Introduction to Computational Fluid Dynamics using OpenFOAM and Octave

Lakshman Anumolu Kumaresh Selvakumar (Session-3)

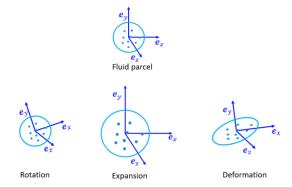
Instructions: Mon, Wed, Thu (5:30PM-6:30PM IST)

Query session: Sundays 8AM-8:30AM IST

Quick Recap

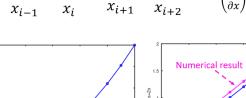
What Did We Discuss?

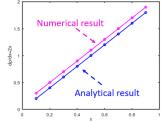
Fluid Behavior



Gradient

• Numerical Approximation





Mathematical Operations

• Divergence

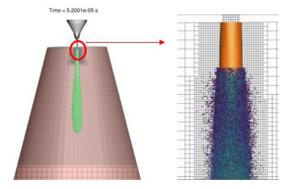
$$\nabla \cdot \boldsymbol{u} = \left(\frac{\partial}{\partial x}\boldsymbol{e}_x + \frac{\partial}{\partial y}\boldsymbol{e}_y + \frac{\partial}{\partial z}\boldsymbol{e}_z\right) \left(u\boldsymbol{e}_x + v\boldsymbol{e}_y + w\boldsymbol{e}_z\right) = \left(\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z}\right) \quad \boldsymbol{e}_y$$

- Numerical approximation
 - Same as earlier
- Physical significance
 - Positive value : Source or expansion of fluid volume
 - Negative value: Sink
 - Zero signifies incompressible nature or no change in volume

What Did We Discuss?

$$\frac{D\phi(\boldsymbol{X}(\boldsymbol{p}_i,t),t)}{Dt} = \frac{\partial\phi}{\partial t} + \frac{\partial\phi}{\partial x}\frac{DX}{Dt} + \frac{\partial\phi}{\partial y}\frac{DY}{Dt} + \frac{\partial\phi}{\partial z}\frac{DZ}{Dt}$$

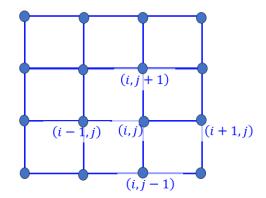
$$\frac{D\phi}{Dt} = \frac{\partial\phi}{\partial t} + \boldsymbol{u} \cdot \nabla\phi$$



Finite Difference – Finite Volume

Differential form

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0$$



Integral form

$$\frac{\partial}{\partial t} \int_{V}^{\square} \rho dV + \oint_{S}^{\square} \rho \boldsymbol{u} \cdot d\boldsymbol{S} = 0$$

	(i, j + 1))	
(i-1,j)	(i,j)	•(<i>i</i> +	1, j
	(i,j-1)		

Current Session

Overview

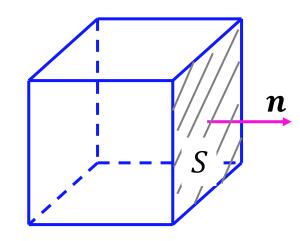
- Gauss Divergence Theorem
- Reynolds Transport Theorem

Basic Quantities

• Surface Area Vector: S

$$S = |S|n$$

$$S = Sn$$

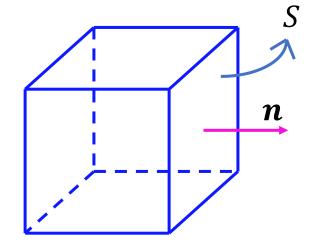


- Extensive property: Φ
- Intensive property: ϕ
 - Conserved property per unit mass
- Mass: $\rho V = \int_V \rho dV$

• For a vector: **F**

$$\int (\nabla \cdot F) dV \approx \sum F \cdot S$$

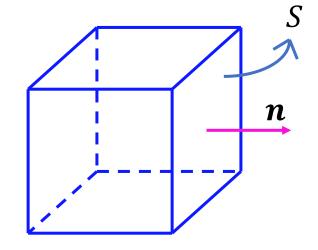
 Rate of change of a quantity over a control volume = Rate of flow through control surface.



• For a vector: **F**

$$\int (\nabla \cdot F) dV \approx \sum F \cdot S$$

Let:
$$\mathbf{F} = x\mathbf{e}_x + y\mathbf{e}_y$$



$$\int (\nabla \cdot \mathbf{F}) d\mathbf{V} = \int \left(\frac{\partial}{\partial x} \mathbf{e}_x + \frac{\partial}{\partial y} \mathbf{e}_y \right) \cdot (x \mathbf{e}_x + y \mathbf{e}_y) d\mathbf{V}$$

$$\nabla \cdot \boldsymbol{u} = \left(\frac{\partial}{\partial x}\boldsymbol{e}_x + \frac{\partial}{\partial y}\boldsymbol{e}_y + \frac{\partial}{\partial z}\boldsymbol{e}_z\right) \left(u\boldsymbol{e}_x + v\boldsymbol{e}_y + w\boldsymbol{e}_z\right) = \left(\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z}\right)$$

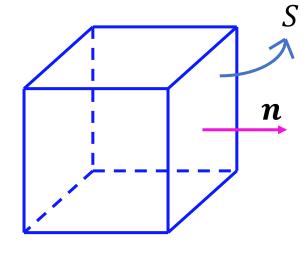
$$\int (\nabla \cdot \mathbf{F}) d\mathbf{V} \approx \sum \mathbf{F} \cdot \mathbf{S}$$
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$$= \int \left(\frac{\partial x}{\partial x} + \frac{\partial y}{\partial y}\right) dV = 2V$$

$$\sum \mathbf{F} \cdot \mathbf{S} = \sum (x\mathbf{e}_x + y\mathbf{e}_y) \cdot \mathbf{S}$$



$$S = \Delta x \Delta y$$

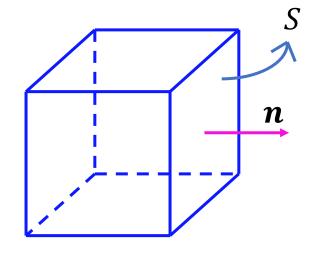
$$V = \Delta x \Delta y \Delta z$$

$$\sum \mathbf{F} \cdot \mathbf{S} = \sum (x\mathbf{e}_x + y\mathbf{e}_y) \cdot \mathbf{S}$$

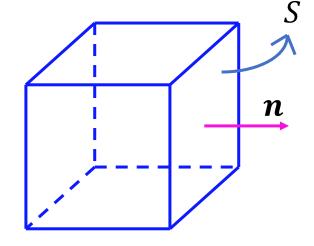
$$= \left(x + \frac{\Delta x}{2}\right)S - \left(x - \frac{\Delta x}{2}\right)S - \left(y - \frac{\Delta y}{2}\right)S + \left(y + \frac{\Delta y}{2}\right)S$$

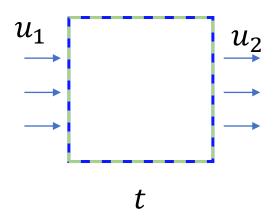


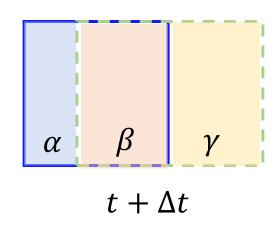
$$= 2V$$



$$\frac{d}{dt} \int_{V_S} \rho \phi dV = \frac{d}{dt} \int_{V_{CV}} \rho \phi dV + \int_{S} \rho \phi \mathbf{u} \cdot \mathbf{n} dS$$







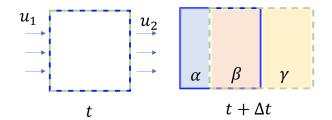
$$\frac{d}{dt} \int_{V_S} \rho \phi dV = \frac{d}{dt} \int_{V_{CV}} \rho \phi dV + \int_{S} \rho \phi \mathbf{u} \cdot \mathbf{n} dS$$

(1)
$$\Phi_S(t) = \Phi_{CV}(t)$$

(2)
$$\Phi_S(t + \Delta t) = \Phi_{CV}(t + \Delta t) - \Phi_\alpha + \Phi_V$$

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(2)
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Subtract (1) from (2)

$$\left(\frac{\Phi(t+\Delta t)-\Phi(t)}{\Delta t}\right)_{System} = \left(\frac{\Phi(t+\Delta t)-\Phi(t)}{\Delta t}\right)_{CV} - \dot{\Phi}_{\alpha} + \dot{\Phi}_{\gamma}$$

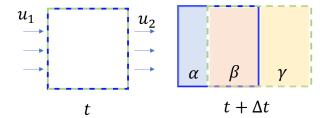
$$\frac{d\Phi}{dt}_{System} = \frac{d\Phi}{dt}_{CV} - \dot{\Phi}_{\alpha} + \dot{\Phi}_{\gamma}$$

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$$\Phi_{\alpha} = \phi_{\alpha} m_{\alpha} = \phi_{\alpha} \rho_{\alpha} V_{\alpha} = \phi_{\alpha} \rho_{\alpha} (u_1 \Delta t) S$$

Using $\Phi = \int \rho \phi dV$ and net flux as $\int \rho \phi u \cdot n dS$

$$\frac{d}{dt} \int_{V_S} \rho \phi dV = \frac{d}{dt} \int_{V_{CV}} \rho \phi dV + \int_{S} \rho \phi \boldsymbol{u} \cdot \boldsymbol{n} dS$$



Conservation Laws

Conservation of mass

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0; \quad \nabla \cdot (\rho \mathbf{u}) = \frac{\partial (\rho u)}{\partial x} + \frac{\partial (\rho v)}{\partial y} + \frac{\partial (\rho w)}{\partial z}$$

Conservation of momentum

$$\frac{\partial \rho \boldsymbol{u}}{\partial t} + \nabla \cdot (\rho \boldsymbol{u} \boldsymbol{u}) = -\nabla p + \nabla \cdot \boldsymbol{\sigma} + \rho \boldsymbol{g};$$

Scalar conservation law

$$\frac{\partial \rho \phi}{\partial t} + \nabla \cdot (\rho \boldsymbol{u} \phi) = \nabla \cdot (\Gamma \nabla \phi) + S_{\phi}$$

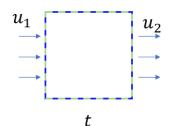
$$\frac{d}{dt} \int_{V_S} \rho \phi dV = \frac{d}{dt} \int_{V_{CV}} \rho \phi dV + \int_{S} \rho \phi \mathbf{u} \cdot \mathbf{n} dS$$

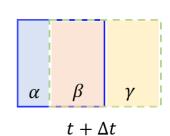
Quick Summary

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$$\int (\nabla \cdot F) dV \approx \sum F \cdot S$$

Reynolds Transport Theorem



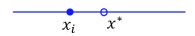


$$\frac{d}{dt} \int_{V_S} \rho \phi dV = \frac{d}{dt} \int_{V_{CV}} \rho \phi dV + \int_{S} \rho \phi \boldsymbol{u} \cdot \boldsymbol{n} dS$$

Next Session

- Taylor series analysis
- Numerical discretization

Taylor Series: Discrete Operations

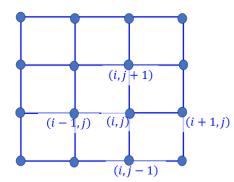


$$\rho(x^*) = \rho(x_i) + (x^* - x_i) \left(\frac{\partial \rho}{\partial x}\right)_i + (x^* - x_i)^2 \left(\frac{\partial^2 \rho}{\partial x^2}\right)_i + (x^* - x_i)^3 \left(\frac{\partial^3 \rho}{\partial x^3}\right)_i + \cdots$$

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