

CarbonCloud - Feasibility Study

A Distributed Residential Direct Air Capture Concept

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Abstract

Our considers a dual challenge: the urgent need for Gigaton-scale Carbon Dioxide Removal (CDR) and increasing economic pressure on households. This project investigated a solution to address both: a decentralized Direct Air Capture (DAC) network utilizing the existing HVAC infrastructure found in 75% of American homes.

The core concept proposed a “gig economy” model for carbon: homeowners retrofit their forced-air systems with a smart filter containing a CO₂-selective sorbent. By leveraging airflow already paid for by the homeowner, we hypothesized this network could bypass the massive capital expenses and land-use requirements of centralized industrial DAC plants while providing passive income to families.

In analyzing the concept, we determined the model requires a centralized plant for regeneration of CO₂ gas from saturated sorbent, and thus also requires a logistics network to move sorbent between homes and the regeneration plant.

Our research decomposed this model into four distinct lanes of feasibility:

- **Sorbent Viability:** The chemical capture mechanism is technically feasible. Research indicates Class IV Amine-based sorbents are currently the optimal choice for residential deployment, offering a capture capacity of ≈ 2.5 mmol/g under standard indoor conditions. However, strictly residential constraints (e.g., the prohibition of toxic materials like NaOH, a maximum comfortable lift weight of 10kg) limit the total capture volume per unit.
- **Net-Carbon Logistics:** The “last mile” distribution of filters is net carbon-negative, even for diesel vehicles in dense geographies. The captured CO₂ yield of this scheme is small (9MMT) compared to e.g. passenger car emissions (1000MMT), but we find the total possible amount of CO₂ in residential homes is much larger.
- **CO₂ Regeneration:** While capturing the carbon is passive (using existing fans), releasing the carbon for sequestration or utilization requires the input of a significant quantity of external energy (thermal and/or electrical). Using a centralized regeneration facility, the energy cost is significant but still potentially workable. Powering the process with industrial waste heat or off-grid renewables could substantially improve both the financial and emissions cost. However, the construction of a centralized regeneration facility would defeat the original intent of avoiding the construction of a high CAPEX DAC plant.
- **Market Economics:** The original business model of paying homeowners for their carbon is not currently viable. With beverage-grade CO₂ trading at maximum \sim \$600–\$1000/metric ton, the maximum yield per household is approximately \$5 per month. This amount is insufficient to incentivize behavior change or justify the “gig economy” narrative. Worse, the logistics network to transport saturated filters to a centralized regeneration facility costs more per pickup than the revenue generated by the carbon.

Based on these findings, an “AirBnB for Carbon” income model is not currently supported by market prices for CO₂ and due to the high costs associated with deploying CO₂ transportation and logistics for such a decentralized capture network. However, the infrastructure advantage remains valid. For this venture to proceed *today*, we would recommend a strategic pivot from an income-generation model to a consumer-product model. Rather than paying homeowners, the system would be marketed as a premium “Ultra-Pure Air” service (e.g., \$100/year subscription) that removes indoor pollutants while passively capturing carbon dioxide.

1 Introduction

The global conversation regarding climate change has shifted. While reducing greenhouse gas emissions remains critical, the scientific consensus is clear: mitigation alone is insufficient. In order to avoid the worst impacts of climate change, humanity must also remove CO₂ from the atmosphere. Since the dawn

of the industrial age, humanity has emitted an estimated 2.5 trillion metric tons of CO₂. To avoid the most catastrophic effects of warming, we must begin the monumental task of drawing that number down.

The mandate for Carbon Dioxide Removal (CDR) is clear, but the mechanism of delivery is not. Most current efforts focus on Direct Air Capture (DAC) through massive, centralized industrial projects. While technologically impressive, these “green megaprojects” face significant headwinds. They require immense capital expenditure to acquire land and construct facilities, they must navigate complex governmental permitting and licensing, and they are increasingly vulnerable to political volatility.

There is, however, an alternative approach: decentralization. Climate solutions that are modular and scalable have the distinct advantage of incremental deployment. By utilizing existing infrastructure and spreading capital risk, a decentralized network can scale organically, bypassing hurdles that stall centralized plants. As the logic goes: stopping a single reforestation project on 1,000 acres is legally simple; preventing 1,000 individual homeowners from planting ten trees each is nearly impossible.

The primary criticism of DAC is the concentration problem. With atmospheric CO₂ concentrations having recently crossed past 420 ppm (up from \approx 280ppm in pre-industrial times), capturing carbon is frequently likened to finding 420 blue ping-pong balls in a pool of one million white ones. Catching those molecules requires processing massive volumes of air through a dedicated capture material (solid sorbent, or liquid solvent). In traditional DAC models, this means deploying many large industrial fans, which introduces a new, significant energy penalty.

However, a massive infrastructure for moving air already exists. Hotels, offices, schools, and many millions of homes utilize central Heating, Ventilation and Air Conditioning (HVAC) systems. In the United States, a vast majority of households—approximately 75%—rely on forced-air systems to heat and cool their homes. Taken together, these systems circulate immense volumes of air, fueled by energy the homeowner has already paid for.

This pre-existing distributed asset presents a unique hypothesis: Can we leverage the airflow from installed HVAC systems to extract carbon dioxide without additional kinetic energy expenditure? Furthermore, given the economic pressures of inflation and the normalization of the “gig economy,” could homeowners be compensated for this service? Just as residential solar panels distribute electricity generation to the grid, could residential HVAC systems distribute carbon capture for the planet?

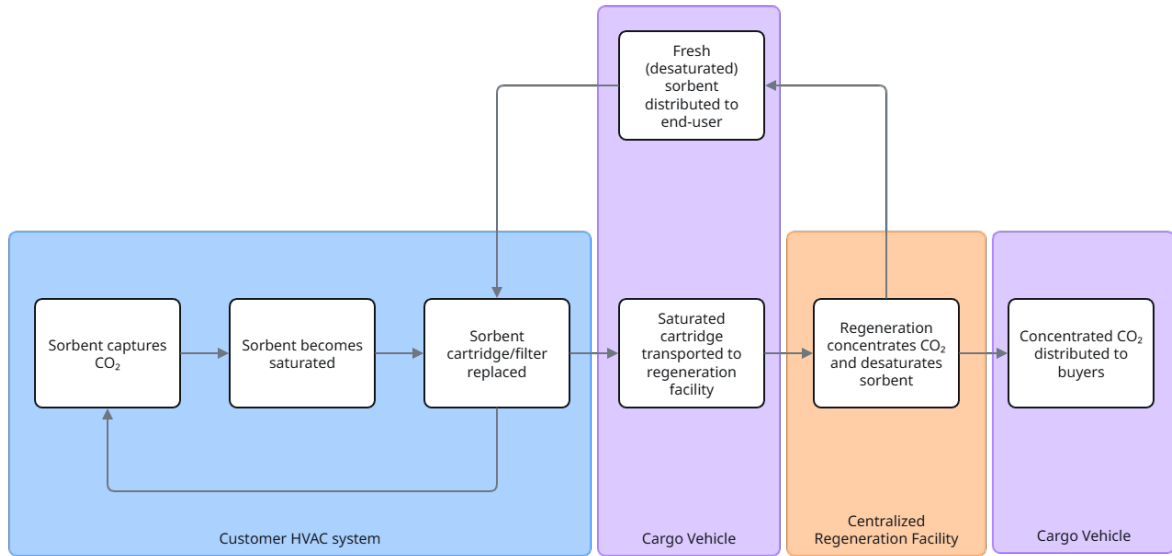


Figure 1: illustration of the proposed distributed carbon capture network

1.1 Proposed distributed direct air capture model

In working through the concept, we designed a solution involving 4 operational steps (illustrated in Figure 1):

1. **CO₂ Capture:** CO₂ from the interior air of a home passing through the home’s HVAC system is captured in a filter or cartridge containing a solid sorbent.

2. **Cartridge swap:** A logistics network delivers a fresh filter/cartridge and manually swaps it in for the saturated one, bringing the saturated cartridges to a centralized plant.
3. **Regeneration:** Instead of regenerating the CO₂ inside the home, saturated filters are delivered to a central plant where CO₂ gas is liberated from the saturated cartridges via an industrial regeneration process and stored in concentrated form.
4. **Sale:** The concentrated CO₂ is shipped to buyers in the industrial wholesale market for use as a process input or permanently sequestered.

1.2 Scope of Analysis

This white paper investigates the feasibility of a residential, distributed DAC network. Our research aims to answer the critical questions: Can we harness existing residential airflow for carbon capture? Is the lifecycle carbon negative? And finally, who pays for the captured carbon?

The remainder of this paper details these findings as follows:

- Section 2 presents the basic details of carbon capture technology with examples of commercial projects in a range of formats.
- Section 3 provides a technical review of the state-of-the-art in sorbent technology, specifically analyzing Class IV Amine-based sorbents suitable for safe, residential use.
- Section 4 models the logistics of a decentralized “last-mile” system, analyzing the emissions caused by distributing and reclaiming filters versus the carbon captured.
- Section 5 examines regeneration methods, outlining the energy requirements (OpEx) and complexity (CapEx) that currently threaten the viability of the model.
- Section 6 discusses the economics of this venture, analyzing markets for captured carbon dioxide, the revenue potential of selling food and beverage grade CO₂ versus carbon credits and other potential commodities, and considering the costs of operation.
- Section 7 summarizes our findings and outlines the technological and economic developments required to make decentralized residential DAC a reality.

2 Background

2.1 Overview of Carbon Capture processes

Scientists and engineers have researched a range of technologies and processes for capturing carbon dioxide from gas mixtures, including ambient air and combustion/industrial exhaust. Generally, these processes can be divided into two families based on the concentration of CO₂ in the input airstream:

- **Point-Source Capture** refers to scrubbing CO₂-rich gas mixtures, generally associated with the exhaust gas from furnaces, vehicles or industrial chimneys. The precise concentration of CO₂ varies, but research in this area often assumes a minimum 10% CO₂ concentration.
- **Direct Air Capture (DAC)** refers to scrubbing CO₂ from ambient air, where its concentration is around 422 parts per million (or $\sim 0.04\%$).

2.1.1 Emissions Reduction vs. Carbon Removal

Though the technologies involved may be similar or even identical, there is an important difference between capturing CO₂ from the atmosphere (carbon removal) versus capturing CO₂ from an exhaust stream before it enters the atmosphere (emissions reduction). Point-source capture projects are always examples of emissions reduction, whereas DAC projects generally represent carbon removal.

The concentration of greenhouse gases (GHGs) in the atmosphere drives climate change. The most widespread GHG is carbon dioxide. According to the Intergovernmental Panel on Climate Change, the average global temperature will stop rising when we stop increasing the concentration of GHGs in the atmosphere, i.e. when we reach “net-zero” emissions. Net-zero can be achieved by a combination of

eliminating human-caused GHG emissions (for example, by replacing fossil fuels with renewable energy sources) and offsetting any remaining emissions with new carbon removals.

While carbon capture for emissions reduction is geared towards abating carbon emissions, it is never 100% effective, meaning that any project with carbon capture for emissions *reduction* is still ultimately a source of carbon emissions that need to be halted entirely or offset by carbon *removals*. Permanent emissions reductions remain an absolutely critical part of the global response to climate change, particularly in the short to medium term, while carbon removals will be necessary in the long term to reach net-zero and eventually net-negative carbon emissions.

2.2 Point-Source Capture

Point-Source carbon capture systems have been in operation at industrial scale since at least the 1980s. In general, point-source capture systems operate at higher temperature, pressure, and humidity than DAC systems (and always at higher CO₂ concentration). Point-source capture systems are usually installed in close proximity to sources of waste heat and/or pressure gradients (i.e. energy generated from the systems/processes that are emitting CO₂) that might serve to offset the energy requirements of regeneration.

The Shute Creek Carbon Capture, Utilization and Storage (CCUS) site operated by Exxon-Mobile in Wyoming, US, serves as an early example of industrial-scale point-source capture. Oil and gas companies developed CCUS not as an emission-reductions process, but as a way to extract additional revenue from their methane value chain by selling captured CO₂ back to oil companies, who use it as part of an enhanced technique to pump hard-to-extract oil from otherwise-depleted wells. While the pumped CO₂ remains underground, the recovered oil - once burned for fuel - releases additional CO₂ that negates the carbon capture benefits.

According to a 2022 report from the Institute for Energy Economics and Financial Analysis [1], Shute Creek has produced approximately 240 million metric tons (MMT) of CO₂ over its lifetime. Of that total, the facility vented approximately half into the atmosphere. A further $\approx 47\%$ of that CO₂ was sold to oil companies for enhanced oil recovery, leaving only $\approx 3\%$ (or 6MMT) that has been sequestered and prevented from reaching the atmosphere.

The Illinois Industrial Carbon Capture and Storage Project in Decatur, Illinois opened in 2011 - one of a small number of point-source capture facilities in the U.S. whose primary purpose is to permanently sequester captured CO₂. The capture system feeds off of a corn ethanol production facility run by Archer Daniels Midland (ADM), which means that rather than use a chemical process to adsorb CO₂ in a sorbent or solvent, this project releases CO₂ as the output of a biological fermentation process, capturing 10–12% of that plant’s annual CO₂ emissions totalling ≈ 4 MMT per year. The project has received hundreds of millions of dollars of U.S. government subsidies. Environmental advocates, such as the Environmental Integrity Project[2], criticize the project for its relatively high expense and low efficiency as an emissions-reduction project.

2.3 Direct Air Capture

Direct Air Capture (DAC) systems for climate mitigation were first considered in the late 1990s, though chemical approaches for removing CO₂ from air have been used in life-support applications (in submarines, and later, spacecraft) for hundreds of years (perhaps even as early as the 1600s according to contemporaneous accounts including that of Robert Boyle in his 1660 *New Experiments Physico-Mechanicall, Touching the Spring of the Air*).

The company Climeworks opened the world’s first commercial Direct Air Capture (DAC) project in 2017 in Switzerland. Climeworks opened a second facility in Iceland (named Orca) in 2021 and a third (named Mammoth) in 2024, capable of removing 4,000 metric tons and 36,000 metric tons respectively. Climeworks has partnered with another company, CarbFix, to permanently sequester the captured carbon from the latter two projects onsite. Climeworks plans to open a plant with a megaton annual capacity by 2030, and a gigaton capacity by 2050.

As of late 2025, there are many companies pursuing various DAC technologies, but only a small number of operational commercial projects at similar scale to the Climeworks projects, including Heimdal’s Project Bantam in Oklahoma. Notably, 1PointFive and Carbon Engineering expect to commission their Stratos facility by 2026, with a planned initial capture and storage capacity of 500,000 metric tonnes (i.e. 0.5 MMT) per year.

2.4 Point-Source Capture vs Direct Air Capture

The general shape of the capture process is the same between these families: a solid sorbent or liquid solvent is exposed to a gas mixture and it absorbs CO_2 . Once saturated, the sorbent/solvent is exposed to a change of pressure and/or temperature to release the CO_2 .

While the small number of commercial point-source capture projects operate at higher scale than the even-smaller number of commercial DAC projects, point-source systems cannot serve the purpose of carbon removal. Limiting warming to 1.5°C above pre-industrial levels requires *removing* CO_2 from the atmosphere.

Table 1: Examples of commercial carbon capture

| Example | Capture Type | Siting | Adsorption Medium | Regeneration Process | Scale (per year) |
|-------------------------|--------------|-------------------------|----------------------|--------------------------|--------------------------|
| Shute Creek CCUS | Point-source | Gas processing plant | Liquid Amine | Temperature Swing | ≈ 6.2 MMT |
| Illinois Industrial CCS | Point-source | Corn ethanol plant | N/A (fermentation) | N/A (fermentation) | ≈ 4 MMT |
| Climeworks Mammoth | DAC | Dedicated plant | Solid amine | Temperature-Vacuum Swing | $\approx 36,000$ MT |
| Remora Carbon | Point-source | Freight truck | <i>not disclosed</i> | Vacuum swing | ≈ 150 MT |
| Seabound UBC Cork | Point-source | Cargo ship | Calcium hydroxide | N/A (mineralization) | likely low 10,000s MT |
| Soletair Aarhus pilot | DAC | Building HVAC | Solid amine | Temperature-Vacuum swing | ≈ 15 MT/ |
| Carbon Reform NJ pilot | DAC | Building HVAC | <i>Not disclosed</i> | N/A (mineralization) | <i>not disclosed</i> |
| Atalanta Climate Ovi | DAC | Consumer device in-room | Amine-based resin | Chemical swing | <1 MT |

2.5 Distributed Carbon Capture

In contrast to the capture systems described above where a single project site collects a large volume of CO_2 , distributed carbon capture describes projects where many individual sites each capture relatively small amounts of CO_2 . This nascent area of carbon capture can include examples of both point-source emissions reduction and atmospheric carbon removal.

2.5.1 Point-Source Reduction from Heavy Transportation

The transportation sector is responsible for 16-23% of global CO_2 emissions. The fast adoption of electric autos is driving significant emissions reductions for passenger road travel (which accounts for $\approx 45\%$ of transportation emissions), but other forms of transportation are harder to decarbonize. Freight trucks are responsible for $\approx 30\%$ of transportation emissions globally.

Remora Carbon, founded in 2020, has partnered with U.S. freight shipping companies to bring to market an on-vehicle point-source capture technology that retrofits onto existing vehicles.

Remora claims their technology captures up to 90% of CO_2 emissions from the exhaust streams of semi-trucks and diesel locomotives. The captured CO_2 is regenerated on-vehicle using a vacuum-swing process and eventually sold as food and beverage grade CO_2 with the profits of sale shared between Remora and the vehicle owner. Press releases from 2025 claim that Remora’s technology would be actively piloted on roads and rail in 2025 but no data is publicly available about the scale of current deployment.

Maritime transport represents around 3% of global GHG emissions. Experts consider the sector hard to decarbonize since large vessels often remain at sea for extended periods making plug-in battery storage systems infeasible. Seabound, founded in 2021, sells a modular onboard carbon capture system that retrofits existing seagoing vessels. Their technology uses a calcium hydroxide sorbent (a.k.a. slaked lime) that captures CO_2 and transforms into calcium carbonate (a.k.a. limestone) that can be sold as a raw material for the production of cement.

Seabound launched their first commercial system in 2025 on the UBC Cork (a cement-shipping vessel). Seabound claims their technology can capture up to 95% of a vessel’s CO_2 emissions and they plan to capture at least 100 MMT of CO_2 annually by 2040, representing around 10% of current shipping emissions[3].

2.5.2 Direct Air Capture from Commercial Buildings

Building operations are responsible for 26-27% of global CO₂ emissions due to a combination of:

- **Direct emissions:** On-site burning of fossil fuels (e.g. for heating/cooling of air or water)
- **Indirect emissions:** Off-site burning of fossil fuels to produce electricity used for heating/cooling, lighting, and other functions

While total global emissions are higher from residential buildings than commercial buildings, commercial buildings represent a more-concentrated source of CO₂ emissions in a setting that often has (at least in the U.S. context) substantial mechanical infrastructure that can serve as a point of entry for capture systems.

Soletair, founded in 2016, is currently piloting a modular DAC system that can be integrated into commercial Heating, Ventilation and Air Conditioning (HVAC) systems. Their technology feeds off of fresh outdoor intake air.

Soletair's technology uses amine functionalized sorbents and a temperature-vacuum swing regeneration process on-site. The regenerated CO₂ gas is compressed, stored in a tank, and eventually transported offsite for permanent storage or sale to a buyer.

Soletair's system is in pilot commercial deployment in an office building in Aarhus, Denmark, which they claim is the "world's first facility capturing CO₂ from the ventilation air in an office building." This pilot project captures approximately 15 tons of CO₂ per year at a purity of around 98%^[4].

Carbon Reform, founded in Philadelphia, PA, USA in 2020, has developed a similar solution, though their technology removes CO₂ from the HVAC system's *return air* where it is more highly-concentrated than the outdoor intake air. The Carbon Reform system retrofits onto existing HVAC systems and diverts the return air into a "Carbon Capsule" consisting of various filters and a CO₂ removal medium. The system produces limestone as an output, like Seabound's maritime system, which is collected and sold for application in construction materials.

In addition to emissions reduction, Carbon Reform's system is marketed for its co-benefits, including purification of indoor air from CO₂, particulate matter, pathogens, and Volatile Organic Compounds (VOCs); and decreasing building operations costs (since the purified return air can be recirculated, reducing the need to move and heat/cool outdoor air)^[5].

Carbon Reform achieved their first commercial installation in July 2025 at a facility owned by New Jersey Natural Gas. They have not publicly release information about the scale of the installed unit.

2.5.3 Direct Air Capture from Residential Buildings

While residential buildings represent the larger portion of building operations emissions (owing to the vastly larger number of residential buildings than commercial and industrial buildings), their emissions are less concentrated.

Atalanta Climate launched their first product, Ovi, in September 2025, with expected shipments in 2026. Ovi is a consumer device, similar in profile to existing home air purifiers and it performs filtration of particulates, pathogens, and VOCs in addition to CO₂ removal.

According to a 2025 CleanTechnica article, Ovi uses an amine-based resin as a sorbent and performs regeneration onboard, combining the sorbent with mildly salty water to produce a sodium hydroxide solution that is then washed over gypsum capsules to form a calcium carbonate powder as a waste product that can be removed by the system's user. The system uses a similar amount of electricity compared with standard air purifiers and, according to Atalanta's testing, is net carbon negative in its lifecycle, emitting around 500g of CO₂ for every 1000g removed. The system requires its user to periodically add fresh gypsum capsules and water. Atalanta claims that a single Ovi unit removes an amount of CO₂ equivalent to having "thousands of spider plants in the room"^[6].

3 Adsorption

3.1 Sorbent Landscape

The current Direct Air Capture (DAC) landscape is characterized by two main architectural approaches:

1. **Solid Sorbent:** This architecture employs porous filters that are often functionalized with an active chemisorption agent such as amines. Atmospheric air is drawn through the filter, where CO₂ chemically binds to the sorbent's surface.

2. **Liquid Solvent:** This method moves air through a chemical solution such as potassium hydroxide (KOH, also known as caustic potash) in an "air contactor" (like a cooling tower) where CO₂ is absorbed into the solution oftentimes as a carbonate salt.

Residential DAC would be an innovative hybrid approach. It adopts the core solid sorbent technology typical of large-scale DAC but decentralizes the capture units. This distribution is specifically designed to capitalize on the distinct atmospheric and environmental conditions found within the built environment. The residential setting offers a unique thermodynamic advantage:

- **CO₂ Enrichment:** Human respiration elevates indoor CO₂ levels significantly above ambient. In an occupied bedroom or living room, levels frequently reach approximately around 800 ppm [20].
- **Isotherm Implications:** Operating at 800 ppm rather than 400 ppm effectively doubles the partial pressure driving force. For many sorbents, this can increase the working capacity by 30-50 percent compared to an outdoor unit. A residential DAC system effectively "feeds" on the occupants' exhalations, turning the home into a pre-concentrator and improving the overall system efficiency.

The critical component of the Residential DAC system is the sorbent material. Unlike industrial settings where liquid solvents like caustic potash (KOH) are acceptable, the residential context demands materials that are non-toxic, solid-state, and capable of operating at ambient temperatures and varying humidity levels.

3.2 Properties of Sorbents

Selecting the best sorbent is a multi-faceted optimization challenge. The following properties[15] need to be considered while selecting the sorbent for a specific application – residential DAC in the present case:

- **Absorption Capacity (Gravimetric):** This is the most crucial logistical factor, measured as the weight of CO₂ captured per unit weight of the sorbent. Higher capacity minimizes the mass that needs to be sourced, handled and transported.
- **Kinetics (Uptake Rate):** A faster rate of CO₂ absorption enables the use of smaller devices and allows for lower fan speeds, which directly reduces noise levels.
- **Regeneration Parameters:** This refers to the energy input (specifically the required temperature and pressure) needed to release the captured CO₂ for disposal or reuse. Section 5 of this white paper examines regeneration in detail. .
- **Stability:** The degree to which the material resists degradation (such as oxidation or hydrolysis), which determines the working life of the sorbent in terms of capture and release cycles.
- **Atmospheric Range:** The sorbent must be engineered to perform optimally within the narrow temperature range (18–25°C) and humidity range (30–60% RH) characteristic of occupied living spaces.

The fundamental challenge in Residential DAC absorption is competition. The atmosphere is predominantly Nitrogen (N₂) and Oxygen (O₂), but the most aggressive competitor is Water Vapor (H₂O). At 25°C and 50% Relative Humidity (RH), the concentration of water vapor is approximately 1.5%, nearly 40 times higher than the (CO₂) concentration (0.04%). If a sorbent attracts water and CO₂ with equal strength (non-selective physisorption), the water molecules will statistically overwhelm the active sites, effectively drowning the sorbent. The material must therefore be chemically selective, interacting with CO₂ through specific molecular recognition (acid-base chemistry) rather than generic surface adhesion. This thermodynamic reality drives the preference for chemisorbents (amines) over physisorbents (zeolites) in humid environments[15].

3.3 Comparative Sorbent Matrix

1. **Solid Supported Amines:** Solid amines currently represent the gold standard for Direct Air Capture due to their robust performance in humid conditions. They attempt to replicate the

efficacy of liquid amine scrubbers used in power plants but anchor the active molecules to a solid substrate to prevent off-gassing and corrosion – essential requirements for residential safety.

Amines are organic derivatives of ammonia (NH_3). In the context of DAC, they function as bases that react with the acidic (CO_2) molecule. The reaction pathway is heavily influenced by the presence of water, making them uniquely suited for the "atmospheric range" of a home. This reaction pathway operates differently in presence and absence of humidity. In the absence of water (dry pathway), primary and secondary amines react with CO_2 to form ammonium carbamate. This mechanism requires two amine groups to bind one CO_2 molecule, resulting in a maximum theoretical efficiency of 0.5 moles of CO_2 per mole of amine. Whereas, in the humid air (wet pathway) of a residence, water molecules participate in the reaction, facilitating the formation of bicarbonates. This pathway allows for a 1:1 stoichiometry. Consequently, humidity, which is often a poison for other sorbents, actually enhances the capacity of amine-based materials[15][16].

To select the best sorbent, one must distinguish between the classes of solid amines, each offering a different trade-off between capacity and stability[15].

- *Class 1 (Physically Impregnated):*

- Structure: High-molecular-weight polymers like Polyethylenimine (PEI) are physically "stuffed" into the pores of a support (e.g., silica or alumina).
- Pros: Exceptional capacity (high amine density). Low manufacturing cost.
- Cons: The amines are held only by weak physical forces. They can leach out over time or volatilize. The potential for "amine leaching" poses a significant customer acceptance risk. The smell of amines (resembling rotting fish or ammonia) in a home would likely be a dealbreaker for most homeowners.

- *Class 2 (Covalently Tethered):*

- Structure: Silane (SiH_4) chemistry is used to form a permanent covalent bond between the amine and the silica support.
- Pros: Extreme stability. The amine cannot wash off or volatilize, guaranteeing no off-gassing.
- Cons: Lower amine density compared to Class 1 (limited by surface area). Higher manufacturing cost.

- *Class 3 (In-situ Polymerized Amines):*

- Structure: Monomers are polymerized directly inside the pores, creating a hybrid structure.
- Pros: Balances high capacity with better stability than Class 1.
- Cons: Currently an area of active R&D, potentially offering a future upgrade path.

- *Class 4: Hybrid / Crosslinked Solid Amine Networks:*

- Structure: Uses a cross-linker to tie liquid amine molecules (like Polyethyleneimine - PEI) together into a rigid, 3D net that is chemically locked in place. The material acts like a solid but has the high CO_2 -grabbing density of a liquid.
- Pros: High stability. Amines are chemically locked, which prevents leaching and eliminates the risk of "off-gassing." High concentration of amine groups allows for a much smaller physical capture device.
- Cons: Sensitive to heat (above 120°C) and oxygen, which causes degradation. High density slows reaction kinetics, possibly necessitating stronger (and louder) fans. Expensive, specialized manufacturing process and an active thermal regeneration cycle for cleaning.

Amines are susceptible to oxidative degradation. Exposure to oxygen at high temperatures (during regeneration) causes the amine chains to break down, forming urea linkages that permanently deactivate the material. The regeneration cycle must be performed in an oxygen-depleted environment (vacuum or steam purge). This adds complexity and further challenges to the centralized regeneration facility but preserves the cartridge life for hundreds of cycles.

2. **Metal-Organic Frameworks (MOFs):** Metal-Organic Frameworks are crystalline polymers composed of metal nodes (clusters) connected by organic linkers. They are often described as "molecular sponges" due to their unprecedented internal surface areas (up to $7,000 \text{ m}^2/\text{g}$)[18].

Materials such as *Mg-MOF-74* and *UiO-66-NH₂* have shown promise. *Mg-MOF-74* has open metal sites that bind CO₂ strongly, while UiO-66 offers a robust zirconium backbone for stability. Despite their lab performance, MOFs struggle with the "atmospheric range" of a residential environment.

Early MOFs (like MOF-5) would collapse structurally upon exposure to humidity, turning into a non-porous powder. While newer generations are water-stable, they still face competitive adsorption. Water molecules, being polar, are often attracted to the same sites as CO₂.

Synthesis of MOFs requires expensive metal salts and complex organic ligands. Currently, MOF production costs are orders of magnitude higher than amines or zeolites (\$500-\$5,000/kg vs \$10-\$50/kg). For a residential business model reliant on affordable consumer cartridges, the high production cost of MOFs is currently prohibitive unless the cycle life extends to thousands of uses, which has not yet been demonstrated in real-world atmospheric conditions.

3. **Moisture Swing Adsorbents (MSA):** Moisture Swing Adsorbents allow for a paradigm shift in the regeneration process. While TSA (Temperature Swing) and PSA (Pressure Swing) use energy to drive off CO₂, MSA uses water[19].

These materials are typically anion-exchange resins consisting of a polymer backbone functionalized with quaternary ammonium cations. When the material is dry, the cations are exposed and bind CO₂ strongly as bicarbonate or carbonate. When the material is exposed to liquid water or very high humidity, the hydration energy of the ions overcomes the binding energy of the CO₂. The structure releases the CO₂ to solvate itself with water.

MSAs offer the lowest theoretical energy penalty. The release of CO₂ consumes no heat. The cost is the evaporation of the water from the material to return it to the dry state for the next capture cycle. In arid climates, this drying can happen passively using ambient wind and solar energy. In the context of a centralized industrial facility, regeneration would consist of wetting the cartridges to release gas, then drying them.

Being polymer-based (like plastic beads), MSAs are mechanically robust and resistant to oxidation, offering excellent reusability. However, during adsorption, the capture rate is inversely proportional to humidity. In a typically-humid U.S. home (e.g., >50% RH), the sorbent would behave as if it is partially in "regeneration mode," preventing effective capture. Overcoming the challenge would mean requiring some kind of conditioning/dehumidifying step within the HVAC system, at least some of the time.

4. **Zeolites (Physical Adsorbents):** Zeolites are naturally occurring or synthetic aluminosilicate minerals with rigid, microporous crystalline structures. Zeolites are commoditized and incredibly cheap (\$2-\$5/kg). Zeolite 13X is the industry standard for CO₂ removal in closed-loop life support (e.g., ISS, submarines) and industrial gas purification[20].

Zeolite 13X is extremely hydrophilic – it loves to bond with water. The heat of adsorption for water on Zeolite 13X is significantly higher than for CO₂. In any atmosphere containing moisture, the zeolite will preferentially fill its pores with water molecules. To use zeolites for DAC, the air stream must first be essentially bone-dry. This could be achieved with a "guard bed" of desiccant (like silica gel) placed before the zeolite.

However, the desiccant for the guard bed would need to be regularly replaced or regenerated by applying heat to remove the water it absorbed. This might be feasible in a system with on-site regeneration for the sorbent, though it would significantly increase the regeneration energy requirements. With centralized regeneration of the sorbent, the desiccant would either need its own in-home regeneration system, or to be transported alongside the sorbent to a central facility. Either approach represents significant expense compared to other sorbent types like solid amines.

3.4 Tentative Conclusions and Recommendations:

Solid Amines are the best fit for the immediate future. They offer the necessary resilience against humidity and oxidation required for a distributed consumer product. However, the long-term viability of the business model likely depends on the maturation of MOFs, which promise the increased gravimetric densities necessary to solve the logistics equation.

Table 2: Comparative Sorbent Matrix

| Feature | Solid Amines | MOFs | Moisture Swing | Zeolites (13X) |
|-----------------------------|----------------------------|-----------------------|---------------------------------|---------------------------|
| Mechanism | Chemisorption (Co-valent) | Physisorption | Chemisorption / Ion Exch. | Physisorption |
| Capacity (400ppm) | High (1.5 - 2.5 mmol/g) | Very High (3+ mmol/g) | Moderate (0.8 - 1.5 mmol/g) | Negligible (in humid air) |
| Regeneration Trigger | Heat (Temp Swing) | Heat or Vacuum | Moisture (Humidity Swing) | Heat (High Temp) |
| Regen Temp | 80°C – 100°C | 60°C – 150°C | Ambient (Requires Water) | > 150°C |
| Humidity Effect | Positive | Negative | Negative Capture / Regen Driver | Fatal |
| Reusability | Moderate | Low/Moderate | High | Very High |
| Est. Cost | Moderate (\$50 - \$100/kg) | Very High (\$500+/kg) | Moderate (\$50 - \$150/kg) | Low (\$2 - \$10/kg) |

Research should focus not just on chemical capacity, but on volumetric density. How much amine can be packed into a cartridge without creating a pressure drop that requires loud fans? One promising direction is to use structured monoliths (honeycombs) rather than the standard packed beds.

4 Sorbent Distribution Logistics

4.1 Analysis of Carbon Neutrality

To evaluate the viability of a distributed Direct Air Capture (DAC) network, we constructed a simplified transportation model that compares the carbon emissions of moving sorbent materials against the carbon captured by those materials.

4.1.1 Sorbent and Cartridge Constraints

Based on our material analysis above, we assume a nominal sorbent capacity (Q_e) of 2.5 mmol/g given previously published findings. We would note that given the higher concentrations of CO₂ in indoor settings, it is possible that this sorbent capacity might be higher in practice. To maximize the “carbon return” per trip, the cartridge is designed to hold the maximum amount of active sorbent manageable by a single person in a residential setting. Based on similarly sized consumer products, such as dry dog food or water softener salt, we anticipate homeowners can manage weights in the range of 10-20kg. We thus model a cartridge with 9 kg of active sorbent and a 1 kg housing structure. This yields an unloaded unit weight of 10 kg (approx. 22 lbs), which remains ergonomically viable for last-mile logistics even when fully saturated (\approx 11 kg). In this model, we anticipate a “worst” case delivery scenario where the saturated filter is returned to a central processing facility, whereas in-home regeneration is more amenable to delivery logistics and warrants a different emissions model (residential energy mix).

4.1.2 Vehicle Emissions and Dynamics

We define the “carbon cost” of recovery as mainly a function of vehicle fuel economy over distance. There are two additional factors that will diminish fuel economy in practice: payload weight and idling time. We approximate both in our model here by using conservative fuel economy ratings, decreasing published numbers 5%.

For fuel economy, the model considers two standard logistics vehicles:

- Internal Combustion (ICE): A standard step van (e.g., Freightliner MT45) utilizing diesel fuel.
- Electric Vehicle (EV): A modern delivery van (e.g., Rivian EDV 700) utilizing grid electricity.

We find that burning diesel fuel emits 10.19kg of CO₂ per gallon¹. Fuel economy for diesel vans in delivery settings has been reported at 10.2mpg, based on a US DOE report[33]. With a 5% inefficiency, we use 9.7mpg as the diesel truck fuel economy.

¹https://www.eia.gov/environment/emissions/co2_vol_mass.php

We base our electric vehicle on the Rivian EDV 700, popularized by Amazon. The current standard production Rivian EDV 700 uses a 100 kWh Lithium Iron Phosphate (LFP) battery pack², with an EPA estimated range of 153 miles ($1.53mi/kWh$). With a similar inefficiency tax of 5%, we use $1.45mi/kWh$ as the electric van fuel economy. The emissions due to charging are based on the US average grid intensity ($0.386kgCO_2/kWh$)³. Note that this variable approaches zero for fleets powered by on-site solar, representing a significant future efficiency upside.

We can then relate the carbon footprint between these two vehicles in terms of kilograms of CO_2 emitted per mile.

4.1.3 Operational Efficiency

A core assumption in our model is that we are operating with a “milkman” scheme where human drivers visit participating homes and drop off or retrieve cartridges that are already placed outdoors.

There are several variables that constrain the number of cartridges that can be reclaimed by a single vehicle-operator in a given 8-hour shift:

- The density of stops on a route
- The total amount of weight a driver can lift in a shift
- The number of cartridges the truck can carry
- The saturation capacity of the sorbent itself

We find that in dense urban areas, delivery drivers are able to make 20-30 stops an hour [34]. For our purposes here, we linearly scale this value as a rough estimate (24, 16, and 8 stops in the urban, suburban, and rural conditions respectively). As we are moving heavy items, we must also mind the amount of total manual labor performed during the shift. By applying the guidelines provided by NIOSH, we anticipate a driver can safely manage a maximum of 140 cartridges in a given shift[35]. We keep with a single driver for now, acknowledging that a second operator in vehicle would double the personnel costs. The diesel truck has a max payload of 4500kg (400 saturated cartridges), while the electric van has a max payload of just over 1000kg (93 saturated cartridges) [37, 38].

The resulting *Efficiency Ratio* (η_{sys}) compares the mass of CO_2 successfully recovered to the mass of CO_2 emitted by the logistics network during the recovery process.

4.1.4 Model Calculations

Hypothetical parameters of the distribution model are shown in Table 3. The main variables of the model are the fuel type of the vehicle (Diesel Truck vs Electric Van), and the estimated mileage of the trip in different settings.

Table 3: Comparative Efficiency Analysis: Driver & Vehicle Constraints

| Variable | Description | Diesel (Freightliner MT45) | | | EV (Rivian EDV 700) | | |
|------------------------------------|-------------------------------------|----------------------------|-------------|-------------|---------------------|----------------|-------------|
| | | Urban | Suburb | Rural | Urban | Suburb | Rural |
| Q_e | Sorbent Capacity (mmol/g) | 2.50 | 2.50 | 2.50 | 2.50 | 2.50 | 2.50 |
| W_{cart} | Saturated Cartridge Weight (kg) | 10.99 | 10.99 | 10.99 | 10.99 | 10.99 | 10.99 |
| m_{CO_2} | Mass CO_2 per Cartridge (kg) | 0.99 | 0.99 | 0.99 | 0.99 | 0.99 | 0.99 |
| <i>Logistics & Constraints</i> | | | | | | | |
| R_{emit} | Emission Rate (kg CO_2 /mi) | 1.05 | 1.05 | 1.05 | 0.27 | 0.27 | 0.27 |
| D_{trip} | Trip Distance (miles) | 25 | 50 | 100 | 25 | 50 | 100 |
| S_{hr} | Stops per Hour (Rate) | 24 | 16 | 8 | 24 | 16 | 8 |
| N_{total} | Total Stops / Shift (Actual) | 140 | 128 | 64 | 93 | 93 | 64 |
| | <i>Limiting Factor:</i> | <i>Driver</i> | <i>Time</i> | <i>Time</i> | <i>Payload</i> | <i>Payload</i> | <i>Time</i> |
| <i>Net Carbon Impact</i> | | | | | | | |
| M_{emit} | Total CO_2 Emitted (kg) | 26.3 | 52.5 | 105.1 | 6.7 | 13.3 | 26.6 |
| M_{rec} | Total CO_2 Reclaimed (kg) | 138.6 | 126.7 | 63.4 | 92.1 | 92.1 | 63.4 |
| η_{sys} | Efficiency Ratio | 5.28 | 2.41 | 0.60 | 13.84 | 6.92 | 2.38 |

²https://www.greencarreports.com/news/1145719_rivian-opens-electric-van-sales-to-all-fleets

³<https://news.mit.edu/2024/cutting-carbon-emissions-us-power-grid-0311>

4.1.5 Results

The results of the simple model sweep indicates that this distribution framework is *net carbon negative* under most modeled conditions ($\eta_{sys} > 1$). Again, note that this models distribution logistics only, leaving the carbon impact of regeneration for the following section, and the carbon impact of filter manufacturing to future work. Somewhat surprisingly, diesel-powered logistics scenarios are carbon-negative in sufficiently dense geographies, while a fleet of electric vans are carbon negative in all scenarios. As fleets transition to solar-charged EVs, the emission penalty approaches zero, transforming the logistics leg from a “necessary cost” into a minor factor in the system’s total lifecycle analysis.

Note also that this model remains slightly idealized. The cartridges themselves may be less than fully saturated, and delays at pickup are likely to diminish the driver’s stops per hour. We are also making assumptions that moving heavy objects like these can be safely handled for an 8-hour shift, and that lower limits are not required. Finally, this also assumes that a reclamation run can be completed to capacity without “no-shows” (planned stops with no cartridge to pick up).

4.2 Analysis of Carbon Dioxide Yield

In order to understand the potential impact of this model in helping alleviate the climate crisis, we estimate the amount of CO₂ present in residential environments, and compare this with the theoretical upper bound of CO₂ that may be captured under this model.

As a point of comparison, we note that the annual new emissions of the US Civilian Passenger Fleet (passenger cars, SUVs, and light-duty trucks), approach 1,000 Million Metric Tonnes (MMT) of CO₂ per year. In our view, an impactful carbon capture scheme would come close to matching, if not exceed, major sources of CO₂ emissions.

4.2.1 Addressable In-Home Carbon Dioxide

To evaluate the feasibility of residential direct air capture, we estimate the total mass of CO₂ available for removal passing through the ventilation systems of U.S. households annually. Unlike industrial point-source capture, residential systems cannot strip air to zero concentration. Instead, we define the “addressable” fraction as the mass of CO₂ exceeding pre-industrial atmospheric levels (above 280ppm).

The addressable mass flux (\dot{m}_{avail}) leaving a single residence per hour is calculated as the product of airflow and the concentration differential:

$$\dot{m}_{avail} = V_{home} \cdot \lambda \cdot (C_{indoor} - C_{base}) \cdot \rho_{CO_2} \quad (1)$$

Where:

- V_{home} is the average volume of a U.S. residence (412 m^3), derived from EIA floor area data [23].
- λ is the air exchange rate estimated at 0.5 h^{-1} [25].
- C_{indoor} is the steady-state indoor concentration, assumed at 1,000 ppm (0.001) based on metabolic loading [24].
- C_{base} is the pre-industrial atmospheric concentration floor, set at 280 ppm (0.00028). We assume removal below this limit is not the primary objective of a climate-focused retrofit.
- ρ_{CO_2} is the density of CO₂ at 20°C (1.84 kg/m^3) [26].

Substituting these values yields the hourly addressable mass flux per household:

$$\dot{m}_{avail} = 412 \cdot 0.5 \cdot (0.001 - 0.00028) \cdot 1.84 \approx 0.273 \text{ kg/h} \quad (2)$$

Extrapolating this flux over one year (8,760 hours) for the total count of U.S. households (132.2 million) [22], we estimate the total addressable residential CO₂ potential in Table 4.

Table 4: Estimated Annual Addressable CO₂ Flux

| Parameter | Value | Notes |
|------------------------------------|---------------------|-------------------------|
| Avg. Home Volume | 412 m ³ | EIA RECS [23] |
| Ventilation Rate | 0.5 h ⁻¹ | EPA Factors [25] |
| Indoor Concentration | 1,000 ppm | Metabolic Load |
| Capture Floor (C_{base}) | 280 ppm | Pre-industrial Baseline |
| Addressable Delta | 720 ppm | $C_{indoor} - C_{base}$ |
| Hourly Flux (Per Home) | 0.273 kg/h | Calculated |
| Annual Potential (Per Home) | 2.4 tonnes | Calculated |
| Total U.S. Addressable Flux | ≈ 316 MMT | Calculated |

4.2.2 Theoretical Maximum Yield

Having established the total mass of CO₂ flowing through the residential housing stock, we next calculate the maximum possible capture yield. This scenario assumes a “perfect” adoption rate where every compatible household maximizes its capture potential using existing HVAC infrastructure.

We define the Service Addressable Market (SAM) as the subset of U.S. households equipped with central forced-air systems necessary for filter integration. According to EIA RECS data, approximately 75% of U.S. homes utilize central air conditioning or central warm-air furnaces with ductwork [27].

The theoretical yield (Y_{max}) is calculated as:

$$Y_{max} = N_{hh} \cdot R_{sam} \cdot F_{rate} \cdot M_{cap} \quad (3)$$

Where:

- N_{hh} is the total households (132.2 million).
- R_{sam} is the addressable market rate (75%), resulting in ≈ 99 million homes.
- F_{rate} is the filter replacement cadence (High-intensity cycling of 50–75 filters per year).
- M_{cap} is the mass yield per filter (1kg CO₂) based on our weight-limited filter size of 10kg unsaturated.

Applying these parameters provides a range of annual yield per home and total national yield:

$$Y_{home} = 50 \text{ to } 75 \text{ filters} \times 1\text{kg} \approx 50 \text{ to } 75 \text{ kg/yr} \quad (4)$$

$$Y_{total} = 99 \times 10^6 \times Y_{home} \approx 4.95 \text{ to } 7.4 \text{ MMT/yr} \quad (5)$$

Under these idealized conditions, the U.S. residential sector would capture between 4.95 and 7.4 Million Metric Tonnes (MMT) of CO₂ annually.

4.2.3 Discussion

While our estimates show the potential to capture a massive volume of gas ($\approx 5 - 7 \text{ MMT}$), it represents only **1.6% to 2.4%** of the total estimated carbon dioxide fluxing through residential settings (316 MMT). While the ventilation volume is vast, the capture system is rate-limited by filter saturation capacity and our assumptions about homeowners’ willingness to service these filters. This idealized maximum yield is equivalent to less than 1% of annual U.S. civilian passenger vehicle emissions. As such, residential distributed HVAC-based carbon capture cannot serve as a primary decarbonization strategy in the proposed form, as the emissions from personal vehicles are two orders of magnitude larger.

However, a critical finding of this analysis is that the limiting factor for residential DAC is not the availability of CO₂ in-home nor the sorbent technology itself. The limit emerges from the logistical tradeoff between sorbent capacity, centralized regeneration, and core assumptions about an acceptable maintenance burden on the homeowner.

A larger in-home filter would be able to capture more CO₂ without increasing the maintenance burden (frequency) of filter changes, but make the cartridge difficult to install and exchange. At the current size (or smaller), one home would need many filters, exchanged multiple times a week, or stored on-site until bulk collection is possible. Neither of these alterations seem particularly feasible, and so some other

upstream assumption or constraint would need to change in order for this capture scheme to realize its full potential.

We see two possible avenues for unlocking higher CO₂ yield. A modest and straightforward approach is the continued advance of sorbent capacity by weight. Continued research and development of class IV solid amines sorbents, MOFs, or the eventual discovery of others classes and methods could hold more CO₂ per unit mass.

However, on some level, the sorbent or other capture substrate will always represent a dead-weight tax on logistics. We argue, the sustainable long-term path is probably in-home regeneration capable of “charging” concentrated cannisters that can have small modular footprints, like a SodaStream or whipped cream charger.

There are many advantages to this approach in a distributed residential setting. The filter, once installed, does not need to move until it reaches the end of its service life, which relaxes the limitations on its size and complexity. Concentrated CO₂, or perhaps even pure carbon, is lighter and smaller when decoupled from the filter assembly, which eases the burden on reclamation (in terms of both weight and cubic volume) *and* the homeowner. A filter could potentially be made to be self-servicing, and could regenerate several cartridges in-place before requiring human intervention.

Combined, these changes would dramatically increase the amount of carbon captured per homeowner maintenance event. The primary challenge, of course, would be the introduction of a potentially high-energy, high-heat process into residential settings. We leave a deeper discussion of regeneration to the following section.

5 Regeneration

Regeneration is the process to release CO₂ from an adsorption medium (i.e. the saturated sorbent) into a concentrated gas stream. This is not a thermodynamically favorable reaction, but rather requires energy input (generally thermal or electrical) to reverse the original adsorption process.

We examined two potential cases for regenerating the captured CO₂ from the in-home system:

1. Regenerating the saturated filters in the home:

Requires additional hardware installation in the home system to apply the necessary heat and electricity for the regeneration process, as well as process equipment for purifying the CO₂ stream and compressing it into on-site storage. The process would also feed off the homeowner’s electricity supply.

2. Transporting the saturated filters to a centralized regeneration facility:

Requires a dedicated transportation and logistics network, as well CAPEX to build the facility, and OPEX to run the process at industrial scale. Depending on location, there is a potential opportunity to reduce the energy input requirement by co-locating the facility with a source of waste heat such as from a data center, nuclear or geothermal plant, or another high temperature industrial process such as steel milling.

Separately, we considered the possibility of not performing regeneration at all, but rather allowing the CO₂ to be converted to limestone (CaCO₃). While a calcium-based sorbent was not selected for our analysis, the commodity market and potential profit of a non-regenerated limestone product is examined in the upcoming *Economics* section.

5.1 Landscape of Regeneration Techniques

Methods for regenerating CO₂ from sorbents that have reached maturity include:

- **Thermal-Vacuum-Swing Adsorption (TVSA):** Involves heating the saturated sorbent at minimum 80–100°C to release physisorbed and chemisorbed CO₂. Vacuum is added to enhance the purity of the offgassed stream. Has reached pilot and commercial scale, for example with the company Climeworks. [28]
- **Calcination:** Involves decomposition under high temperatures (up to 950°C) of solid calcium carbonate (CaCO₃) into CaO and CO₂. Has reached pilot and commercial scale, for example with the companies Carbon Engineering, 1PointFive, and Heirloom.

- **Pressure/Vacuum Swing (PSA/VP SA):** CO₂ is absorbed under high pressure by the sorbent. For regeneration, the pressure is reduced to atmospheric level (or below) with vacuum often being used to release the CO₂ in a highly pure stream.
- **Electrochemical (ECC) / Bipolar Membrane Electrodialysis (BPMED):** A liquid solvent would typically absorb CO₂ at a high pH as a basic carbonate compound. The solution is passed through an electrochemical cell whereupon a redox reaction occurs, oxidizing the H₂O at the anode, and releasing hydrogen ions which lower the pH of the solution and react with the dissolved carbonates to release CO₂ gas. This has reached pilot scale with the company Verdox pursuing this approach.
- **Moisture Swing (MSA):** Uses a resin-based sorbent that absorbs CO₂ in dry conditions, and displaces the CO₂ in a highly humid environment, often a concentrated spray of water vapor. The company Avnos is bringing this technology into the commercial phase.

5.2 Analysis of available regeneration techniques

For our use-case of low pressure drop in-home HVAC system filters capturing CO₂, a solid sorbent such as an amine composite material would typically be regenerated using the thermal-swing adsorption method. Breaking the chemical bonds associated with the chemisorbed CO₂ within the amine group requires heat to reach an activation temperature upon which the original chemical reaction is reversed, releasing CO₂ into a pure stream.

TVSA is already proven at scale and does not require additional expensive purge gases such as nitrogen. With our selected sorbent medium, TVSA can also be performed at relatively low temperatures of 80–100°C [28] which opens the possibility of performing TVSA at a central plant or in-home.

Due to the humid adsorption environment inside of home HVAC systems, we expect the MSA process would not work in that environment.

Likewise, while the inside of the HVAC ducting may be slightly above atmospheric pressure conditions due to the presence of the HVAC blower fan, this pressure gradient is not nearly sufficient for PSA so the adsorption step would require significant additional energy input and equipment. Additionally, filters would then be exposed to ambient conditions during the swapping process and thus would likely spontaneously offgas CO₂ before the intended regeneration time and location.

Calcination could be a useful approach for concentrating CO₂ only if the output of the in-home capture system were CaCO₃. That process requires very high temperatures making it highly energy intensive as well as likely infeasible in-home.

An electrochemical separation process would work in theory, however the liquid solvent for capturing CO₂ would not be ideal for the residential DAC use case due to the high air flow requirements on the adsorption side, and the challenges involved with enabling a continuous flow of a caustic liquid solvent such as KOH in a home environment. For these reasons and for those outlined in Section 3, solid sorbents such as an amine group that can be regenerated using a TVSA process were chosen.

5.3 Exploration of costs of processes for selected sorbents

There is a direct relationship between the financial cost to regenerate a sorbent and the energy input required. To analyze the net carbon negativity of the regeneration process, the metric of regeneration efficiency in kilowatt hours (kWh) per metric ton (mTonne) is examined.

There are several distinct energy costs involved in a TVSA regeneration process. First, there is the active thermal energy component, directly linked to releasing the stored CO₂. The electrical energy required to run the equipment associated with the process (including motors in pumps, compressors, and fans) generate additional costs. In the case of regeneration performed in a central facility, one must also account for the operational energy consumption for the entire facility (lighting, HVAC, IT, etc.).

While the electrical energy requirement to power the *adsorption* process has been widely documented by various organizations, our in-home DAC system would theoretically have a 0 kWh/mTonne contribution due to the utilization of an already-present HVAC blower fan. On the other hand, the available literature on electrical energy requirements for regeneration is thin, with values heavily dependent on the scale of regeneration facility (a large central facility has the best efficiency). Regardless, *thermal* energy dominates the costs in our application. Therefore, this analysis focuses on thermal energy costs alone.

According to published analyses, thermal energy consumption for chemisorbent based systems have been evaluated between 1170 and 2000 kWh/mTonne[29]. With grid electricity rates in the US in late

2025 ranging between \$0.07 and \$0.42 per kWh depending on location, time of use, and residential vs commercial rates[30], we can calculate a best-case regeneration cost of **\$81.9/mTonne**. In the case of our in-home filter with 9 kg of active sorbent material and a Q_e of 2.5 mmol/g, which yields approximately 1 kg of CO₂, this amounts to **1.2 kWh and \$0.084-0.50 per filter regeneration cycle**. In the following *Markets* section, we will compare this to the value of the regenerated CO₂ depending on various commodity markets.

5.4 Discussion

Regeneration is energy-intensive due to the thermodynamic requirements for releasing the stored CO₂ back into a gas from the filter. In addition, the logistics of regenerating the saturated filters is non-trivial, requiring either additional hardware and energy input to perform recovery in the home and store pressurized CO₂ on-site, or a logistics network to implement transportation of saturated filters to a centralized regeneration facility.

In the case of in-home regeneration, the additional energy burden on the homeowner, onsite storage of CO₂ requirement, high heat and potentially caustic chemicals present serious challenges. Meanwhile, a centralized regeneration facility poses a significant CAPEX burden that threatens to undermine the original intent of distributing the DAC process. Furthermore, the costs to operate the saturated filter transportation network would be a significant additional contribution to the total overhead. For these reasons, the regeneration process poses significant challenges to the viability of our proposed approach.

6 Economics

6.1 Revenue and Markets

The business case for pursuing a decentralized carbon capture network relies on the value of captured CO₂. We primarily investigated the revenue potential of selling purified CO₂ as a commodity (i.e. food and beverage grade) at a bulk wholesale price in \$/ton. Alternatively, we considered the possibility of performing permanent sequestration of the captured CO₂ and relying on the tax credit market within the US for revenue. Lastly, in the case where regeneration was not performed, we considered the possibility of selling non-regenerated limestone.

The following table illustrates the potential revenue in dollars per metric ton for each source.

Table 5: Comparative Product Value Matrix

| Product | \$/metric ton | Requirement(s) |
|---|-------------------|--|
| Food and Beverage Grade CO ₂ | \$600-\$1000 [31] | $\geq 99.9\%$ of purity CO ₂ , limits on impurities set by ISBT |
| CaCO ₃ | \$40-\$800 [32] | High purity for pharmaceutical/food grade |
| Geologic Sequestration | \$180 | Above 1000 tons yearly of permanent geologic sequestration at an EPA class IV well per facility, entered in to construction prior to 2033 (USA 45Q Tax Credit) |

In this analysis we find that selling food and beverage grade CO₂ to be the most valuable. Carbon capture companies, such as Remora Carbon, have begun to emerge selling captured CO₂ on this market, as a form of an early beachhead to bootstrap their business.

Using the assumptions from the preceding sections, a single saturated filter produces 1 kg CO₂ that yields \$0.60 – 1 in gross value based on the commodity pricing for food and beverage grade CO₂[31]. We assume that homeowners might be willing to participate in a filter swap between once per month and once per week. Given the commodity value, this would yield a maximum gross revenue of:

- at a frequency of once per month: \leq \$1 per month
- at a frequency of once per two weeks: \leq \$2.17 per month
- at a frequency of once per week: \leq \$5.20 per month

Even if the homeowner collected the full revenue each month (with no revenue used to cover costs or generate profit), it is hard to imagine this amount would suffice to incentivize a homeowner to sign up, let alone to lug an 11kg filter to the street and back each cycle.

6.2 Costs

A careful analysis of costs is *not* the focus of this paper. Still, a coarse model of factors contributing to costs would look something like this:

Capital Expenses (CAPEX)

- Construction of a regeneration facility
- Purchase of vehicles for distribution fleet

Operational Expenses (OPEX)

- HVAC refit per customer (materials and labor) amortized over total number of cartridges in system lifetime
- New cartridge cost amortized over cartridge cycle life
- Logistics cost per cartridge replacement
- Regeneration energy cost per cartridge cycle (\$0.10 as calculated in Section 5)
- Additional purification of the regenerated CO₂. Would most likely be required for food and beverage grade CO₂.

Unfortunately, we needn't examine these costs deeply to determine that the costs are not borne by the minimal unit revenue calculated above. A very brief analysis of the logistics cost per replacement trip alone guarantees unprofitability in the U.S. market:

- Driver salary likely dominates logistics costs.
- The logistics model in Section 4 assumes a driver makes between 8 and 24 stops per hour
- Assume a driver is paid \$20 per hour (it is likely higher), then each delivery/swap costs between \$0.83 and \$2.50.

So the delivery driver cost alone costs 1–2x the total potential revenue of the CO₂ captured by a cartridge. It is therefore clear that the proposed business model operates at a loss.

In the face of the unfavorable economic potential of this venture, we considered a few other potential alternatives to the existing business model:

- H₂O : in the case of amine based sorbents, H₂O would also be captured alongside the CO₂ in a ratio depending on the selectivity of the sorbent material, and could thus be regenerated and potentially sold as a commodity along with the CO₂. In applications such as data centers, industrial grade cooling water would potentially be a very attractive secondary market for our application, specifically in the case of the centralized regeneration facility. While the pricing, markets, and logistics for capturing and distributing H₂O were not a focus of this study, we recommend examining this further in future analyses on direct air capture
- Shifting away from a commodity market and paying the user to charging the user for a service, *i.e.* in-home air purifier with CO₂ capture as a co-benefit. This would be in line with the product Atalanta Climate has already released, and therefore would have first mover advantage.

7 Conclusions

This feasibility study aimed to investigate a provocative hypothesis: that the existing HVAC infrastructure found in 75% of American homes could be deputized as a decentralized, gig-scale Direct Air Capture (DAC) network. Our research decomposed this model into three distinct vectors of feasibility: the thermodynamic reality of sorbent behavior in residential environments, the net-carbon impact of a distributed logistics network, and the economic viability of a “gig economy” payout model for homeowners.

The synthesis of these models leads us to a nuanced conclusion. While the physics of residential capture are sound and the logistics are surprisingly carbon-negative, the economic engine required to drive a manual-swap network is currently broken. The following sections detail these findings and propose a strategic pivot for the technology to remain viable.

7.1 Summary of Findings

7.1.1 Carbon Negativity

Perhaps the most counter-intuitive finding of this study is that the "last mile" distribution network appears to be net carbon negative. We initially hypothesized that the emissions generated by diesel delivery vehicles would negate the relatively small mass of CO₂ captured per trip. However, our models indicate that even with conventional fossil-fuel logistics, the system returns a positive carbon yield. We also note that the energy intensity of regeneration, at least when performed in a centralized facility, is likely manageable in this scheme, especially if the facility can be co-located with renewable energy sources or industrial waste heat to minimize emissions.

However, this conclusion carries a significant caveat: our model did not account for the lifecycle emissions associated with filter manufacturing or global supply chain logistics. While the *operation* of the network is negative, the *production* of millions of disposable or semi-disposable sorbent cartridges represents a large unknown variable. If these complex chemical units are manufactured outside of the U.S. and require trans-oceanic shipping, the margins of net-negativity we observed in the logistics phase could easily be erased.

7.1.2 Headwinds for a “Gig Economy” Model

It is a central economic premise of this project that homeowners could be incentivized to participate in a decentralized carbon capture scheme by earning passive income. Putting the data together, there is not enough revenue generated to motivate homeowners on commodity proceeds alone. With food and beverage grade CO₂ trading at a maximum of \$1000/ton, the maximum theoretical revenue for a household is approximately \$5-7 per month. Even under the most optimistic scenarios, a homeowner would earn less than \$100 annually.

This creates a critical gap in the business model. To induce behavioral change and consistent participation, we estimate that household incentives would need to approach \$1,000 annually. Currently, the operational expense (OpEx) of the logistics network exceeds the value of the carbon recovered, making the unit economics more unfavorable. This structural deficit makes it difficult to subsidize the network upfront with Venture Capital funding. The key takeaway is that there is simply insufficient market demand for the molecule itself to support an “AirBnB for Carbon” narrative.

7.1.3 Total Climate Impact vs. Human Constraints

Finally, we must address the total climate impact. In its current “manual swap” configuration, the theoretical ceiling of this scheme is roughly 7MMT annually, a tiny fraction compared to the emissions of the U.S. passenger vehicle sector alone (1000MMT).

It is crucial to note, however, that this ceiling is defined by human factors, not physics. The total volume of CO₂ fluxing through American homes is massive (estimated at 316 MMT). The limiting factor is the “homeowner labor cap”, in that it is impractical to expect homeowners to swap filters daily. The opportunity for in-home capture remains enormous; if the bottleneck of manual servicing can be removed, a variation of this infrastructure could contribute meaningfully to bending the global emissions curve backwards.

7.2 Strategic Directions and Future Work

For this technology to bridge the gap between a theoretical curiosity and a scalable climate solution, we recommend three focus areas for future R&D.

7.2.1 Demand-Side R&D: Creating Valuable Utilization

The economic failure of the distributed model is a function of the low market value of captured carbon. If the market for the output product expands, the entire logistics chain becomes viable. We see two distinct avenues for this work:

- **Useful Sequestration (Green Concrete):** Research should prioritize the integration of residential carbon into “green concrete” and aggregates, or other products that permanently sequester carbon while producing a necessary market good. We argue that this dual-value is essential; the industry cannot rely on altruism or charity to pay for the burial of carbon that has no captured monetary value.
- **High-Value “Bridge” Fuels:** Converting captured CO₂ into synthetic fuels *e.g.* Methanol or E-Kerosene, could command prices exceeding \$1,000/tonne. We acknowledge the inherent contradiction here: the eventual combustion of these fuels releases the carbon back into the atmosphere, undermining the sequestration goal. This transforms DAC from a carbon removal strategy to an emissions reduction strategy by creating a net-zero-emissions synthetic fuel. These high-margin products could serve as a necessary beachhead, providing the revenue required to fund the network’s early growth before pivoting to permanent sequestration methods.

7.2.2 Supply-Side R&D: In-Home Regeneration

Moving the regeneration process from a centralized plant to a distributed in-home process would solve the logistics bottleneck.

Such a model poses significant engineering challenges, as the filter unit would become more complex, heavier, and require active heating elements. However, this challenge may mask an opportunity for synergy. Future research should investigate utilizing the resistive heat required for sorbent regeneration to supplement the home’s HVAC heating load. If a device can capture and regenerate carbon automatically – timing its cycles to align with excess solar availability or low grid demand – a single home could capture roughly 10x the volume of the current model without any additional labor from the homeowner.

7.2.3 Business Model Pivot: Premium Health Product

Absent the R&D advancements theorized above, the currently-modeled system could be productized as a premium consumer health appliance.

By marketing the device as a best-in-class air purifier that removes VOCs, allergens, and CO₂ for the health of the occupants, the revenue model shifts from commodity sales to consumer hardware. In this scenario, the homeowner funds the deployment of the hardware for personal wellness, allowing the carbon capture network to scale as a secondary, cumulative asset class. While this strategy inevitably reduces the Total Addressable Market (TAM) by pricing out lower-income households, it could serve as a beachhead to prove the technology and build the distributed infrastructure required for gigaton-scale capture.

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