

SH2702
Nuclear Reactor Technology

Project work Task 5

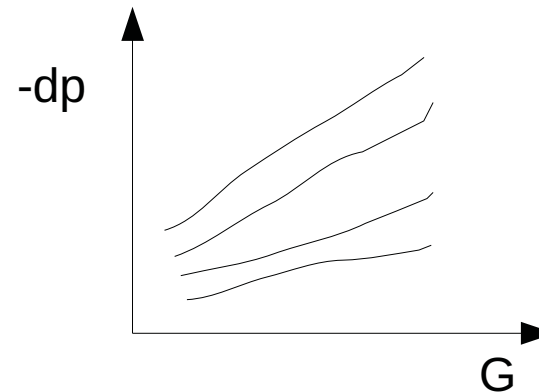
Project work

Topic numbers	Topics
1	Design, operation and safety features of NuSCALE
2	Design, operation and safety features of ABWR
3	Design, operation and safety features of ESBWR
4	Design, operation and safety features of EPR
5	Design, operation and safety features of AP1000

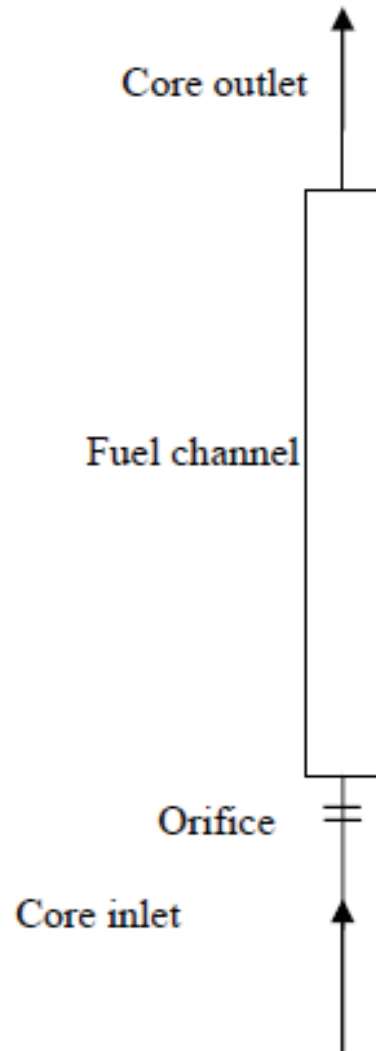
- Task 1 – General design specification of the nuclear power plant with selected reactor type
- Task 2 – Operational principles of the power plant
- Task 3 – Safety features of the power plant
- Task 4 – Calculation of selected core parameters
- Task 5 – Calculation of CHF margins in a hot channel
- Task 6 – Calculation of the maximum cladding and fuel pellet Temperature

Task 4

- 1. Data collection
 - Tables are recommended
- 2. core-averaged thermal-hydraulic calculations
 - Axial enthalpy/temperature distribution
 - Axial void fraction distribution
 - BWRs, from subcooled to saturated
 - Axial pressure distribution
 - Inlet orifices pressure loss, BWRs (50%), PWRs (25%)
 - Flow characteristic of the core $(-dp)=f(G)$
 - 0%, 50%, 100%, 150% power
 - 1% to 150% flow



Task 4

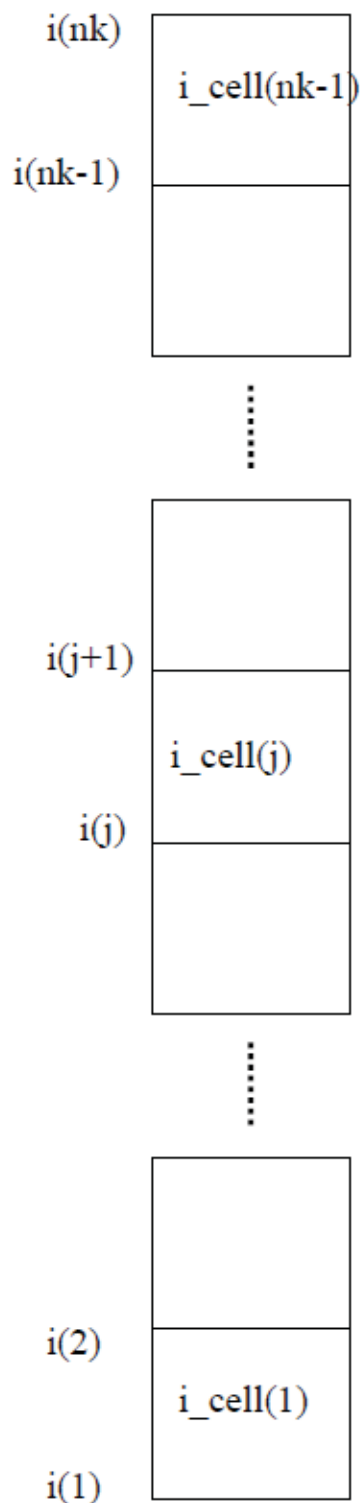


- Inlet orifices pressure loss
 - BWRs (50% at nominal operating conditions)
 - PWRs (25% at nominal operating conditions)

$$\Delta p = p_{out} - p_{in} = \Delta p_{FuelChannel} + \Delta p_{Orifice}$$

$$|\Delta p_{Orifice}| = \xi_{Orifice} \frac{\rho U^2}{2} = \xi_{Orifice} \frac{G^2}{2\rho}$$

Task 4 Nodalization and numerical solution



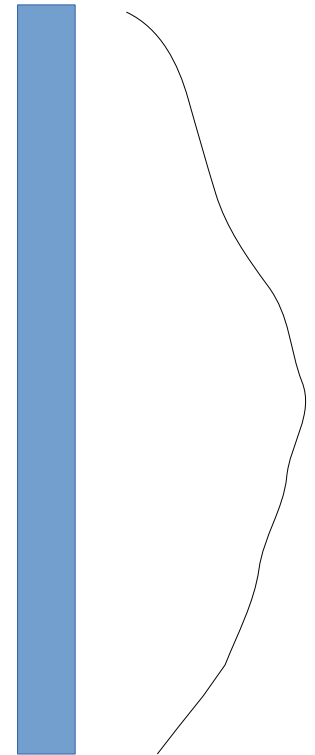
- for $j = 2$ to nk
 - $i(j) = i(j-1) + q_cell(j-1) / W$ (energy balance)
- end for
- while p not converged
 - $p(1) = p_{in} + dp_{InletOrifice}$
 - for $j = 2$ to nk
 - $xe(j), xa(j), \alpha(j)$ (void fraction model)
 - $dpf_cell(j-1), dp_g_cell(j-1), dpa_cell(j-1), dpl_cell(j-1)$
 - $dp_cell(j-1)$ (pressure drop calculation)
 - $p(j) = p(j-1) + dp_cell(j-1)$
 - end for
- end while p
- $T(j)$
 - $f(p(j), i(j))$ for subcooled water
 - $T_{sat}(j)$ for saturated water
- Inlet orifices pressure loss coefficient (designed for nominal condition)
- Flow characteristic of the core $(-dp)=f(G)$

Task 5

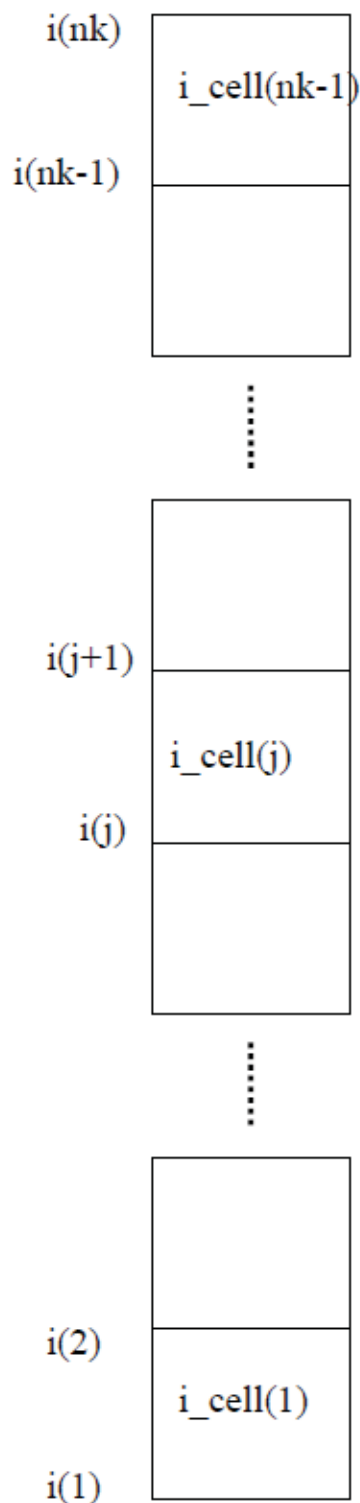
- 1. Hot channel
 - Find data on power distribution, otherwise use the simplified shape

$$q''(r, z) = q_0'' J_0 \left(\frac{2.405r}{\tilde{R}} \right) \cos \left(\frac{\pi z}{\tilde{H}} \right)$$

- Find peaking factor in radial direction
- 2. CHF
 - Find CHF, DNB for PWRs, Dryout for BWRs
 - Calculate thermal margin parameters
 - MDNBR, MCPR
- 3. Hot channel result
 - Axial enthalpy/temperature distribution
 - Axial void fraction distribution
 - BWRs, from subcooled to saturated
 - Axial pressure distribution
 - *Axial distribution of DNBR and location of MDNBR, for PWRs*

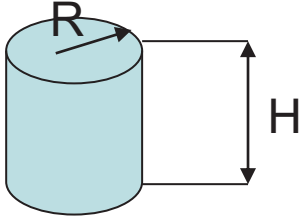
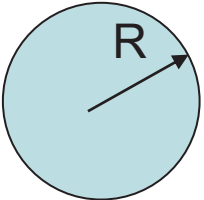
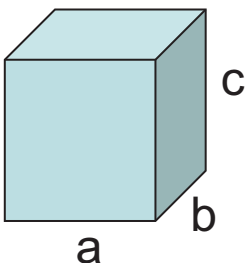


Task 5 Nodalization and numerical solution



- for $j = 2$ to nk
 - $q_cell = q_cell * fR$
 - $i(j) = i(j-1) + q_cell(j-1) / W$ (energy balance)
- end for
- while p not converged
 - $p(1) = p_{in} + dp_{InletOrifice}$
 - for $j = 2$ to nk
 - $xe(j), xa(j), \alpha(j)$ (void fraction model)
 - $dpf_cell(j-1), dp_g_cell(j-1), dpa_cell(j-1), dpl_cell(j-1)$
 - $dp_cell(j-1)$ (pressure drop calculation)
 - $p(j) = p(j-1) + dp_cell(j-1)$
 - end for
- end while p
- $T(j)$
 - $f(p(j), i(j))$ for subcooled water
 - $T_{sat}(j)$ for saturated water
- $q2cr(j), xcr(j), DNBR, CPR$

Power Distribution

	Volume	Power density distribution	Mean power density
	$V = \pi R^2 H$	$q'''(r, z) = q_0''' J_0 \left(\frac{2.405 r}{\tilde{R}} \right) \cos \left(\frac{\pi z}{\tilde{H}} \right)$	$\bar{q}''' = q_0''' \frac{2\tilde{R}}{2.405 R} J_1 \left(\frac{2.405 R}{\tilde{R}} \right) \frac{2\tilde{H}}{H\pi} \sin \left(\frac{\pi H}{2\tilde{H}} \right)$
	$V = \frac{4}{3} \pi R^3$	$q'''(r) = q_0''' \left(\frac{\tilde{R}}{\pi} \right) \frac{\sin \frac{\pi r}{\tilde{R}}}{r}$	$\bar{q}''' = 3q_0''' \left(\frac{\tilde{R}}{\pi R} \right)^2 \left[\frac{\tilde{R}}{\pi R} \sin \left(\frac{\pi R}{\tilde{R}} \right) - \cos \left(\frac{\pi R}{\tilde{R}} \right) \right]$
	$V = a \cdot b \cdot c$	$q'''(x, y, z) = q_0''' \cos \left(\frac{\pi x}{\tilde{a}} \right) \cos \left(\frac{\pi y}{\tilde{b}} \right) \cos \left(\frac{\pi z}{\tilde{c}} \right)$	$\bar{q}''' = q_0''' \frac{\tilde{a}\tilde{b}\tilde{c}}{abc} \left(\frac{2}{\pi} \right)^3 \sin \left(\frac{\pi a}{2\tilde{a}} \right) \sin \left(\frac{\pi b}{2\tilde{b}} \right) \cdot \sin \left(\frac{\pi c}{2\tilde{c}} \right)$

Peaking Factors (1)

- Peaking factor is a ratio of the maximum to average power densities in a reactor core

- Peaking factor can be calculated for the whole core volume:

$$f_V = \frac{q_0'''}{\bar{q}'''} = \frac{q'''(0,0)}{\frac{1}{V} \int_V q''' dV}$$

- In a cylindrical core, we have in addition radial and axial peaking factors:

$$f_R(z_P) = \frac{q'''(0, z_P)}{\frac{1}{\pi R^2} \int_0^R q'''(r, z_P) 2\pi r dr} \quad f_A(r_P) = \frac{q'''(r_P, 0)}{\frac{1}{H} \int_{-H/2}^{H/2} q'''(r_P, z) dz}$$

- Here z_P and r_P are fixed values of the axial and radial coordinates at which peaking factors are defined

Peaking Factors (2)

- For example for a fuel rod located at $r=r_p$ distance from the centreline, the axial peaking factor is found as:

$$f_A(r_p) = \frac{q_0''' J_0\left(\frac{2.405 r_p}{\tilde{R}}\right) \cos(0)}{\frac{1}{H} \int_{-H/2}^{H/2} q_0''' J_0\left(\frac{2.405 r_p}{\tilde{R}}\right) \cos\left(\frac{\pi z}{\tilde{H}}\right) dz} =$$

$$\frac{1}{\frac{1}{H} \int_{-H/2}^{H/2} \cos\left(\frac{\pi z}{\tilde{H}}\right) dz} = \frac{\pi H}{2 \tilde{H} \sin\left(\frac{\pi}{2} \cdot \frac{H}{\tilde{H}}\right)}$$

- As can be seen the axial peaking factor does not depend on r_p

Peaking Factors (3)

- Similarly for a core cross-section located at $z=z_p$, the radial peaking factor is found as:

$$f_R(z_p) = \frac{q_0''' J_0(0) \cos\left(\frac{\pi z_p}{\tilde{H}}\right)}{\frac{1}{\pi R^2} \int_0^R q_0''' J_0\left(\frac{2.405r}{\tilde{R}}\right) 2\pi r \cos\left(\frac{\pi z_p}{\tilde{H}}\right) dr} =$$

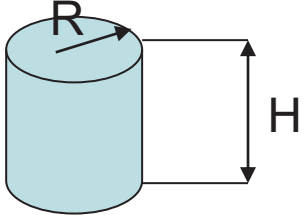
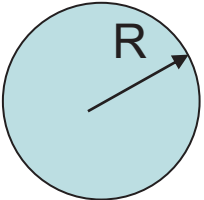
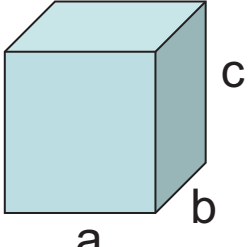
$$\frac{1}{\frac{1}{\pi R^2} \int_0^R J_0\left(\frac{2.405r}{\tilde{R}}\right) 2\pi r dr} = \frac{2.405 \cdot R}{2\tilde{R} \cdot J_1\left(\frac{2.405R}{\tilde{R}}\right)}$$

- As can be seen the radial peaking factor does not depend on z_p

Power Distribution – Peaking Factors

Mean power density

Assuming extrapolation length equal to zero

	$\bar{q}''' = q_0''' \frac{2\tilde{R}}{2.405R} J_1\left(\frac{2.405R}{\tilde{R}}\right) \frac{2\tilde{H}}{H\pi} \sin\left(\frac{\pi H}{2\tilde{H}}\right)$	$\bar{q}''' = 0.274824q_0'''$ $q_0''' = 3.63869\bar{q}'''$
	$\bar{q}''' = 3q_0''' \left(\frac{\tilde{R}}{\pi R}\right)^2 \left[\frac{\tilde{R}}{\pi R} \sin\left(\frac{\pi R}{\tilde{R}}\right) - \cos\left(\frac{\pi R}{\tilde{R}}\right) \right]$	$\bar{q}''' = \frac{3q_0'''}{\pi^2} \approx 0.303964q_0'''$ $q_0''' = 3.28986\bar{q}'''$
	$\bar{q}''' = q_0''' \frac{\tilde{a}\tilde{b}\tilde{c}}{abc} \left(\frac{2}{\pi}\right)^3 \sin\left(\frac{\pi a}{2\tilde{a}}\right) \sin\left(\frac{\pi b}{2\tilde{b}}\right) \sin\left(\frac{\pi c}{2\tilde{c}}\right)$	$\bar{q}''' = \frac{8q_0'''}{\pi^3} \approx 0.258012q_0'''$ $q_0''' = 3.87579\bar{q}'''$

Example

- Calculate the total peaking factor in a cylindrical core assuming

$$\frac{R}{\tilde{R}} \cong \frac{H}{\tilde{H}} \cong \frac{5}{6}$$

Example

•Solution:

$$f_A = \frac{\pi H}{2\tilde{H} \sin\left(\frac{\pi}{2} \cdot \frac{H}{\tilde{H}}\right)} = \frac{\pi}{2} \frac{5}{6} \frac{1}{\sin\left(\frac{\pi}{2} \frac{5}{6}\right)} \simeq 1.355$$

$$f_R = \frac{2.405 \cdot R}{2\tilde{R} \cdot J_1\left(\frac{2.405R}{\tilde{R}}\right)} = \frac{2.405}{2} \frac{5}{6} \frac{1}{J_1\left(2.405 \frac{5}{6}\right)} \simeq 1.738$$

• Answer: the total peaking factor is $f_A \cdot f_R = 2.35578$

DNB Correlations

- Correlations are derived from experimental data obtained in rod bundles

- Typical DNB correlation has a form:

$$q''_{cr} = q''_{cr} (G, p, x, D_h, L, \dots)$$

G – mass flux

p – pressure

x – quality $= (i - i_f) / i_{fg}$

D_h – hydraulic diameter

L – heated length

- That is, the correlation predicts the value of the critical heat flux (when DNB occurs) as a function of local parameters and channel geometry
- DNB occurs at location where $q'' > q''_{cr}$

Bowring Correlation

$$q_{cr}'' = \frac{A + D \cdot G \cdot \Delta i_{subi} / 4}{C + L}$$

$$A = \frac{0.579 F_{B1} D \cdot G \cdot i_{fg}}{1 + 0.0143 F_{B2} D^{1/2} G}$$

$$C = \frac{0.077 F_{B3} D \cdot G}{1 + 0.347 F_{B4} (G/1356)^n}$$

$$n = 2.0 - 0.5 p_R$$

$$p_R = \frac{p}{6.895 \cdot 10^6}$$

$$F_{B1} = \begin{cases} \frac{p_R^{18.942} \exp[20.8(1 - p_R)] + 0.917}{1.917} & p_R \leq 1 \\ p_R^{-0.368} \exp[0.648(1 - p_R)] & p_R > 1 \end{cases}$$

$$\frac{F_{B1}}{F_{B2}} = \begin{cases} \frac{p_R^{1.316} \exp[2.444(1 - p_R)] + 0.309}{1.309} & p_R \leq 1 \\ p_R^{-0.448} \exp[0.245(1 - p_R)] & p_R > 1 \end{cases}$$

$$F_{B3} = \begin{cases} \frac{p_R^{17.023} \exp[16.658(1 - p_R)] + 0.667}{1.667} & p_R \leq 1 \\ p_R^{-0.219} & p_R > 1 \end{cases}$$

$$\frac{F_{B4}}{F_{B3}} = p_R^{1.649}$$

136 < G < 18600 kg/m²s – mass flux

2 · 10⁵ < p < 190 · 10⁵ Pa – pressure

2 < D < 45 mm – diameter

0.15 < L < 3.7 m – heated length

Δi_{sub} = i_f - i_{in}, J/kg – inlet subcooling

GE Correlation for Uniform q''

(Jansen & Levy)

$$q''_{cr} = q''_{cr70} + 6.2 \cdot 10^3 (70 - p)$$

$$q''_{cr70} = \begin{cases} 10^6 (2.24 + 0.55 \cdot 10^{-3} G) & \text{if } x < x_1 \\ 10^6 (5.16 - 0.63 \cdot 10^{-3} G - 14.85x) & \text{if } x_1 \leq x < x_2 \\ 10^6 (1.91 - 0.383 \cdot 10^{-3} G - 2.06x) & \text{if } x_2 \leq x \end{cases}$$

$$x_1 = 0.197 - 0.08 \cdot 10^{-3} G$$

$$x_2 = 0.254 - 0.019 \cdot 10^{-3} G$$

q''_{cr} - critical quality, [W/m²]

G – mass flux, [kg/m² s]

x – equilibrium quality

p – pressure [bar]

Applicability range:

42 < p < 102 bar

540 < G < 8100 kg/m²s

0.0 < x < 0.45

6.2 < D_h < 32 mm

0.74 < L < 2.8 m

Westinghouse Correlation for Uniform q'' : W-3

$$q''_{cr,U}(z) = A \left\{ (2.022 - 0.0004302 p_R) + (0.1722 - 0.0000984 p_R) e^{[(18.177 - 0.004129 p_R)x]} \right\} \times \\ \left[(0.1484 - 1.596x + 0.1729x|x|) G_R + 1.037 \right] (1.157 - 0.869x) \times \\ (0.2664 + 0.8357 e^{-3.151 D_e}) (0.8258 + 0.000794 \Delta i_R) \quad \text{in MW/m}^2$$

$$p_R = \frac{p(z)}{6.8947 \cdot 10^3}$$

$p(z)$ – pressure at
location z , Pa

$$\Delta i_R = \frac{i_f - i_{in}}{2326}$$

i_f – specific enthalpy
at saturation, J/kg
 i_{in} – specific enthalpy
at inlet, J/kg

$$G_R = \frac{G(z)}{1.3562 \cdot 10^3}$$

$G(z)$ - mass flux at
location z , kg/m²s

$$A = 3.1544$$

$$D_e = \frac{D_h}{0.0254}$$

D_h - hydraulic
diameter, m

Validity range:

$$5.5 < p < 16 \text{ MPa}$$

$$1356 < G < 6800 \text{ kg/m}^2\text{s}$$

$$5 < D_h < 18 \text{ mm}, \quad 0.254 < L < 3.7 \text{ m}$$

$$-0.15 < x < 0.15$$

Effect of Non-Uniform Power Distribution

- GE correlation by Jansen and Levy is commonly used for PWR conditions with uniform heat distribution along the channel
- For non-uniform power distribution the W-3 correlation is applicable, where the following correction factor has to be applied:

$$F_c(z) \equiv \frac{q''_{cr,U}(z)}{q''_{cr,NU}(z)} = \frac{C}{q''(z)(1 - e^{-C \cdot z})} \int_0^z q''(z') e^{-C(z-z')} dz'$$

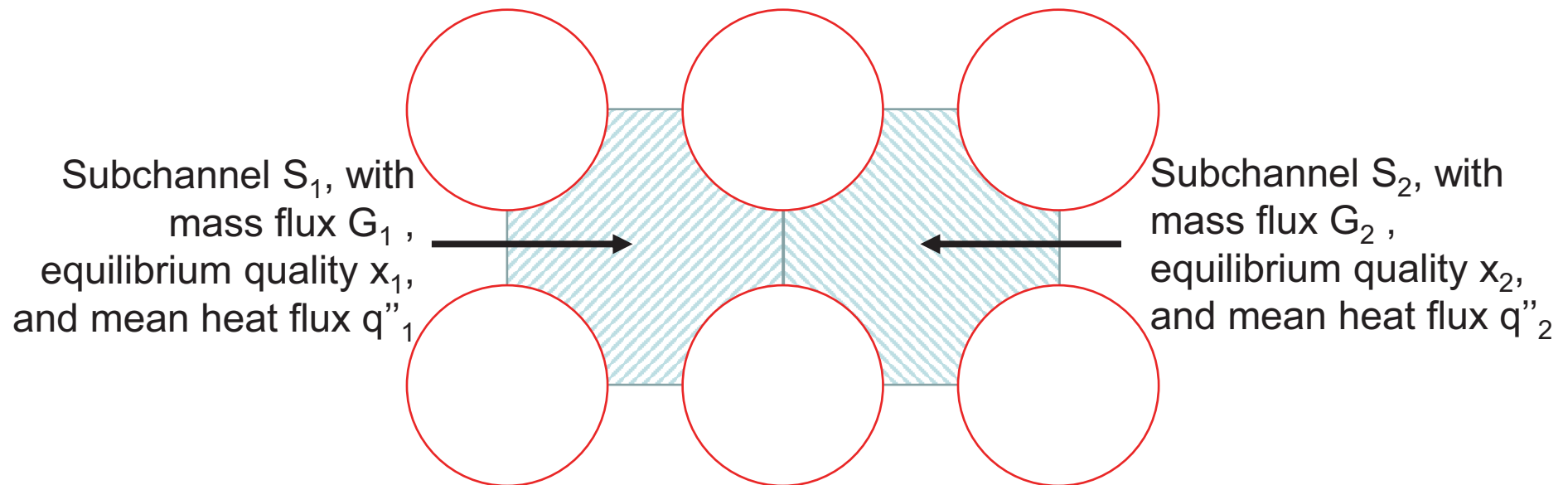
$q''_{cr,U}(z)$ - critical heat flux found with uniform power distribution, MW/m²

$$C = 185.6 \frac{(1 - x_{cr,NU})^{4.31}}{G^{0.478}}$$

$x_{cr,NU}$ – equilibrium quality at DNB location found with non-uniform power distribution
 G – mass flux, kg/m²s

Subchannel DNB

- The DNB correlations discussed so far are applicable to whole bundle
- Sometime a more detailed approach is required, in which conditions in individual subchannels are considered



Subchannel CHF Correlation

- Reddy and Fighetti developed a generalized subchannel CHF correlation for both PWR and BWR fuel assemblies (both DNB and dryout)

$$q''_{cr}(\mathbf{r}) = B \frac{A - x_{in}}{C + \frac{x(\mathbf{r}) - x_{in}}{q''_R(\mathbf{r})}}$$

$$A = a_1 p_R^{a_2} G_R^{(a_3 + a_4 p_R)} \quad G_R = G / 1356.23$$

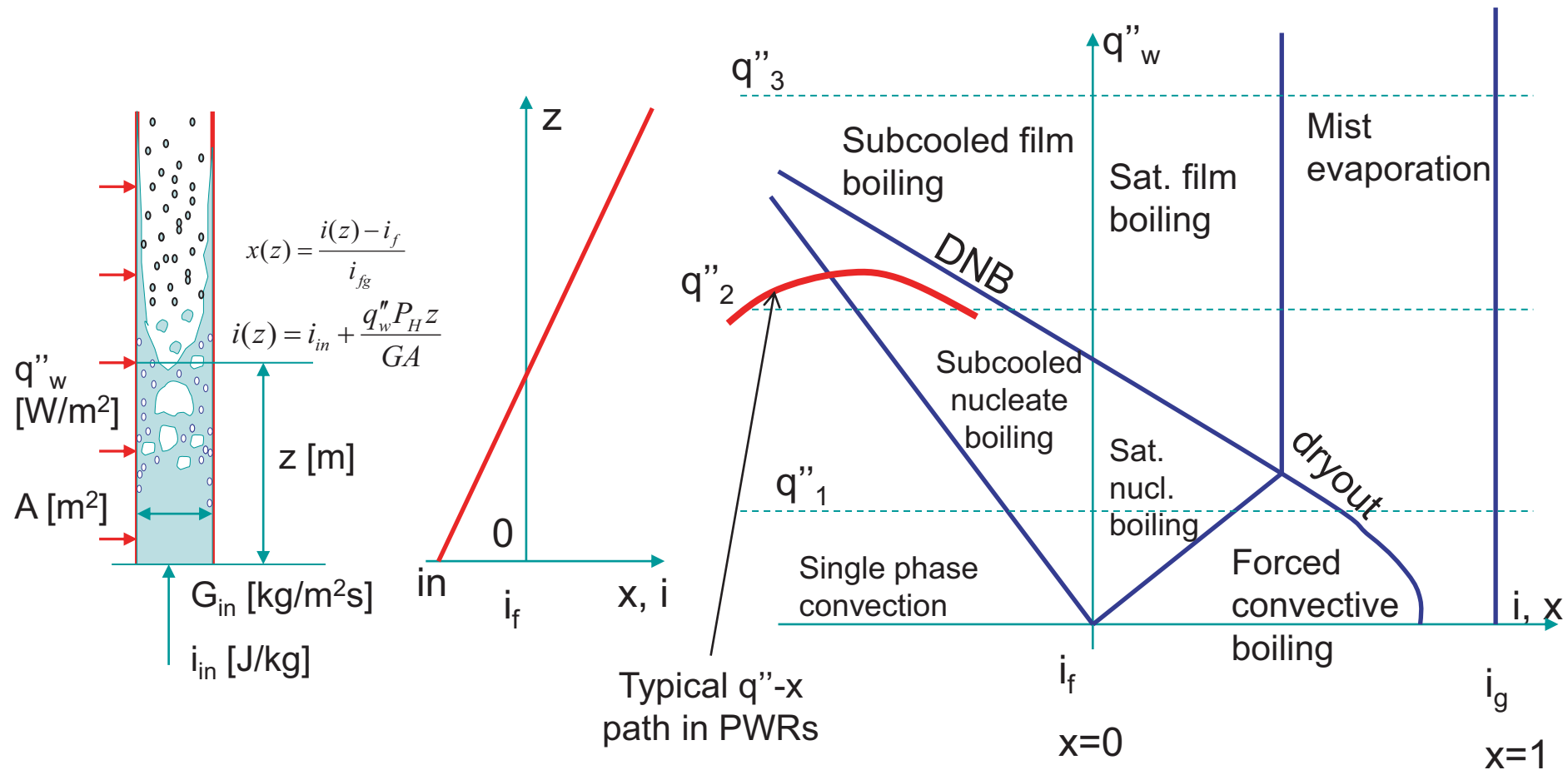
$$B = 3.1544 \times 10^6 \quad p_R = p / p_{cr}$$

$$C = c_1 p_R^{c_2} G_R^{(c_3 + c_4 p_R)} \quad q''_R(\mathbf{r}) = q''(\mathbf{r}) / 3.1544e6$$

q_{cr} – critical heat flux, W/m², x_{in} – inlet equilibrium quality, G – mass flux, kg/m²s, p – pressure, Pa, p_{cr} – critical pressure, Pa, $a_1 = 0.5328$, $a_2 = 0.1212$, $a_3 = -0.3040$, $a_4 = 0.3285$, $c_1 = 1.6151$, $c_2 = 1.4066$, $c_3 = 0.4843$, $c_4 = -2.0749$, \mathbf{r} - location

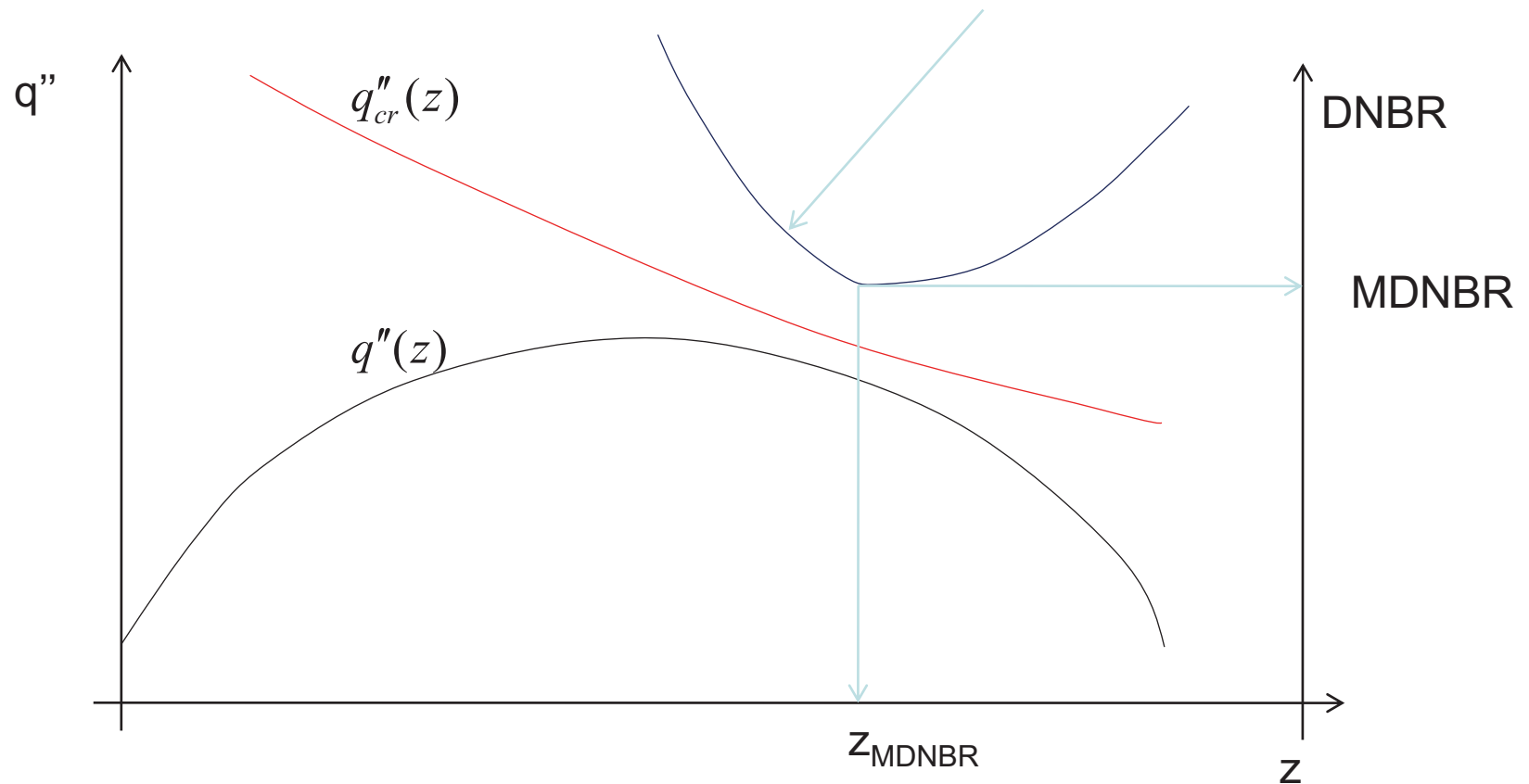
Applicability range: $147 < G < 3023$ kg/m²s, $13.8 < p < 169.9$ bar, $8.9 < D_h < 13.9$ mm, $6.3 < D_H < 13.9$ mm, $-0.25 < x < 0.75$, $-1.10 < x_{in} \leq 0.0$, $0.762 < L < 4.267$ m

Boiling Regimes on q'' - x Plain



DNB Ratio - DNBR

- DNB Ratio (DNBR) is defined as: $DNBR(z) = \frac{q''_{cr}(z)}{q''(z)}$



DNBR, MNDBR and z_{MNDBR}

- DNBR is a local parameter function
- DNBR(z) has to be calculated along the whole assembly
- The minimum value of DNBR is called Minimum DNBR (MDNBR)
- Both MDNBR and its location z_{MNDBR} need to be determined for a bundle or subchannel when predicting thermal margins

Dryout (1)

- Dryout occurs in channels with high quality
- This type of CHF is a concern in BWRs
- Typical dryout correlation has a form

$$x_{cr} = x_{cr}(G, p, D_h, L_B, \dots)$$

- That is, the correlation predicts the quality at which dryout occurs

Dryout (2)

- Example of a dryout correlation – Levitan-Lantsman

$$x_{cr}|_{8mm} = \left[0.39 + 1.57 \frac{p}{98} - 2.04 \left(\frac{p}{98} \right)^2 + 0.68 \left(\frac{p}{98} \right)^3 \right] \left(\frac{G}{1000} \right)^{-0.5} \quad x_{cr} = x_{cr}|_{8mm} \cdot \left(\frac{8}{D_h} \right)^{0.15}$$

p – pressure (bar), G mass flux (kg/m².s), D_h – hydraulic diameter, mm

- To predict the dryout it is thus necessary to find quality in a channel and compare it with the critical value
- Dryout will occur if at any point: $x(z) \geq x_{cr}(z)$

CISE Correlation

- Original CISE correlation was developed for tubes
- General Electric extended the correlation to rod bundles based on their experimental data

$$x_{cr} = \frac{A \cdot L_B^*}{B + L_B^*} \left(\frac{1.24}{R_f} \right) \quad L_B^* = L_B / 0.0254 \quad L_B - \text{boiling length in [m]}$$

$$R_f - \text{radial peaking factor, [-]}$$

$$A = 1.055 - 0.013 \left(\frac{p_R - 600}{400} \right)^2 - 1.233 G_R + 0.907 G_R^2 - 0.285 G_R^3 \quad G_R = G / 1356.23$$

$$B = 17.98 + 78.873 G_R - 35.464 G_R^2$$

$$p_R = p / 6894.757$$

Valid for 7x7 bundle; B=B/1.12 for 8x8 bundle

G [kg/m².s]; p [Pa]

Hench and Gillis Correlation

$$x_{cr} = \frac{0.50 \cdot G_R^{-0.43} \cdot Z}{165 + 115 \cdot G_R^{2.3} + Z} \times \left[2 - J_1 + \frac{0.19}{G_R} (J_1 - 1)^2 + J_3 \right] + 0.006 - 0.0157 p_R - 0.0714 p_R^2$$

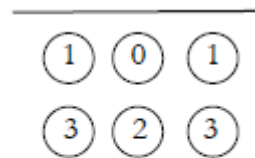
$G_R = G/1356.23$ G – mass flux, kg/m²s

$Z = n \pi d_r L_B / A$ n – number of rods, d_r – rod diameter, m; L_B – boiling length, m

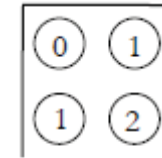
$p_R = (p / 6894.7 - 800) / 1000$ A – bundle flow area, m², p – pressure, Pa

$$J_1 = \begin{cases} \frac{1}{32} (25R_{f0} + 3 \sum R_{f1} + R_{f2}) & \text{for corner rods} \\ \frac{1}{32} (22R_{f0} + 3 \sum R_{f1} + 2R_{f2} + \sum R_{f3}) & \text{for side rods} \\ \frac{1}{32} (20R_{f0} + 2 \sum R_{f1} + \sum R_{f2}) & \text{for central rods} \end{cases}$$

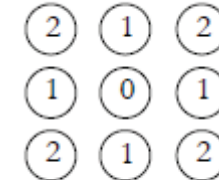
$$J_3 = \begin{cases} 0 & \text{for corner rods} \\ \frac{0.07}{G_R + 0.25} - 0.05 & \text{for side rods} \\ \frac{0.14}{G_R + 0.25} - 0.10 & \text{for central rods} \end{cases}$$



Side



Corner



Center

Critical Power Ratio - CPR

- CPR (Critical Power Ratio) for a fuel assembly is defined as:

$$\text{CPR} = q_{\text{cr}}/q_{\text{ac}}$$

here: q_{cr} [W] is the total power of a bundle at which dryout occurs

q_{ac} [W] is the actual power of the bundle