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# Implementation and Performance Analyses of a Highly Efficient Algorithm for Pressure-Velocity Coupling

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## Abstract

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One crucial decision in designing algorithms to numerically solve the incompressible Navier-Stokes equations is how to treat the inherent coupling between the dependent variables velocity and pressure. Due to advances regarding processor and memory hardware technology in the past decades, fully-coupled solution algorithms, which denominate algorithms that simultaneously solve a system of partial differential equations for all involved variables, have become attractive in the field of CFD (*Computational Fluid Dynamics*). The objective of the present thesis is to implement and analyse a pressure based fully-coupled solution algorithm based on a finite-volume discretization of the Navier-Stokes equations including additional coupling to the temperature equation. The method uses a cell-centered co-located variable arrangement and is able to handle non-orthogonal, three-dimensional, locally refined block structured grids with hanging nodes. The implementation has been parallelized using the PETSc framework. After the verification using a manufactured solution, the single processor and parallel performance of the implementation are analysed on a parallel benchmark, a benchmark involving a duct flow with complex geometry and the heated cavity benchmark for buoyancy driven flows. The performance analysis always consists of a comparison involving an implementation of a segregated solution algorithm that was developed using the same environment. In all tests the fully coupled algorithm did outperform the segregated algorithm, provided that the number of involved unknowns was high enough. The solution of the involved linear systems was carried out using black-box solvers from the PETSc framework. It is assumed that major improvements regarding the parallel scalability of the implemented algorithm can be achieved through the use of a special algebraic multigrid method as preconditioner.

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## 1 Introduction

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The growing involvement of numerical methods in sciences and industrial practice due to the advancements in computer architecture and algorithms has had a great impact on academic research and industrial development processes in the past decades. Numerical methods nowadays form an integral part in forming a better understanding of physical phenomena and modelling the behaviour of technical systems besides purely theoretical or experimental approaches. Especially numerical methods for the simulation of fluid flow, also known as *CFD* (*Computational Fluid Dynamics*), have continuously been creating new challenges for the ongoing process of hardware and software improvements. Not only more complexity has to be reflected in computational methods to solve fluid flow problems but also less time to generate results is preferable to accelerate development processes. Parallel computing on high performance computer clusters represents an additional field of study since many numerical methods rely on hardware requirements that cannot be met by office workstations. As are the fields of study, the possibilities to further increase performance of scientific applications are manifold. Advancements in numerical methods and mathematical models, programming paradigms and tailored libraries for new computer architectures that use the hardware to full capacity and the new hardware itself contribute to the continuous expansion of the boundaries of what is *computable*.

The incompressible Navier-Stokes equations represent the commonly used mathematical model for incompressible flows. Among other properties this model incorporates a coupling between the involved variables velocity and pressure. Algorithms that tend to solve for incompressible flow fields thus have to address the so called pressure-velocity coupling. A common approach is to resolve this coupling through segregated solution methods. With this methods the algebraic equations for each of the dependent variables are solved sequentially using approximate values for the other involved variables. Achieving inter variable coupling is part of an iterative solution process such that in the end the solution field will fulfill all involved equations. One common representative of this type of algorithms is the SIMPLE algorithm that has been widely used in scientific codes or industrial solvers due to its small memory requirements. Reference [2] reviews the evolution of this type of algorithms.

The use of segregated solution algorithms comes with significant drawbacks. To stabilize the iteration for the coupling process, the obtained solutions have to be under relaxed, where the amount of under relaxation is furthermore dependent on the problem to be solved. Not only does this degrade the solver performance, but also there don't exist strict rules for the optimal choosing of the under relaxation. The resolution of the pressure-velocity coupling forms an essential part for the performance of a flow solver and hence creates the need for new coupling algorithms that are more robust or even independent of parameters and at the same time resource efficient in their application. An analysis of the pressure-velocity coupling can be found in [63].

One alternative approach to pressure-velocity coupling is by means of the simultaneous solution of the momentum and mass balance equations. Algorithms of this type, that perform on co-located grids have been used in [13, 20, 27, 29, 46, 52, 77]. It was shown that the principal advantages of coupled solution approaches complement the drawbacks of segregated solution algorithms. Not only the computational time was reduced, also the robustness of the solution algorithm was increased. According to [20] no under relaxation was necessary to obtain a robust implementation.

So far only [29, 77] additionally coupled a temperature equation to the two-dimensional Navier-Stokes equations and investigated the impact of different methods to achieve implicit temperature-to-velocity/pressure coupling on the solver performance. The objectives of the present thesis are to implement a fully coupled solution algorithm for the three-dimensional Navier-Stokes equations and the temperature equation and analyse their single and multi-processor performance.

The thesis begins by introducing the mathematical and physical fundamentals of flow problems. In this first chapter the main frame of partial differential equations to be solved numerically is introduced. Each subsection presents a brief derivation from the continuum mechanical point of view and shows common or necessary simplifications. This embraces not only a presentation of the Navier-Stokes equations for incompressible fluids but also the Boussinesq approximation that is widely used for incompressible flows that experience buoyant forces.

Section number three outlines the fundamentals of finite-volume methods in general. At first the necessary terminology for numerical grids is established. Then the main approximation principles for the discretization of integral or differential operators are introduced. Since in the present work no further requirements are demanded other than grid structure, one subsection gives an overview over common methods to handle non-orthogonal grids. The chapter concludes by presenting the main method of linearization for the Navier-Stokes equations used throughout the work.

The fourth section focusses on segregated solution methods as many ideas of the commonly used SIMPLE algorithm are relevant for the implementation of coupled solution methods. The section starts by discretizing the mass balance coming directly from the continuum mechanical introduction of the first section, outlining its drawbacks on their applicability to co-located variable arrangements. The following sections then first introduce a remedy to the *checker-boarding* effect that would surge from an unmodified discretization of the mass balance by introducing a modification of the commonly used Rhie-Chow [66] momentum interpolation scheme. This modification is proven to yield results that do not depend on under-relaxation which is important for later comparison studies with the coupled solution algorithm. Then the popular SIMPLE algorithm is derived using the previously demonstrated interpolation scheme as basis for the construction of a

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pressure correction equation. In the following subsections the pressure equation and the two remaining sets of equations, the three momentum balances and the temperature equation, are discretized. Each section concludes with a complete list of the resulting discretized equations and calculations of the coefficients as they are implemented in the developed solver framework. The next subsections are dedicated to the implementation of boundary conditions. For each boundary condition, including the treatment of block boundaries, the necessary modifications to the discretized equations are presented. Since in most of the cases the boundary conditions lead to a singular system for the pressure correction the following chapter describes methods to constrain the pressure in incompressible flows. The section concludes by presenting the non-zero structure of the resulting assembled linear system, taking into account the special treatment of block boundaries with hanging nodes.

The structure of the fifth section, which describes the implemented coupled solution algorithm, is similar to the fourth section, since both solution approaches share a great part of their components. This is why special emphasize lays on pointing out the differences between both algorithms. The first subsection of this section therefore is a revision of the pressure velocity coupling that accounts for the implicit consideration of the pressure in the momentum balances. A major difference to segregated solution methods is then presented in the subsequent section and subsections: the coupling to the temperature equation. Here, different methods, varying in their relation of implicit to explicit coupling of velocities, pressure and temperature are derived. Then the necessary modifications for boundary conditions are presented. The final subsection presents the final form of the discretized equations and the resulting structure of the assembled linear systems with special emphasize on the effects of the different methods to achieve coupling of the velocities to the temperature equation and vice versa.

In section six the developed *CAFFA* (*Computer Aided Fluid Flow Analysis*) framework is introduced for which the preceding chapters present the theoretical basis. The framework is linked to the PETSc library, a sophisticated framework for the parallelisation of solver applications as they surge in scientific computing and a set of efficient preconditioners and Krylov subspace solvers for the solution of linear systems. The following sections then introduce the other building blocks of the framework, beginning with a grid generator for arbitrarily refined block structured grids and a preprocessor program ending with implementation details of the *CAFFA* solver. These details embrace the used message passing model, the control of convergence and the data composition in the context of parallel computations.

Section seven presents the results of a conducted convergence study to verify of the *CAFFA* framework. After a brief introduction to the theory behind the verification of scientific codes via manufactured solutions is given, an own manufactured solution for the Navier-Stokes equations using the Boussinesq approximation is proposed, followed by the results of a grid convergence study to prove the order of accuracy of the developed solvers within the *CAFFA* framework. The section concludes with the results of a short study on the effect of the under-relaxation factors of the velocities on the final result of calculations.

Section eight presents the results of the performance analyses conducted on the high performance cluster *HHLR* (*Hessischer Hochleistungsrechner*) of TU Darmstadt. After introducing the used hardware and deployed software configuration and the relevant performance metrics, program runtimes are measured and application speedup is calculated. The section concludes with performance analyses regarding the efficiency of coupled and segregated solution algorithms for flow problems involving complex geometries and buoyancy forces.

The last section concludes the thesis by summarizing the core results of the conducted work and giving an outlook for further investigations.

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## 2 Fundamentals of Continuum Physics for Thermo-Hydrodynamical Problems

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This section covers the set of fundamental equations for thermo-hydrodynamical problems, which the numerical solution techniques of the following chapters are aiming to solve. Furthermore, the notation regarding the physical quantities to be used throughout this thesis is introduced. The following paragraphs are based on [4, 28, 47, 75]. For a thorough derivation of the matter to be presented the reader may consult the mentioned sources. Since the present thesis focusses on the application of finite-volume methods, the focus lays on stating the integral forms of the relevant conservation laws. However, in the process of deriving the final set of equations, the use of differential formulations of the stated laws is required. Einstein's convention for taking sums over repeated indices is used to simplify certain expressions. For the remainder of this thesis, non-moving inertial frames in a Cartesian coordinate system with the coordinates  $x_i, i = 1, \dots, 3$  are used. This approach is also known as *Eulerian approach*.

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### 2.1 Conservation of Mass – Continuity Equation

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The conservation law of mass, also known as the continuity equation, embraces the physical concept that, neglecting relativistic and nuclear reactions, mass cannot be created or destroyed. Using the notion of a mathematical control volume, which is used to denote a constant domain of integration, one can state the integral mass balance of a control volume  $V$  with control surface  $S$  with surface unit normal vector  $\mathbf{n} = (n_i)_{i=1,\dots,3}$  using Gauss' theorem as

$$\iiint_V \frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x_i} (\rho u_i) dV = \iiint_V \frac{\partial \rho}{\partial t} dV + \iint_S \rho u_i n_i dS = 0,$$

where  $\rho$  denotes the material density,  $t$  denotes the independent variable of time and  $\mathbf{u} = (u_i)_{i=1,\dots,3}$  is the velocity vector field. Since this equation remains valid for arbitrary control volumes, the equality has to hold for the integrands as well. In this sense, the differential form of the conservation law of mass can be formulated as

$$\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x_i} (\rho u_i) = 0. \quad (1)$$

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### 2.2 Conservation of Momentum – Cauchy-Equations

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The conservation law of momentum, also known as Newton's Second Law, axiomatically demands the balance of the temporal change of momentum and the sum of all attacking forces on a body. Those forces can be divided into body forces and surface forces. Let  $\mathbf{k} = (k_i)_{i=1,\dots,3}$  denote a mass specific force and  $\mathbf{t} = (t_i)_{i=1,\dots,3}$  the stress vector. A first form of the integral momentum balance in the direction of  $x_i$  can be formulated as

$$\iiint_V \frac{\partial}{\partial t} (\rho u_i) dV + \iint_S \rho u_i (u_j n_j) dS = \iiint_V \rho k_i dV + \iint_S t_i dS. \quad (2)$$

In general, the stress vector  $\mathbf{t}$  is a function not only of the location  $\mathbf{x} = (x_i)_{i=1,\dots,3}$  and of the time  $t$  but also of the surface unit normal vector  $\mathbf{n}$ . A central simplification can be introduced, namely Cauchy's stress theorem, which states that the stress vector is the image of the unit normal vector under a linear mapping  $\mathbf{T}$ . With respect to the Cartesian canonical basis  $(\mathbf{e}_i)_{i=1,\dots,3}$  the mapping  $\mathbf{T}$  is represented by the coefficient matrix  $(\tau_{ji})_{i,j=1,\dots,3}$  and Cauchy's stress theorem reads

$$\mathbf{t}(\mathbf{x}, t, \mathbf{n}) = \mathbf{T}(\mathbf{x}, t, \mathbf{n}) = (\tau_{ji} n_j)_{i=1,\dots,3}.$$

Assuming the validity of Cauchy's stress theorem, one can derive Cauchy's first law of motion, which in differential form can be formulated as

$$\frac{\partial}{\partial t} (\rho u_i) + \frac{\partial}{\partial x_j} (\rho u_i u_j) = \rho k_i + \frac{\partial \tau_{ji}}{\partial x_j} \quad (3)$$

and represents the starting point for the modelling of fluid mechanical problems. One should note, that Cauchy's first law of motion does not take any assumptions regarding material properties, which is why the set of equations (1,3) is not closed in the sense that there exists an independent equation for each of the dependent variables.

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## 2.3 Closing the System of Equations – Newtonian Fluids

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Resulting from the application of Cauchy's theorem, the stress vector  $\mathbf{t}$  can be specified once the nine components  $\tau_{ji}$  of the coefficient matrix are known. As shown in [47, 75], by formulating the conservation law of angular momentum, the coefficient matrix is symmetric,

$$\tau_{ji} = \tau_{ij}, \quad (4)$$

hence the number of unknown coefficients may be reduced to six unknown components. In a first step it is assumed that the coefficient matrix can be decomposed into fluid-static and fluid-dynamic contributions,

$$\tau_{ij} = -p\delta_{ij} + \sigma_{ij},$$

where  $p$  is the thermodynamic pressure,  $\delta_{ij}$  is the *Kronecker-Delta* and  $\sigma_{ij}$  is the so called *deviatoric stress tensor*.

In the present thesis, viscous fluids are modelled using a linear relation between the components of the deviatoric stress tensor and the symmetric part of the transpose of the Jacobian of the velocity field  $(S_{ij})_{i,j=1,\dots,3}$ ,

$$S_{ij} = \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right).$$

If one now imposes material-isotropy and the mentioned stress-symmetry (4) restriction, it can be shown [6] that the constitutive equation for the deviatoric stress tensor reads

$$\sigma_{ij} = 2\mu S_{ij} + \lambda S_{mm} \delta_{ij},$$

where  $\lambda$  and  $\mu$  denominate scalars which depend on the local thermodynamical state. Taking everything into account, (3) can be formulated as the differential conservation law of momentum for Newtonian fluids, better known as the *Navier-Stokes equations* in differential form:

$$\frac{\partial}{\partial t}(\rho u_i) + \frac{\partial}{\partial x_j}(\rho u_i u_j) = \rho k_i - \frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_j} \left( \mu \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \right) + \frac{\partial}{\partial x_i} \left( \lambda \frac{\partial u_m}{\partial x_m} \right) \quad (5)$$

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## 2.4 Conservation of Scalar Quantities

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The modelling of the transport of scalar or vector quantities by a flow field  $\mathbf{u}$ , also known as convection, is necessary if the fluid mechanical problem to be analyzed includes for example heat transfer. Other scenarios that involve the necessity to model scalar transport surge, when turbulent flows are to be modeled by two-equation models like the *k-ε-model* [64].

Since this thesis focusses on the transport of the scalar temperature  $T$ , this section introduces the conservation law of energy in differential form, formulated in terms of the temperature,

$$\frac{\partial (\rho T)}{\partial t} + \frac{\partial}{\partial x_j} \left( \rho u_j - \kappa \frac{\partial T}{\partial x_j} \right) = q_T,$$

where  $\kappa$  denotes the thermal conductivity of the modelled material and  $q_T$  is a scalar field representing sources and sinks of heat throughout the domain of the problem. This equation is also known as the temperature equation.

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## 2.5 Necessary Simplification of Equations

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The purpose of this section is to motivate and introduce further common simplifications of the previously presented set of constitutive equations.

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### 2.5.1 Incompressible Flows and Hydrostatic Pressure

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A common simplification when modelling low Mach number flows ( $Ma < 0.3$ ), is the assumption of *incompressibility*, or the assumption of an *isochoric* flow. If one furthermore assumes homogeneous density  $\rho$  in space and time, a restrictive assumption that will be partially alleviated in the following section, the continuity equation in differential form (1) can be simplified to

$$\frac{\partial u_i}{\partial x_i} = 0.$$

In other words: In order for a velocity vector field  $\mathbf{u}$  to be valid for an incompressible flow it has to be free of divergence, or *solenoidal* [6, 75].

If furthermore one assumes the dynamic viscosity  $\mu$  to be constant, which can be suitable in the case of isothermal flow or if the temperature differences within the flow are small, the Navier-Stokes equations in differential form can be reduced to

$$\frac{\partial}{\partial t}(\rho u_i) + \rho \frac{\partial}{\partial x_j}(u_i u_j) = \rho k_i - \frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_j} \left( \mu \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \right) \quad (6a)$$

$$= \rho k_i - \frac{\partial p}{\partial x_i} + \mu \frac{\partial}{\partial x_j} \left( \frac{\partial u_i}{\partial x_j} \right) \quad (6b)$$

by using *Schwartz's* lemma to interchange the order of differentiation. Another common simplification to further simplify the set of equations is the assumption of a volume specific force  $\rho \mathbf{k}$  that can be modelled by a potential, such that it can be represented as the gradient of a scalar field  $\Phi_{\mathbf{k}}$  as

$$-\rho k_i = \frac{\partial \Phi_{\mathbf{k}}}{\partial x_i}.$$

In the case of this thesis this assumption is valid since the mass specific force is the mass specific gravitational force  $\mathbf{g} = (g_i)_{i=1,\dots,3}$  and the density is assumed to be constant, so the potential can be modelled as

$$\Phi_g = -\rho g_j x_j.$$

This term can be interpreted as the hydrostatic pressure  $p_{hyd}$  and can be added to the thermodynamical pressure  $p$  to simplify calculations

$$\begin{aligned} \rho g_i - \frac{\partial p}{\partial x_i} &= \frac{\partial}{\partial x_i}(\rho g_j x_j) - \frac{\partial p}{\partial x_i} \\ &= \frac{\partial}{\partial x_i}(\rho g_j x_j) - \frac{\partial}{\partial x_i}(\hat{p} + p_{hyd}) \\ &= -\frac{\partial \hat{p}}{\partial x_i}. \end{aligned}$$

Since in incompressible fluids only pressure differences matter, this has no effect on the solution. After finishing the calculations  $p_{hyd}$  can be calculated and added to the resulting pressure  $\hat{p}$ .

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### 2.5.2 Variation of Fluid Properties – The Boussinesq Approximation

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When modelling of an incompressible flow involves heat transfer, fluid properties like the density change with varying temperature. If the variation of temperature is small one can still assume a constant density to maintain the structure of the advection and diffusion terms in (5) and only consider changes of the density in the gravitational term. If linear variation of density with respect to temperature is assumed this approximation is called *Boussinesq*-approximation [31]. This approximation furthermore consists in assuming, that all other fluid properties are constant and viscous dissipation can be neglected. In this case the Navier-Stokes equations are formulated using a reference density  $\rho_0$  at the reference temperature  $T_0$  and the now temperature dependent density  $\rho$

$$\rho(T) = \rho_0(1 - \beta(T - T_0)). \quad (7)$$


---

Here  $\beta$  denotes the coefficient of thermal expansion. Under the use of the Boussinesq approximation the incompressible Navier-Stokes equations in differential form can be formulated as

$$\begin{aligned}
\rho_0 \frac{\partial (u_i)}{\partial t} + \rho_0 \frac{\partial}{\partial x_j} (u_i u_j) &= \rho_0 g_i + (\rho - \rho_0) g_i - \frac{\partial p}{\partial x_i} + \mu \frac{\partial}{\partial x_j} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \\
&= \frac{\partial}{\partial x_i} (\rho_0 g_j x_j) + (\rho - \rho_0) g_i - \frac{\partial p}{\partial x_i} + \mu \frac{\partial}{\partial x_j} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \\
&= - \frac{\partial \hat{p}}{\partial x_i} + (\rho - \rho_0) g_i + \mu \frac{\partial}{\partial x_j} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \\
&= - \frac{\partial \hat{p}}{\partial x_i} - \rho_0 \beta (T - T_0) + \mu \frac{\partial}{\partial x_j} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right)
\end{aligned}$$

using  $\rho g$  as the mass specific force.

---

## 2.6 Final Form of the Set of Equations

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In the previous subsections different simplifications have been introduced which will be used throughout the thesis. The final form of the set of equations to be used is thereby presented. As further simplification the modified pressure  $\hat{p}$  will be treated as  $p$  and since the use of the Boussinesq approximation replaces the variable  $\rho$  by a linear function of the temperature  $T$  the reference density  $\rho_0$  for the remainder of this thesis will be referred to as  $\rho$ . Note that incompressibility has been taken into account:

$$\frac{\partial u_i}{\partial x_i} = 0. \quad (8a)$$

$$\rho \frac{\partial (u_i)}{\partial t} + \rho \frac{\partial}{\partial x_j} (u_i u_j) = - \frac{\partial p}{\partial x_i} - \rho \beta (T - T_0) + \mu \frac{\partial}{\partial x_j} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \quad (8b)$$

$$\frac{\partial (\rho T)}{\partial t} + \frac{\partial}{\partial x_j} \left( \rho u_j T - \kappa \frac{\partial T}{\partial x_j} \right) = q_T. \quad (8c)$$

---

### 3 Finite-Volume Methods for Incompressible Flows – Theoretical Basics

---

This section deals with the fundamentals of the numerical solution via a finite-volume method of the formerly presented set of partial differential equations (8). The focus of this section is to provide an overview over the methods to be used in the present thesis. The information contained in this section is based on [?, 28, 42, 68]. The overview starts by mentioning the different grid types to be used and the discretization techniques to be applied. On the basis of integral formulations of the equations to be solved, the therein contained integrals and differential operators have to be discretized. Since the accuracy of the default concepts for discretizing differential operators degrades with decreasing grid quality, this chapter furthermore presents different approaches to handle corrections for cases in which the cause of degrading grid quality is increased non-orthogonality.

The goal of the finite-volume method is to provide linear algebraic equations which can be used to determine an approximate solution of a partial differential equation. However since the Navier-Stokes equations are in general non-linear an intermediate step, before solvers for linear equation systems can be applied, has to be taken, by linearizing the discrete equations. This leads to the need of an iteration process, the *Picard iteration*, which will also be explained briefly.

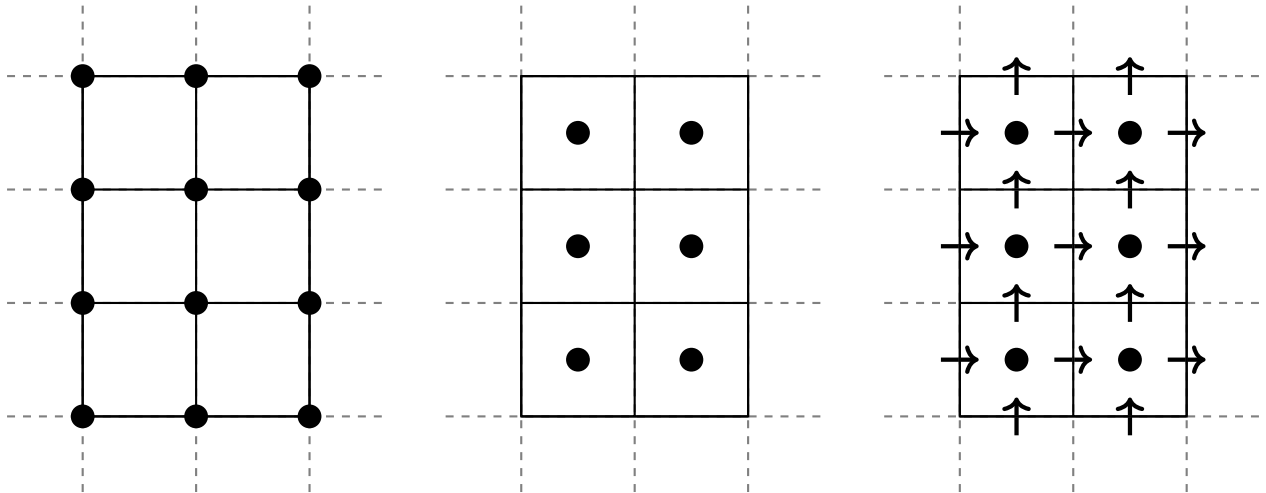
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#### 3.1 Numerical Grid

---

In this subsection a brief overview of the general grid structure to be used in the present thesis is given. The main idea behind finite-volume methods is to solve partial differential equations by integrating them over the specified continuous problem domain and dividing this domain into a finite number of subdomains, the so called *control volumes*. The result of this finite partition of a continuous problem domain is called the numerical grid. The grid consists of a finite number of control volumes which represent the boundaries of a discrete domain of integration. Depending on whether the numerical solution of an equation is to be calculated on the boundary vertices or in the center of a grid cell, the variable arrangement is denoted to be vertex or cell center oriented. For the remainder of the present thesis it is assumed that the variables reside in the cell centers of the respective control volumes.

Another option to arrange variables specifically for algorithms that solve the Navier-Stokes equations is the so called *staggering*. This method stores the variable values of different variables at different grid locations, which facilitates the interpolation of the respective values. As the methods employed in the present thesis are intended to be generally applicable to complex geometries the cell centered non-staggered approach offers more flexibility. Figure 8.2 shows the different variable arrangement options on a two dimensional grid.



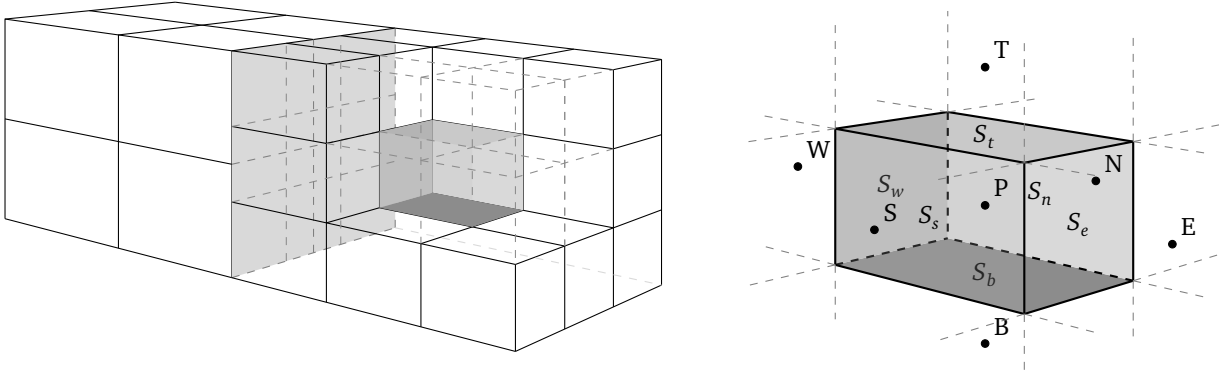
**Figure 1:** Vertex centered, cell centered and staggered variable arrangement. For the staggered arrangement the arrows denote the velocity component and their location on the grid. The centered dot denotes the location of the pressure and further scalar quantities

Regarding the treatment of domain boundaries and the ordering of the cells within the problem domain different types of numerical grids can be distinguished. The present thesis makes use of so called boundary fitted, block structured grids with hexahedron cells. A structured grid is characterized by a constant amount of grid cells in each coordinate direction. The high regularity of structured grids benefits the computational efficiency of algorithms to be used on this type of grid. A block structured grid consists of different grid blocks of which each considered individually is structured, but if the topology of the grid is considered, it is unstructured. An example of a block structured grid with distinguishable



grid blocks is given in figure 2. The use of block structured grids is motivated by the need to increase the adaptivity of structured grids while maintaining high computational efficiency. Furthermore it naturally embraces the concept of domain decomposition which facilitates the implementation of parallel algorithms for the decomposed computational domain. Boundary fitted grids represent domain boundaries by means of the geometry of the control volumes residing on those boundaries. This approach may lead to skewed cells which furthermore affects the accuracy of the results obtained in these boundary cells. The mentioned affects can be alleviated by using local grid refinement techniques to refine the grid in regions of geometrically complex boundaries.

Inside a structured grid block, cells with the shape of hexahedrons are used. In addition to the geometric boundaries of each control volume a numerical grid also provides a mapping that assigns to each control volume with index  $P$  a set of indexes of neighbouring control volumes  $NB(P) := \{W, S, B, T, N, E\}$ , which are named after the geographic directions. Figure 2 shows a single grid cell with its direct neighbours. The faces  $\{S_w, S_s, S_b, S_t, S_n, S_e\}$  of each hexahedral control volume represent the mentioned geometric boundaries.



**Figure 2:** Block structured grid consisting of two blocks

### 3.2 Approximation of Integrals and Derivatives

In the course of transforming a partial differential equation into a system of linear algebraic equations, integrals and derivatives have to be approximated. The simplest method for approximating an integral is by using the *midpoint rule*. This rule is similar to the mean value theorem of integration, which states that there exists a point  $\xi \in V$  for a Riemann integrable function  $\phi$  such that  $\phi(\xi) \int_V dV = \int_V \phi(x) dV$ . For the midpoint rule  $\xi$  is taken to be the center of mass of  $V$ . If the integration domain  $V$  is indeed a volume, fortunately the calculation of  $\phi(\xi)$  with  $\xi := (\int_V x_i dV / \int_V dV)_{i=1,\dots,3}$  presents no difficulties since, due to the collocated variable arrangement, the value of  $\phi$  is stored in the cell center, which corresponds to the location  $\xi$ . However, if the domain of integration is a surface, a preceding interpolation step is necessary.

On the other hand, to transform a partial differential equation into a linear algebraic equation it is necessary to discretize the differential operators of the equations. For numerical reasons two different discretization techniques are used in this thesis. A common task is to discretize expressions of the form

$$(\nabla \phi)_e \cdot \mathbf{n}_e,$$

where  $(\nabla \phi)_e$  is the Gradient of  $\phi$  on a boundary face  $S_e$ . One method is to directly interpret this expression as a directional derivative and approximate it with a central difference

$$(\nabla \phi)_e \cdot \mathbf{n}_e \approx \frac{\phi_P - \phi_E}{\|\mathbf{x}_P - \mathbf{x}_E\|_2}. \quad (9)$$

Another method would be to first calculate the cell center gradients  $(\nabla \phi)_P$  and  $(\nabla \phi)_E$  and interpolate them linearly before calculating the projection onto  $\mathbf{n}_e$

$$(\nabla \phi)_e \cdot \mathbf{n}_e \approx [\gamma_e (\nabla \phi)_P + (1 - \gamma_e) (\nabla \phi)_E] \cdot \mathbf{n}_e, \quad (10)$$

where  $\gamma_e := \|\mathbf{x}_P - \mathbf{x}_e\|_2 / \|\mathbf{x}_P - \mathbf{x}_E\|_2$  is a geometric interpolation factor. For calculating the cell center gradients a method based on Gauss' integration theorem and the midpoint rule for volume integration is employed



$$(\nabla\phi)_{i,p} = \left( \frac{\partial\phi}{\partial x_i} \right)_p \approx \sum_f \phi_f n_i S_f \quad (11)$$

---

### 3.3 Treatment of Non-Orthogonality of Grid Cells

---

Unfortunately real applications involve complex geometries, which in turn affects the orthogonality of the grid. On non-orthogonal meshes the directional derivative in direction of the face unit normal vector  $\mathbf{n}_e$  can no longer be approximated as in (9). On the other side the exclusive usage of (11) is not desirable due to the bigger truncation error that comes with this approximation [42]. Hence a compromise is made and the surface vector  $\mathbf{S}_e := S_e \mathbf{n}_e$  is decomposed as

$$\mathbf{S}_e = \mathbf{\Delta} + \mathbf{k}, \quad (12)$$

where  $\mathbf{\Delta}$  is parallel to the vector  $\mathbf{d}_e := (\mathbf{x}_E - \mathbf{x}_P)$  that directly connects the center  $\mathbf{x}_P$  of the control volume  $P$  with the center  $\mathbf{x}_E$  of its neighbour  $E$ . This vector controls the *orthogonal* contribution to the directional derivative. The vector  $\mathbf{k}$  controls the influence of the *non-orthogonal* contribution. In the next paragraphs the three main decompositions of the surface vector  $\mathbf{S}_e$  will be presented by stating the respective expression for  $\mathbf{\Delta}$ . The resulting vector  $\mathbf{k}$  can be calculated by using (12). One important characteristic that all of the presented approaches have in common, is that the non-orthogonal contribution vanishes, when an orthogonal grid is used. For simplicity the presentation of the decompositions is chosen to be two-dimensional. A geometrical interpretation of the three approaches is given in 3.3.3. The last subsection handles the integration of one generic approach into the discretization process.

---

#### 3.3.1 Minimum Correction Approach

---

This is the approach as proposed in [?]. The reader should note, that even though [28] references [?], they use a different approach to be presented in the next paragraph. This method is designed to keep the non-orthogonal contribution minimal by always choosing  $\mathbf{k}$  to be orthogonal to  $\mathbf{\Delta}$ , which leads to

$$\mathbf{\Delta} = (\mathbf{d} \cdot \mathbf{S}_e) \frac{\mathbf{d}}{\|\mathbf{d}\|_2}.$$

It should be noted that the Influence of the orthogonal contribution decreases with increasing non-orthogonality of the grid.

---

#### 3.3.2 Orthogonal Correction Approach

---

The following method for decomposing the surface normal vector is presented in [28] and the approach implemented in the developed solvers. In this approach a simple projection is used which is independent of the non-orthogonality of the grid. As a result the orthogonal contribution  $\|\mathbf{\Delta}\|_2 = \|\mathbf{S}_e\|_2$  and is thus modelled as

$$\mathbf{\Delta} = S_e \frac{\mathbf{d}}{\|\mathbf{d}\|_2}.$$

---

#### 3.3.3 Over-Relaxed Approach

---

The last approach is used in [20, 42] and is characterized by an increasing influence of the orthogonal contribution with increasing grid non-orthogonality, as opposed to the minimum correction approach. The orthogonal contribution is calculated as

$$\mathbf{\Delta} = S_e^2 \frac{\mathbf{d}}{\mathbf{d} \cdot \mathbf{S}_e}.$$

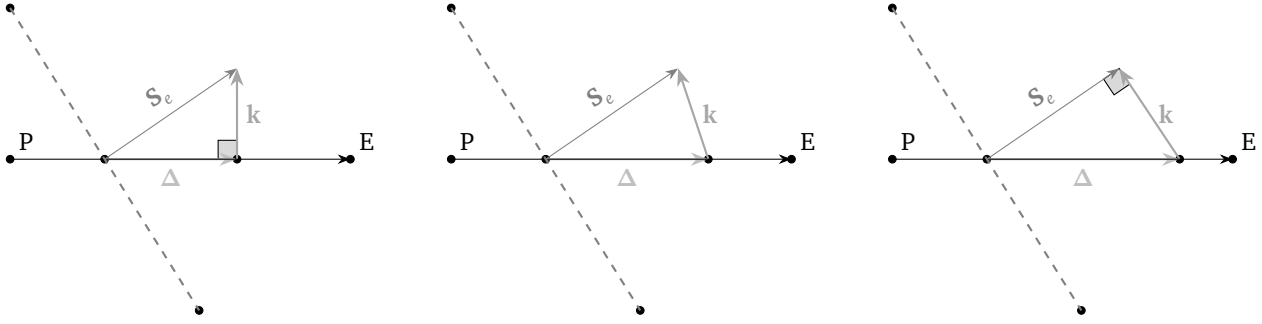
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#### 3.3.4 Deferred Non-Orthogonal Correction

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In order to reduce the computational stencil that would be necessary to handle the non-orthogonal correction implicitly the correction will be treated explicitly using a deferred correction which guarantees that in the case of a fully converged solution only the face normal derivative has been taken into account. Generally the discretization using a non-orthogonal correction would yield

$$(\nabla\phi)_e \cdot \mathbf{S}_e \approx (\nabla\phi)_e \cdot \mathbf{\Delta} + (\nabla\phi)_e \cdot \mathbf{k}.$$



**Figure 3:** Minimum correction, orthogonal correction and over-relaxed approach

Where the first term can be approximated using a central differencing scheme for the directional derivative and the second by interpolating cell center gradients. If one furthermore uses the fact that this method comes to play in a solution algorithm for a non-linear system of partial differential equations, a deferred correction can be implemented which ensures a smaller error from the non-orthogonality. In the case of the previously mentioned discretization techniques for partial derivatives a possible deferred correction approach reads

$$(\nabla \phi)_e \cdot \mathbf{S}_e \approx \|\Delta\|_2 \frac{\phi_P - \phi_E}{\|\mathbf{x}_P - \mathbf{x}_E\|_2} - (\nabla \phi)_e^{(n-1)} \cdot (\Delta - \mathbf{S}_e).$$

It should be noted that the use of a deferred correction in conjunction with the requirement that the non-orthogonal correction vanishes on orthogonal grid introduces an inconsistent discretization of  $(\nabla \phi)_e \cdot \Delta$ .

### 3.4 Numerical Solution of Non-Linear Systems – Linearization Techniques

In the process of solving non-linear systems normally two levels of iterations are distinguished: The *inner* iterations, which account for the iterations needed to solve a given system of linear equations, and *outer* iterations within which is dealt with a possible non-linearity or coupling of the equations. As shown in section 3.3 outer iterations are also necessary if one chooses the deferred correction approach to blend higher and lower order discretization schemes or to apply non-orthogonal correctors.

The system of partial differential equations (8) is non-linear due to the terms  $\rho u_i u_j$  which often are denoted as the convective terms of the Navier-Stokes equations. It is a common approach to linearize those terms according to the *Picard-Iteration*. For the convective terms of the Navier-Stokes equations or the temperature equation this means to guess the mass flux  $\rho u_j$  and approximate as

$$\rho u_j u_i \approx (\rho u_j)^0 u_i.$$

The same procedure is applied to the convective terms of the temperature equation  $\rho u_j T$ . The advantages of this linearization technique are the low memory requirements and the small computational effort for one iteration, this is why this method is commonly found to be implemented in solution programs for flow problems that use a segregated solution algorithm similar to the one implemented in this thesis. Compared to Newton-like methods, this approach does however need more iterations to converge. Another method to linearize convective terms that comes into play when using a fully coupled solution algorithm will be presented in section 5.2.3.

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## 4 Implicit Finite-Volume Method for Incompressible Flows – Segregated Approach

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The purpose of this section is to present the discretization applied to the set of equations (8). Since the system of partial differential equations to be solved always exhibits a coupling, at least between the dependent variables pressure and velocity, a first solution algorithm, namely the *SIMPLE* algorithm, addressed to resolve the pressure velocity coupling, is introduced. Furthermore an under-relaxation factor independent method of calculating mass fluxes by interpolation is introduced and the detailed derivation of all coefficients that result from the discretization process is presented. Finally the boundary conditions, that are relevant for the present thesis will be shown.

---

### 4.1 Discretization of the Mass Balance

---

Integration of equation (8a) over the integration domain of a single control volume  $P$ , after the application of Gauss' integration theorem and the additivity of the Riemann integral, yields

$$\iint_{S_f} u_i n_i dS = \sum_{f \in \{w,s,b,t,n,e\}} \iint_{S_f} u_i n_i dS = 0.$$

In the present work the mass balance is discretized using the midpoint integration rule for the surface integrals and linear interpolation of the velocity to the center of mass of the surface. This leads to the following form of the mass balance:

$$\sum_{f \in \{w,s,b,t,n,e\}} u_{i,f} n_{f_i} S_f = 0, \quad (13)$$

where no interpolation to attain the values of  $u_i$  at the face  $S_f$  is performed yet, since the straightforward linear interpolation will lead to undesired oscillations in the solution fields. An interpolation method to circumvent this so called *checker-boarding* effect is presented in subsection 4.2.

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### 4.2 A Pressure-Weighted Interpolation Method for Velocities

---

The advantages of using a cell-centered variable arrangement are evident: The treatment of non-orthogonality is simplified and the conservation property of finite-volume methods is retained [15, 51, 59, 81]. A major drawback with cell centered variable arrangements is that the pressure field may delink, which will then lead to unphysical oscillations in both the pressure and the velocity results. If the oscillations are severe enough the solution algorithm might even get unstable and diverge. The described decoupling occurs, when the pressure gradient in the momentum balances and the mass fluxes in the continuity equation are discretized using central differences.

A common practice to eliminate this behaviour is the use of a momentum interpolation technique, also known as *Rhie-Chow Interpolation* [66]. The original interpolation scheme however does not guarantee a unique solution, independent of the amount of under-relaxation. The performance of one of the algorithms that are used in the present thesis heavily relies on the under-relaxation of variables to accomplish stability. Furthermore the original method as proposed by [66] does not account for large body forces which also may lead to unphysical results. These issues will be addressed in this subsection which at the end will present an interpolation method that assures an under-relaxation independent solution: the *pressure-weighted interpolation method* [59].

The starting point of the pressure-weighted interpolation method is formed by the discretized momentum balances at node  $P$  and an arbitrary neighbouring node  $Q$ . The discretization for finite-volume methods and details including the incorporation of under-relaxation factors will be handled in subsection 4.5. The semi-discrete implicit momentum balances, if one solves for the velocity at node  $P$  or  $Q$ , read

$$u_{i,P}^{(n)} = -\frac{\alpha_{uP}}{a_P^{u_i}} \left( \sum_{F \in NB(P)} a_F^{u_i} u_{i,F}^{(n)} + b_{P,u_i}^{(n-1)} - V_P \left( \frac{\partial p}{\partial x_i} \right)_P^{(n-1)} \right) + (1 - \alpha_u) u_{i,P}^{(n-1)} \quad (14a)$$

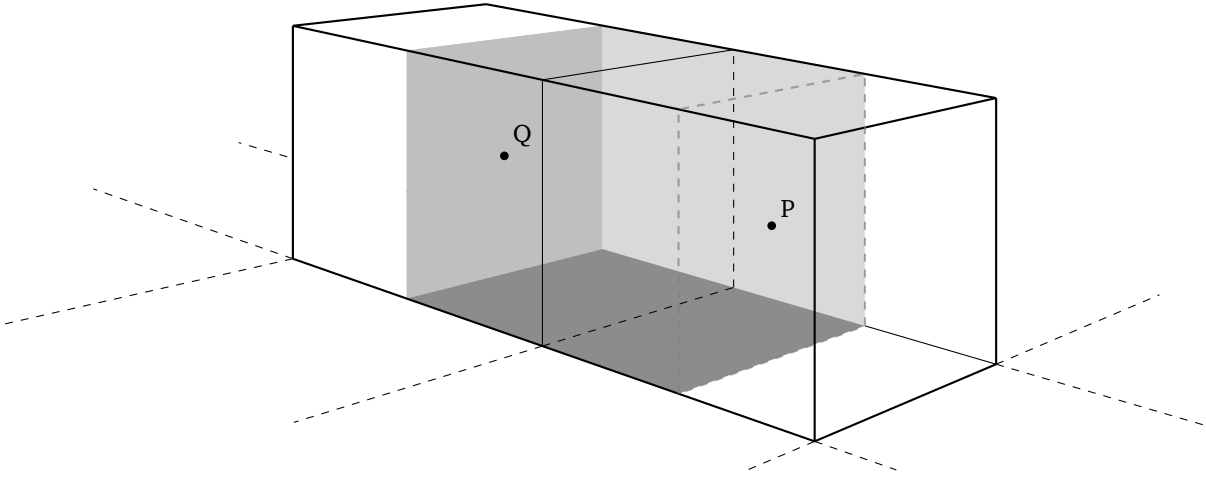
$$\text{and } u_{i,Q}^{(n)} = -\frac{\alpha_{uQ}}{a_Q^{u_i}} \left( \sum_{F \in NB(Q)} a_F^{u_i} u_{i,F}^{(n)} + b_{Q,u_i}^{(n-1)} - V_Q \left( \frac{\partial p}{\partial x_i} \right)_Q^{(n-1)} \right) + (1 - \alpha_u) u_{i,Q}^{(n-1)}, \quad (14b)$$

where the superscript  $(n-1)$  denotes the previous outer iteration number. The reader should note, that the pressure gradient has not been discretized yet. This has the advantage that the selective interpolation technique [68] can be

applied, which is crucial for the elimination of the mentioned oscillations. In almost the same way a semi-discrete implicit momentum balance can be formulated for a virtual control volume located between nodes  $P$  and  $Q$ .

$$u_{i,f}^{(n)} = -\frac{\alpha_u}{a_f} \left( \sum_{F \in NB(f)} a_F^{u_i} u_{i,F}^{(n)} + b_{f,u_i}^{(n-1)} - V_f \left( \frac{\partial p}{\partial x_i} \right)_f^{(n-1)} \right) + (1 - \alpha_u) u_{i,f}^{(n-1)}. \quad (15)$$

Figure 4.2 gives an interpretation of the virtual control volume.



**Figure 4:** Possible interpretation of a virtual control volume (grey) located between nodes  $P$  and  $Q$

To guarantee convergence of this expression for  $u_{i,f}$ , under-relaxation is necessary [51]. To eliminate the undefined artifacts surging from the virtualization of a control volume the following assumptions have to be made to derive a closed expression for the velocity on the boundary face  $S_f$

$$\frac{\alpha_u}{a_f} \left( \sum_{F \in NB(f)} a_F^{u_i} u_{i,F}^{(n)} \right) \approx (1 - \gamma_f) \frac{\alpha_u}{a_P} \left( \sum_{F \in NB(P)} a_F^{u_i} u_{i,F}^{(n)} \right) + \gamma_f \frac{\alpha_u}{a_Q} \left( \sum_{F \in NB(Q)} a_F^{u_i} u_{i,F}^{(n)} \right), \quad (16a)$$

$$\frac{\alpha_u}{a_f} b_{f,u_i}^{(n-1)} \approx (1 - \gamma_f) \frac{\alpha_u}{a_P} b_{P,u_i}^{(n-1)} + \gamma_f \frac{\alpha_u}{a_Q} b_{Q,u_i}^{(n-1)} \quad (16b)$$

$$\text{and } \frac{\alpha_u}{a_f} \approx (1 - \gamma_f) \frac{\alpha_u}{a_P} + \gamma_f \frac{\alpha_u}{a_Q}, \quad (16c)$$

where  $\gamma_f$  is a geometric interpolation factor.

Using the assumptions made in equation (16) the expression in equation (15) can be closed in a way that it only depends on the variable values in node  $P$  and  $Q$

$$\begin{aligned}
u_{i,f}^{(n)} &\approx (1 - \gamma_f) \left( -\frac{\alpha_u}{a_p^{u_i}} \sum_{F \in NB(P)} a_F^{u_i} u_{i,F}^{(n)} \right) + \gamma_f \left( -\frac{\alpha_u}{a_Q^{u_i}} \sum_{F \in NB(Q)} a_F^{u_i} u_{i,F}^{(n)} \right) \\
&\quad + \frac{\alpha_u}{a_f^{u_i}} b_{f,u_i}^{(n-1)} - \frac{\alpha_u}{a_f^{u_i}} V_f \left( \frac{\partial p}{\partial x_i} \right)_f^{(n-1)} + (1 - \alpha_u) u_{i,f}^{(n-1)} \\
&= (1 - \gamma_f) u_{i,p}^{(n)} - (1 - \gamma_f) \frac{\alpha_u}{a_p^{u_i}} \left( b_{p,u_i}^{(n-1)} - V_p \left( \frac{\partial p}{\partial x_i} \right)_p^{(n-1)} \right) + \gamma_f u_{i,Q}^{(n)} - \gamma_f \frac{\alpha_u}{a_Q^{u_i}} \left( b_{Q,u_i}^{(n-1)} - V_Q \left( \frac{\partial p}{\partial x_i} \right)_Q^{(n-1)} \right) \\
&\quad + \frac{\alpha_u}{a_f^{u_i}} b_{f,u_i}^{(n-1)} - \frac{\alpha_u}{a_f^{u_i}} V_f \left( \frac{\partial p}{\partial x_i} \right)_f^{(n-1)} + (1 - \alpha_u) u_{i,f}^{(n-1)} \\
&= \left[ (1 - \gamma_f) u_{i,p}^{(n)} + \gamma_f u_{i,Q}^{(n)} \right] \\
&\quad - \left[ \left( (1 - \gamma_f) \frac{\alpha_u V_p}{a_p^{u_i}} + \gamma_f \frac{\alpha_u V_Q}{a_Q^{u_i}} \right) \left( \frac{\partial p}{\partial x_i} \right)_f^{(n-1)} - (1 - \gamma_f) \frac{\alpha_u V_p}{a_p^{u_i}} \left( \frac{\partial p}{\partial x_i} \right)_p^{(n-1)} - \gamma_f \frac{\alpha_u V_Q}{a_Q^{u_i}} \left( \frac{\partial p}{\partial x_i} \right)_Q^{(n-1)} \right] \\
&\quad + (1 - \alpha_u) \left[ u_{i,f}^{(n-1)} - (1 - \gamma_f) u_{i,p}^{(n-1)} - \gamma_f u_{i,Q}^{(n-1)} \right] \\
&\approx \left[ (1 - \gamma_f) u_{i,p}^{(n)} + \gamma_f u_{i,Q}^{(n)} \right] \\
&\quad - \left( (1 - \gamma_f) \frac{\alpha_u V_p}{a_p^{u_i}} + \gamma_f \frac{\alpha_u V_Q}{a_Q^{u_i}} \right) \left[ \left( \frac{\partial p}{\partial x_i} \right)_f^{(n-1)} - (1 - \gamma_f) \left( \frac{\partial p}{\partial x_i} \right)_p^{(n-1)} - \gamma_f \left( \frac{\partial p}{\partial x_i} \right)_Q^{(n-1)} \right] \\
&\quad + (1 - \alpha_u) \left[ u_{i,f}^{(n-1)} - (1 - \gamma_f) u_{i,p}^{(n-1)} - \gamma_f u_{i,Q}^{(n-1)} \right]. \tag{17}
\end{aligned}$$

It should be noted that the argumentation that led to the last expression, is that the task of the underlined pressure gradient corrector in equation (17) is to suppress oscillations in the converged solution for the pressure field. If there are no oscillations this part should not become active. As long as the behaviour of this corrector remains consistent, i.e. that there are no oscillations in the pressure field within a converged solution, it can be multiplied with arbitrary constants [28]. This is however true on equidistant grids, where  $\gamma_f = 1/2$  and central differences are used to calculate the gradients. On arbitrary orthogonal grids another modification has to be performed which is based on a special case of the mean value theorem of differential calculus and the following

**Proposition.** Let  $x_1, x_2 \in \mathbb{R}$  with  $x_1 \neq x_2$  and  $p(x) = a_0 + a_1 x + a_2 x^2$  a real polynomial function. Then

$$\frac{dp}{dx} \left( \frac{x_1 + x_2}{2} \right) = \frac{p(x_2) - p(x_1)}{x_2 - x_1},$$

i.e. the slope of the secant equals the value of the first derivative of  $p$  exactly half the way between  $x_1$  and  $x_2$ .

*Proof.* Evaluation of the derivative yields

$$\frac{dp}{dx} \left( \frac{x_1 + x_2}{2} \right) = a_1 + 2a_2 \frac{x_1 + x_2}{2} = a_1 + a_2(x_1 + x_2).$$

On the other hand the slope of the secant, using the third binomial rule can be expressed as

$$\begin{aligned}\frac{p(x_2) - p(x_1)}{x_2 - x_1} &= \frac{a_0 + a_1x_2 + a_2x_2^2 - (a_0 + a_1x_1 + a_2x_1^2)}{x_2 - x_1} \\ &= \frac{a_1(x_2 - x_1) + a_2(x_2^2 - x_1^2)}{x_2 - x_1} \\ &= a_1 + a_2(x_2 + x_1).\end{aligned}$$

The comparison of both expressions completes the proof.  $\square$

It is desirable for the pressure corrector to vanish independent of the grid spacing if the profile of the pressure is quadratic and hence does not exhibit oscillations. According to the preceding proposition this can be accomplished by modifying equation (17) to average the pressure gradients from node  $P$  and  $Q$  instead of interpolating linearly

$$\begin{aligned}u_{i,f}^{(n)} &= \left[ (1 - \gamma_f) u_{i,p}^{(n)} + \gamma_f u_{i,Q}^{(n)} \right] \\ &\quad - \left( (1 - \gamma_f) \frac{\alpha_u V_P}{a_p^{u_i}} + \gamma_f \frac{\alpha_u V_Q}{a_Q^{u_i}} \right) \left[ \left( \frac{\partial p}{\partial x_i} \right)_f^{(n-1)} - \frac{1}{2} \left( \frac{\partial p}{\partial x_i} \right)_P^{(n-1)} - \frac{1}{2} \left( \frac{\partial p}{\partial x_i} \right)_Q^{(n-1)} \right] \\ &\quad + \underline{(1 - \alpha_u) \left[ u_{i,f}^{(n-1)} - (1 - \gamma_f) u_{i,p}^{(n-1)} - \gamma_f u_{i,Q}^{(n-1)} \right]}.\end{aligned}\tag{18}$$

Comparing this final expression with the standard interpolation scheme, it is evident that normally, the underlined term is not taken into consideration [28]. However section 7.4 shows, that neglecting this term indeed creates under-relaxation factor dependent results. This section concludes with a final

**Proposition.** *The pressure weighted momentum interpolation scheme (18) guarantees the converged solution for  $u_{i,f}$  to be independent of the velocity under-relaxation  $\alpha_u$ .*

*Proof.* An equivalent formulation of (18) is given by

$$\begin{aligned}\alpha_u u_{i,f}^{(n-1)} + u_{i,f}^{(n-1)} - u_{i,f}^{(n)} &= \alpha_u \left[ (1 - \gamma_f) u_{i,p}^{(n-1)} + \gamma_f u_{i,Q}^{(n-1)} \right] \\ &\quad + \left[ (1 - \gamma_f) (u_{i,p}^{(n)} - u_{i,p}^{(n-1)}) + \gamma_f (u_{i,Q}^{(n)} - u_{i,Q}^{(n-1)}) \right] \\ &\quad - \alpha_u \left( (1 - \gamma_f) \frac{V_P}{a_p^{u_i}} + \gamma_f \frac{V_Q}{a_Q^{u_i}} \right) \left[ \left( \frac{\partial p}{\partial x_i} \right)_f^{(n-1)} - \frac{1}{2} \left( \frac{\partial p}{\partial x_i} \right)_P^{(n-1)} - \frac{1}{2} \left( \frac{\partial p}{\partial x_i} \right)_Q^{(n-1)} \right].\end{aligned}$$

Upon convergence  $u_{i,p}^{(n)} = u_{i,p}^{(n-1)}$  and  $u_{i,f}^{(n)} = u_{i,f}^{(n-1)}$ . This leads to

$$\begin{aligned}\alpha_u u_{i,f}^{(n-1)} &= \alpha_u \left[ (1 - \gamma_f) u_{i,p}^{(n-1)} + \gamma_f u_{i,Q}^{(n-1)} \right] \\ &\quad - \alpha_u \left( (1 - \gamma_f) \frac{V_P}{a_p^{u_i}} + \gamma_f \frac{V_Q}{a_Q^{u_i}} \right) \left[ \left( \frac{\partial p}{\partial x_i} \right)_f^{(n-1)} - \frac{1}{2} \left( \frac{\partial p}{\partial x_i} \right)_P^{(n-1)} - \frac{1}{2} \left( \frac{\partial p}{\partial x_i} \right)_Q^{(n-1)} \right],\end{aligned}$$

which shows, after division by  $\alpha_u > 0$ , that  $u_{i,f}$  is independent of the under-relaxation factor.  $\square$

### 4.3 Implicit Pressure Correction and the SIMPLE Algorithm

The goal of finite-volume methods is to deduce a system of linear algebraic equations from a partial differential equation. In the case of the momentum balances the general structure of this linear equations is

$$u_{i,p}^{(n)} = -\frac{\alpha_{u_p}}{a_p^{u_i}} \left( \sum_{F \in NB(P)} a_F^{u_i} u_{i,F}^{(n)} + b_{P,u_i}^{(n-1)} - V_P \left( \frac{\partial p}{\partial x_i} \right)_P^{(n-1)} \right) + (1 - \alpha_u) u_{i,p}^{(n-1)},$$

where the pressure gradient has been discretized only symbolically and  $b_{p,u_i}^{(n-1)}$  denotes the source term evaluated at the previous outer iteration.

At this stage the equations are still coupled and non-linear. As described in section 3.4 the Picard iteration process can be used to linearize the equations. Every momentum balance equation then only depends on the one dominant variable  $u_i$ . Furthermore the coupling of the momentum balances through the convective term ( $u_i u_j$ ) is resolved in the process of linearization. The decoupled momentum balances can then be solved sequentially for the dominant variable  $u_i$ . All coefficients  $a_{\{p,F\}}^{u_i}$ , the source term and the pressure gradient will be evaluated explicitly by using results of the preceding outer iteration ( $n-1$ ). For the pressure gradient this means to take the pressure of the antecedent outer iteration as a first guess for the following iteration. This guess has to be corrected in an iterative way until all the non-linear equations are fulfilled up to a certain tolerance. Section (6.3.2) presents a suitable convergence criterion and its implementation. This linearization process in conjunction with the pressure guess leads to the linear equation

$$u_{i,p}^{(n*)} = -\frac{\alpha_u}{a_p^{u_i}} \left( \sum_{F \in NB(P)} a_F^{u_i} u_{i,F}^{(n*)} + b_{p,u_i}^{(n-1)} - V_p \left( \frac{\partial p}{\partial x_i} \right)_p^{(n-1)} \right) + (1 - \alpha_u) u_{i,p}^{(n-1)}. \quad (19)$$

Here (\*) indicates that the solution of this equation still needs to be corrected to also fulfill the discretized mass balance

$$\sum_{F \in NB(P)} (u_i)_f^{(n)} n_i S_f = 0. \quad (20)$$

Applying the same procedure as in section 4.2 to equation (19) results in the following expression for the face velocities after solving the discretized momentum balances using as pressure guess the pressure from the previous outer iteration

$$\begin{aligned} u_{i,f}^{(n*)} &= \left[ (1 - \gamma_f) u_{i,p}^{(n*)} + \gamma_f u_{i,Q}^{(n*)} \right] \\ &\quad - \left( (1 - \gamma_f) \frac{\alpha_u V_p}{a_p^{u_i}} + \gamma_f \frac{\alpha_u V_Q}{a_Q^{u_i}} \right) \left[ \left( \frac{\partial p}{\partial x_i} \right)_f^{(n-1)} - (1 - \gamma_f) \left( \frac{\partial p}{\partial x_i} \right)_p^{(n-1)} - \gamma_f \left( \frac{\partial p}{\partial x_i} \right)_Q^{(n-1)} \right] \\ &\quad + (1 - \alpha_u) \left[ u_{i,f}^{(n-1)} - (1 - \gamma_f) u_{i,p}^{(n-1)} - \gamma_f u_{i,Q}^{(n-1)} \right]. \end{aligned} \quad (21)$$

The lack of an equation with the pressure as dominant variable leads to the necessity to alter the mass balance as the only equation left. Methods of this type are called projection methods [28]. A common class of algorithms of this family of methods uses an equation for the additive pressure correction  $p'$  instead of the pressure itself and enforces continuity by correcting the velocities with an additive corrector  $u'_i$ , such that

$$u_{i,p}^{(n)} = u_{i,p}^{(n*)} + u'_{i,p}, \quad u_{i,f}^{(n)} = u_{i,f}^{(n*)} + u'_{i,f} \quad \text{and} \quad p_p^{(n)} = p_p^{(n-1)} + p'_p.$$

It is now possible to formulate the discretized momentum balance for the corrected velocities and the corrected pressure as

$$u_{i,p}^{(n)} = -\frac{\alpha_u}{a_p^{u_i}} \left( \sum_{F \in NB(P)} a_F^{u_i} u_{i,F}^{(n)} + b_{p,u_i}^{(n-1)} - V_p \left( \frac{\partial p}{\partial x_i} \right)_p^{(n)} \right) + (1 - \alpha_u) u_{i,p}^{(n-1)}. \quad (22)$$

It should be noted that the only difference to the equation which will be solved in the next outer iteration is that the source term  $b_{p,u_i}$  has not been updated yet. In the same way the discretized momentum balance for the face velocity  $u_{i,f}$  can be formulated as

$$\begin{aligned} u_{i,f}^{(n)} &= \left[ (1 - \gamma_f) u_{i,p}^{(n)} + \gamma_f u_{i,Q}^{(n)} \right] \\ &\quad - \left( (1 - \gamma_f) \frac{\alpha_u V_p}{a_p^{u_i}} + \gamma_f \frac{\alpha_u V_Q}{a_Q^{u_i}} \right) \left[ \left( \frac{\partial p}{\partial x_i} \right)_f^{(n)} - (1 - \gamma_f) \left( \frac{\partial p}{\partial x_i} \right)_p^{(n)} - \gamma_f \left( \frac{\partial p}{\partial x_i} \right)_Q^{(n)} \right] \\ &\quad + (1 - \alpha_u) \left[ u_{i,f}^{(n-1)} - (1 - \gamma_f) u_{i,p}^{(n-1)} - \gamma_f u_{i,Q}^{(n-1)} \right]. \end{aligned} \quad (23)$$

To couple velocity and pressure correctors one can subtract equation (19) from (22) and equation (21) from (23) to get

$$u'_{i,p} = -\frac{\alpha_u}{a_p^{u_i}} \left( \sum_{F \in NB(P)} a_F^{u_i} u'_{i,F} - V_P \left( \frac{\partial p'}{\partial x_i} \right)_P^{(n)} \right) \quad \text{and} \quad (24)$$

$$u'_{i,f} = [(1-\gamma_f)u'_{i,p} + \gamma_f u'_{i,Q}] - \left( (1-\gamma_f) \frac{\alpha_u V_P}{a_p^{u_i}} + \gamma_f \frac{\alpha_u V_Q}{a_Q^{u_i}} \right) \left[ \left( \frac{\partial p}{\partial x_i} \right)'_f - (1-\gamma_f) \left( \frac{\partial p}{\partial x_i} \right)'_P - \gamma_f \left( \frac{\partial p}{\partial x_i} \right)'_Q \right]. \quad (25)$$

The majority of the class of pressure correction algorithms has these equations as a common basis. Each algorithm then introduces special distinguishable approximations of the velocity corrections that are, at the moment of solving for the pressure correction, still unknown. The method used in the present work is the *SIMPLE* Algorithm (*Semi-Implicit Method for Pressure-Linked Equations*) [62]. The approximation this algorithm performs is severe since the term containing the unknown velocity corrections is dropped entirely. The respective term has been underlined in equation (24). Since the global purpose of the presented method is to enforce continuity by implicitly calculating a pressure correction, the velocity correction has to be expressed solely in terms of the pressure correction. This can be accomplished by inserting equation (24) into equation (25). This gives an update formula

$$u'_{i,f} = - \left( (1-\gamma_f) \frac{\alpha_u V_P}{a_p^{u_i}} + \gamma_f \frac{\alpha_u V_Q}{a_Q^{u_i}} \right) \left( \frac{\partial p}{\partial x_i} \right)'_f, \quad (26)$$

which is then, together with (21), inserted into the discretized continuity equation (20) to obtain

$$\sum_{F \in NB(P)} \left( (1-\gamma_f) \frac{\alpha_u V_P}{a_p^{u_i}} + \gamma_f \frac{\alpha_u V_F}{a_F^{u_i}} \right) \left( \frac{\partial p}{\partial x_i} \right)'_f n_i S_f = b_{p,p}, \quad (27)$$

where the right hand side  $b_{p,p}$  is defined as

$$b_{p,p} := \sum_{F \in NB(P)} u_{i,f}^{(n*)} n_i S_f. \quad (28)$$

The complete discretization with central differences as approximation for the gradient of the pressure correction is straightforward and will be presented in subsection 4.4.

The approximation performed in the SIMPLE algorithm affects convergence in a way that the pressure correction has to be under-relaxed with a parameter  $\alpha_p \in [0, 1]$

$$p_p^{(n)} = p_p^{(n-1)} + \alpha_p p'_p. \quad (29)$$

It should be noted that there are better approximations for the pressure correction which will not rely on pressure under-relaxation for convergence. One example that uses a more consistent approximation is the *SIMPLEC* algorithm (*SIMPLE Consistent*) [78]. A similar derivation of the pressure weighted interpolation method and its implementation for the SIMPLEC algorithm can be found in [59].

As shown in section 4.2 the behaviour of the pressure weighted interpolation method on non-equidistant grids can be improved by replacing the linear interpolation of pressure gradients with a simple average in equation (21). This leads to the following equation for calculating mass fluxes

$$\begin{aligned} u_{i,f}^{(n*)} &= \left[ (1-\gamma_f) u_{i,p}^{(n*)} + \gamma_f u_{i,Q}^{(n*)} \right] \\ &- \left( (1-\gamma_f) \frac{\alpha_u V_P}{a_p^{u_i}} + \gamma_f \frac{\alpha_u V_Q}{a_Q^{u_i}} \right) \left[ \left( \frac{\partial p}{\partial x_i} \right)^{(n-1)}_f - \frac{1}{2} \left( \frac{\partial p}{\partial x_i} \right)^{(n-1)}_P - \frac{1}{2} \left( \frac{\partial p}{\partial x_i} \right)^{(n-1)}_Q \right] \\ &+ (1-\alpha_u) \left[ u_{i,f}^{(n-1)} - (1-\gamma_f) u_{i,p}^{(n-1)} - \gamma_f u_{i,Q}^{(n-1)} \right]. \end{aligned} \quad (30)$$

Generally the SIMPLE algorithm can be represented by an iterative procedure as shown in Algorithm 4.3.



---

**Algorithm 1** SIMPLE Algorithm

---

INITIALIZE variables

**while** (convergence criterion not accomplished) **do**

    SOLVE linearized momentum balances, equation (19)

    CALCULATE mass fluxes using (23) or (30)

    SOLVE pressure correction equation to assure continuity, equation (27)

    UPDATE pressure using (29)

    UPDATE velocities and mass fluxes using (24)

**if** (coupled scalar equation) **then**

        SOLVE scalar equation as described in (4.6)

**end if**

**end while**

---

---

#### 4.4 Discretization of the Mass Fluxes and the Pressure Correction Equation

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Subsections 4.2 and 4.3 introduced the concept of pressure weighted interpolation to avoid oscillating results and an algorithm to calculate a velocity field that obeys continuity. The derived equations have not been discretized completely, furthermore the approach has not been generalized to non-orthogonal grids.

The discretized mass balance (13) only depends on the normal velocities  $u_{i,f} n_{i,f}$ . By analogy with equation (30) an interpolated normal face velocity and thus the mass flux can be calculated as

$$\begin{aligned} u_{i,f}^{(n*)} n_{i,f} = & \left[ (1 - \gamma_f) u_{i,p}^{(n*)} + \gamma_f u_{i,Q}^{(n*)} \right] n_{i,f} \\ & - \left( (1 - \gamma_f) \frac{\alpha_u V_p}{a_p^{u_i}} + \gamma_f \frac{\alpha_u V_Q}{a_Q^{u_i}} \right) \left[ \left( \frac{\partial p}{\partial n} \right)_f^{(n-1)} - \frac{1}{2} \left( \frac{\partial p}{\partial n} \right)_p^{(n-1)} - \frac{1}{2} \left( \frac{\partial p}{\partial n} \right)_Q^{(n-1)} \right] \\ & + (1 - \alpha_u) \left[ u_{i,f}^{(n-1)} - (1 - \gamma_f) u_{i,p}^{(n-1)} - \gamma_f u_{i,Q}^{(n-1)} \right] n_{i,f}, \end{aligned} \quad (31)$$

where the scalar product of pressure gradients and the normal vector has been replaced by a directional derivative in the direction of the face normal vector. In the present work pressure gradients in (31) and pressure correction gradients in equation (27) will be discretized by central differences

$$\left( \frac{\partial p}{\partial n} \right)_f \approx \frac{p_p - p_Q}{(\mathbf{x}_p - \mathbf{x}_Q) \cdot \mathbf{n}_f} \quad \text{and} \quad \left( \frac{\partial p'}{\partial n} \right)_f \approx \frac{p'_p - p'_Q}{(\mathbf{x}_p - \mathbf{x}_Q) \cdot \mathbf{n}_f}.$$

This discretization can then be inserted into the semi-discretized pressure correction equation (27)

$$\sum_{F \in NB(P)} \left( (1 - \gamma_f) \frac{\alpha_u V_p}{a_p^{u_i}} + \gamma_f \frac{\alpha_u V_F}{a_F^{u_i}} \right) \frac{p'_p - p'_F}{(\mathbf{x}_p - \mathbf{x}_F) \cdot \mathbf{n}_f} S_f = b_{p,p}. \quad (32)$$

The resulting coefficients for the pressure correction equation

$$a_p^{p'} p'_p + \sum_{F \in NB(P)} a_F^{p'} p'_F = b_{p,p'},$$

can be calculated as

$$a_F^{p'} = - \left( (1 - \gamma_f) \frac{\alpha_u V_p}{a_p^{u_i}} + \gamma_f \frac{\alpha_u V_F}{a_F^{u_i}} \right) \frac{S_f}{(\mathbf{x}_p - \mathbf{x}_F) \cdot \mathbf{n}_f} \quad \text{and} \quad a_p^{p'} = - \sum_{F \in NB(P)} a_F^{p'}. \quad (33)$$

The right hand side can be calculated as in equation (28), if the presented discretization is applied.

## 4.5 Discretization of the Momentum Balance

If the stationary momentum balance is integrated over a single control volume  $P$  the result reads

$$\underbrace{\iint_S (\rho u_i u_j) n_j dS}_{\text{convective term}} - \underbrace{\iint_S \left( \mu \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \right) n_j dS}_{\text{diffusive term}} = - \underbrace{\iiint_V \frac{\partial p}{\partial x_i} dV}_{\text{pressure sourceterm}} - \underbrace{\iiint_V \rho \beta (T - T_0) dV}_{\text{temperature sourceterm}}, \quad (34)$$

where the different terms to be addressed individually in the following sections are indicated. The reader should note that the form of this equation has been modified by using Gauss' integration theorem. The terms residing on the left will be treated in an implicit and due to deferred corrections also in an explicit way, whereas the terms on the right will be treated exclusively in an explicit way.

### 4.5.1 Linearization and Discretization of the Convective Term

The convective term  $(\rho u_i u_j)$  of the Navier-Stokes equations is the reason for the non-linearity of the equations. In order to deduce a set of linear algebraic equations from the Navier-Stokes equations this term has to be linearized. As introduced in section (3.4), the non linearity will be dealt with by means of an iterative process, the Picard iteration. The part dependent on the non dominant dependent variable therefore will be approximated by its value from the previous iteration as  $\rho u_i^{(n)} u_j^{(n)} \approx \rho u_i^{(n)} u_j^{(n-1)}$ . However this linearization will not be directly visible because it will be covered by the mass flux  $\dot{m}_f = \iint_{S_f} \rho u_j^{(n-1)} n_j dS$ .

Using the additivity of the Riemann integral the first step is to decompose the surface integral into individual contributions from each boundary face of the control volume  $P$

$$\iint_S \rho u_i u_j n_j dS = \sum_{f \in \{w,s,b,t,n,e\}} \iint_{S_f} \rho u_i u_j n_j dS = \sum_{f \in \{w,s,b,t,n,e\}} F_{i,f}^c,$$

where  $F_{i,f}^c := \iint_{S_f} \rho u_i^{(n)} u_j^{(n-1)} n_j dS$  is the convective flux of the velocity  $u_i$  through the boundary face  $S_f$ .

To improve diagonal dominance of the resulting linear system while maintaining the smaller discretization error of a higher order discretization, a blended discretization scheme is applied and combined with a deferred correction. Since due to the non-linearity of the equations to be solved, an iterative solution process is needed by all means, the overall convergence does not degrade noticeably when using a deferred correction [28]. Blending and deferred correction result in a decomposition of the convective flux into a lower order approximation, which is treated implicitly, and the explicit difference between the higher and lower order approximation for the same convective flux. Since for coarse grid resolutions the use of higher order approximations may lead to oscillations of the solution, which in turn may degrade or even impede convergence, the schemes can be blended by a control factor  $\eta \in [0, 1]$ . Furthermore the use of low-order approximations increases the diagonal dominance of the matrix, which then benefits the convergence of iterative solvers for the linear systems [68].

To show the generality of this approach all further derivations are presented for the generic boundary face  $S_f$  that separates control volume  $P$  from its neighbour  $F \in NB(P)$ . This decomposition then leads to

$$F_{i,f}^c \approx \underbrace{F_{i,f}^{c,l}}_{\text{implicit}} + \eta \underbrace{[F_{i,f}^{c,h} - F_{i,f}^{c,l}]}_{\text{explicit}}^{(n-1)}.$$

It should be noted that the convective fluxes carrying an  $l$  for *lower* or an  $h$  for *higher* as exponent, already have been linearized and discretized. The discretization applied to the convective flux in the present work is using the midpoint integration rule and blends the upwind interpolation scheme with a linear interpolation scheme. Applied to above decomposition one can derive the following approximations

$$\begin{aligned} F_{i,f}^{c,l} &= u_{i,F} \min(\dot{m}_f, 0) + u_{i,P} \max(0, \dot{m}_f) \\ F_{i,f}^{c,h} &= u_{i,F} \gamma_f + u_{i,P} (1 - \gamma_f), \end{aligned}$$

where the variable values have to be taken from the previous iteration step  $(n-1)$  as necessary and the mass flux  $\dot{m}_f$  has been used as result of the linearization process. The results can now be summarized by presenting the convective contribution to the matrix coefficients  $a_{F,u_i}$  and  $a_P^{u_i}$  and the right hand side  $b_{P,u_i}$  which are calculated as

$$a_F^{u_i,c} = \min(\dot{m}_f, 0), \quad a_P^{u_i,c} = \sum_{F \in NB(P)} \max(0, \dot{m}_f) \quad (35a)$$

$$\text{and } b_{P,u_i}^c = \sum_{F \in NB(P)} \eta \left( u_{i,F}^{(n-1)} (\min(\dot{m}_f, 0) - \gamma_f) \right) + \eta \left( u_{i,P}^{(n-1)} (\max(0, \dot{m}_f) - (1 - \gamma_f)) \right). \quad (35b)$$

#### 4.5.2 Discretization of the Diffusive Term

The diffusive term contains the first partial derivatives of the velocity as a result of the material constitutive equation that characterizes the behaviour of Newtonian fluids. As pointed out in section 3.3, directional derivatives can be discretized using central differences on orthogonal grids or in the more general case of non-orthogonal grids using central differences implicitly and an explicit deferred correction comprising the non-orthogonality of the grid. As seen in equation (6) the diffusive term of the Navier-Stokes equations can be simplified using the mass balance in the case of an incompressible flow with constant viscosity  $\mu$ . To sustain the generality of the presented approach this simplification will be omitted.

As before, by using the additivity and furthermore linearity of the Riemann integral, the integration of the diffusive term will be divided into integration over individual boundary faces  $S_f$

$$\iint_S \left( \mu \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \right) n_j dS = \sum_{f \in \{w,s,b,t,n,e\}} \left[ \iint_{S_f} \mu \frac{\partial u_i}{\partial x_j} n_j dS + \iint_{S_f} \mu \frac{\partial u_j}{\partial x_i} n_j dS \right] = \sum_{f \in \{w,s,b,t,n,e\}} F_{i,f}^d,$$

where  $F_{i,f}^d$  denotes the diffusive flux through an individual boundary face. Section 3.3 only covered the non-orthogonal corrector for directional derivatives. Since the velocity is a vector field and not a scalar field, the results of section 3.3 may only be applied to the underlined term. The other term will be treated explicitly since it is considerably smaller than the underlined term, furthermore does not cause oscillations and thus will not derogate convergence [28]. First, all present integrals will be approximated using the midpoint integration rule. The diffusive flux  $F_{i,f}^d$  for a generic face  $S_f$  located between the control volumes  $P$  and  $F$  then reads

$$F_{i,f}^d \approx \underbrace{\mu \left( \frac{\partial u_i}{\partial x_j} \right)_f}_{\text{diffusive flux}} n_j S_f + \mu \left( \frac{\partial u_j}{\partial x_i} \right)_f n_j S_f.$$

Using central differences for the implicit discretization of the directional derivative and furthermore using the *orthogonal correction* approach from 3.3.2 the approximation can be derived as

$$\begin{aligned} F_{i,f}^d &\approx \mu \left( \frac{\|\Delta_f\|_2}{\|\mathbf{x}_P - \mathbf{x}_F\|_2} \frac{u_{P_i} - u_{F_i}}{\|\mathbf{x}_P - \mathbf{x}_F\|_2} - (\nabla u_i)_f^{(n-1)} \cdot (\Delta_f - \mathbf{S}_f) \right) + \mu \left( \frac{\partial u_j}{\partial x_i} \right)_f^{(n-1)} n_{f_i} \\ &= \mu \left( S_f \frac{u_{P_i} - u_{F_i}}{\|\mathbf{x}_P - \mathbf{x}_F\|_2} - \left( \frac{\partial u_i}{\partial x_j} \right)_f^{(n-1)} (\xi_{f_i} - n_{f_i}) S_f \right) + \mu \left( \frac{\partial u_j}{\partial x_i} \right)_f^{(n-1)} n_{f_i}, \end{aligned}$$

where the unit vector pointing in direction of the straight line connecting control volume  $P$  and control volume  $F$  is denoted as

$$\xi_f = \frac{\mathbf{x}_P - \mathbf{x}_F}{\|\mathbf{x}_P - \mathbf{x}_F\|_2}.$$

The interpolation of the cell center gradients to the boundary faces is performed as in (10). Now the contribution of the diffusive part to the matrix coefficients and the right hand side can be calculated as

$$a_F^{u_i,d} = -\frac{\mu S_f}{\|\mathbf{x}_p - \mathbf{x}_F\|_2}, \quad a_p^{u_i,d} = \sum_{F \in NB(P)} \frac{\mu S_f}{\|\mathbf{x}_p - \mathbf{x}_F\|} \quad (36a)$$

$$\begin{aligned} b_{F,u_i}^d &= - \sum_{F \in NB(P)} \left( \frac{\partial u_i}{\partial x_j} \right)_f^{(n-1)} (\xi_{f_i} + n_{f_i}) S_f - \mu \left( \frac{\partial u_j}{\partial x_i} \right)_f^{(n-1)} n_{f_i} S_f \\ &= - \sum_{F \in NB(P)} \left( \frac{\partial u_i}{\partial x_j} \right)_f^{(n-1)} \xi_{f_i} S_f + \mu \left( \left( \frac{\partial u_i}{\partial x_j} \right)_f^{(n-1)} + \left( \frac{\partial u_j}{\partial x_i} \right)_f^{(n-1)} \right) n_{f_i} S_f. \end{aligned} \quad (36b)$$

#### 4.5.3 Discretization of the Source Terms

Since in the segregated solution approach in every equation all other variables but the dominant one are treated as constants and furthermore the source terms in equation (34) do not depend on the dominant variable, the discretization is straightforward. The source terms of the momentum balance are discretized using the midpoint integration rule for volume integrals, which leads to the source term

$$- \iiint_V \frac{\partial p}{\partial x_i} dV - \iiint_V \rho \beta (T - T_0) dV \approx - \left( \frac{\partial p}{\partial x_i} \right)_p^{(n-1)} V_p - \rho \beta (T_p^{(n-1)} - T_0) V_p = b_{p,u_i}^{sc}. \quad (37)$$

#### 4.6 Discretization of the Temperature Equation

The discretization of the temperature equation is performed by the same means as for the momentum balance. The only difference is a simpler diffusion term. The integral form of the temperature equation, after applying the Gauss' theorem of integration, is

$$\underbrace{\iint_S \rho u_j T n_j dS}_{\text{advective term}} - \underbrace{\iint_S \kappa \frac{\partial T}{\partial x_j} n_j dV}_{\text{diffusive term}} = \underbrace{\iiint_V q_T dV}_{\text{source term}}.$$

Proceeding as in the previous subsections one can now discretize the advective term, the diffusive term and the source term. Since this process does not provide further insight, just the final results will be presented. The discretization yields the matrix coefficients as

$$a_F^T = \min(\dot{m}_f, 0) + \frac{\kappa S_f}{\|\mathbf{x}_p - \mathbf{x}_F\|_2} \quad (38a)$$

$$a_p^T = \sum_{F \in NB(P)} \max(0, \dot{m}_f) - \frac{\kappa S_f}{\|\mathbf{x}_p - \mathbf{x}_F\|_2} \quad (38b)$$

$$\begin{aligned} b_{p,T} &= \sum_{F \in NB(P)} \eta \left( T_F^{(n-1)} (\min(\dot{m}_f, 0) - \gamma_f) \right) + \eta \left( T_p^{(n-1)} (\max(0, \dot{m}_f) - (1 - \gamma_f)) \right) \\ &\quad + \sum_{F \in NB(P)} \left( \frac{\partial T}{\partial x_j} \right)_f^{(n-1)} (\xi_{f_j} - n_{f_j}) S_f \\ &\quad + q_{T_p} V_p. \end{aligned} \quad (38c)$$

Again it is possible, though not always necessary as in the case of the velocities, to under-relax the solution of the resulting linear system with a factor  $\alpha_T$ . This can be accomplished as will be shown in subsection 4.9.

---

## 4.7 Boundary Conditions

---

As the antecedent subsections showed, it is possible to deduce a linear algebraic equation for each control volume by the finite-volume method. The approach presented in the preceding subsections however did not cover the treatment of control volumes at domain boundaries yet. This subsection introduces the boundary conditions which are relevant for the present work and furthermore deals with transitional conditions at block boundaries.

### 4.7.1 Dirichlet Boundary Conditions

---

The first boundary condition is the Dirichlet boundary condition. This type of boundary condition is used to model inlet conditions for flow problems. For the temperature equation it may also be used at walls as will be shown in subsection 4.7.2. It is characterized by specifying the value of the variable for which the equation is solved explicitly. As a result boundary fluxes can be calculated directly. Especially the mass flux  $\dot{m}_f$  is known and hence does not have to be calculated using the pressure weighted interpolation method. Since no special modifications have to be made, as the resulting coefficient for a neighbouring control volume laying past the boundary is considered on the right hand side of the linear system, the implementation approach will be presented only for the temperature equation. Since there is no boundary condition that fixes the gradient at Dirichlet boundaries it is assumed that the partial derivatives of the respective variable are constant and can hence be extrapolated

$$\left( \frac{\partial T}{\partial x_j} \right)_f \approx \left( \frac{\partial T}{\partial x_j} \right)_p.$$

The modification to the central coefficient of the linear equation can be recursively formulated as

$$a_p^T = a_p^T + \left( \max(0, \dot{m}_f) - \frac{\kappa S_f}{\|\mathbf{x}_p - \mathbf{x}_f\|_2} \right),$$

whereas the contribution to the right hand side reads

$$b_{p,T} = b_{p,T} - \left( \min(\dot{m}_f, 0) - \frac{\kappa S_f}{\|\mathbf{x}_p - \mathbf{x}_f\|_2} \right) T_f + \left( \frac{\partial T}{\partial x_j} \right)_p^{(n-1)} (\xi_{fj} - n_{fj}) S_f$$

The reader should note, that even though the gradient discretization at domain boundaries is realized by a one sided forward differencing scheme instead of a central differencing scheme. This does not drastically affect accuracy because the distance used in the differential quotient is half the distance used on a central difference inside the domain [68].

### 4.7.2 Treatment of Wall Boundaries

---

A common boundary to the solution domain is given by solid walls. For all kind of flows this boundary condition first of all has a kinematic character, since the concept of impermeable walls dictates a zero normal velocity at the wall. In viscous flows, wall boundaries can be interpreted furthermore as a no-slip condition, i.e. a Dirichlet boundary condition for the velocities. Convective fluxes through solid walls are thus zero by definition however the diffusive fluxes require special treatment not only for the velocities but also for the temperature. To approximate the fluid behavior on a wall boundary correctly, special modifications have to be taken into account to model the normal a shear tension. Furthermore diffusive fluxes for the temperature can be given by Neumann or Dirichlet boundary conditions.

The derivation of the discretized diffusive flux through wall boundaries starts from the integral momentum balance (2) for the vector  $\mathbf{u}$ . Here only the term for surface forces is needed

$$\mathbf{F}_w = \iint_{S_w} \mathbf{t} dS = \iint_{S_w} \mathbf{T}(\mathbf{n}_w) dS \quad (39)$$

For the purpose of treating wall boundary conditions it is appropriate to use a local coordinate system  $n, t, s$  where  $n$  denotes the wall normal coordinate,  $t$  denotes the coordinate tangential to the wall shear force and,  $s$  is the binormal coordinate. With respect to this coordinate system the wall normal vector is represented by  $\mathbf{n}_w = (1, 0, 0)^T$  and the image of the wall normal vector  $\mathbf{T}(\mathbf{n}_w)$  is represented by

$$\mathbf{T}(\mathbf{n}_w) = \begin{bmatrix} \tau_{nn} & \tau_{nt} & \tau_{ns} \\ \tau_{nt} & \tau_{tt} & \tau_{ts} \\ \tau_{ns} & \tau_{ts} & \tau_{ss} \end{bmatrix} \begin{bmatrix} 1 \\ 0 \\ 0 \end{bmatrix} = \begin{bmatrix} \tau_{nn} \\ \tau_{nt} \\ \tau_{ns} \end{bmatrix}$$

The velocity of the wall is assumed to be constant [68], so the directional derivative of the tangential velocity vanishes on the wall

$$\tau_{tt} = \frac{\partial u_t}{\partial x_t} = 0,$$

which in conjunction with the continuity equation in differential form (1) leads to

$$\frac{\partial u_n}{\partial x_n} + \frac{\partial u_t}{\partial x_t} = \frac{\partial u_n}{\partial x_n} = 0, \quad (40)$$

what is equivalent to  $\tau_{nn} = 0$  at the wall. It should be noted that the velocity is assumed to have no component in the binormal direction. A physical interpretation of 40 would be, that the transfer of momentum at the wall occurs by shear forces exclusively. Furthermore the coordinate direction  $t$  is chosen to be parallel to the shear force which is no restriction because of the possibility to rotate the coordinate system within the plane. This leads to  $\tau_{ns} = 0$ . The absolute value of the surface force hence only depends on the normal derivative of the velocity tangential to the wall. After transforming the coordinates back to the system  $(x_1, x_2, x_3)$  the surface force can be calculated and the integral can be discretized using the midpoint integration rule by

$$\mathbf{F}_w = \iint_{S_w} \mathbf{t}_w \tau_{nt} dS = \iint_{S_w} \mathbf{t}_w \mu \frac{\partial u_t}{\partial n} dS = \mathbf{t}_w \mu \left( \frac{\partial u_t}{\partial n} \right)_w S_w, \quad (41)$$

where  $\mathbf{t}_w$  denotes the transformed tangential vector  $(0, 1, 0)^T$  with respect to the coordinate system  $(x_1, x_2, x_3)$ . In the discretization process this tangential vector will be calculated from the velocity vector as

$$\mathbf{t}_w = \frac{\mathbf{u}_t}{\|\mathbf{u}_t\|_2}, \quad \text{where} \quad \mathbf{u}_t = \mathbf{u} - (\mathbf{u} \cdot \mathbf{n}_w) \mathbf{n}_w.$$

According to [28] this force should not be handled explicitly for convergence reasons. On the other side, if the surface force is expressed by the velocities  $u_i$  the discretization process would lead to different central matrix coefficients, which would affect memory efficiency.

The discretization approach used in the present thesis uses a simpler implicit discretization coupled with a deferred correction that combines the explicit discretization of the surface force (41) with a central difference. At first the contained directional derivative is discretized implicitly by

$$\left( \frac{\partial u_t}{\partial n} \right)_{t_{wi}} \approx \left( \frac{\partial u_i}{\partial \xi} \right) \approx \frac{u_{i,p} - u_{i,w}}{\|\mathbf{x}_p - \mathbf{x}_w\|_2}$$

and explicitly by

$$\left( \frac{\partial u_t}{\partial n} \right)_{t_{wi}} \approx \frac{(u_{i,p} - u_{i,w}) - (u_{j,p} - u_{j,w}) n_j n_i}{(\mathbf{x}_p - \mathbf{x}_w) \cdot \mathbf{n}_w}.$$

Therefore the contributions to the central coefficient and the right hand side of the linear equation that results from the presented discretization process are

$$a_p^{u_i} = a_p^{u_i} + \mu \frac{S_f}{\|\mathbf{x}_p - \mathbf{x}_w\|_2} \quad \text{and} \\ b_{p,u_i} = b_p^{u_i} + \mu \frac{S_f}{\|\mathbf{x}_p - \mathbf{x}_w\|_2} u_{i,p}^{(n-1)} + \frac{(u_{i,p}^{(n-1)} - u_{i,w}) - (u_{j,p}^{(n-1)} - u_{j,w}) n_j n_i}{(\mathbf{x}_p - \mathbf{x}_w) \cdot \mathbf{n}_w}.$$

The reader should note that since the deferred correction uses a Dirichlet boundary condition, no correction of the value of the wall velocity  $u_{i,w}$  has to be accounted for.

If the solution of the flow field is coupled to the solution of a temperature equation, different options for the boundary condition at walls may be chosen. If the wall temperature is known, a Dirichlet boundary condition for the temperature is the choice. A wall of this type is called to be *isothermal*. If on the other side only the heat flux is known, a Neumann boundary condition is used. In the special case of zero heat flux the wall is called to be *adiabatic*. For adiabatic walls, which are besides isothermal walls used for the present thesis, the implementation is straight forward since no coefficients have to be calculated.

---

#### 4.7.3 Treatment of Block Boundaries

---

If block structured grids are used to decompose the problem domain, the characterizing property of structured grids, which is the constant amount of grid cells in each direction, gives each inner cell exactly six neighbours. If more than one grid block is used this property is violated if the number of grid cells of each block is chosen to be arbitrary. The arbitrariness of the grid resolution is a main benefactor for the adaptivity of block structured grids.

To maintain the conservation property of finite-volume methods, block boundaries should not be interpreted as boundaries in the classical sense. Instead conditions have to be formulated to guarantee that flows through block boundaries are conserved. The method to treat block boundaries used in the present thesis was presented by [50]. Another method was presented in [48]. However, the first method was chosen since it allows a fully implicit consideration of the block boundary fluxes. This method calculates fluxes through separate face segments  $S_l$  that come up on *non-matching* grid blocks. Each of this face segments gets assigned a control volume  $L$  and a control volume  $R$  which exclusively share this face segment. An algorithm to provide this needed information has been implemented in the present thesis.

Once the geometric data, including the information regarding the interpolation coefficients at block boundaries, has been provided, the fluxes through these boundaries can be calculated as presented in the antecedent subsections. The connectivity of neighbouring control volumes of different grid blocks is represented by matrix coefficients  $a_L^\phi$  and  $a_R^\phi$ , where  $\phi \in \{u_1, u_2, u_3, p, T\}$ .

---

#### 4.8 Treatment of the Singularity of the Pressure Correction Equation with Neumann Boundaries

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It has to be noted that the derived pressure correction equation is a Poisson equation. As can be proven [35], the linear  $N \times N$  systems surging from the presented discretization on a grid with  $N$  control volumes have a nullspace of dimension one, i.e.

$$\text{null}(A_{p'}) = \text{span}(\mathbb{1}),$$

where  $\mathbb{1} = (1)_{i=1,\dots,N} \in \mathbb{R}^N$  is the vector spanning the nullspace. This singularity accounts for the property of incompressible flows, that pressure can only be determined up to a constant. To fix this constraint various possibilities exist [28]. A common method is to set the pressure correction to zero in one reference control volume and hence fix the pressure at one reference point in the problem domain. This can be done before solving the system by applying this Dirichlet-type condition, or it can be done afterwards when pressure is calculated from the pressure correction. This approach is not suitable for grid convergence studies since without proper interpolation it is not guaranteed that the reference pressure correction is taken at the correct location.

Since some comparisons performed in the present work rely on grid convergence studies another approach for reducing the lose constraint of the pressure correction system has been used: The reference pressure correction is taken to be the mean value of the pressure correction over the domain

$$p'_{\text{ref}} = \frac{\int_V p' dV}{\int_V dV} \approx \frac{\sum_{p=1}^N p'_p V_p}{\sum_{p=1}^N V_p}$$

such that the net pressure correction amounts to zero. This modifies equation (29) to read

$$p_p^{(n)} = p_p^{(n-1)} + \alpha_p (p'_p - p'_{\text{ref}}).$$

---

#### 4.9 Structure of the Assembled Linear Systems

---

The objective of a finite-volume method is to create a set of linear algebraic equations by discretizing partial differential equations. In the case of the discretized momentum balance, taking all contributions together leads to the following linear algebraic equation for each control volume  $P$

$$a_p^{u_i} u_{p_i} + \sum_{F \in NB(P)} a_F u_{F_i} = b_{p_{u_i}},$$

where the coefficients are composed as

$$\begin{aligned} a_p^{u_i} &= a_p^{u_i,c} - a_p^{u_i,d} \\ a_F^{u_i} &= a_F^{u_i,c} - a_F^{u_i,d} \\ b_{p_{u_i}} &= b_{p_{u_i},c} - b_{p_{u_i},d} + b_{p_{u_i}}^{sc}. \end{aligned}$$

Similar expressions for the pressure correction equation and the temperature equation exist. In the case of control volumes located at boundaries some of the coefficients will be calculated in a different way. This aspect is addressed in section 4.7.

For the decoupled iterative solution process of the Navier-Stokes equations it is necessary to reduce the change of each dependent variable in each iteration. Normally this is done by an *under-relaxation* technique, a convex combination of the solution of the linear system for the present iteration ( $n$ ) and from the previous iteration ( $n - 1$ ) with the under-relaxation parameter  $\alpha_{u_i} \in (0, 1]$ , where  $\alpha_{u_i} = 1$  refers to no under-relaxation. Generally speaking, this parameter can be chosen individually for each equation. Since there are no rules for choosing this parameters in a general setting, the under-relaxation parameter for the velocities is chosen to be equal for all three velocities,  $\alpha_{u_i} = \alpha_u$  [68]. This has the further advantage that, in case the boundary conditions are implemented with the same intention, the linear system for each of the velocities remains unchanged except for the right hand side. This helps to increase memory efficiency.

Let the solution for the linear system without under-relaxation be denoted as

$$\tilde{u}_{p_i}^{(n)} := \frac{b_{p,u_i} - \sum_{F \in NB(P)} a_F u_{F_i}}{a_p^{u_i}},$$

Which is only a formal expression for the case the underlying linear system is solved exactly. A convex combination as described yields

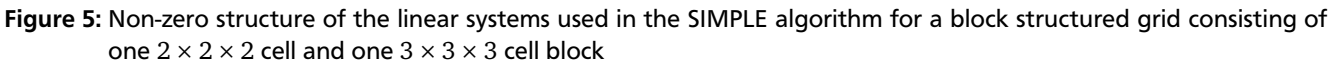
$$\begin{aligned} u_{p_i}^{(n)} &:= \alpha_u \tilde{u}_{p_i}^{(n)} + (1 - \alpha_u) u_{p_i}^{(n-1)} \\ &= \alpha_u \frac{b_{p,u_i} - \sum_{F \in NB(P)} a_F u_{F_i}}{a_p^{u_i}} + (1 - \alpha_u) u_{p_i}^{(n-1)}, \end{aligned}$$

an expression that can be modified to derive a linear system whose solution is the under-relaxed velocity

$$\frac{a_p^{u_i}}{\alpha_u} u_{i,p} + \sum_{F \in NB(P)} a_F^{u_i} u_{i,F} = b_{p,u_i} + \frac{(1 - \alpha_u) a_p^{u_i}}{\alpha_u} u_{i,p}^{(n-1)}.$$

After all matrix coefficients have been successfully calculated, the linear system system can be represented by a system matrix  $A$  and a right hand side vector  $b$ . Figure 6.3.4 shows the non-zero structure of a linear system for a grid consisting of a  $2 \times 2 \times 2$  cell and a  $3 \times 3 \times 3$  cell block.





## 5 Implicit Finite-Volume Method for Incompressible Flows – Fully Coupled Approach

Since the antecedent section 4 already discussed the discretization details on the involved equations, this section aims at a comparison at the algorithmic level of the SIMPLE algorithm, presented in section 4.3, as a method to resolve the pressure-velocity coupling, and an implementation of a fully coupled solution algorithm. It should be noted that the discretization of the equations to be solved is not changed in any way to maintain comparability, so the presented differences are exclusively due to difference in the solution algorithm. Successful implementations of a fully coupled solution algorithm for incompressible Navier-Stokes equations have been presented in [13, 20, 27, 77]. In addition the presented work will extend the solution approach presented in [27] to three-dimensional domains. Furthermore this section will present various approaches to incorporate different degrees of velocity-to-temperature and temperature-to-velocity/pressure coupling. Finally the structure of the resulting linear system to be solved is discussed.

### 5.1 The Fully Coupled Algorithm – Pressure-Velocity Coupling Revised

This subsection motivates the use of a fully coupled algorithm to resolve pressure-velocity coupling and mentions the differences to the approach presented in subsection 4.3. The mentioned subsection presented a common solution approach to solve incompressible Navier-Stokes equations: After the linearization of the equations, momentum balances were solved using the pressure from the previous iteration as a guess. Since in general the velocity field obtained by solving a momentum balance with a guessed pressure does not obey continuity, the velocity field and the pressure field had to be corrected. This in turn would lead to an inferior solution regarding the residual of the momentum balances. To avoid this iterative guess-and-correct solution process another class of approaches to the pressure-velocity coupling problematic, represented by algorithms that are *fully coupled*, will be introduced now.

The central aspect of fully coupled solution methods for Navier-Stokes equations is, that instead of solving for the velocities and pressure corrections sequentially, the velocity field and the pressure are solved for simultaneously [68], so every velocity field that is calculated obeys conservation of momentum and mass, without the need to be corrected. As a result the under-relaxation of pressure and velocities is no longer required, which accelerates convergence significantly in terms of needed outer iterations. The only reason for still needing an iterative solution process is the non-linearity of the Navier-Stokes equations which is accounted for by the use of the Picard iteration process, which has been presented in subsection 3.4. The iterations fortunately make room for deferred corrections as introduced in subsection 4.5. It should be noted that it is also possible to use the coupled solution algorithm to calculate pressure corrections. Reference [46] uses this approach to solve the Navier-Stokes equations.

On the downside implementations of fully coupled solution methods require significantly more system memory than segregated methods. This is due to the higher amount of information that has to be available at the same time and the resulting linear systems which also require more memory, due to the increased amount of unknowns to solve for. Furthermore the bad condition of the linear algebraic system [68] tends to slow down the convergence of the equation solver algorithm.

As in the case of segregated methods it is not advisable to solve the mass balance equation directly [68]. Instead of deriving an equation for the pressure correction  $p'$ , as shown in 4.3, an equation for the pressure is derived by using the pressure-weighted interpolation method, which has been introduced in 4.2 and is used to approximate the velocities in the discretized mass balance (13). Concretely equation (18) is adapted for the use in a fully coupled algorithm

$$u_{i,f}^{(n)} = \left[ (1 - \gamma_f) u_{i,p}^{(n)} + \gamma_f u_{i,Q}^{(n)} \right] - \left( (1 - \gamma_f) \frac{V_p}{a_p^{u_i}} + \gamma_f \frac{V_Q}{a_Q^{u_i}} \right) \left[ \left( \frac{\partial p}{\partial x_i} \right)_f^{(n)} - \frac{1}{2} \left( \left( \frac{\partial p}{\partial x_i} \right)_p^{(n-1)} + \left( \frac{\partial p}{\partial x_i} \right)_Q^{(n-1)} \right) \right].$$

The changes comprise the removal of last term of (18) accounting for the under-relaxation, since no under-relaxation is needed in fully coupled algorithms which is equivalent to an under-relaxation factor  $\alpha_u = 1$ . Furthermore the underlined partial derivatives are now going to be treated implicitly. This leads to the semi-implicit pressure equation

$$\begin{aligned} \sum_{F \in NB(P)} \rho \left[ (1 - \gamma_f) u_{i,p}^{(n)} + \gamma_f u_{i,F}^{(n)} \right] S_f - \rho \left( (1 - \gamma_f) \frac{V_p}{a_p^{u_i}} + \gamma_f \frac{V_F}{a_F^{u_i}} \right) \left[ \left( \frac{\partial p}{\partial x_i} \right)_f^{(n)} \right] S_f \\ = - \sum_{F \in NB(P)} \rho \left( (1 - \gamma_f) \frac{V_p}{a_p^{u_i}} + \gamma_f \frac{V_F}{a_F^{u_i}} \right) \left[ \frac{1}{2} \left( \left( \frac{\partial p}{\partial x_i} \right)_p^{(n-1)} + \left( \frac{\partial p}{\partial x_i} \right)_F^{(n-1)} \right) \right] S_f. \end{aligned} \quad (43)$$

Even though this equation is solved for the pressure  $p$  while equation (27) is solved for the pressure correction  $p'$  the matrix coefficients from the pressure correction discretization of equation (33) and the calculation of the right hand

side is given in equation (28). For the implicit coupling to the velocities  $u_i$  additional matrix coefficients have to be considered. These can be calculated as

$$a_F^{p,u_i} = \rho \gamma_f S_f \quad \text{and} \quad a_p^{p,u_i} = \sum_{F \in NB(P)} \rho (1 - \gamma_f) S_f.$$

On the other side the discretized momentum balance gives matrix coefficients to account for the implicit velocity-pressure coupling. They are calculated as

$$a_F^{u_i,p} = \gamma_f S_f \quad \text{and} \quad a_p^{u_i,p} = \sum_{F \in NB(P)} (1 - \gamma_f) S_f.$$

If the Boussinesq approximation is used implicitly, an additional coefficient  $a_p^{u_i,T}$  to account for the velocity temperature coupling has to be considered. This will be handled in subsection 5.2

---

**Algorithm 2** Fully Coupled Solution Algorithm

---

```

INITIALIZE variables
while (convergence criterion not accomplished) do
  if (temperature coupling) then
    SOLVE the linear system for velocities, pressure and temperature
  else
    SOLVE the linear system for velocities and pressure
  end if
  CALCULATE mass fluxes using REFERENCE
  if (decoupled scalar equation) then
    SOLVE scalar equation as described in (4.6)
  end if
end while

```

---



---

## 5.2 Coupling to the Temperature Equation

---

Since the present work also aims at analyzing the efficiency of different methods to couple the temperature equation to the velocities and vice-versa this subsection discusses different approaches to handle the coupling of the temperature equation to the Navier-Stokes equations if the Boussinesq-Approximation, as introduced in subsection 2.5.2, is used. The effectiveness of realizing a strong coupling of the temperature equation to the Navier-Stokes equations depends on the flow problem. The physical coupling tends to increase in flow scenarios of natural convection, where the temperature difference and hence the buoyancy term in the Navier-Stokes equations dominates the fluid movement. Generally speaking: The higher the physical coupling of temperature and flow, the greater are the benefits of using an implementation that uses a strong coupling to the temperature equation. The following subsections present different approaches that can be used for different intensities of coupling.

---

### 5.2.1 Decoupled Approach – Explicit Velocity-to-Temperature Coupling

---

The decoupled approach is similar to the treatment of the velocity-temperature coupling described in subsection 4.5. If this approach is chosen no special measures have to be taken. The momentum balances receive a contribution  $b_p^{u_i,T}$  with

$$b_p^{u_i,T} := -\rho \beta (T_p^{(n-1)} - T_0) V_p,$$

that handles the coupling explicitly by using the temperature result of the previous outer iteration. In some cases it might be necessary to under-relax the temperature each iteration

---

### 5.2.2 Implicit Velocity-to-Temperature Coupling

---

In the same way it is possible to realize the coupling described in the previous subsection by implicitly considering the temperature in the momentum balances, which leads to an additional matrix coefficient  $a_p^{u_i,T}$  and an additional contribution to the right hand side accounting for the coupling to the temperature equation

$$a_p^{u_i,T} = \rho \beta V_p \quad \text{and} \quad b_p^{u_i,T} = \rho \beta T_0 V_p.$$


---

### 5.2.3 Temperature-to-Velocity/Pressure Coupling – Newton-Raphson Linearization

The previous section discussed the velocity temperature coupling and so far only the momentum balances were affected by the realization of the coupling methods. Independently it is possible to couple the temperature equation not only to the momentum balances but also to the pressure equation. In section 4.6 the non-linear partial differential equation was linearized using a Picard iteration method. Specifically the convective term  $\rho u_j T$  was linearized by taking the mass flux from the antecedent solve of the momentum and pressure correction equations. If the decoupled approach is used, this treatment remains valid. But, if an implicit temperature coupling is sought, a coupling of the temperature equation to the momentum balances which considers the mass fluxes is desirable. Methods that exhibit the described property can be found in [29, 61, 72, 77]. A common denomination of the therein used linearization method is called *Newton-Raphson linearization* which can be interpreted as a bilinear approximation of the convective term by the linear terms of the respective Taylor polynomial.

The Newton-Raphson linearization technique is applied to the convective term of the temperature equation as follows. A first order Taylor approximation of the mass specific convective flux through the boundary face  $S_f$  around the  $(n-1)$ st iteration value yields for the approximation at the  $n$ th iteration

$$\begin{aligned} (u_{j,f} T_f)^{(n)} &\approx (u_{j,f} T_f)^{(n-1)} + \frac{\partial}{\partial u_{j,f}} (u_{j,f} T_f)^{(n-1)} (u_{j,f}^{(n)} - u_{j,f}^{(n-1)}) + \frac{\partial}{\partial T_f} (u_{j,f} T_f)^{(n-1)} (T_f^{(n)} - T_f^{(n-1)}) \\ &= (u_{j,f} T_f)^{(n-1)} + T_f^{(n-1)} (u_{j,f}^{(n)} - u_{j,f}^{(n-1)}) + u_{j,f}^{(n-1)} (T_f^{(n)} - T_f^{(n-1)}) \\ &= \underline{u_{j,f}^{(n-1)} T_f^{(n)}} + u_{j,f}^{(n)} T_f^{(n-1)} - u_{j,f}^{(n-1)} T_f^{(n-1)}. \end{aligned}$$

A comparison with section 4.5.1 shows, that the underlined term coincides with the term from the usual linearization. The first of the two new terms will be treated implicitly and explicitly after using the pressure-weighted interpolation method from section ?? to interpolate the value of  $u_{j,f}$ . The second term will be treated explicitly. The use of the pressure-weighted interpolation method does not only create a temperature-to-velocity but also a temperature-to-pressure coupling. Applying the pressure-weighted interpolation, the equation for the mass specific convective flux reads

$$\begin{aligned} (u_{j,f} T_f)^{(n)} &\approx \underline{u_{j,f}^{(n-1)} T_f^{(n)}} + T_f^{(n-1)} \left[ (1 - \gamma_f) u_{j,p}^{(n)} + \gamma_f u_{j,Q}^{(n)} \right] \\ &\quad - T_f^{(n-1)} \left( (1 - \gamma_f) \frac{\alpha_u V_p}{a_p^{u_j}} + \gamma_f \frac{\alpha_u V_Q}{a_Q^{u_j}} \right) \left[ \left( \frac{\partial p}{\partial x_j} \right)_f^{(n)} - \frac{1}{2} \left( \frac{\partial p}{\partial x_j} \right)_p^{(n-1)} - \frac{1}{2} \left( \frac{\partial p}{\partial x_j} \right)_Q^{(n-1)} \right] \\ &\quad - u_{j,f}^{(n-1)} T_f^{(n-1)}. \end{aligned}$$

If this semi-implicit, semi-discrete equation is discretized completely new matrix and contributions can be calculated

$$\begin{aligned} a_F^{T,u_i} &= \rho T_f^{(n-1)} \gamma_f n_{f,i} S_f \\ a_P^{T,u_i} &= \sum_{F \in NB(P)} \rho T_f^{(n-1)} (1 - \gamma_f) n_{f,i} S_f \\ a_F^{T,p} &= -\rho T_f^{(n-1)} \left( (1 - \gamma_f) \frac{\alpha_u V_p}{a_p^{u_i}} + \gamma_f \frac{\alpha_u V_F}{a_F^{u_i}} \right) \frac{S_f}{(\mathbf{x}_P - \mathbf{x}_F) \cdot \mathbf{n}_f} = \rho T_f^{(n-1)} a_F^p \\ \text{and } a_P^{T,p} &= - \sum_{F \in NB(P)} T_f^{(n-1)} a_F^{T,p}. \end{aligned}$$

The explicit parts resulting from the Newton-Raphson linearization yield additional contributions to the right hand side

$$b_P^{T,NR} = \rho u_{j,f}^{(n-1)} T_f^{(n-1)} n_{f,j} S_f - \rho T_f^{(n-1)} \left( (1 - \gamma_f) \frac{\alpha_u V_p}{a_p^{u_j}} + \gamma_f \frac{\alpha_u V_Q}{a_Q^{u_j}} \right) \left[ \frac{1}{2} \left( \frac{\partial p}{\partial x_j} \right)_p^{(n-1)} + \frac{1}{2} \left( \frac{\partial p}{\partial x_j} \right)_Q^{(n-1)} \right] n_{j,f} S_f$$

### 5.3 Boundary Conditions on Domain and Block Boundaries

The treatment of boundary conditions and transitional conditions at block boundaries is very similar to the way presented in section 4.7. The main difference results from the fact that in addition to the necessary changes from section 4.7, modifications are necessary to the new matrix coefficients from the discretized momentum balance and the pressure equation in the coupled solution algorithm. The purpose of this section is therefore to only focus on these additional changes.

How Dirichlet boundary conditions, also known as inlet boundaries, affect the matrix coefficients that only correspond to the velocities has been presented in section 4.7.1. It is common to use Neumann boundary conditions for the pressure at Dirichlet boundaries with respect to the velocities [20]. Under the assumption that the gradient of the pressure vanishes at inlet boundaries, the matrix coefficients for the velocity-to-pressure coupling have to be modified to

$$a_p^{u_i,p} = a_p^{u_i,p} + n_{f,i} S_f.$$

Wall boundary conditions are treated likewise with the additional modifications to the right hand side contribution as presented in section 4.7.2.

The treatment of velocity Dirichlet boundary conditions in the pressure equation is straightforward, since the correspond to mass fluxes through the boundary faces. Hence the matrix coefficients remain unchanged and only the right hand side contributions embrace the fact that no implicit interpolation is necessary to calculate the mass flux through the boundary face.

Finally it should be noted that the Newton-Raphson linearization technique does not apply to the velocities on boundary faces, since the value of the velocities is known exactly and a linearization of the convective contribution becomes unnecessary.

At block boundaries the new matrix coefficients  $a_L^{u_i,p}$  and  $a_R^{u_i,p}$  for the velocity-to-pressure coupling and the matrix coefficients  $a_L^{p,u_i}$  and  $a_R^{p,u_i}$  have to be taken into account. This does not present any drawbacks on the presented approach.

### 5.4 Assembly of Linear Systems – Final Form of Equations

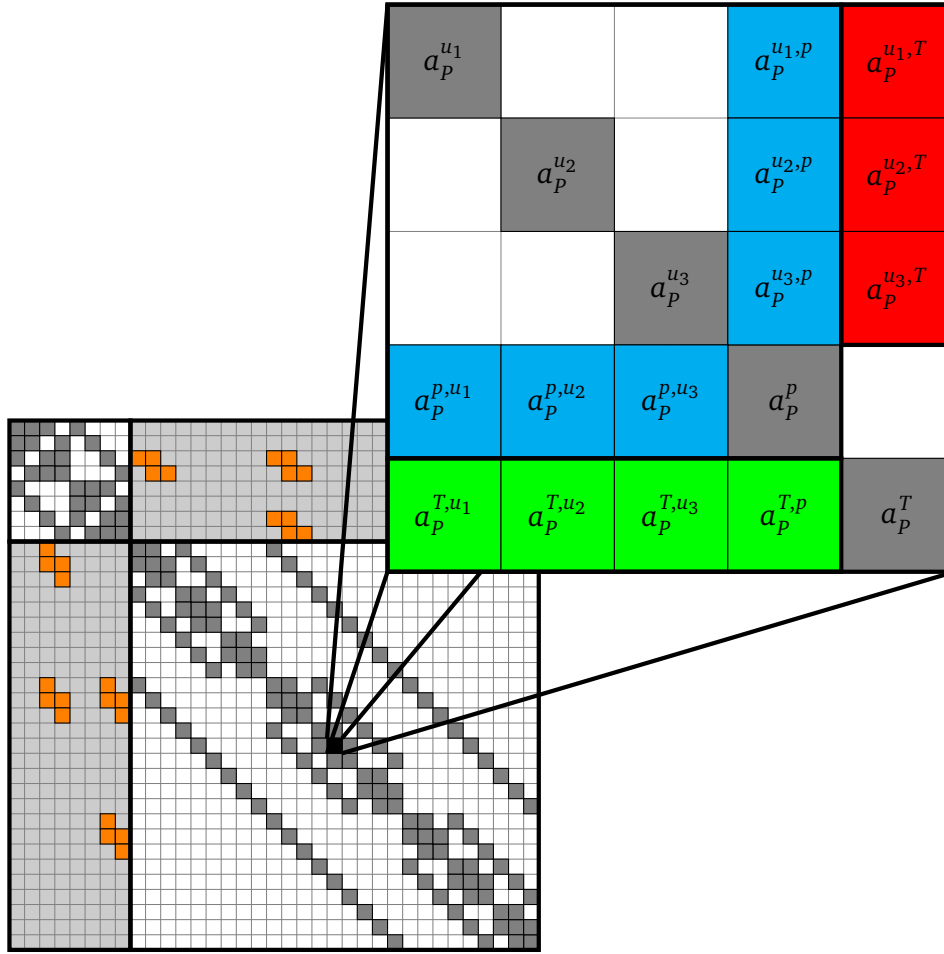
Concluding this section presents the final form of the derived linear algebraic equations. Based on the presented discretization each equation only contains variable values of neighbouring control volumes. The set of five equations reads

$$a_p^{u_i} u_{p,i} + \sum_{F \in NB(P)} a_F^{u_i} u_{F,i} + \underbrace{a_p^{u_i,p} p_p + \sum_{F \in NB(P)} a_F^{u_i,p} p_F}_{\text{Pressure-velocity coupling}} + \underbrace{a_p^{u_i,T} T_p}_{\text{Boussinesq approximation}} = b_{p,u_i} \quad i = 1, \dots, 3 \quad (44)$$

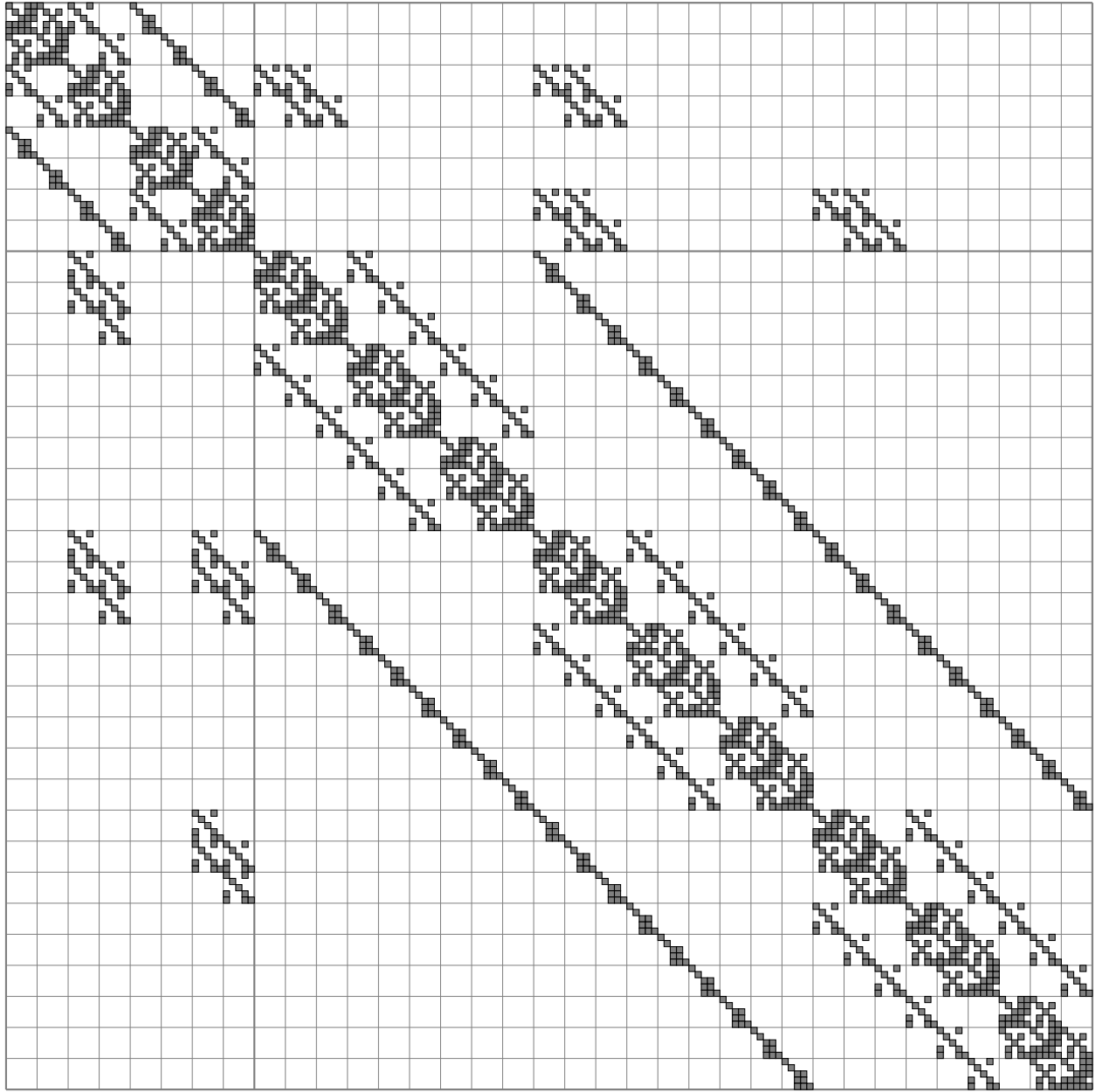
$$a_p^p p_p + \sum_{F \in NB(P)} a_F^p p_F + \underbrace{\sum_{j=1}^3 \left( a_p^{u_j,p} u_{p,j} + \sum_{F \in NB(P)} a_F^{p,u_j} u_{F,j} \right)}_{\text{Pressure-velocity coupling}} = b_{p,p} \quad (45)$$

$$a_p^T T_p + \sum_{F \in NB(P)} a_F^T T_F + \underbrace{\sum_{j=1}^3 \left( a_p^{T,u_j} u_{p,j} + \sum_{F \in NB(P)} a_F^{p,u_j} u_{F,j} \right)}_{\text{Newton-Raphson linearization}} + a_p^{T,p} p_p + \sum_{F \in NB(P)} a_F^{T,p} p_F = b_{p,T}. \quad (46)$$

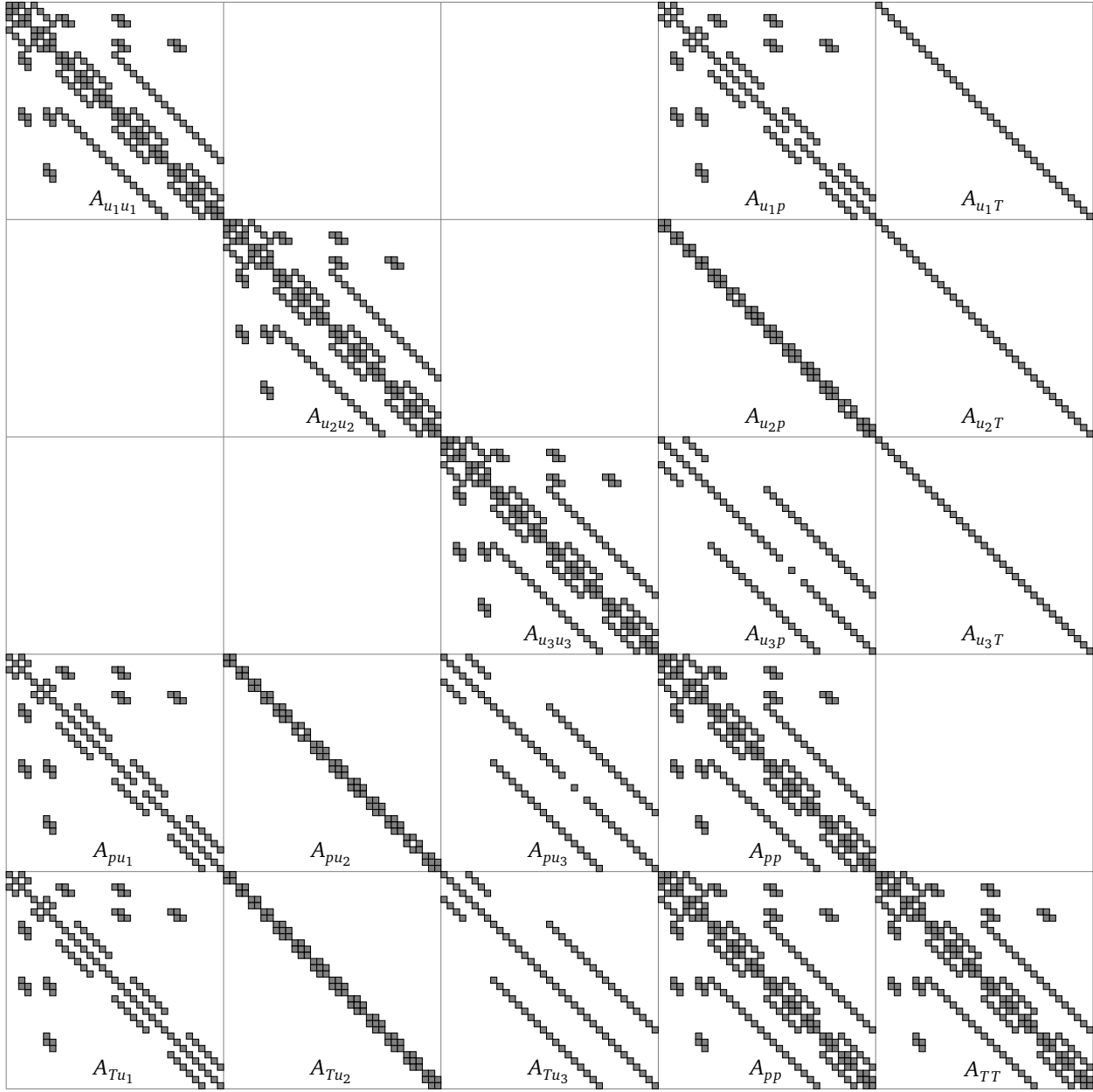
The different degrees of coupling between the different equations will affect the matrix structure. Depending on the variable arrangement other matrix structures are possible. Figure 5.4 shows the resulting block matrix structure if the fields are treated as interlaced quantities. Figure ?? shows the non-zero structure of a block matrix for the same case if no field interlacing is used. It should be noted, that the variable arrangement only affects the storage of the matrices not the way the matrix is used, since it is possible to arbitrarily reorder the matrix entries through the underlying index sets to obtain other matrix representations.



**Figure 6:** Non-zero structure of block submatrices of the linear systems used in the coupled solution algorithm for a block structured grid consisting of one  $2 \times 2 \times 2$  cell and one  $3 \times 3 \times 3$  cell block. The blue coefficients represent the pressure-velocity coupling, the red coefficients correspond to the velocity-to-temperature coupling and the green coefficients result from the Newton-Raphson linearization technique.



**Figure 7:** Non-zero structure of the linear system used in the coupled solution algorithm for a block structured grid consisting of one  $2 \times 2 \times 2$  cell and one  $3 \times 3 \times 3$  cell block. The variables have been interlaced and the matrix consists of blocks as shown in figure 5.4.



**Figure 8:** Non-zero structure the linear system used in the coupled solution algorithm for a block structured grid consisting of one  $2 \times 2 \times 2$  cell and one  $3 \times 3 \times 3$  cell block. The variables have been ordered such that each major matrix block refers to only one variable or the coupling between exactly two variables.



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## 6 CAFFA Framework

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This section presents the CAFFA framework that has been extended for the present thesis. *CAFFA* is an acronym and stands for *Computer Aided Fluid Flow Analysis*. The solver framework is based on Perić's CAFFA code [?,?] that has been modified to handle three-dimensional problem domains and block structured grids with non-matching blocks. Furthermore, the framework has been parallelized making extensive use of the PETSc library. One characteristic of the solver framework is, that arbitrary block boundaries are handled in a fully implicit way. Details on how those transitional conditions are handled can be found in section 4.7.3. The framework consists of two different solver algorithms, a segregated solver and a fully coupled solver, which have been introduced in sections 4 and 5 respectively. In addition, the framework features an own implementation of a grid generator for block structured grids as well as a mapper program to convert grids created with ICEM CFD [?] into a format understandable by the CAFFA code. To prepare the grid data for the later use in the solvers, a preprocessor program has been integrated into the framework. Furthermore the solver programs exhibit different export functionalities to visualize the numerical grid and the results within ParaView [38] and the export of binary vectors and matrices to MATLAB ® [54].

The following subsections will now briefly introduce the PETSc framework, present the components of the CAFFA framework and finally sketch the program flow.

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### 6.1 PETSc Framework

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*PETSc* is an acronym for *Portable Extensible Toolkit for Scientific Computation* and is a software suite that comprises data structures and an extensive set of linear solver routines [8, 9]. A great part of the data structures is designed to work in parallel on high performance computers, also the solver routines have been parallelized using the MPI standard for message passing. PETSc provides the tools that can be used to build large-scale application codes for scientific calculations. The great advantage of PETSc is that it adds multiple additional layers of abstraction that make its use in applications straightforward and allow the users to focus on the essential implementations of their own code instead of having to deal with parallel data structures and algorithms, which furthermore represents an additional source for programming errors. PETSc provides different interfaces through which the user can parallelize his code, what furthermore increases readability and maintainability of the developed code. Last but not least, the implementations used for data structures and solvers in PETSc have are not only verified and updated on a regular basis, they have furthermore proven to be highly efficient in the creation of large-scale computer applications on high performance clusters [11, 34, 43].

The data structures PETSc reflect the commonly used elements in scientific codes. Vectors, matrices and index sets are among these basic data structures. Beyond that PETSc offers a variety of options for its data structures. Vectors can either be used sequentially or in parallel in which case PETSc distributes the vector components to the processes inside a specific MPI communicator. Furthermore parallel matrix formats are available that allow the processes to assemble different parts of one global matrix simultaneously. PETSc contains other data structures that can be used to fetch and distribute either vector or matrix elements from remote processes.

On the other side PETSc contains a large collection of parallel solvers for linear systems. The major part comprises Krylov subspace methods which have been introduced in section ?? . Among the variety of solver options that are available for further optimization of the performance, the Krylov subspace methods can be combined with elements of another thorough collection of preconditioners and other third party packages like Hypre [26] or ML [30]. For further details on the available data structures and subroutines the reader is referred to [7, 8].

In addition to the mentioned tools PETSc also comes with an internal profiler tool that collects a variety of information on the used PETSc objects and bundles them into a human readable log file. The log file and other dynamic output which can be triggered by command line arguments facilitate the optimization process of developed applications and allow the accurate determination of performance measures.

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### 6.2 Grid Generation and Preprocessing

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A grid generator has been developed to generate hexahedral block structured grids. To provide flexibility for testing locally refined and skewed grids the grid generator deploys a random number generator which moves grid points within the domain and varies the number of grid cells of each block optionally. Key feature of the developed framework is the handling of block structured locally refined grids with non-matching block interfaces. The neighbouring relations are represented by a special type of boundary condition.

After the grid has been generated a preprocessor program comes to application, which prepares the numerical grid for the use in the solver program. An essential part of the preprocessing step is the application of various matching algorithms depending on the type of block boundary condition. The preprocessor program differentiates between three block boundary types of which each is a subtype of the other. The most simple block boundary condition is given by a one-to-one relation between two neighbouring boundary cells. The generalisation of this condition involves several boundary cells, that share only one neighbouring boundary cell in the neighbouring block. This relation is also known as a many-to-one relation. The third boundary condition on block boundaries implements the most general many-to-many

relation, which needs special consideration in the preprocessing step, because the number of neighbours on cell can have is not known a priori.

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### 6.3 Implementation of CAFFA

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This section provides an overview of the implementation aspects of the developed CAFFA framework. Since applications for modern computers have to be able to efficiently use the provided resources the concept for the parallelization of the application is presented. A separate section presents how convergence is monitored and controlled. Later on, this section presents how to use the data structures that store the variables and how to realize the domain composition as central part of the parallelization process.

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#### 6.3.1 The Message-Passing Model

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The PETSc framework makes thoroughly use of the message-passing computational model [33]. This model assumes that a set of processes with local memory is able to communicate with other processes by passing, i.e. sending and receiving messages. *MPI* is an acronym for *Message Passing Interface* and is a software library that collects features of message-passing systems. More importantly it provides a widely used standard that assures portability of application that make use of this library as does PETSc.

The message-passing model is not only reflected in the application as a programming paradigm, but also in the design of parallel computers and their communication network. Under this perspective the message-passing model is complementary to the distributed memory design, which encapsulates the idea of local memory and the exchange of data through a network. High performance computers are seldom designed exclusively as a distributed memory system, rather they incorporate features of another model, namely the shared memory model. This memory model is characterized by a common address space, which each of the processes can access uniformly, i.e. with a location independent latency, or non-uniformly. Latter systems are also called *NUMA* systems (*Non-Uniform Memory Access*). A widely used system design, as for the system the performance tests of section REFERENCE are performed on, comprises features of both models by using NUMA computing nodes that share local memory and are able to exchange messages with other NUMA nodes via an interconnect.

One important advantage of using software that uses the message passing model and hence applications that were parallelized within this programming paradigm, is their compatibility with computers that use combinations of distributed and shared memory.

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#### 6.3.2 Convergence Control

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One part of the PETSc philosophy is to provide great flexibility in choosing solvers and parameters from within the command line. However, the developed framework implements a non-linear iteration process without using the SNES objects provided by PETSc. This creates the need for a hard-coded implementation of convergence control. Convergence control for the used Picard iteration method comprises two parts. One part controls the overall convergence, and determines when the calculations have finished. The other part controls convergence on an outer iteration basis. The convergence criteria are met if the actual residual falls below the upper bound for the residual  $r_{final}$ . The bound for final convergence is hereby determined to

$$r_{final} = r_{initial} * 10^{-8},$$

which states that a decrease of the initial residual of  $10^{-8}$  indicates convergence. This criterion will be fixed for all further analyses since it controls the overall accuracy of the solver results and hence maintains comparability of solver performance.

The other convergence criterion can be handled with more flexibility, since it controls the relative decrease of the residual in each outer iteration. This parameter should not affect the overall accuracy but instead convergence speed, within the individual bounds on the solver algorithm. This means that, depending on the coupling algorithm, low relative solver tolerances will not always benefit convergence speed. On the other hand low relative solver tolerances will affect the number of inner iterations and hence the execution time of the solver program. The convergence criterion for each outer iteration is implemented as

$$r_{final}^{(k)} = r_{initial}^{(k)} * rtol,$$

where  $rtol$  indicates the relative decrease of the residual in each outer iteration.

---

### 6.3.3 Indexing of Variables and Treatment of Boundary Values

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All variables needed by the CAFFA solver are represented by one-dimensional arrays. To establish a mapping between a location  $(i, j, k)$  of the numerical grid and the respective variable values location  $(ijk)$  inside the array the following formula is used

$$(ijk) = N_i N_j (k - 1) + N_j (i - 1) + j,$$

where  $N_i$  and  $N_j$  are the Number of grid cells in the respective coordinate direction plus two additional boundary cells. The inclusion of the boundary cells circumvents the need to provide an additional data structure for boundary values. Furthermore the same mapping rule can be used for the grid vertex coordinates. This variable indexing will be used to assemble the matrices surging from the discretization process. This will lead to rows for the boundary values, that that are decoupled from the rest of the linear system. PETSc provides two different approaches to handle boundary values. In the first approach another abstraction layer is introduced via an object, that redistributes the data and removes the rows containing the boundary values. This approach has been tested with the conclusion that the redistribution not only causes significant overhead but also hides important data for debugging solver convergence. In the present work a second approach is used, that retains boundary values and adapts the right hand side accordingly. This approach has proven to be more efficient with the drawback of memory overhead and the need to reset the boundary values after a linear system has been solved with a high relative tolerance.

This simple indexing model is not capable to handle neither block structured grids nor grids that have been distributed across various processors within the MPI programming model. This characteristic is implemented through the use of additional mappings that return a constant offset  $(ijk)_b$  for each block and  $(ijk)_p$  for each processor

$$(ijk) = (ijk)_p + (ijk)_b + N_i N_j (k - 1) + N_j (i - 1) + j.$$

The introduction of the processor offset is needed to provide a mapping between locally and globally indexed values. Within a process only the local indexing

$$(ijk)_{loc} = (ijk)_b + N_i N_j (k - 1) + N_j (i - 1) + j.$$

will be used, since these indexes can be mapped directly to memory addresses. For inter process communication however, global indices have to be provided to the respective PETSc subroutines by adding the processor offset

$$(ijk)_{glo} = (ijk)_{loc} + (ijk)_p. \quad (47)$$

It should be noted that the presented mappings do not include the index mappings from FORTRAN applications, which use 1-based indexing, to the PETSc subroutines which use 0-based indices.

As presented in section 5, the use of a coupling algorithm leads to a global linear system that contains the linear algebraic equations for different variables. The implementation used for the present thesis interlaces this values, which increases data locality and hence improves memory efficiency. The presented mapping is easily extended to handle arrays of values that contain  $n_{eq}$  variables and use an interlaced storing approach by multiplying (48) with the number of interlaced values

$$(ijk)_{interglo} = n_{eq} * ((ijk)_{glo} - 1) + c_{eq},$$

where  $c_{eq} = 1, \dots, n_{eq}$ .

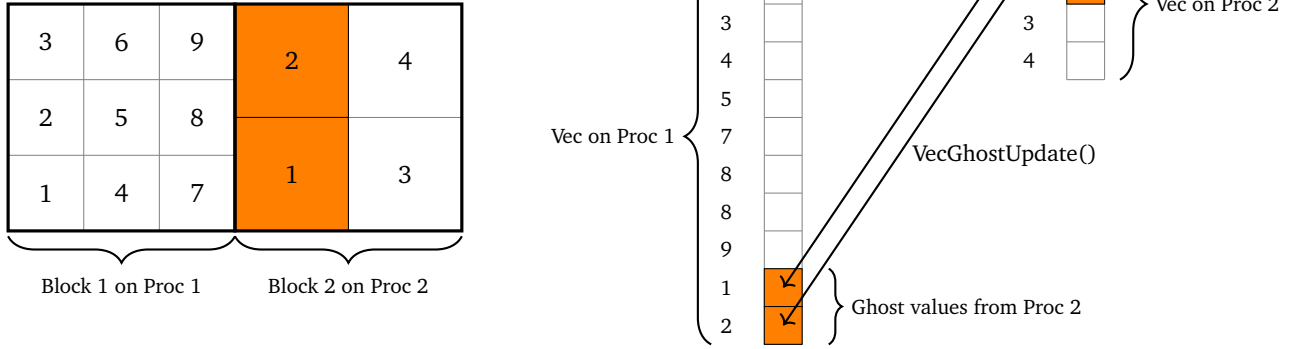
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### 6.3.4 Domain Decomposition, Exchange of Ghost Values and Parallel Matrix Assembly

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The developed CAFFA framework is able to solve a given problem across different processors. For this, before each solve, the relevant data has to be distributed among all involved processes. Within the solver parallelization three types of this data distribution are considered with respect to their frequency of communication and redistribution among all or only a part of the processes involved in the solution process.

The first type of data refers to the distribution of stationary data that will not change throughout the solution process. This refers mostly to geometry related data as the coordinates of the grid points. The distribution of the data is already part of the domain composition process and hence can be done even before the solver starts as it is implemented in the developed solver framework. It should be noted that in the case that local dynamic refinement strategies are used the geometric data at block boundaries has to be redistributed. If additionally dynamic load balancing is used even geometric data from the inside of the problem domain might be redistributed. This however imposes other design guidelines for the involved processes which is not inside the scope of the present thesis.



**Figure 9:** Storage and update of ghost values related to variables on multi block domains

The distribution of stationary data takes place throughout the preprocessing program within the developed framework before the CAFFA solver is launched. Each processor is assigned a binary file with the respective data. Since the solver is not able to handle adaptive grid refinement or dynamic load balancing this approach is straightforward.

The second type of data has to be distributed in a regularly since this data changes at least every outer iteration. The necessity to interchange values, also known as *ghosting*, between processors surges when calculations of variable gradients or coefficients are made for block boundary control volumes. PETSc provides special interfaces for ghosted vectors that allow to perform different types of vector updates through top-level subroutines. The central part are the involved vector scatter and gather routines which allow to calculate contributions to source terms of control volumes located at block boundaries accurately or update ghost values for the control volumes that rely on variable values from neighbouring blocks to calculate fluxes or gradients. It should be noted that the modelling approach for ghosting values is not symmetric in the sense that each block saves ghost values of the neighbouring blocks. On the contrary, for each block boundary only one of the neighbored blocks is responsible for the calculation of the fluxes and gradient contributions. This maintains the same amount of data communicated through the interconnect while almost splitting the computational effort into half.

Another advantage of the PETSc environment for ghosting values that reside in the memory space of other processes is the unified approach of data coherence, since on the top level only one vector object to store all data related to a variable, e.g. the velocity  $u_1$ , has to be created. Through precise information provided in the creation step of these vector objects, PETSc distributes the vector object to all involved processes and uses the provided information to realize ghosting through the internal vector scatter and gather routines.

The present solver framework treats the calculation of matrix coefficients for block boundary control volumes in a special way. To reduce communication overhead and redundant data only one of the two involved processors calculates this coefficients and then sends them to the respective neighbour. The data needed to calculate the matrix coefficients of a neighbouring processor embraces not only the values of the dominant variables from the last outer iteration but also the values of the cell center gradients. For the ghosting of variable values PETSc offers special vector types, that comprise a user friendly interface to use the gather and scatter routines provided by PETSc. During the creation of these vectors a set of global indices referring to the values that are to be ghosted has to be provided. After this, the interchange of values is realized through a single subroutine call to `VecGhostUpdate`, since PETSc handles the concrete communication process necessary to accomplish the value interchange. The local representation of a ghosted vector hence not only comprises the data local to one processor but provides space for ghosted values that are repeatedly updated. The parallel vector layout and the process of ghosting are schematically shown in figure 9 for a two dimensional domain consisting of two grid blocks.

The last type of data distribution refers to global reduce operations, in which a single processes gathers data from all other processes and after some modification redistributes the data. A common scenario for global reduce operations is the calculation of the mean pressure throughout the domain which has been introduced in section 4.8.

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## 7 Verification of the developed CAFFA Framework

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The systematical verification of program code is an essential part of the development process of software for scientific calculations, since it insures that the respective equations are solved correctly [60]. Scientific applications that solve partial differential equations can be verified using the method of manufactured solutions [67]. In addition, the method of manufactured solutions will be used to proof that both solvers within the developed framework, namely the segregated and the fully coupled solver, use the same discretization of the underlying partial differential equations. Before the performance of the developed CAFFA framework will be discussed in section ??, this section presents the results of the verification process performed in the present work via the *Method of Manufactured Solutions*. After mentioning the main aspects of this procedure, this section will furthermore present the theoretical discretization error of the finite-volume method as it is applied in the present thesis. The subsections that follow will then present a concrete manufactured solution and the results of using it in the verification process.

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### 7.1 The Method of Manufactured Solutions for Navier-Stokes Equations

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The method of manufactured solutions comprises a systematical, formal procedure for code verification based on analytical solutions of the partial differential equations to be solved [67]. Using this analytical solutions the accuracy of the produced results can be assessed and, after the establishment of an acceptance criterion, used to verify the computer program. A common acceptance criterion is the *Order-of-Accuracy* criterion, since in addition to the formal order of accuracy of a developed solver algorithm it verifies its consistency. It should be noted that by the method of manufactured solutions it is not possible to detect errors in the physical model.

The basic idea of the method of manufactured solutions is the inversion of the solution process of partial differential equations. Instead of trying to find the solution  $x$  to a given equation  $F(x) = b$  with source term  $b$ , a solution  $x$  is *manufactured* and the source term is constructed by applying  $F$  to  $x$ . This has the advantage of choosing a solution that exercises all parts of the solution process and hence provides a thorough testing environment. On the downside the integration of boundary conditions other than Dirichlet boundary conditions REFERENCE might be challenging. Furthermore the program code has to be able to handle arbitrary source terms.

The different guidelines that have to be followed in order to apply the method of manufactured solutions successfully, can be found in [67]. According to the reference, manufactured solutions should be composed of infinitely often differentiable analytic functions whose derivatives are bounded by small constants. Furthermore the solution domain should not be chosen to be symmetric, but as arbitrary as possible within the limitations of the code. This may however conflict with the application of the method of manufactured solutions to verify a code to solve the Navier-Stokes equations. Subsection 7.2 presents the manufactured solution including the resulting source terms for the set of partial differential equations (8).

The verification of a solver for incompressible Navier-Stokes equations comes with additional conditions, that have to be considered: First, if the solver is not able to handle source terms in the continuity equation and respectively the pressure correction equation, a velocity field should be chosen that is inherently divergence free. This can be achieved by defining the velocity field  $\mathbf{u}$  through the curl of a vector field  $\Psi$  as

$$\mathbf{u} = \nabla \times \Psi.$$

Using the property that the divergence of the rotation of a vector field vanishes, one gets

$$\nabla \cdot \mathbf{u} = \nabla \cdot (\nabla \times \Psi) = 0,$$

i.e. a locally divergence free velocity field, which implies that globally the continuity equation also is fulfilled in an integral sense for arbitrary domains of integration. This is not necessarily true in the discrete sense as integrals are to be approximated by, in the case of the present thesis, the midpoint rule of integration, as shown in subsection 3.2. In the general case for arbitrary solution domains global mass conservation cannot be guaranteed even though the integrands are exact quantities at the domain boundaries. Thus in the case of finding manufactured solutions the problem domain should be fixed before manufacturing a solution. The velocity field for the manufactured solution should then either vanish on the domain boundaries, which is the case of the commonly used Taylor-Green vortex [76], or should exhibit further symmetry that leads to cancelling non-zero mass fluxes across the domain boundaries. The studies performed within the scope of the present showed, that convergence of the pressure correction equation can no longer be guaranteed if the velocity field does not obey continuity in the discrete sense at the domain boundaries.

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### 7.2 Manufactured Solution for the Navier-Stokes Equations and the Temperature Equation

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This subsection presents the manufactured solution for the system of partial differential equations (8). The manufactured solutions and the computations needed to derive the respective source terms were performed by the computer algebra

system Maple ® [53]. After the computation the terms were directly translated into FORTRAN source code, such that the manufactured solution could be directly integrated into the solver framework. In the following paragraphs the used solutions for the velocity vector  $(u_1, u_2, u_3)$ , the pressure  $p$  and the temperature  $T$  will be formulated. The manufactured solution for the velocities was formulated as

$$\begin{aligned}u_1 &= 2 \cos(x_1^2 + x_2^2 + x_3^2) x_2 + 2 \sin(x_1^2 + x_2^2 + x_3^2) x_3 \\u_2 &= 2 \cos(x_1^2 + x_2^2 + x_3^2) x_3 - 2 \cos(x_1^2 + x_2^2 + x_3^2) x_1 \\u_3 &= -2 \sin(x_1^2 + x_2^2 + x_3^2) x_1 - 2 \cos(x_1^2 + x_2^2 + x_3^2) x_2.\end{aligned}$$

The manufactured solution for the pressure  $p$  was created as

$$p = \sin(x_1^2 + x_2^2 + x_3^2) \cos(x_1^2 + x_2^2 + x_3^2).$$

Since the velocity field was created as a solenoidal field no pressure source had to be calculated. The manufactured solution for the temperature  $T$  reads

$$T = \sin(x_1^2) \cos(x_2^2) \sin(x_3^2).$$

The resulting source terms for the momentum balances read

$$\begin{aligned}b_1 &= 8 \cos(x_1^2 + x_2^2 + x_3^2) x_1^2 x_2 + 8 \cos(x_1^2 + x_2^2 + x_3^2) x_2^3 + 8 \cos(x_1^2 + x_2^2 + x_3^2) x_3^2 x_2 \\&\quad + 8 \sin(x_1^2 + x_2^2 + x_3^2) x_1^2 x_3 + 8 \sin(x_1^2 + x_2^2 + x_3^2) x_2^2 x_3 + 8 \sin(x_1^2 + x_2^2 + x_3^2) x_3^3 \\&\quad + 7 \sin(x_1^2) \cos(x_2^2) \sin(x_3^2) + 4 (\cos(x_1^2 + x_2^2 + x_3^2))^2 x_1 + 4 (\cos(x_1^2 + x_2^2 + x_3^2))^2 x_3 \\&\quad - 4 \cos(x_1^2 + x_2^2 + x_3^2) \sin(x_1^2 + x_2^2 + x_3^2) x_2 - 20 \cos(x_1^2 + x_2^2 + x_3^2) x_3 + 20 \sin(x_1^2 + x_2^2 + x_3^2) x_2 - 6 x_1 \\b_2 &= -8 \cos(x_1^2 + x_2^2 + x_3^2) x_1^3 + 8 \cos(x_1^2 + x_2^2 + x_3^2) x_1^2 x_3 - 8 \cos(x_1^2 + x_2^2 + x_3^2) x_2^2 x_1 \\&\quad - 8 \cos(x_1^2 + x_2^2 + x_3^2) x_3^2 x_1 + 8 \cos(x_1^2 + x_2^2 + x_3^2) x_2^2 x_3 + 8 \cos(x_1^2 + x_2^2 + x_3^2) x_3^3 \\&\quad + 13 \sin(x_1^2) \cos(x_2^2) \sin(x_3^2) - 4 (\cos(x_1^2 + x_2^2 + x_3^2))^2 x_2 - 4 \cos(x_1^2 + x_2^2 + x_3^2) \sin(x_1^2 + x_2^2 + x_3^2) x_1 \\&\quad - 4 \cos(x_1^2 + x_2^2 + x_3^2) \sin(x_1^2 + x_2^2 + x_3^2) x_3 - 20 \sin(x_1^2 + x_2^2 + x_3^2) x_1 + 20 \sin(x_1^2 + x_2^2 + x_3^2) x_3 - 2 x_2 \\b_3 &= -8 \cos(x_1^2 + x_2^2 + x_3^2) x_1^2 x_2 - 8 \cos(x_1^2 + x_2^2 + x_3^2) x_2^3 - 8 \cos(x_1^2 + x_2^2 + x_3^2) x_3^2 x_2 \\&\quad - 8 \sin(x_1^2 + x_2^2 + x_3^2) x_1^3 - 8 \sin(x_1^2 + x_2^2 + x_3^2) x_2^2 x_1 - 8 \sin(x_1^2 + x_2^2 + x_3^2) x_3^2 x_1 \\&\quad - 19 \sin(x_1^2) \cos(x_2^2) \sin(x_3^2) + 4 (\cos(x_1^2 + x_2^2 + x_3^2))^2 x_1 + 4 (\cos(x_1^2 + x_2^2 + x_3^2))^2 x_3 \\&\quad - 4 \cos(x_1^2 + x_2^2 + x_3^2) \sin(x_1^2 + x_2^2 + x_3^2) x_2 + 20 \cos(x_1^2 + x_2^2 + x_3^2) x_1 - 20 \sin(x_1^2 + x_2^2 + x_3^2) x_2 - 6 x_3.\end{aligned}$$

Finally the source term for the temperature equation was calculated as

$$\begin{aligned}b_T &= -4 \sin(x_1^2) \cos(x_2^2) \cos(x_3^2) \cos(x_1^2 + x_2^2 + x_3^2) x_2 x_3 - 4 \sin(x_1^2) \cos(x_2^2) \cos(x_3^2) \sin(x_1^2 + x_2^2 + x_3^2) x_1 x_3 \\&\quad + 4 \sin(x_1^2) \sin(x_3^2) \sin(x_2^2) \cos(x_1^2 + x_2^2 + x_3^2) x_1 x_2 - 4 \sin(x_1^2) \sin(x_3^2) \sin(x_2^2) \cos(x_1^2 + x_2^2 + x_3^2) x_2 x_3 \\&\quad + 4 \cos(x_2^2) \sin(x_3^2) \cos(x_1^2) \cos(x_1^2 + x_2^2 + x_3^2) x_1 x_2 + 4 \cos(x_2^2) \sin(x_3^2) \cos(x_1^2) \sin(x_1^2 + x_2^2 + x_3^2) x_1 x_3 \\&\quad + 4 x_1^2 \sin(x_1^2) \cos(x_2^2) \sin(x_3^2) + 4 \sin(x_1^2) \cos(x_2^2) x_2^2 \sin(x_3^2) \\&\quad + 4 x_3^2 \sin(x_1^2) \cos(x_2^2) \sin(x_3^2) - 2 \sin(x_1^2) \cos(x_2^2) \cos(x_3^2) \\&\quad + 2 \sin(x_1^2) \sin(x_3^2) \sin(x_2^2) - 2 \cos(x_2^2) \sin(x_3^2) \cos(x_1^2).\end{aligned}$$



---

### 7.3 Measurement of Error and Calculation of Order

---

In this subsection the result of the verification process via the formerly in subsection 7.2 stated manufactured solutions will be presented. To verify the solver framework using the Order-of-Accuracy test criterion an error measure has to be chosen on which the evaluation is based upon. According to [67] the error measure for each variable  $\phi$  will be calculated at the end of each computation as the normalized  $L_2$ -norm of the deviation of the exact solution  $\tilde{\phi}$ , sometimes referred to as the normalized global error or the RMS error

$$\text{err}(\phi) = \sqrt{\frac{\iiint_V (\phi - \tilde{\phi})^2 dV}{\iiint_V dV}} \approx \sqrt{\frac{\sum_{n=1}^N (\phi_n - \tilde{\phi}_n)^2 V_n}{\sum_{n=1}^N V_n}}.$$

Herein  $N$  denotes the number of control volumes of the discretized solution domain  $V$ . Each control volume has the volume  $V_n$ . The numerical and the exact solution are evaluated at the center of each control volume for the error calculations. In order to calculate the normalized global error of the pressure  $p$  the same modification as in subsection 4.8 has to be performed on the analytical solution  $\tilde{p}$ , which in the case of the present work means to subtract the weighted mean value

$$\text{mean}(\tilde{p}) = \frac{\iiint_V \tilde{p} dV}{\iiint_V dV} \approx \frac{\sum_{n=1}^N \tilde{p}_n V_n}{\sum_{n=1}^N V_n}$$

from it and to calculate the error as

$$\text{err}(p, N) \approx \sqrt{\frac{\sum_{n=1}^N (p_n - \tilde{p}_n - \text{mean}(\tilde{p}))^2 V_n}{\sum_{n=1}^N V_n}}.$$

The following tables will list the calculated error terms for the velocities, the pressure and the temperature for different grid resolutions and both solver algorithms. The grid resolutions ( $n \times n \times n$ ) are chosen such that  $n$ , the number of control volumes in each coordinate direction, will be a power of two. The Errors were evaluated after the maximal relative residual of all linear systems in one outer iteration fell below the threshold  $1 \times 10^{-14}$ . The concrete implementation of the tolerance criterion to accept a converged solution is found in section 6.3.2.

A comparison of the results leads to the first conclusion, namely that the results from the segregated solver algorithm and the coupled solver algorithm coincide which implies that the same discretization is used in both cases. According to [67] the next step comprises the calculation of the formal order of accuracy  $\hat{p}_\phi$  for each variable that the program solves for. This can be done by evaluating the quotient of two different resolutions  $n1$  and  $n2$  as

$$\hat{p}_\phi = \frac{\log\left(\frac{\text{err}(\phi, n1)}{\text{err}(\phi, n2)}\right)}{\log\left(\frac{n1}{n2}\right)}.$$

The discretization techniques used in the present thesis yield an asymptotic discretization error of two [?]. Comparing with the results in the tables 1, 2 and 3 shows the asymptotic behavior of the calculated order which leads to the conclusion that the discretization has been implemented with success.

---

### 7.4 Influence of the Under-Relaxation Factor for the Velocities

---

In section ?? the main purpose of introducing the pressure weighted interpolation method was to assure comparability of the generated results from the segregated solver algorithm and the coupled solver algorithm. Section ?? showed good agreement of the error calculated with the segregated solver using the pressure weighted interpolation method and the coupled solver. This section presents the results that are attained if the standard Rhie-Chow interpolation technique with different under-relaxation factors  $\alpha_u$  is used to interpolate the velocities to the boundary faces instead of the pressure weighted interpolation technique. Figure 10 shows the normalized  $L_2$  norm of the error of the results for the velocity  $u_1$  for different under-relaxation factors. The  $L_2$  norms have been normalized by the  $L_2$  norm of the respective calculation that uses the pressure weighted interpolation method.

It is evident that the higher the under-relaxation factor the smaller the deviation of the results obtained with the standard Rhie-Chow interpolation technique from the results obtained with the pressure weighted interpolation method. This can be justified by the fact that, for an under-relaxation factor  $\alpha_u = 1$ , the pressure weighted interpolation and the

**Table 1:** Comparison of the errors of the velocity calculated by the segregated and the coupled solver for different grid resolutions and the resulting order of accuracy

Resolution	Error of $\mathbf{u}$ from Segregated Solver	Error of $\mathbf{u}$ from Coupled Solver	Observed Order $\hat{p}$
8x8x8	3.170450230115786E-002	3.1704502290288525E-002	
	3.037011030746674E-002	3.0370110306195783E-002	
	3.163609515028456E-002	3.1636095141306442E-002	
16x16x16	7.914356673006179E-003	7.9143566730065350E-003	2.0021
	7.534314612440339E-003	7.5343146124409056E-003	2.0111
	7.811316741535871E-003	7.8113167415361021E-003	2.0179
32x32x32	1.933302886747634E-003	1.9333250814097063E-003	2.0334
	1.867599197138540E-003	1.8676512523175990E-003	2.0123
	1.894813910088982E-003	1.8948223205995562E-003	2.0435
64x64x64	4.746894199493598E-004	4.7468942001527124E-004	2.0260
	4.629259933395594E-004	4.6292599348776502E-004	2.0123
	4.630008203550293E-004	4.6300082038027822E-004	2.0330
128x128x128	1.172266972290949E-004		2.0177
	1.150024026498247E-004		2.0091
	1.140471182846354E-004		2.0214
256x256x256	2.876932445431025E-005		2.0267
	2.771472789328757E-005		2.0529
	2.826736500332136E-005		2.0124

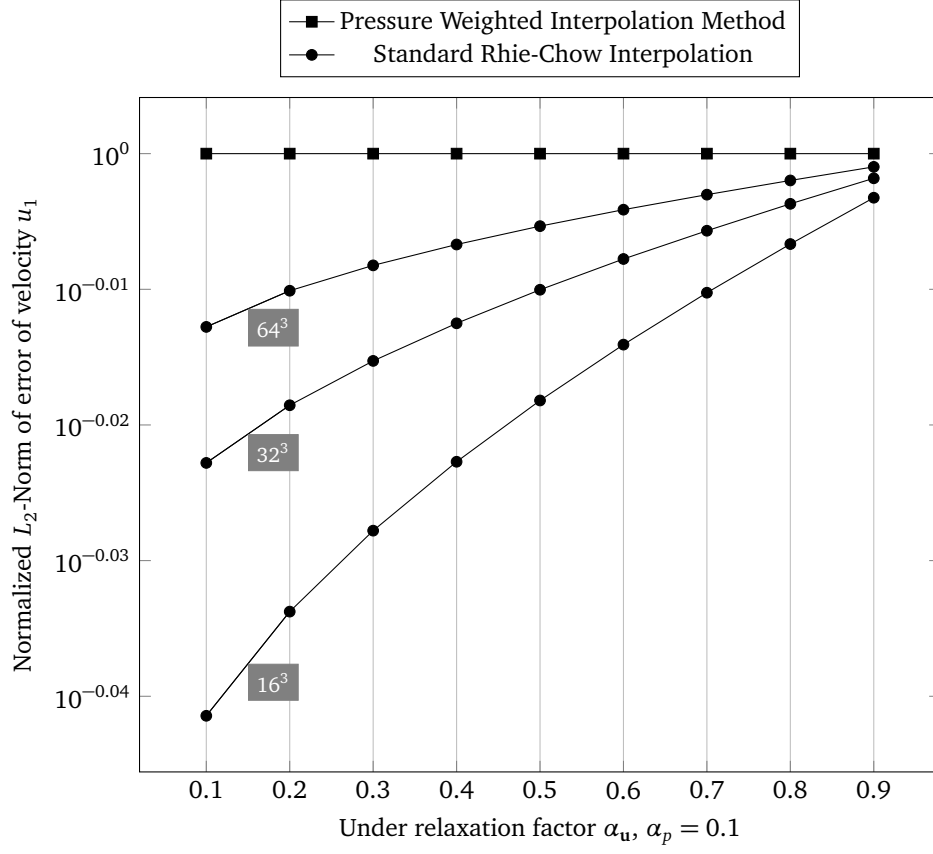
**Table 2:** Comparison of the errors of the pressure calculated by the segregated and the coupled solver for different grid resolutions and the resulting order of accuracy

Resolution	Error of $p$ from Segregated Solver	Error of $p$ from Coupled Solver	Observed Order $\hat{p}$
8x8x8	0.183035893121686	0.1830358946646808	
16x16x16	8.967727683983406E-002	8.9677276839825765E-002	1.0293
32x32x32	3.796485688816108E-002	3.7964815814009345E-002	1.2401
64x64x64	1.438780100622541E-002	1.4387801006156546E-002	1.3998
128x128x128	5.160705648852031E-003		1.4792
256x256x256	1.809811107444374E-003		1.5117

**Table 3:** Comparison of the errors of the temperature calculated by the segregated and the coupled solver for different grid resolutions and the resulting order of accuracy

Resolution	Error of $T$ from Segregated Solver	Error of $T$ from Coupled Solver	Observed Order $\hat{p}$
8x8x8	4.067532377541200E-003	4.0675323775378296E-003	
16x16x16	1.132477318394773E-003	1.1324773183947821E-003	1.8447
32x32x32	2.931009801582052E-004	2.9310096243402903E-004	1.9500
64x64x64	7.410021974469997E-005	7.4100219743344219E-005	1.9838
128x128x128	1.858846421984987E-005		1.9951
256x256x256	4.651911366447223E-006		1.9985





**Figure 10:** Comparison of calculated error for different under relaxation factors  $\alpha_u$  on a grid with different grid resolutions unknowns

Rhie-Chow interpolation would yield the same result according to equation (18). Furthermore it can be observed that the deviation decreases with increasing mesh resolution which is the expected behaviour [28].

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## 8 Comparison of Solver Concepts

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This section conducts the performance analysis of both developed solvers. In the first part of this section the used hardware and software are described, furthermore important performance measures are introduced. After performing a preliminary benchmark to measure the sustainable bandwidth the Speedup is measured for both solver programs. The second part of this section tests the performance of the algorithm on a test case with complex geometry and on the heated cavity benchmark.

---

### 8.1 Parallel Performance

---

In many cases, scientific code is used to solve complex problems regarding memory requirements or to make calculation results available within short time. In both scenarios, code that is able to run in parallel can alleviate the mentioned challenges. Code that runs in parallel can allocate more memory resources which makes the calculation of complex problems feasible. If the code is scalable the program execution can be shortened by involving more processes to solve a problem of constant size on the compatible hardware.

The solver framework that has been developed in the course of the present thesis, has been parallelized using the PETSc library. After introducing the used hardware and software, the central measures of parallel performance are presented. Then preliminary test results using low-level benchmarks are performed, which establish upper performance bounds on the parallel efficiency and the scalability of the developed solver framework. The results of the efficiency evaluation of the solver framework are presented in the last subsections.

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#### 8.1.1 Employed Hardware and Software – The Lichtenberg-High Performance Computer

---

All performance analyses that are presented in this thesis were conducted on the Lichtenberg-High Performance Computer, also known as *HHLR (Hessischer Hochleistungsrechner)* [1]. The cluster consist of different sections according to the used hardware. Throughout the thesis, tests were performed using the first and the second MPI section of the cluster. The first section consists of 705 nodes of which each runs two Intel®Xeon®E5-2670 processors and offers 32GB of memory. The second section consists of 356 nodes of which each runs two Intel Xeon E5-2680 v3 processors and offers 64GB of memory. As interconnect for both sections FDR-14 InfiniBand is used.

All tests programs were compiled using the Intel compiler suite version 15.0.0 and the compiler options

`—O3 —xHost`

As MPI implementation Open MPI version 1.8.2 was chosen. Furthermore the PETSc version 3.5.3 was configured using the options

```
—with-blas-lapack-dir=/shared/apps/intel/2015/composer_xe_2015/mkl/lib/intel64/ \
—with-mpi-dir=/shared/apps/openmpi/1.8.2_intel \
COPTFLAGS="—O3 —xHost" \
FOPTFLAGS="—O3 —xHost" \
CXXOPTFLAGS="—O3 —xHost" \
—with-debugging=0 \
—download-hypre \
—download-ml
```

It should be noted that as the configurations options show, to maximize the efficiency of PETSc, a math kernel library should be used that has been optimized for the underlying hardware architecture as is in the case of the present thesis the Intel *MKL (Math Kernel Library)*. The Open MPI library was compiled using Intel compilers as well.

---

#### 8.1.2 Measures of Performance

---

This section establishes the needed set of measures to evaluate the performance of a solver program, which will be used in the following sections. The first measure is the plain measure of runtime  $T_p$  taken by a computer to solve a given problem, where  $P \in \mathbb{N}$  denotes the number of involved processes. This so called *wall-clock* time can be measured directly by calling subroutines of the underlying operating system and corresponds to the human perception of the time, that has passed. It must be noted, that this time does not correspond to the often mentioned *CPU* time. In fact, CPU time is only one contributor to wall-clock time. Wall-clock time further contains the time needed for communication and I/O and hence considers idle states of the processor. On the other side CPU time only considers the time in which the processor is actively working. This makes wall-clock time not only a more complete but also more accurate time measure when dealing with parallel processors, since processor idle times due to communication are actively considered while neglected in CPU time.

While wall-clock time is an absolute measure that can be used to compare different solver programs, further relative measures are needed to evaluate the efficiency of one program regarding the parallelisation implementation. The main

purpose of these measures is to attribute the different causes of degrading efficiency due to heavy parallelisation to the different contributing factors. A simple model [28, 68] considers three contributions, that form the total efficiency

$$E_p^{tot} = E_p^{num} \cdot E_p^{par} \cdot E_p^{load}.$$

The *numerical efficiency*

$$E_p^{num} := \frac{\text{FLOPS}(1)}{P \cdot \text{FLOPS}(P)}$$

considers the degradation of the efficiency of the underlying algorithm due to the parallelisation. Many efficient algorithms owe their efficiency to recursions inside the algorithm. In the process of decomposing this recursions, the efficiency of the algorithm degrades. It follows that this efficiency is completely independent of the underlying hardware.

The *parallel efficiency*

$$E_p^{par} := \frac{\text{TIME}(\text{parallel Algorithm on one processor})}{P \cdot \text{TIME}(\text{parallel Algorithm on } P \text{ processors})}$$

describes the impact of the need for inter process communication, if more than one processor is involved in the solution process. It should be noted, that this form of efficiency does explicitly exclude any algorithm related degrading, since the time measured corresponds to the exact same algorithms. It follows that the parallel efficiency only depends on the implementation of the communication and the hardware related latencies.

The *load balancing efficiency*

$$E_p^{load} := \frac{\text{TIME}(\text{calculation on complete domain})}{P \cdot \text{TIME}(\text{calculation on biggest subdomain})}$$

is formed by the quotient of the wall times needed for the complete problem domain and partial solves on subdomains. This measure does neither depend on hardware nor on the used implementation. Instead it directly relates to the size and partition of the grid.

It is not possible to calculate all three efficiencies at the same time using only plain wall-clock time measurements of a given application. Different solver configurations have to be used to calculate them separately. Since the focus of investigation of the present thesis does not lie on load balancing, for the remainder of the thesis  $E_p^{load} = 100\%$  is assumed. This does not present a considerable drawback, since an ideal load balancing is easily obtainable nowadays by the use of sophisticated grid partitioning algorithms [?] REFERENCES. Using identical algorithms for different numbers of involved processes implicitly achieves  $E_p^{num} = 100\%$ . In this case the parallel efficiency of an application can be measured through the quotient of the needed wall-clock time. To measure the numerical efficiency of an algorithm the respective hardware counters have to be evaluated. This can be done using the built in log file functionality of PETSc as presented in section REFERENCE. Hence the determination of numerical efficiency does not rely on wall-clock time.

Another common performance measure is the *Speed-Up*

$$S_p = \frac{T_1}{T_p} = P \cdot E_p^{tot}.$$

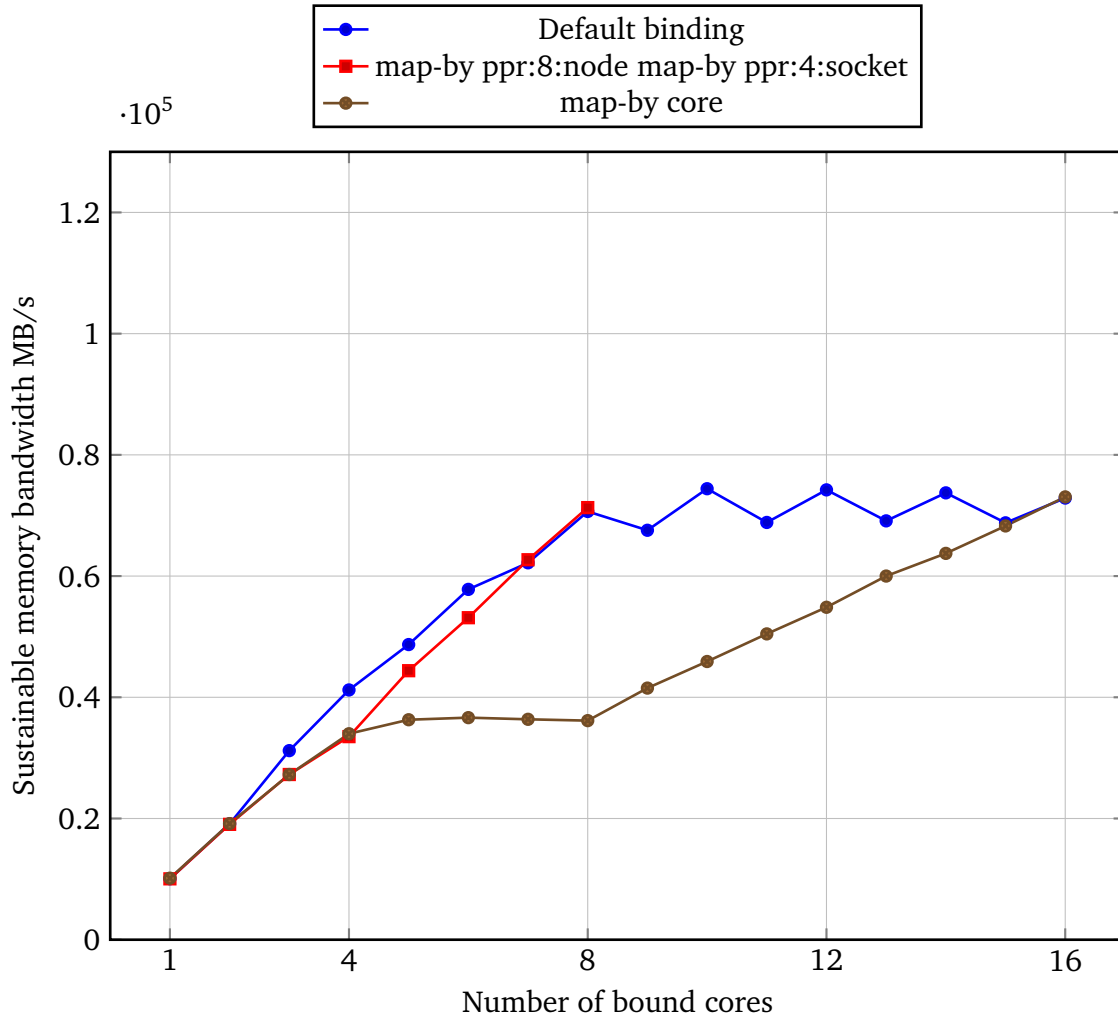
Speedup and parallel efficiency characterize the parallel scalability of an application and determine the regimes of efficient use of hardware resources.

---

### 8.1.3 Preliminary Upper Bounds on Performance – The STREAM Benchmark

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Scientific applications that solve partial differential equations rely on sparse matrix computations, which usually exhibit the sustainable memory bandwidth as bottleneck with respect to the runtime performance of the program [37]. The purpose of this section is to establish a frame in terms of an upper bound on performance in which the efficiency of the developed solver framework can be evaluated critically. As common measure for the maximum sustainable bandwidth, low-level benchmarks can be used, which focus on evaluating specific properties of the deployed hardware architecture. In this case the STREAM benchmark suite [55, 56] provides apt tests, which are designed to work with data sets that exceed the cache size of the involved processor architecture. This forces the processors to stream the needed data directly from memory instead of reusing the data residing in their caches. These types of tests can be used to calculate an upper bound on the memory bandwidth for the CAFFA framework.

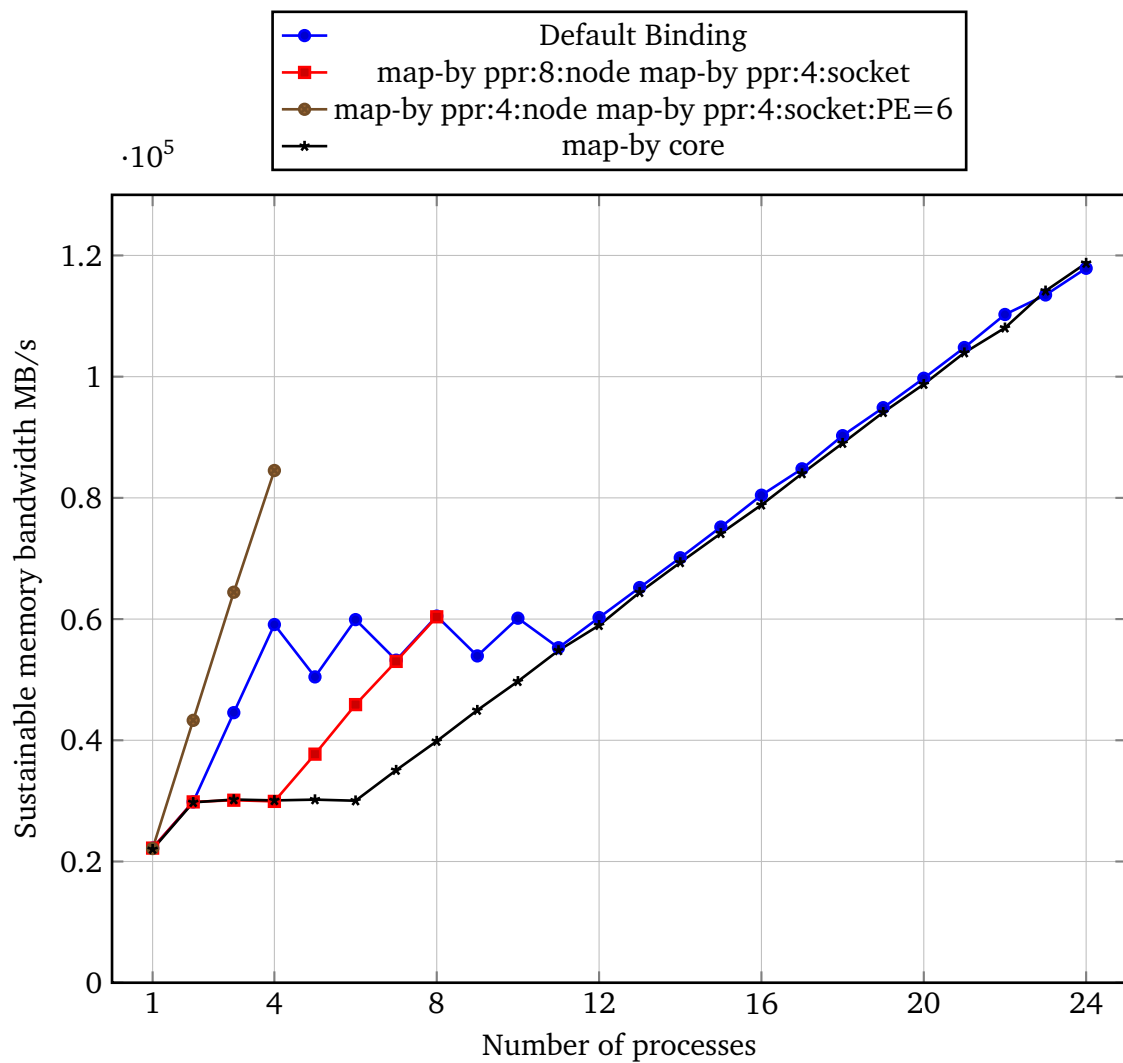


**Figure 11:** Sustainable memory bandwidth as determined by the STREAM benchmark (Triad) for different process binding options on one node of the MPI1 section

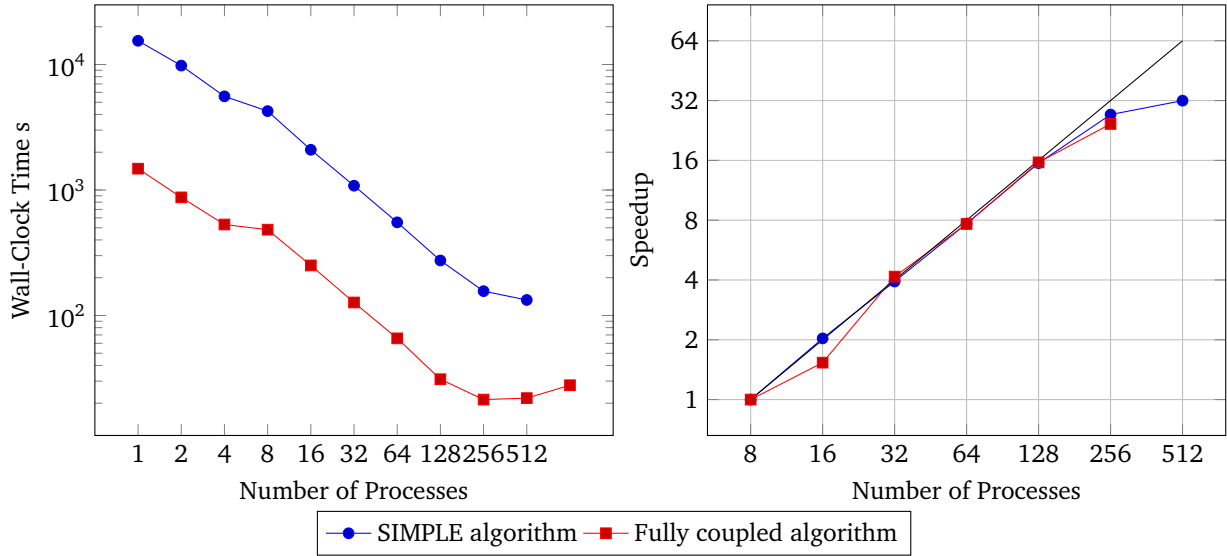
In terms of parallel scalability, the STREAM benchmark can also be used as an upper performance bound. According to [8] the parallel performance of memory bandwidth limited codes correlates with the parallel performance of the STREAM benchmark, i.e. a scalable increase in memory bandwidth is necessary for scalable application performance. The intermediate results of the benchmark can then be used to test different configurations that bind hardware resources to the involved processes. Figures ?? and ?? show the test results of the STREAM benchmark on the two different sections of the HHRL. It should be noted that it is central for the results to be reproducible to always run the tests exclusively on each node, i.e. that no other process is running on the node.

As can be seen from figure 11 and 12, the scaling of the sustainable bandwidth behaves rather erratic, such that for process counts up until eight for the MPI1 section no reliable results can be obtained from the STREAM benchmark. It is assumed that this kind of behaviour is due to the automatic turbo boost the deployed processors apply, which cannot be controlled other than by turning it off directly from the nodes BIOS. For the following performance analyses with respect to parallel performance it is desirable to minimize this kind of unpredictable side effects. Since all performance measures are relative but the plain measurement of wall-clock time, the reference value for the following performance measurements will be taken from the program execution for the maximum number of processes that can be bound without overlap to one deployed socket.

It should be taken into account that the STREAM benchmark used to test the present architecture was provided by the PETSc framework. Special effort has been made to adapt this benchmark to handle the described problem, by always using all available cores per socket but only running the benchmark on  $n$  processes while the other  $24 - n$  or  $16 - n$  processes run calculations that only use data from the L1 cache of their corresponding core. The intention of this approach was to regulate the turbo boost effects by keeping a constant load on the processors for different numbers of STREAM benchmark processes. However this approach didn't generate results different from figures 11 and 12.



**Figure 12:** Sustainable memory bandwidth as determined by the STREAM benchmark (Triad) for different process binding options on one node of the MPI2 section



**Figure 13:** Speedup comparison for segregated and fully-coupled solution algorithm solving for an analytical solution on a grid with  $128^3$  cells

#### 8.1.4 Speedup Measurement and Impact of Coupling Algorithm for Analytic Test Case

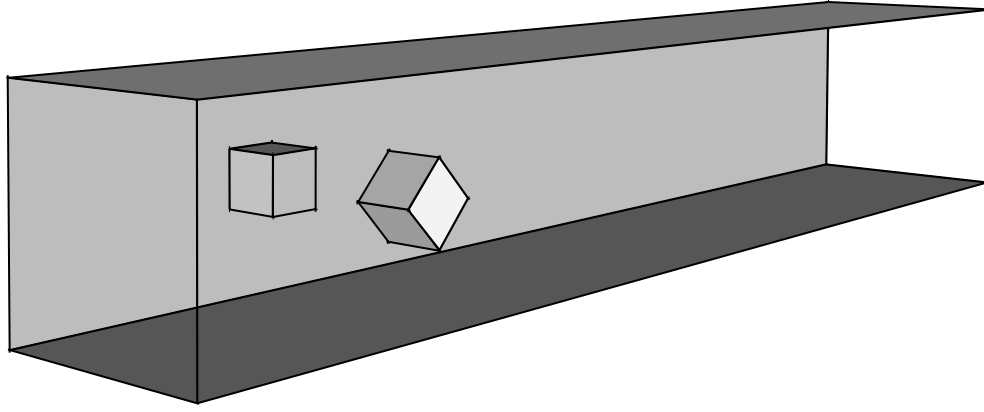
This section presents the results from the speedup measurements conducted on the supercomputer HHLR which has been presented in section 8.1.1. Furthermore the impact of the scaling algorithm on the running time of the corresponding solver program will be shown. All tests are conducted on the previously introduced HHLR cluster using the MPI1 and MEM2 section. The performance analyses will present the absolute time needed to solve for the flow of the analytical solution presented in section 7.2. In order to evaluate the parallel performance furthermore the speedup will be calculated based on the presented results.

The performance of all solvers significantly depends on the performance of the linear solvers and the corresponding preconditioners used in the solution process. For all conducted tests the linear system for the discretized momentum balances will be solved with a GMRES (*Generalized Minimal Residual*) [?] Krylov subspace solver and an incomplete LU-factorization as preconditioner. The pressure correction equation is solved by a CG (*Conjugated Gradient*) solver with GAMG (*Geometric Algebraic Multi Grid*) preconditioner. The coupled systems are solved by a GMRES Krylov subspace solver with GAMG preconditioning. The GAMG preconditioner was chosen so that a high numerical efficiency is obtained, constituting a basis for further parallel performance measurements based on plain wall-clock time measurements. All further solver parameters are listed in table 4.

Property	Value	Unit
Density	1E-0	$kg/m^3$
Viscosity	1E-0	$Ns/m^2$
Under relaxation u	0.9	
Under relaxation p	0.1	
Relative tolerance	1E-8/1E-4	

**Table 4:** Characteristic problem properties used in the performance measurements solving for an analytic solution

From the comparison in figures ?? and 13 it is evident that both algorithms are scalable and the coupled solution algorithm accelerates the solution process up to one order of magnitude. It has to be noted, that the presented results for the coupled solution algorithm were obtained using black-box solvers from the PETSc framework. It is assumed that the performance of the coupled solution algorithm with respect to the needed wall-clock time would benefit from multigrid solvers especially designed for the coupled system of linear equations. Examples for such special solvers can be found in [20, 46, 52]. Another approach is represented by *physics-based* solvers which take advantage of the matrix structure as shown in figure 8. References [12, 57] describe how PETSc can be used to construct physics based preconditioners.



**Figure 14:** Sketch of the channel flow problem domain

## 8.2 Realistic Testing Scenario – Complex Geometry

Fluid flow inside closed applications is a common situation in mechanical engineering. The flow through a channel with rectangular cross section can be seen as a simple test case that is a part of complex applications. This section compares the single process performance of the segregated and the fully coupled solution algorithm for a flow problem within a complex geometry. The geometry of the domain is based on a channel flow problem with square cross section, with the special property that inside the channel reside two obstacles with a square cross section of which one has been twisted against the other. Figure 14 shows a sketch of the problem domain.

This case exercises all of the previously introduced boundary conditions for flow problems including the treatment of non-matching block boundaries. For the velocities at the inflow boundary the parabolic distribution

$$\mathbf{u}(x_1, x_2, x_3) = \begin{bmatrix} u_1 \\ u_2 \\ u_3 \end{bmatrix} = \begin{bmatrix} \frac{16 * 0.45 * x_2 * x_3 * (0.41 - x_2) * (0.41 - x_3)}{0.41^4} \\ 0 \\ 0 \end{bmatrix}$$

was chosen. All the other problem parameters were chosen such that the flow problem resides in the regime of a non-turbulent stationary flow for which the presented solver framework has been developed. Table 5 lists the remaining material and geometrical characteristics of the test case.

**Table 5:** Characteristic problem properties used in the channel flow test case

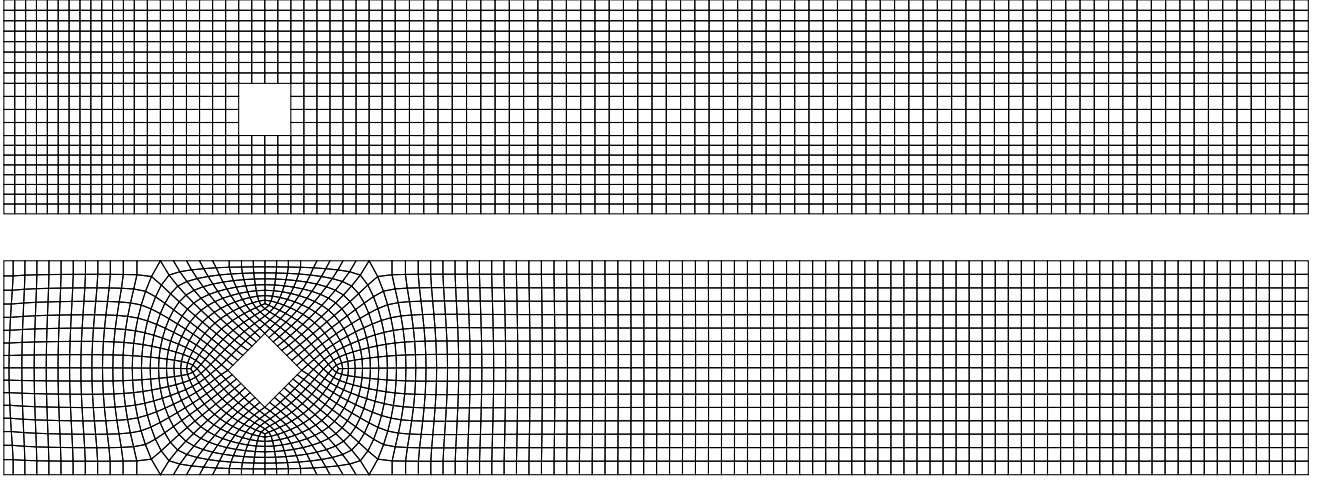
Property	Value	Unit
Density	1E-0	kg/m <sup>3</sup>
Viscosity	1E-3	Ns/m <sup>2</sup>
Height	0.41	m
Length	2.5	m
Side length cube	0.1	m
Under relaxation u	0.9	
Under relaxation p	0.1	

Using the data from table 5 and the maximal inflow velocity of 0.45m/s the Reynolds number  $Re$  can be calculated as

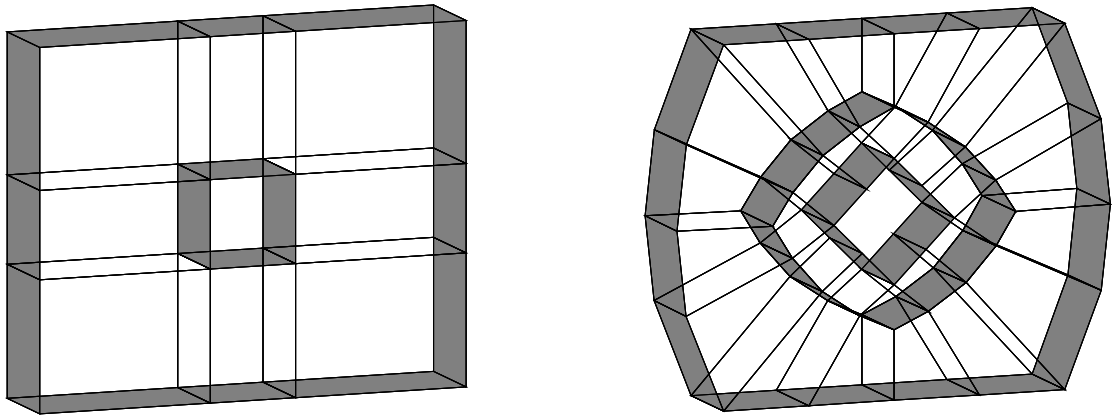
$$Re = \frac{\rho \text{mean}(u_1)l}{\mu} = 20,$$

where  $\text{mean}(u_1) = 0.45 * \frac{4}{9} \text{m/s} = 0.2 \text{m/s}$ . This shows that the flow resides in a laminar regime.

The present test case shows one advantage of the treatment of block boundaries, which has been introduced in section 4.7.3. Since no assumptions on the geometry of a neighboring block are necessary each block can be constructed indepen-



**Figure 15:** East boundary of the numerical grid for the channel flow problem



**Figure 16:** Blocking for the two different obstacles within the problem domain of the channel flow

dently which increases the flexibility of the meshing of geometries. Furthermore, because of the fully implicit handling of block boundaries, the number of used blocks does not impact on the convergence properties of the deployed linear solvers. Figure 15 shows the mesh at the left and right bounding walls. It is evident that this mesh leads to non-trivial transitions between the blocks. Figure 16 shows the domain decomposition into structured grid blocks around the two obstacles within the problem domain and emphasizes the need for accurate handling of non-matching block boundaries.

The solution of the linear systems resulting from the discretization of the problem takes up more time for the coupled solution algorithm than in the segregated coupled algorithm. For small problem sizes the additional overhead for the solution methods for linear systems and the property that the segregated solution algorithm does not need many outer iterations to converge leads to the conclusion that moderate to big problems with respect to the number of involved unknowns are necessary for the coupled solution algorithm to dominate through performance.

In contrast to the segregated algorithm, the fully coupled solution algorithm achieves an approximately constant amount of needed outer iterations, independent of the number of involved unknowns. The tests regarding the weak scaling of the coupled solution algorithm emphasize this property. Table 6 compares the measured wall-clock time for different numbers of unknowns. The mesh shown in figure 15 and was generated for the first number of unknowns and successively refined to achieve higher mesh resolutions. The two other numbers result from up to three times bisectioning the mesh in each direction, every time scaling the number of unknowns by a factor of approximately eight. The tests were conducted on the formerly presented HHLR cluster, using the MPI2 and MEM2 section.

The timing results show, that already after the first grid refinement step the fully coupled solution algorithm performs better with respect to the needed wall-clock time for computation. This effect is even more clearly visible for higher mesh resolutions.



No. of Unknowns	Seg. - time	Cpld - time	Seg. - its	Cpld - its
75768	0.2226E+02	0.2674E+02	151	67
408040	0.4053E+03	0.1500E+03	355	42
2611080	1.1352E+05	0.3105E+04	1592	39

**Table 6:** Performance analysis results of the channel flow problem

### 8.3 Classical Benchmarking Case – Heat-Driven Cavity Flow

This section deals with the evaluation and comparison not only of the pressure-velocity coupling but also of the velocity-to-temperature coupling through the Boussinesq approximation and the temperature-velocity/pressure coupling through the Newton-Raphson linearization of the convective term in the temperature equation. For this the standard heat-driven cavity flow [18,21] is adapted for a three dimensional domain and the material and geometric parameters are chosen such that a non-turbulent stationary flow exists, which means that the solution lies within the regime of the approximations made by the solver.

Essential for this benchmarking case is the nature of the flow. The fluid motion is a consequence of the effect of volume forces caused by temperature differences in the solution domain, hence the mathematical problem exhibits a strong coupling between the involved variables velocity, pressure and temperature. This relation is represented by the Rayleigh and Prandtl number. It is assumed that for this kind of flow the fully implicit treatment of the temperature coupling will yield further benefits with respect to wall time, compared with solution approaches that solve for the temperature separately. Table 7 lists the geometrical and solver parameters used for the performance analysis of this section.

**Table 7:** Characteristic problem properties used in the heated cavity flow test case

Property	Value	Unit
Density	1.19	$kg/m^3$
Viscosity	1.8E-5	$Ns/m^2$
Height	0.021277	m
Temperature difference	10	K
Coefficient of thermal expansion	0.00341	$1/K$
Under relaxation u	0.8	
Under relaxation p	0.2	
Under relaxation T	1.0	
Relative tolerance	1E-8/1E-4	

Using the data from table 7 and given Prandtl number for the flow problem  $Pr = 0.71$  the Rayleigh number  $Ra$ , a dimensionless number used to characterize buoyancy driven flows, can be calculated. From the definition of the Prandtl number the thermal diffusivity  $\alpha$  can be calculated as

$$\alpha = \frac{\mu}{\rho Pr} = 2.1304E - 5.$$

It follows that the Rayleigh number can be determined to

$$Ra = \frac{\rho g \beta \Delta T h^3}{\mu \alpha} \approx 10^4,$$

which implies according to ?? that the flow is still stationary and non-turbulent.

The tests were conducted on the formerly presented HHLR cluster, using the MPI2 and MEM2 section. For the tests involving higher resolutions the relative tolerance for convergence was increased to  $1E - 4$ . Table 8

The presented results are in good agreement with [77], which show monotonic decrease of the number of iterations with increased implicit coupling. It is notable that the pressure velocity coupling is responsible for the biggest decrease

Resolution	Solver configuration	Time	Non-linear it.
32x32x32	SEG	0.3719E+02	203
	CPLD	0.6861E+02	62
	TCPLD	0.1012E+03	31
	NRCPLD	0.2153E+02	22
64x64x64	SEG	0.1997E+04	804
	CPLD	0.7687E+03	63
	TCPLD	0.1278E+04	59
	NRCPLD	0.4240E+03	17
128x128x128	SEG	0.5197E+05	3060
	CPLD	0.1860E+05	74
	TCPLD	0.1950E+05	50
	NRCPLD	0.6155E+04	18

**Table 8:** Performance analysis results of the heated cavity flow problem

in the number of non-linear iterations. Different to the results presented in section 8.2 this does not yield significant performance benefits with respect to wall-clock time. In order to achieve the benefits of a fully coupled solution algorithm the coupling has to be increased to also involve temperature-to-velocity/pressure and velocity-to-temperature coupling.

Furthermore it can be noticed that the solely use of velocity-to-temperature coupling does not result in benefits compared to the coupled solution for velocities and pressure combined with a decoupled solve for the temperature equation. This is accredited to the treatment of the non-linearity of the temperature equation in the TCPLD solver configuration. Even though the momentum balances implicitly use the temperature from the next iteration, the temperature equation does not use the velocities of the next iteration. Instead the convective fluxes are calculated with the velocities from the previous iteration. Even though the implicit velocity-to-temperature coupling reduces the number of needed non-linear iterations an increase in the needed wall-clock time for computation can be noticed. This is attributed to the augmented costs during the application of the linear solver algorithm as a result of the additional degree of freedom that the linear system embraces. The necessary number of outer iterations is higher than in the NRCPLD configuration since the convective fluxes in the temperature equation are not coupled to the momentum balances which degrades the convergence of the non-linear iteration process.

It can be concluded that in order to profit from the benefits of implicit coupling the key lays in the temperature-to-velocity/pressure coupling. However, it should be noted that the implicit consideration of the corresponding terms furthermore increases the amount of memory needed for computation and hence does not come without drawbacks.

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## 9 Conclusion and Outlook

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In the present thesis a fully-coupled solution algorithm for the Navier-Stokes equations with a finite-volume method on co-located, locally refined block structured grids was implemented. The main difference of this algorithm compared to the common segregated solution algorithms was the implicit pressure-velocity coupling. The pressure-velocity coupling is a characterizing aspect of solution algorithms for Navier-Stokes equations with the potential to significantly reduce the time for computation. Furthermore the solution algorithm was extended to solve for flows involving buoyant forces, by using an implicit Boussinesq approximation in the momentum balances to achieve velocity-to-temperature coupling and a Newton-Raphson linearization to realize implicit temperature-to-velocity/pressure coupling.

The CAFFA solver framework, that was extended in the thesis was verified using a grid convergence study and a three-dimensional manufactured solution for the velocities, the pressure and the temperature. Further studies on the segregated solution algorithm showed, that a special modification of the widely used Rhie-Chow momentum interpolation scheme is necessary to calculate results that are independent of the under relaxation factor and thus comparable with the results obtained with a fully-coupled solution algorithm. In the implementation of the algorithm the further use on high performance computers was considered, using the PETSc library for parallelisation of the involved data structures and solving the resulting linear systems with solvers and preconditioners provided from the same toolkit.

A comparison study was performed dealing with the effect of implicit pressure-velocity coupling in the solution of the Navier-Stokes equations. Parallel performance measurements showed that for the implementation of the segregated and the coupled solution algorithm scalable program behaviour is possible for high numbers of involved unknowns. Performance studies on flows through complex geometries showed that the fully couple solution algorithm outperforms the segregated solution algorithm.

The analyses regarding the different degrees of velocity-to-temperature and temperature-to-velocity/pressure coupling showed that the implicit temperature-to-velocity/pressure coupling is the key aspect of maintaining high efficiency regarding the computation time for flow problems involving temperature transport and strong coupling between the velocities, the pressure and the temperature.

The present thesis revealed different starting points to further examine the effects of coupled solution algorithms in the context of finite-volume flow solvers. In the present thesis only stationary problems were solved. Due to the moderate Rayleigh number for the heated cavity test case a stationary solution existed. By increasing the Rayleigh number the coupling between the velocities, the pressure and the temperature would get stronger, however the flow will get instationary. A further investigation could examine if coupled solution methods maintain the higher efficiency compared to segregated solution algorithms when applied to instationary flows.

In this thesis a temperature equation was successfully coupled to the modelling equations of a fluid. One straightforward application of the solver would deal with conjugate heat transfer problems. On the other side in practice there exist other similar transport equations that exhibit strong coupling to the velocities. Examples are the scalar transport of volume fractions, when multiphase flows are solved with Volume-of-Fluid methods or turbulent flows which depending on the turbulence model involve further scalar quantities that are strongly coupled to the velocities. Subsequent studies could examine if the corresponding transport equations if a coupling can be efficiently implemented.

All linear systems surging from the discretization process of the coupled system of partial differential equations were solved using black-box implementations of the available solvers in the PETSc library. As studies on finite-volume [?,20,46] and finite-element [?, ?, 12,24,25,73] discretizations show, a lot of information has not been used in the solution process of the linear system yet, which imposes a barrier on performance. In order to exploit the coupling and the structure of the linear systems two different approaches can be considered. On approach features so called *physics-based* preconditioners as the SIMPLE preconditioner or other Schur-type preconditioners introduced in [24,46]. These kind of preconditioners accelerate the solution of the linear systems by taking into account the matrix structure as it is presented in figure 8. At the moment further active research is needed to develop preconditioners for fully-coupled systems surging from finite-volume discretizations. Another approach that additionally maintains high scalability of the solution algorithm of the resulting linear systems have been presented in [?,20]. In these approaches algebraic multigrid methods are constructed, that, different to the GAMG preconditioner in PETSc, take into account the matrix structure.

As the studies in the present thesis showed, segregated solution algorithms can perform well compared to fully coupled solution algorithms for smaller numbers of unknowns. Furthermore due to the lower requirements on system memory, the problems that can be solved with segregated solution algorithms may for high numbers of unknowns not be computable with fully-coupled solution algorithms. Especially for flows involving temperature transport many other implementations of segregated solution algorithms exist, whose performance has not been compared with a coupled solution method. Examples can be found in ??.

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