Eqs.

2

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4 1 Paper

Eq1

$$Profit = BioCH_4 - Cost_{AmineSystem}$$
 (1)

Eq2

$$Cost_{AmineSystem} = C_{Steam} \sum_{i} \frac{Q_i}{\lambda} \cdot \tau_{year} + \frac{1}{K} Cost_{Amine} \cdot fc_{Amine} \cdot \tau_{year}$$
 (2)

Eq3

$$Profit = BioCH_4 - Cost_{ZeoliteSystem}$$
 (3)

Eq4

$$Cost_{ZeoliteSystem} = C_{Electricity} \cdot W_{Compressor} + \frac{1}{K} M_{Zeolite} \cdot C_{Zeolite} \cdot N_{Cycle}$$
 (4)

$$Profit = BioCH_4 - Cost_{MembraneSystem}$$
 (5)

Eq6

$$Cost_{MembraneSystem} = C_{Electricity} \cdot W_{Compressor} + \frac{1}{K} \cdot C_{Membrane} \cdot \frac{1}{Lf} \cdot N_{Membranes} (\sum_{i \in stages} Area_i)$$
(6)

Eq7

$$Profit = BioCH_4 - Cost_{MembraneSystem} - Cost_{ZeoliteSystem} - Cost_{AmineSystem}$$
 (7)

5 2 Supplementary Material

Eq1

$$fc_{amine} = \frac{MW_{amine}}{[amine]} \cdot \left(\frac{CO2_{eff} \cdot fc_{CO_2}}{MW_{CO_2}}\right) \cdot \left(\frac{1}{GPSA}\right)$$
(8)

Eq2

$$fc_{amine} = fc_{recycledamine} + fc_{freshamine}$$
 (9)

Eq3

$$Q = F_{\text{amine}} \cdot q_{\text{heat,amine}} \tag{10}$$

Eq4

$$Q_{Col1} = \Delta H_{\text{react,amine}} \cdot CO2_{\text{eff}} \cdot fc_{CO_2}$$
(11)

$$Q_{Cond} = F_{Cond} \cdot q_{Cond,amine}$$

$$Q_{Reb} = F_{Reb} \cdot q_{Reb,amine}$$
(12)

Eq6

$$Q_{Cooling} = F_{Cooling} \cdot q_{Cooling, a \min e}$$
 (13)

Eq7

$$p_{\text{aminessolution}} = \text{Exp}\left(A - \frac{B}{(C + T_{\text{top}})}\right)$$
(14)

Eq8

$$Y = \frac{MW_{Wa}}{MW_{\text{outletgas}}} \cdot \frac{p_{\text{aminessolution}}}{(P_{Col2} - p_{\text{aminessolution}})}$$
(15)

Eq9

$$T_{out/compressor} = T_{in/compressor} + T_{in/compressor} \left(\left(\frac{P_{out/compressor}}{P_{in/compressor}} \right)^{\frac{z-1}{z}} - 1 \right) \frac{1}{\eta_c}$$

$$W_{(Compressor)} = (F) \cdot \frac{R \cdot z \cdot \left(T_{in/compressor} \right)}{((Mw) \cdot (z-1))} \frac{1}{\eta_c} \left(\left(\frac{P_{out/compressor}}{P_{in/compressor}} \right)^{\frac{z-1}{z}} - 1 \right)$$

$$(16)$$

Eq10

 CO_2 stream:

$$fc_{CO_2}|_{out} = \eta fc_{CO_2}|_{in}$$

$$fc_{CH_4}|_{out} = 0.02 \cdot fc_{CH_4}|_{in}$$

$$CH_4\text{stream}:$$

$$fc_{CO_2}|_{out} = (1 - \eta) fc_{CO_2}|_{in}$$

$$fc_{CH_4}|_{out} = 0.98 \cdot fc_{CH_4}|_{in}$$
(17)

$$q = \frac{q_m \cdot K \cdot P_{CO_2}}{1 + K \cdot P_{CO_2}} \tag{18}$$

Eq12a and 12b

$$q_m = -3.1555110^{-2}T(^{\circ}C) + 5.02915$$

$$K = 1.6307010^{(} - 03)T(^{\circ}C)^2 - 3.6866210^{(} - 01)T(^{\circ}C) + 27.3737$$
(19a)

$$q_m = -1.8235510^{-2}T(^{\circ}C) + 3.72021$$

 $K = 1.6307010^{-03}T(^{\circ}C)^2 - 3.6866210^{-1}T(^{\circ}C) + 27.3737$ (19b)

Eq13

$$m_{Zeolite} = \frac{1}{q \cdot 0.65} \frac{f_{CCO_2} \cdot 1000}{MW_{(CO_2)}} \eta \cdot \tau$$
 (20)

Eq22

$$Profit = BioCH_4 - Cost_{ZeoliteSystem}$$
 (21)

Eq23

$$Cost_{ZeoliteSystem} = C_{Electricity} \cdot W_{Compressor} + \frac{1}{K} M_{Zeolite} \cdot C_{Zeolite} \cdot N_{Cycle}$$
 (22)

Eq14

$$F_{feed} = F_{permeate} + F_{retentate} \tag{23}$$

Eq15

$$F_{feed} \cdot y_{i,feed} = F_{permeate} \cdot y_{i,permeate} + F_{retentate} \cdot y_{i,retentate}; i \in (CO_2, CH_4)$$
 (24)

$$J_i = \frac{F_{permeate} \cdot y_{i,permeate}}{A_{membrane}}; i \in (CO_2, CH_4)$$
(25)

Eq17

$$J_{i} = \varepsilon_{i} \left[y_{feedside} \cdot P_{feed} - y_{i,permeate} \cdot P_{Permeate} \right]; i \in (CO_{2}, CH_{4})$$
(26)

Eq18

$$y_{feedside} = \frac{y_{i,feed} - y_{i,retentate}}{\ln\left(\frac{y_{i,feed}}{y_{i,retentate}}\right)}; i \in (CO_2, CH_4)$$
(27)

Eq19

$$\varepsilon_i = \frac{Perm_i}{\delta}; i \in (CO_2, CH_4)$$
 (28)

Eq20

$$Profit = BioCH_4 - Cost_{MembraneSystem}$$
 (29)

Eq21

$$Cost_{MembraneSystem} = C_{Electricity} \cdot W_{Compressor} + \frac{1}{K} \cdot C_{Membrane} \cdot \frac{1}{Lf} \cdot N_{Membranes} (\sum_{i \in stages} Area_i)$$

$$(30)$$

Eq22

$$D_C = 44\sqrt{\frac{F_{gas}(MMsfd)}{P(psia)}}$$
(31)

$$D_R = 3.0\sqrt{F_{a\min e}(gal/\min)}$$
(32)