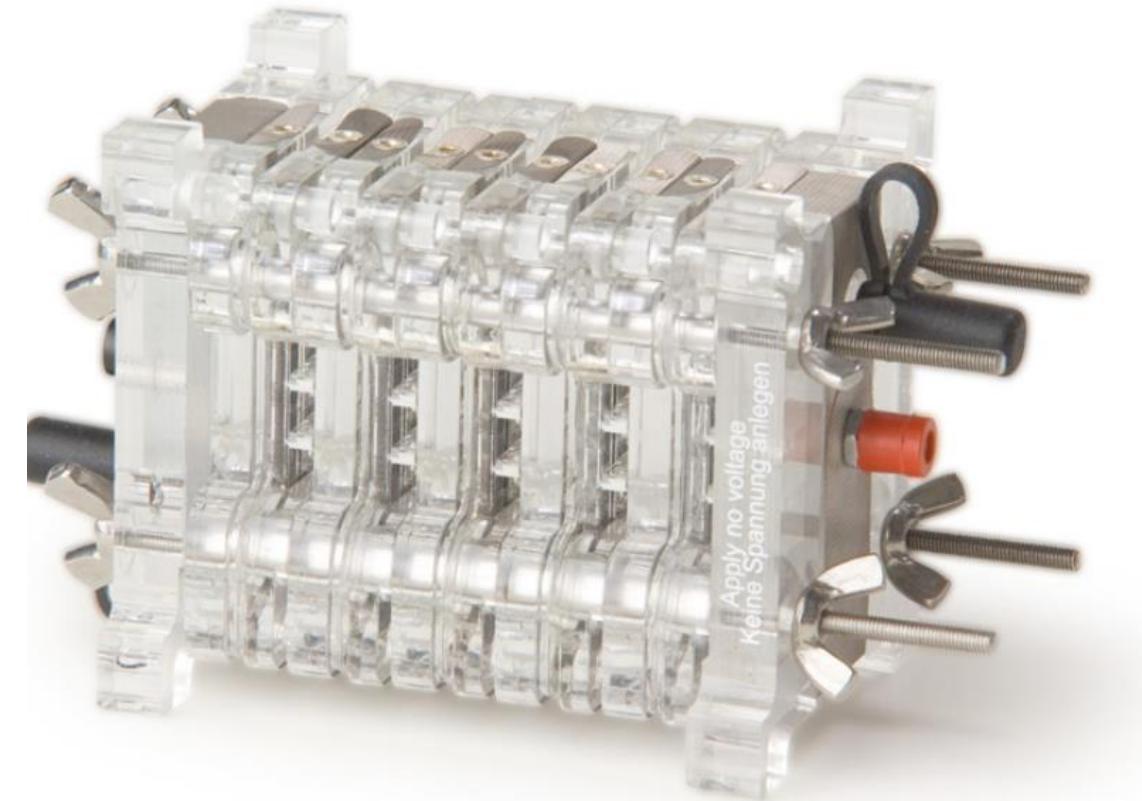


Storing hydrogen at high pressures and cryogenic temperatures is dangerous and heavy.



# Generate and Store Hydrogen

ERH2's purpose  
is to create an  
energy  
demonstrator to  
generate and  
store hydrogen.





# System Requirements

## Produce Hydrogen

*1.1.1 The system must produce enough hydrogen to get the fuel cell to steady state and then run for 10 minutes at 1 watt.*

*1.1.2 The system must be able to determine the rate of hydrogen gas produced.*

## Store Hydrogen

*1.2 The storage method must run the fuel cell for a minimum of 5 minutes.*

*1.2.1 The system must measure the amount of hydrogen stored.*

## Run Fuel Cell

*1.4 The system must interface with the Embry-Riddle fuel cell.*

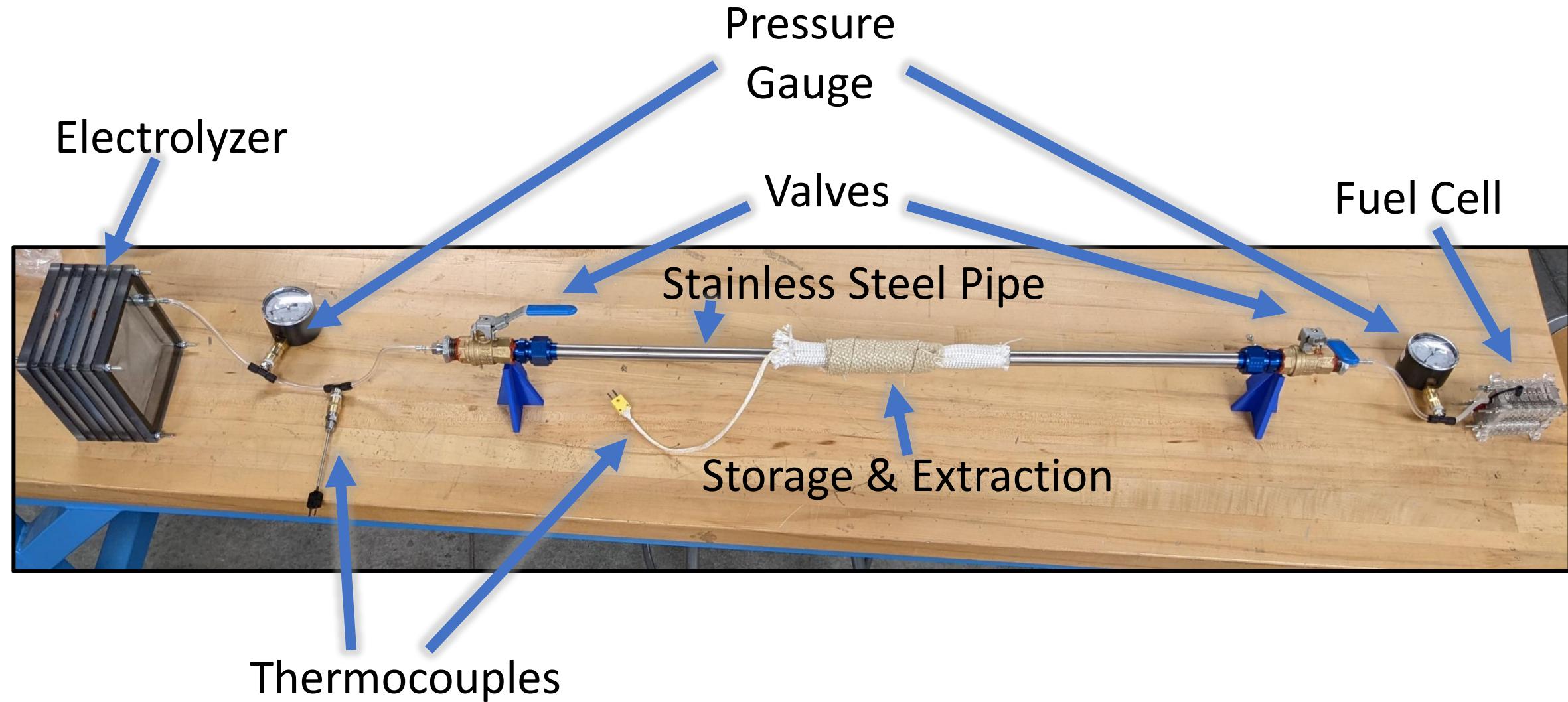
*1.4.1 The system output must be a  $\frac{1}{4}$ " PTFE tube.*



**ERH<sub>2</sub>**

# **System Description**

# ERH<sub>2</sub> System Overview

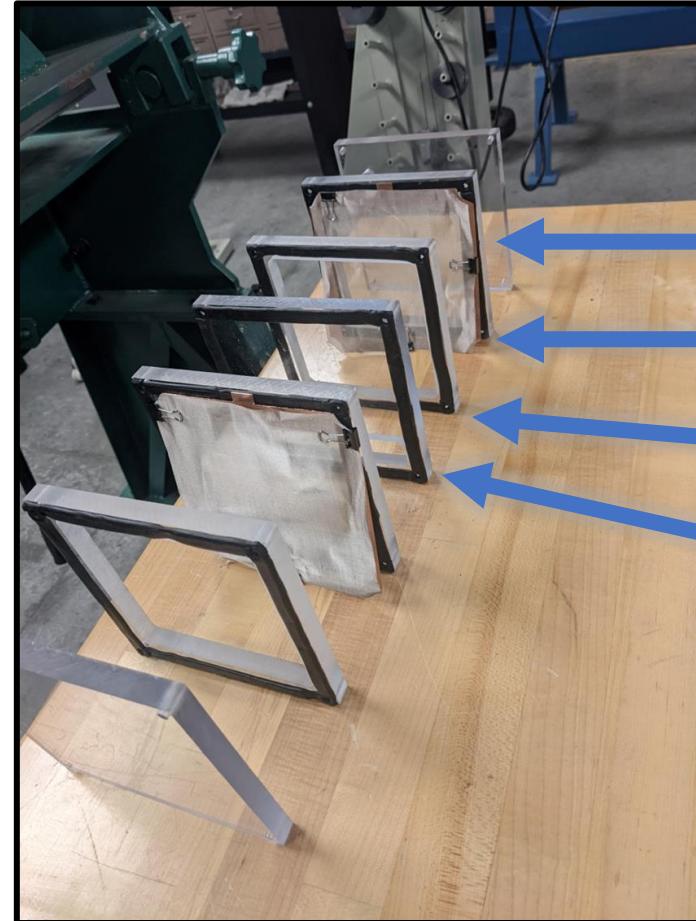


# ERH<sub>2</sub> System Overview





# Electrolyzer Exploded View



Copper Bus

Nickle Mesh

Rubber Gasket

Polycarbonate  
Spacer



# System Interfaces – Tee Fittings



J-Type Thermocouple



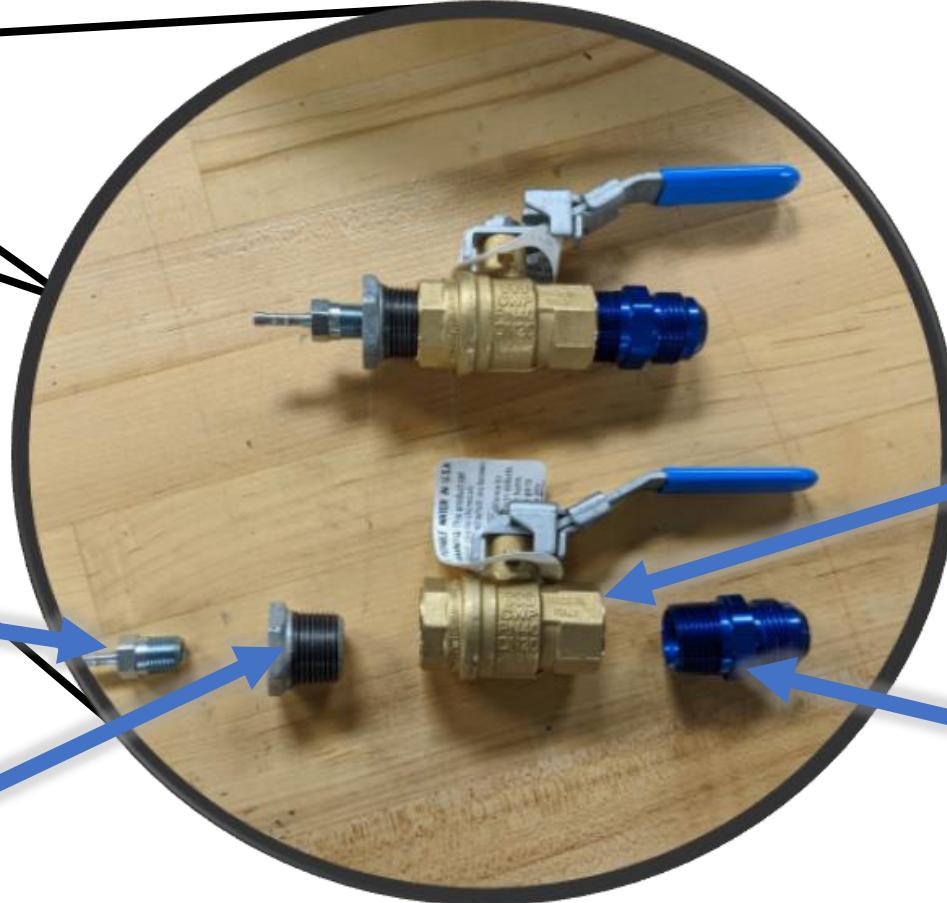
¼ NPT Female to ¼ NPT Female  
¼ OD Compression Tee to ¼ NPT



Pressure Gauge



# System Interfaces – Valve Assembly



Barbed  
Fitting

1/4 to 3/4 NPT  
Reducer

3/4 NPT Brass  
Ball Valve

3/4 NPT to  
AN Flare  
Adaptor

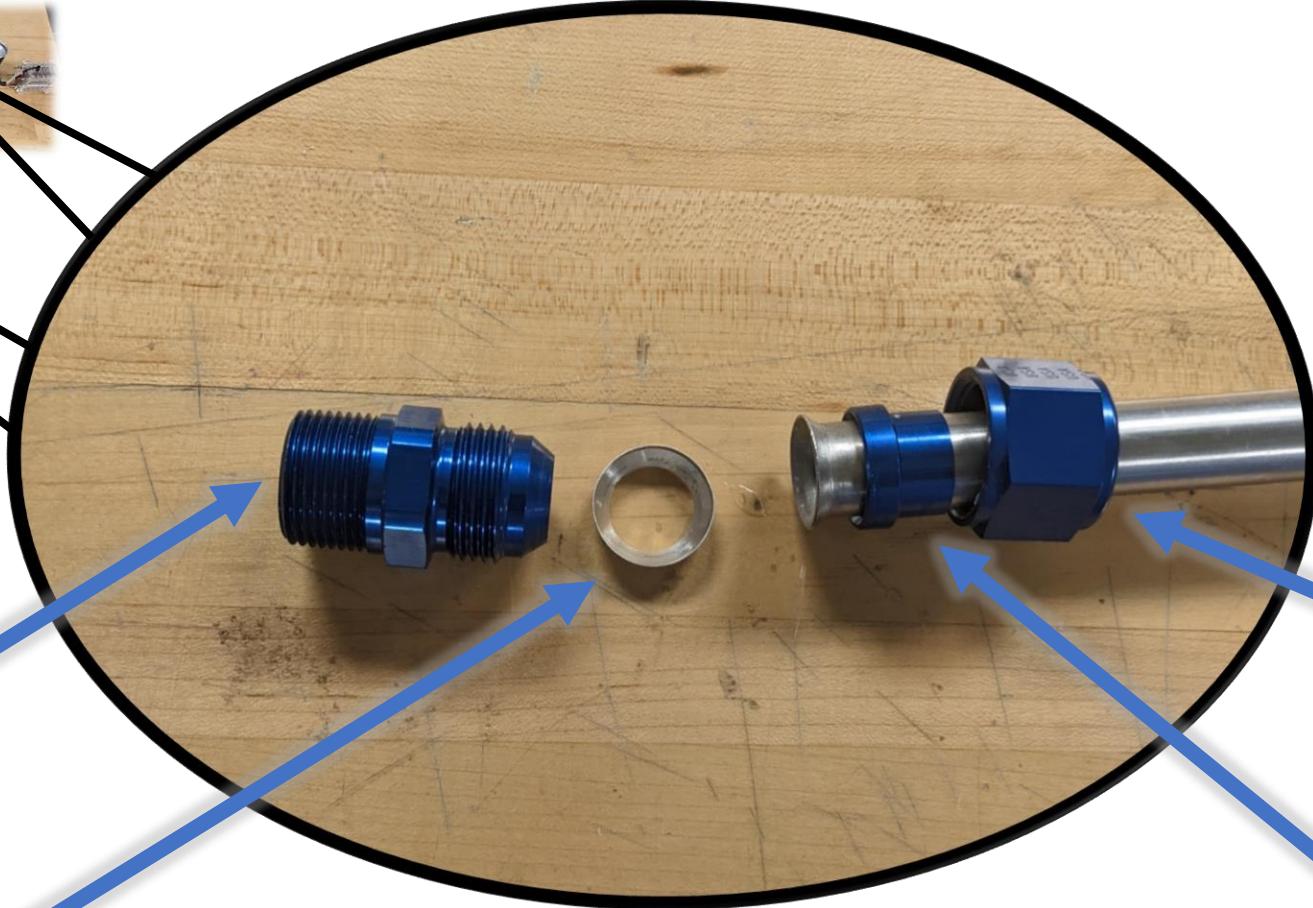
# System Interfaces – Pipe Assembly



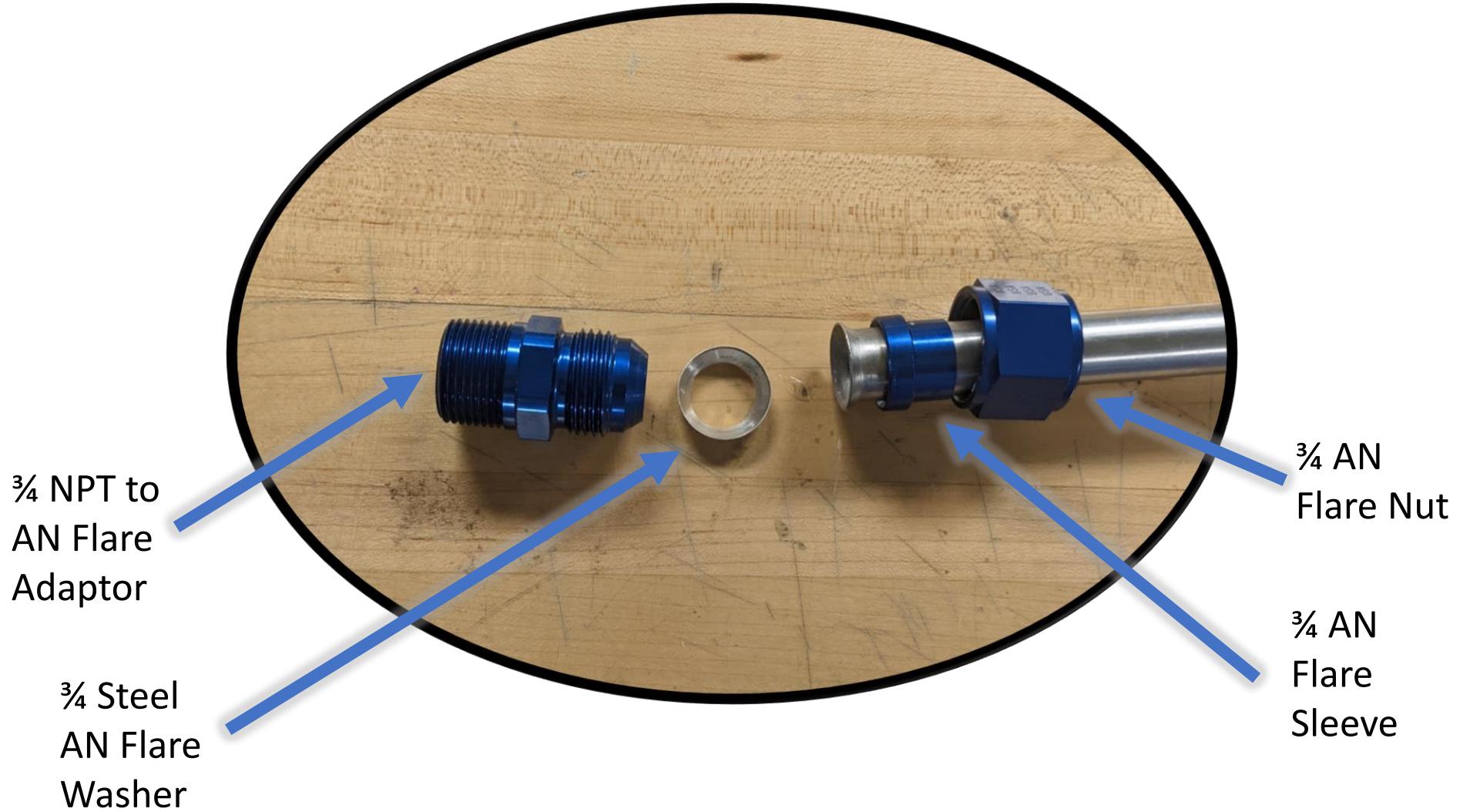
$\frac{3}{4}$  NPT to  
AN Flare  
Adaptor

$\frac{3}{4}$  Steel  
AN Flare  
Washer

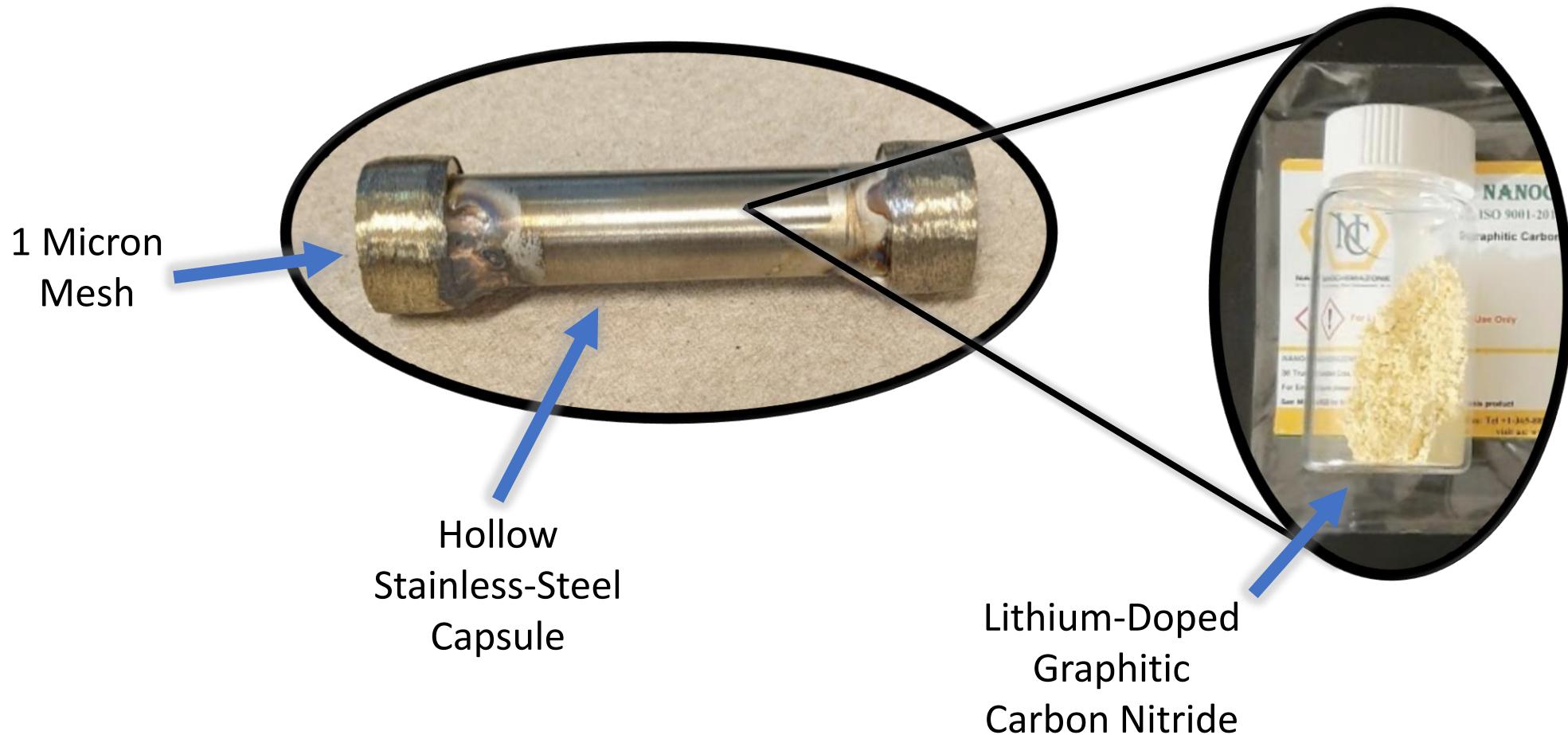
$\frac{3}{4}$  AN  
Flare Nut  
 $\frac{3}{4}$  AN  
Flare  
Sleeve



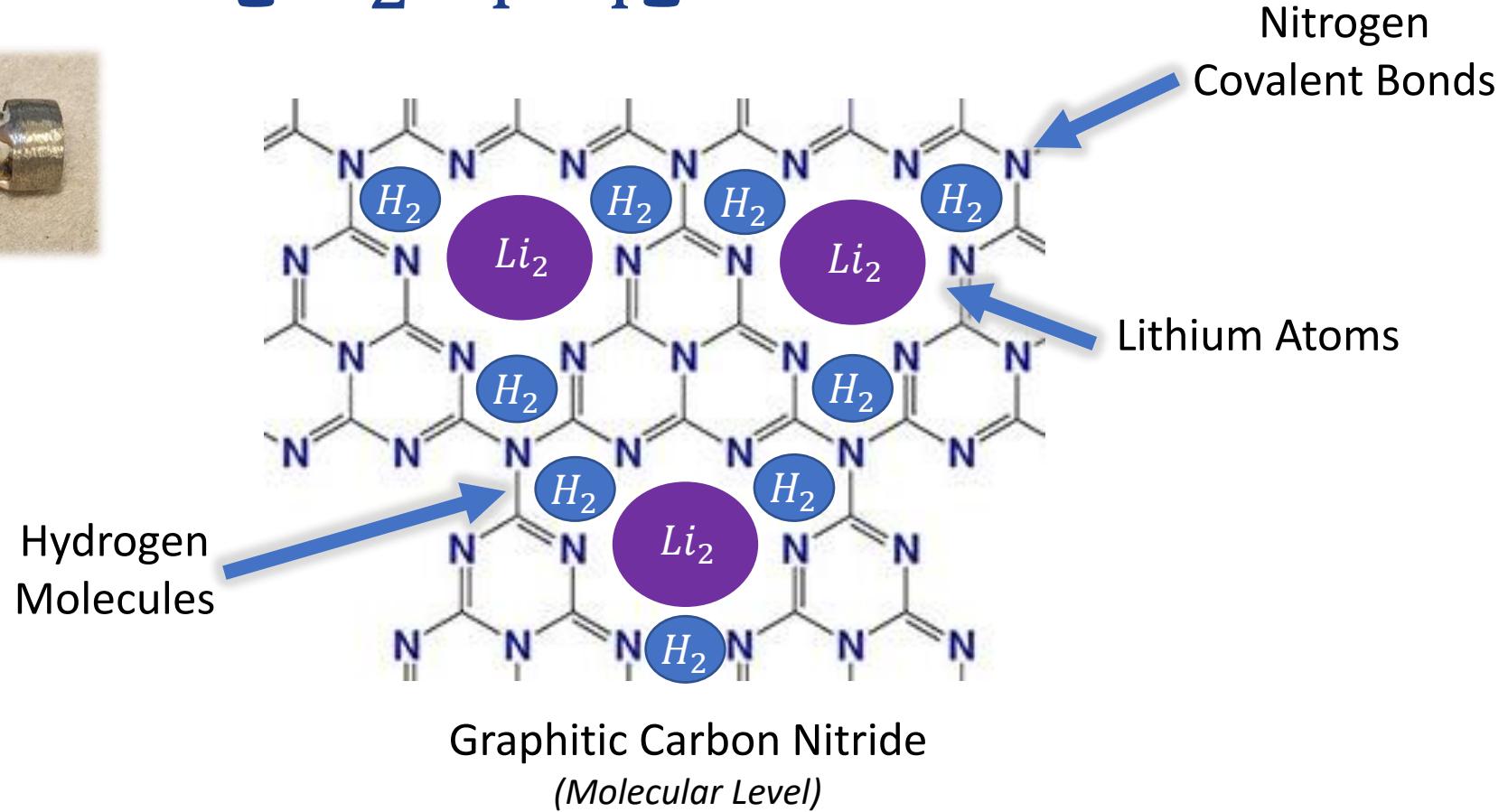
# System Interfaces – Pipe Assembly



# Material Storage



# Lithium-Doped Graphitic Carbon Nitride [Li<sub>2</sub>C<sub>4</sub>N<sub>4</sub>]

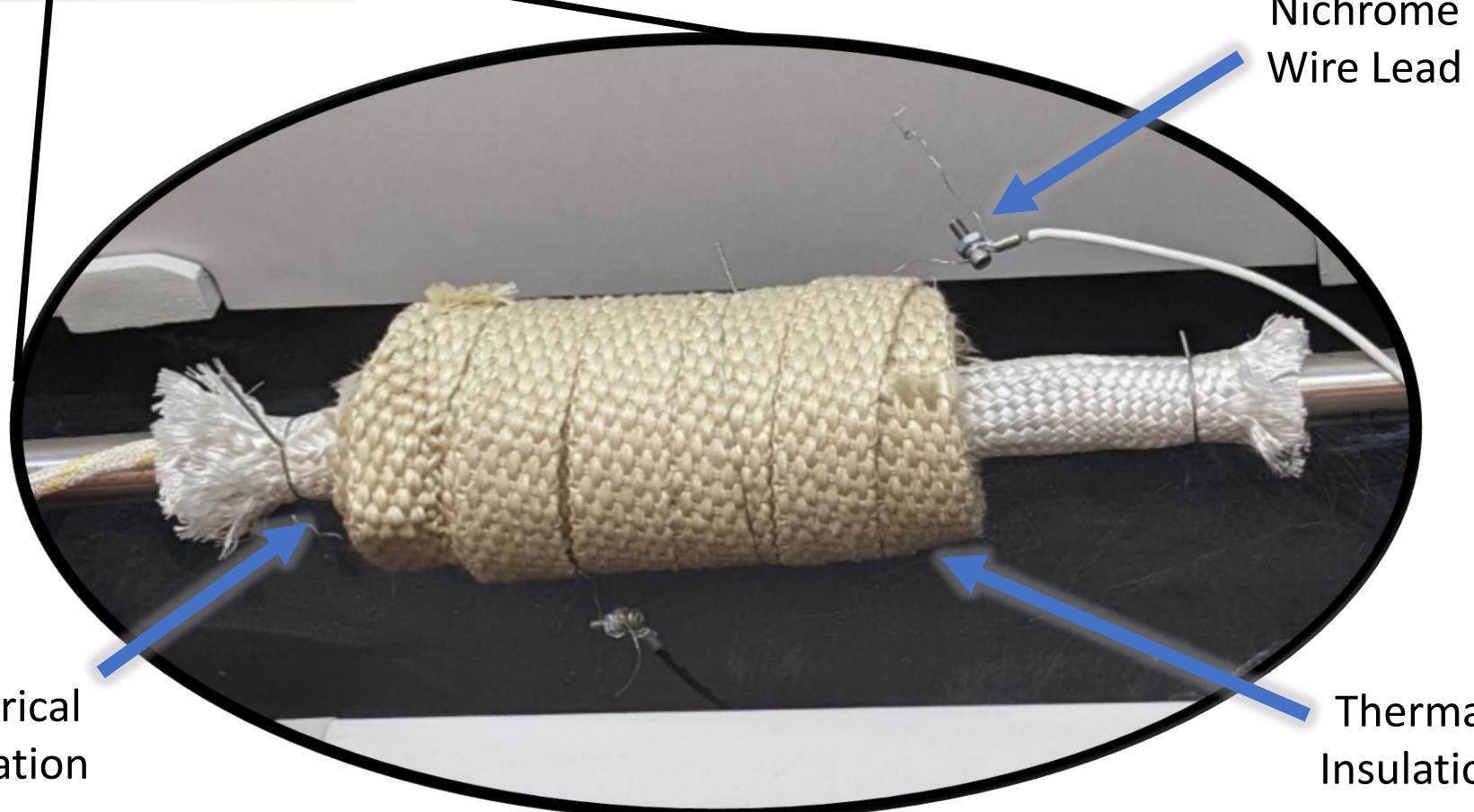


300°C will break the bonds to allow the hydrogen to escape.





# Extraction Zone

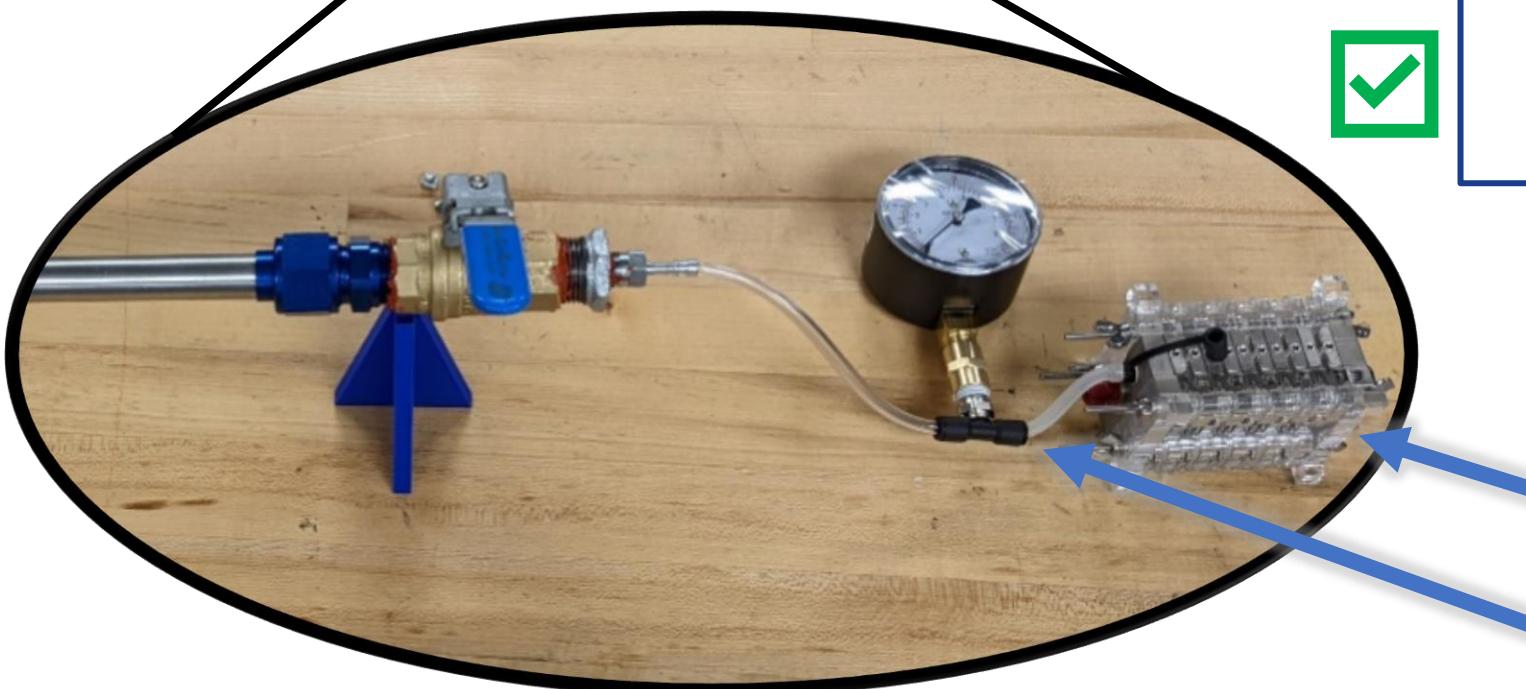


Electrical  
Insulation

Nichrome  
Wire Lead

Thermal  
Insulation

# Fuel Cell Integration



*Requirement 1.4*

"The system must interface with the Embry-Riddle fuel cell."



*Requirement 1.4.1*

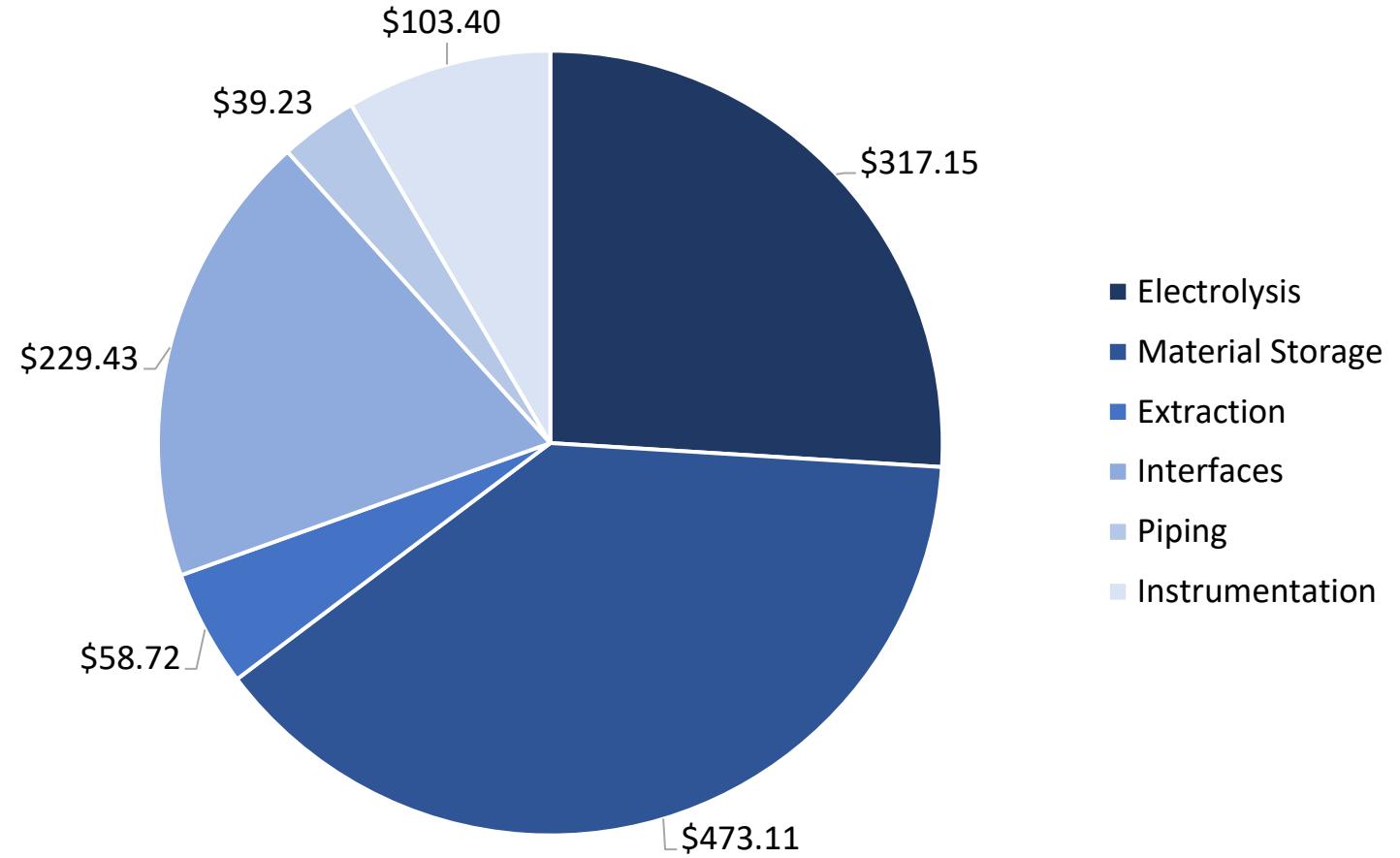
"The system output must be a  $\frac{1}{4}$ " PTFE tube."



# Budget

Total:  
\$1221.04

\$78.96 under  
budget



- Electrolysis
- Material Storage
- Extraction
- Interfaces
- Piping
- Instrumentation



# Concept of Operations

1 Weigh material storage capsule

2 Load capsule into pipe with rod

3 Attach valve assembly onto pipe

4 Turn on electrolysis and flush pipe until light turns on

5 Close exit valve to begin loading material storage

6 Run electrolysis until pressure gauge reads maximum pressure



# Concept of Operations

7 Turn off electrolysis, disconnect pipe from valve, remove and weigh the capsule

8 Reinsert capsule into pipe using loading rod

9 Turn on electrolysis and flush pipe until light turns on

10 Let fuel cell light turn off, close both valves and turn on heating element

11 Once at 300°C, slowly open exit valve to power fuel cell

# Concept of Operations

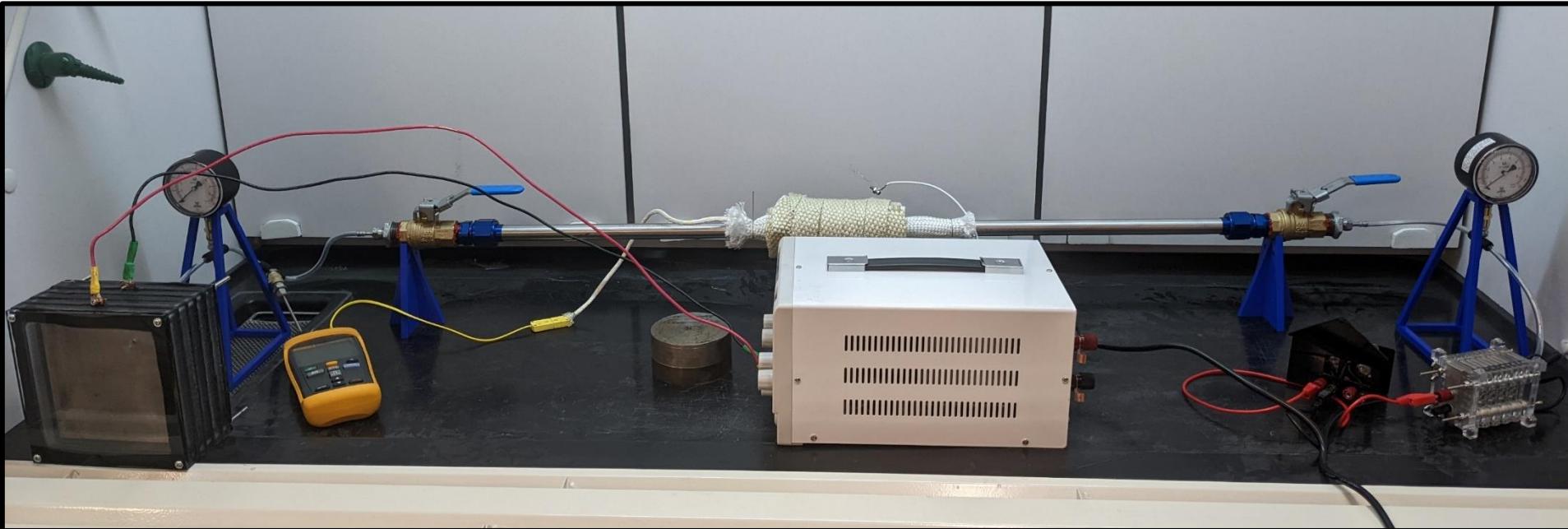




# Concept of Operations

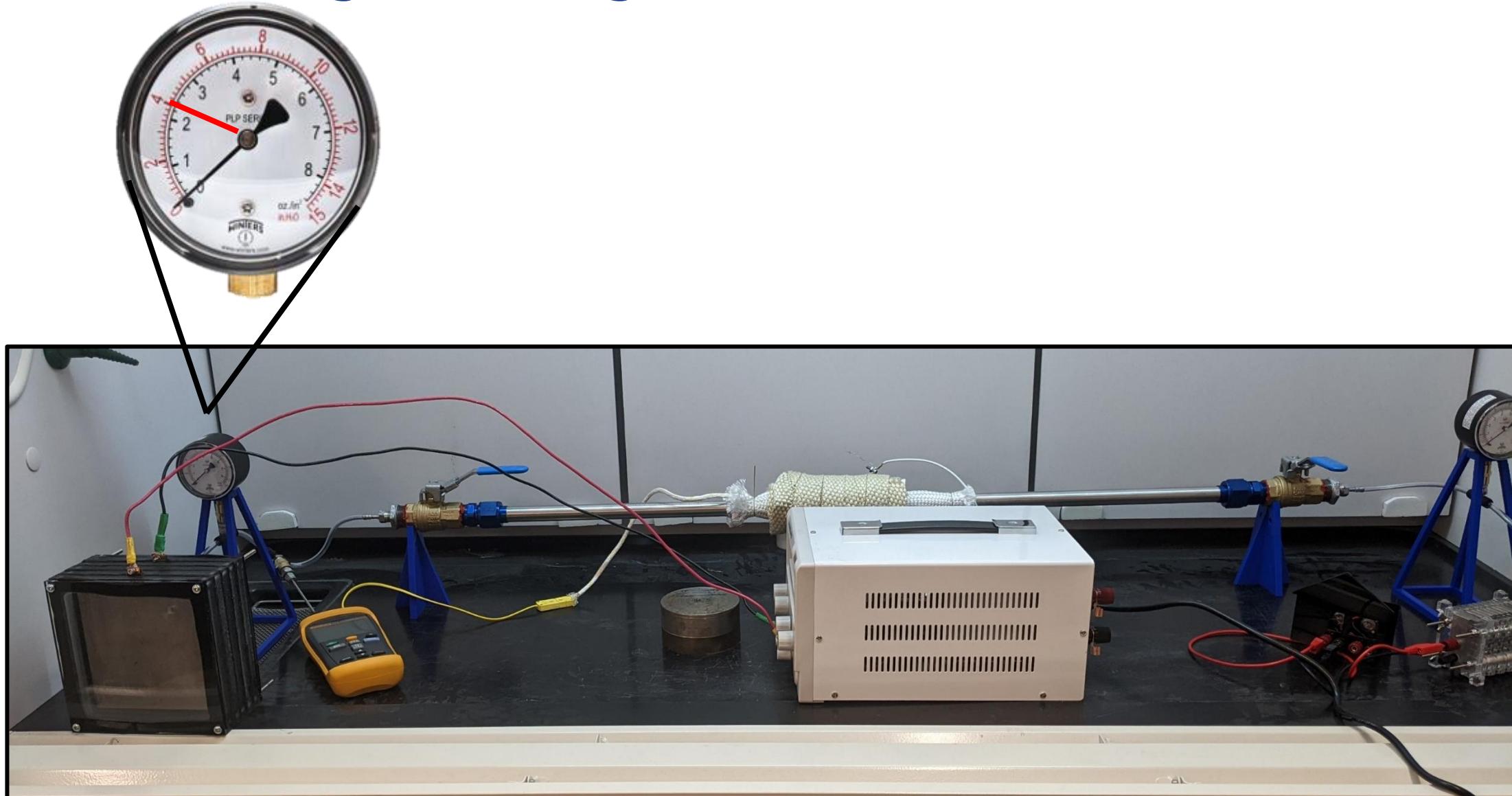
Step 3: Reattach interfaces, ensure all valves are open.

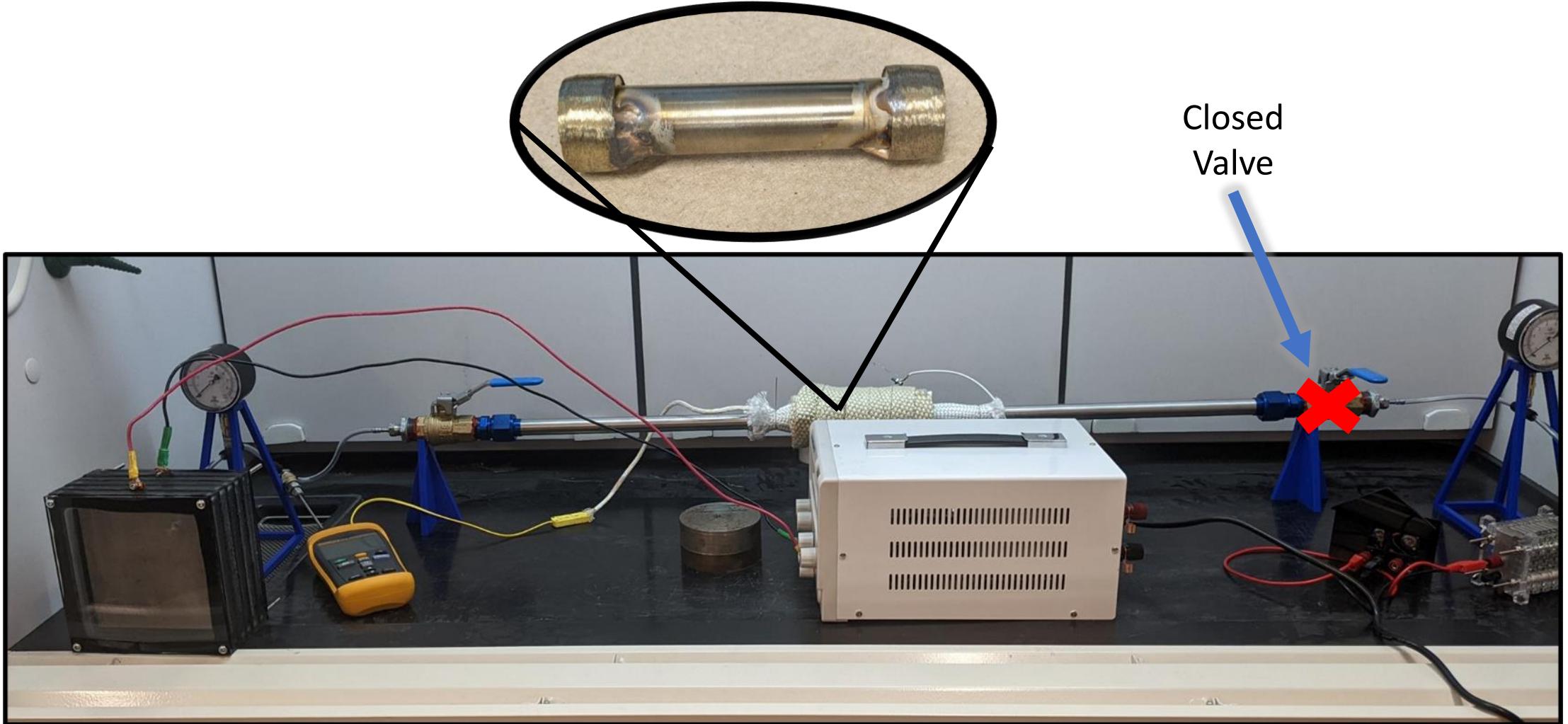
Step 4: Turn on the electrolyzer and run until the fuel cell light turns on.





# Concept of Operations







# Concept of Operations

Step 7: Turn off electrolyzer, disconnect pipe from valve, remove capsule, and weigh again.

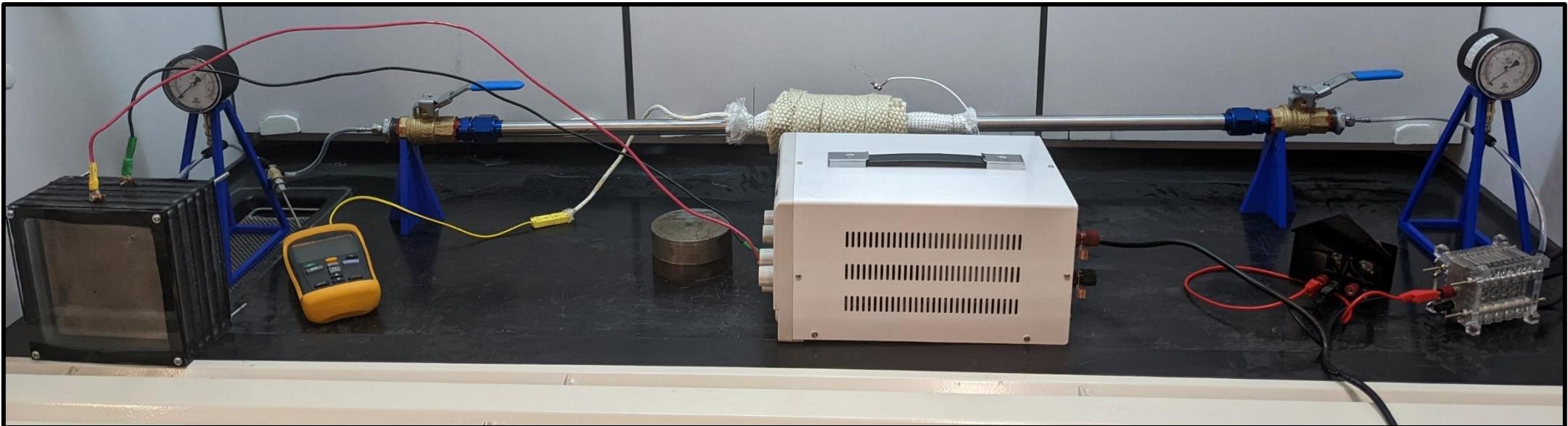




# Concept of Operations

Step 8: Reload capsule into pipe.

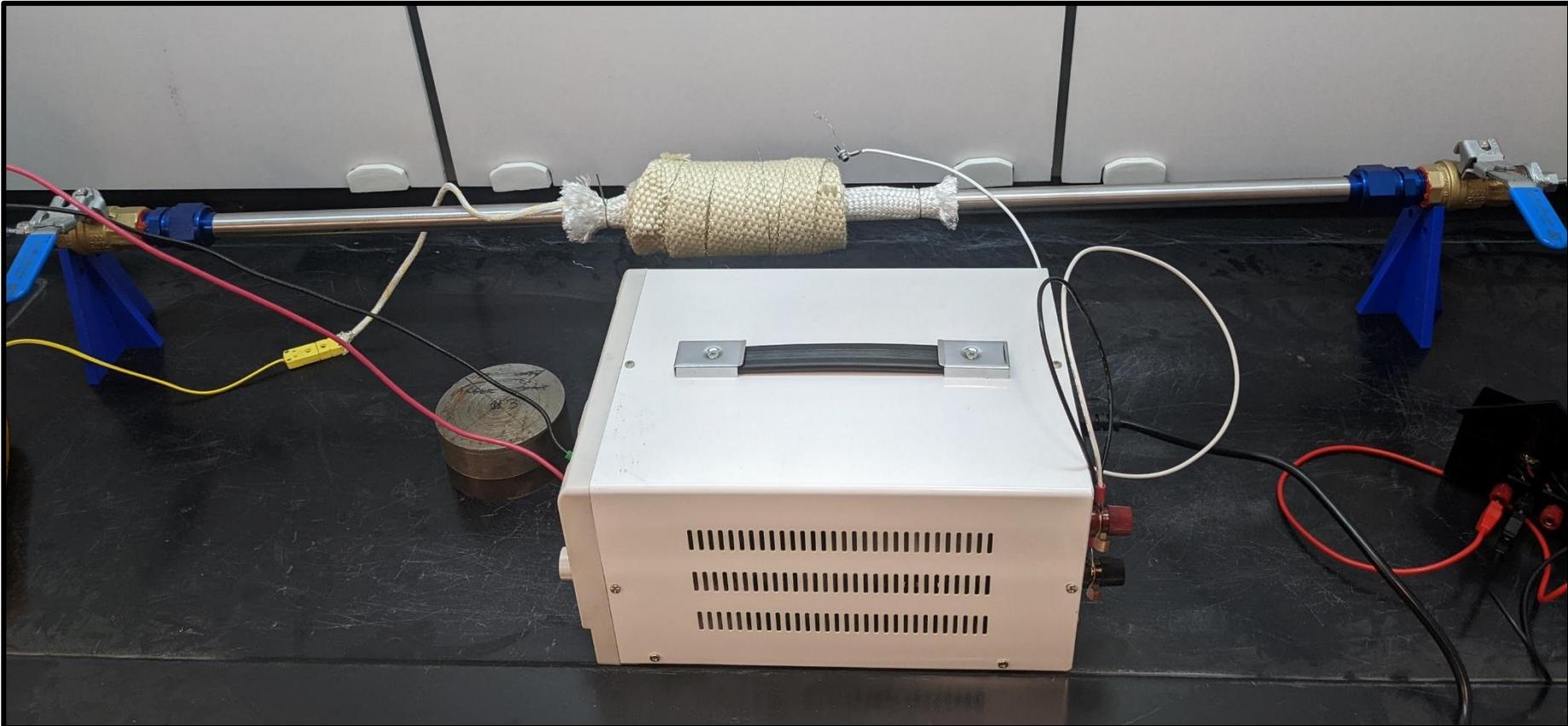
Step 9: Run another flush.





# Concept of Operations

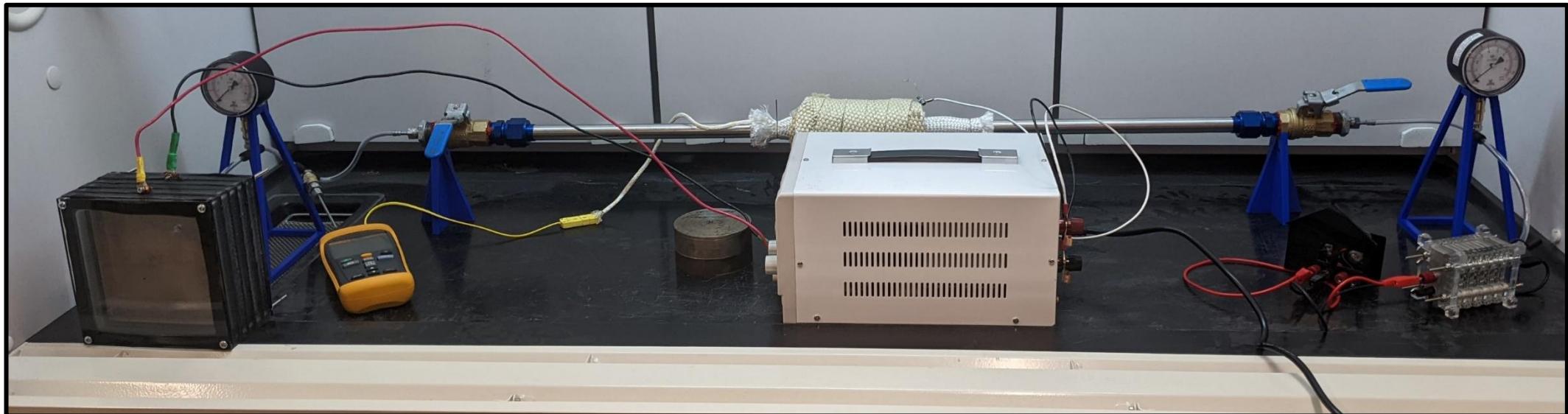
Step 10: Close both valves and turn on the heating element.





# Concept of Operations

Step 11: Once the capsule reaches 300°C, slowly open the valve to the fuel cell. Start a timer to measure how long the fuel cell light stays on.





**ERH<sub>2</sub>**

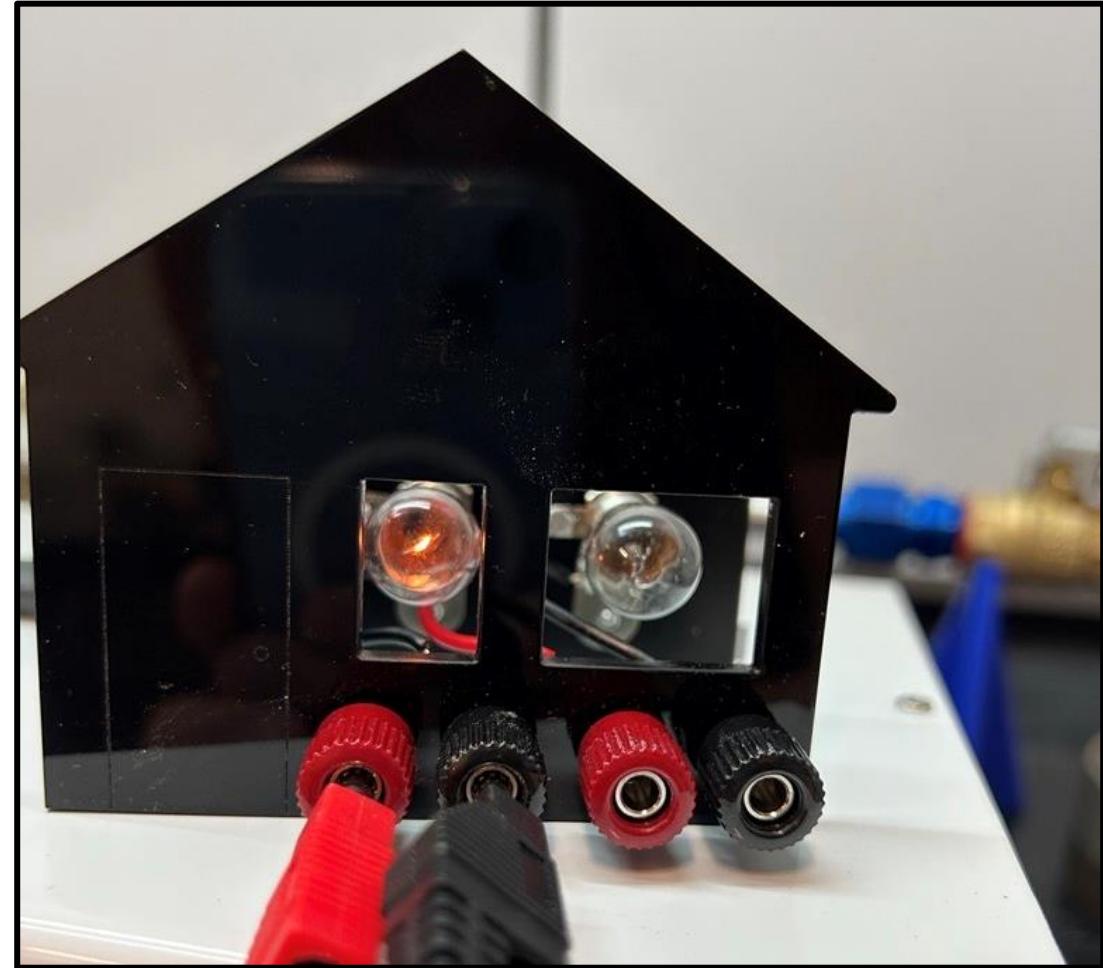
**Verification Tests**



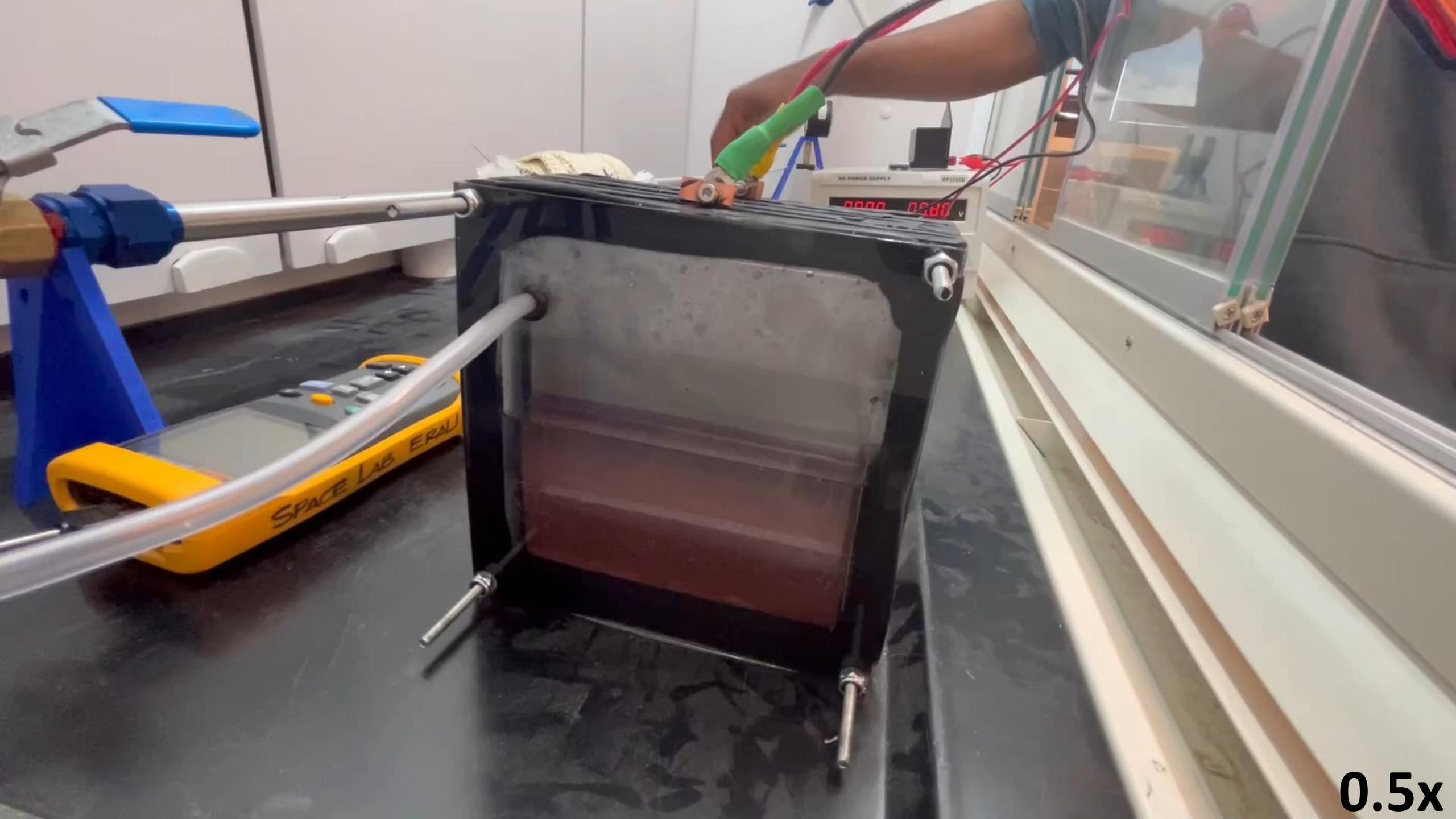
# Production Rate

## *Requirement 1.1.1*

“The system must produce enough hydrogen to get the fuel cell to steady state and then run for 10 minutes at 1 watt.”



0.5x



# Material Storage

Starting Mass:  
37.294(g)



Ran the electrolyzer for 30 minutes.



Ending Mass:  
37.314(g)



$$37.314(g) - 37.294(g) = 0.020(g) \text{ of hydrogen stored}$$



# Material Capacity

Mass of Stored Hydrogen: 0.020 (g)

Mass of Material Total: 0.517 (g)

$$wt\% = \frac{m_1}{m_{tot}} 100\% = \frac{0.020(g)}{0.517(g)} 100\% = 3.87\%$$

*Requirement 4.4*

“The storage material must have a minimum hydrogen density of 2 wt%.”



TEST  
INCOMPLETE



# Material Storage Benefits

	Compressed Storage	Material Storage
Energy Density	592.9-3796 J/m	140-280 J/m <sup>3</sup>
Weight Percentage	3.53%	3.87%
Storage Pressure	60-500 bar	1 bar

# System Heating

*Requirement 4.1*

"The storage material must be heated to 300°C and not exceed 350°C."

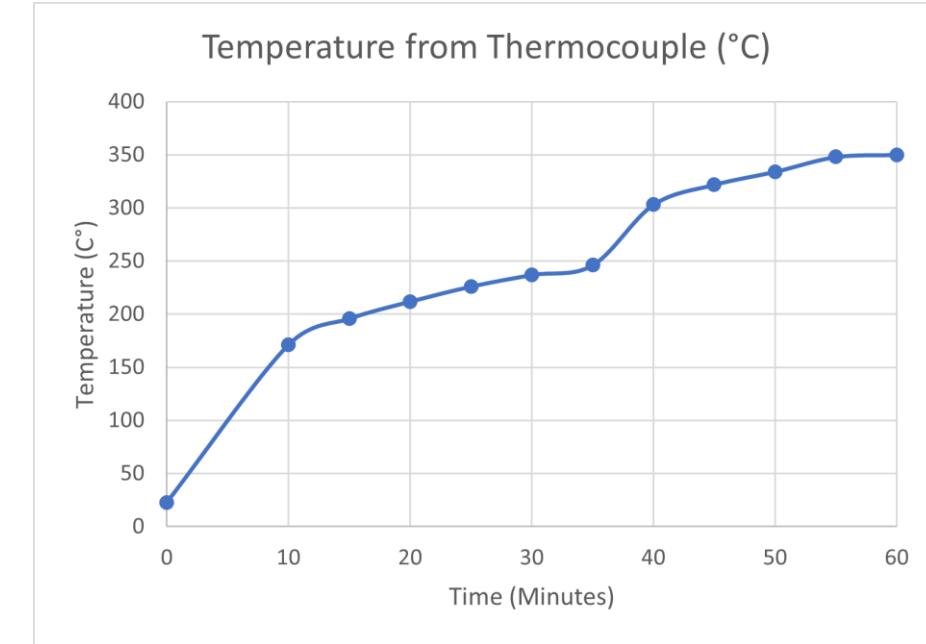


TEST  
INCOMPLETE

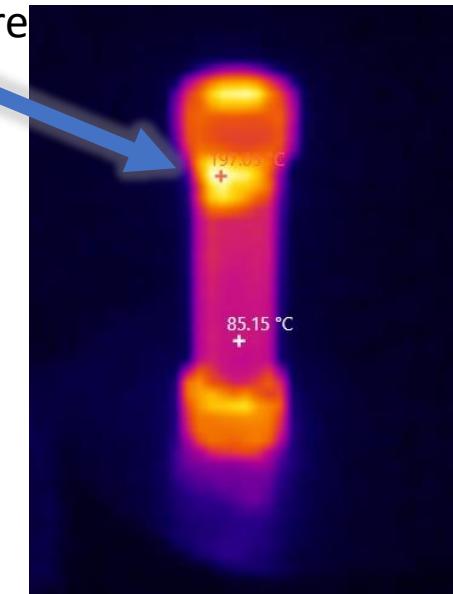
Applied Power

300°C Minimum  
Power: **16.77W**

350°C Minimum  
Power: **23.56W**



Max Temperature  
(200°C)





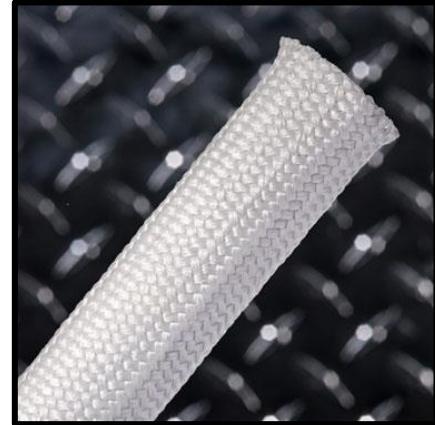
# Thermal Survivability



Aluminum Silicate Fiber  
*Resistant to 815 °C*

*Requirement 5.2*

“The system must withstand temperatures up to 350°C.”



Silica Sleeve  
*Resistant to 1260 °C*

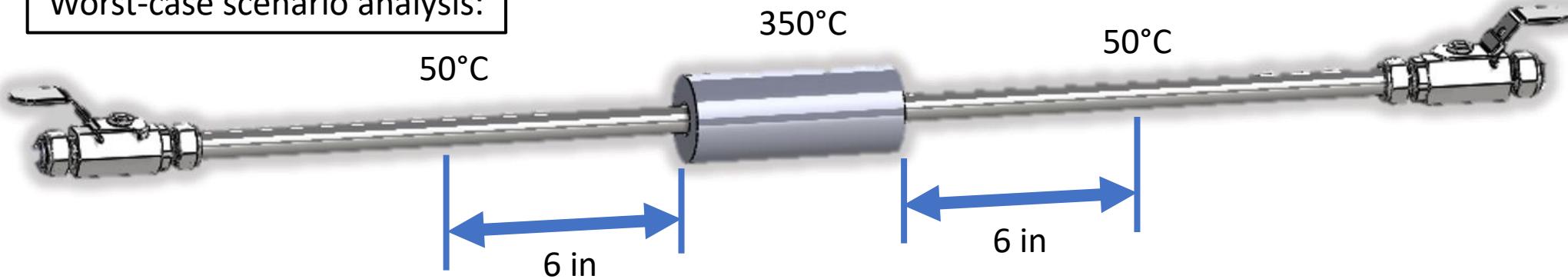


Nichrome  
Wire Lead

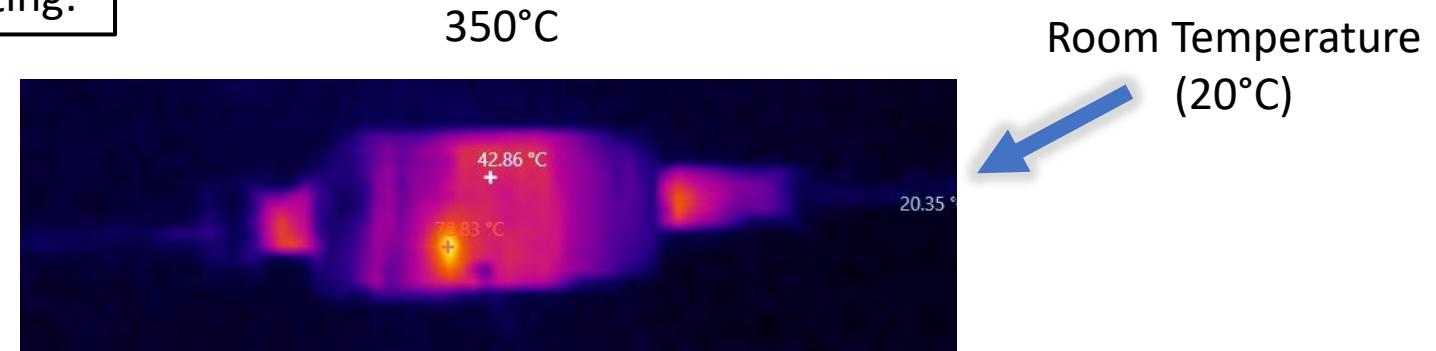


# Pipe Heat Transfer

Worst-case scenario analysis:



Worst-case scenario testing:



*Requirement 5.3*  
“The temperature at the valves  
must not exceed 50°C.”





Number	Requirement	Status
1.1	The system must produce hydrogen gas.	<input checked="" type="checkbox"/>
1.1.1	The system must produce enough hydrogen to get the fuel cell to steady state and then run for 10 minutes at 1 watt.	<input checked="" type="checkbox"/>
1.1.2	The system must be able to determine the rate of hydrogen gas produced.	<input checked="" type="checkbox"/>
1.2	The storage method must run the fuel cell for a minimum of 5 minutes.	<input checked="" type="checkbox"/>
1.2.1	The system must measure the amount of hydrogen stored.	<input checked="" type="checkbox"/>
1.3	The system must fit into the STEM 114 vent hood.	<input checked="" type="checkbox"/>
1.4	The system must interface with the Embry-Riddle fuel cell.	<input checked="" type="checkbox"/>
1.4.1	The system output must be a $\frac{1}{4}$ " PTFE tube.	<input checked="" type="checkbox"/>
1.5	The fuel cell must not exceed the pressure of 0.29 psi.	<input checked="" type="checkbox"/>
2.1	The system must allow for safe production and extraction of hydrogen gas.	<input checked="" type="checkbox"/>
2.2	The system must follow Embry-Riddle Prescott Campus' safety requirements.	<input checked="" type="checkbox"/>
3.1	The system must be able to be disassembled and reassembled to replace parts.	<input checked="" type="checkbox"/>
3.2	The machine must not allow the hydrogen and oxygen produced to mix.	<input checked="" type="checkbox"/>
3.3	The machine components must not be embrittled by hydrogen.	<input checked="" type="checkbox"/>
3.4	The amperage going into the system must be controlled and limited to 22.89 amps.	<input checked="" type="checkbox"/>
4.1	The storage material must be heated to $300^{\circ}\text{C}$ and not exceed $350^{\circ}\text{C}$ .	<input checked="" type="checkbox"/>
4.2	The storage material must be fully contained within the system.	<input checked="" type="checkbox"/>
4.3	The storage material must be at the end of the hydrogen flow.	<input checked="" type="checkbox"/>
4.4	The storage material must have a minimum hydrogen density of 2%wt.	<input checked="" type="checkbox"/>
5.1	The subsystem must transport hydrogen gas from the electrolyzer to the material storage, and from the material storage to the fuel cell.	<input checked="" type="checkbox"/>
5.2	The system must withstand temperatures up to $350^{\circ}\text{C}$ .	<input checked="" type="checkbox"/>
5.3	The temperature at the valves must not exceed $50^{\circ}\text{C}$ .	<input checked="" type="checkbox"/>
6.1	The instrumentation subsystem must be self-reliant	<input checked="" type="checkbox"/>



**ERH<sub>2</sub>**

## **Limiting Factors**

***“Murphy always gets a vote.”***

*- Dr. Michael Fabian*



# Blown-up Material Storage Capsule

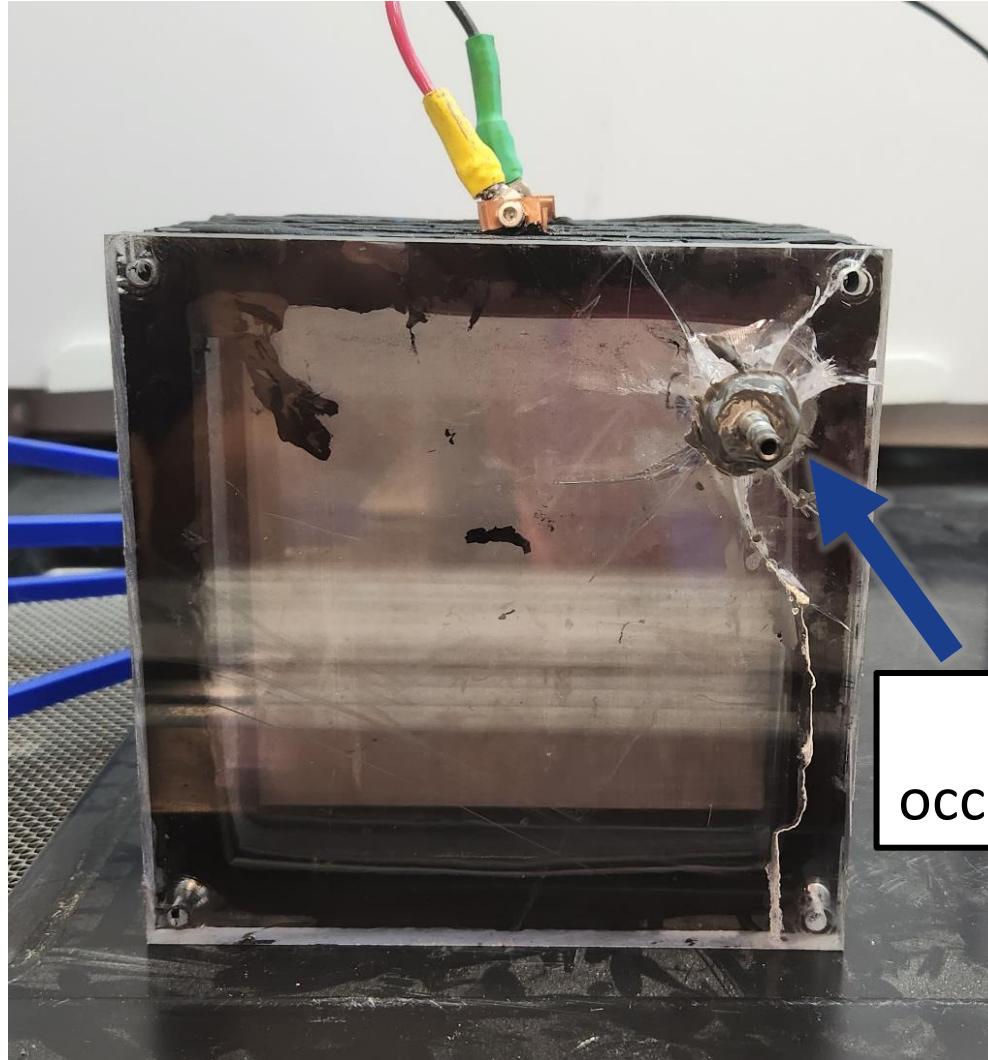




# New Material Storage Capsule



# Cracked Electrolyzer

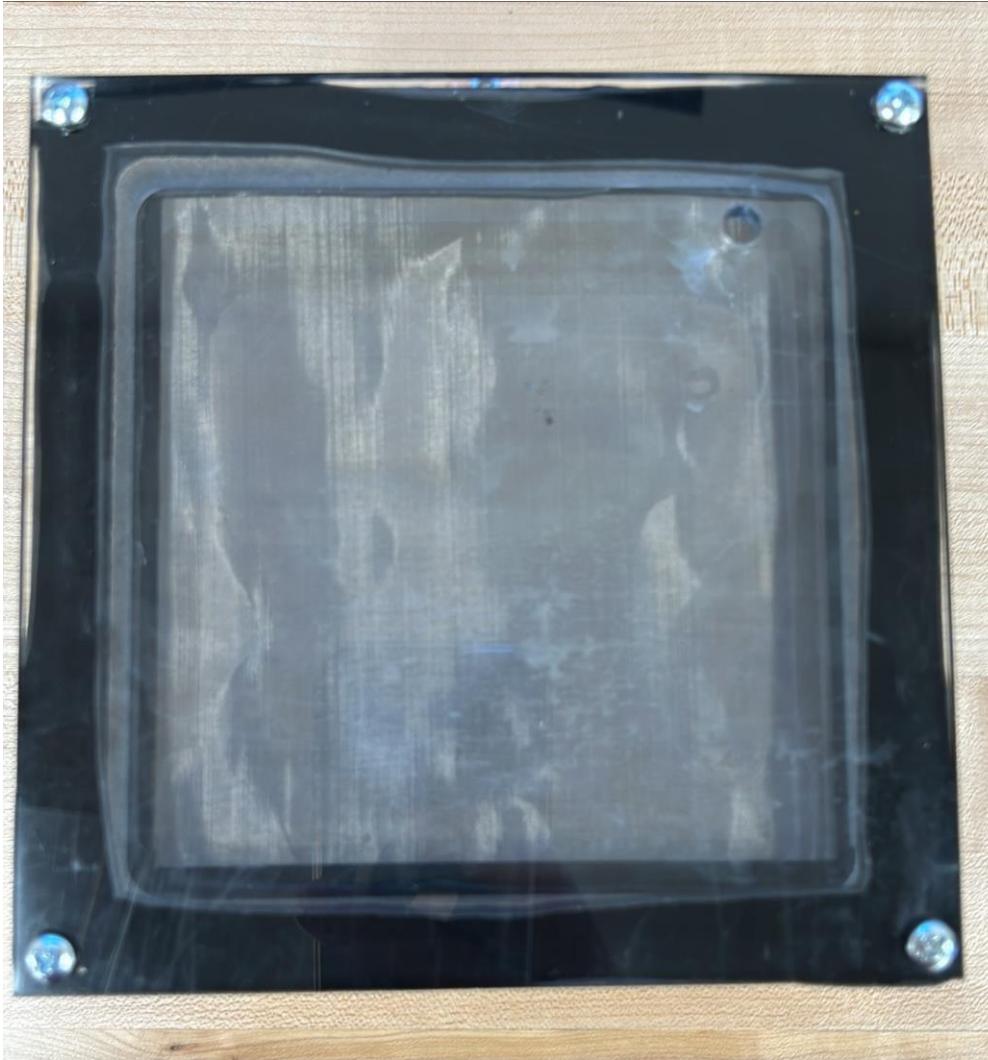


Greatest chemical attack  
occurs at stress concentrations.





# New Electrolyzer End Panels

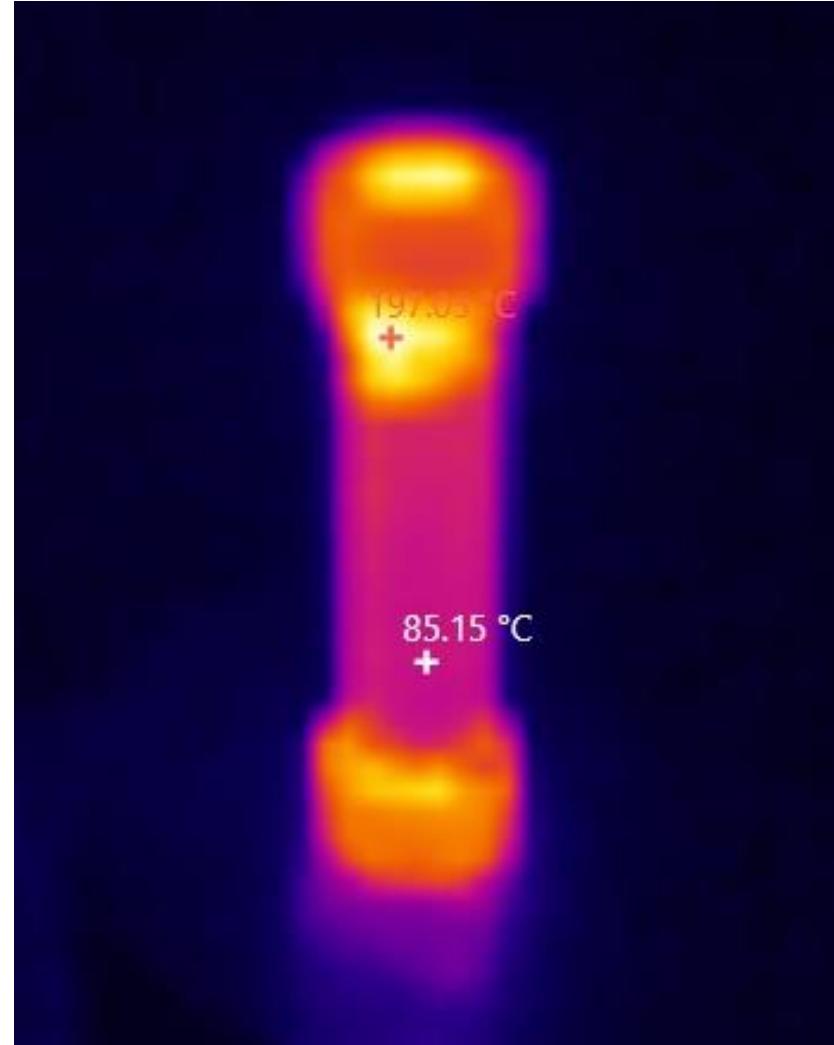




**ERH<sub>2</sub>**

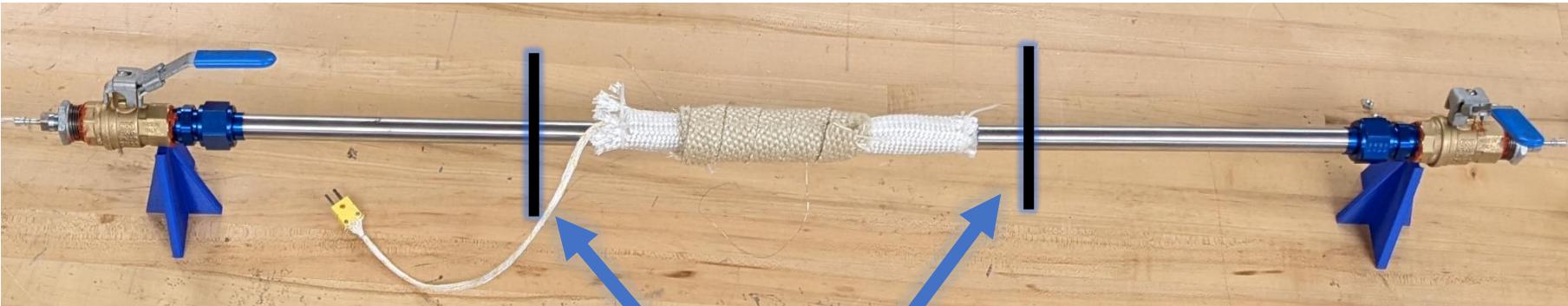
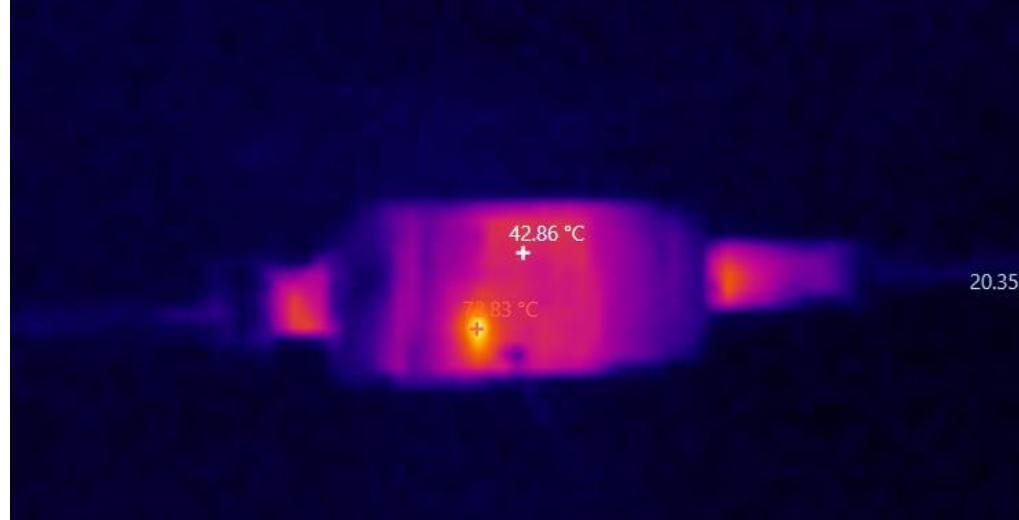
## **Future Recommendations**

# Improve Heat Transfer to Capsule





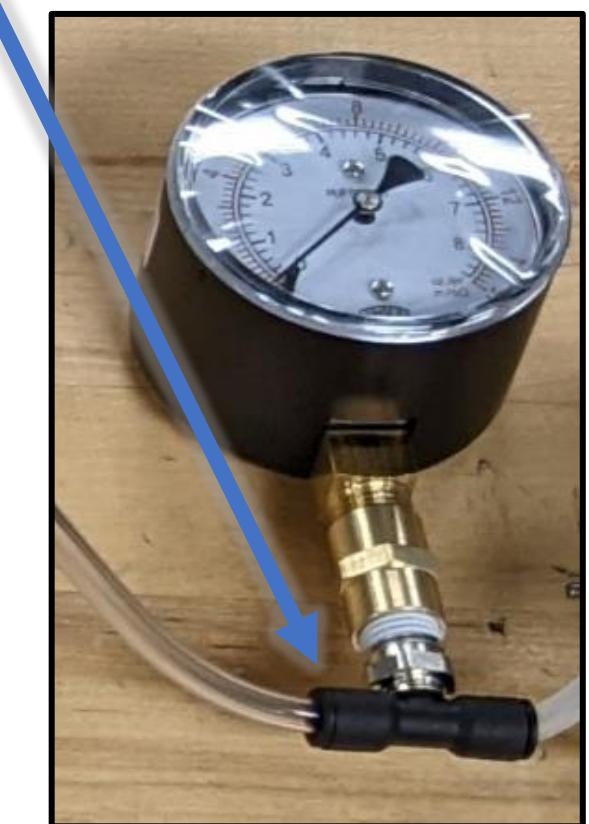
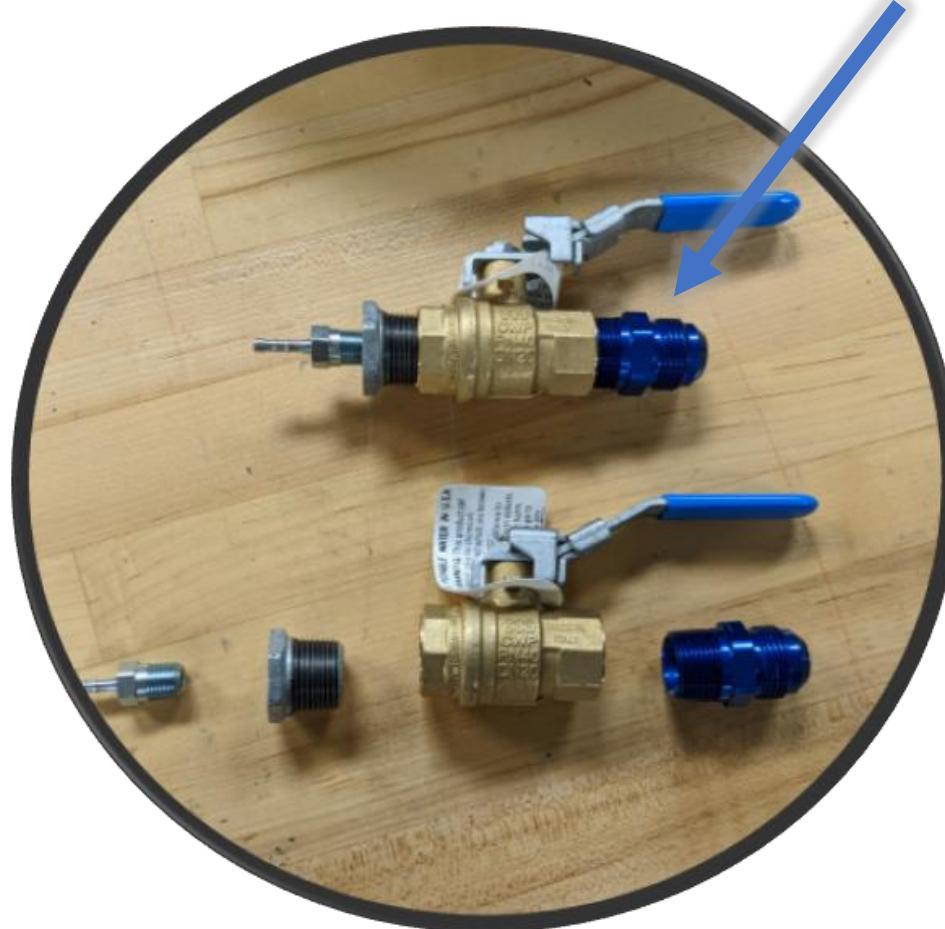
# Shorten Pipe



Cut & Reflare

# Prevent Hydrogen Leakage

Potential Problem Spots



# Future Tests

Capacity  
Tests

Release  
Tests

To be performed next Monday



# Questions?





# References

- [1] A. Murali, M. Sakar, S. Priya, R. J. Bensingh, and M. A. Kader, “Graphitic-Carbon Nitride for Hydrogen Storage,” in Nanoscale Graphitic Carbon Nitride, Elsevier, 2022, pp. 487–514. doi: 10.1016/B978-0-12-823034-3.00017-0.
- [2] “Fast leakage test,” *Unitem Wrocław*, 28-Apr-2022. [Online]. Available: <https://unitemmachines.com/our-offer/fast-leakage-test/>. [Accessed: 08-Dec-2022].
- [3] “Remington Industries.” [Online]. Available: <https://www.remingtonindustries.com/>
- [4] “McMaster-Carr.” [Online]. Available: <https://www.mcmaster.com/>
- [5] <https://www.scielo.br/j/qn/a/KyQvF9DMHK6ZJXyL5zQNy7N/?lang=en&format=pdf>
- [6] <https://www.gichemicals.ie/Potassium-hydroxide.html#:~:text=Potassium%20Hydroxide%20is%20manufactured%20using,concentrated%20to%2050%25%20using%20evaporation>.
- [7] “Aluminum silicate fiber felt and board,” *Aluminum Silicate Fiber Felt and Board*. [Online]. Available: <https://www.samaterials.com/ceramic-material/2515-aluminum-silicate-fiber-felt-and-board.html>. [Accessed: 21-Feb-2023].
- [8] Heat Transfer Textbook

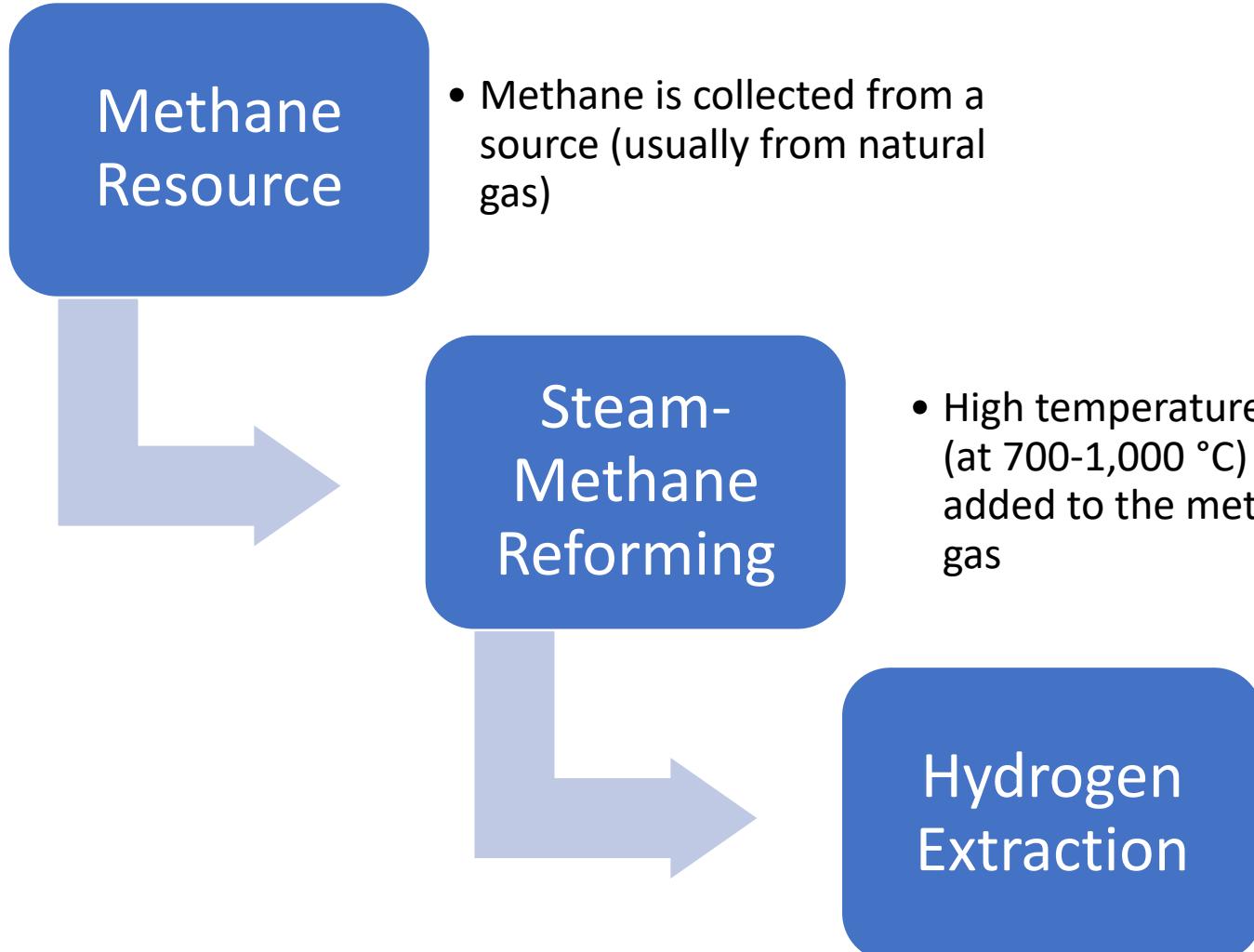
# Additional Slides

- Requirements
- Generation
  - Natural Gas
  - Photobiological
  - Microbial Biomass conversion
- Storage
  - Physical
  - Material
- Equations
- Graphic Design
- Schedule
- Ideal Gas

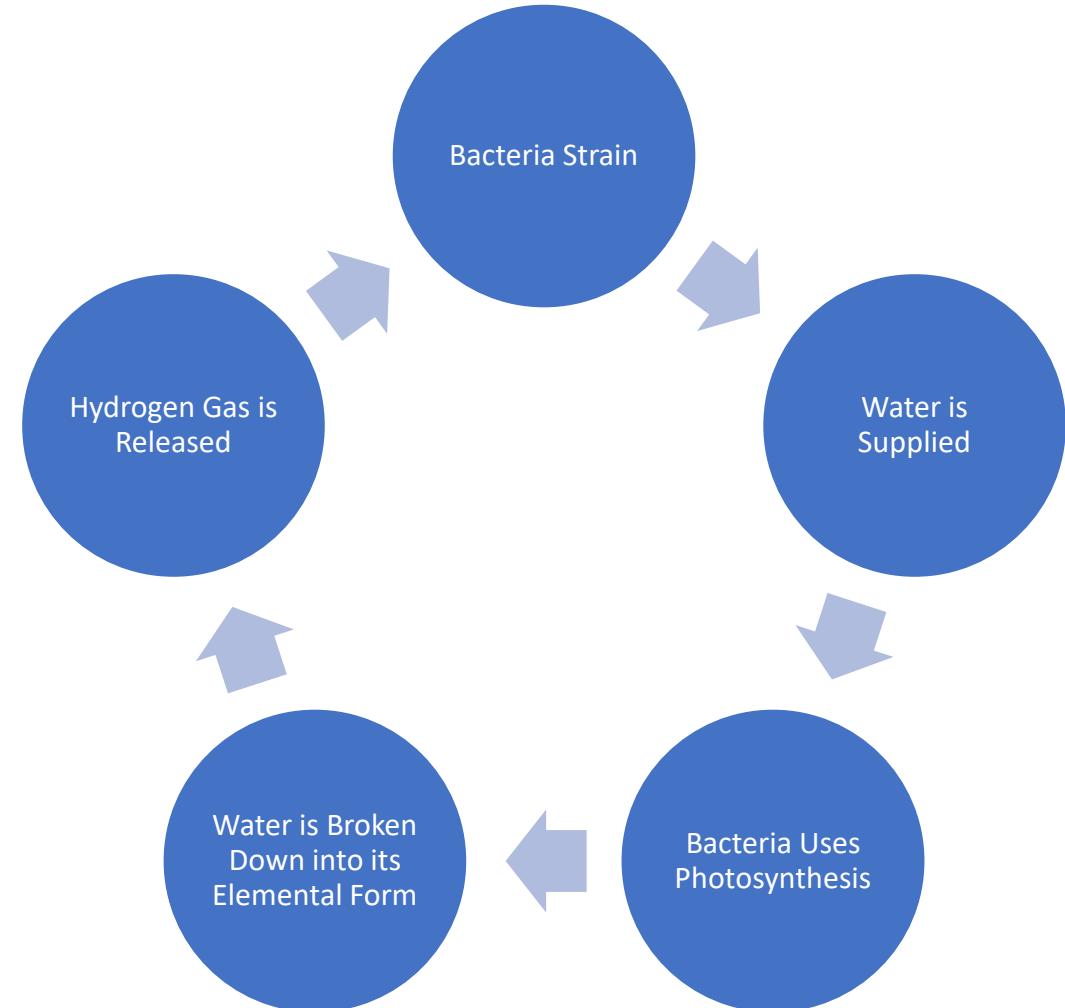




# Generation - Natural Gas



# Generation - Photobiological



# Generation - Microbial Biomass Conversion



# Storage – Physical Storage

Compressed

5,000-  
10,000 PSI

Unique  
Pressure  
Vessels

Cryogenic

Liquid H<sub>2</sub> at  
-252.2 °C

Solid H<sub>2</sub> at  
-259.14°C



# Storage – Material Storage

Adsorbtion

Hydrogen is  
Stuck to the  
Compound's  
Surface

Absorption

Hydrogen is  
Encased by the  
Compound





# Equations – Area of Mesh

$$64 \text{ (in}^2\text{)} * 0.66 = 42.24 \text{ (in}^2\text{)}$$



# Equations – Max Current

$$\frac{0.084 \text{ (A)}}{1 \text{ (cm}^2\text{)}} * \frac{1 \text{ (cm}^2\text{)}}{0.155 \text{ (in}^2\text{)}} * 42.24 \text{ (in}^2\text{)} = 22.89 \text{ (A)}$$



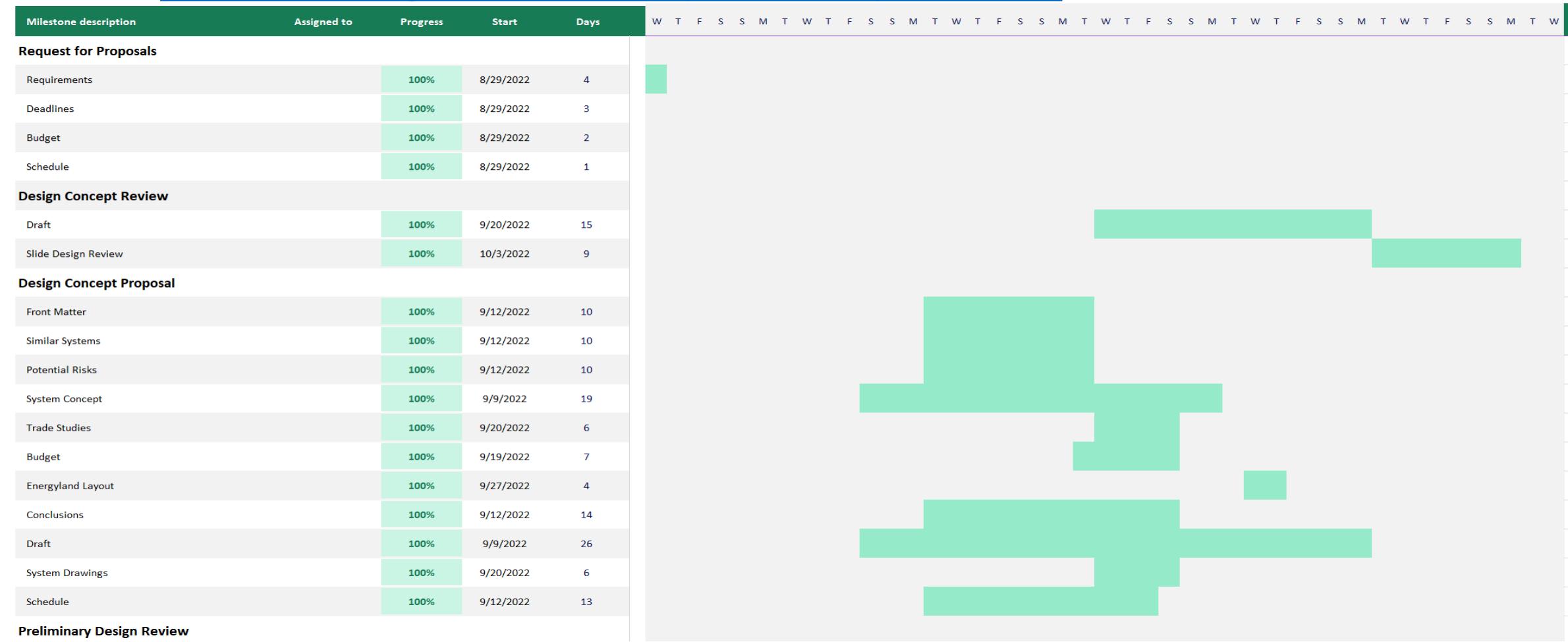
# Equations – Rate of O<sub>2</sub> Production

$$\frac{22.89 \text{ (C)}}{1 \text{ (s)}} * \frac{600 \text{ (s)}}{96,485 \text{ (C)}} * \frac{1 \text{ (mol O}_2\text{)}}{4 \text{ (mol e}^-\text{)}} * \frac{31.998 \text{ (g O}_2\text{)}}{1 \text{ (mol O}_2\text{)}}$$
$$= 1.139 \text{ (g O}_2\text{)}$$



# Schedule of Project

- Date tracking Gantt ERH2 (version 1).xlsb.xlsx





# Ideal Gas Law

$$PV = nRT$$

Where:

$P$  = Absolute pressure of the gas (KPa)

$V$  = Volume of the gas (L)

$n$  = Amount of the gas (g)

$R$  = Ideal gas constant (KJ/Kg\*K)

$T$  = Absolute temperature of the gas (K)

## Calculations



# Heat Loss / Required Power

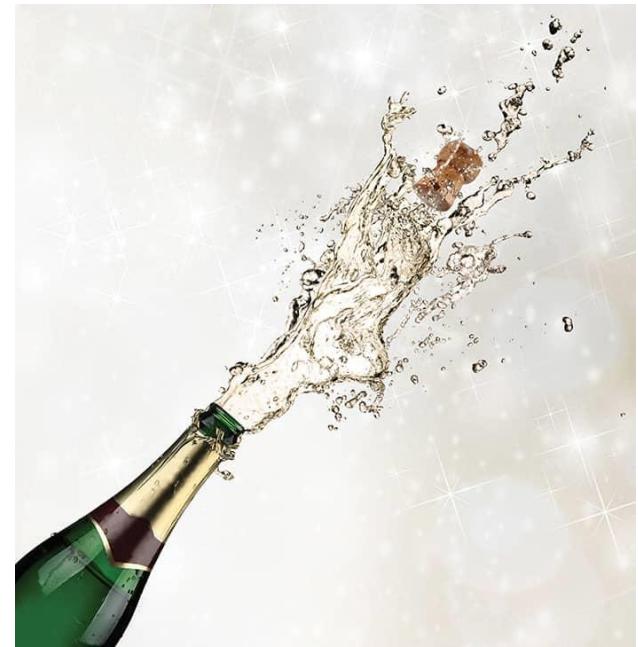
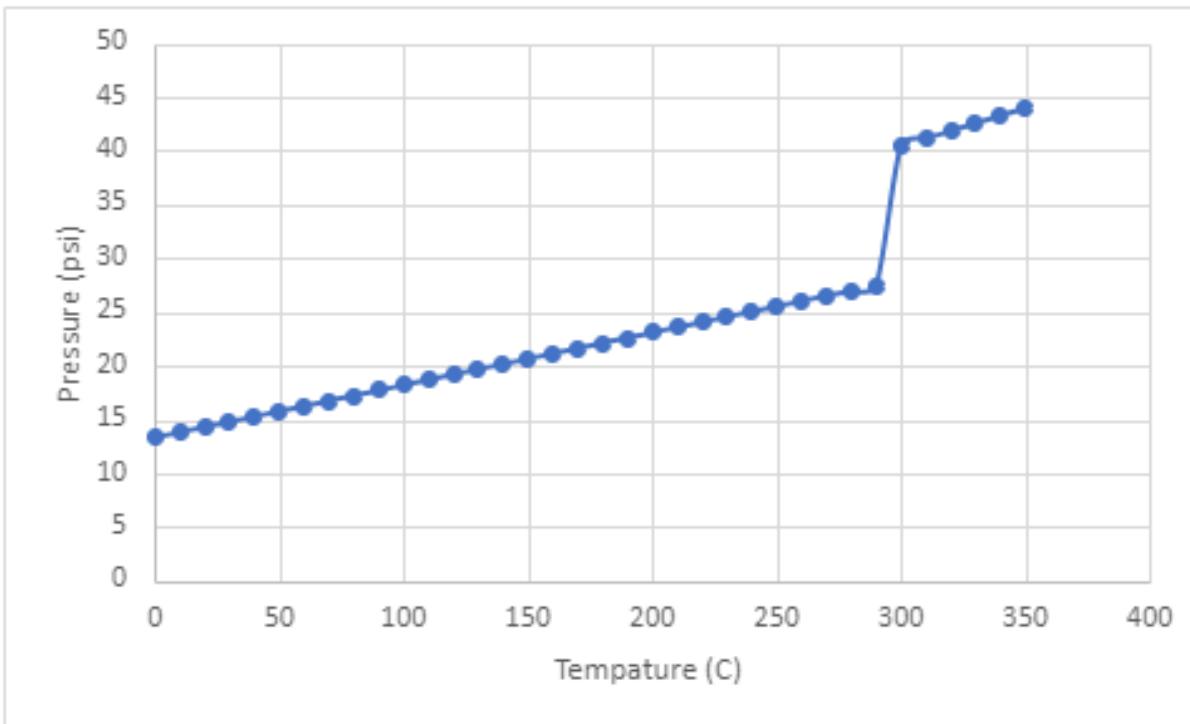
Outer Diameter:	0.75	0.75 (in)
Inner Diameter:	0.68	0.68 (in)
Thermal Conductivity	20	20 (W/m*K)
Surface Temperature	350	50 (°C)
Outer Diameter	0.01905	0.01905 (m)
Gravitational Constant	9.81	9.81 (m/s^2)
Bulk Temperature	20	20 (°C)
Volume Expansion Coefficie	2.18E-03	3.27E-03 (K^-1)
Kinematic Viscosity	3.26E-05	1.66E-05 (m^2/s)
Grashof Number	4.59E+04	2.43E+04
Prandtl	0.69884	0.7268
Rayleigh	3.21E+04	1.76E+04
*Rayleigh < 10^12, we can use the book's equation!		
Nusselt Number	5.80E+00	5.03E+00
Thermal Conductivity	0.036726	0.02625 (W/m*K)
Convection Coefficient	1.12E+01	6.93E+00 (W/m^2*K)
Inner Diameter	0.017272	(m)
Perimeter	0.05984734	(m)
Cross-sectional Area	5.07214E-05	(m^2)
Thermal Conductivity	381.62	395.5433071 (W/m*K)
x	11	
Convection Coefficient, Avg	9.06E+00	(W/m^2*K)
Thermal Conductivity, Avg	20	(W/m*K)
m	2.31E+01	
cosh^-1(x)	3.088969905	
Length	1.34E-01	(m)
Qdot through Fin	7.71E+00	(W)

Outer Diameter:	0.75	0.75 (in)
Inner Diameter:	0.68	0.68 (in)
Thermal Conductivity	20	20 (W/m*K)
Surface Temperature	300	50 (°C)
Outer Diameter	0.01905	0.01905 (m)
Gravitational Constant	9.81	9.81 (m/s^2)
Bulk Temperature	20	20 (°C)
Volume Expansion Coefficient	2.18E-03	3.27E-03 (K^-1)
Kinematic Viscosity	3.26E-05	1.66E-05 (m^2/s)
Grashof Number	3.89E+04	2.43E+04
Prandtl	0.69884	0.7268
Rayleigh	2.72E+04	1.76E+04
*Rayleigh < 10^12, we can use the book's equation!		
Nusselt Number	5.57E+00	5.03E+00
Thermal Conductivity	0.036726	0.02625 (W/m*K)
Convection Coefficient	1.07E+01	6.93E+00 (W/m^2*K)
Inner Diameter	0.017272	(m)
Perimeter	0.05984734	(m)
Cross-sectional Area	5.07214E-05	(m^2)
Thermal Conductivity	381.62	395.5433071 (W/m*K)
x	9.333333333	
Convection Coefficient, Avg	8.83E+00	(W/m^2*K)
Thermal Conductivity, Avg	20	(W/m*K)
m	2.28E+01	
cosh^-1(x)	2.92385707	
Length	1.28E-01	(m)
Qdot through Fin	6.45E+00	(W)



# Vessel Pressure

- Maximum Vessel Pressure: 40.43psia
  - Champagne Bottle: 90psia
  - Soda Can: 30psia





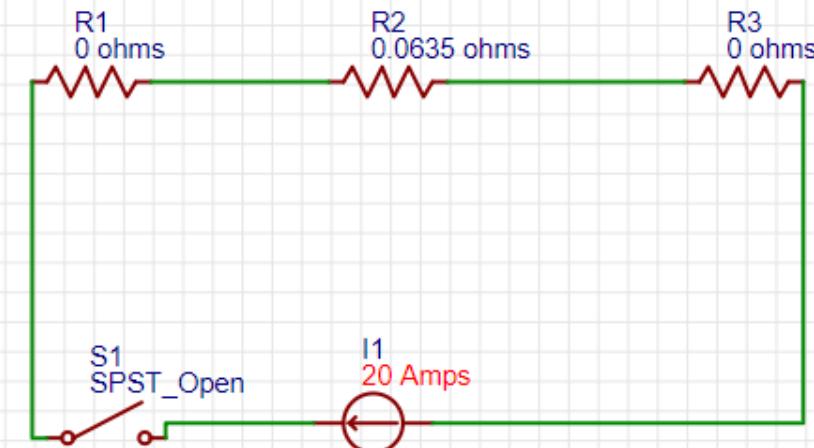
# Electrolysis Power Circuit

$$R_1 = R_3$$

- Nickel Mesh

$$R_2$$

- Salt Water





# Risk Matrix – Before Mitigation

Asset or Operation at Risk	Hazard	Scenario	Opportunities for Prevention or Mitigation	Probability	Overall Hazard Rating
Overall System	Explosion	Hydrogen Leak, normal operation	Sealant	Seldom	2B
Electrolysis	Electrocution	Short Circuit	Insulator	Seldom	2C
Electrolysis	Fire	Excess Oxygen	Planned Dispersion	Seldom	2B
Electrolysis	Ozone	Ozone production	Capture	Improbable	1C
Heating Element	Burns	Contact with Heating Element	Warning Sign	Occasional	3C

Risk Probability	Risk Severity				
	Catastrophic A	Critical B	Moderate C	Minor D	Negligible E
5 – Frequent	5A	5B	5C	5D	5E
4 – Likely	4A	4B	4C	4D	4E
3 - Occasional	3A	3B	3C	3D	3E
2 – Seldom	2A	2B	2C	2D	2E
1 – Improbable	1A	1B	1C	1D	1E



# Detecting Leaks

ERH2 will follow ASHRAE  
Bubble Method under  
Chapter 29.9 Leak  
Detection in the 2017  
edition ASHRAE  
Handbook.



[2]