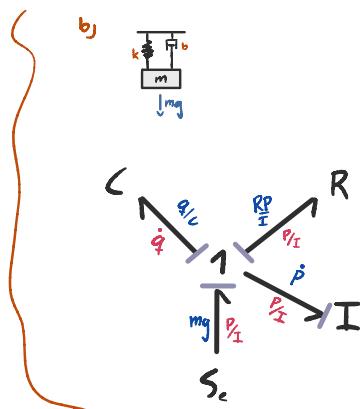
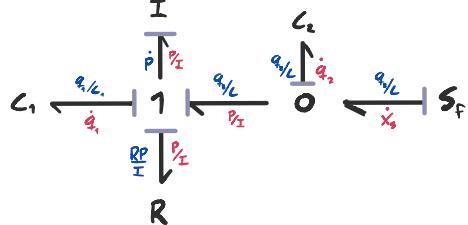


# TEP4240

## System Simulation

### Exercise 4

#### Mechanical Translatory



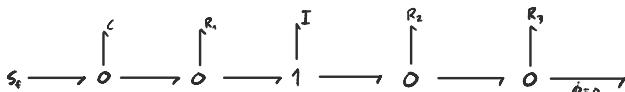
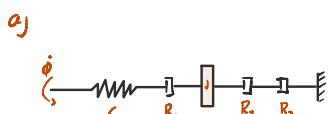
$$\begin{bmatrix} \dot{q} \\ \dot{p} \end{bmatrix} = \begin{bmatrix} \frac{p}{I} \\ mg - \frac{R_P}{I} - \frac{q}{L} \end{bmatrix}$$

Order of the system: 2

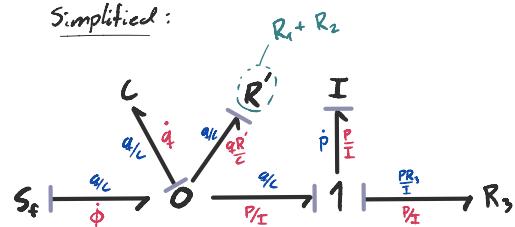
$$\begin{bmatrix} \dot{q}_2 \\ \dot{q}_1 \\ \dot{p} \end{bmatrix} = \begin{bmatrix} \dot{x}_s - \frac{p}{I} \\ -\frac{p}{I} \\ \frac{q_2}{L} - \frac{q_1}{L} - \frac{R_P}{I} \end{bmatrix}$$

Order of the system: 3

#### Mechanical Rotational



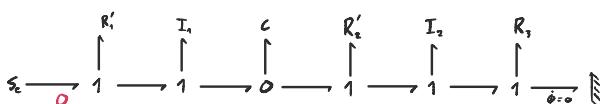
Simplified:



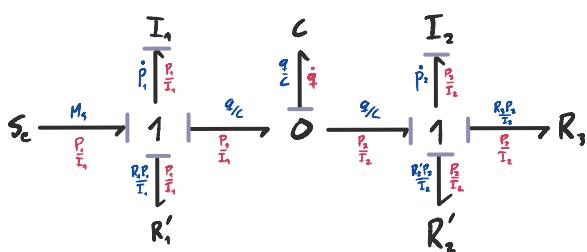
$$\Rightarrow \begin{bmatrix} \dot{p} \\ \dot{q} \end{bmatrix} = \begin{bmatrix} \frac{q}{C} - \frac{PR_3}{I} \\ \dot{\phi} - \frac{q}{C}(R_1+R_2) - \frac{P}{I} \end{bmatrix}$$

Order of the system: 2

c) Let the two resistances be set to a  $R'_1: 2b_1$  and  $R'_2: 2b_2$  since flow is same on both sides of each mass.



Simplified:

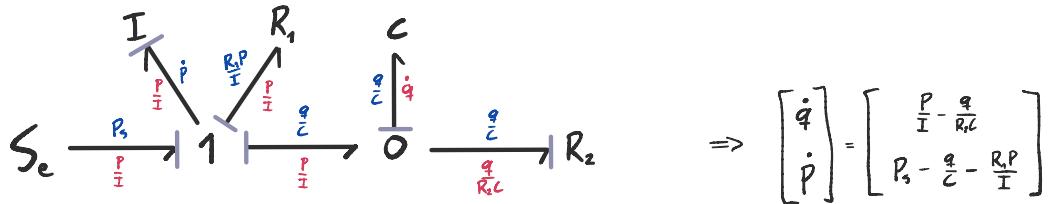


$$\begin{bmatrix} \dot{p}_1 \\ \dot{p}_2 \\ \dot{q} \end{bmatrix} = \begin{bmatrix} M_s - \frac{R'_1 p_1}{I_1} - \frac{q}{C} \\ \frac{q}{C} - \frac{R'_2 p_2}{I_2} - \frac{R'_1 p_1}{I_1} \\ \frac{p_1}{I_1} - \frac{p_2}{I_2} \end{bmatrix}$$

Order of the system: 3

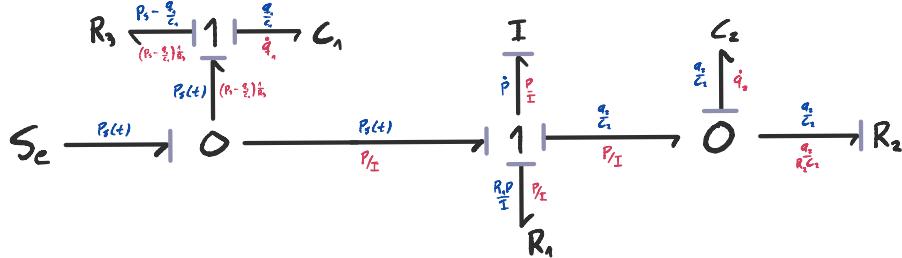
## Fluid

a)



Order of the system: 2

d)



$$\Rightarrow \begin{bmatrix} \dot{q}_1 \\ \dot{q}_2 \\ \dot{P} \end{bmatrix} = \begin{bmatrix} \frac{1}{R_1} \left( P_s(t) - \frac{q_1}{C_1} \right) \\ \frac{P}{I} - \frac{q_2}{R_2 C_2} \\ P_s(t) - \frac{R_p P}{I} - \frac{q_2}{C_2} \end{bmatrix}$$

(Order 3) Where  $P_s$  is gauge pressure for the pump.

For the simulation:

$$\begin{aligned} C_1 &= \frac{A_1}{\rho g} & R_1 &= b_1 \\ C_2 &= \frac{A_2}{\rho g} & R_2 &= b_2 \\ I &= \frac{\rho L}{A_c} & R_p &= b_3 \end{aligned}$$

---

```

clc
close all
clear all

% Differential equations for Fluid system d)
% q1_dot = 1/R3 * (Ps - q1/C1)
% q2_dot = P/I - q2/(R2*C2)
% p_dot = Ps - R1*p/I - q2/C2

% Constants:
rho = 1000; % kg/m3
g = 9.81; % m/s2
A1 = pi*(0.3)^2; % m2
A2 = pi*(0.3)^2; % m2
Ac = pi*(0.5)^2; % m2
b1 = 10; % Ns/m
b2 = 1000; % Ns/m
b3 = 1000; % Ns/m
L = 15; % m

% Definitions
R1 = b1;
R2 = b3;
R3 = b3;
I = rho*L/Ac;
C1 = A1/(rho*g);
C2 = A2/(rho*g);

% Initial conditions
q1_0 = 0; q2_0 = 0; p_0 = 0;
y0 = [q1_0 q2_0 p_0];

%[t, Y] = ode45(@odefun_ex4,[0 40],y0);
[t, Y] = ode45(@(t, y) odefun_ex4(t, y, I, C1, C2, R1, R2, R3), ...
[0 2], y0);
q1 = Y(:,1); q2 = Y(:,2); p = Y(:,3);

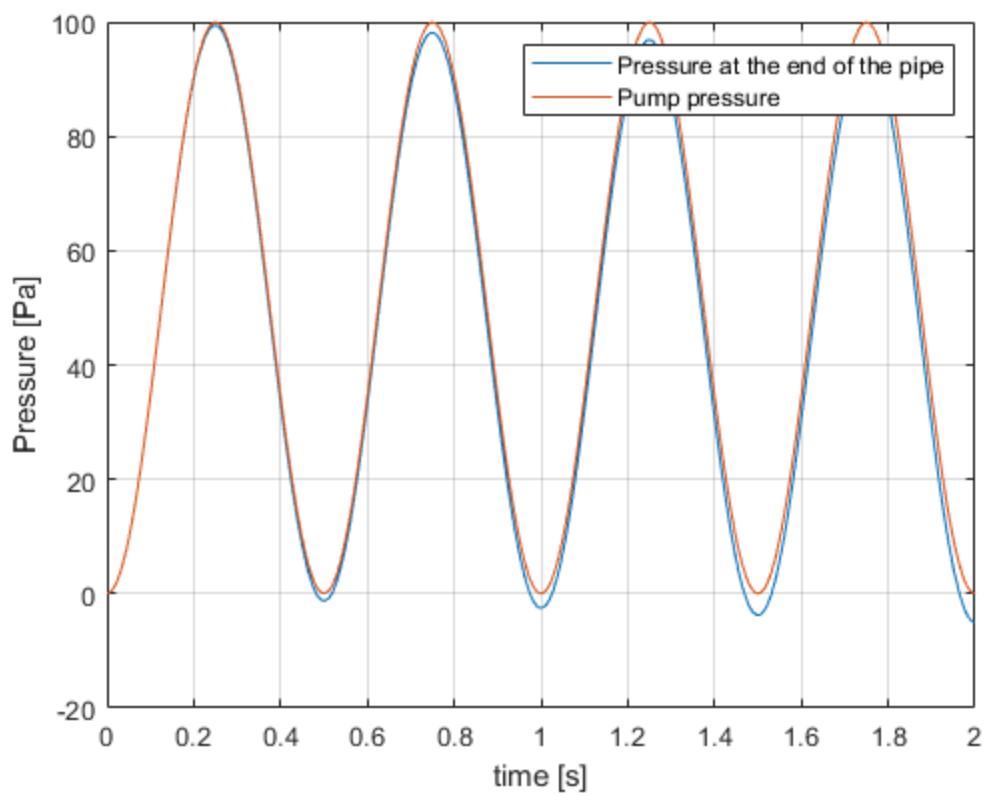
Ps = 100*(sin(2*pi*t)).^2;

q1_dot = 1/R3 * (Ps - q1/C1);
q2_dot = p/I - q2/(R2*C2);
p_dot = Ps - R1*p/I - q2/C2;

plot(t,p_dot, t,Ps);
legend('Pressure at the end of the pipe', 'Pump pressure' )
xlabel('time [s]')
grid on
ylabel('Pressure [Pa]')

```

---



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```
function dydt = odefun_ex4(t, y, I, C1, C2, R1, R2, R3)
    % Extract variables from the y vector
    q1 = y(1);
    q2 = y(2);
    p  = y(3);

    t;
    Ps = 100*(sin(2*pi*t)).^2; % Pascals

    % Define the system of ODEs
    q1_dot = 1/R3 * (Ps - q1/C1);
    q2_dot = p/I - q2/(R2*C2);
    p_dot  = Ps - R1*p/I - q2/C2;

    % Pack the derivatives into a column vector
    dydt = [q1_dot; q2_dot; p_dot];
end

Not enough input arguments.

Error in odefun_ex4 (line 4)
    q1 = y(1);
```

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