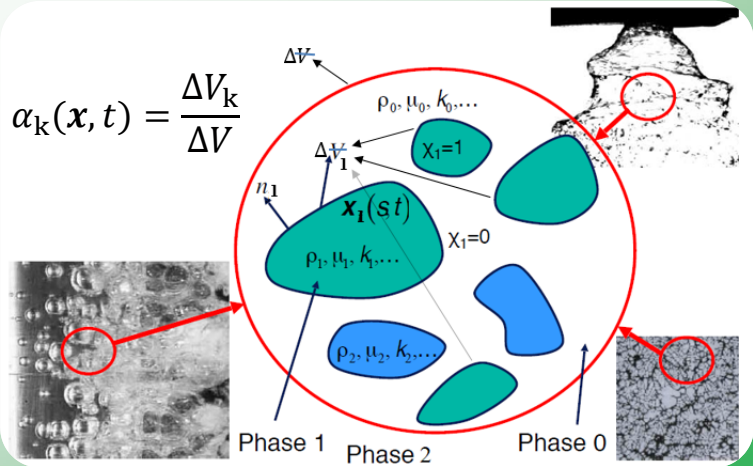


Hands-on practice

- **HW#1:**
 - ✓ **Fluent installation and preliminary practice**

Volume fraction

● Definition:

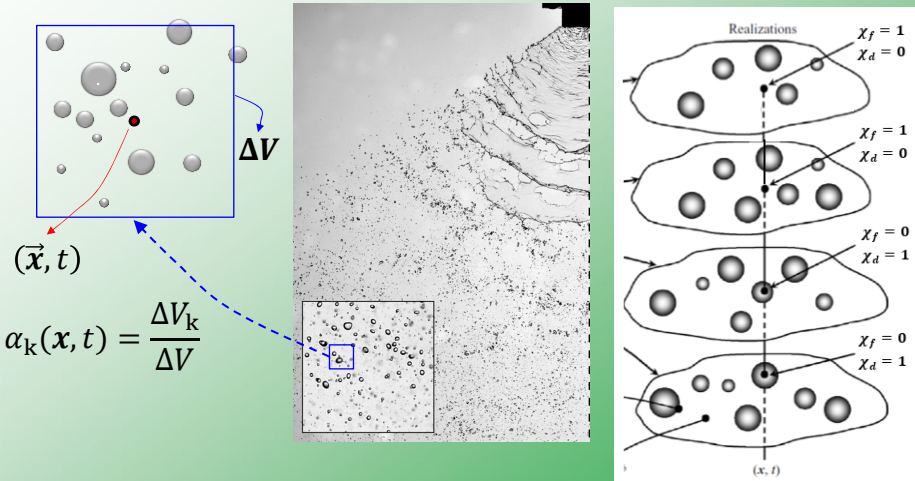


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Volume fraction

● A better alternative:



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Volume fraction

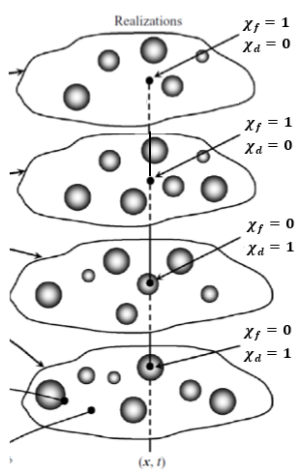
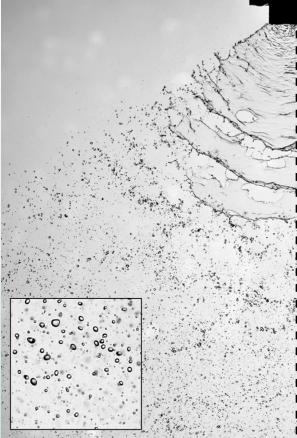
- A better alternative:

Phase indicator function

$$\chi_k(x, t) = \begin{cases} 1 & ; (x, t) \text{ is in phase } k \\ 0 & ; \text{otherwise} \end{cases}$$

$\alpha_k(x, t) = \langle \chi_k(x, t) \rangle$

Ensemble averaging operator

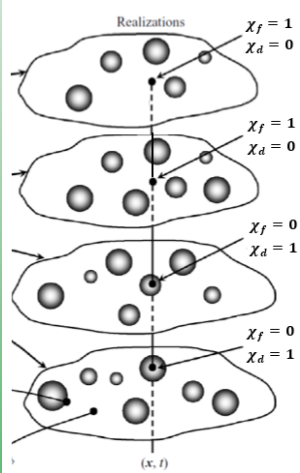


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Basic concepts and key definitions

- Volume fraction (continued)
 - ⇒ Lecture Notes: 2.1
- Averaging operators in multiphase flows
 - ⇒ Lecture Notes: 2.2



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Different kinds of averaging


	Statistical (ensemble-based) Naud (2000)	Volume-based [2,5,6]	Kernel-based Capecelatro (2013)
Average	$\bar{Q}_k \equiv \langle Q_k \chi_k \rangle$	$\bar{Q}_k \equiv \frac{1}{\Delta V} \int_{\Delta V_k} Q_k dV$	$\bar{Q}_k \equiv \int_D \chi_k(\vec{y}) Q_k(\vec{y}) \times k(\vec{x} - \vec{y}) d\vec{y}$
Phasic average	$\langle Q \rangle_{ k} \equiv \frac{\langle Q_k \chi_k \rangle}{\langle \chi_k \rangle}$	$\langle Q \rangle_{ k} \equiv \frac{1}{\Delta V_k} \int_{\Delta V_k} Q_k dV$	$\langle Q \rangle_{ k} \equiv \frac{\bar{Q}_k}{\int_D \chi_k(\vec{y}) k(\vec{x} - \vec{y}) d\vec{y}}$
Mass-weighted average	$\tilde{Q}_k \equiv \frac{\overline{\rho_k Q_k}}{\overline{\rho_k}}$	$\tilde{Q}_k \equiv \frac{\overline{\rho_k Q_k}}{\overline{\rho_k}}$	$\tilde{Q}_k \equiv \frac{\overline{\rho_k Q_k}}{\overline{\rho_k}}$
Mixture average	$\bar{Q} \equiv \sum_{k=1}^N \bar{Q}_k$	$\bar{Q} \equiv \sum_{k=1}^N \bar{Q}_k$	$\bar{Q} \equiv \sum_{k=1}^N \bar{Q}_k$
		Time average [5] $\bar{Q}^t \equiv \frac{1}{\Delta t} \int_{\Delta t_k} Q_k dt$	

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Basic concepts and key definitions

- For incompressible flows:
$$\tilde{Q}_k \equiv \frac{\overline{\rho_k Q_k}}{\overline{\rho_k}} = \frac{\langle \chi_k \rho_k Q_k \rangle}{\langle \chi_k \rho_k \rangle} = \frac{\langle \chi_k Q_k \rangle}{\langle \chi_k \rangle} = \langle Q \rangle_{|k} \quad (15.2)$$
- Other key parameters
- Area-weighted averaging for channel flows

 Lecture Notes: 2.3

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Non-dimensional parameters

- Several important parameters of multi-phase flows [9]:

- Geometric scales

- Phasic **physical properties** ratios:

$$\frac{\rho_1}{\rho_2}, \quad \frac{\mu_1}{\mu_2}, \dots$$

- Force ratios:

Reynolds number $\leftarrow \quad Re = \frac{LU}{v_1} \sim \frac{\text{inertia force}}{\text{viscous force}}$

\swarrow 1 is usually taken as the liquid phase

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Non-dimensional parameters

- Several important parameters of multi-phase flows [9]:

- Force ratios:

Reynolds number $\leftarrow \quad Re = \frac{LU}{v_1} \sim \frac{\text{inertia force}}{\text{viscous force}}$

Weber number $\leftarrow \quad We = \frac{\rho_1 LU^2}{\sigma} \sim \frac{\text{inertia force}}{\text{capillary force}}$

Froude number $\leftarrow \quad Fr = \frac{U^2}{gL} \sim \frac{\text{inertia force}}{\text{gravity force}}$

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Non-dimensional parameters

- Several important parameters of multi-phase flows [9]:

- Force ratios (dependent parameters):

$$\text{Capillary number} \quad \leftarrow \quad Ca = \frac{\mu_1 U}{\sigma} = ReWe$$

$$\text{Eotvos number} \quad \leftarrow \quad Eo = \frac{\Delta\rho g L^2}{\sigma} = \frac{We}{Fr}$$

$$\text{Archimedes number} \quad \leftarrow \quad Ar = \frac{g\rho_1\Delta\rho L^3}{\mu_1^2} = \frac{\Delta\rho}{\rho_1} \frac{Re^2}{Fr}$$

- ▲ For **buoyancy-driven** flows with no explicit reference velocity if

$$U = \sqrt{(\Delta\rho/\rho_1)gL} \quad \rightarrow \quad Ar = Re^2$$

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Non-dimensional parameters

- Several important parameters of multi-phase flows [9]:

- Force ratios (dependent parameters):

$$\text{Capillary number} \quad \leftarrow \quad Ca = \frac{\mu_1 U}{\sigma} = ReWe$$

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$$\text{Archimedes number} \quad \leftarrow \quad Ar = \frac{g\rho_1\Delta\rho L^3}{\mu_1^2} = \frac{\Delta\rho}{\rho_1} \frac{Re^2}{Fr}$$

$$\text{Ohnesorge number} \quad \leftarrow \quad Oh = \frac{\mu_1}{\sqrt{\rho_1\sigma L}} = \frac{\sqrt{We}}{Re} = \frac{1}{\sqrt{La}} = \frac{1}{Z}$$

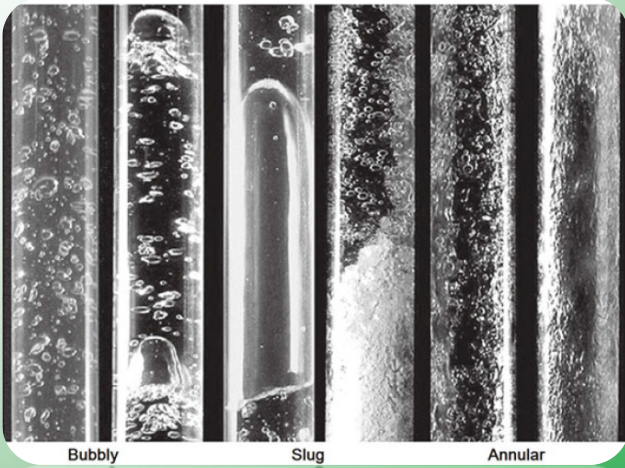
$$\text{Morton number} \quad \leftarrow \quad M = \frac{\Delta\rho g \mu_1^4}{\rho_1^2 \sigma^3} = \frac{Eo^3}{Ar^4} = Eo \frac{Re^4}{We^2}$$

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Regime diagrams

- Gas-liquid flow in vertical pipes

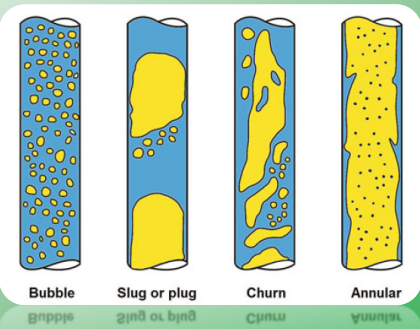
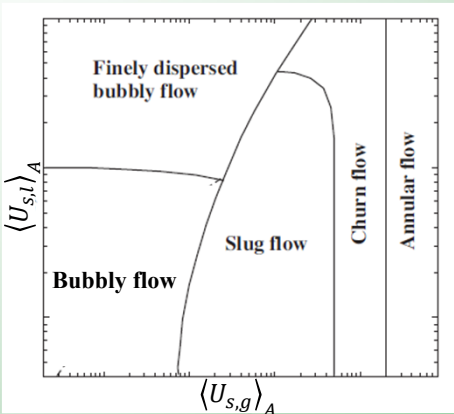


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Regime diagrams

- Gas-liquid flow in vertical pipes




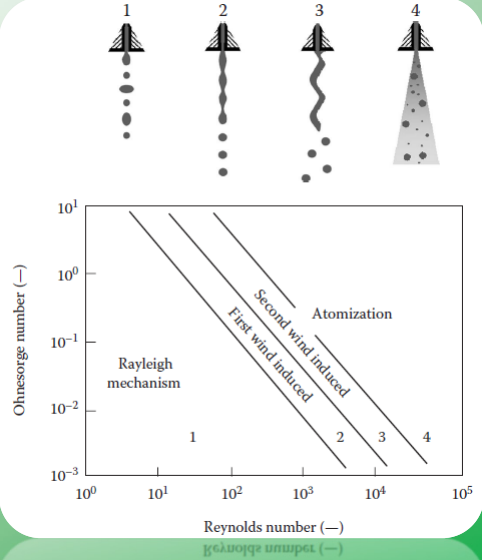
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Regime diagrams

- Droplet generation





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Regime diagrams

- Rising bubbles, falling drops

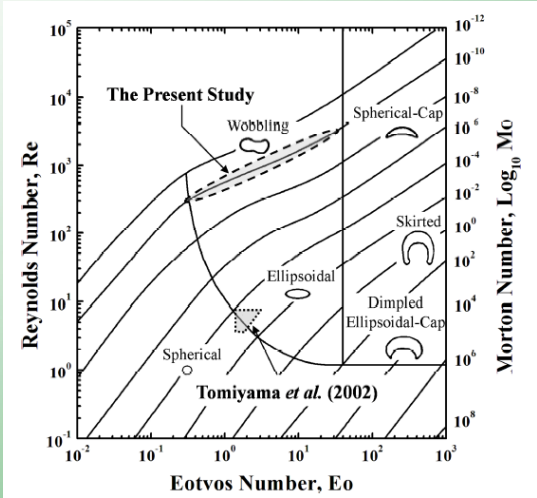


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Regime diagrams

- Rising bubbles, falling drops

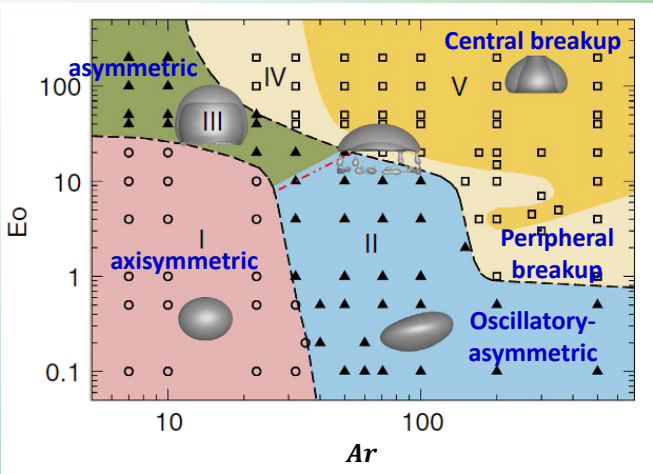


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Regime diagrams

- Rising bubbles, falling drops

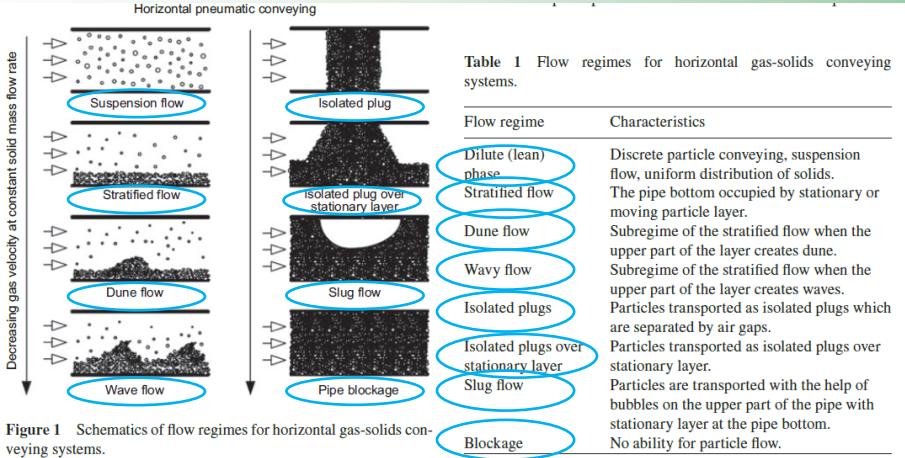


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Regime diagrams

Gas-solid flow in horizontal ducts



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➡ Regime diagram? (HW)

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Hands-on practice

- HW#2:
 - Python installation
 - CFD with python (preliminary experience)
 - Getting familiar with the python NS solver “NSMF1.py”
 - Finding resources on the Net

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