

# A Validity Study for Perfusion Measurements in the Capillary System

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The usage of one-compartment (1C) models within perfusion imaging for estimation of cerebral blood flow (perfusion), cerebral blood volume and mean transit times is widespread. The classical 1C models were originally developed for larger regions of interest (ROIs) where the arterial input function is a valid tracer source function for the entire domain. The extended usage of classical 1C models voxelwise or for smaller block-sizes than the entire organ is not necessarily transferable since the arterial input function is dispersed for a majority of the computational sub-units. In this work we generate a digital phantom for capillary blood flow in order to investigate whether the classical 1C models are applicable to various types of sub-division of the imaged organ. Our results support the usage of classical 1C models for entire organs, but also indicate that the application of these models to smaller block-sizes is questionable and should be further investigated.

## 1 Introduction

Quantitative medical measurements based on tracer kinetic models is an important field both in research and in clinical practice [1, 2, 3]. In the present work, we focus on mathematical models for estimating blood perfusion in the brain (cerebral blood flow, CBF) from contrast-enhanced dynamic MR imaging data. Still, the theory on tracer dynamics covered here will also be of relevance in general perfusion studies using other image modalities.

While hardware limitations in medical imaging for decades have confined studies to only handle larger tissue regions or full organs, modern MR technology and voxel based analysis give rise to aspirations about detailed perfusion maps with millimeter precision. Examples of estimated parameter maps are found in i.e. [?]. The quantitative perfusion maps (and other parameter maps arising from tracer kinetic modelling) can be combined with anatomical information, and the maps have proven to be of particular value in e.g. stroke studies for localization of trauma [?]. Among the physiological parameters

obtainable from tracer kinetic models, CBF has proven to be particularly difficult to reliably describe on a voxel-basis [4]. In several studies, CBF is therefore only reported in relative values and the corresponding parameter maps are mostly used in a qualitative manner [5]. The methodological limitations in perfusion estimations are caused both by issues in the numerical implementation, but also by over-simplified dynamic models. It has been widely studied how delay and dispersion of the contrast bolus between the AIF and the voxel as well as assumptions about directional flow [6, 7] effects the perfusion estimation. Still, even though the validity has not been established, voxel wise estimates of CBF are extensively reported in the literature [8, 9, 10, 11, 12].

In [7], a mathematical theory for voxelwise perfusion is introduced and proposed as an alternative to the classical ROI (region of interest) based models for perfusion. In this work, we will use some of the same physical concepts introduced for voxelwise perfusion, and relate them to the classical ROI based perfusion models. We will further discuss limitations of classical models applied voxel wise, and study their validity in an unstructured flow field. The pharmacokinetic models, and how they behave under different ROI/voxel sizes and shapes, are analyzed mathematically and evaluated within a synthetic flow field. A mathematical framework is also derived, in which the medical notion of perfusion can be understood in a physically more precise manner.

Evaluation of perfusion models using a synthetic flow field is also performed in i.e. [13]. Here, the synthetic model is based on solution of Navier-Stokes equations within the arterial system and the effect of dispersion is studied. In the present work, we model the contrast agent (CA) propagation through a small section of the capillary system. Both these approaches require several clarifying assumptions on flux and propagation. In pharmacokinetic analysis it is often assumed that each ROI (voxel) is an autonomous system that can be modeled by standard pharmacokinetic theory [?]. As in [13], we study CA propagation through a larger area with a highly developed capillary/arterial system and thereby consider a range of connected problems where each voxel can be regarded as an inlet for the surrounding voxels. This more accurately mimics the nature of blood flow in the tissue. Unlike Calamante et al. [13] we also distinguish between scalar perfusion maps, describing flow normalized over a volume, and the physical, vector valued flux field, describing flow normalized over a surface area.

The rest of this paper is arranged as follows: In Section 2, we outline classical methods for perfusion estimation and discuss two widespread solution methods. In Section 3 we describe how a synthetic flow field in the capillary system can be modelled using simple models valid within porous media. We also discuss mathematical similarities between the flow field models and the classical theory outlined in Section 2. **Some missing sections here?** In Section 6 we evaluate the performance of classical models by applying them to the synthetic flow field. The results and concluding remarks are summarized in Section 6.

## 2 Classical Models for perfusion

Classical theory for pharmacokinetic modelling is used to recover CBF, cerebral blood volume (CBV), as well as mean transit times (MTT) from data displaying propagation of a contrast agent through the tissue. The so-called deconvolution model (DM) is used in vast amount of publications [14, 15, 16, 17, 18]. Restoration of CBF yields reasonable results [?], however validation is a problem as ground-truth CBF is hard to determine. Validation of novel implementations is usually done in the so-called *inverse crime* setting. This means that the forward model used to generate data and the backward model to reconstruct parameters are similar, if not identical. However, the physical validity of the model can still be questionable. Another model for perfusion which has been used for restoring CBF and MTT is the so-called maximum slope model (MS) [19, 20]. The maximum slope model only considers early time points and it has been shown to exhibit advantages over the deconvolution model especially if uptake curves are degraded in the late phase [15]. However, since it relies on point-wise estimates, application to real data is nevertheless difficult and prone to noisy measurements. Also, the maximum slope model inherently assumes that no outflow takes place when the AIF peaks (see Sec. 2.2). This assumption is questionable for arbitrary, maybe pathological tissue.

The classical perfusion models consider the tracer concentration  $C(t)$  within a defined compartment, with a compartmentalisation ranging from voxels to entire organs. On the other hand, a field model always describes the tracer concentration locally as  $C(x, t)$ . As a issue on notation, when classical models are discussed the tracer concentration  $C$  refers to a spatial average  $C(t) \leftarrow (1/|\Omega_i|) \int_{\Omega_i} C(x, t) dx$  where  $\Omega_i$  can be compartments ranging from single voxels to larger ROIs.

Following [18], we now briefly present the common theoretical basis of two the models. Let  $\Omega_i$  be a control volume with one inlet and one outlet and let  $C(t)$  denote the average CA concentration within  $\Omega_i$  at timepoint  $t$ . These assumptions lead to the differential equation  $C'(t) = Q_a c_a(t) - Q_v c_v(t)$ , reflecting mass balance of the tracer. Here  $c_a, c_v$  are the CA concentrations at the inlet and outlet of  $\Omega_i$ , and  $Q_a, Q_v$  are the corresponding volume fluxes at these locations. Assuming incompressibility of flow leads to  $Q_a = Q_v$  and hence we obtain the general form

$$C'(t) = Q_a (c_a(t) - c_v(t)). \quad (1)$$

In the next step, the deconvolution model and the maximum slope model are diverging based on different assumptions.

### 2.1 The Convolution Model: Theory and Implementation

For the deconvolution model it is assumed that there is a probability distribution of transit times  $h(t)$  through  $\Omega_i$ . This leads to

$$c_v(t) = (h * c_a)(t) := \int_0^t c_a(s) h(t - s) ds. \quad (2)$$

Combining this with (1) yields  $C'(t) = Q_a c_a(t) - Q_a (h * c_a)(t)$ . Integrating this equation and using basic properties of the convolution one obtains

$$C(t) = (I * c_a)(t). \quad (3)$$

Here the *impuls-response function*  $I$  is defined as  $I(t) := Q_a(1 - \int_0^t h(s) ds)$ , and it fulfills the following properties:

- $I(0) = Q_a$ ,
- $I$  is monotonously decreasing,
- $I \geq 0$ .

The task of identifying  $I(t)$  given a tissue curve  $C(t)$  and an arterial input function  $c_a(t)$  is a deconvolution problem. If  $I(t)$  is recovered,  $Q_a$  can subsequently be estimated as  $Q_a = \max_t I(t)$ . There are several methods to perform the deconvolution. A standard approach using Fourier-based algorithms is sensitive to the presence of noise [14, 21]. Another class of deconvolution algorithms gaining increasing attention are based on Bayesian modeling [22, 23]. Recent evaluations are showing good performance [24], however the numerical handling is still difficult since complex and error-prone numerical integration has to be performed. The most popular among deconvolution algorithms are based on singular value decomposition (SVD) [14]. These algorithms have shown to be robust for a reasonable noise level. Also, they can be easily adapted to be robust against delays in tracer arrival using block-circular structures (bSVD cf. [25]). In order to identify the impuls-response function  $I(t)$  from simulated data, we hence decided to use the bSVD model as proposed in [25].

Both CBV and  $\phi$  describe the relative fluid volume of a control volume, and they are therefore essentially equal. Our digital phantom introduced later has a very clear physical interpretation from geophysics, and we therefore decided to use the notation of porosity  $\phi$  instead of CBV. If we make the assumption of  $\Omega_i$  as a well-mixed compartment where  $C(t) = \phi c_v(t)$  for a  $0 \leq \phi \leq 1$ , equation (1) reduces to the initial value problem

$$\begin{aligned} (\phi c_v)' &= Q_a c_a - Q_a c_v, \\ c_v(0) &= 0, \end{aligned} \quad (4)$$

where we also assume no tracer within the compartment for  $t = 0$ .

Denote the mean transit time  $T := Q_a/\phi$  for  $\phi \neq 0$ , and (4) yields the solution

$$C(t) = Q_a \int_0^t e^{-(t-s)/T} c_a(s) ds \quad (5)$$

with the impulse response function  $I(t) = Q_a e^{-t/T}$ .

## 2.2 The Maximum Slope Model

In the MS model it is assumed that at the beginning when  $c_a$  peaks, only a negligible amount of CA is leaving the system (cf. [20]). For this time interval equation (1) reduces to

$$C'(t) = Q_a c_a(t), \quad (6)$$

in case one can see that if  $c_a$  has a maximum, also  $C'$  must have a maximum since stationarity in  $Q_a$  is assumed. Hence, it holds that

$$Q_a = \frac{\max_t C'(t)}{\max_t c_a(t)}. \quad (7)$$

## 3 A Synthetic Model for Capillary Perfusion

Structurally, the model-assumptions for both classical methods presented in Section 2 are similar. The validity of both methods rely on a ROI having only one inlet and one outlet, and that the CA concentration is well mixed within the entire compartment. In fact, the assumption of one inlet and one outlet is questionable when we locally describe CA propagation through a larger area with a highly developed capillary system. For this type of model system we expect instead a set of coupled equations where each voxel can be regarded as an inlet for surrounding voxels. Hence, in order to make a realistic synthetic model for capillary flow, we decided to describe the CA propagation as a spatially coupled transport process. This synthetic field model is used for validation of the classical models for perfusion.

Within the porous capillary system we expect the blood flow to be driven mainly by pressure differences as modelled by Darcy's law [?]. Traditional tracer kinetic modelling is using volume normalized fluid flow with units  $[\text{mm}^3/\text{s}/\text{mm}^3]$  as a quantity to describe fluid transport. However, the concept of volume normalized fluid flow is discretization dependent, and for the current flow simulations we instead use vector valued surface fluid flux  $q = q(x)$  with units  $[\text{mm}^3/\text{s}/\text{mm}^2]$ , in agreement with geoscience and reservoir simulation theory. The fluid flux is a vector field describing the volume of fluid per unit time flowing across a sliced unit area of the sample. A model to convert vector valued flux to scalar valued perfusion with units  $[\text{mm}^3/\text{s}/\text{mm}^3]$  will be introduced in Section 3.5. The tracer flux is assumed to be a product of the fluid flux and the CA concentration,  $c(x, t)q(x)$   $[\text{mmol}/\text{s}/\text{mm}^2]$ . Apart from the normalization with respect to surface, the assumptions of linearity and stationarity in the fluid flux are in complete agreement with standard pharmacokinetic modeling [18]. We will now describe the construction of the digital phantom in detail.

### 3.1 Modelling the Capillary Blood Flow

We model the blood flow as a fluid flow through a porous medium. The fluid density  $\rho$  [mg/mm<sup>3</sup>] is denoted by  $\rho = \rho(x, t)$ . The flux  $q$  [mm<sup>3</sup>/s/mm<sup>2</sup>] as well as the porosity  $\phi$  are assumed to be stationary and hence independent of time. Fluid entering and leaving the system is described by a source- and sink term  $\tilde{Q} = \tilde{Q}(x)$  [mg/s/mm<sup>3</sup>]. The continuity equation describing conservation of fluid mass states

$$\frac{\partial(\phi\rho)}{\partial t} + \nabla \cdot (\rho q) = \tilde{Q}. \quad (8)$$

Furthermore, assuming that the fluid flow is steady-state and that the density of blood  $\rho$  is constant in space, we obtain

$$\nabla \cdot q = \frac{\tilde{Q}}{\rho}. \quad (9)$$

In order to scale away the density  $\rho$  we define another source term  $Q$  [mm<sup>3</sup>/s/mm<sup>3</sup>] having the relation  $\tilde{Q} := Q\rho$ , thus transforming (9) into

$$\nabla \cdot q = Q \quad (10)$$

where the right hand side is a volume flux, only non-zero within the source or the sink locations. Elsewhere, (10) is concurrent with divergence free flow of an incompressible fluid.

Low velocity fluid flux in porous media is described by Darcy's law [26]

$$q = -\frac{\mathbf{k}}{\mu}(\nabla p + \rho g \nabla z). \quad (11)$$

Here  $g$  is the gravitational acceleration,  $\mathbf{k}$  [mm<sup>2</sup>] is the permeability tensor,  $z$  is the spatial position along the gravitational field,  $p$  [kPa] is the pressure, and  $\mu = \mu(x)$  [kPas] is the viscosity of the fluid. For the current synthetic model, the flux field is chosen to be perpendicular to the gravitational field and the gravitational term can thereby be discarded,

$$q = -\frac{\mathbf{k}}{\mu} \nabla p. \quad (12)$$

Equations (10) and (12) can be combined, and further it is assumed that  $\mathbf{k}$  is a symmetric and positive definite tensor with only nonzero diagonal elements  $\mathbf{k}_{ii} = k$ . This yields the following elliptic partial differential equation in the pressure-field  $p$ ,

$$\left| \begin{array}{ll} \nabla \cdot \left( -\frac{k}{\mu} \nabla p \right) = Q & x \in \Omega, \\ n \cdot \nabla p = 0 & x \in \partial\Omega \end{array} \right| \quad (13)$$

where we also added Neuman boundary conditions reflecting zero fluid flux  $q(x)$  across  $\partial\Omega$ . Here,  $\partial\Omega$  denotes the boundary of  $\Omega$  and  $n$  the outward unit normal vector. Note that (13) defines a solution which is only unique up to constant [27]. After solving (13), the flux field can be computed according to (12) from the obtained pressure map.

### 3.2 Modelling Indicator Dilution in the Flux Field

This section describes how the CA propagates in the tissue as it is dissolved in the evolving fluid. We assume that the CA is entering the domain along with the fluid flowing in via the source, and similarly extracted at a sink. The resulting CA concentration map is a simulation of the CA concentration one would observe within MRI measurements.

In order to define meaningful continuous contrast agent concentrations, we first describe the average CA concentration in an (arbitrarily) small tissue volume  $\Omega_i$  where  $C_i(t) := C(x_i, t)$  and  $\phi_i := \phi(x_i)$  are assumed to be constant within  $\Omega_i$ . Assume that  $V_i$  is the volume of  $\Omega_i$  and  $v_i$  the blood volume within  $\Omega_i$ . By definition, porosity is given by  $\phi_i = v_i/V_i$ . Let  $C_i(t)$  denote the CA concentration in  $\Omega_i$  with respect to the whole volume  $V_i$  at timepoint  $t$ . The CA concentration with respect to the blood volume  $v_i$  is denoted by  $c_i(t)$ . From the definition of  $c_i, C_i$  and  $\phi_i$  we obtain the relation  $C_i(t) = \phi_i c_i(t)$ . The rate of change of tracer molecules within the control volume  $\Omega_i$  can be phrased as

$$\frac{d}{dt} \int_{\Omega_i} C_i(t) dx = \int_{\Omega_i} \frac{d}{dt} (\phi_i c_i(t)) dx = \int_{\Omega_i} \phi_i \frac{dc_i}{dt} dx. \quad (14)$$

where the assumption of stationary  $\phi_i$  was used. Since we expect mainly transport along the vessels and marginal diffusion, the change in tracer mass within  $\Omega_i$  occurs only from advective flow and the source and sink field  $Q$ . Let us write the source- and the sink term as  $Q = Q_{\text{si}} + Q_{\text{so}}$  where  $Q_{\text{si}} < 0$  is the sink and  $Q_{\text{so}} > 0$  is the source. Both are assumed to be zero everywhere except at in the respective source and sink locations. Note that  $\int_{\Omega} Q dx = 0$ . The change in contrast agent at time point  $t$  can be written as

$$- \int_{\partial\Omega_i} c_i(t) (q_i \cdot n) ds + \int_{\Omega_i} c_a(t) Q_{\text{so},i} dx + \int_{\Omega_i} c_i(t) Q_{\text{si},i} dx, \quad (15)$$

where  $n$  is the outward unit normal on  $\partial\Omega_i$ . In standard pharmacokinetic modeling,  $c_a$  is referred to as the arterial input function (AIF). From the principle of conservation of tracer molecules, equations (14) and (15) must balance such that

$$\int_{\Omega_i} \phi_i \frac{dc_i}{dt} dx + \int_{\partial\Omega_i} c_i(t) (q_i \cdot n) ds = \int_{\Omega_i} c_a(t) Q_{\text{so},i} dx + \int_{\Omega_i} c_i(t) Q_{\text{si},i} dx. \quad (16)$$

Now, let the contrast agent concentrations, porosity, volume fluxes, and surface flux be continuous functions of space and time. Equation (16) is then consistent with the continuity equation on local form

$$\left| \begin{array}{ll} \phi \frac{\partial c}{\partial t} + \nabla \cdot (cq) = c_a Q_{\text{so}} + c Q_{\text{si}} & x \in \Omega, t > 0, \\ c(x, t) = 0 & x \in \Omega, t = 0. \end{array} \right| \quad (17)$$

where we also added the initial value  $c(x, 0) = 0$  to ensure uniqueness. Equation (17) is a linear transport equation in  $c(x, t)$ . Following [27], equation (17) admits a unique local solution.

### 3.3 Relating the transport equation model with the classical deconvolution model for perfusion

Consider the solute transport equation (17), and rewrite it as

$$\frac{\partial c}{\partial t} + \frac{q}{\phi} \cdot \nabla c = \frac{(c_{so} - c)Q_{so}}{\phi}. \quad (18)$$

for a nonzero  $\phi$ , and where we used (10) and  $Q = Q_{so} + Q_{si}$ . We follow the method of characteristics and convert from Eulerian coordinates  $(x, t)$  to Lagrangian coordinates  $(x_0, t)$ , where  $x_0$  corresponds to the beginning of a streamline for  $t = t_0$ . The parameterization parameter for the streamline emerging at  $(x_0, t_0)$  is denoted by  $s$ . Substituting  $x = x(s)$ ,  $t = t(s)$  and denoting  $c(s) := c(x(s), t(s))$ ,  $Q_{so}(s) := Q_{so}(x(s))$ ,  $\phi(s) := \phi(x(s))$  and  $c_a(s) := c_a(t(s))$  yields the following system of ODEs [27]:

$$c'(s) + \frac{Q_{so}(s)}{\phi(s)}c(s) = \frac{c_{so}(s)Q_{so}(s)}{\phi(s)}, \quad c(0) = 0 \quad (19a)$$

$$x'(s) = \frac{q(s)}{\phi(s)}, \quad x(0) = x_0 \quad (19b)$$

$$t'(s) = 1, \quad t(0) = t_0, \quad (19c)$$

The notation  $c'(s)$  refers to the total derivative (material derivative) of  $c$  with respect to the parameterisation  $s$ . The solution variable  $c(s)$  can be regarded the concentration curve of a particle which originated at  $(x_0, t_0)$  and where  $(x(s), t(s))$  is the wavefront at artificial time point  $s$ .

Equation (19a), which governs the behaviour along the streamline, has the general solution

$$c(s) = \int_0^s e^{-(R(s)-R(v))} c_{so}(v) \frac{Q_{so}(v)}{\phi(v)} dv. \quad (20)$$

Here  $R(v) = \int_0^v Q_{so}(x(u))/\phi(x(u))du$ . We can interpret  $R(v)$  as the amount of contrast agent which is accumulated within the source field  $\Omega_{so}$  while a particle moves through the source field. **Can we? There is no contrast involved in  $R(v)$ . I think its rather accumulation of flow** If we now assume that the source volume  $\Omega_{so}$  is small, the particle is not accumulating tracer. **Hmm, in this case I interpret (20) the following way: If  $\Omega_{so}$  is small, it holds that  $R(s) = k$  for all  $s$  which are bigger than some  $s_0$  (if the particle has left the source-field after timepoint  $s_0$ , no additional tracer is accumulated). In this case the exponential term becomes  $e^{-(k-R(v))}$  for all  $s > s_0$ . This means that for  $v > s_0$  the exponential term will become 1 and the rest of the integral will become 0, since  $Q_{so}(v) = 0$ . Hence it holds that  $c(s) = k_2$  for all  $s > s_0$  and for some constant  $k_2 > 0$ . The case considered below corresponds to  $Q_{so}(x) = Q_a$  for all  $x \in \Omega$ , since in this case  $R(v) = Q_a v$ .**

The integral (20) can be written as

$$c(t) = \int_0^{t_1} e^{-(R(t_1)-R(s))} c_{so}(s) \frac{Q_{so}(s)}{\phi(s)} ds. \quad (21)$$



Later time points will not contribute since here  $Q_{so} = 0$  at these locations. Denote the mean transit time as  $T := \phi/Q_{so}$ , and use the assumption of constant source term within  $\Omega_{so}$ , such that

$$c(t) = \int_0^{t_1} e^{-(t_1-s)/T} c_{so}(s) \frac{Q_{so}(s)}{\phi(s)} ds. \quad (22)$$

Now, let the source field  $Q_{so}$  be positive everywhere within  $\Omega$ , such that  $\Omega_{so} = \Omega$ ,

$$c(t) = \int_0^t e^{-(t-s)/T} c_{so}(s) \frac{Q_{so}(s)}{\phi(s)} ds. \quad (23)$$

Backpropagating  $C = c\phi$ , and emphasising the dependency of  $x_0$  results in

$$C(x_0, t) = Q_{so}(x_0) \int_0^t e^{-(t-s)/T} c_{so}(x_0, s) ds \quad (24)$$

A comparison with (5) shows that these expressions are equal provided  $Q_a \rightarrow Q_{so}$  and  $c_{so} \rightarrow c_a$ . Thus, we have shown that the classical model is equivalent to a (voxelwise) field model for tracer transport in accordance with: (i) The source term must be positive everywhere in the domain, such that  $\Omega_{so} = \Omega$ . This is equivalent to having an arterial input which is equal for all sub-units, which is generally not the situation in a real-world scenario. (ii) The source term and the porosity must be constant within entire  $\Omega_{so}$ . Constant porosity is reasonable to assume, but constant source term is challenging since it requires (i) to be fulfilled.

### 3.4 Relating the Classical Method and the Digital Phantom

In order to test the standard models for their abilities to restore CBF and CBV, we need to convert the flux  $q$  with units  $\text{mm}^3/\text{s}/\text{mm}^2$  to perfusion  $Q$  with units  $\text{mm}^3/\text{s}/\text{mm}^3$ . A method to do that will be presented in Section 3.5. In Section 3.6 we will give an analytical proof that the local porosity can be estimated from the standard relationship  $\phi(x) = (\int_0^\infty C(x, s) ds) / (\int_0^\infty c_a(s) ds)$ .

### 3.5 Converting Flow to Perfusion

The model described in (12) - (13) uniquely determines the flux field  $q(x)$ . However, in pharmacokinetic modeling the parameter of interest is usually the CBF, which we will denote by  $Q(x)$  as the voxel wise field of perfusion. The surface flux and perfusion are physically distinct, and it is not obvious how to transform a vector flux field  $q(x)$  into a scalar perfusion field  $Q(x)$ . There are at least two differences between  $q(x)$  and  $Q(x)$ . First, the flux is a vector field and the perfusion is a scalar field. Second, the flux is normalized to a surface area and the perfusion is normalized to a volume. Thus, the surface flux and the perfusion are strictly, mathematically different but still conceptually related. In the following we describe a method for converting flux into perfusion. The other

way around, converting perfusion into flux has no obvious incentive since the vector flux field contains both scalar and directional information compared to the scalar perfusion field.

The common understanding of perfusion or volume flux  $Q(x)$  is the amount of blood feeding a tissue volume per unit time, with units  $[\text{mm}^3/\text{s}/\text{mm}^3]$ . For inter-subject comparison it is common to scale this quantity to normalized perfusion having units  $\text{ml}/\text{min}/100\text{ml}$ . One obvious approach for converting flux into perfusion could be to estimate the perfusion as the total inflow (or outflow) of fluid (e.g. arterial blood) into a control region per unit time, and then normalizing with the control region volume. This is a valid approach only if every control region is separated from other control regions and not feeding each other, and this approach is thereby well-founded for an entire organ. Such understanding of perfusion is in line with the theoretical foundation of classical compartment models for perfusion where a control region has its own source of feeding arterial blood, independent of the neighbor regions.

On the other hand, if the control region is a single voxel or a sub-division of an organ with common feeding arterial blood, the classical model assumptions are violated since every control region will feed its neighbours, thus becoming a coupled system of flow. Simply summing the total inflow into a voxel and dividing by the voxel volume will strongly over-estimate the perfusion since the normalization would refer to the wrong volume. The problematic issue is that the incoming blood is feeding more ROIs than the current ROI, and the perfusion values thereby become discretization dependent. This phenomenon is demonstrated in Fig. 1 where the volume on the left has the true perfusion of  $Q_1 = F_0/(2V)$  for an incoming flow  $F_0$   $[\text{mm}^3/\text{s}]$  and distribution volume  $2V$   $[\text{mm}^3]$ . However, for another discretization as shown in the middle, the perfusion within each of these sub-volumes becomes  $Q_2 = F_0/V = 2Q_1$ . Taking the average across the two sub-volumes, it is clear that the perfusion is over-estimated with a factor of two. A discretization dependent perfusion estimate is not recommendable, and the perfusion estimate of  $Q_2$  is clearly wrong.

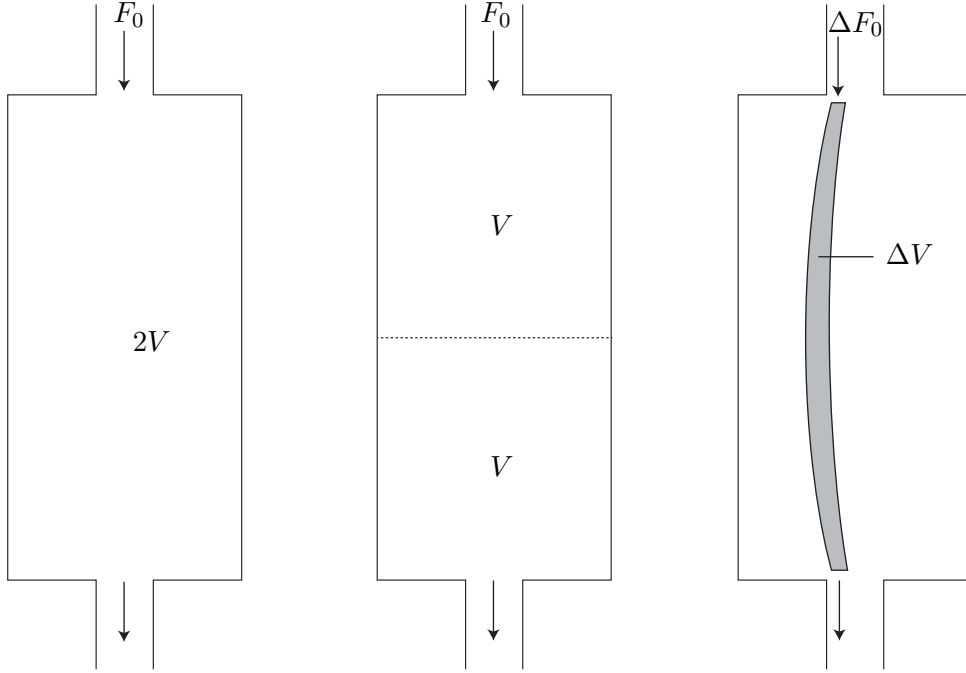


Figure 1: Perfusion within a small volume. Left: A compartment with volume  $2V$  is exposed to a flow  $F_0$  [ $\text{mm}^3/\text{s}$ ] of fluid. By definition, the perfusion within this compartment becomes  $Q_1 = F_0/(2V)$ . Middle: The same volume is divided into two compartments (e.g. voxels), and the perfusion for each of the compartments becomes  $Q_2 = F_0/V = 2Q_1$ . The discrepancy between the two discretizations occurs because the flow is counted twice as it is fed from one voxel to the other. Right: As a solution to the described problem we rather pick out a true distribution volume  $\Delta V$  (area in this 2D sketch), which is a small area around a given streamline along the centre line of the grey area. This is the true distribution volume (area in this 2D sketch) which is fed with arterial blood from the incoming fractional flow  $\Delta F_0$ . The correct perfusion within  $\Delta V$  is therefore  $\Delta F_0/\Delta V$ . The entire compartment can further be divided into similar infinitesimal distribution volumes, thus providing locally correct perfusion estimates.

The reason for the discrepancy is that  $Q_2$  has been counted twice since the voxels are coupled and we are dividing by the wrong distribution volume. The concept of perfusion has a very precise meaning, as the amount of arterial blood per time unit delivered to a capillary bed in a biological tissue, and then scaled by the fed tissue volume. Therefore, the incoming flow must be divided by the total distribution volume that is covered by the fluid streamlines. This formulation coincides with the classical understanding of perfusion, and the correct distribution volume will rather be the volume that the fluid particles within an infinitesimal cross-sectional area around the streamlines are covering. Assuming laminar flow, the streamlines are not crossing each other and we can estimate

the true distribution volume that is fed by a given arterial blood flow.

Let us fix a point  $y \in \Omega$  and consider the streamline crossing through  $y$ . For the time being, denote the flux along this streamline as  $q = q(s)$  for a parameterization  $s$  along the streamline, noting that the direction of the streamline is identical to the direction of the flux. Let  $A_\varepsilon$  be a 2-D disc with radius  $\varepsilon(s)$ , where  $A_\varepsilon$  is orthogonal to  $q(s)$  and the radius along the streamline is varying proportionally with the distance between a referencing neighbouring streamline. The volume flow [mm<sup>3</sup>/s] over the disc is independent of the position along the streamlines, and can be expressed as

$$F = \int_{A_\varepsilon} (q \cdot n) \, dA = \int_{A_\varepsilon} \left( q \cdot \frac{q}{\|q\|} \right) \, dA \quad (25)$$

for any  $0 \leq s \leq L$  where  $L$  is the length of the streamline, and thereby for any  $\varepsilon$  along the streamline. Provided  $q$  is continuous along the streamlines, we know  $\exists \tilde{\varepsilon}, 0 \leq \tilde{\varepsilon} \leq \max_s \varepsilon(s)$ , such that the volume  $V$  of the tube can be expressed as  $V = \tilde{\varepsilon}^2 \pi L$ . Hence we can express the perfusion  $Q_\varepsilon$  for the sub volume  $V$  as

$$Q_\varepsilon = \frac{F}{V} = \frac{1}{\tilde{\varepsilon}^2 \pi L} \int_{A_\varepsilon} \left( q \cdot \frac{q}{\|q\|} \right) \, dA. \quad (26)$$

Letting  $\tilde{\varepsilon} \rightarrow 0$  and using the relation  $F/(\tilde{\varepsilon}^2 \pi) \rightarrow \|q\|$  provided  $q$  is continuous, yields a locally defined value for the perfusion  $Q(y)$

$$Q(y) = \frac{\|q(y)\|}{L}. \quad (27)$$

We note that (26) is valid for any  $0 \leq \tilde{\varepsilon} \leq \max_s \varepsilon(s)$  since both  $F$  and  $V$  are independent of  $\varepsilon$ , and relation (27) is thereby valid for any position along the streamline. Equation (27) is an explicit formula for converting flux into perfusion and is later used for evaluation of the classical model for perfusion.

### 3.6 A Method to Estimate local Porosity

It is known from literature on classical models for perfusion that CBV for the entire compartment can be expressed as

$$\phi = \frac{\int_0^\infty C(t) dt}{\int_0^\infty c_a(t) dt}. \quad (28)$$

where  $C(t)$  are the tracer concentration within a well mixed compartment and  $c_a(t)$  is the tracer concentration of the arterial input. However, it is not obvious that (28) is valid also for a continuous field model where the voxels are feeding each other. We will now proof that (28) is nevertheless valid.

Returning to the local definition of fluid tracer concentration as  $c(x, t)$ , the PDE in (17) is consistent with

$$\phi \frac{\partial c}{\partial t} = -q \cdot \nabla c. \quad (29)$$

for locations  $x$  where  $Q(x) = 0$ . Integrating from  $t_0$  to  $t_1$  results in the model

$$\phi[c(x, t_1) - c(x, t_0)] = - \int_{t_0}^{t_1} q \cdot \nabla c \, dt. \quad (30)$$

Approaching the limit  $t_0 = 0, t_1 = \infty$ , using the boundary conditions  $c(x, 0) = c(x, \infty) = 0$  and defining  $E(x) := \int_0^\infty c(x, t) \, dt$  leads to

$$0 = q \cdot \nabla E(x). \quad (31)$$

We can interpret this equation such that  $q$  lies parallel with the level-sets of the function  $E(x)$ , which means that  $E(x)$  is constant along the streamlines of the fluid flow, and thereby also valid when approaching the source  $\Omega_{Q_{so}} = \{x : Q_{so}(x) > 0\}$  along the streamlines:

$$\int_0^\infty c(x, t) \, dt = \lim_{x \rightarrow \Omega_{Q_{so}}} \int_0^\infty c(x, t) \, dt. \quad (32)$$

Using  $C(x, t) = \phi(x)c(x, t)$  we obtain

$$\phi(x) = \frac{\int_0^\infty C(x, t) \, dt}{\lim_{x \rightarrow \Omega_{Q_{so}}} \int_0^\infty c(x, t) \, dt}. \quad (33)$$

For all practical applications with a source field  $\Omega_{Q_{so}}$  of limited extension and homogeneous and simultaneous CA input one can replace the denominator by  $\int_0^\infty c_a(t) \, dt$ . Equation (33) for porosity coincides with the classical formula (28) for  $\phi$  and is hereby proven analytically also for local estimations of the porosity  $\phi$ .

## 4 Numerical Implementations of the Synthetic Model for Capillary Perfusion

In this section we describe how the models were implemented numerically. For simplicity the domain is discretized by a regular cartesian grid of size  $n \times n$  with a regular cell-spacing  $h$ . The proposed method may be extended for non-regular grids in an analogous fashion.

To solve (13) we used the two-point flux approximation finite volume method (TPFA) [?]. The transport equation (17) was solved by first order upwinding [28] applied to (16).

#### 4.1 Discretization of the Single Phase Flow Model using TPFA

Equation (13) was solved using the TPFA method widely used in reservoir mechanics [29]. Integrating (13) across a small domain (voxel)  $\Omega_i \subset \Omega$  and applying the divergence theorem yields

$$\int_{\partial\Omega_i} -(\lambda \nabla p) \cdot n \, ds = \int_{\Omega_i} Q \, dx \quad (34)$$

with conductivities  $\lambda := k/\mu$ . Defining  $\partial\Omega_{ij}$  as the boundary between neighboring voxels  $\Omega_i$  and  $\Omega_j$ , only the flux component perpendicular to  $\partial\Omega_{ij}$  will drive the flow between these voxels. The component of  $\nabla p$  pointing along the normal vector of  $\partial\Omega_{ij}$  can in terms of cell centered pressure values  $p_i$  and  $p_j$  be replaced by  $\Delta p_{ij} := (p_j - p_i)/h$ . Hence, the total flux across the face  $\Gamma_{ij}$  can be approximated by

$$\Delta p_{ij} \int_{\partial\Omega_{ij}} \lambda \, ds \approx (p_i - p_j) \underbrace{\frac{\lambda_{ij} |\partial\Omega_{ij}|}{h}}_{:=t_{ij}}. \quad (35)$$

Here,  $\lambda_{ij}$  denotes an approximation of the mean conductivity on  $\partial\Omega_{ij}$ , where  $\lambda_{ij}$  is computed by harmonic averaging from the requirement of continuity in  $p$  on the mid-line of  $\partial\Omega_{ij}$ . The terms in (35) not depending on the pressure  $p$  are collected into the transmissibilities  $t_{ij} := |\partial\Omega_{ij}| \lambda_{ij}/h$ . Approximating the right hand side of (35) as  $\int_{\Omega_i} Q \, dx \approx Q_i |\Omega_i|$  yields a linear system which can be solved for the pressure  $p$ . Due to the Fredholm alternative, we imposed Dirichlet boundary conditions for one voxel within  $\Omega$  to ensure uniqueness. Note that  $p, k, Q$  and  $\mu$  are defined cell-centered whereas the resulting flux  $q$  is discretized on a staggered grid, corresponding to the voxel faces.

#### 4.2 Discretization of the Transport Equation

The transport described in (16) was implemented using first order upwinding [28]. Let  $c_{ij}$  be a cell centered voxel tracer concentration with respect to the fluid volume on the cell face  $\partial\Omega_{ij}$  adjacent to voxel  $i$  and voxel  $j$ , and let  $n_{ij}$  be the outer normal vector of  $\partial\Omega_{ij}$ . Also, the cell staggered fluid flux is represented as a vector  $q_{ij}$ . The total CA-flux over the face  $\partial\Omega_{ij}$  for any time point was approximated by

$$\int_{\partial\Omega_{ij}} c_{ij} (q_{ij} \cdot n_{ij}) \, ds \approx \begin{cases} c_i q_{ij,n} |\partial\Omega_{ij}| & \text{if } q_{ij,n} \geq 0, \\ c_j q_{ij,n} |\partial\Omega_{ij}| & \text{if } q_{ij,n} < 0, \end{cases} \quad (36)$$

where  $q_{ij,n} = q_{ij} \cdot n_{ij}$  is the normal component of the flux across  $\partial\Omega_{ij}$ . Keeping track of in- and outflow for each voxel yields an explicit discretization scheme to set up the transport simulation. We used a time step of  $\Delta t = 0.002s$  in a forward Euler time stepping of (16). A conversion of  $c_i$  into  $C_i$  was performed via the relation  $C_i = c_i \phi_i$ . The overall concentration map  $C_i$  was later used for the inverse problem of restoring CBV and CBF.

We chose a standard arterial input function [14], a gamma-variate [30] function

$$c_a(t) := D_0(t - t_0)^\alpha e^{-(t-t_0)/\beta} \quad (37)$$

for  $\alpha = 3$ ,  $D_0 = 1$ ,  $\beta = 1.5$  s and  $t_0 = 0$  s.

## 5 Numerical Experiments and Results

### 5.1 Parameter settings

Based on (13) and (17) we set up a forward simulation of blood-flow and indicator dilution through the capillary system. An overview of parameter settings used for the numeral simulations are shown in Table 1. Total inflow within the source is denoted  $F_{so} = \int_{\Omega} Q_{so}(x)dx$ , as well as for the sink  $F_{si} = \int_{\Omega} Q_{si}(x)dx$ . We chose an average input perfusion of 50ml/min/100ml, which can be converted into a flow of  $F_{so} = 0.83$  mm<sup>3</sup>/s for the closed domain  $\Omega = \{x = (x_1, x_2, x_3) : 0 \leq x_1 \leq 10\text{mm}, 0 \leq x_2 \leq 10\text{mm}, 0 \leq x_3 \leq 1\text{mm}\}$ .

Table 1: Parameters used in the numerical experiments, optimized for a slab of the capillary system in the human brain. In order to achieve a transparent simulation, permeability was assumed to be isotropic, and both the permeability and porosity were assumed to be constant across the domain. A typical porosity of  $\phi = 0.05$  was chosen [31].

Description	Type	Symbol	Value(s)	Unit
Surface flux	Vector	$q$	-	mm <sup>3</sup> /s/mm <sup>2</sup>
Average perfusion within $\Omega$	Scalar	$\bar{Q}$	50	ml/min/100ml
Volume flux/perfusion	Scalar	$Q$	-	mm <sup>3</sup> /s/mm <sup>3</sup>
Absolute flow in source, derived from $\bar{Q}$	Scalar	$F_{so}$	0.83	mm <sup>3</sup> /s
Absolute flow in sink	Scalar	$F_{si}$	$-F_{so}$	mm <sup>3</sup> /s
Volume flux in source, derived from $F_{so}$	Scalar	$Q_{so}$	34.13	mm <sup>3</sup> /s/mm <sup>3</sup>
Volume flux in sink	Scalar	$Q_{si}$	$-Q_{so}$	mm <sup>3</sup> /s/mm <sup>3</sup>
Concentration w.r.t. fluid space	Scalar	$c$	-	mmol/mm <sup>3</sup>
Concentration w.r.t. $\Omega_i$	Scalar	$C$	-	mmol/mm <sup>3</sup>
Fluid density blood [32]	Scalar	$\rho$	1	mg/mm <sup>3</sup>
Permeability	Scalar	$k$	$5 \times 10^{-6}$	mm <sup>2</sup>
Porosity / CBV [31]	Scalar	$\phi$	0.05	mm <sup>3</sup> /mm <sup>3</sup>
Spatial resolution	Vector	-	(64, 64, 1)	-
Physical FOV	Vector	-	(10, 10, 1)	mm
Voxel size	Vector	-	(0.156, 0.156, 1)	mm

We aimed at creating a transparent synthetic test case and kept all optional parameters as simple as possible. Therefore, permeability and porosity were assumed constant in

space and in time. The source term was assigned to the upper left voxel and the sink term was assigned to the lower right voxel.

## 5.2 Indicator dilution in the porous media and the convolution model

From the porous media model, streamlines were found from tracking of the flux vector field  $q$ , using a method closely related to FACT [33] used for tracking within DTI (Diffusion Tensor Imaging) for tractography. Both length and position of the streamlines was during the tracking process assigned. The voxel-wise perfusion field  $Q$  was calculated according to (27) using the computed streamline length and the flux field  $q$  from (12). The pressure field, the flux and voxel wise perfusion is displayed in Fig. 2. The flow field visualized in Fig. 2 (b) is vector flux integrated across cell surface,  $\int_{\partial\Omega_{ij}} q ds$  [mm<sup>3</sup>/s].

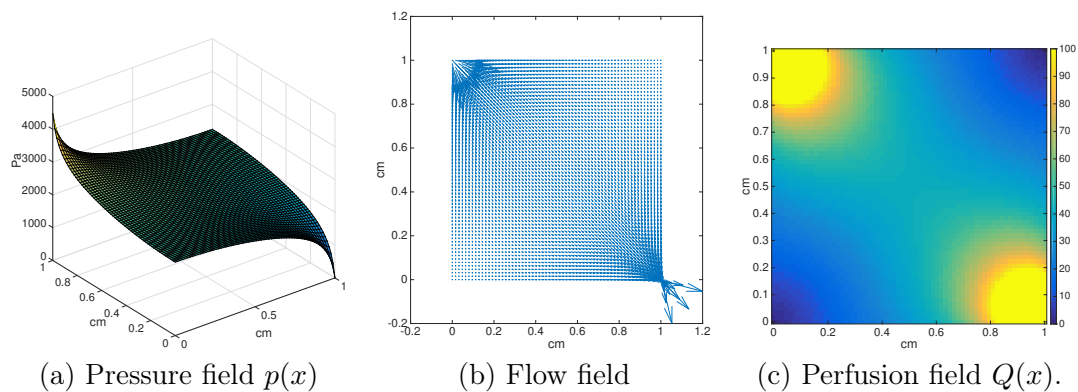


Figure 2: Porous media (PM) flow model with a source in the upper left corner and a sink in the lower right corner. (a) Pressure field [Pa] from solving the linear system in (13), (b) Flow field  $\int_{\partial\Omega_{ij}} q ds$  [mm<sup>3</sup>/s], (c) Voxelwise perfusion  $Q(x)$  [ml/min/100ml] according to (27).

Maps of CA concentrations were computed by two means. (i) First, by simulating the transport equation (16), and (ii) second by the forward convolution model (5). For (i), known values of flux, porosity, fluid density, and fluid flow within the source and sink were fed into the equation. We refer to this map as  $C_T(x, t)$ . For the forward convolution model (ii), the estimated voxelwise perfusion  $Q_i$  and the porosity were used for the simulations with known values of  $Q_a \leftarrow Q_i$ . We refer to this map as  $C_C(x, t)$ . A comparison of the tissue curves between  $C_T(x, t)$  and  $C_C(x, t)$  at different positions of the tissue can be found in Figure 3. Note that the convolution dataset was set up under the assumption that each voxel is a well-mixed compartment. Since one assumption of the maximum-slope model is that no outflow takes place during the peak of the AIF, we cannot expect the maximum slope model to recover perfusion on a voxel basis for  $C_C(x, t)$ .



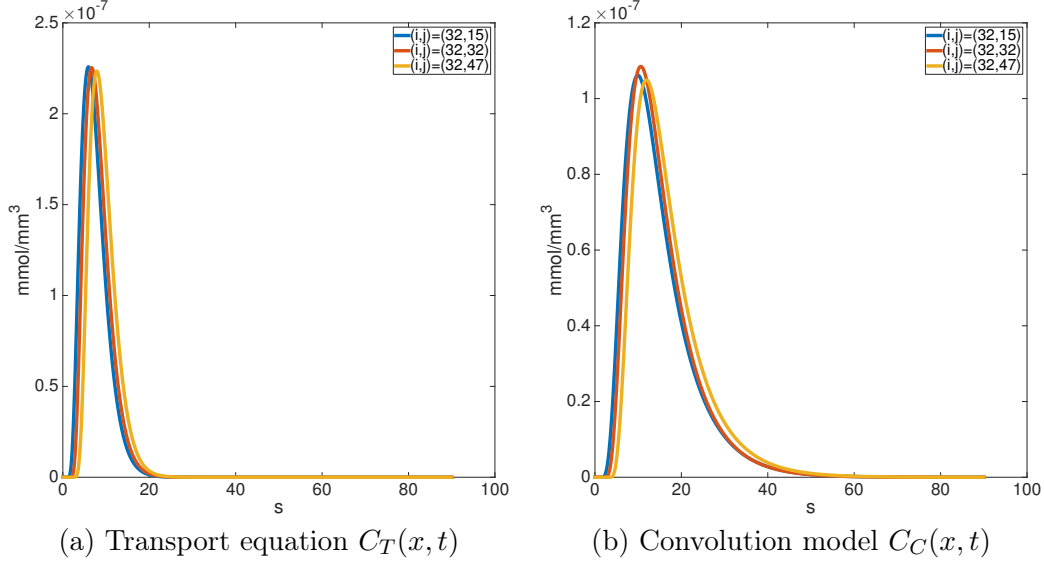


Figure 3: Comparison of tissue curves using the transport equation  $C_T(x, t)$  (a) and the convolution model  $C_C(x, t)$  (b). Curves were sampled in the middle row  $i = 32$  and columns  $j \in \{15, 32, 47\}$ . The convolution model creates a more dispersed signal compared to the transport equation.

### 5.3 Reconstruction of Perfusion by classical Models

We tested the the convolution based classical model (bSVD) (3) as well as maximum-slope (MS) model (7) for their capability to recover the perfusion values. Success of restoration was measured in terms of the relative error of the recovered perfusion with respect to the true perfusion,

$$RE := \frac{|Q_{\text{rec}} - Q_{\text{true}}|}{Q_{\text{true}}} \cdot 100\%. \quad (38)$$

Prior to reconstruction, the maps  $C_T(x, t)$  and  $C_C(x, t)$  of CA in time and space were downsampled to a time-resolution of 0.2s in order to stay within comparable time sampling existing on modern MR equipment for dynamic imaging. In order to simulate different spatial resolutions of the scanning process, the data was averaged using different block-sizes ranging from (1, 1) to (64, 64). Results are displayed in Figure 4 as well as in Table 2. Impulse response function reconstructed from the transport equation are displayed in Figure 5.

Table 2: Relative error  $RE$  (%) for reconstructing perfusion  $Q$ . Displayed is the median  $RE$ . Both reconstruction models MS and bSVD are able to restore the perfusion for the entire domain, but fail for smaller block sizes. The bSVD model is able to restore the voxelwise perfusion when it was generated by the convolution model.

Forward data	Reconstruction	Block Size (voxels)			
	model	(1,1)	(5,5)	(10,10)	entire domain
Transport equation	MS	170.09	165.03	158.57	2.65
	bSVD	859.06	768.58	664.84	1.25
Convolution model	MS	23.23	24.26	25.75	63.53
	bSVD	3.16	4.53	8.80	54.32

Table 3: Relative error  $RE$  (%) for reconstructing  $\phi$ . The porosity (CBV)  $\phi$  was computed according to (28). Relative error was computed block-wise as  $RE = |\phi_{\text{rec}} - \phi_{\text{true}}|/\phi_{\text{true}} \cdot 100\%$ . Displayed is the median  $RE$ . The reconstruction errors are small for all block sizes and both forward models.

Forward data	Block Size (voxels)			
	(1,1)	(5,5)	(10,10)	entire domain
Transport equation	$4.37 \cdot 10^{-5}$	$4.37 \cdot 10^{-5}$	$4.37 \cdot 10^{-5}$	$4.37 \cdot 10^{-5}$
Convolution model	$1.94 \cdot 10^{-2}$	$1.93 \cdot 10^{-2}$	$2.12 \cdot 10^{-2}$	1.13

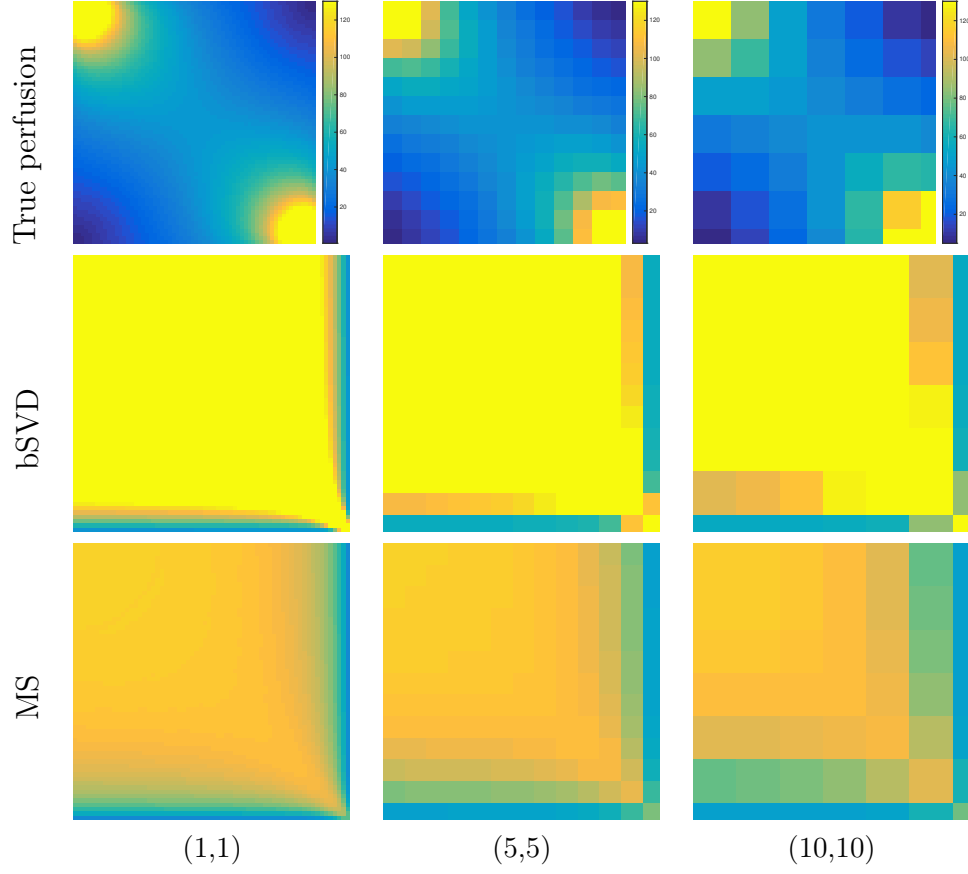
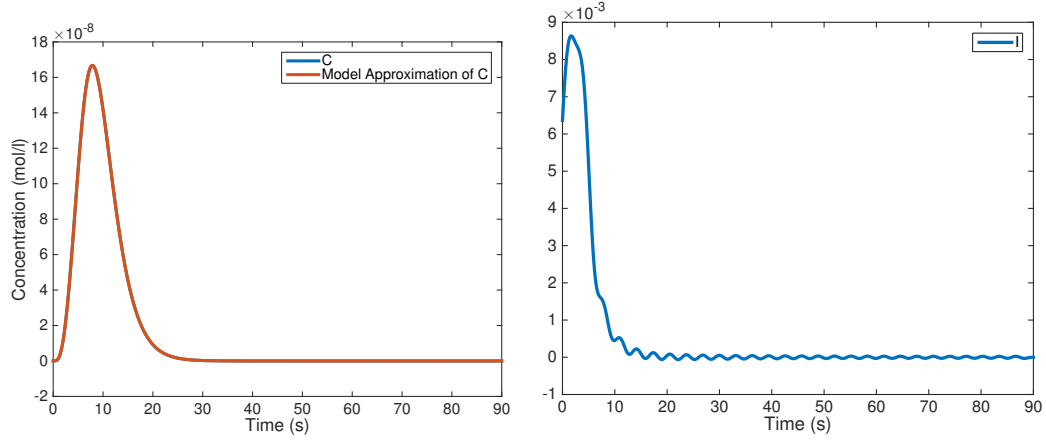
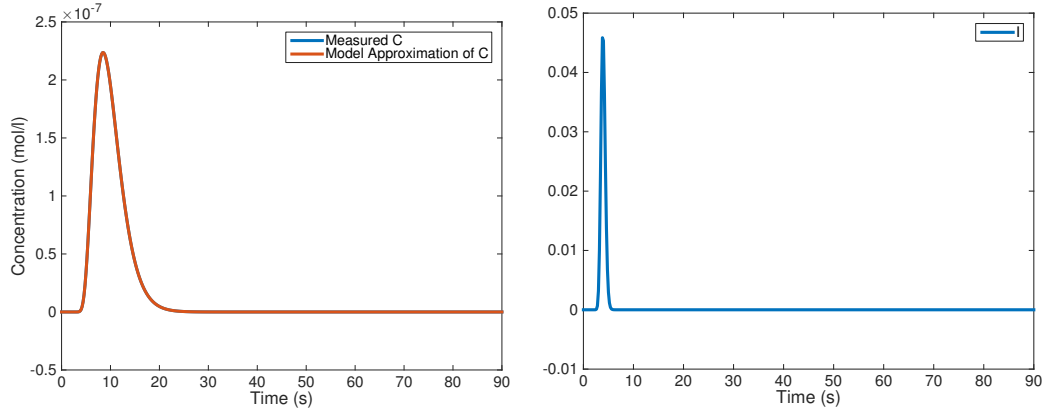


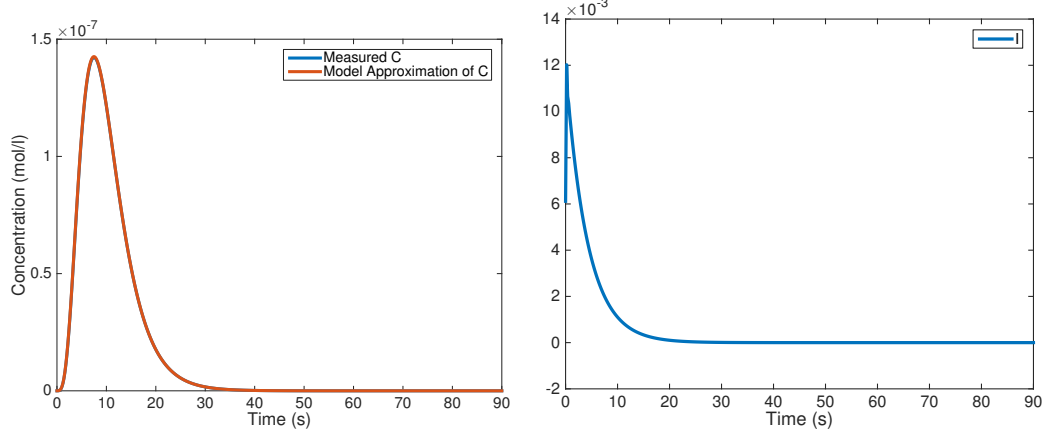
Figure 4: Restoring the perfusion for different levels of discretization, displayed within the columns. Block size in voxels is shown in brackets. All results are given in [ml/min/100ml]. First Row: Ground-truth perfusion (cf. Section 3.5). Second Row: Perfusion as estimated by bSVD. Third Row: Perfusion as estimated by the MS model. Both reconstruction methods fail in restoring the true perfusion, also reflected in the relative errors of Table 2.



(a) Entire Domain,  $C_T(x, t)$



(b) Inside the capillary bed,  $C_T(x, t)$  at  $(i, j) = (50, 50)$



(c) Inside the capillary bed,  $C_C(x, t)$  at  $(i, j) = (50, 50)$

Figure 5: Deconvolution by bSVD. First row: Results of bSVD applied to the map  $C_T(x, t)$  generated with the transport equation (16) using block-size (64,64) (i.e. entire domain). Second row: Results of bSVD applied to a single voxel of  $C_T(x, t)$  in the inside of the domain. Third row: Results of bSVD applied to a single voxel of the convolution data  $C_C(x, t)$  in the inside of the domain. In all cases the model restored the measured concentration curves almost perfectly. Left to right: Reconstructed concentration  $C(t)$  (left) and the impuls-response function  $I(t)$  (right).

## 6 Discussion

Accurate measurements of CBV, CBF and MTT within the brain can provide crucial information used in clinical decision making. Originally, the classical 1C models providing these parameters were developed for larger ROIs, and their validity for usage in field models has not properly been established. In this work we have developed a digital phantom for simulating blood flow within a slab of the capillary system. From the obtained flux field, we generate a perfusion map that was used to create two data sets of propagating concentration agent. The first data set was created as the solution of a linear transport equation, where every voxel acts as an arterial input to its neighbours. The other data set is based on a forward convolution model, where every voxel is exposed to the same arterial input function. The latter data set was mainly used to validate the numerical stability of the deconvolution methods, while the first data set was meant to represent a realistic data set as it can be obtained from a MR examination.

Considering the data set created from the transport equation,  $C_T(x, t)$ , the results presented in Table 2 indicate low errors or  $RE \leq 2.6\%$  of both the MS and the bSVD model for restoration of the perfusion when applied to the entire domain. Using an arterial input function valid for the region as a whole is in agreement with physical assumptions required to derive the theory for classical models. Thus, these results support the usage of classical compartment models for whole organs with only one inlet and one outlet.

However, the reconstruction of perfusion using MS and bSVD fails to a large extend with relative errors up to 859% for other block sizes than the entire domain, the error apparently increasing for smaller block size. This observation of over-estimation indicates that classical models for reconstructing perfusion are not valid for a situation where the global arterial input is not the correct arterial input for each of the smaller computational units. These results are also supported by the analytical analysis in Section 3.3, stating that the computed voxel wise perfusion computed by classical deconvolution methods is the actual perfusion at the arterial input, and not in the voxel itself. The observed over-estimation of perfusion is also predicted by the theoretical analysis, stating that the perfusion will be over-estimated with a factor proportional to the length of the streamlines.

Considering the data set created from convolution,  $C_C(x, t)$ , from Table 2 it is clear that the bSVD model for deconvolution has a low error of 2.43% for voxel wise reconstruction. This result is closely related to the previously described "inverse-crime" where we used the same model for constructing the data as for reconstruction. However, in our case it provides evidence that the deconvolution algorithm used, the bSVD, is numerically stable, and that errors in true perfusion are unlikely to arise from numerical instabilities of the deconvolution. This conclusion is also supported by Fig. 5, where the measured and the restored concentration curves are more or less identical for various block sizes and various input data. However, despite the success of restoring the concentration curves, the usage of a model in an "inverse-crime" settings can not be used to support the physical validity of the model, but only the numerical stability of the deconvolution in this case.

Interestingly, the MS model fails in restoring the perfusion for all block sizes of the forward convolution data. The reason for this is probably that within the MS model there is an assumption of no output of CA as the arterial input peaks. This assumption is clearly violated as the forward convolution model assumes an instantaneous transport of CA both into as well as out of the domain due to the assumption of well-mixed compartments.

Regarding the CBV estimates, one can observe from Table 3 that both data sets  $C_T(x, t)$  and  $C_C(x, t)$  could successfully be used to restore the CBV. Various block sizes also had little impact on the results. These results are in well agreement with the analytical proof of CBV in Section 3.6, stating that equation (28) is valid for entire organs as well as for single voxels. Thus, these results support the usage of (28) for computing the CBV with high accuracy for any type of block size, including single voxels.

In light of our current findings we want to focus on the usage of classical compartment models for voxel wise perfusion in the brain. Our results indicate the classical models should only be used for larger computational units where the arterial input is an actual arterial input for the domain as a whole. The development of new field models for perfusion is therefore highly demanded, in line with approaches described in [7].

With these conclusions in mind, our results are only valid for one-compartment systems like the brain with an intact blood-brain-barrier. For other organs or pathological situations with a leakage of tracer into the extravascular space, the observed effects described in this work are yet to be discovered.

Apparently, the true perfusion in a brain is unknown, and a gold standard is therefore not accessible for real data on a voxel wise basis. As an alternative, we propose to use simulated data sets like ours for benchmarking of new perfusion reconstruction algorithms. Applying various reconstruction methods to the same data set with a known ground truth would make it easier to compare and evaluate the performance.

Concluding, we have proposed a novel method to validate classical models for perfusion analysis. We have shown that within the assumption of a common arterial valid for the entire domain, classical models for restoring the perfusion are reliable. However, when sub-dividing the computational units into smaller ROIs, even down to voxels, significant errors are introduced. Furthermore, these errors are not likely to be related to the deconvolution method, but are rather related to violation of the physical model assumptions, and the computed perfusion will be over- or under-estimated with a factor proportional to the streamline length. Still, voxel wise perfusion estimates are extensively reported in the literature [8, 9, 10, 11, 12], even though the validity of used methods has not been established. In light of these results, future work should rather include the development of field models for perfusion measurements, taking into account the local constellation and neighbourhood of voxels. By these means one could develop reliable models also for voxel wise estimates. In this process it is useful to have benchmarking models for judging reliability of the models. We suggest that our simulated flow model could be used for such comparisons.

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