

# Introduction

# Reynolds-Averaged-Numerical-Simulation or Reynolds-Averaged-Navier-Stokes (RANS)

• The ensemble averaged momentum equation:

$$\frac{\partial \langle U_i \rangle}{\partial t} + \langle U_i \rangle \frac{\partial \langle U_i \rangle}{\partial x_j} = \nu \frac{\partial^2 \langle U_i \rangle}{\partial x_j \partial x_j} - \frac{\partial \langle u_i u_j \rangle}{\partial x_j} - \frac{1}{\rho} \frac{\partial \langle p \rangle}{\partial x_i}$$

- RANS: For stationary flows, the ensemble average,  $\langle . \rangle$ , can be regarded as the time average,  $\langle . \rangle_T$ .
- ightharpoonup Closure problem: Six additional unknowns  $\langle u_i u_j \rangle$

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## V.1 Turbulent viscosity models

## Boussinesq's gradient diffusion assumption

Based on the similarity between turbulent and viscous stress:

$$-\langle \vec{u}\vec{u} \rangle = 2\nu_T \langle \underline{S} \rangle - \frac{2}{3}k\underline{I}$$

$$\langle u_i u_j \rangle = -\nu_T \left( \frac{\partial \langle U_i \rangle}{\partial x_j} + \frac{\partial \langle U_j \rangle}{\partial x_i} \right) + \frac{2}{3}k\delta_{ij}$$
Turbulent viscosity

- The closure is reduced to one variable, i.e.,  $\nu_T$ .
- Exercise: What are the values of normal Reynolds stresses based on this assumption? Does it impose any limitation to the generality of the model?
- A large group of models  $\rightarrow$  ...

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# V.2 Two-equation models

## $k - \varepsilon$ model

- **Modeling:** 
  - Since k and  $\varepsilon$  are key parameters in turbulent flows, assume that:  $v_T = f(k, \varepsilon)$
  - Based on a simple dimensional analysis (exercise):

$$v_T = C_\mu k^2 / \varepsilon$$
 (5.13)

Empirical model constant

Transport equation of k, Eq. (3.21):

$$\frac{\overline{D}k}{\overline{D}t} + \vec{\nabla}.\vec{T}' = \mathcal{P} - \varepsilon$$

Exercise: Substituting Eq. (5.11) into Eq. (3.19), derive  $\mathcal{P}$  in the Cartesian coordinates system and show that this term is not unknown anymore.  $\mathcal{P} = -\langle u_i u_j \rangle \frac{\partial \langle U_i \rangle}{\partial x_i} \quad (3.19)$ 

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# V.2 Two-equation models

## $k - \varepsilon$ model

- Modeling:

A gradient diffusion assumption for 
$$\vec{T}'$$
:
$$\vec{T}' = -\frac{v_T}{\sigma_k} \vec{\nabla} k \qquad (5.14)$$
Empirical model constant

The modeled (closed) transport equation for k:

$$\frac{\overline{D}k}{\overline{D}t} = \vec{\nabla} \cdot \left(\frac{\nu_T}{\sigma_k} \vec{\nabla}k\right) + \mathcal{P} - \varepsilon \tag{5.15}$$

An alternative form, assuming  $\varepsilon \sim \tilde{\varepsilon}$  (HW#2):

$$\frac{\overline{D}k}{\overline{D}t} = \vec{\nabla} \cdot \left[ \left( \nu + \frac{\nu_T}{\sigma_k} \right) \vec{\nabla}k \right] + \mathcal{P} - \varepsilon \quad (5.15)'$$

Similarly, a modeled equation for  $\varepsilon$  can be derived.

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# V.2 Two-equation models

## $k - \varepsilon$ model

Final model:

$$\nu_{T} = C_{\mu}k^{2}/\varepsilon \qquad (5.11)$$

$$\frac{\overline{D}k}{\overline{D}t} = \vec{\nabla} \cdot \left(\frac{\nu_{T}}{\sigma_{k}}\vec{\nabla}k\right) + \mathcal{P} - \varepsilon \qquad (5.15)$$

$$\frac{\overline{D}\varepsilon}{\overline{D}t} = \vec{\nabla} \cdot \left(\frac{\nu_{T}}{\sigma_{\varepsilon}}\vec{\nabla}\varepsilon\right) + C_{\varepsilon 1}\frac{\mathcal{P}\varepsilon}{k} - C_{\varepsilon 2}\frac{\varepsilon^{2}}{k} \qquad (5.16)$$

- 5 model constants:  $C_{\mu}$ ,  $\sigma_k$ ,  $\sigma_{\varepsilon}$ ,  $C_{\varepsilon 1}$ , and  $C_{\varepsilon 2}$
- To be tuned experimentally.
- May be case dependent or even variable in a single problem (generality!!)

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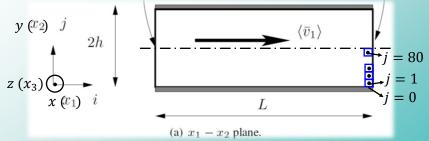
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# **Hands-on practice**

## HW#3 (continue):

Calculating different RANS statistics using DNS data



DNS with a  $192 \times 160 \times 192$  grid, however, data on:

$$192 \times 81 \times 192 \text{ nodes}$$

$$1 + 160/2$$

$$y = 0$$

For this problem, consider  $\langle . \rangle$  as the spatial average in (x, z)

plane rather than the time average,  $\langle . \rangle_T$ . Chap 5

# **Hands-on practice**

## HW#3 (continue)::

DNS data variables (superscript "\*" indicates dimensional variables):

$$x_i = \frac{x_i^*}{h}, U_i = \frac{U_i^*}{u_\tau}, p = \frac{p^*}{\rho u_\tau^2}$$

In your report, you need the wall unit:

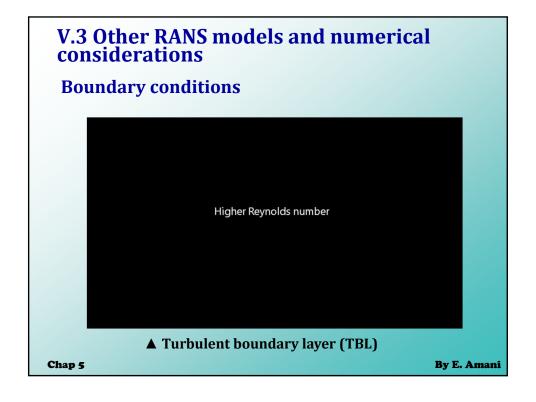
$$x_{i}^{+} = \frac{u_{\tau}x_{i}^{*}}{v} = Re_{\tau}x_{i}, U_{i}^{+} = \frac{U_{i}^{*}}{u_{\tau}} = U_{i}$$
Friction Reynolds number

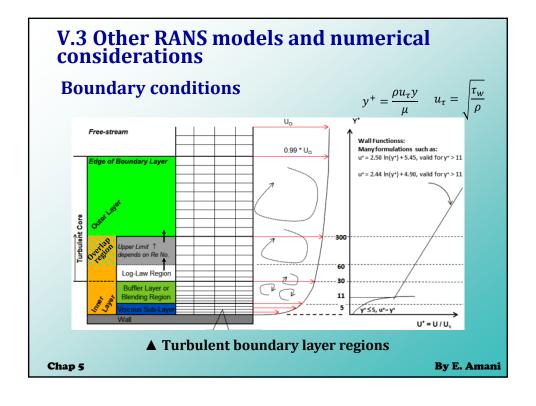
e channel Reynolds number vs. friction Reynolds

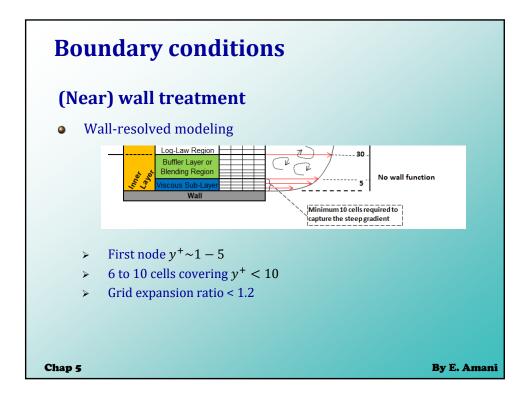
The channel Reynolds number vs. friction Reynolds number:

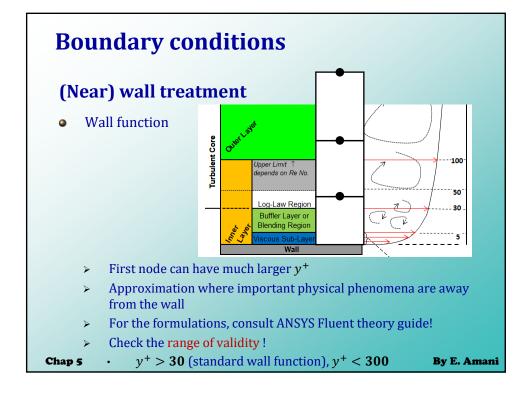
 $Re = \frac{U_b^* h}{v} = \frac{U_b^*}{u_\tau} u_\tau \frac{h}{v} = Re_\tau U_b$ 

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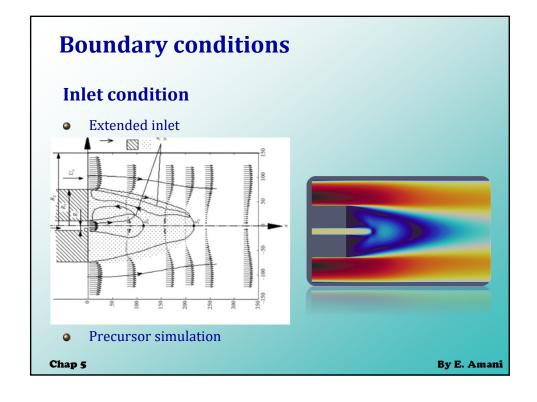


# **Boundary conditions**

## (Near) wall treatment

- Post-processing *y*<sup>+</sup> check\_\_\_  $y^{+} = \frac{\rho u_{\tau} y}{\mu} \qquad u_{\tau} = \sqrt{\frac{\tau_{w}}{\rho}}$
- Pre-processing  $y^{+} = \frac{\rho u_{\tau} y}{\mu} \iff y = \frac{\mu y^{+}}{\sqrt{\rho \tau_{w}}}$ 
  - > Approximation,
    - ✓ Flat plate TBL:  $\tau_{w} = \frac{1}{2} C_{f} \rho U_{\infty}^{2} \qquad C_{f} = 0.058 Re_{L}^{-0.2}$
    - Very Pipe flow:  $\tau_w = \frac{1}{8} f \rho U_b^2 \quad f = [0.79 \ln(Re_D) 1.64]^{-2}$
    - Flow between parallel plates (height 2h):  $D_h = 4h$   $\tau_w = \frac{1}{8} f \rho U_b^2 \quad f = \left[0.79 \ln(0.64 Re_{D_h}) 1.64\right]^{-2}$ RVF.

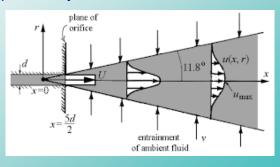
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# **Other RANS models**

## $k - \varepsilon$ model issues

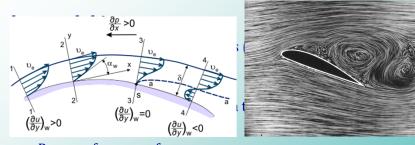
- Valid for fully turbulent regimes (needs near-wall modifications)
  - Low-Re damping term
  - > Tow-layer modeling (switch to other models for  $y^+<30$ )
- Round-jet anomaly



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# **Other RANS models**

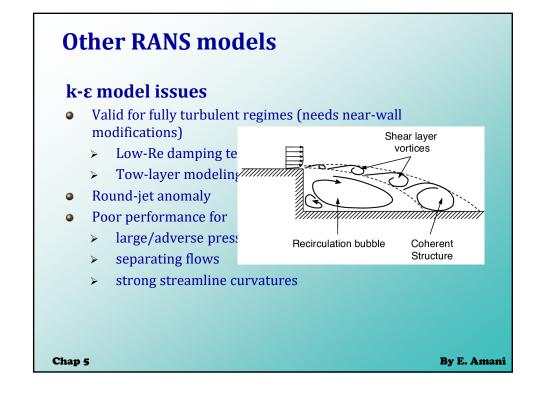


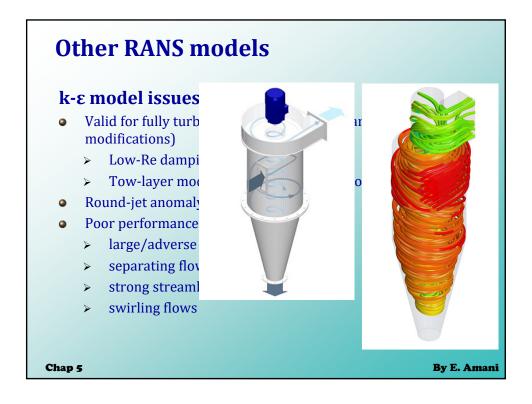
- Poor performance for
  - > large/adverse pressure gradients

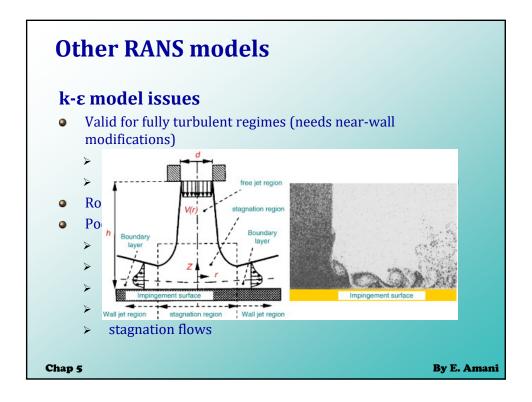
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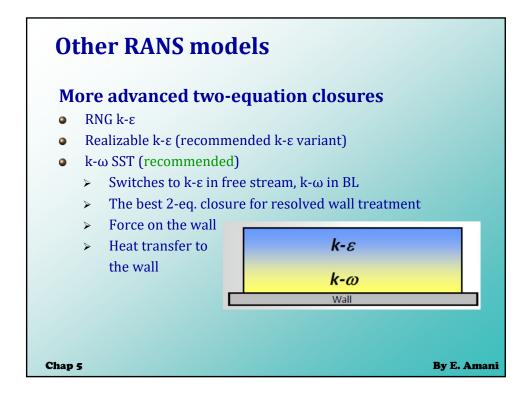
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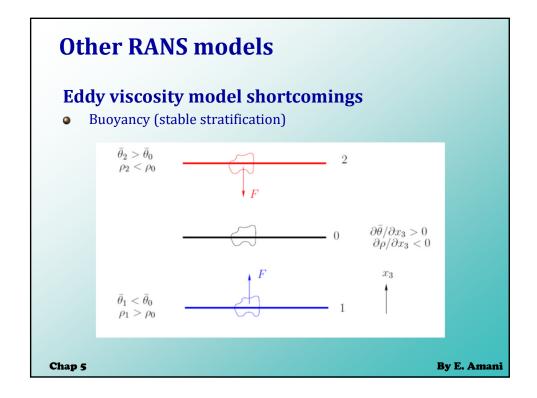
# Chap 5 Chap 5 Chap 5 Walid for fully turbulent regimes (needs near-wall modifications) Low-Re damping term Low-layer modeling (switch to other models for y + < 30)</li> Round-jet anomaly Poor performance for large/adverse press separating flows Chap 5 By E. Amani











## Other RANS models

## **Eddy viscosity model shortcomings**

- Buoyancy (stable stratification)
- Normal stress prediction (anisotropy)
- Swirling and recirculating flows (curvature effect)
- Stagnation flows (irrotational strain)
- Avoiding eddy viscosity assumption:
  - Reynolds Stress Model (RSM)

$$\frac{\overline{D}\langle u_i u_j \rangle}{\overline{D}t} = \nu \frac{\partial^2 \langle u_i u_j \rangle}{\partial x_k \partial x_k} - \frac{\partial T_{kij}}{\partial x_k} + P_{ij} + R_{ij} - \tilde{\varepsilon}_{ij}$$
 (5.17)

+ The epsilon or omega equation (7 equations)

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## **Other RANS models**

#### **RSM** model

Closed production term:

Production
rate tensor

$$\mathcal{P}_{ij} = -\left[\langle u_i u_k \rangle \frac{\partial \langle U_j \rangle}{\partial x_k} + \langle u_j u_k \rangle \frac{\partial \langle U_i \rangle}{\partial x_k}\right] \quad (5.18)$$

- Exercise: What is the relation of  $\mathcal{P}_{ij}$  with  $\mathcal{P}$  in k equation? Why?
- Closures:

The local isotropy assumption for 
$$\tilde{\varepsilon}_{ij}$$
:
$$\tilde{\varepsilon}_{ij} \sim \tilde{\varepsilon}_{ij} = \frac{2}{3} \varepsilon \delta_{ij} \qquad (5.22)$$

A gradient-diffusion assumption for 
$$T_{kij}$$
:
$$T_{kij} = -\frac{v_T}{\sigma_k} \frac{\partial \langle u_i u_j \rangle}{\partial x_k}$$
 (5.23)

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## Other RANS models RSM model

- **Closures:** 
  - There is more involved in the modeling of the pressure-strain
  - In addition to k and  $\varepsilon$ ;  $\langle S_{ij} \rangle$ ,  $\langle \Omega_{ij} \rangle$ , and  $b_{ij}$  (the anisotropy tensor) are important, where:

$$b_{ij} = \frac{\langle u_i u_j \rangle}{2k} - \frac{1}{3} \delta_{ij} \qquad (5.26)$$

$$b_{ij} = \frac{1}{2k} - \frac{1}{3} \delta_{ij} \qquad (3.26)$$

$$\Rightarrow \quad \text{Quadratic pressure-strain model:}$$

$$R_{ij} = -C_1 \varepsilon b_{ij} + C_2 \varepsilon \left( b_{ik} b_{kj} - \frac{1}{3} b_{mn} b_{mn} \delta_{ij} \right) + C_3 k \langle S_{ij} \rangle +$$

$$C_4 k \left( b_{ik} \langle S_{jk} \rangle + b_{jk} \langle S_{ik} \rangle - \frac{2}{3} b_{mn} \langle S_{mn} \rangle \delta_{ij} \right) + C_5 k \left( b_{ik} \langle \Omega_{jk} \rangle + b_{jk} \langle \Omega_{ik} \rangle \right)$$

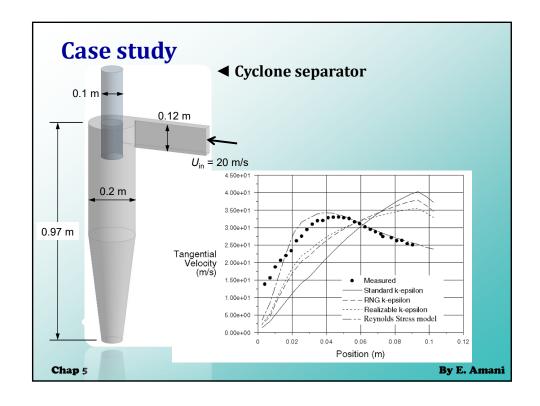
$$\Rightarrow \quad 9 \text{ model constants: } \sigma_k, \sigma_\varepsilon, C_{\varepsilon 1}, C_{\varepsilon 2}, \text{ and } C_1 \text{ to } C_5$$

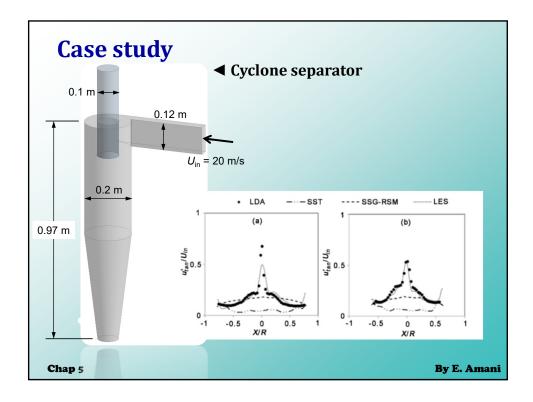
$$(5.22)$$

9 model constants:  $\sigma_k$ ,  $\sigma_{\varepsilon}$ ,  $C_{\varepsilon 1}$ ,  $C_{\varepsilon 2}$ , and  $C_1$  to  $C_5$ 

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# **Unsteady RANS (URANS)**

- Adding unsteady terms (simple URANS)
  - For example, k-ω SST:

$$\left( \frac{\partial (\rho k)}{\partial t} + \frac{\partial (\rho u_j k)}{\partial x_j} \right) = \frac{\partial}{\partial x_j} \left[ \left( \mu + \frac{\mu_t}{\sigma_k} \right) \frac{\partial k}{\partial x_j} \right] + \tilde{P} - \beta^* \rho k \omega$$

$$\left( \frac{\partial (\rho \omega)}{\partial t} \right) + \frac{\partial (\rho u_j \omega)}{\partial x_j} = \frac{\alpha \tilde{P}}{\nu_t} - \beta \rho \omega^2 + \frac{\partial}{\partial x_j} \left[ \left( \mu + \frac{\mu_t}{\sigma_\omega} \right) \frac{\partial \omega}{\partial x_j} \right] + 2(1 - F_1) \rho \sigma_{\omega_2} \frac{1}{\omega} \frac{\partial k}{\partial x_j} \frac{\partial \omega}{\partial x_j}$$

- However, RANS is too dissipative!
- Reducing  $\mu_t$  locally and allowing unsteadiness to grow (improved URANS)
  - For example, scale-adaptive simulation (SAS)
    - k-ω SST SAS: additional source term in ω equation

$$\frac{\partial(\rho\omega)}{\partial t} + \frac{\partial(\rho u_j\omega)}{\partial x_j} = \frac{\alpha\tilde{P}}{\nu_t} - \beta\rho\omega^2 + \frac{\partial}{\partial x_j} \left[ \left(\mu + \frac{\mu_t}{\sigma_\omega}\right) \frac{\partial\omega}{\partial x_j} \right] + 2(1 - F_1)\rho\sigma_{\omega_2} \frac{1}{\omega} \frac{\partial k}{\partial x_j} \frac{\partial\omega}{\partial x_j} + \mathbf{Q}_{SAS}$$

•  $\mu_t \sim \rho k/\omega$ :  $\omega \uparrow \rightarrow \mu_t \downarrow$  (depending on grid size)

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