



Conservation of mass (continuity)

● For a general control volume

$$\frac{Dm_s}{Dt} = 0 \quad (1.7) \quad B = m \xrightarrow{1} b \equiv \frac{dB}{dm} = \frac{dm}{dm} = 1$$

$$\xrightarrow[\text{1st RTT}]{(7.6)} \frac{Dm_s}{Dt} = \frac{d}{dt} \int_{V_\sigma} \rho b dV + \int_A \rho b (\vec{V} - \vec{V}_\sigma) \cdot \vec{n} dA = 0 \quad (1.7)$$

$$\rightarrow \underbrace{\frac{d}{dt} \iiint_{V_\sigma} \rho dV}_{\text{Rate of change of mass in the control volume}} + \underbrace{\oint_A \rho \vec{V}_r \cdot \vec{n} dA}_{\text{Net outlet mass flowrate from the control surface}} = 0 \quad (2.7) \quad \frac{dm_\sigma}{dt} + \sum_{\text{out}} \dot{m} - \sum_{\text{in}} \dot{m} = 0$$

● For a fixed Control Volume (C.V.) ($\vec{V}_\sigma = 0$)

$$\xrightarrow{(2.7)} \frac{\partial}{\partial t} \iiint_{V_\sigma} \rho dV + \oint_A \rho \vec{V} \cdot \vec{n} dA = 0 \quad (3.7)$$

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Conservation of mass (continuity)

● Simplified forms

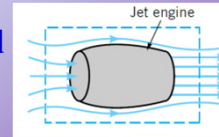
1. For a fixed C.V. in a steady flow:

$$\frac{\partial}{\partial t} \iiint_{V_\sigma} \rho dV = \iiint_{V_\sigma} \frac{\partial \rho}{\partial t} dV = 0 \quad (3.7)$$

$$\oiint_A \rho \vec{V} \cdot \vec{n} dA = 0 \quad (4.7) \quad \sum_{\text{out}} \dot{m} = \sum_{\text{in}} \dot{m}$$

2. For a moving, non-deforming C.V. and a steady flow (in the C.V.-attached reference frame)

$$(2.7) \rightarrow \oiint_A \rho \vec{V}_r \cdot \vec{n} dA = 0 \quad (4.7)'$$



3. For an incompressible flow (and single-phase):

$$(2.7) \rightarrow \rho = cte \rightarrow \rho \frac{d}{dt} \iiint_{V_\sigma} dV + \rho \oiint_A \vec{V}_r \cdot \vec{n} dA = 0 \rightarrow \frac{dV_\sigma}{dt} + \oiint_A \vec{V}_r \cdot \vec{n} dA = 0 \quad (4.7)''$$

$$\sum_{\text{out}} Q - \sum_{\text{in}} Q = 0$$

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Conservation of mass (continuity)

● Simplified forms

4. For a moving, non-deforming C.V. and an incompressible flow (in the C.V.-attached reference frame)

$$(4.7)'' \rightarrow \oiint_A \vec{V}_r \cdot \vec{n} dA = 0 \quad (5.7) \quad \sum_{\text{out}} Q = \sum_{\text{in}} Q$$

5. For a 1D inlet or outlet normal to the flow

$$\dot{m} = \iint \rho \vec{V}_r \cdot \vec{n} dA = \rho V_r A \quad Q = \iint \vec{V}_r \cdot \vec{n} dA = V_r A$$

- **Note:** It can be shown that Eqs. (4.7)'' and (5.7) also valid for incompressible **multiphase flows** ($D\rho/Dt = 0$ instead of $\rho = cte$).

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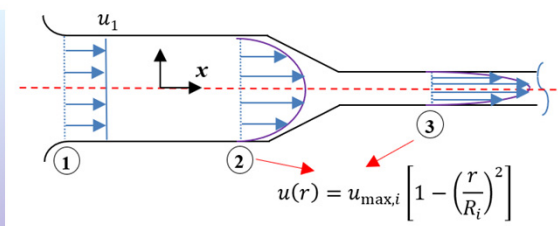
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Conservation of mass (continuity)

Sample problem

A steady-state incompressible flow develops in a pipe system. The velocity profiles are shown at three different sections. Determine the maximum velocity at sections 2 and 3 as a function of the inlet velocity, u_1 , and pipe sizing ($R_1 = R_2 = 2R_3$). The flow is assumed parallel, in the x direction.

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The (linear) momentum equation

For a general control volume

➡ Lecture Notes

$$\sum \vec{F}_\sigma = \frac{d}{dt} \iiint_{V_\sigma} \vec{V} \rho dV + \oint_A \vec{V} (\rho \vec{V}_r \cdot \vec{n}) dA \quad (10.7)$$

Resultant external
force acting on the
control volume

Rate of change of
momentum in the
control volume

Net momentum
outflow rate from the
control surface

Simplified forms

1. For an inertial C.V. (moving with a constant velocity)

$$\vec{V} \rightarrow \vec{V}_r \quad \sum \vec{F}_\sigma = \frac{d}{dt} \iiint_{V_\sigma} \vec{V}_r \rho dV + \oint_A \vec{V}_r (\rho \vec{V}_r \cdot \vec{n}) dA \quad (11.7)$$

✓ Exercise: For an inertial C.V. both Eqs. (10.7) and (11.7) are valid. Therefore, the right-hand-side of these equations should be equal. Show this equality with the aid of the continuity.

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The (linear) momentum equation

- Simplified forms

2. For an inertial C.V. and a steady flow in the C.V.-attached reference frame

$$\frac{d}{dt} \iiint_{V_\sigma} \vec{V}_r \rho dV = \iiint_{V_\sigma} \frac{d}{dt} [\rho(\vec{V} - \vec{V}_\sigma)] dV$$

Non-deforming

$$\xrightarrow{(11.7)} \sum \vec{F}_\sigma = \oint_A \vec{V}_r (\rho \vec{V}_r \cdot \vec{n}) dA \quad (12.7)$$

3. For 1D inlets and outlets:

$$\xrightarrow{(10.7)} \sum \vec{F}_\sigma = \frac{d\vec{P}_\sigma}{dt} + \sum_{\text{out}} \dot{m} \vec{V} - \sum_{\text{in}} \dot{m} \vec{V} \quad (10.7)'$$

$$\xrightarrow{(11.7)} \sum \vec{F}_\sigma = \frac{d\vec{P}_{\sigma,r}}{dt} + \sum_{\text{out}} \dot{m} \vec{V}_r - \sum_{\text{in}} \dot{m} \vec{V}_r \quad (11.7)'$$

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The (linear) momentum equation

- Example: Pelton turbine

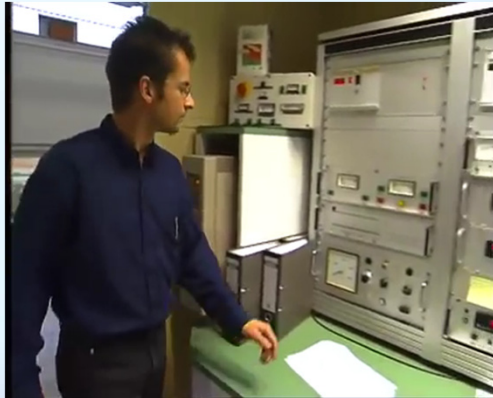


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The (linear) momentum equation

- Example: Pelton turbine

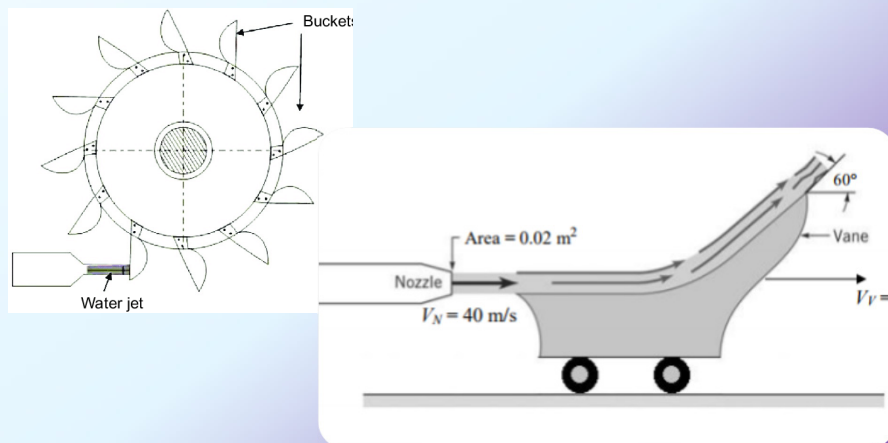


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The (linear) momentum equation

- A simplified model: vane on wheels



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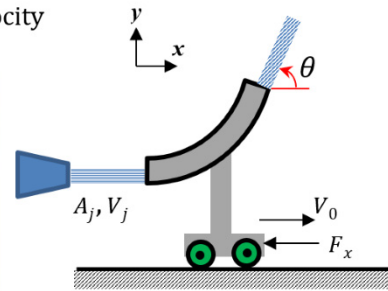
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The (linear) momentum equation

● Sample problem

A water jet impinges upon a vane on wheel as shown in the figure. Calculate the horizontal force, F_x , exerted on the vane system as a function of the given parameters, stating all assumptions you make, when

- The system is immobile.
- The system moves with a fixed velocity of V_0 .



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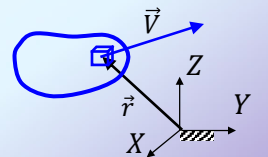
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The angular momentum equation

● For a general control volume

$$\sum \vec{M}_\sigma = \frac{d}{dt} \iiint_{V_\sigma} (\vec{r} \times \vec{V}) \rho dV + \iint_A (\vec{r} \times \vec{V})(\rho \vec{V}_r \cdot \vec{n}) dA \quad (17.7)$$



\vec{r} is the location vector from a fixed point in the inertial frame

● Simplified forms

1. For an inertial C.V.

$$\xrightarrow[\vec{V} \rightarrow \vec{V}_r]{(17.7)} \sum (\vec{r} \times \vec{F}_\sigma) = \frac{d}{dt} \iiint_{V_\sigma} (\vec{r} \times \vec{V}_r) \rho dV + \iint_A (\vec{r} \times \vec{V}_r)(\rho \vec{V}_r \cdot \vec{n}) dA \quad (18.7)$$

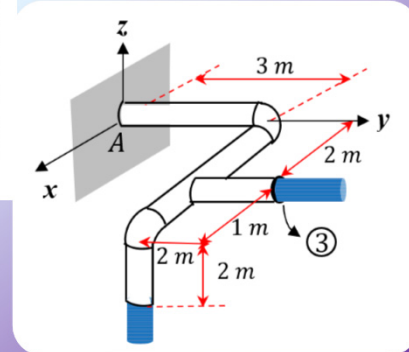
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The angular momentum equation

● Sample problem

The piping system shown in the figure has been attached to the structure at section A. Water flows steadily in the system. The water flow rate and pressure at section A are $Q_A = 0.01 \text{ m}^3/\text{s}$ and $p_A = 300 \text{ kPa}$. Calculate the resultant force and moment exerted from the water and piping system on the wall structure. Water outflow at section 3 is $Q_3 = 0.004 \text{ m}^3/\text{s}$, the internal pipe cross-sectional area is $A_{in} = 2580 \text{ mm}^2$, the specific weight of the system (pipe and water) per unit length of pipes is $W' = 300 \text{ N/m}$, and $\rho_{\text{water}} = 1000 \text{ kg/m}^3$.



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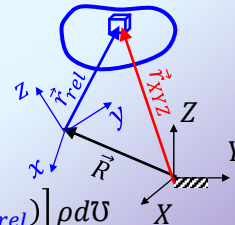
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The (linear) momentum equation

● Using a noninertial reference frame

➡ Lecture Notes



$$\sum \vec{F}_\sigma - \iiint_{V_\sigma} [\ddot{\vec{R}} + 2\vec{\omega} \times \vec{V}_{rel} + \dot{\vec{\omega}} \times \vec{r}_{rel} + \vec{\omega} \times (\vec{\omega} \times \vec{r}_{rel})] \rho dV$$

$$= \frac{d}{dt} \iiint_{V_\sigma} \vec{V}_{rel} \rho dV + \iint_A \vec{V}_{rel} (\rho \vec{V}_r \cdot \vec{n}) dA \quad (14.7)$$

$$\vec{V}_{rel} = \vec{V}_{XYZ} - (\dot{\vec{R}} + \vec{\omega} \times \vec{r}_{rel}) \quad \vec{V}_r = \vec{V}_{XYZ} - \vec{V}_\sigma$$

● Simplified forms (noninertial reference frame)

1. For a nondeforming (rigid-body-like moving) C.V. and the C.V.-attached local reference frame

$$\vec{V}_{rel} = \vec{V}_r$$

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The (linear) momentum equation

- **Simplified forms (noninertial reference frame)**
 2. **For a nondeforming C.V. in a linear motion (uniform $\ddot{\vec{R}}$ and $\vec{\omega} = \dot{\vec{\omega}} = 0$) and the C.V.-attached local reference frame**

$$\iiint_{V_\sigma} \ddot{\vec{R}} \rho dV = \ddot{\vec{R}} \iiint_{V_\sigma} \rho dV = \ddot{\vec{R}} m_\sigma \longrightarrow$$

$$\sum \vec{F}_\sigma - m_\sigma \ddot{\vec{R}} = \frac{d}{dt} \iiint_{V_\sigma} \vec{V}_r \rho dV + \iint_A \vec{V}_r (\rho \vec{V}_r \cdot \vec{n}) dA \quad (15.7)$$

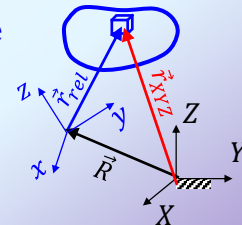
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The angular momentum equation

- **Using a noninertial reference frame**
 - **Exercise: Show that**

$$\begin{aligned} & \sum (\vec{r}_{rel} \times \vec{F}_\sigma) - \\ & \iiint_{V_\sigma} \vec{r}_{rel} \times \left[\ddot{\vec{R}} + 2\vec{\omega} \times \vec{V}_{rel} + \dot{\vec{\omega}} \times \vec{r}_{rel} + \vec{\omega} \times (\vec{\omega} \times \vec{r}_{rel}) \right] \rho dV = \\ & \frac{d}{dt} \iiint_{V_\sigma} (\vec{r}_{rel} \times \vec{V}_{rel}) \rho dV + \iint_A (\vec{r}_{rel} \times \vec{V}_{rel}) (\rho \vec{V}_r \cdot \vec{n}) dA \quad (21.7) \end{aligned}$$



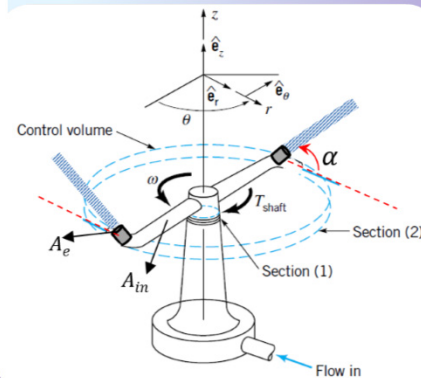
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The angular momentum equation

● Sample problem

The rotary water sprinkler shown in the figure rotates with the constant angular velocity of ω . Calculate the frictional torque on the axis of the sprinkler as a function of the other parameters. The water inflow is q , the length each is arm $\ell/2$, and A_{in} and A_e are the inner cross-sectional area of the arm and ejector exit.



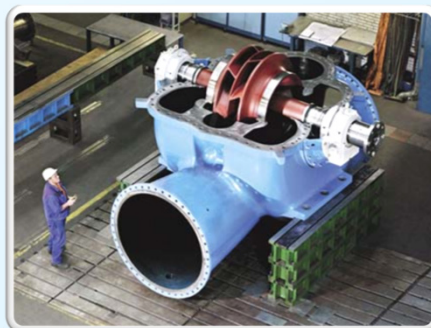
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Turbomachinery

● Radial-flow: centrifugal pump



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Turbomachinery

- Radial-flow: centrifugal pump

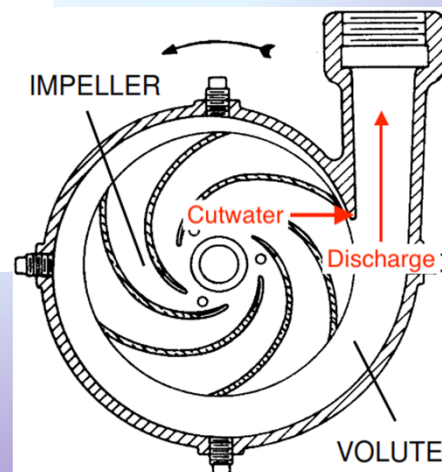


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Turbomachinery

- Radial-flow: centrifugal pump

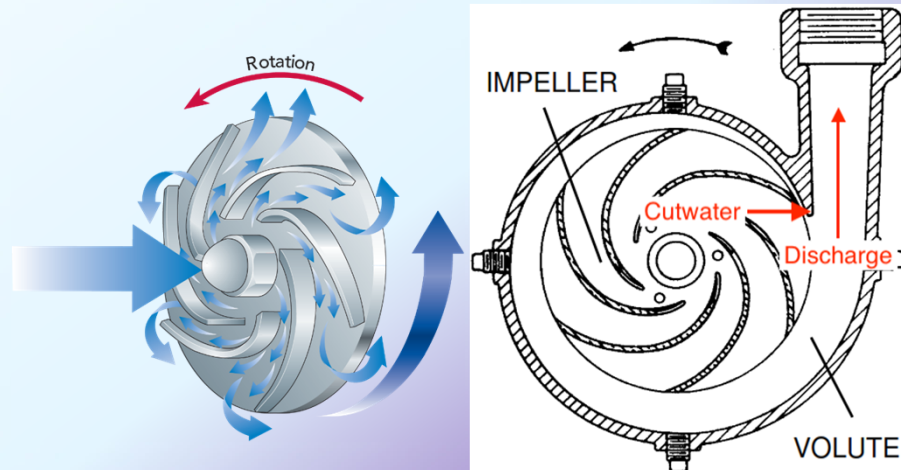


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Turbomachinery

- Radial-flow: centrifugal pump



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- Radial-flow: centrifugal pump



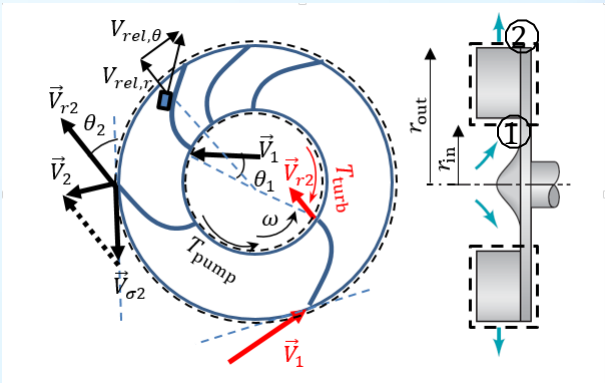
This is an excerpt from our **Centrifugal Pumps** training course.
All of our courses can be found at www.ConvergenceTraining.com

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Turbomachinery

- Radial-flow



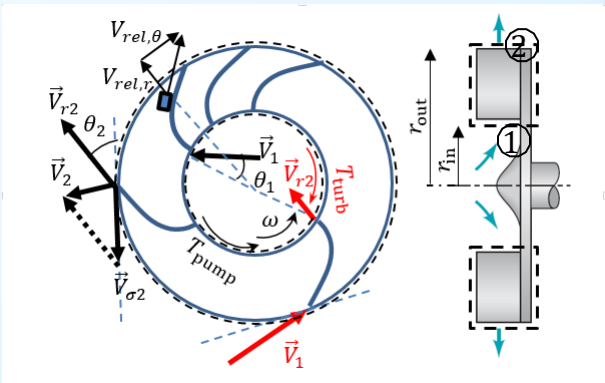
$$\left. \begin{aligned} \vec{V}_r &\rightarrow \vec{W} \\ \vec{V}_\sigma &\rightarrow \vec{U} = r\omega\hat{e}_\theta \end{aligned} \right\} \rightarrow W_r = V_r$$

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Turbomachinery

- Radial-flow



$$T_{shaft} = (-\dot{m}_{in})(r_{in}V_{\theta,in}) + (\dot{m}_{out})(r_{out}V_{\theta,out})$$
$$\dot{W}_{shaft} = T_{shaft} \omega$$

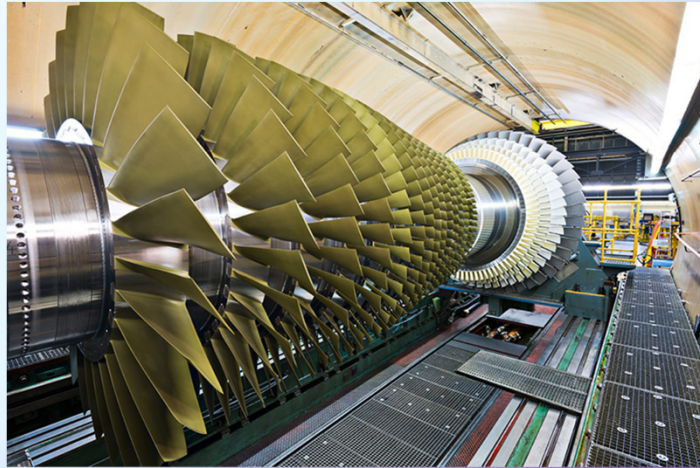
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Proof: Appendix A

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Turbomachinery

- Axial-flow: axial compressor

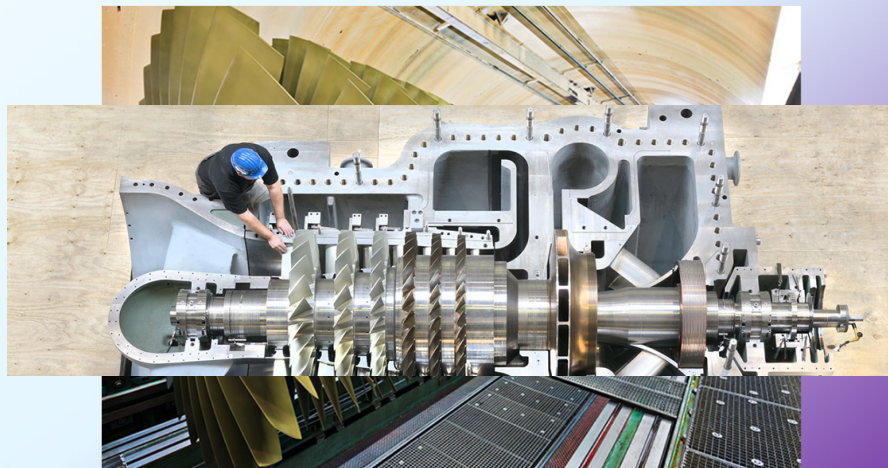


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- Axial-flow: axial compressor

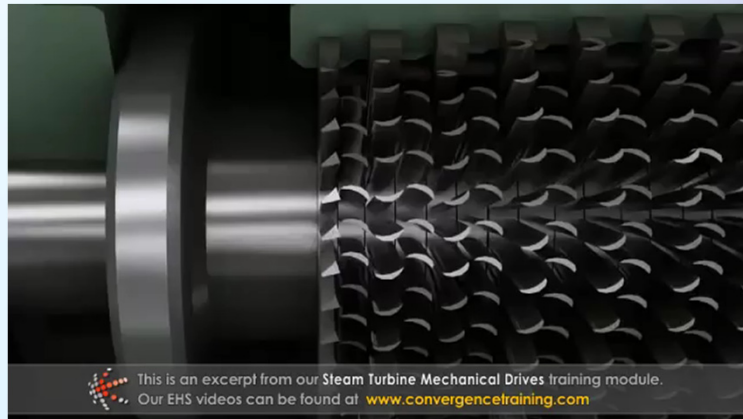


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- Axial-flow: axial compressor

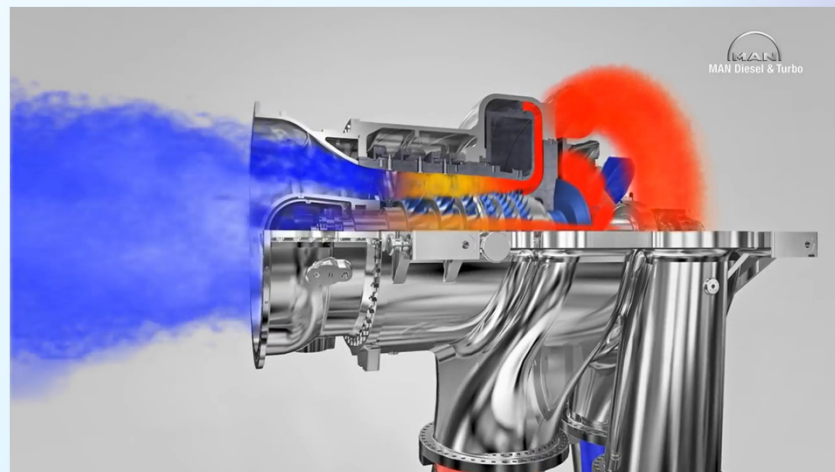


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- Axial-flow: axial compressor

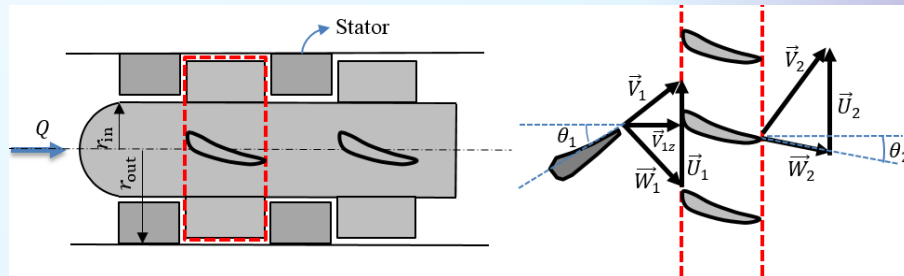


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● Axial-flow



$$V_{1z} = \frac{Q}{A_{out} - A_{in}}$$

$$U = \bar{r}\omega = \left(\frac{r_{out} + r_{in}}{2}\right)\omega$$

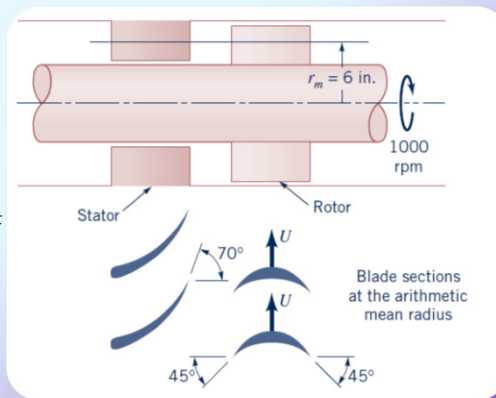
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● Sample problem

The sketch of the arithmetic mean radius blade sections of an axial-flow water turbine is shown in the figure. The rotor speed is 1000 rpm. The inner and outer radius of the blades are $r_{in} = 4 \text{ in}$ and $r_{out} = 8 \text{ in}$. The water flowrate within the turbine is $Q = 0.5 \text{ ft}^3/\text{s}$. Calculate the output power of the turbine. The water density is assumed as 1.94 slug/ft^3 .



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The end of chapter 7

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