

Fluid-particle momentum interaction summary

Interaction	Formulation																					
Drag Force [1]	$\mathbf{F}_D = m_p \frac{\mathbf{u}_r}{\tau_p}, \tau_p = \tau_v = \frac{\tau_{v,St}}{f_D}, \tau_{v,St} = \frac{\rho_p d_p^2}{18 \rho_f \nu_f}, \quad f_D = \begin{cases} 1 & Re_p \leq 0.1 \\ 1 + \frac{1}{6} Re_p^{\frac{2}{3}} & 0.1 < Re_p \leq 1000 \end{cases}$ $\mathbf{u}_r = \mathbf{u}_s - \mathbf{u}_p = \mathbf{u}_f - \mathbf{u}_p, \quad Re_p = \frac{ \mathbf{u}_r d_p}{\nu_f}, \quad s \leftrightarrow f \leftrightarrow c$																					
Drag Torque [2]	$\mathbf{T}_D = \begin{cases} -\pi \rho_f \nu_f d_p^3 \boldsymbol{\omega}_r & ; Re_\omega \leq 1 \\ -\frac{C_R}{64} \rho_f d_p^5 \boldsymbol{\omega}_r \boldsymbol{\omega}_r & ; Re_\omega > 1 \end{cases}, \quad C_R = \left(\frac{C_1}{Re_\omega^{0.5}} + \frac{C_2}{Re_\omega} \right), \boldsymbol{\omega}_r = \boldsymbol{\omega}_p - \boldsymbol{\omega}_f, \quad \boldsymbol{\omega}_f = 0.5 \nabla \times \mathbf{u}_f$ $Re_\omega = \frac{ \boldsymbol{\omega}_r d_p^2}{\nu_f} ; \quad C_1 \text{ and } C_2 \rightarrow$ <div><div>Dennis et al.(1980)</div><table><tr><th>Re_ω</th><th>C_1</th><th>C_2</th></tr><tr><td>$Re_\omega < 32$</td><td>0</td><td>64π</td></tr><tr><td>$32 < Re_\omega < 1000$</td><td>12.9</td><td>128.4</td></tr></table><div>Takagi</div><table><tr><th>Re_ω</th><th>C_1</th><th>C_2</th></tr><tr><td>$10 < Re_\omega < 20$</td><td>5.32</td><td>37.2</td></tr><tr><td>$20 < Re_\omega < 50$</td><td>6.44</td><td>32.2</td></tr><tr><td>$50 < Re_\omega < 100$</td><td>6.45</td><td>32.1</td></tr></table></div>	Re_ω	C_1	C_2	$Re_\omega < 32$	0	64π	$32 < Re_\omega < 1000$	12.9	128.4	Re_ω	C_1	C_2	$10 < Re_\omega < 20$	5.32	37.2	$20 < Re_\omega < 50$	6.44	32.2	$50 < Re_\omega < 100$	6.45	32.1
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Virtual Mass Force [3]	$\mathbf{F}_{vm} = C_{vm} \frac{\rho_f \nabla_p}{2} \left(\frac{D\mathbf{u}_f}{Dt} - \frac{d\mathbf{u}_p}{dt} \right), \quad C_{vm} = 1$																					
History (Basset) Force [4, 5]	$\mathbf{F}_H = C_B \frac{3}{2} d_p^2 \sqrt{\pi \mu_f \rho_f} \left[\int_0^t \frac{\frac{d\mathbf{u}_r}{dt'}}{\sqrt{t-t'}} dt' + \frac{\mathbf{u}_{r,0}}{\sqrt{t}} \right], \quad C_B = 1 - 0.527 \left[1 - \exp(-0.14 Re_p Sl^{0.82})^{2.5} \right],$ $Sl = \frac{1}{2\pi f \tau_p}$																					
Saffman Lift force [6]	$\mathbf{F}_L = 1.61 C_s \rho_f d_p^2 \left(\frac{2\nu_f}{ \boldsymbol{\omega}_f } \right)^{\frac{1}{2}} \mathbf{u}_r \times \boldsymbol{\omega}_f,$ $C_s = \begin{cases} \left(1 - 0.3314 \lambda_v^{\frac{1}{2}} \right) \exp\left(-\frac{Re_p}{10}\right) + 0.3314 \lambda_v^{\frac{1}{2}} & ; Re_p \leq 40 \\ 0.0524 (\lambda_v Re_p)^{1/2} & ; Re_p > 40 \end{cases}, \quad \lambda_v = d_p \frac{ \boldsymbol{\omega}_f }{ \mathbf{u}_r }$																					
Magnus Lift force [7, 8]	$\mathbf{F}_L = 0.5 C_{LR} \rho_f A_p \frac{ \mathbf{u}_r }{ \boldsymbol{\omega}_r } (\mathbf{u}_r \times \boldsymbol{\omega}_r),$ $C_{LR} = \begin{cases} \frac{Re_\omega}{Re_p} & ; Re_p \leq 1 \\ 0.45 + \left(\frac{Re_\omega}{Re_p} - 0.45 \right) \exp\left(-0.05684 Re_\omega^{0.4} Re_p^{0.3}\right) & ; Re_p < 2000 \end{cases}$																					
Brownian Force [9, 10]	$\mathbf{F}_B = m_p \sqrt{\frac{\pi S_0}{\delta t}} \zeta \boldsymbol{\eta}, S_0 = \frac{216 \mu_f K_B T_f}{\pi^2 d_p^5 \rho_p^2 C_c}, C_c = 1 + \frac{2\lambda}{d_p} \left[1.257 + 0.4 \exp\left(-\frac{1.1 d_p}{2\lambda}\right) \right]$ $\boldsymbol{\eta} = a \cos(\theta) \mathbf{i} + a \sin(\theta) \mathbf{j} + u \mathbf{k}, \theta = 2\pi X, u = 2Y - 1, a = \sqrt{1 - u^2}, X, Y \in U(0,1), \zeta \in N(0,1)$																					
Thermophoretic Force [11]	$\mathbf{F}_T = -D_{T,p} \frac{\nabla T}{T}, D_{T,p} = \frac{6\pi d_p \mu_f^2 C_s \left(\frac{\lambda_f}{\lambda_p} + C_t \frac{2\lambda}{d_p} \right)}{\rho_f \left(1 + 3C_m \frac{2\lambda}{d_p} \right) \left(1 + 2\frac{\lambda_f}{\lambda_p} + 2C_t \frac{2\lambda}{d_p} \right)}, C_c = 1.17, C_t = 2.18, C_m = 1.14$																					
Wall Force [12]	$\mathbf{F}_W = C_w \frac{\pi}{12} \rho_f d_p^4 \mathbf{u}_r ^2 \left(\frac{1}{y_w^2} - \frac{1}{(D - y_w)^2} \right) \mathbf{n}$																					

Heat and Mass transfer Summary

$$\dot{m}_p = \frac{dm_p}{dt} = -\frac{m_p}{\tau_M}; \tau_M = \frac{\rho_p d_p^2}{6\rho_m D_m \text{Sh}^* \ln(1 + B_M)} \quad (46.9)$$

$$\frac{dT_p}{dt} = \frac{T_s - T_p}{\tau_T} - \frac{1}{\tau_M} \frac{L_{v,\text{surf}}}{c_p} + \frac{q_R}{m_p c_p}; \tau_T = \frac{\rho_p c_p d_p^2}{6\lambda_m \text{Nu}_m} \quad (48.9)$$

Heat and Mass transfer correlation [13, 14]

$$\begin{aligned} \text{Sh}^* &= \frac{2 + 0.87 \text{Re}_p^{1/2} \text{Sc}_m^{1/3}}{(1 + B_M)^{0.7}}; \text{Sc}_m = \mu_m / \rho_m D_m \\ \text{Nu}_m &= \frac{\ln(1 + B_T)}{B_T} \text{Nu}_{0,m} \\ \text{Nu}_{0,m} &= \begin{cases} 2 + 0.552 \text{Re}_p^{1/2} \text{Pr}_m^{1/3} & ; \text{Re}_p > 10 \\ 1 + (1 + \text{Re}_p \text{Pr}_m)^{\frac{1}{3}} \max(1, \text{Re}_p^{0.077}) & ; \text{otherwise} \end{cases} \\ B_T &= \frac{-\dot{m}_p C_v}{\pi d_p \lambda_m \text{Nu}_m} \\ \text{Pr}_m &= \mu_m C_m / \lambda_m \end{aligned}$$

References

- Schiller, L. and A. Naumann, *A drag coefficient correlation*. *Vdi Zeitung*, 77: 318–320, 1935. Cité page. **38**.
- Sommerfeld, M., *Theoretical and experimental modelling of particulate flows*. Lecture series, 2000. **6**: p. 3-7.
- Auton, T., J. Hunt, and M. Prud'Homme, *The force exerted on a body in inviscid unsteady non-uniform rotational flow*. *Journal of Fluid Mechanics*, 1988. **197**: p. 241-257.
- Reeks, M. and S. McKee, *The dispersive effects of Basset history forces on particle motion in a turbulent flow*. *The Physics of fluids*, 1984. **27**(7): p. 1573-1582.
- Michaelides, E.E. and A. Roig, *A reinterpretation of the Odar and Hamilton data on the unsteady equation of motion of particles*. *AIChE Journal*, 2011. **57**(11): p. 2997-3002.
- Mei, R. and J. Klausner, *Shear lift force on spherical bubbles*. *International journal of heat and fluid flow*, 1994. **15**(1): p. 62-65.
- Rubinow, S. and J.B. Keller, *The transverse force on a spinning sphere moving in a viscous fluid*. *Journal of Fluid Mechanics*, 1961. **11**(3): p. 447-459.
- Oesterle, B. and T.B. Dinh, *Experiments on the lift of a spinning sphere in a range of intermediate Reynolds numbers*. *Experiments in Fluids*, 1998. **25**(1): p. 16-22.
- Li, A. and G. Ahmadi, *Dispersion and deposition of spherical particles from point sources in a turbulent channel flow*. *Aerosol science and technology*, 1992. **16**(4): p. 209-226.
- Ounis, H., G. Ahmadi, and J.B. McLaughlin, *Brownian particle deposition in a directly simulated turbulent channel flow*. *Physics of Fluids A: Fluid Dynamics*, 1993. **5**(6): p. 1427-1432.
- Brock, J.R., *On the theory of thermal forces acting on aerosol particles*. *Journal of Colloid Science*, 1962. **17**(8): p. 768-780.
- Tomiya, A., *Struggle with computational bubble dynamics*. *Multiphase Science and Technology*, 1998. **10**(4): p. 369-405.
- Amani, E. and M. Nobari, *A calibrated evaporation model for the numerical study of evaporation delay in liquid fuel sprays*. *International journal of heat and mass transfer*, 2013. **56**(1): p. 45-58.
- Amani, E. and M. Nobari, *Systematic tuning of dispersion models for simulation of evaporating sprays*. *International Journal of Multiphase Flow*, 2013. **48**: p. 11-31.