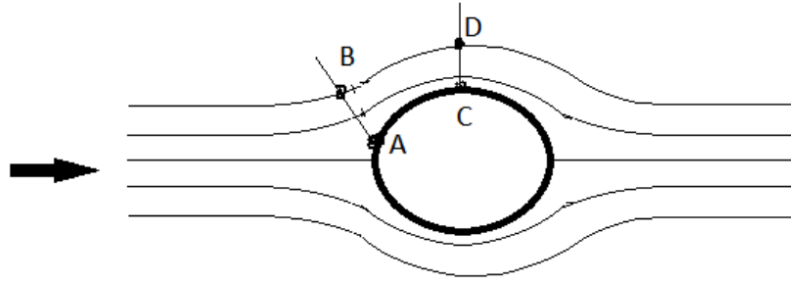


# XE-2016

EE24Btech11022 - Eshan Sharma

- 1) The flow field shown over a bluff body has considerably curved streamlines. A student measures pressures at points A, B, C, and D and denotes them as  $P_A$ ,  $P_B$ ,  $P_C$ , and  $P_D$  respectively. State which one of the following statements is true. The arrow indicates the freestream flow direction.



- a)  $P_A = P_B$  and  $P_C > P_D$   
 b)  $P_A > P_B$  and  $P_C > P_D$   
 c)  $P_A = P_B$  and  $P_C < P_D$   
 d)  $P_A > P_B$  and  $P_C < P_D$
- 2) A 2-D incompressible flow is defined by its velocity components in m/s as  $u = -\frac{cy}{x^2+y^2}$  and  $v = \frac{cx}{x^2+y^2}$ . If the value of the constant  $c$  is equal to  $0.1 \text{ m}^3$ , the numerical value of vorticity at the point  $x = 1 \text{ m}$  and  $y = 2 \text{ m}$  is \_\_\_\_\_  $\text{s}^{-1}$ .
- 3) Two flow configurations are shown below for flow of incompressible, viscous flow. The inlet velocity for the diverging nozzle (Fig (i)) and free-stream velocity for flow past the bluff body (Fig (ii)) is constant. Points A and B are separation points and flow is laminar. The relation regarding velocity gradients at point A and B is ( $y$  is the direction normal to the surface at the point of separation).

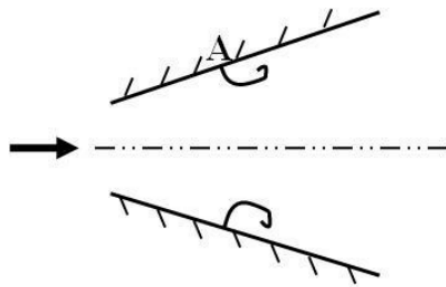


Fig (i)

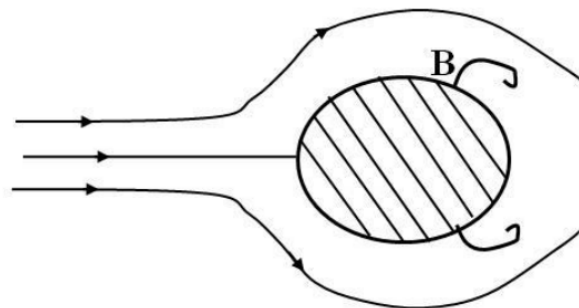
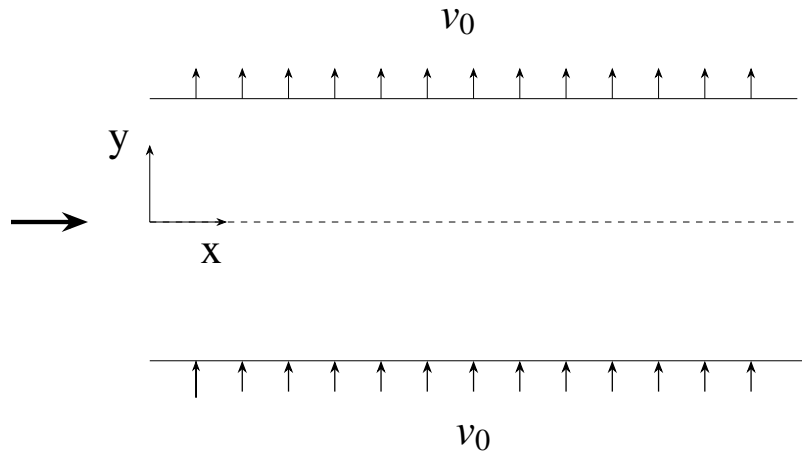


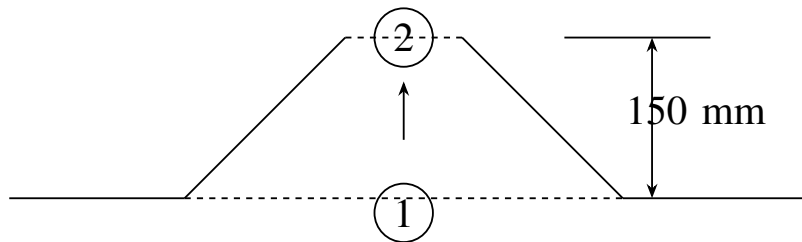
Fig (ii)

- a)  $\left. \frac{\partial u}{\partial y} \right|_A = \left. \frac{\partial u}{\partial y} \right|_B$       b)  $\left. \frac{\partial u}{\partial y} \right|_A > \left. \frac{\partial u}{\partial y} \right|_B$       c)  $\left. \frac{\partial u}{\partial y} \right|_A < \left. \frac{\partial u}{\partial y} \right|_B$       d)  $\left. \frac{\partial^2 u}{\partial y^2} \right|_A = \left. \frac{\partial^2 u}{\partial y^2} \right|_B$
- 4) Consider a fully developed, steady, incompressible, 2-D, viscous channel flow with uniform suction and blowing velocity  $v_0$  as shown in the figure below. The centerline velocity of the channel is 10

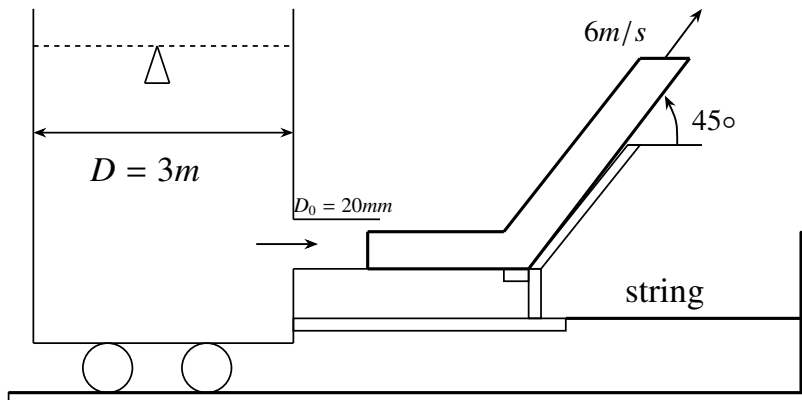
m/s along the  $x$ -direction. If the value of  $v_0$  at both the walls is 1 m/s, the value of the  $y$ -component of velocity inside the flow field is \_\_\_\_\_ m/s.



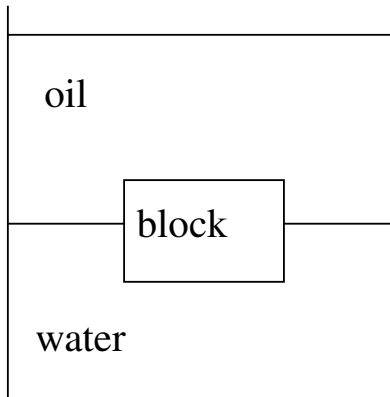
- 5) Exhaust from a kitchen goes into the atmosphere through a tapered chimney as shown. The area of cross-section of a chimney at location-1 is twice of that at location-2. The flow rate is assumed to be steady with constant exhaust density of  $1 \text{ kg/m}^3$  and acceleration due to gravity,  $g = 9.8 \text{ m/s}^2$ . If the steady uniform exhaust velocity at location-1 is  $U = 1 \text{ m/s}$ , the pressure drop across the chimney is \_\_\_\_\_ Pa.



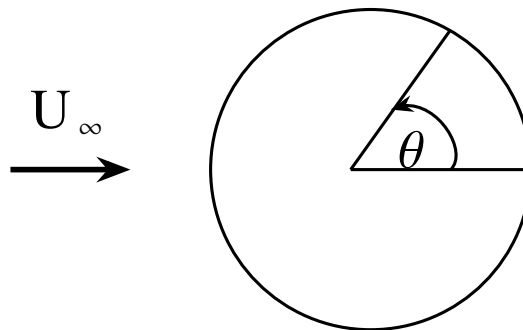
- 6) A jet of diameter 20 mm and velocity 6 m/s coming out of a water-tank standing on a frictionless cart hits a vane and gets deflected at an angle of  $45^\circ$  as shown in the figure below. The density of water is  $1000 \text{ kg/m}^3$ . Neglect all minor and viscous losses. If the cart remains stationary, the magnitude of tension in the supporting string connected to the wall is \_\_\_\_\_ N.



- 7) A block is floating at the oil-water interface as shown. The density of oil is two-thirds that of water. Given that the density of the block is  $800 \text{ kg/m}^3$  and that of water is  $1000 \text{ kg/m}^3$ , the fraction of the total height of block in oil is \_\_\_\_\_.



- 8) A horizontal pipe is feeding water into a reservoir from the top with a time-dependent volumetric flow rate,  $Q(m^3/h) = 1 + 0.1 \times t$ , where  $t$  is in hours. The area of the base of the reservoir is  $0.5m^2$ . Assuming that initially the reservoir is empty, the height of the water level in the reservoir after 60 minutes is \_\_\_\_\_ m.
- 9) Velocity field of a 2-D steady flow is provided as  $\mathbf{V} = c(x^2 - y^2)\hat{i} - 2cxy\hat{j}$ . The equation of streamlines of this flow is:
- a)  $x^2y - \frac{y^2}{3} = \text{Constant}$                       c)  $xy - \frac{y}{3} = \text{Constant}$   
b)  $xy^2 - \frac{y^2}{3} = \text{Constant}$                       d)  $x^2y - \frac{y^3}{3} = \text{Constant}$
- 10) Velocity potential and stream function in polar coordinates  $(r, \theta)$  for a potential flow over a cylinder with radius  $R$  is given as  $\phi = U_\infty \left(r + \frac{R^2}{r}\right) \cos \theta$  and  $\psi = U_\infty \left(r - \frac{R^2}{r}\right) \sin \theta$ , respectively. Here,  $U_\infty$  denotes uniform freestream velocity, and  $\theta$  is measured counter clockwise as shown in the figure. How does the velocity magnitude,  $q$ , over the surface of the cylinder will vary?



- a)  $q = 2U_\infty \cos \theta$                       c)  $q = 2U_\infty \sin 2\theta$   
b)  $q = U_\infty \cos 2\theta$                       d)  $q = 2U_\infty \sin \theta$
- 11) Consider a laminar flow of water over a flat plate of length  $L = 1 \text{ m}$ . The boundary layer thickness at the end of the plate is  $\delta_w$  for water, and  $\delta_a$  for air for the same freestream velocity. If the kinematic viscosities of water and air are  $1 \times 10^{-6} \text{ m}^2/\text{s}$  and  $1.6 \times 10^{-5} \text{ m}^2/\text{s}$ , respectively, the numerical value

of the ratio  $\frac{\delta_w}{\delta_a}$  is \_\_\_\_.

- 12) Prototype of a dam spillway (a structure used for controlled release of water from the dam) has characteristic length of 20 m and characteristic velocity of 2 m/s. A small model is constructed by keeping Froude number same for dynamic similarity between the prototype and the model. What is the minimum length-scale ratio between prototype and the model such that the minimum Reynolds' number for the model is 100? The density of water is  $1000 \text{ kg/m}^3$  and viscosity is  $10^{-3} \text{ Pa}\cdot\text{s}$ .
- a)  $1.8 \times 10^{-4}$                       b)  $1 \times 10^{-4}$                       c)  $1.8 \times 10^{-3}$                       d)  $9.1 \times 10^{-4}$
- 13) An orifice meter, having orifice diameter of  $d = \frac{20}{\sqrt{\pi}}$  mm, is placed in a water pipeline having flow rate,  $Q_{\text{act}} = 3 \times 10^{-4} \text{ m}^3/\text{s}$ . The ratio of orifice diameter to pipe diameter is 0.6. The contraction coefficient is also 0.6. The density of water is  $1000 \text{ kg/m}^3$ . If the pressure drop across the orifice plate is 43.5 kPa, the discharge coefficient of the orifice meter at this flow Reynolds number is \_\_\_\_\_.