

열역학(다)

Report #1

기계공학부, 2022****, 2학년

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작성날짜 : 2025-12-27

R1 - 1

R1 - 2

R1 - 3

R1 - 4

[R1 - 2]

$$T_1 = 300^\circ\text{C}, \quad P = 0.5 \text{ MPa} = \text{const.}, \\ m = 0.6 \text{ kg}, \quad x = 0.48$$

- (a) Find T_2 , v_2 , m_{f2} .
(b) Determine ΔV .
(c) Draw a T - v diagram.

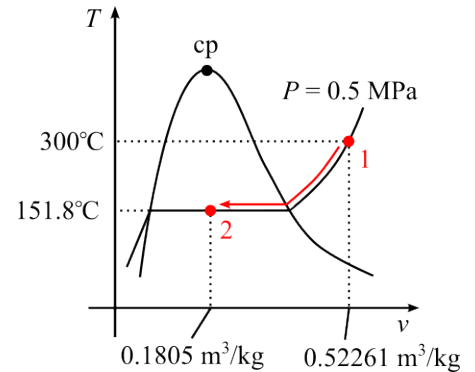
[Solution]

Before cooling,

$$P_{\text{sat}} @ 300^\circ\text{C} = 8587.9 \text{ kPa} > P = 500 \text{ kPa} \\ \Rightarrow \text{superheated vapor} \\ v_1 = v_{@ 0.5 \text{ MPa}, 300^\circ\text{C}} = 0.52261 \text{ m}^3/\text{kg}$$

After cooling,

$$0 < x < 1 \Rightarrow \text{wet vapor} \\ m_{f2} = m(1 - x) = (0.6)(1 - 0.48) = 0.312000 \\ \approx 0.3120 \text{ kg} \\ T_2 = T_{\text{sat}} @ 500 \text{ kPa} = 151.83^\circ\text{C} \\ v_{f2} = v_{f@ 500 \text{ kPa}} = 0.001093 \text{ m}^3/\text{kg} \\ v_{g2} = v_{g@ 500 \text{ kPa}} = 0.37483 \text{ m}^3/\text{kg} \\ v_2 = v_{f2} + x(v_{g2} - v_{f2}) \\ = 0.001093 + (0.48)(0.37483 - 0.001093) \\ = 0.18048676 \approx 0.18049 \text{ m}^3/\text{kg} \\ \Delta V = m(v_2 - v_1) \\ = (0.6)(0.18048676 - 0.52261) \\ = -0.205273944 \approx -0.2053 \text{ m}^3$$



[R1 - 3]

$$P_1 = P_2 = 3.5 \text{ MPa} \neq P_3, \quad T_2 = T_{\text{sat}} @ 3.5 \text{ MPa} \\ T_1 = T_2 + 5^\circ\text{C}, \quad T_3 = 200^\circ\text{C}, \quad v_1 \neq v_2 = v_3$$

- (a) Find T_1 .
(b) Find $\Delta h_{1 \rightarrow 2}$.
(c) Find P_3 and x_3 .
(d) Draw a T - v diagram.

[R1 - 1]

$$m = 1 \text{ kg}, \quad V = 0.15 \text{ m}^3 = \text{const.}, \\ P_1 = 2 \text{ MPa}, \quad T_2 = 40^\circ\text{C}$$

- (a) Find T_1 .
(b) Find P_2 .
(c) Draw a T - v diagram.

[Solution]

Before cooling,

$$v = \frac{V}{m} = 0.15 \text{ m}^3/\text{kg} \\ v_{f@ P_1} = v_{f@ 2000 \text{ kPa}} = 0.001177 \text{ m}^3/\text{kg} \\ v_{g@ P_1} = v_{g@ 2000 \text{ kPa}} = 0.099587 \text{ m}^3/\text{kg} \\ v > v_{g, @ P_1} \Rightarrow \text{superheated vapor}$$

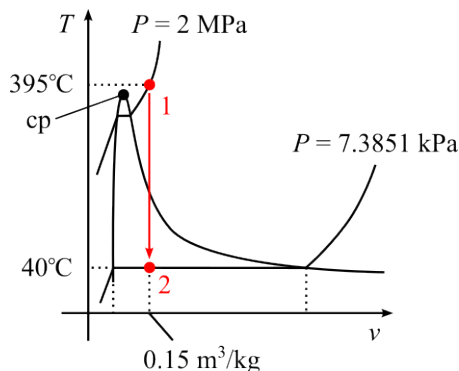
@ $P = 2 \text{ MPa}$

$T [^\circ\text{C}]$	$v [\text{m}^3/\text{kg}]$
350	0.13860
T_1	0.15000
400	0.15122

$$T_1 = \frac{400 - 350}{0.15122 - 0.13860}(0.15 - 0.13860) + 350 \\ = 395.1664025 \approx 395.17^\circ\text{C}$$

After cooling,

$$v_{f@ T_2} = v_{f@ 40^\circ\text{C}} = 0.001008 \text{ m}^3/\text{kg} \\ v_{g@ T_2} = v_{g@ 40^\circ\text{C}} = 19.515 \text{ m}^3/\text{kg} \\ v_{f@ T_2} \leq v \leq v_{g@ T_2} \Rightarrow \text{wet vapor} \\ P_2 = P_{\text{sat}} @ 40^\circ\text{C} = 7.3851 \text{ kPa}$$



[Solution]

At the state 1, it is superheated vapor. Therefore,

$$T_1 = T_{\text{sat @ 3.5 MPa}} + 5^\circ\text{C} = 242.56 + 5 = 247.56000 \\ \approx 248^\circ\text{C}$$

@ $P = 3.5 \text{ MPa}$

$T [^\circ\text{C}]$	$h [\text{kJ/kg}]$
242.56	2802.7
247.56	h_1
250.00	2829.7

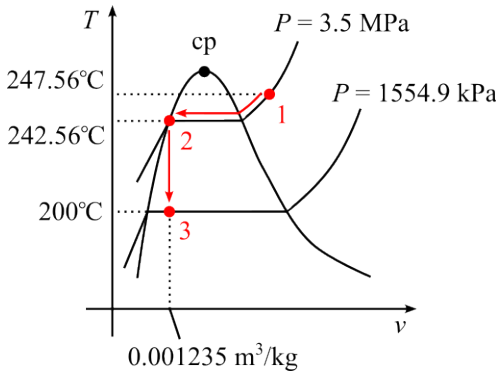
$$h_1 = \frac{247.56 - 242.56}{250 - 242.56}(2829.7 - 2802.7) + 2802.7 \\ = 2820.845161 \approx 2821 \text{ kJ/kg}$$

At the state 2, it is saturated liquid water. Therefore,

$$h_2 = h_{f@3.5 \text{ MPa}} = 1049.7 \text{ kJ/kg} \\ \Delta h_{1 \rightarrow 2} = h_2 - h_1 = 1049.7 - 2820.845161 \\ = -1771.145161 \approx -1771.1 / \text{kJ/kg} \\ v_2 = v_{f@3.5 \text{ MPa}} = 0.001235 \text{ m}^3/\text{kg}$$

At the state 3, it is wet vapor. Therefore,

$$\text{given : } T_3 = 200^\circ\text{C} \\ P_3 = P_{\text{sat @ } 200^\circ\text{C}} = 1554.9 \text{ kPa} \\ v_3 = v_2 = 0.001235 \text{ m}^3/\text{kg} \\ v_{f3} = v_{f@200^\circ\text{C}} = 0.001157 \text{ m}^3/\text{kg} \\ v_{g3} = v_{g@200^\circ\text{C}} = 0.12721 \text{ m}^3/\text{kg} \\ x_3 = \frac{v_3 - v_{f3}}{v_{g3} - v_{f3}} = \frac{0.001235 - 0.001157}{0.12721 - 0.001157} \\ = 6.187873355 \times 10^{-4} \approx 0.0619\%$$



$$= \frac{(10)(293.15)(300)}{(302.15)(170)} - 10 = 7.1214141788 \\ \approx 7.1214 \text{ kg}$$

[R1 - 4]

$$T_1 = 20^\circ\text{C}, \quad P_1 = 170 \text{ kPa}, \quad m_1 = 10 \text{ kg} \\ T_2 = 29^\circ\text{C}, \quad P_2 = 300 \text{ kPa}, \quad V = \text{const.}, \quad Z = 1$$

Determine Δm .

[Solution]

$$T_1 = (20 + 273.15) \text{ K} = 293.15 \text{ K} \\ T_2 = (29 + 273.15) \text{ K} = 302.15 \text{ K} \\ PV = mRT \Rightarrow \frac{R}{V} = \frac{P}{mT} = \text{const.} \\ \frac{P_1}{m_1 T_1} = \frac{P_2}{m_2 T_2} \Rightarrow m_2 = \frac{m_1 T_1 P_2}{T_2 P_1} \\ \Delta m = m_2 - m_1 = \frac{m_1 T_1 P_2}{T_2 P_1} - m_1$$