

# Reactive Transport in the Hydrosphere

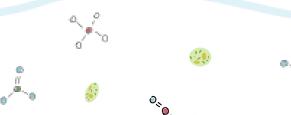
Department of Earth Sciences, Faculty of Geosciences, Utrecht University

Lecturers: Lubos Polerecky and Karline Soetaert

Illustrations, narration and video editing: Renee Hageman Additional contributions: Dries Bonte, University Ghent Audio effects: mixkit.co



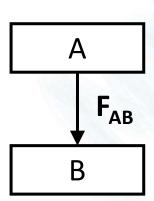






### Model formulation

#### Rate laws



$$\frac{dA}{dt} = -F_{AB} + \dots$$

$$\frac{d\mathbf{B}}{dt} = + F_{AB} + \dots$$

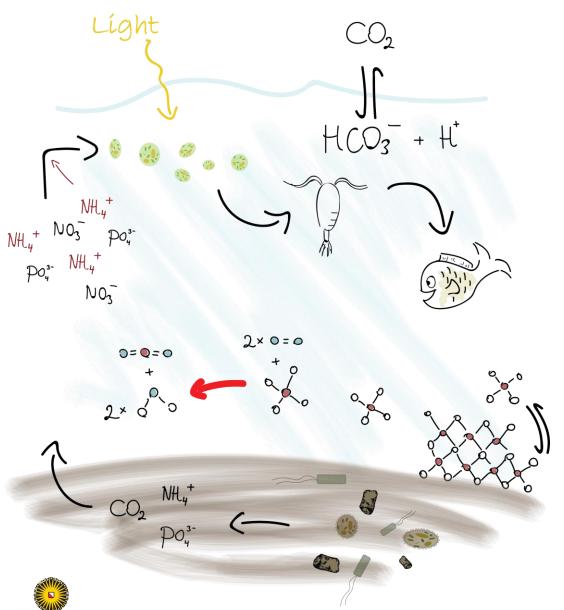


**How** does the rate **depend** on other state variables?

Rate laws describe how the process rates are regulated

$$F_{AB} = f(A, B, t, p1, p2, ...)$$

#### Rate laws for . . .



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#### **Chemical reactions**

- Irreversible
- Reversible
- Enzyme-catalyzed (metabolic)
  - Substrate limitation
  - Substrate inhibition
  - Rate saturation

#### Large-scale models

#### Partitioning between phases

- Mineral dissolution / precipitation
- Gas exchange

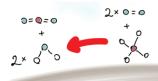
#### **Ecological interactions**

Grazing, predator-prey type

**Transport** 



## Modeling rates of chemical reactions



- Difficult if reactions are complex (e.g., involve several intermediate steps, etc.)
- Generally, reaction stoichiometry does not translate directly into a rate law!!

For example: 
$$2A + 3B -> 2C \rightarrow R = k \cdot [A]^2 \cdot [B]^3$$

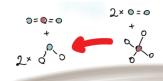
#### **BUT:**

- Every reaction can be written as a sequence of elementary reactions!
- For elementary reactions, the stoichiometry can be directly translated into a rate law.





### Irreversible elementary chemical reactions



**Bi-molecular elementary reaction** 

$$A + B \xrightarrow{k} AB$$

**Probability** that A and B **encounter** is proportional to the **product** of **concentrations** of A and B.

$$R = k \cdot [A] \cdot [B]$$

Reaction rate:

Unit of k: m<sup>3</sup> mol<sup>-1</sup> s<sup>-1</sup>

Rate constant, describes the rate of encounters between A and B that result in the formation of AB.

Mass balance equations:

$$\frac{d[A]}{dt} = -R$$

$$\frac{d[B]}{dt} = -R$$

$$\frac{d[A]}{dt} = -R \qquad \qquad \frac{d[B]}{dt} = -R \qquad \qquad \frac{d[AB]}{dt} = +R$$





### Irreversible elementary chemical reactions



Tri-molecular elementary reaction

$$A + 2B \xrightarrow{k} AB_2$$

**Probability** that A, B and B **collide** is proportional to the **product** of **concentrations** of A and B and B.

$$R = k \cdot [A] \cdot [B]^2$$
 Unit of k: m<sup>6</sup> mol<sup>-2</sup> s<sup>-1</sup>

Reaction rate:

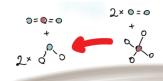
Rate constant, describes the rate of collisions between A and 2xB that result in the formation of AB<sub>2</sub>.

Mass balance equations:

$$\frac{d[A]}{dt} = -R \qquad \qquad \frac{d[B]}{dt} = -2R \qquad \qquad \frac{d[AB_2]}{dt} = +R$$







$$AB \stackrel{\mathsf{k_f}}{\rightleftharpoons} A + B$$

Forward reaction:

$$R_f = k_f \cdot [AB]$$

$$k_f$$
 = rate constant of the **forward**

reaction (s<sup>-1</sup>)

Backward reaction:

$$R_b = k_b \cdot [A] \cdot [B]$$

 $k_b$  = rate constant of the **backward** 

reaction (mol<sup>-1</sup> m<sup>3</sup> s<sup>-1</sup>)

Mass balance equations:

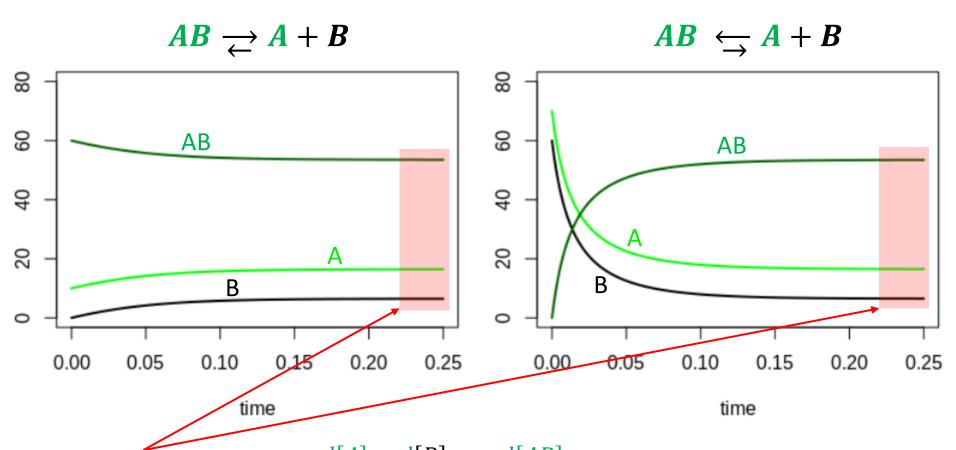
$$\frac{d[A]}{dt} = \frac{d[B]}{dt} = -\frac{d[AB]}{dt} = (R_{f} - R_{b})$$







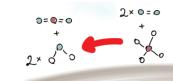
$$AB \underset{\mathsf{k}_{\mathsf{b}}}{\overset{\mathsf{k}_{\mathsf{f}}}{\rightleftharpoons}} A + B \qquad \frac{d[A]}{dt} = \frac{d[B]}{dt} = -\frac{d[AB]}{dt} = (\mathsf{R}_{\mathsf{f}} - \mathsf{R}_{\mathsf{b}})$$



Equilibrium:

$$\frac{d[A]}{dt} = \frac{d[B]}{dt} = -\frac{d[AB]}{dt} = (R_f - R_b) = 0$$



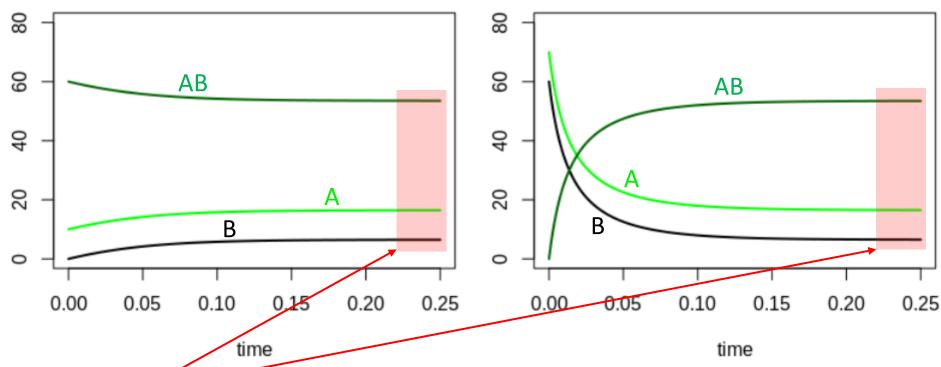


$$AB \underset{\mathsf{k}_{\mathsf{b}}}{\overset{\mathsf{k}_{\mathsf{f}}}{\rightleftharpoons}} A + B$$

$$\frac{d[A]}{dt} = \frac{d[B]}{dt} = -\frac{d[AB]}{dt} = (R_f - R_b)$$

$$AB \rightleftharpoons A + B$$

$$AB \leftarrow A + B$$



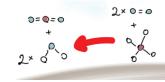
Equilibrium:

$$(R_f - R_b) = 0$$



$$\frac{k_f}{k_b} = \frac{\left[A_{eq}\right] \cdot \left[B_{eq}\right]}{\left[AB_{eq}\right]}$$





$$AB \stackrel{\mathsf{k}_{\mathsf{f}}}{\rightleftharpoons} A + B$$

$$\frac{d[A]}{dt} = \frac{d[B]}{dt} = -\frac{d[AB]}{dt} = (R_f - R_b)$$

Equilibrium: 
$$K_{eq} = \frac{k_f}{k_b} = \frac{A_{eq} \cdot [B_{eq}]}{[AB_{eq}]}$$

**Equilibrium constant** 

Composition of the system in equilibrium.





#### **Example:**

$$NH_3(aq) \rightleftharpoons NH_3(g)$$

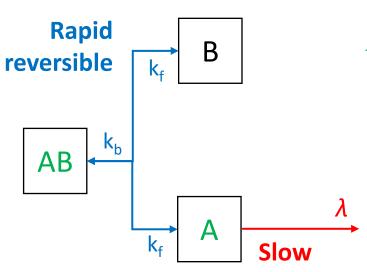
Air-water exchange (slow)

$$NH_4^+(aq) \rightleftharpoons NH_3(aq) + H^+$$

Dissociation in water (fast)







$$AB \stackrel{\mathsf{k}_{\mathsf{f}}}{\rightleftharpoons} A + B \qquad A + \cdots \stackrel{\lambda}{\longrightarrow} \cdots$$

Mass balance equations:

$$\frac{d[A]}{dt} = -k_b \cdot [A] \cdot [B] + k_f \cdot [AB] - \lambda \cdot [A]$$

$$\frac{d[B]}{dt} = -k_b.[A].[B] + k_f.[AB]$$

$$\frac{d[AB]}{dt} = +k_b.[A].[B] - k_f.[AB]$$

Sum (1) and (3):

Sum (2) and (3):



$$\frac{d([A] + [AB])}{dt} = -\lambda \cdot [A]$$

$$\frac{d([B] + [AB])}{dt} = 0$$



We consider **new state variables**: • **Lump sum** of A:  $\Sigma A = A + AB$ 

• Lump sum of B:  $\Sigma B = B + AB$ 

Conceptual diagram and mass balance equations are dramatically simplified!

$$\frac{d[\Sigma B]}{dt} = 0 \tag{1}$$

$$\frac{d[\Sigma A]}{dt} = -\lambda . [A] \tag{2}$$

How do we "get rid of" [A] in equation 2?

**Local equilibrium assumption:** on the time-scale of the slow process, we assume that the fast reversible reaction reached an **equilibrium**.

#### What does the local equilibrium assumption imply?

$$AB \underset{k_{b}}{\rightleftharpoons} A + B \longrightarrow K_{eq} \equiv \frac{k_{f}}{k_{b}} = \frac{[A] \cdot [B]}{[AB]} \longrightarrow [AB] = \frac{[A] \cdot [B]}{K_{eq}}$$

$$[\Sigma A] = [A] + [AB] = [A] \cdot \left(1 + \frac{[B]}{K_{eq}}\right) \longrightarrow \frac{d[\Sigma A]}{dt} = -\lambda. [A]$$

$$\frac{d[\Sigma A]}{dt} = -L. [\Sigma A] \qquad L = \lambda \frac{K_{eq}}{K_{eq} + [B]}$$
First-order kinetics! How do we "get rid of" [B]?





#### What does the local equilibrium assumption imply?

$$AB \underset{k_b}{\overset{k_f}{\rightleftharpoons}} A + B \longrightarrow K_{eq} \equiv \frac{k_f}{k_b} = \frac{[A] \cdot [B]}{[AB]} \longrightarrow [A] = \frac{[AB] \cdot K_{eq}}{[B]}$$

$$[\Sigma A] = [A] + [AB] \xrightarrow{\text{Solve for [AB]}} [AB] = [\Sigma A] \frac{[B]}{K_{eq} + [B]}$$

$$[\Sigma B] = [B] + [AB] \xrightarrow{\text{Simplify for [B]}} [B] + [\Sigma A] \frac{[B]}{K_{eq} + [B]} = [\Sigma B]$$

$$[Solve quadratic equation for [B]]$$

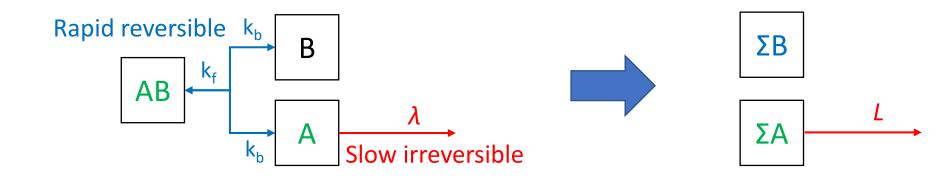
$$[B] = \frac{1}{2} \left( -\beta + \sqrt{\beta^2 + 4K_{eq} \cdot [\Sigma B]} \right)$$

 $\beta = K_{eq} + [\Sigma A] - [\Sigma B]$ 

[B] is only a function of  $[\Sigma A]$  and  $[\Sigma B]$ 



Modify state variables, conceptual diagram, and rate laws



• Modify state variables:

$$\Sigma A = A + AB$$

$$\Sigma B = B + AB$$

Modify rate laws:

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$$\frac{d[\Sigma A]}{dt} = -L.[\Sigma A]$$

$$\frac{d[\Sigma B]}{dt} = 0$$

$$L = \lambda \frac{K_{eq}}{K_{eq} + [B]}$$

$$[B] = \frac{1}{2} \left( -\beta + \sqrt{\beta^2 + 4K_{eq} \cdot [\Sigma B]} \right)$$

$$K_{eq} = \frac{k_f}{k_b}$$

$$\beta = K_{eq} + [\Sigma A] - [\Sigma B]$$



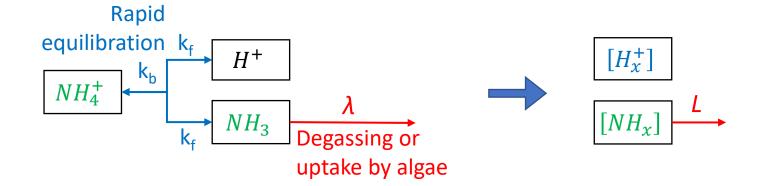
#### **Generally applicable approach:**

- If we carefully choose state variables, we can describe the system by a much simpler model.
- The **choice depends on the time-scale** we want to study the behavior of the system.
  - Example: if we are **not interested in fast equilibration processes**, we can use **lump sums** rather than individual species.
- Saves considerable computational resources to solve models numerically.





#### Example



 $[H_{\nu}^{+}] = [H^{+}] + [NH_{\Lambda}^{+}]$ New state variables (lump sums): **Total** positive charge:

**Total** dissolved ammonia:  $[NH_x] = [NH_3] + [NH_4^+]$ 

Approximate mass balance equations:

$$\frac{d[H_x^+]}{dt} = 0$$

$$\frac{d[NH_x]}{dt} = -L.[NH_x^+]$$

$$L = \lambda \frac{K_{eq}}{K_{eq} + [H^+]}$$

ce equations: 
$$pH = -log[H^+]$$
 
$$\downarrow$$
 
$$L = \lambda \frac{K_{eq}}{K_{eq} + [H^+]}$$
 
$$[H^+] = \frac{1}{2} \left( -\beta + \sqrt{\beta^2 + 4K_{eq} \cdot [H_x^+]} \right)$$

$$K_{eq} \equiv \frac{k_f}{k_h} \qquad \beta = K_{eq} + [NH_x] - [H_x^+]$$



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