#### Lectures on Thermal-Hydraulics in Nuclear Energy Engineering

Lecture No 03

Title:

TH Design of Fuel Assemblies with Variable Thermal Conductivity

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#### Outline of the Lecture

- Heat conduction and temperature distribution in fuel rods with temperature-dependent thermal conductivity
- Fuel restructuring
- Fuel-cladding gap behavior
- Cladding thermal analysis
- Coolant-to-cladding heat transfer with crud deposition

- The following assumptions are made in the thermal analysis:
  - radial distribution of heat sources in a pin is uniform (no neutronic self-shielding within a pin)
  - heat conduction in the axial direction is small and can be neglected
- With theses assumptions, the conduction equation in a fuel pin is as follows:

$$\frac{1}{r}\frac{d}{dr}\left(r\lambda_F\frac{dT_F(r)}{dr}\right) = -q'''(z)$$

Fuel element

 $r_{Co}$ 

Fuel

Gas gap

Clad

The following two boundary conditions are needed:

(1) 
$$\frac{dT_F}{dr}\Big|_{r=0} = 0$$
 Symmetry at the centerline

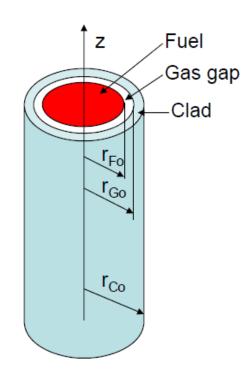
$$(2) T_F \big|_{r=r_{Fo}} = T_{Fo}$$

(2)  $T_F|_{r=r_{Fo}} = T_{Fo}$  Constant temperature at pellet surface

Integration of the equation yields

$$r\lambda_F \frac{dT_F(r)}{dr} + q'''(z)\frac{r^2}{2} = C_1$$

and from boundary condition (1),  $C_1 = 0$ .



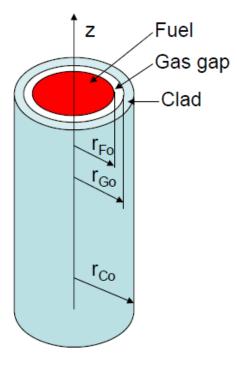
Fuel element

The second integration yields:

$$\int_{T(r)}^{T_{Fo}} \lambda_F dT_F + q'''(z) \int_r^{r_{Fo}} \frac{r}{2} dr = 0$$

 We can see that if the thermal conductivity as a function of temperature is known and the temperature at the pellet surface is given, temperature at any radius r can be found from the following equation:

$$\int_{T_{Fo}}^{T(r)} \lambda_F dT_F = \frac{q'''(z)}{4} (r_{Fo}^2 - r^2)$$



Fuel element

In particular, for r = 0 (at the centerline) we get:

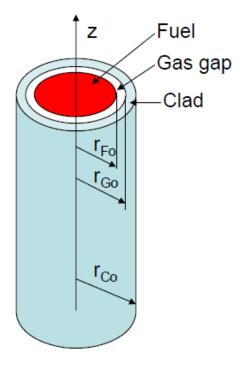
$$\int_{T_{Fo}}^{T_{Fc}} \lambda_F dT_F = \frac{q'''(z)r_{Fo}^2}{4}$$
 T<sub>Fc</sub> – temperature at the centerline

 We can introduce into this equation the linear power q', which is related to the power density q" as follows:

$$q'(z) = q'''(z)\pi r_{Fo}^2$$

Thus:

$$q'(z) = 4\pi \int_{T_{Fo}}^{T_{Fc}} \lambda_F dT_F$$



Fuel element

 We obtained a relationship between the linear power and the fuel maximum temperature (at centerline):

$$q'(z) = 4\pi \int_{T_{Fo}}^{T_{Fc}} \lambda_F dT_F$$

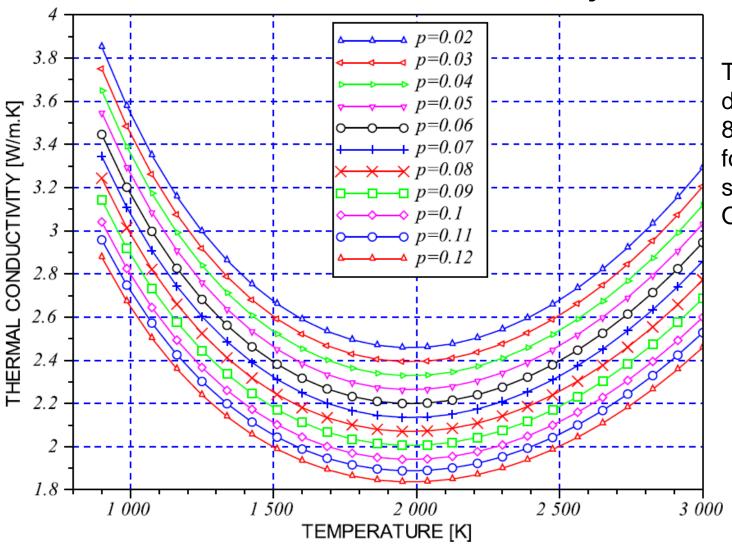
- However, to find the value of q', we need to perform the integration. For that, we need to know the function  $\lambda_F(T_F)$
- For various types of fuels, this function is given in analytical form based on experimental data

 For mixed oxide fuel (80% U, 20% Pu) at 95% theoretical density and O/M (oxigen/metal)=2.0, the fuel thermal conductivity can be given as (Washington, 1973)

$$\lambda_F(T) = (0.042 + 2.71 \times 10^{-4} T)^{-1} + 6.9 \times 10^{-11} T^3$$

where  $\lambda_F$  is in W/m·K and T in K. For porosity different from 5%, the thermal conductivity is found as:

$$\lambda_{Fp}(T) = \begin{cases} \lambda_{F}(T) \frac{1 - 2.5p}{0.875} & p \le 0.1\\ \lambda_{F}(T) \frac{1 - p}{0.875(1 + 2p)} & p > 0.1 \end{cases}$$



Thermal conductivity of 80% U+20% Pu for various porosities p, with O/M=2.0

- Typical design tasks for fuel pin can be as follows:
  - (1) given linear power and pellet surface temperature, find the pellet maximum temperature at the centerline
  - (2) knowing the pellet surface temperature and the fuel melting temperature, calculate the maximum allowed linear power before fuel starts melting
- To solve (1), we use a so-called **conductivity integral**,

$$I_C(T) \equiv \int_{T_{ref}}^T \lambda_F dT_F$$

 $T_{ref}$  – arbitrary reference temperature

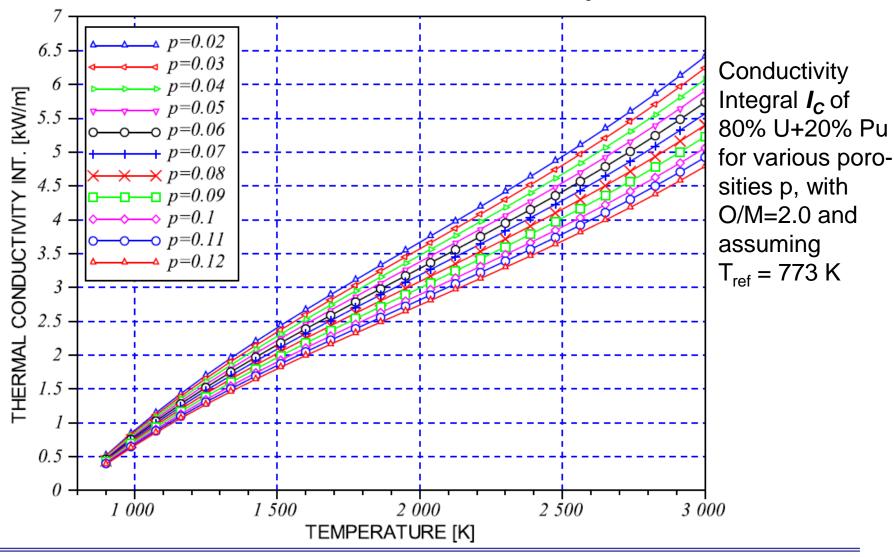
Using the conductivity integral, we have:

$$q'(z) = 4\pi \int_{T_{Fo}}^{T_{Fc}} \lambda_F dT_F = 4\pi \left( \int_{T_{ref}}^{T_{Fc}} \lambda_F dT_F + \int_{T_{Fo}}^{T_{ref}} \lambda_F dT_F \right) = 4\pi \left( \int_{T_{ref}}^{T_{Fc}} \lambda_F dT_F - \int_{T_{ref}}^{T_{Fo}} \lambda_F dT_F \right) = 4\pi \left[ I_C(T_{Fc}) - I_C(T_{Fo}) \right]$$

 The conductivity integral can be obtained in an analytical form (for 80%U+20%Pu with porosity 5%) as follows:

$$I_{C}(T) = \int_{T_{ref}}^{T} \lambda_{F} dT_{F} = \frac{1}{2.71 \times 10^{-4}} \ln(0.042 + 2.71 \times 10^{-4}T) + \frac{6.9 \times 10^{-11}}{4} T^{4}$$
$$-\frac{1}{2.71 \times 10^{-4}} \ln(0.042 + 2.71 \times 10^{-4}T_{ref}) - \frac{6.9 \times 10^{-11}}{4} T_{ref}^{4}$$

This function is often represented in a graph (for various porosities)



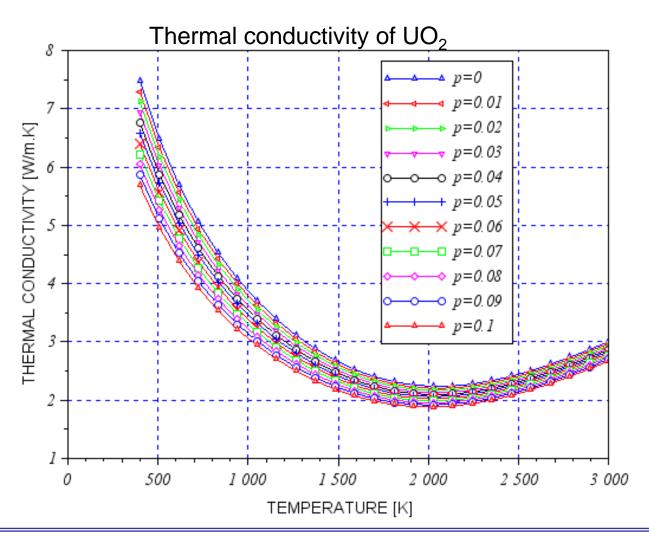
 For solid UO<sub>2</sub> with 95% density the recommended equation for the thermal conductivity is

$$\lambda_F(T) = \frac{100}{7.5408 + 17.692t + 3.6142t^2} + \frac{6400}{t^{5/2}} \exp\left(-\frac{16.35}{t}\right)$$

• where  $\lambda_F$  is in W/m·K, t = T/1000 and T is temperature in K. For porosity different from 5%, the thermal conductivity is found as:

$$\lambda_0 = \frac{\lambda_p}{1 - (2.6 - 0.5t)p}$$
 Here  $\lambda_0$  is the thermal conductivity of fully dense UO<sub>2</sub> (that is p = 0) and  $\lambda_p$  is the thermal conductivity of UO<sub>2</sub> with porosity p.

$$\lambda_p = \lambda_0 \left[ 1 - \left( 2.6 - 0.5t \right) p \right] = \lambda_F(T) \frac{1 - \left( 2.6 - 0.5t \right) p}{1 - \left( 2.6 - 0.5t \right) 0.05}$$



Conductivity integral to melt (CIM) is defined as

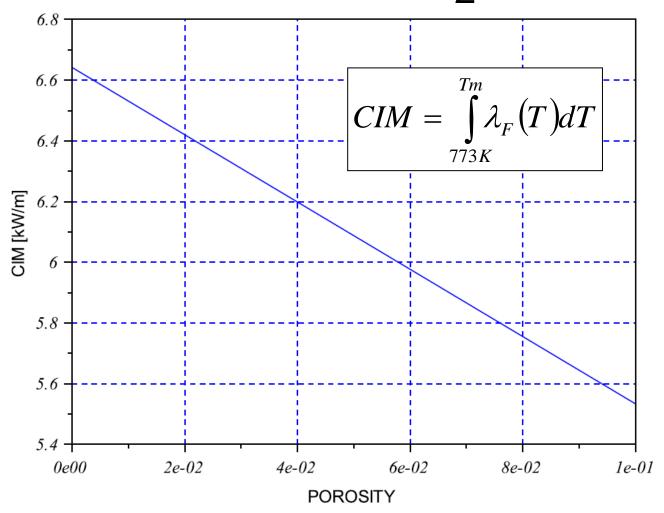
$$CIM = \int_{773K}^{Tm} \lambda_F(T) dT$$

Here  $T_m$  is the melting temperature of  $UO_2$  (3120 K ±30K)

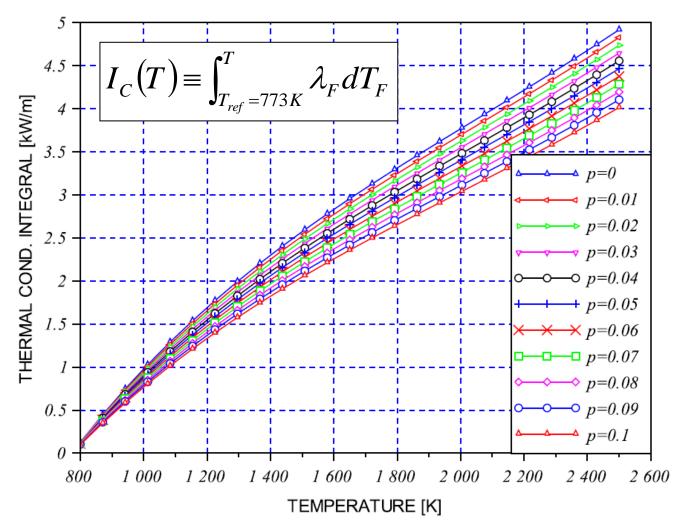
The linear power density at which fuel will start melting is thus related to CIM as follows

$$q'_{m}(z) = 4\pi \int_{T_{Fo}}^{T_{m}} \lambda_{F} dT_{F} = 4\pi \left( \int_{773K}^{T_{m}} \lambda_{F} dT_{F} - \int_{773K}^{T_{Fo}} \lambda_{F} dT_{F} \right) = 4\pi \left( CIM - \int_{773K}^{T_{Fo}} \lambda_{F} dT_{F} \right) = 4\pi \left[ CIM - I_{C}(T_{Fo}) \right]$$

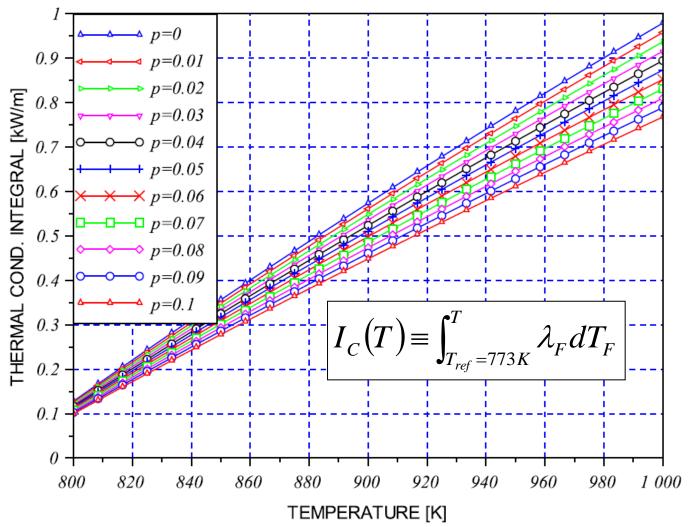
## CIM for UO<sub>2</sub>



# Conductivity Integral for UO<sub>2</sub>



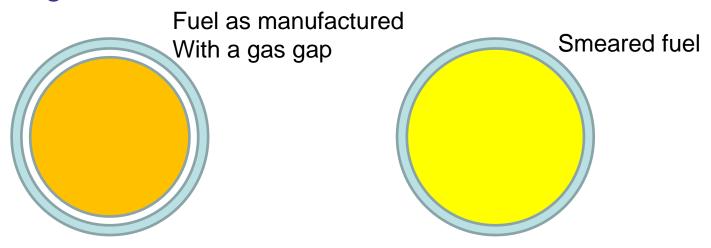
# Conductivity Integral for UO<sub>2</sub>



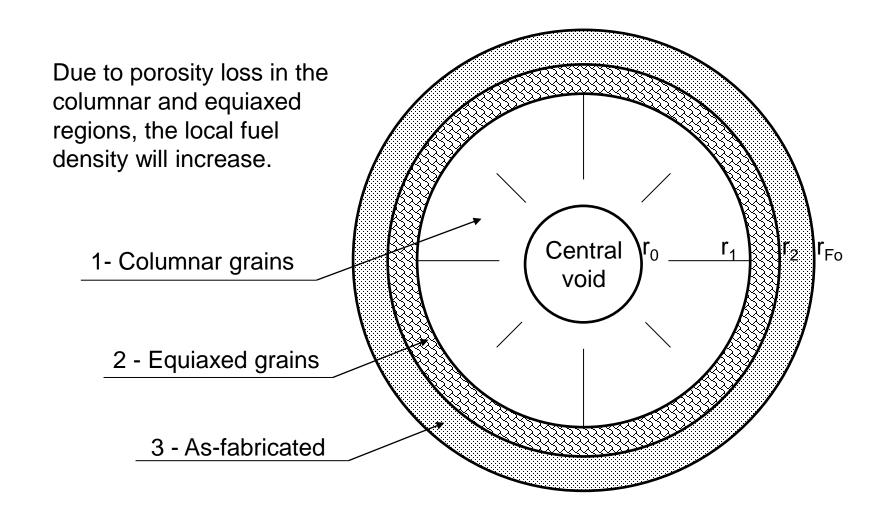


### **Fuel Smeared Density**

- A parameter called smear density is used in calculating atom densities for the fuel
- The smeared density is the density of the fuel if it were uniformly spread or smeared throughout the inside of the cladding



- Metal, carbide and nitride fuels do not restructure and the previously discussed procedure holds
- Mixed oxide fuels do restructure at high temperatures and this must be taken into account in the thermal analysis, especially for fast reactors, where fuel may have higher temperature near the center
- The most important effects are creation of central void, changes in thermal conductivity, density and volumetric heat generation rates in the columnar and equiaxed regions (see next slide)



- Density change in regions 1 and 2 are causing changes of the volumetric power density
- Since the linear power is not affected by fuel restructuring, the volumetric power densities in regions 1 through 3 are as follows:

$$q_{3}''' = q''' = \frac{q'}{\pi r_{Fo}^{2}} \qquad \frac{q_{1}'''}{q'''} = \frac{\rho_{1}}{\rho_{3}} \Rightarrow q_{1}''' = \frac{q'}{\pi r_{Fo}^{2}} \frac{\rho_{1}}{\rho_{3}} \qquad q_{2}''' = \frac{q'}{\pi r_{Fo}^{2}} \frac{\rho_{2}}{\rho_{3}}$$

 With these new values, conductivity equation can be solved in each region

 The radii and the densities in the restructured regions are related according to the following mass conservation equation

$$\rho_1(r_1^2 - r_0^2) + \rho_2(r_2^2 - r_1^2) = \rho_3 r_2^2$$

 Using this, one can solve conductivity equations in all regions. In region 3 (unrestructured fuel) we get:

$$\lambda_{F3} \frac{dT}{dr}\Big|_{r_{Fo}} = -\frac{q'''r}{2}\Big|_{r_{Fo}} + \frac{C}{r}\Big|_{r_{Fo}} = -\frac{q'''r_{Fo}}{2} \Rightarrow C = 0 \quad \Longrightarrow \quad \int_{T_{Fo}}^{T_2} \lambda_{F3} dT = \frac{q'}{4\pi} \left[ 1 - \left(\frac{r_2}{r_{Fo}}\right)^2 \right]$$

here  $T_2$  is the temperature at  $r=r_2$ 

In region 2 (equiaxed fuel) we get:

$$\int_{T_2}^{T_1} \lambda_{F2} dT = \frac{q'}{4\pi} \frac{\rho_2}{\rho_3} \left(\frac{r_2}{r_{Fo}}\right)^2 \left[ 1 - \left(\frac{r_1}{r_2}\right)^2 - 2\left(1 - \frac{\rho_3}{\rho_2}\right) \ln \frac{r_2}{r_1} \right]$$

here T<sub>1</sub> is the temperature at r=r<sub>1</sub>

• In region 1 (columnar fuel) we have:

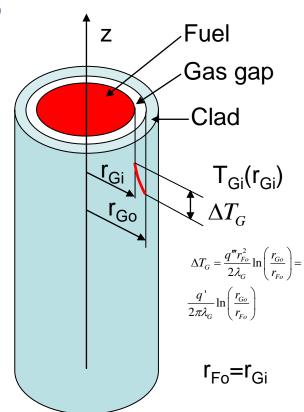
$$\int_{T_1}^{T_0} \lambda_{F1} dT = \frac{q'}{4\pi} \frac{\rho_1}{\rho_3} \left(\frac{r_1}{r_{Fo}}\right)^2 \left[1 - \left(\frac{r_0}{r_1}\right)^2 - 2\left(\frac{r_0}{r_1}\right)^2 \ln \frac{r_1}{r_0}\right]$$

here  $T_0$  is the fuel temperature at  $r=r_0$ 

- T<sub>0</sub> is the fuel maximum temperature, which should be found from the known linear power density and fuel outer surface temperature
- The procedure is as follows:
  - knowing q' and  $T_{Fo}$ , find  $T_2$  from  $\int_{T_{Fo}}^{T_2} \lambda_{F3} dT = \frac{q'}{4\pi} \left| 1 \left( \frac{r_2}{r_{Fo}} \right)^2 \right|$  using graph
  - in a similar manner find  $T_1$  from  $\int_{T_2}^{T_1} \lambda_{F2} dT = \frac{q'}{4\pi} \frac{\rho_2}{\rho_3} \left(\frac{r_2}{r_{Fo}}\right)^2 \left[1 \left(\frac{r_1}{r_2}\right)^2 2\left(1 \frac{\rho_3}{\rho_2}\right) \ln \frac{r_2}{r_1}\right]$
  - and finally  $T_0$  from  $\int_{T_1}^{T_0} \lambda_{F_1} dT = \frac{q'}{4\pi} \frac{\rho_1}{\rho_3} \left(\frac{r_1}{r_{F_0}}\right)^2 \left[1 \left(\frac{r_0}{r_1}\right)^2 2\left(\frac{r_0}{r_1}\right)^2 \ln \frac{r_1}{r_0}\right]$

- To determine fuel temperature at the center it is necessary to know the fuel pellet outer temperature  $T_{\rm Fo}$
- This temperature can be determined through a consideration of heat transfer through the fuel-cladding gap, through cladding and liquid film to the bulk coolant
- Of these three heat transfer barriers, the gap provides the greatest resistance to heat flow
- Initially, in unirradiated fuel, the gap is open and temperature drop through it is twice as big as two others

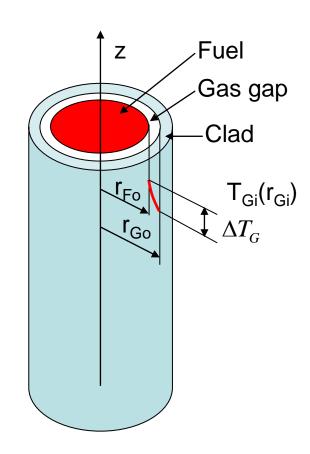
- After short period of irradiation the gap closes due to fuel swelling
- Assuming first the gap as-fabricated and filled with a stationary gas mixtture, the temperature drop in the gap can be calculated from a solution of the conduction equation
- We then assume that the thermal conductivity  $\lambda_G$  of gas mixture is constant and known



Fuel element

 The temperature drop through the fuel-cladding gap is then

$$\Delta T_G = \frac{q'}{2\pi\lambda_G} \ln\left(\frac{r_{Go}}{r_{Fo}}\right)$$



Fuel element

In calculations, an equivalent gap heat transfer
 coefficient (called gap conductance) h<sub>G</sub> is introduced:

$$q' = h_G 2\pi r_{Fo} \Delta T_G$$

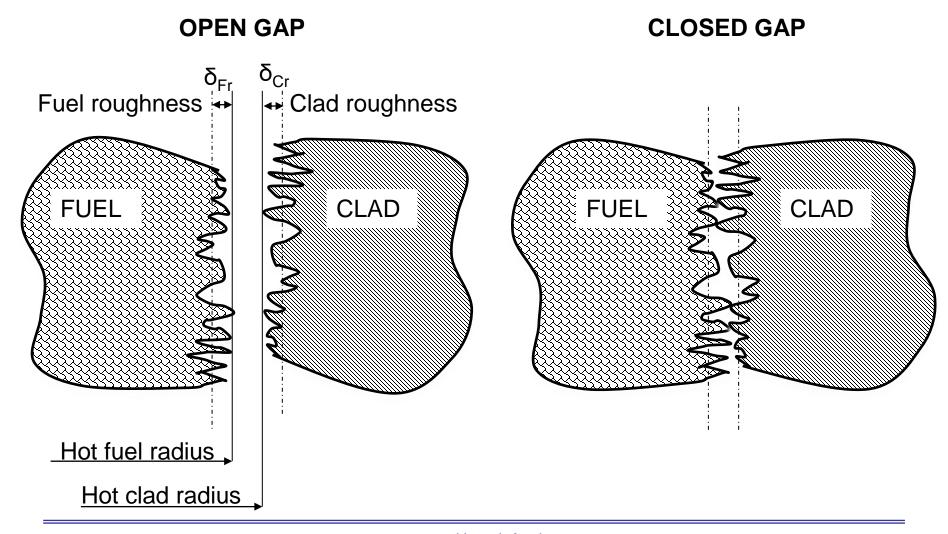
 In this equation the curvature effects are neglected and the gap conductance for open gap is approximated as:

$$h_G \approx \frac{\lambda_G}{\delta_G}$$

• Here  $\delta_G = r_{Go} - r_{Fo}$  is the gap thickness

- More exact expressions for open gap conductance take into account the wall roughness
- Reported wall roughness for both cladding and fuel vary in a range from 10<sup>-4</sup> to 10<sup>-2</sup> mm
- This can be compared with the initial hot gap of about 0.1 mm
- For such conditions, the gap conductance is

$$h_G = \lambda_G/(\delta_G + \delta_{Fr} + \delta_{Cr})$$
  $\delta_{Fr}$  – fuel roughness,  $\delta_{Cr}$  – clad roughness



- For closed gap, the heat transfer resistance is not reduced to zero due to roughness
- The gap conductance is now a sum of two parts:
  - direct contact between clad and fuel
  - gas layer due to roughness
- The gap htc is now:

$$h_G = \frac{C \cdot k_s \cdot P_{FC}}{H \sqrt{\delta_{EFFr}}} + \frac{\lambda_G}{\delta_{Fr} + \delta_{Cr}}$$
 rough

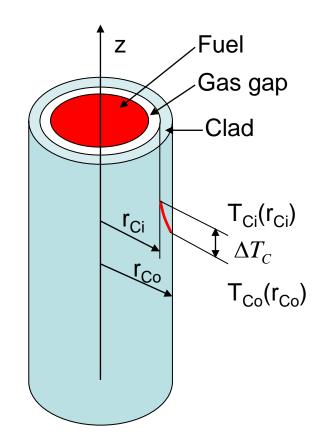
 $\delta_{Fr}$  – fuel roughness,  $\delta_{Cr}$  – clad roughness, C – empirical constant,  $k_s$  – effective conductivity fuel-clad, H – Mayer hardness of the softer material,  $\delta_{EFFr}$  – effective roughness,  $P_{FC}$  – contact pressure

$$\delta_{EFFr} = \sqrt{\left(\delta_{Fr}^2 + \delta_{Cr}^2\right)/2}$$

• Assuming a constant thermal conductivity of the clad material  $\lambda_C$ , the temperature drop in cladding is found as follows

$$\Delta T_C = \frac{q'}{2\pi\lambda_C} \ln\left(\frac{r_{Co}}{r_{Ci}}\right)$$

 Thermal conductivity of actual cladding materials is a function of temperature, however

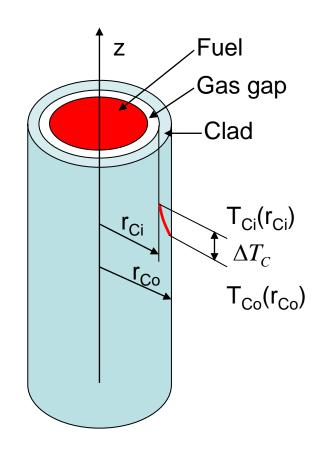


Fuel element

 For Zircaloy-2 and Zircaloy-4 (αphase), the thermal conductivity can be found as

$$\lambda_C = 12.6 + 0.0118T$$

- here: T [°C] temperature, λ<sub>C</sub> [W/mK] thermal conductivity
- valid for 20 < T < 800 °C</li>
- uncertainty ±1.01 W/mK



Fuel element

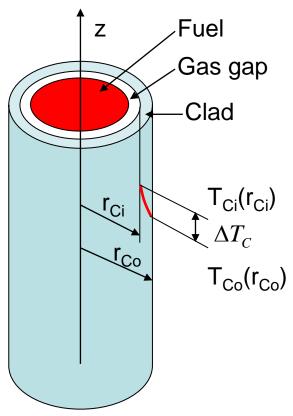
 The heat conduction equation in the clad with variable thermal conductivity is

$$\frac{1}{r}\frac{d}{dr}\left(r\lambda_C\,\frac{dT_C}{dr}\right) = 0$$

with condition

$$-\lambda_C \left. \frac{dT_C}{dr} \right|_{r=r_{Co}} = q_{Co}''$$

• Here  $q_{Co}''$  is the heat flux at clad outer surface, which can be found as  $q_{Co}'' = q'/2\pi r_{Co}$ 



Fuel element

 Integration of the conduction equation gives

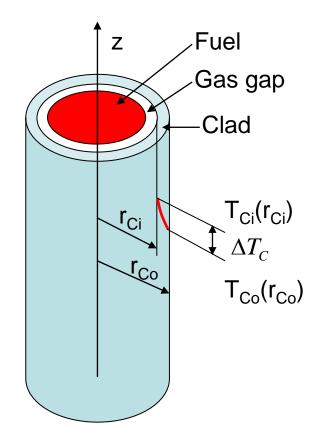
$$r\lambda_C \frac{dT_C}{dr} = C$$

Applying the boundary condition

$$-r_{Co}\lambda_C \frac{dT_C}{dr}\bigg|_{r=r_{Co}} = -C = \frac{q'}{2\pi}$$

Thus we have the following equation

$$r\lambda_C \frac{dT_C}{dr} + \frac{q'}{2\pi} = 0$$



Fuel element

We integrate the equation over clad

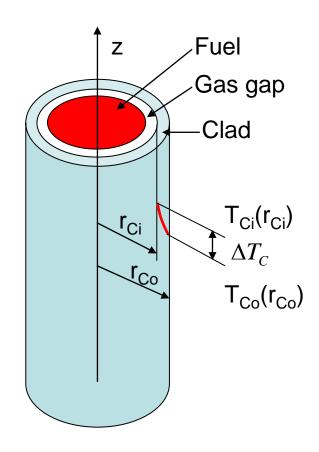
$$\int_{T_{Ci}}^{T_{Co}} \lambda_C dT_C + \frac{q'}{2\pi} \int_{r_{Ci}}^{r_{Co}} \frac{dr}{r} = 0$$

Assuming the thermal conductivity as

$$\lambda_C = a + bT$$

We get

$$a(T_{Co} - T_{Ci}) + \frac{b}{2}(T_{Co}^2 - T_{Ci}^2) + \frac{q'}{2\pi} \ln \frac{r_{Co}}{r_{Ci}} = 0$$



Fuel element

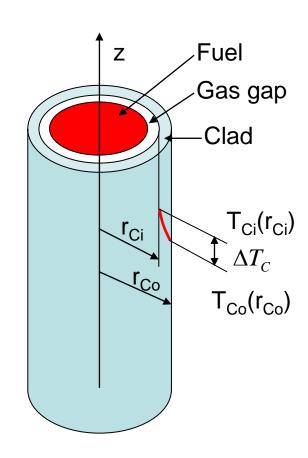
 The clad inner temperature can be now found as

$$T_{Ci} = \frac{1}{b} \left( \sqrt{(a + bT_{Co})^2 + \frac{bq'}{\pi} \ln \frac{r_{Co}}{r_{Ci}}} - a \right)$$

Exercise: show that for b = 0, the above solution gets the following form

Hint: use l'Hôspital's rule once taking b→0

$$T_{Ci} = T_{Co} + \frac{q'}{2\pi a} \ln \frac{r_{Co}}{r_{Ci}}$$



Fuel element

### Coolant to Cladding Heat Transfer

 The temperature drop in the thermal boundary layer in coolant can be found from the Newton equation for the convective heat transfer:

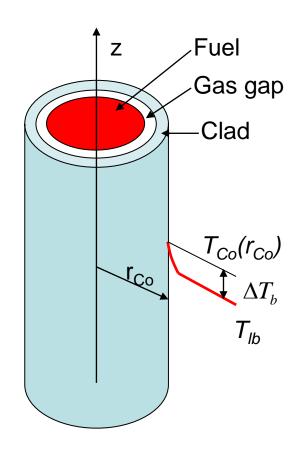
$$q''|_{T_{Co}} = h \cdot (T_{Co} - T_b) = h \cdot \Delta T_b$$

since

$$q''\big|_{r_{Co}} \cdot 2\pi r_{Co} \cdot dz = q' \cdot dz \Rightarrow q''\big|_{r_{Co}} = \frac{q'}{2\pi r_{Co}}$$

thus

$$\Delta T_b = \frac{q'}{2\pi r_{Co}h}$$



Fuel element

#### Coolant to Cladding Heat Transfer

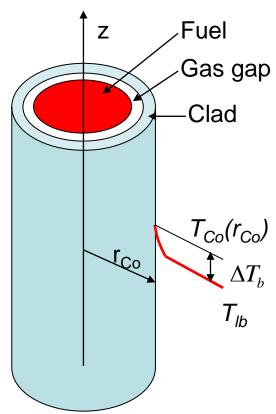
The clad outer temperature T<sub>Co</sub> at any axial location z is found as

$$T_{Co}(z) = T_{lb}(z) + \Delta T_b(z) + \Delta T_{ox}(z) + \Delta T_{crud}(z)$$

where the last term accounts for additional heat transfer resistance due to crud:

$$\Delta T_{crud} = \frac{q'}{2\pi\lambda_{cr}} \ln \left( \frac{r_{Co} + S + S_{cr}}{r_{Co} + S} \right)$$

S- the oxide layer thickness,  $S_{cr}-$  crud layer thickness (~2.4µm in PWR),  $\lambda_{cr}-$  crud thermal conductivity Fuel element (= 0.5 W/mK for BWR and 0.865 W/mK for PWR)

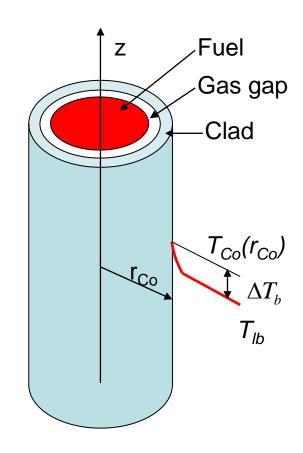


### Coolant to Cladding Heat Transfer

 The temperature drop over the oxide layer is as follows

$$\Delta T_{ox} = \frac{q'}{2\pi\lambda_{ox}} \ln\left(\frac{r_{Co} + S}{r_{Co}}\right)$$

S – the oxide layer thickness,  $\lambda_{ox}$  – oxide thermal conductivity (=1.56 W/mK for BWR and 2.0 W/mK for PWR)



Fuel element

### Oxide Layer

#### PWR

- Oxidation kinetics correlations are used to predict the oxide layer thickness
- After some initial transition time, the oxide layer thickness is assumed to grow linearly with time as  $\frac{dS}{dt} = c \exp(-Q/RT)$  where c, Q –constants, T temp. R gas constant

#### BWR

 Corrosion consists of athermal oxidation, which is linearly varying with the time, and thermal oxidation, which in addition depends on the metal/oxide surface temperature

#### **Crud Deposition**

#### PWR

 Crud sampling measurements performed in nuclear reactors indicate no correlation between crud deposition and the irradiation time. It can be assumed that independent of time crud thickness is about 2.4 µm.

#### BWR

It is assumed that the crud deposition rate is constant:

$$\frac{dS_{cr}}{dt} = 2 \times 10^{-4} \, (\mu \text{m/h})$$