

# Problem 1

$$P = 1 \text{ atm}$$

$$T_\infty$$

$$u_\infty$$

$$L = 0.5 \text{ m}$$

$$w = 0.2 \text{ m}$$

$$u_\infty = 50 \text{ m/s}, T_\infty = 10^\circ\text{C}$$

$$T_s = 200^\circ\text{C}$$

$$s$$

a)  $s$  s.t. external flow, find  $\dot{q}$  for single plate, both sides

$$\dot{q}_{2s} = 2 \cdot \dot{q}_{1s} \xrightarrow{u_\infty, T_\infty}$$

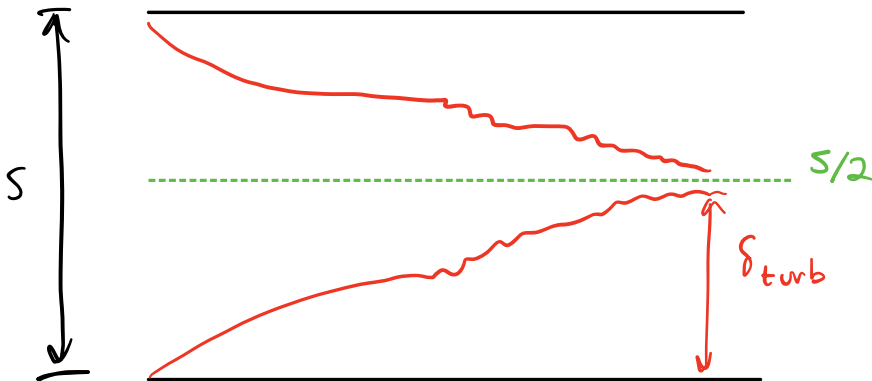
$$T_s$$

$$T_{\text{film}} = \frac{T_s + T_\infty}{2} = 378.15 \text{ [K]}$$

$$Re_{\text{crit}} = \frac{\rho u_\infty x_{\text{crit}}}{\mu} = 5 \times 10^5 \rightarrow x_{\text{crit}} = 0.2359 \text{ [m]} < L = 0.5 \text{ [m]}$$

$\rightarrow$  laminar & turbulent correlations

b)



$$\rightarrow s_{\text{mh}} = 2 \cdot \delta_{\text{turb}}$$

\$unitsystem SI C J Pa

**"Problem 1"**

$$L = 0.5 \text{ [m]}$$

$$W = 0.2 \text{ [m]}$$

$$u_{\infty} = 50 \text{ [m/s]}$$

$$T_{\infty} = 10 \text{ [C]}$$

$$T_s = 200 \text{ [C]}$$

$$P = 1 \text{ [atm]} * \text{convert(atm, Pa)}$$

$$A_s = L * W$$

$$T_{\text{film}} = (T_s + T_{\infty}) / 2$$

$$Re_{\text{crit}} = 5e5$$

$$Re_{\text{crit}} = \rho * u_{\infty} * x_{\text{crit}} / \mu$$

$$\rho = \text{density}(\text{Air}, T = T_{\text{film}}, P = P)$$

$$\mu = \text{viscosity}(\text{Air}, T = T_{\text{film}})$$

**"part a correlation"**

$$Re_L = \rho * u_{\infty} * L / \mu$$

$$Pr = \text{prandtl}(\text{Air}, T = T_{\text{film}})$$

$$Nus_{\text{bar}}_L = 0.6774 * Pr^{(1/3)} * Re_{\text{crit}}^{0.5} / (1 + (0.0468 / Pr)^{(2/3)})^{(1/4)} + 0.0158 * Pr^{(1/3)} * (Re_L^{(6/7)} - Re_{\text{crit}}^{(6/7)}) \text{ "use laminar and turbulent correlation since } x_{\text{crit}} < L \text{ "}$$

$$Nus_{\text{bar}}_L = h_{\text{bar}} * L / k$$

$$k = \text{conductivity}(\text{Air}, T = T_{\text{film}})$$

$$\dot{q}_{\text{dot}}_{\text{oneside}} = h_{\text{bar}} * A_s * (T_s - T_{\infty})$$

$$\dot{q}_{\text{dot}}_{\text{total}} = 2 * \dot{q}_{\text{dot}}_{\text{oneside}}$$

**"part b"**

$$\delta_{\text{turb}} = 0.16 * L / Re_L^{(1/7)}$$

*"max thickness at end of plate, s needs to be at least twice this value for external flow"*

$$s = \delta_{\text{turb}} * 2$$

**SOLUTION****Unit Settings: SI C Pa J mass deg**

$$A_s = 0.1 \text{ [m}^2\text{]}$$

$$L = 0.5 \text{ [m]}$$

$$Pr = 0.711 \text{ [-]}$$

$$Re_L = 1.060E+06 \text{ [-]}$$

$$T_{\infty} = 10 \text{ [C]}$$

$$x_{\text{crit}} = 0.2359 \text{ [m]}$$

$$\delta_{\text{turb}} = 0.01102 \text{ [m]}$$

$$\mu = 0.00002202 \text{ [Pa-S]}$$

$$\dot{q}_{\text{oneside}} = 1653 \text{ [W]}$$

$$\rho = 0.9335 \text{ [kg/m}^3\text{]}$$

$$T_s = 200 \text{ [C]}$$

$$\bar{h} = 86.99 \text{ [W/m}^2\text{-K]}$$

$$Nus_L = 1390 \text{ [-]}$$

$$\dot{q}_{\text{total}} = 3306 \text{ [W]}$$

$$s = 0.02205 \text{ [m]}$$

$$u_{\infty} = 50 \text{ [m/s]}$$

$$k = 0.0313 \text{ [W/m-K]}$$

$$P = 101325 \text{ [Pa]}$$

$$Re_{\text{crit}} = 500000 \text{ [-]}$$

$$T_{\text{film}} = 105 \text{ [C]}$$

$$W = 0.2 \text{ [m]}$$

No unit problems were detected.

**KEY VARIABLES**

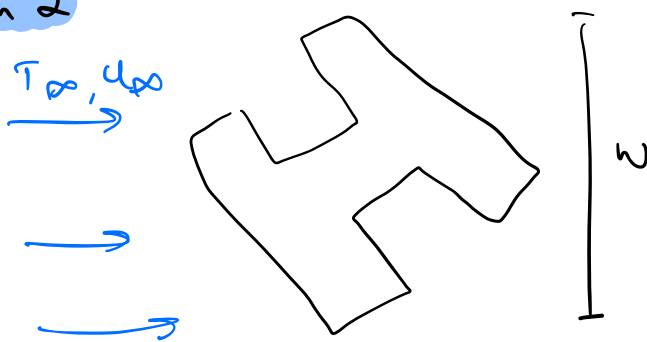
$$\dot{q}_{\text{total}} = 3306 \text{ [W]}$$

$$s = 0.02205 \text{ [m]}$$

*a) total heat transfer from single plate, both sides**b) minimum spacing s such that boundary layers do not touch by the end of the length*

## Problem 2

$T_\infty, u_\infty$



$$per = 2.1 \cdot w$$

$$Nu = a_0 \cdot Re_L^{a_1} \cdot Pr^{a_2}$$

\$unitsystem SI C J Pa  
\$tabstops 0.2 0.4 0.6 1.5

"

*Starter file.*

*Homework 7 - correlation problem*

*ME 364 - Fall 2023"*

\$varinfo u\_infty[] units='m/s'  
\$varinfo rho[] units='kg/m^3'  
\$varinfo mu[] units='Pa-s'  
\$varinfo c[] units='J/kg-K'  
\$varinfo k[] units='W/m-K'  
\$varinfo current[] units='A'  
\$varinfo voltage[] units='V'  
\$varinfo T\_infty[] units='C'  
\$varinfo T\_s[] units='C'

*"Geometry"*

L = 0.5 [m] *"Length of structure"*

W = 0.075 [m] *"Profile width in flow"*

per = 2.1 \* W *"Perimeter of the shape"*

A\_s = per\*L *"Surface area - ignore ends"*

N\_lookup = 30 *"Rows in the lookup table"*

**"! To inspect data, go to Lookup table window"**

*"Retrieve table data as arrays"*

Duplicate i=1,N\_lookup

u\_infty[i] = lookup('data', i, 'u\_infty')

rho[i] = lookup('data', i, 'rho')

mu[i] = lookup('data', i, 'mu')

c[i] = lookup('data', i, 'c')

k[i] = lookup('data', i, 'k')

current[i] = lookup('data', i, 'current')

voltage[i] = lookup('data', i, 'voltage')

T\_infty[i] = lookup('data', i, 'T\_infty')

T\_s[i] = lookup('data', i, 'T\_s')

*"...Calculations here..."*

ReL[i] = rho[i]\*u\_infty[i]\*L/mu[i]

Pr[i] = mu[i]\*c[i]/k[i]

q\_dot[i] = current[i]\*voltage[i]

q\_dot[i] = h\_bar[i]\*A\_s\*(T\_s[i]-T\_infty[i])

Nu\_bar[i] = h\_bar[i]\*L/k[i]

Nu\_p[i] = a0 \* (rho[i]\*u\_infty[i]\*L/mu[i])^(a1) \* (mu[i]\*c[i]/k[i])^(a2)

*"error"*

err[i] = abs(Nu\_p[i]-Nu\_bar[i])/Nu\_bar[i]

End

*{a0 = 1*

*a1 = 1*

$a_2 = 1$

"Cumulative error"

$\text{err\_tot} = \text{sum}(\text{err}[i], i=1, 30)$

"part c"

"Yes, the predicted Nusselt number values closely match the experimental data, indicating a good correlation with these coefficients."

#### SOLUTION

**Unit Settings: SI C Pa J mass deg**

Minimization of  $\text{err\_tot}(a_0, a_1, a_2)$  806 iterations: Variable Metric method (Rel. Tol=1.0E-06)

$a_0 = 1.207$  [-]       $a_1 = 0.3408$  [-]       $a_2 = 0.491$  [-]       $A_s = 0.07875$  [m<sup>2</sup>]       $\text{err\_tot} = 1.994$  [-]

$L = 0.5$  [m]       $N_{\text{lookup}} = 30$  [-]       $\text{per} = 0.1575$  [m]       $W = 0.075$  [m]

No unit problems were detected.

#### KEY VARIABLES

Minimization of  $\text{err\_tot}(a_0, a_1, a_2)$  806 iterations: Variable Metric method (Rel. Tol=1.0E-06)

$a_0 = 1.207$  [-]      b)  $a_0$  coefficient

$a_1 = 0.3408$  [-]      b)  $a_1$  coefficient

$a_2 = 0.491$  [-]      b)  $a_2$  coefficient

