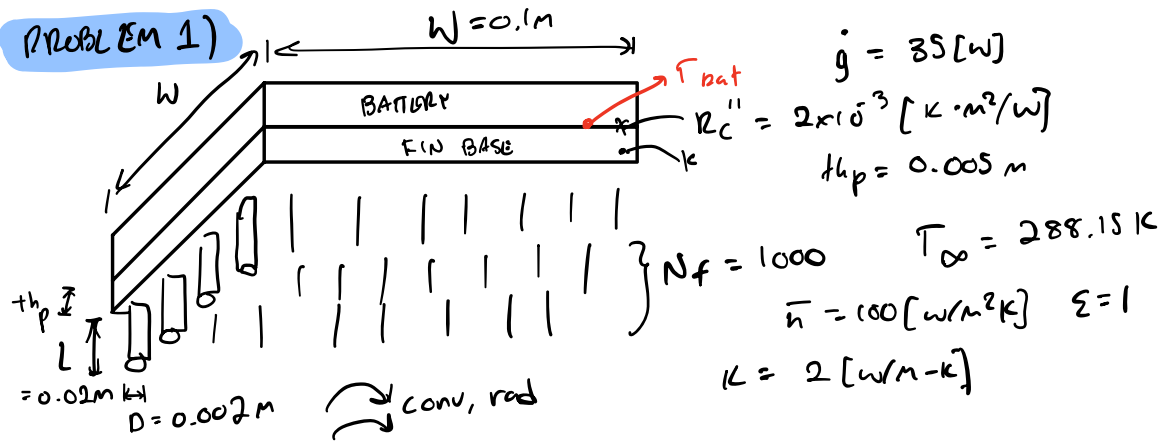


PROBLEM 1)



1a) Single fin, find Biot number & decide 1D or NOT

$$Bi = \frac{R_{\text{cond, xverse}}}{R_{\text{surr}}}, \quad R_{\text{cond, xverse}} = \frac{D/2}{k \cdot \pi/4 D^2}$$

$$R_{\text{surr}} = \left[\frac{1}{R_{\text{conv}}} + \frac{1}{R_{\text{rad}}} \right]^{-1}$$

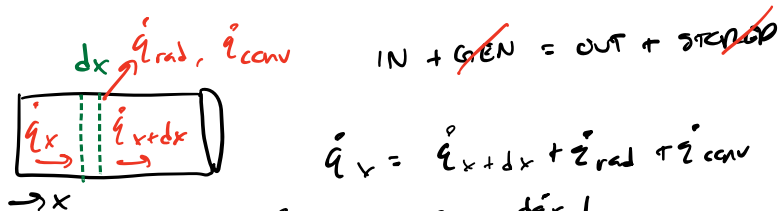
$$R_{\text{conv}} = \frac{1}{\bar{h} A_s}, \quad R_{\text{rad}} = \frac{1}{\sigma \epsilon A_s 4 \bar{T}^3}$$

$$A_s = \frac{\pi}{4} D^2 + \pi D L, \quad \bar{T} = 300 \text{ K (GUESS)}$$

$\rightarrow \text{EES}$

1b)

ASSUME 1D APPROX. VALID, FIND $T(x)$, ASSUME $\bar{T} = 300 \text{ K}$



$$\dot{q}_x = \dot{q}_{x+dx} + \dot{q}_{\text{rad}} + \dot{q}_{\text{conv}}$$

$$\dot{q}_x = -k A_c \frac{dT}{dx}$$

$$\dot{q}_{x+dx} = \dot{q}_x + \frac{d\dot{q}_x}{dx} dx$$

$$\rightarrow 0 = \frac{d\dot{q}_x}{dx} dx + \underbrace{\bar{h} dA_s (T(x) - T_\infty)}_{\dot{q}_{\text{conv}}} + \underbrace{\sigma \epsilon dA_s 4 \bar{T}^3 (T(x) - T_\infty)}_{\dot{q}_{\text{rad}}}$$

$$0 = \frac{d\dot{q}_x}{dx} dx + \bar{h} (\text{per} \cdot dx) (T(x) - T_\infty) + \sigma \epsilon (\text{per} \cdot dx) 4 \bar{T}^3 (T(x) - T_\infty)$$

$$Q = \frac{d}{dx} \left[-k A_c \frac{dT}{dx} \right] + (\bar{h} + \sigma \varepsilon 4 T^3) \cdot \text{per} \cdot (T(x) - T_\infty)$$

$$0 = -kA_c \frac{d^2 T}{dx^2} \quad \text{+} \quad \text{"} \quad \text{"}$$

$$\rightarrow \frac{d^2 T}{dx} = \frac{(\bar{h} + \sigma \varepsilon 4 \bar{T}^3) \cdot \text{per} \cdot (T(x) - T_\infty)}{\kappa A_c}$$

$$\frac{d^2 T(x)}{dx^2} - \frac{(\bar{h} + \sigma \varepsilon_4 \bar{T}^3) \cdot \text{per}}{\kappa A_c} T(x) = - \frac{(\bar{h} + \sigma \varepsilon_4 \bar{T}^3) \cdot \text{per}}{\kappa A_c} T_\infty$$

1c) $T = T_h + T_p$

HOMOGENEOUS SOLUTIONS:

$$\frac{d^2 T(x)}{dx^2} - \frac{(\bar{h} + \sigma \varepsilon_4 \bar{T}^3) \cdot \text{per}}{k d_c} T(x) = 0$$

SOL: $\frac{d^2 T_h}{dx^2} - m^2 T_h = 0$; $T_h = C_1 \exp(mx) + C_2 \exp(-mx)$

$$\rightarrow m = \sqrt{\frac{(\bar{h} + \sigma \varepsilon_4 \bar{T}^3) \pi D}{k A_c}}$$

$$\therefore T_h = C_1 \exp(mx) + C_2 \exp(-mx)$$

PARTICULAR SOLUTION:

GUESS SAME FORM AS RHS: $T_p = C_3$

→ PLUG IN C_3 FOR $T(x)$:

$$\frac{d^2 C_3}{dx^2} - \frac{(\bar{n} + 0.24T^3) \cdot \text{per}}{K A_c} C_3 = - \frac{(\bar{n} + 0.24T^3) \cdot \text{per}}{K A_c} T_\infty$$

$$\therefore C_3 = T_\infty = T_p$$

$$T = T_h + T_p = C_1 \exp(mx) + C_2 \exp(-mx) + T_\infty$$

1d) \rightarrow EES

$$\text{BC 1)} \quad T(x=0) = T_0$$

$$\text{BC 2)} \quad \dot{q}|_{x=L} = \dot{q}_{\text{conv}} + \dot{q}_{\text{rad}}$$

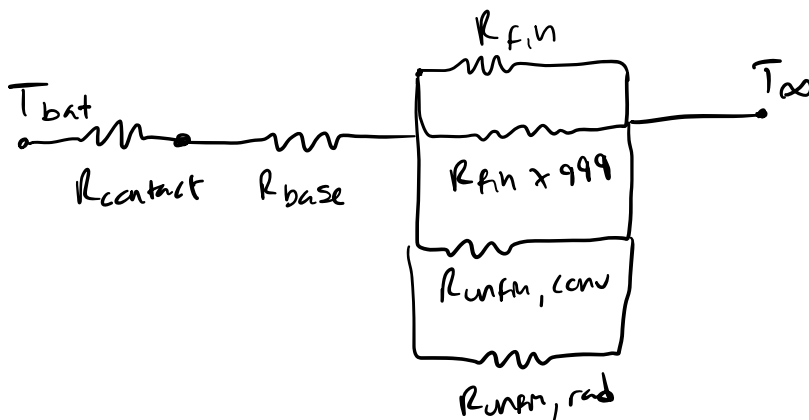
$$-kA_c \left. \frac{dT}{dx} \right|_{x=L} = \bar{h} A_c (T_s - T_\infty) + \sigma \varepsilon A_c 4\bar{T}^3 (T_s - T_\infty)$$

$$-kA_c [C_1 m e^{mL} - C_2 m e^{-mL}] = (\bar{h} + \sigma \varepsilon 4\bar{T}^3) A_c (T_s - T_\infty)$$

$$1e) \quad \eta_f = \frac{\tanh(mL) + m \frac{A_c}{\text{per}}}{mL \left(1 + \frac{A_c}{\text{per} \cdot L}\right) \cdot \left(1 + mL \frac{A_c}{\text{per} \cdot L} \tanh(mL)\right)}$$

$$m = 2 \sqrt{\frac{\bar{h} + \sigma \varepsilon 4\bar{T}^3}{D_{1c}}}$$

A_f = total fin area
 A_c = cross section



\$UNITSYS SI K Pa J mass rad

// Problem 1)

// Givens

W = 0.1 [m]

g_dot = 35 [W]

th_p = 0.005 [m]

R_dprime_C = 2e-3 [K*m^2/W]

T_infinity = 288.15 [K]

N_f = 1000 [-]

h_bar = 100 [W/m^2-K]

epsilon = 1 [-]

D = 0.002 [m]

//L = 0.02 [m]

// comment for part f,

k = 2 [W/m-K]

// 1a)

T_bar = 300 [K]

// guess value above T_infinity

A_S = pi#4*D^2 + pi#D*L

// total surface area including tip

A_C = pi#4*D^2

// cross sectional area

A_S_xverse = pi#D*L

// surface area excluding tip

//The course textbook (5.1.1) indicates it is appropriate to use the ratio of the volume to the surface area as the "*conduction length*", and to use the total surface area as the "*cross-sectional area*" normal to the conduction heat flow

R_cond_xverse = (pi#(D/2)^2*L)/(A_S_xverse)/(k*A_S_xverse)
number

// resistance in transverse direction to see if it is signifi

R_conv = 1/(h_bar*A_S)

R_rad = 1/(sigma#epsilon*A_S^4*T_bar^3)

R_surr = (1/R_conv + 1/R_rad)^(-1)

Biot = R_cond_xverse/R_surr

// 1c)

m = sqrt((h_bar+sigma#epsilon*4*T_bar^3)*pi#D/(k*A_C))

// calculated m formula

// T = C_1*exp(m*x) + C_2*exp(-m*x) + T_infinity

// 1d)

T_S = 200 [K] //guess T_S

T_0 = 200 [K] //guess T_0

T_0 = C_1*exp(m*0[m]) + C_2*exp(-m*0[m]) + T_infinity

// BC1

T_L = C_1*exp(m*L) + C_2*exp(-m*L) + T_infinity

// T(x=L) for BC2

-k*(C_1*m*exp(m*L)-C_2*m*exp(-m*L)) = (h_bar+sigma#epsilon*4*T_bar^3)*(T_L-T_infinity)

// BC2

// 1e)

R_base = th_p/(k*W^2)

// conduction resistance through plate

R_contact = R_dprime_C/W^2

// given contact resistance

per = pi#D

// fin perimeter

m_n = 2*sqrt((h_bar+sigma#epsilon*4*T_bar^3)/(D*k))

// m_new

eta_fin = (tanh(m_n*L)+m_n*A_C/(per))/(m_n*L*(1+A_C/(per*L)) * (1+m_n*L*A_C/(per*L)*tanh(m_n*L))) // given

```

R_fin = 1/(h_bar*A_S*eta_fin)           // formula with eta value
A_unf = W^2-N_f*A_C                     // unfinned area
R_unfinned_conv = 1/(h_bar*(A_unf))      // convection of unfinned area
R_unfinned_rad = 1/(sigma#*epsilon*A_unf*4*T_bar^3) // radiation of unfinned area

R_total = R_base + R_contact + 1/( N_f/R_fin + 1/R_unfinned_conv + 1/R_unfinned_rad ) //series and parallel

T_bat = g_dot*R_total + T_infinity      // rearranged q = (T_H - T_C)/R

// 1f)

rho_fin = 3000 [kg/m^3]                 // given fin density
vol_fin = A_C*L                         // fin volume
m_f = rho_fin*vol_fin

t_flight = 3600[s] - (T_bat - 300[K])*(60[s/K]) - N_f*m_f*(1800[s/kg])

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SOLUTION

Unit Settings: SI K Pa J mass radMaximization of $t_{\text{flight}}(L)$ 48 iterations: Quadratic Approximations method (Rel. Tol=1.0E-04)

$A_c = 0.000003142$ [m ²]	$A_s = 0.00003668$ [m ²]
$A_{s,\text{xverse}} = 0.00003354$ [m ²]	$A_{\text{unf}} = 0.006858$ [m ²]
$Biot = 0.02902$ [-]	$C_1 = -1.916$ [K]
$C_2 = -86.23$ [K]	$D = 0.002$ [m]
$\epsilon = 1$ [-]	$\eta_{\text{fin}} = 0.5029$ [-]
$\dot{g} = 35$ [W]	$\bar{h} = 100$ [W/m ² -K]
$k = 2$ [W/m-K]	$L = 0.005338$ [m]
$m = 325.8$ [1/m]	$m_f = 0.00005031$ [kg]
$m_n = 325.8$ [1/m]	$N_f = 1000$ [-]
$per = 0.006283$ [m]	$\rho_{\text{fin}} = 3000$ [kg/m ³]
$R_{\text{base}} = 0.25$ [K/W]	$R_{\text{cond,xverse}} = 7.454$ [K/W]
$R_{\text{contact}} = 0.2$ [K/W]	$R_{\text{conv}} = 272.6$ [K/W]
$R_c = 0.002$ [K*m ² /W]	$R_{\text{fin}} = 542$ [K/W]
$R_{\text{rad}} = 4452$ [K/W]	$R_{\text{surr}} = 256.9$ [K/W]
$R_{\text{total}} = 0.8387$ [K/W]	$R_{\text{unfinned,conv}} = 1.458$ [K/W]
$R_{\text{unfinned,rad}} = 23.81$ [K/W]	$th_p = 0.005$ [m]
$T_0 = 200$ [K]	$\bar{T} = 300$ [K]
$T_{\text{bat}} = 317.5$ [K]	$t_{\text{flight}} = 2459$ [s]
$T_{\infty} = 288.2$ [K]	$T_L = 262.1$ [K]
$T_s = 200$ [K]	$vol_{\text{fin}} = 1.677\text{E-}08$ [m ³]
$W = 0.1$ [m]	

No unit problems were detected.

KEY VARIABLES

Maximization of $t_{\text{flight}}(L)$ 48 iterations: Quadratic Approximations method (Rel. Tol=1.0E-04)

$Biot = 0.02902$ [-]	<i>1a) Biot number is sufficiently less than 1, indicating that the conduction resistance through the fins is low enough compared to the resistance to the surroundings, and can be neglected.</i>
$C_1 = -1.916$ [K]	<i>1d) $C_1 \approx 0$</i>
$C_2 = -86.23$ [K]	<i>1d) C_2</i>

$L = 0.005338$ [m] 1f) optimized length via min/max for flight time
 $R_{\text{total}} = 0.8387$ [K/W] 1e) total thermal resistance
 $T_{\text{bat}} = 317.5$ [K] 1e) battery temperature