

Chapter 1

Thermal equilibrium - state when the macroscopic variables of two objects stop changing

→ achieved by an exchange of energy ← claim

temperature - is a measure of the tendency of an object to spontaneously give up energy

How do we measure temperature?

- volume (constant pressure) (mercury/alcohol)
- pressure (constant volume)
- electrical resistance
- thermal emf (thermocouple)
- radiation

HW#1 | 1, 2, 7

1.) $C_0 = 0$ $F_0 = 32$ $0 = m \cdot 32 + b$ $100 = m(212) + b$
 $C_1 = 100$ $F_1 = 212$
 $C = mF + b$ $m = \frac{5}{9}$ $b = 32$

7.) $\beta = \frac{\Delta V / V}{\Delta T} \rightarrow$ fractional change in volume \propto change in temp
 $\frac{V_f - V_i}{V_i} = \frac{\Delta V}{V} = \beta \cdot \Delta T$

(a) estimate mercury bulb volume \rightarrow cylinder diameter
 $\left(\frac{1}{4} \text{ cm diameter}\right)^3 \approx \frac{1}{64} \text{ cm}^3 \cdot \frac{10^3 \text{ mm}^3}{1 \text{ cm}^3} = 10 \text{ mm}^3 = V$
 ≈ 100

ΔV from 1°C

$$8] \frac{\Delta L}{L} = \alpha \cdot \Delta T$$

$$T_F = 100^\circ F \quad T_C = 10^\circ F$$

$$\Delta T_F = 90^\circ F$$

$$(a) \alpha = 1.1 \cdot 10^{-5} K^{-1}$$

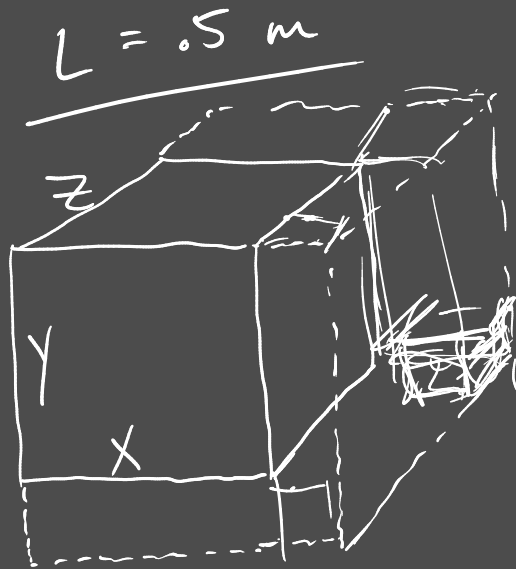
$$\frac{\Delta T_F}{\Delta T_C} = \frac{9}{5} \quad \frac{\Delta T_C}{\Delta T_F} = \frac{5}{9}$$

$$\begin{aligned} \Delta L &= \alpha \Delta T \cdot L \\ &= 1.1 \cdot 10^{-5} \cdot 50^\circ C \cdot 1000 \text{ m} \\ &= 50000 \cdot 10^{-5} \end{aligned}$$

$$\Delta T_C = \frac{5}{9} (90^\circ F)$$

$$\Delta T_C = 50^\circ C$$

(c)



$$\alpha \Delta T = \frac{\Delta L}{L}$$

$$\alpha_x \Delta T = \frac{\Delta x}{x}, \quad \alpha_y \Delta T = \frac{\Delta y}{y}, \quad \alpha_z \Delta T = \frac{\Delta z}{z}$$

$$\beta \Delta T = \frac{\Delta V}{V}$$

$$\Delta V = V_f - V_i = (x + \Delta x)(y + \Delta y)(z + \Delta z) - xyz$$

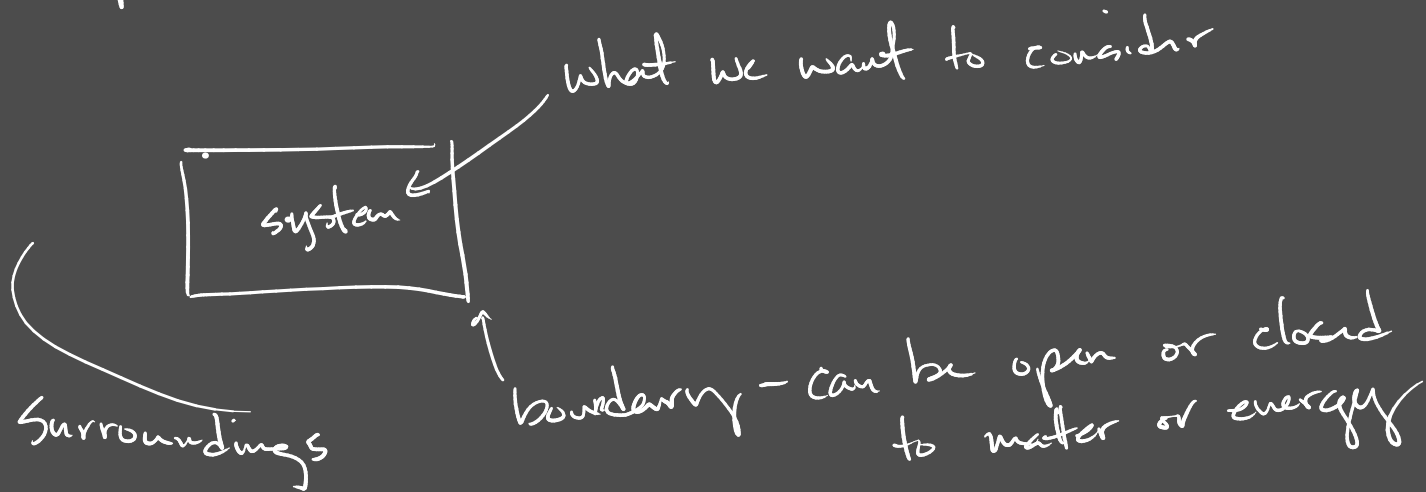
$$\Delta V = (xy + y\Delta x + x\Delta y + \Delta x\Delta y)(z + \Delta z) - xyz$$

$$\Delta V = \cancel{xyz} + xy\Delta z + yz\Delta x + y\Delta x\Delta z + xz\Delta y + x\Delta y\Delta z + z\Delta x\Delta y + \Delta x\Delta y\Delta z - \cancel{xyz}$$

$$\beta \Delta T = \frac{\Delta V}{V} = \frac{\Delta V}{XYZ} = \underbrace{\frac{\Delta Z}{Z}}_{\alpha_Z \Delta T} + \underbrace{\frac{\Delta X}{X}}_{\alpha_X \Delta T} + \underbrace{\frac{\Delta X \Delta Z}{XZ}}_{\approx 0} + \underbrace{\frac{\Delta Y}{Y}}_{\alpha_Y \Delta T} + \underbrace{\frac{\Delta Y \Delta Z}{YZ}}_{\approx 0} + \underbrace{\frac{\Delta X \Delta Y}{XY}}_{\approx 0} + \underbrace{\frac{\Delta X \Delta Y \Delta Z}{XYZ}}_{\approx 0}$$

$$\beta \Delta T = (\alpha_X + \alpha_Y + \alpha_Z) \Delta T$$

Macroscopic View



- Goal:
- ① describe the behavior of system
 - ② describe interactions w/ surroundings
 - ③ BOTH!

Macroscopic description: variables at human scale or larger
 \hookrightarrow easy to measure in a lab

Microscopic description: variables at molecular scale or smaller
↳ very hard to measure directly

Take a cylinder of a gas: (what does it take to describe it)

- mass & composition
- volume
- pressure
- temperature

these form macroscopic coordinates

1. no special assumptions about structure of matter
2. fewest possible to provide description
3. fundamental → suggested by sensory perception.
4. directly measurable

Microscopic view treated w/ statistical mechanics has nearly the opposite of these conditions

$P, V, T \rightarrow$ two can be varied but third is determined by those

An equation that relates the thermodynamic coordinates
 \hookrightarrow equation of state

for a closed system, the equation of state relates temp to two other variables.

Other examples

stretched wire \rightarrow force, length, temperature

1.2 The ideal gas law

$$p \cdot V = N k_B T$$

→ total number of particles
→ Boltzmann's constant → $1.381 \cdot 10^{-23} \frac{\text{J}}{\text{K}}$
→ absolute temp → Kelvin

↳ volume
↳ pressure = $\frac{\text{Force}}{\text{Area}}$

This is experimental. An approximation of low density gases

$$p = n k_B T$$

↳ number density $n = \frac{N}{V}$ $\rho = \frac{M}{V}$

Form used in chemistry (useful large numbers + mixtures)

$$pV = n_m R T$$

→ gas constant
↳ number of moles

$$N = n_m \cdot N_A \rightarrow n_m = \frac{N}{N_A}$$

$$N k_B = n_m R$$

or

$$R = k_B N_A = 8.31 \frac{\text{J}}{\text{K} \cdot \text{mol}}$$

$$N_A = 6.022 \cdot 10^{23} \text{ things/mole}$$

$$k_B = 1.381 \cdot 10^{-23} \text{ J/K}$$

Problem 1.9. What is the volume of one mole of air, at room temperature and 1 atm pressure?

$$PV = N k_B T$$

$$V = \frac{N k_B T}{P}$$

$$V = 0.024 \text{ m}^3$$

$\hookrightarrow \sim 30 \text{ cm cube}$
 $\sim 24 \text{ liters}$

$$N = N_A \quad T = 20^\circ\text{C} = 293$$

$$P = \underline{1 \text{ atm}} = 1.013 \cdot 10^5 \text{ Pa} \left[\frac{\text{N}}{\text{m}^2} \right] = [\text{Pascal}]$$

Problem 1.12. Calculate the average volume per molecule for an ideal gas at room temperature and atmospheric pressure. Then take the cube root to get an estimate of the average distance between molecules. How does this distance compare to the size of a small molecule like N_2 or H_2O ?

$$1 \text{ mol at 1 atm at } 293\text{K}, V = 0.024 \text{ m}^3$$

(N_A)

$$\frac{V}{N_A} = \frac{0.024 \text{ m}^3}{6.02 \cdot 10^{23}} = 4 \cdot 10^{-26} \text{ m}^3 / \text{molecule}$$

$$\downarrow \sqrt[3]{}$$

side length

$$\sqrt[3]{4 \cdot 10^{-26}} = 3.4 \cdot 10^{-9} \text{ m}$$

$$= 3.4 \text{ nm}$$

$$= 34 \text{ \AA}$$

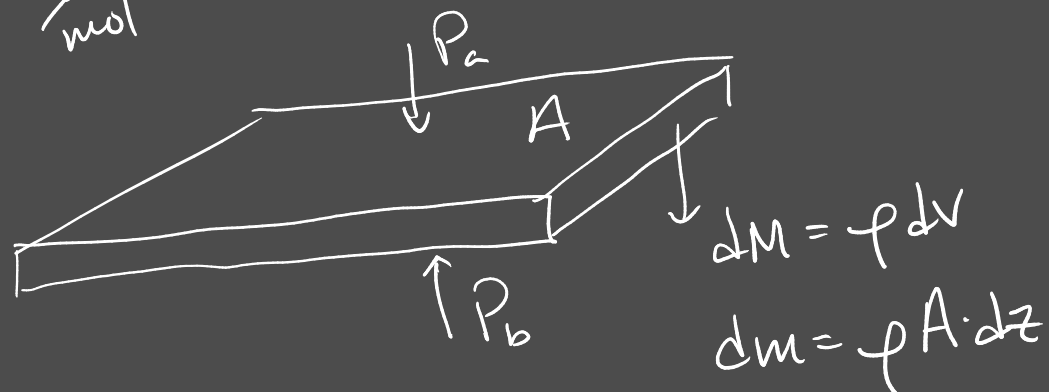
$$\text{H}_2 = 289 \text{ pm} = 2.89 \text{ \AA}$$

$$\text{N}_2 = 364 \text{ pm} = 3.64 \text{ \AA}$$

HW: ★ 12, ★ 13, ★ 14, ★ 16, ★ 17

$$14) \quad 2 \cdot 14 \frac{\text{g}}{\text{mol}} \cdot 0.78 + 2 \cdot 16 \frac{\text{g}}{\text{mol}} \cdot 0.21 + 40 \frac{\text{g}}{\text{mol}} \cdot 0.01 = 29 \frac{\text{g}}{\text{mol}}$$

16)



$$P_b \cdot A - P_a \cdot A - \rho A dz \cdot g = 0$$

$-dP$

$$-dP = \rho dz \cdot g$$

$$\frac{dP}{dz} = -\rho g$$

$$PV = Nk_B T$$

$$\frac{mN}{V} = \frac{mP}{k_B T} \Rightarrow \rho = \frac{mP}{k_B T}$$

$$P(z)$$

$$P_b = P(z)$$

$$P_a = P(z+dz)$$

$$\frac{P_a - P_b}{dz} = \frac{P(z+dz) - P(z)}{dz}$$

$$= \frac{dP}{dz}$$

$$\int \frac{dp}{p} = - \int \frac{mg}{k_B T} dz$$

$$\ln p = - \frac{mg}{k_B T} z$$

$$p(z) = e^{Az}$$

17] c $\left(p + \frac{an^2}{V^2}\right) \underbrace{\left(V - nb\right)}_{= V\left(1 - \frac{nb}{V}\right)} = nRT$

$$pV = nRT \left(1 + \frac{B(T)}{(V/n)} + \frac{C(T)}{(V/n)^2}\right)$$

$$= nRT \left(1 + \frac{n}{V} B(T) + \frac{n^2}{V^2} C(T)\right)$$

$$pV + \frac{an^2}{V} = \frac{nRT}{\left(1 - \frac{nb}{V}\right)}$$

$$\rightarrow pV = \frac{nRT}{1 - \frac{nb}{V}} - \frac{an^2}{V}$$

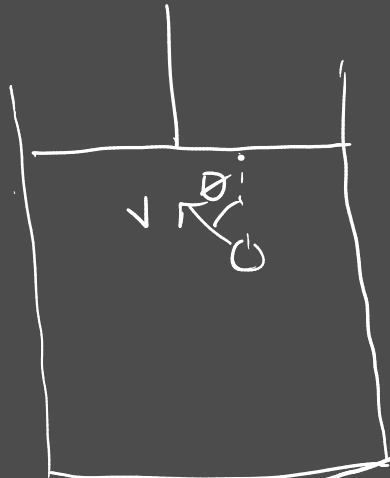
$$pV = nRT \left(\underbrace{\left(1 - \frac{nb}{V}\right)^{-1}}_{\text{apply binomial}} - \frac{a \cdot n}{RTV} \right)$$

apply binomial

we want pressure from a microscopic model:
(elastic collisions)

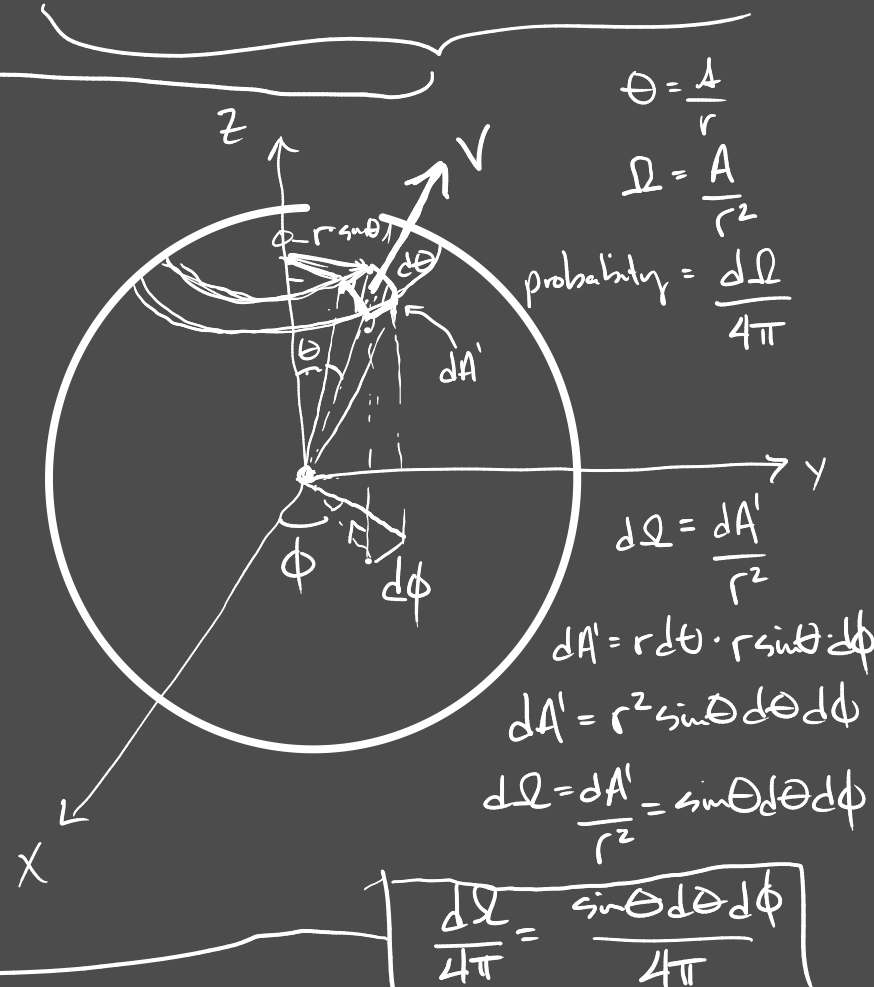
$$\text{pressure} = \frac{F}{A} = \frac{\Delta p}{A \cdot \Delta t} \rightarrow \frac{2mv \cos \theta}{v_y}$$

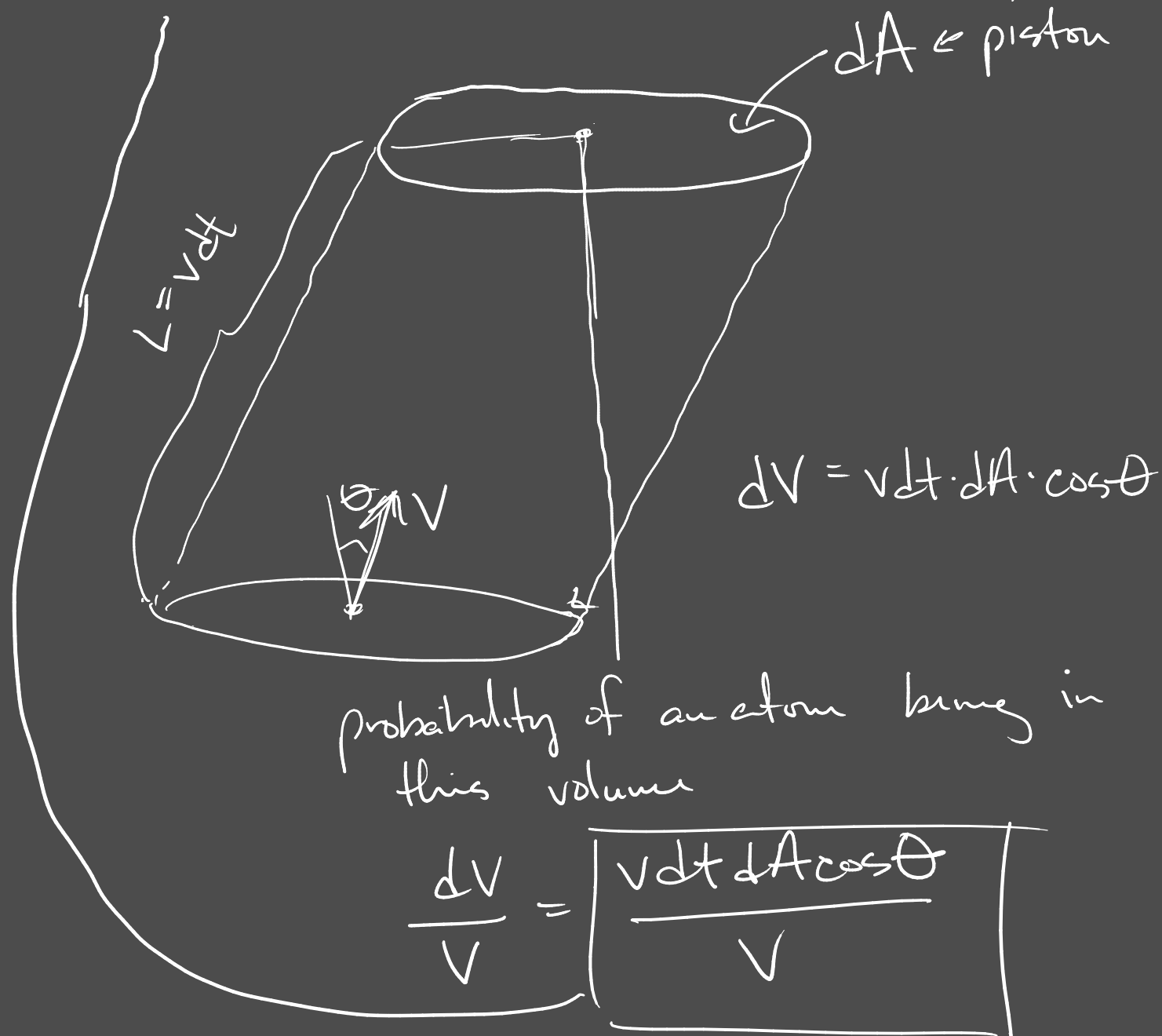
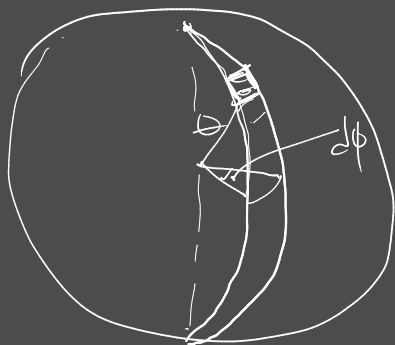
pressure = $\frac{2mv \cos \theta}{dA dt}$. number of particles hitting
Area dA w/ velocity v
in time dt



number of atoms
traveling in this
this particular
direction in the
entire volume.

fraction of those
that are within
striking distance
in time dt .





$N \cdot \frac{d\Omega}{4\pi} \cdot \frac{dV}{V}$. number of particles having a particular speed between v and $v+dv$

$f(v) \rightarrow$ speed distribution function
 fraction of particles w/ speeds
 between v and $v+dv$

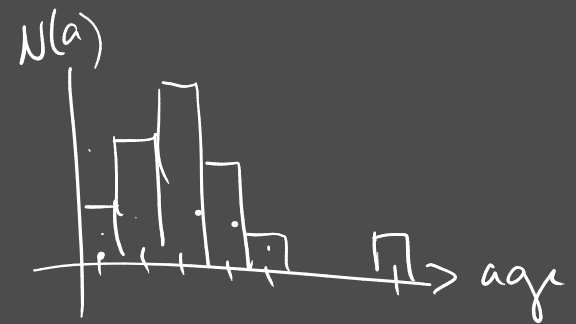
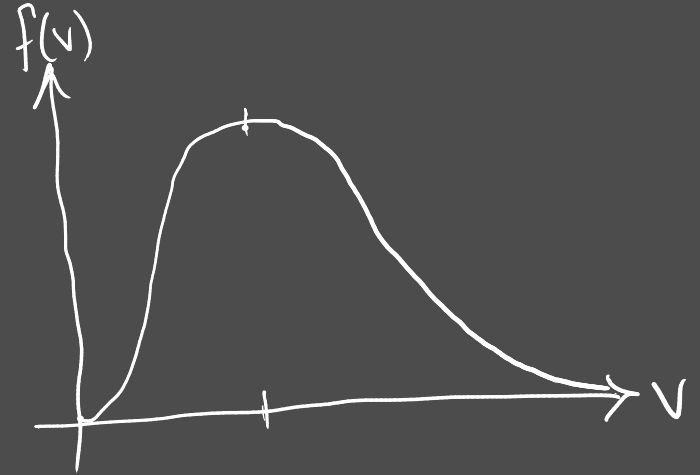
$\rightarrow f(v) \cdot dv$

$\int_0^{\infty} f(v) dv = 1$

$\rightarrow \langle v \rangle = \int_0^{\infty} v f(v) dv$

$\langle v^2 \rangle = \int_0^{\infty} v^2 f(v) dv$

$\langle g(v) \rangle = \int_0^{\infty} g(v) f(v) dv$



$\rho(\text{state}) = \psi^* \psi$

$1 = \int_{-\infty}^{\infty} \psi^* \psi dx$

$\langle x \rangle = \int_{-\infty}^{\infty} \psi^* \cdot x \cdot \psi dx$

$$pressure = \frac{2m v \cos \theta}{dA dt} \cdot N \cdot \frac{d\Omega}{4\pi} \cdot \frac{dv}{v} \cdot f(v) dv$$

$$\int dp = \frac{2m v \cos \theta}{\cancel{dA dt}} \cdot N \cdot \frac{\sin \theta d\theta d\phi}{4\pi} \cdot \frac{\cancel{v dt dA \cos \theta}}{V} \cdot f(v) dv$$

$$pressure = \frac{2m N}{4\pi V} \int_0^\infty \int_0^{\pi/2} \int_0^{2\pi} v^2 f(v) dv \cdot \cos^2 \theta \sin \theta d\theta \cdot d\phi$$

$$pressure = \frac{m N}{\cancel{2\pi} V} \underbrace{\int_0^\infty v^2 f(v) dv}_{\langle v^2 \rangle} \cdot \underbrace{\int_0^{\pi/2} \cos^2 \theta \sin \theta d\theta}_{1/3} \underbrace{\int_0^{2\pi} d\phi}_{\cancel{2\pi}}$$

$$P = \frac{m N}{3V} \cdot \langle v^2 \rangle$$

$$pV = N \frac{m \langle v^2 \rangle}{3}$$

$$pV = N k_B T$$

$$3 k_B T = m \langle v^2 \rangle \rightarrow$$

$$\underline{V_{rms}} = \sqrt{\langle v^2 \rangle} = \sqrt{\frac{3 k_B T}{m}}$$

$$\frac{3}{2} k_B T = \underbrace{\frac{1}{2} m \langle v^2 \rangle}_{\langle K \rangle}$$

$$U = N \langle K \rangle$$

ideal gas

$$\rightarrow U = \frac{3}{2} p \cdot V$$

$$U = \frac{3}{2} N k_B T$$

$$\rightarrow T = \frac{2}{3 k_B} \cdot \frac{U}{N}$$

$$\langle K \rangle = \frac{1}{2} m (\langle v_x^2 \rangle + \langle v_y^2 \rangle + \langle v_z^2 \rangle)$$

21, 22

Equipartition Theorem

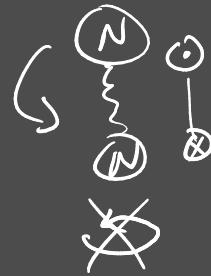
$$U_{\text{thermal}} = \frac{f}{2} N k_B T \rightarrow \text{degree of freedom}$$

quadratic energy terms
 $\frac{1}{2} m v_x^2, \frac{1}{2} I \omega_x^2, \frac{1}{2} k x^2$

↳ not the total energy
energy that changes when temp changes

$f = 3 \leftarrow$ monoatomic gas

$f = 5 \leftarrow$ diatomic gas
(near room temp)



1.23 | 1 liter of He at room temp

Heat + Work

1st Law of Thermo: Conservation of Energy

If the energy of system changes
it must come from the surroundings

So how? \rightarrow heat + work

\downarrow
spontaneous
due to ΔT

\hookrightarrow force applied
but also energy
from current in a resistor

$$dU = \pm Q + \pm W$$

\hookrightarrow inexact differential

can't do $\rightarrow W = \int \pm W$

$\rightarrow \oint \pm W \neq 0 \leftarrow$ path dependent

$$\Delta U = Q + W \leftarrow \text{book form}$$

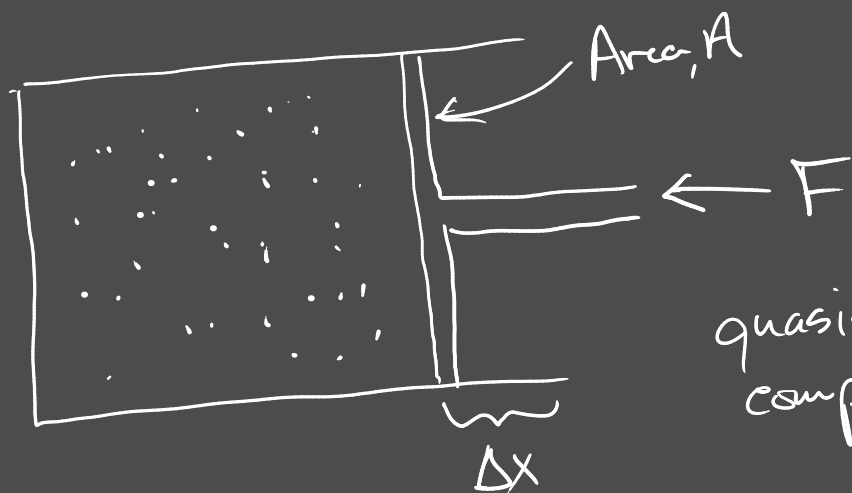
$$dU = \delta Q + \delta W$$

Engineering def:

$$dU = \delta Q - \delta W$$

\uparrow
positive work
is done on
surroundings

Compression/Expansion Work



$$W = \vec{F} \cdot d\vec{r} = F \cdot \Delta x$$

$$\hookrightarrow = P \cdot A$$

quasistatic compression $\rightarrow W = P \cdot \underbrace{A \cdot \Delta x}_{-\Delta V}$

$$W = -P \Delta V$$

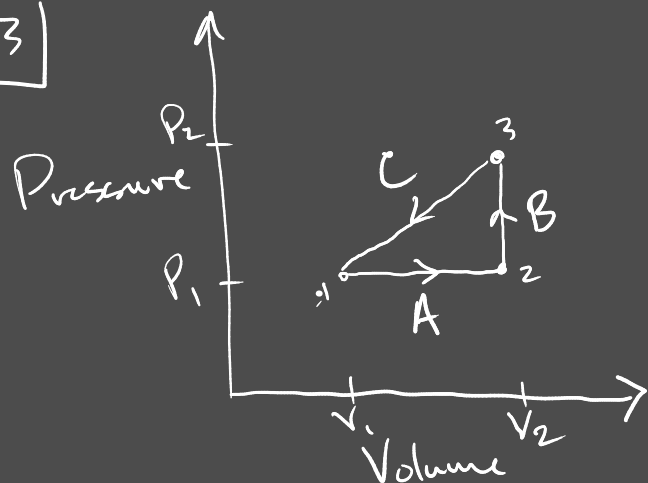
\hookrightarrow constant pressure over ΔV

$$dW = -P \Delta V \rightarrow \pm W = -P(V, T) dV$$

$$W = -\int P dV$$

~~$$W = \int \pm W$$~~

1.33



Sign: Work, energy, heat

$$A: W = - \int_1^2 p dV = -p \int_1^2 dV = -p(V_2 - V_1)$$

$$W < 0$$

$$Q = ?$$

$$\rightarrow U = \frac{f}{2} N k_B T = \frac{f}{2} PV$$

$$\Delta U > 0 \text{ b/c } \Delta V > 0$$

$$\boxed{\Delta U = Q + W}$$

$\begin{matrix} > 0 & & > 0 & & < 0 \end{matrix}$

$$B: W = 0, \Delta V = 0$$

$$\Delta U > 0$$

$$Q > 0$$

$$C: W > 0$$

$$\Delta U = U_f - U_i = \frac{3}{2} (P_f V_f - P_i V_i)$$

$\downarrow \downarrow \quad \uparrow \uparrow$

$$U < 0$$

$$Q < 0$$

$$\Delta U = Q + W$$

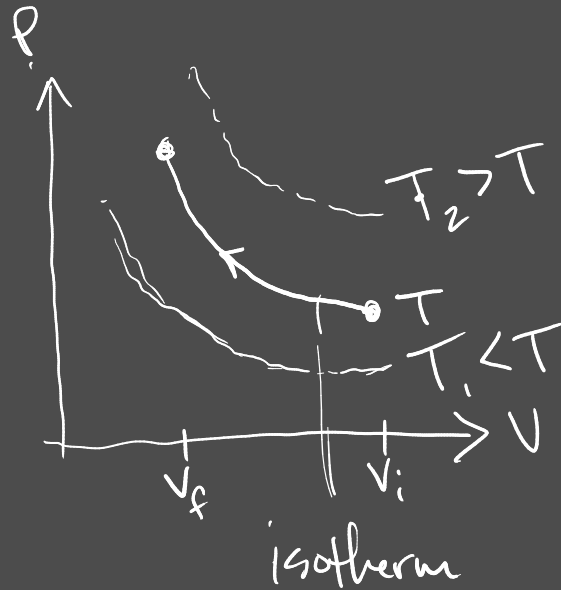
$\begin{matrix} < 0 & < 0 & > 0 \end{matrix}$

Isothermal Process + Adiabatic Process → expansion/compression

↳ constant temperature

↳ no heat escape

Isothermal Compression



$$PV = Nk_B T$$

all constant

$$P = \frac{Nk_B T}{V}$$

hyperbola

$$W = - \int p dV = -Nk_B T \int_{V_i}^{V_f} \frac{1}{V} dV$$

$$W = -Nk_B T \ln\left(\frac{V_f}{V_i}\right)$$

$$W = Nk_B T \ln\left(\frac{V_i}{V_f}\right)$$

what about heat?

$$\Delta U = \frac{f}{2} Nk_B \Delta T$$

isothermic

$$\Delta T = 0$$

first law → $dU = \delta Q + \delta W$

$$\delta Q = -\delta W \rightarrow Q = Nk_B T \ln\left(\frac{V_f}{V_i}\right)$$

Adiabatic Compression \rightarrow no heat added/removed

first law $dU = \cancel{\pm Q}^0 + \pm W$

$$\boxed{dU = \pm W}$$

for ideal gas $U = \frac{f}{2} N k_B T$

$$-p dV$$

$$dU = \frac{f}{2} N k_B dT$$

$$\frac{f}{2} \cancel{N k_B} dT = - \frac{\cancel{N k_B} T}{V} dV$$

$$\frac{f}{2} \frac{dT}{T} = - \frac{dV}{V}$$

now integrate

$$\frac{f}{2} \ln\left(\frac{T_f}{T_i}\right) = - \ln\left(\frac{V_f}{V_i}\right) = \ln\left(\frac{V_i}{V_f}\right)$$

$$\left(\frac{T_f}{T_i}\right)^{f/2} = \frac{V_i}{V_f} \rightarrow V \propto \frac{1}{T^{f/2}} \rightarrow V \cdot T^{f/2} = \text{constant of prop.}$$

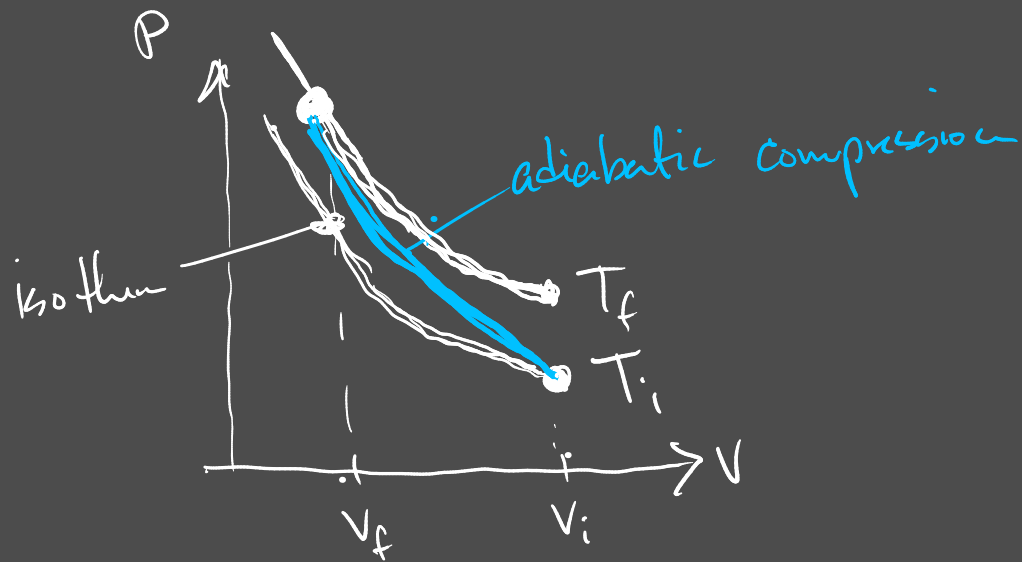
$$T_f^{f/2} \cdot V_f = T_i^{f/2} \cdot V_i$$

$$PV = N k_B T$$

$$P = \frac{N k_B T}{V}$$

$$- \int p dV$$

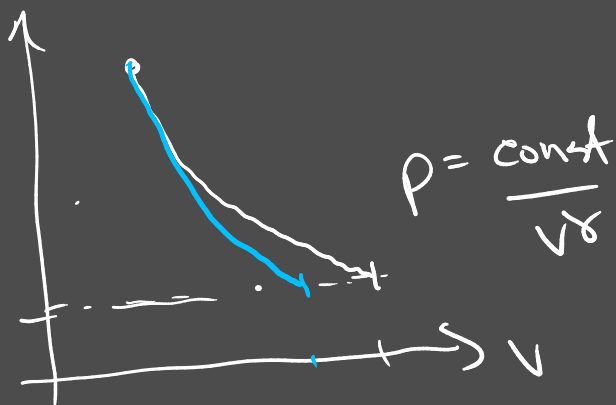
So we can get final temp now, what about final pressure?



$$f=3, \gamma = \frac{5}{3}$$

$$f=5, \gamma = \frac{7}{5}$$

Hint for #38



$$V \cdot T^{f/2} = \text{constant}$$

$$PV = Nk_B T$$

$$T \propto PV$$

$$V \cdot (PV)^{f/2} = \text{new const}$$

$$V \cdot P^{f/2} V^{f/2} =$$

$$\frac{2}{f} \left(V^{1+f/2} \cdot P^{f/2} \right) = \left(\right)^{\frac{2}{f}}$$

$$V^{\frac{2}{f}+1} \cdot P = \text{new const.}$$

$$V^{(2+f)/f} \cdot P = \text{const}$$

$$\gamma = \frac{2+f}{f} \leftarrow \text{adiabatic exponent}$$

$$V^\gamma \cdot P = \text{const}$$

for an ideal gas

$$\downarrow$$

$$\left(\frac{V_f}{V_i} \right)^\gamma = \frac{P_i}{P_f}$$

not exactly 1.40

$$\frac{dT}{dp} = \frac{2}{f+2} \frac{T}{p} \quad \text{or} \quad \left(\frac{\gamma-1}{\gamma} \right) \frac{dT}{dp} = \frac{T}{p}$$

$$\frac{dp}{dz} = - \frac{mg}{k_B T} \cdot p$$

$$P(z) = P(0) e^{-\frac{mgz}{k_B T}}$$

→ depended on
constant T w/ z

$$du = \cancel{\pm Q} + \pm W$$

$$du = \pm W$$

$$\frac{f}{2} N k_B dT = -p dV = -p \underbrace{\frac{dV}{dp}}_{?} dp$$

$$pV = N k_B T$$

$$V = \frac{N k_B T}{p}$$

product
rule

$$\frac{dV}{dp} = -\frac{N k_B T}{p^2} + \frac{N k_B}{p} \frac{dT}{dp}$$

$$\frac{f}{2} N k_B dT = +p \frac{N k_B T}{p^2} dp - p \frac{N k_B}{p} dT$$

$$\left(\frac{f}{2} + 1 \right) dT = \frac{T}{p} dp$$

$$\left(\frac{f}{2} + 1 \right) \frac{dT}{dp} = \frac{T}{p}$$

$$\Rightarrow \left| \frac{dT}{dp} = \frac{2}{f+2} \cdot \frac{T}{p} \right| = \frac{\gamma-1}{\gamma} \frac{T}{p}$$

$$\frac{dP}{dz} = -\frac{mg}{k_B} \cdot \frac{P}{T}$$

$$\frac{dP}{dT} \cdot \frac{dT}{dz} = -\frac{mg}{k_B} \cdot \frac{P}{T}$$

$$\frac{dP}{dT} = \frac{\gamma}{\gamma-1} \frac{P}{T}$$

$$\frac{\gamma}{\gamma-1} \cdot \frac{\cancel{P}}{\cancel{T}} \cdot \frac{dT}{dz} = -\frac{mg}{k_B} \cdot \frac{\cancel{P}}{\cancel{T}}$$

$$\frac{dT}{dz} = -\underbrace{\frac{mg}{k_B} \left(\frac{\gamma-1}{\gamma} \right)}_{\text{constant}}$$

linear change in temp
w/ height

$$du = \underbrace{dQ}_{Tds} + \underbrace{dW}_{-pdV}$$

→ integratin factor

Heat Capacity

$$dU = \pm Q + \underbrace{\pm W}_{-pdV}$$

$$\pm Q = \underbrace{(dU)}_{U(T,V) \text{ or } U(T,P)} + p dV$$

$$dU(T,V) = \left(\frac{\partial U}{\partial T} \right)_V dT + \left(\frac{\partial U}{\partial V} \right)_T dV$$

$$\pm Q = \left(\frac{\partial U}{\partial T} \right)_V dT + \left[\left(\frac{\partial U}{\partial V} \right)_T + p \right] dV$$

We want to know how much heat is needed to change the temperature under certain conditions (constraints)

Two cases : ① Constant volume
② Constant pressure

① Constant volume $\rightarrow dV=0$

$$dQ = \left(\frac{\partial U}{\partial T} \right)_V dT$$

$$C_V = \frac{dQ}{dT} = \left(\frac{\partial U}{\partial T} \right)_V$$

\rightarrow heat capacity at constant volume

★ ★ ★ ★

36, 38, 41, 45

ideal gas

$$U = \frac{f}{2} N k_B T$$

$$U = \frac{f}{2} n_m R T$$

$$\frac{\partial U}{\partial T} = \frac{f}{2} n_m R$$

$\frac{C_V}{n_m} \leftarrow$ molar heat capacity
molar specific heat

$$\frac{C_V}{n_m} = \frac{f}{2} R \rightarrow \sim 12.5 \text{ monatomic}$$

$\rightarrow \sim 20 \text{ diatomic}$

② Constant pressure

$$dQ = \left(\frac{\partial U}{\partial T} \right)_V dT + \left[\left(\frac{\partial U}{\partial V} \right)_T + P \right] dV$$

$$C_p \equiv \left(\frac{dQ}{dT} \right)_P = \underbrace{\left(\frac{\partial U}{\partial T} \right)_V}_{C_v} + \left[\left(\frac{\partial U}{\partial V} \right)_T + P \right] \left(\frac{dV}{dT} \right)_P$$

$$\rightarrow C_p = C_v + \left[\left(\frac{\partial U}{\partial V} \right)_T + P \right] \left(\frac{dV}{dT} \right)_P$$

$$C_p - C_v = \left[\left(\frac{\partial U}{\partial V} \right)_T + P \right] \left(\frac{dV}{dT} \right)_P$$

ideal gas

$$U = \frac{f}{2} n_m R \cdot T$$

$$C_p = \frac{f}{2} n_m R + 0 + P \frac{dV}{dT}$$

$$\left(\frac{\partial U}{\partial V} \right)_T = 0$$

for ideal gas

$$V = \frac{n_m R T}{P}$$

$$\frac{dV}{dT} = \frac{n_m R}{P}$$

$$C_p = \frac{f}{2} n_m R + n_m R$$

for monoatomic

$$f = 3$$

$$C_v = \frac{3}{2} R$$

$$C_p = \frac{5}{2} R$$

$$\frac{C_p}{n_m} = \frac{f}{2} R + R$$

(molar specific heat)

(molar heat capacity)

Schroeder's derivation of C_p (slightly beefed up)

$$dU(T, P) = \left(\frac{\partial U}{\partial T} \right)_P dT + \left(\frac{\partial U}{\partial P} \right)_T dP$$

$$\delta Q = dU + P dV$$

$$C_p = \left(\frac{\delta Q}{dT} \right)_P = \left(\frac{\partial U}{\partial T} \right)_P + \underbrace{\left(\frac{\partial U}{\partial P} \right)_T \frac{dP}{dT}}_{dP=0 \text{ at constant pressure}} + P \frac{dV}{dT}$$

$dP=0$ at constant pressure

$$C_p \equiv \left(\frac{\delta Q}{dT} \right)_P = \left(\frac{\partial U}{\partial T} \right)_P + P \left(\frac{dV}{dT} \right)_P$$

$$C_p = \frac{\Delta U + P \Delta V}{\Delta T}$$

$$\gamma \equiv \frac{C_p}{C_v} \quad \leftarrow \text{adiabatic index} = \frac{(f+2)}{f}$$

↑
for ideal gas

Specific Heat Capacity

$$C_p = \frac{C_p}{M} \leftarrow \text{big one}$$

↑
little see

$$C_v = \frac{C_v}{M}$$

Latent Heat \rightarrow during a phase change

$$C = \frac{dQ}{dT} \leftarrow \text{add some heat}$$

$\leftarrow \Delta$ change in temp

$$C = \infty$$

\leftarrow total heat to complete the phase change

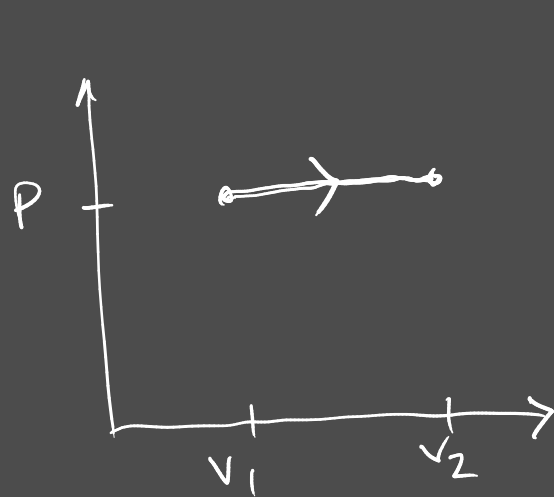
$$\frac{Q}{M} = L \leftarrow \text{latent heat}$$

$L_f \rightarrow$ latent heat of fusion (solid \leftrightarrow liquid)

$L_v \rightarrow$ latent heat of vaporization (liquid \leftrightarrow gas)

Enthalpy

isobaric process \rightarrow constant pressure



#1.341

$$W: -P(V_2 - V_1)$$

$$\Delta U: \frac{f}{2} P \Delta V = \frac{f}{2} P(V_2 - V_1)$$

$$Q: \Delta U - W = \frac{f}{2} P(V_2 - V_1) + P(V_2 - V_1)$$

heat at constant pressure \rightarrow enthalpy

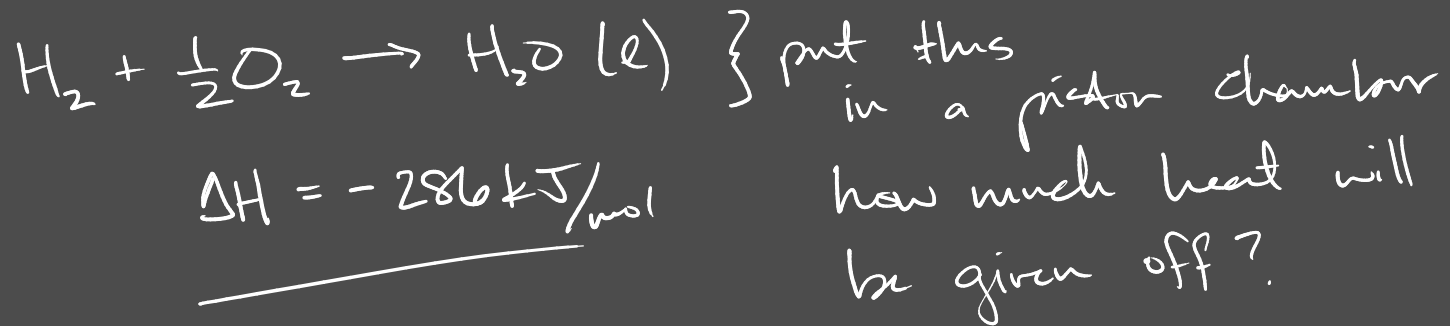
$$H = U - W$$

$$H \equiv U + PV$$

$$\Delta H = \Delta U + P \Delta V$$

$$C_p = \left(\frac{\partial H}{\partial T} \right)_p$$

★ ★
#47, 50



How much of this heat comes from the energy change in the bonds $\rightarrow \Delta U_{\text{int}}$

How much comes from the change in volume?

1.49

$$PV = n_m RT$$

$$10^5 \text{ Pa} \cdot V = 1.5 \text{ mol} (8.31 \text{ J/Kmol}) (273 \text{ K})$$

$$V = 0.34 \text{ m}^3$$

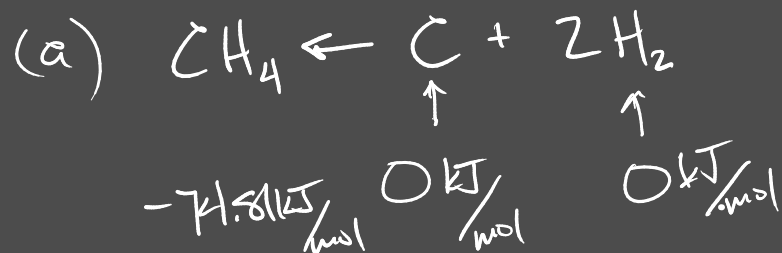
$$= 34 \text{ litres}$$

$$W = -P \int_{34\text{L}}^{0\text{L}} dV = -10^5 \text{ Pa} \cdot (0 \text{ m}^3 - 0.34 \text{ m}^3) = 3400 \text{ J} = 3.4 \text{ kJ}$$

$$\underline{\Delta H = -286 \text{ kJ}} = \Delta U - W \rightarrow \underline{\Delta U = -282.6 \text{ kJ}}$$



$T = 298 \text{ K} \quad P = 10^5 \text{ Pa}$



so it would take 74.8 kJ/mol to convert $\text{C} + \text{H}_2$ to CH_4



$\Delta H = -393.51 \text{ kJ/mol}$



$\Delta H = -241.82 \text{ kJ/mol}$

$\xrightarrow{\times 2 \quad \text{for 2 moles of H}_2\text{O}}$
 -483.64 kJ

(c) $\Delta H_{\text{reaction}} = +74.81 \text{ kJ} - 483.64 - 393.51$
 $= -802.34 \text{ kJ/mol CH}_4$

(d) How much heat is given off to surroundings $\rightarrow 802.34 \text{ kJ}$
 (at constant pressure)

$$(e) \quad W=0$$

$$\Delta H = \Delta U = 802.34 \text{ kJ}$$

if H_2O condenses to liquid

$$p\Delta V = -4.9 \text{ kJ}$$

$$\Delta H \rightarrow \text{H}_2\text{O}(l) \quad -285 \text{ kJ/mol} \times 2 = -571.64 \text{ kJ}$$

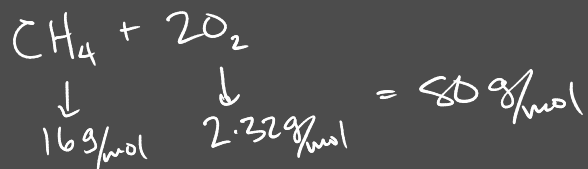
$$\Delta H_{\text{react}} = -890.34 \text{ kJ} = \Delta U + p\Delta V$$

$$\Delta U = -885.41 \text{ kJ}$$

$$(f) \quad m = 2 \cdot 10^{30} \text{ kg}$$

$$P = 3.9 \cdot 10^{26} \text{ Watts} = \frac{\Delta Q}{\Delta t} \rightarrow t = \frac{\Delta Q}{P}$$

$$\Delta Q = 802 \text{ kJ/mol} \cdot \# \text{ mol}$$



$$\frac{802 \text{ kJ}}{\text{mol}} \cdot \frac{1 \text{ mol}}{80 \text{ g}} \cdot \frac{1000 \text{ g}}{1 \text{ kg}} \cdot 2 \cdot 10^{30} \text{ kg} = 2 \cdot 10^{24} \text{ kJ} = 2 \cdot 10^{37} \text{ J}$$

$$t = \frac{2 \cdot 10^{37} \text{ J}}{3.9 \cdot 10^{26} \text{ W}} = 5 \cdot 10^{10} \text{ s} \cdot \frac{1 \text{ hr}}{3600 \text{ s}} \cdot \frac{1 \text{ d}}{24 \text{ hr}} \cdot \frac{1 \text{ yr}}{365 \text{ d}} = \underline{\underline{1585 \text{ yr}}}$$

1.36 (a) $V_1 = 1 \text{ liter} = .001 \text{ m}^3$
 $V_2 = ?$

$P_1 = 1 \text{ atm} = 1 \cdot 10^5 \text{ Pa}$
 $P_2 = 7 \text{ atm} = 7 \cdot 10^5 \text{ Pa}$

γ for air $\frac{7}{5}$

$$\left(\frac{V_2}{V_1}\right)^\gamma = \frac{P_1}{P_2}$$

$$V_2 = V_1 \left(\frac{P_1}{P_2}\right)^{1/\gamma} = 1 \text{ liter} \left(\frac{1 \text{ atm}}{7 \text{ atm}}\right)^{5/7}$$

$$V_2 = 0.249 \text{ liters}$$

$$\frac{V_2}{V_1} = \frac{1}{4}$$

(b) $\boxed{P = \frac{C}{V^\gamma}}$

$PV^\gamma = \text{constant}$

$$\frac{P_2}{P_1} = \frac{V_1^\gamma}{V_2^\gamma}$$

$$P(V) = \frac{P_1 V_1^\gamma}{V^\gamma}$$

$$W = - \int P dV = - P_1 V_1^\gamma \int \frac{dV}{V^\gamma}$$

← now it's a function

$$dU = \pm W$$

$$\Delta U = W$$

$$\Delta U = \frac{5}{2} N k_B \Delta T = W$$

$$\rightarrow \frac{5}{2} N k_B (T_2 - T_1)$$

$$\frac{5}{2} N k_B T_1 \left(\frac{T_2}{T_1} - 1 \right)$$

$$P_1 V_1$$

$$10^5 \cdot .001 \text{ m}^3$$

$$10^2$$

$$\frac{T_2}{T_1} = \left(\frac{V_1}{V_2} \right)^{\gamma/f}$$

$$\left(\frac{T_2}{T_1} \right)^{f/2} = \frac{V_1}{V_2}$$

$$T_2 = 523 \text{ K}$$

$$\Delta T = 223 \text{ K}$$

$$N = \frac{P_1 V_1}{k_B T_1}$$

$$\Delta U = 165 \text{ J}$$

