Alternative Algebraic Perspectives on CO/H₂

PROX over MnO₂ Composite Catalysts

Marco Bertini,[†] Francesco Ferrante,[†] Laura Gueci,[†] Antonio Prestianni,[†]

Dario Duca.*,† Francesco Arena.‡ and Dmitry Yu. Murzin¶

†Dipartimento di Fisica e Chimica "Emilio Segrè", Università degli Studi di Palermo, Viale

delle Scienze Ed. 17, I-90128 Palermo, Italy

‡Dipartimento di Ingegneria, Università degli Studi di Messina, Contrada di Dio, I-98166

Messina, Italy

¶Laboratory of Industrial Chemistry and Reaction Engineering, Johan Gadolin Process

Chemistry Centre, Åbo Akademi University, Henriksqatan 2, 20500 Turku/Åbo, Finland

E-mail: dario.duca@unipa.it

Phone: +39-091-238-97975. Fax: +39-091-590015

GCODE: How to use it

The example provided is currently addressed to the referees of the article of the header. It

constitutes an example to extract, using GCODE, information regarding the PROX catalytic

system at T = 298 K and a total pressure of 100 kPa, with the percentages of CO, O_2 , H_2 ,

and N₂ being 1, 1, 98, and 0, respectively. However, it could also be applied to the study of

other complex catalytic cycles by modifying the input related to the energetic information

and adapting the graph representation to these new cycles.

GCODE for modularity and simplicity, is here shaped by two environments named WATER

and FIRE. In the first, given a starting graph, representing a catalytic mechanism, the

1

spanning tree (Σ -T) and the cycle branched component (X-T) LISP lists needed for the analysis are individuated. In the second this analysis is performed extracting the catalytic information.

The WATER environment is formed by four component codes: W0, W1, W2, W3. The former identifies the possible branches, X-Ts, that connect to the different cycles present in the graph. W0 is also included in this repository although it is extremely simple to extract the component X-Ts of the branched graphs, reported in Figs. 4 and 5 of the title article, through a visual analysis of the starting graph related to the catalytic mechanism. The remaining codes are applied, in the order, W1, W2 and W3. In this work the result of this procedure is summarized by Table S2, including the 62 tuples representing the spanning trees characterizing the whole process considered. These do not include neither cycles nor reversible edges and show all the edges oriented to one of the nodes in the graph (e.g., see Fig. 3).

W1 is employed to extract all the isolable Σ-Ts (in this case 78 graphs). To get this result, W1 receive as input the information of the file graphD_in summing up the list of edges representing the steps of the whole catalytic mechanism. Whereas, to reach the final information on the 62 Σ-Ts, W2 operates on sink_out-1, the file output of W1 containing the tuple representation of the 78 spanning trees including the ones containing cycles as well as reversible edges, and W3 on the one, sink_out_0, of W2, containing the filtered 54 spanning trees not containing internal cycles but still including reversible edges. Of course, the results obtained in the WATER environment do not depend on the temperature.

The FIRE environment is formed by three components, *i.e.* **F1**, **F2** and **F3**. The file **T298**, input of **F1**, contains the values of ΔG^{\ddagger} reported in Table S1 for the involved steps, which are individuated following the node notation reported in Fig. 2(a). The ΔG^{\ddagger} values for the steps involving adsorption processes have been additionally corrected using Eq. 3 at the given temperature, total pressure, and partial pressures considered.

The component code F1 reads information from the file T298 and loads the files $W2_0$,

W2_1 - W2_12 and C2 and C3. The first contains the graphs of all the Σ-T lists, expressed as tuples of edges, characterizing the overall mechanism. The same Σ-Ts are separately grouped, as shown in Table S2, in the files W2_1 - W2_12 while C3 and C2 contain the same information, although referring to the branched cycles of Figs. 4 and 5. These files are all processed, and the result is collected in the corresponding END_X files with X = 0 - 12, C2, C3, which gather the related overall weights of the Σ-Ts and branched cycles, expressed in terms of Total Energy Content (TEC/kJmol⁻¹) values. Each TEC = $\sum_k \Delta G_k^{\ddagger}$ is clearly related to each considered subgraph (either a spanning tree or a branched cycle), with k representing any edge/step component of the latter.

The component $\mathbf{F2}$ is a bridge code that processes the information in the $\mathbf{END}_{-}\mathbf{X}$ files and returns the corresponding files $\mathbf{EXIT}_{-}\mathbf{X}$, with $\mathbf{X}=0-12$, C2, C3. These files collect in a compact form (*i.e.* without redundant information) the tuples of the TEC values for each group of Σ -Ts and branched graphs.

The component F3 reads the files $EXIT_X$ and processes them, generating the complementary $RESULT_X$ files, which report the cumulative probabilities, corresponding to the product of the exponential kernels present in Eqs. 2 and 3, characteristic of the Σ -Ts and branched graphs, containing X-Ts. This information, through Eqs. 5, 7, and 8, enables the calculation of TOF values, surface populations and selectivity, for the given temperature and pressures.

It can be noted that all the **END**, **EXIT** and **RESULTS** files, if present, can be safely erased and easily regenerated while the component codes can be linked through a batch file. In order to calculate the properties of the same system at different temperatures only the **F3** component needs to be modified, introducing the new temperature. Finally, to evaluate the effects of the pressure of the gas phase species, useful for example in determining the reaction orders, the values of ΔG^{\ddagger} for the steps involving adsorption processes in the file **T**, in this case **T298**, must be corrected through Eq. 4.