

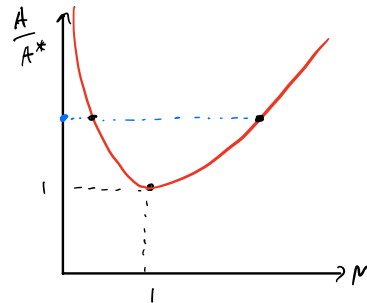
Recap

$$\frac{T}{T_0} = \left(1 + \frac{\gamma-1}{2} M^2\right)^{-1}$$

$$\frac{P}{P_0} = \left(1 + \frac{\gamma-1}{2} M^2\right)^{\frac{\gamma}{1-\gamma}}$$

$$\frac{\rho}{\rho_0} = \left(1 + \frac{\gamma-1}{2} M^2\right)^{\frac{1}{1-\gamma}}$$

$$\frac{A}{A^*} = \frac{1}{M} \left[ \frac{2}{\gamma+1} \left(1 + \frac{\gamma-1}{2} M^2\right) \right]^{\frac{\gamma+1}{2(\gamma-1)}}$$



If  $M=1$  occurs, it can only happen at an area minimum  
in that case,  
 $A_{min} = A_t = A^*$

Existence of  $A_{min}$  does not guarantee  $M=1$  is ever reached

For each value of  $A/A^*$ , 2 possible values of  $M$

iii) values of  $T/T_0$ ,  $P/P_0$ ,  $\rho/\rho_0$ ,  $A/A^*$

✓ online calc.

✓ tabulated

✓ plotted → from plots:

- changes of  $T, P, \rho$  very small for  $M < 1$

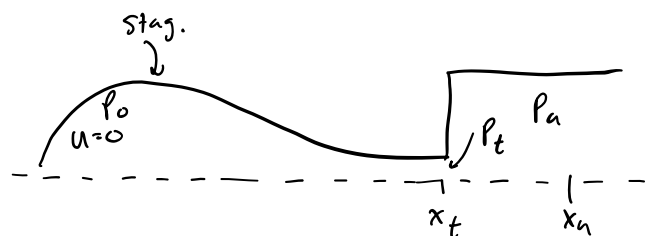
- throughout  $M$  range,  $T, P, \rho$  decrease monotonically

useful to set aside sonic value of  $P$

$$\frac{P^*}{P} = \left(1 + \frac{\gamma-1}{2} M^2\right)^{\frac{\gamma}{1-\gamma}} = \left(1 + \frac{\gamma-1}{2}\right)^{\frac{\gamma}{1-\gamma}}$$

For  $\gamma = 1.4$ ,  $\frac{P^*}{P_0} = 0.5283$

### 4.3 Converging nozzle

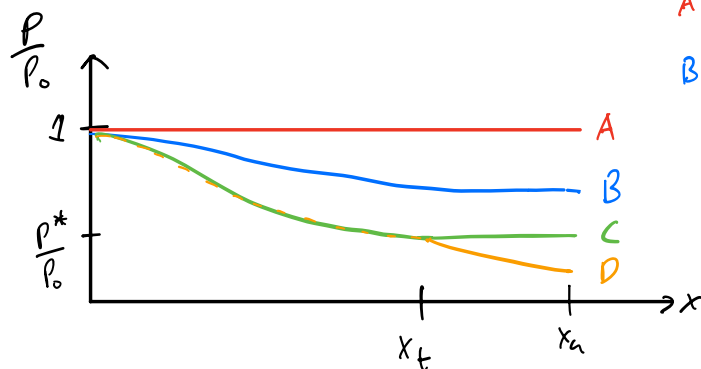


$P_a$  = ambient pressure  
generally  $P_a \neq 1 \text{ atm}$

Keeping  $P_0$  fixed, start w/  
 $P_a = P_0$  and progressively decrease  $P_a$

Flow governed by

$$\begin{cases} A/A^* = \frac{1}{M} \left[ \frac{2}{\gamma+1} \left( 1 + \frac{\gamma-1}{2} M^2 \right) \right]^{\frac{\gamma+1}{2(\gamma-1)}} \\ \frac{P}{P_0} = \left( 1 + \frac{\gamma-1}{2} M^2 \right)^{\frac{\gamma}{1-\gamma}} \end{cases}$$



A:  $P_a = P_0$ ; no flow

B:  $P^* < P_a < P_0$  subsonic flow

$$P_t = P_a$$

$$M(x=x_t) < 1$$

As  $P_a \downarrow$ ,  $\dot{m} \uparrow$  subsonic throughout

C:  $P_a = P^*$  sonic at throat

$$P_t = P^* = P_a$$

D:  $P_a < P^*$  subsonic throughout  
sonic @ throat

pressure decreases after  
nozzle

Since between stagnation & throat  
 $P$ -distribution for cases for C & D  
is exactly the same,  $\dot{m}$  reaches its maximum  
value in case C (sonic throat). Lowering back pressure  
below  $P^*$  does not increase  $\dot{m}$ : the flow is "choked"

#### Example



$$\Gamma \begin{cases} \gamma = 1.4 \\ P_0 = 406 \text{ kPa} \\ T_0 = 368 \text{ K} \\ A_t = 0.01 \text{ m}^2 \\ P_a = 240 \text{ kPa} \end{cases} \quad F = \dot{m}$$

→ Need  $P_t, U_t$  for  $\dot{m}$

1) verify if  $M_t = 1$  or  $< 1$

$$\text{if } P_a \leq P^* \Rightarrow M_t = 1$$

$$\text{if } P_a > P^* \Rightarrow M_t < 1$$

$$\frac{P^*}{P_0} = \left( 1 - \frac{\gamma-1}{2} \right)^{\frac{\gamma}{1-\gamma}} = 0.5283 \rightarrow P^* = 0.5283 P_0 = 214.5 \text{ kPa}$$

$$P_a > P^* \Rightarrow M_t < 1$$

→ this is case B ( $p_t = p_a$ )

$$\frac{p_t}{p_0} = \frac{p_a}{p_0} = \left(1 + \frac{\gamma-1}{2} M_t^2\right)^{\frac{\gamma}{1-\gamma}}$$

$$M_t = \left[ \frac{2}{\gamma-1} \left[ \left(\frac{p_a}{p_0}\right)^{\frac{1-\gamma}{\gamma}} - 1 \right] \right]^{\frac{1}{2}} = 0.9$$

$$\dot{m} = \rho_t u_t A_t$$

$$u_t = M_t a_t$$

$$a_t = \sqrt{\gamma R T_t}$$

$$\frac{T_t}{T_0} = \left(1 + \frac{\gamma-1}{2} M_t^2\right)^{-1} \Rightarrow T_t = 317 \text{ K}$$

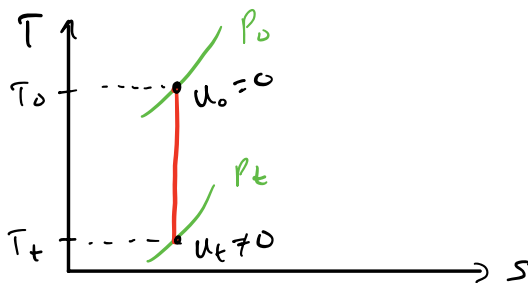
$$\rightarrow a_t = \sqrt{1.4 \cdot 287 \cdot 317} = 358 \text{ m/s}$$

$$u_t = 0.9 \cdot 358 = 322 \text{ m/s}$$

ideal  
gas

$$\rho_t = \frac{p_t}{R T_t} = 2.64 \frac{\text{kg}}{\text{m}^3}$$

$$\rightarrow \dot{m} = 8.5 \text{ kg/s}$$



For fixed  $p_0, p_a, T_0$

once  $M(x_t) = 1$ ,  $\dot{m}$  can no longer increase

Recall  $J = \underbrace{\dot{m} u_e}_{\text{usually dominant}} + (p_e - p_a) A_e$

→ can increase thrust by increasing  $u_e$

→ use divergent bell following throat to increase exit velocity