October 6, 2013



0.1 Introduction

The goal of this thesis is to study and better understand the dynamics of particles in flows, and is a continuation of two previous masters theses [1][8]. This is done by analysing micrometer length glass particles in a shear flow and comparing this to theoretical models. Before discussing either of these processes more in depth some background and basic theory is needed.

0.1.1 Background

The study of particle dynamics in flow began with Einstein's paper from 1905 [4] in which he showed that the viscocity of suspended particles would increase the viscosity of the fluid and how much. Jefferey in his 1922 paper [9] extended these results to ellipsoidal axis-symmetrical particles but then also studied the orientational dynamics of the particles. Disregarding intertial effects the motion was found to be periodic and depending only on the initial condition of the particle.

Development of triaxial particles, started with Gierszewski & Chaffey (1978)[6] and was continued by Hint & Leal (1979) and more recently by Yarin et al in 1993[2]. Now the dynamics found for axis-symmetric particles by Jeffrey were periodic, but it was shown first by Hinch & Leal that some orbits would be doubly periodic, in other words following two separate independent periods. Yarin then was able to use numerical simulations to generate a surface of section [12] for some relations between the two minor axes showing that not only was there double periodic or quasi periodic orbits but for sufficiently large differences in axes there would be chaotic orbits. Several other surfaces of were also produced by Johansson (2012)[1] using the same method as Yarin with higher resolution thanks to improvements in computing power. It was there shown that only very small asymmetries on the order of 1% will lead to quasi-periodic motion for some initial conditions.

Experimental studies of these theoretical results were first done by Goldsmith and Mason in 1962[7] who confirmed that the rotation rate matched well with that predicted from Jeffrey orbits but he did not study the actual orbits. Since then most experimental research, such as CITE SOMETHING HERE has been focused on diluted suspensions of particles and the increased viscocity and other properties this causes. As good summary of both theoretical but primarily experimental results was written by Petrie in 1999 [11].

The first experimental work to try to measure the actual Jeffrey orbits in their Euler angles was done by Einarsson et al [5] in 2011. Although there was some promising results, the vast majority of particles were asymmetric. Moreover the width and length of particles both varies, meaning that the aspect ratio could not accurately be determined.

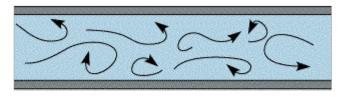
Theory

In order to better understand the results and discussions in this thesis some rather basic results in fluid dynamics, image analysis and other fields need to be understood by the reader.

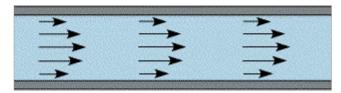
- 1) It is however not the focus of this thesis and as such I will try to be as brief as possible, and an experienced reader can safely skip to the next chapter.
- 2) As the focus of this thesis is experimental I will not go into great detail, but try to briefly motivate and quickly summarize results, and refer the inquisitive reader to more thorough sources. As no recent developments are discussed, readers comfortable in these fields can skip this chapter without any loss in understanding.

1.1 Fluid Dynamics

Turbulent



Laminar



In order to understand the motivations, limitations and behaviour of the experiment we need to know about a few key concepts in fluid dynamics.

1.1.1 Navier Stokes

1.1.2 Reynold's Number

The Reynolds number (Re) is a dimensionless number describing the ratio of inertial forces to viscous forces in a flow. This is not a very strict definition, but suffices to explain that the Reynolds number can be used to characterize the so called flow regime of a system.

The two major flow regimes are Laminar flow, where viscous forces dominate over inertial forces, and the turbulent regime where inertial forces dominate. The area where neither is significantly larger is referred to as transitional flow, which may show either chaotic of laminar behaviour.

A rough characterization of laminar and chaotic flow can be seen in figure 1.1.2

The Reynolds number (Re) is defined as [10]

$$Re = \frac{UL\rho}{\mu} \tag{1.1}$$

where U is the characteristic velocity, L is the characteristic length, ρ is the density and μ is the dynamic viscosity.

As the Reynolds number is a ratio, a flow is predicted to be laminar if Re << 1 which is the primary concern in this thesis.

1.1.3 Stokes Drag and Stokes's law

The drag force exerted by a fluid on a spherical particle for $Re \ll 1$ is found using the so called Stokes's law [3]

$$F_D = 6\pi \mu Rv \tag{1.2}$$

and equating this with the gravitational force acting on the sphere

$$F_G = (\rho_p - rho_l)g \cdot \frac{4\pi R^3}{3} \tag{1.3}$$

the velocity of a steadily sinking sphere is found to be

$$v_s = \frac{2}{9} \frac{\Delta \rho}{\mu} g R^2 \tag{1.4}$$

In order to approximate the falling velocity of our particles we can make use of Stokes law which describes the drag force on an object in laminar flow, and more specifically in the case of a sphere, where $\Delta \rho$ is the difference in density between the sphere and the liquid, g is the specific gravity, μ is the dynamic viscosity and R is the radius of the sphere.

1.1.4 Shear

1.1.5 Péclet Number

The p'clet number describes the ratio of thermal noise to other stuff. I really don't know anything about the piclet number.

1.2 Jeffrey Orbits

The equations of motion for a triaxial ellipsoid particle was first found by Jeffrey [9] but the first dimensionless equation for the Euler Angles was found by Yarin et al. [2] to be

$$\frac{d\theta}{dt} = (g_2 \sin \psi + g_3 \cos \psi) \sin \theta \tag{1.5a}$$

$$\frac{d\phi}{dt} = \frac{1}{2} + g_3 \sin \psi - g_2 \cos \psi \tag{1.5b}$$

$$\frac{d\psi}{dt} = g_1 + (g_2 \cos \psi - g_3 \sin \psi) \cos \theta \tag{1.5c}$$

(1.5d)

where the functions g_i are defined as

$$g_1 = \frac{a_y^2 - a_z^2}{2(a_y^2 + a_z^2)} \left(-\frac{1}{2} (\cos^2 \theta + 1) \sin 2\phi \sin 2\psi + \cos \theta \cos 2\phi \cos 2\psi \right), \quad (1.6a)$$

$$g_2 = \frac{a_z^2 - a_x^2}{2(a_x^2 + a_z^2)} \left(-\cos\theta \sin 2\phi \sin\psi + \cos 2\phi \cos\psi \right), \tag{1.6b}$$

$$g_3 = \frac{a_x^2 - a_y^2}{2(a_x^2 + a_y^2)} (\cos \theta \sin 2\phi \cos \psi + \cos 2\phi \sin \psi)$$
 (1.6c)

1.3 Kalman filter

Method

2.1 Experimental Setup

As the goal is to attempt to verify the Jeffrey equations in eq ?? we need an experimental setup with particles and flow system that satisfy the conditions that the Jeffrey equations apply under. This means our particles have to be bouyant, triaxially symmetric and small enough that inertial effects are not a problem. The flow has to be a linear creeping flow, in other words have a Reynolds number satisfying Re << 1 but have a high unidirectional shear that allows one to detect the orbits in a finite distance.

The particles used in previous measurements were made from apoxy [?] which made them buoyant and small enough to ignore inertial effects, but they were not symmetrical enough to produce reliable periodic Jeffrey orbits. Thus two sets of glass particles from Nippon Glass, Japan[?], have been used. They are cylindrical with a consistent width of $3 \mu m$ and $5 \mu m$ and varying length.

However they are made glass with a density of approximately $2.57\,\mathrm{g/cm^3}$ at $20\,\mathrm{C^\circ}$ which is significantly higher than that of water with a density of $1\,\mathrm{g/cm^3}$ at $20\,\mathrm{C^\circ}$ and glycerol with a density of $1.5\,\mathrm{g/cm^3}$. Thus to correct for the density and limit sinking or floating the water soluble Sodium metatungstate which at $20\,\mathrm{C^\circ}$ has maximum density of $2.94\,\mathrm{g/cm^3}$. To increase the viscosity of the liquid around 8% glycerol is added, resulting in a measured dynamic viscosity of $24\cdot10^{-3}\,\mathrm{Pa}$ s

This liquid with suspended particles is flowed through a channel of Polydimethylsiloxane (PDMS) 4 cm long, 2.5 mm wide and either 200 μ m and 500 μ m. The flow profile of such a channel was calculated by Anton Johansson in his thesis[1] and can be seen in figure ??. The flow rate varies between 2 and $20\,\mu$ l/m in SI units $3.33\cdot10^-10\,\mathrm{m}^3$ /s which with a cross section between means a maximum flow speed of $6.66\,\mathrm{mm/s}$.

To confirm that the flow is a creeping flow we can calculate the maximum Reynolds number using eq 1.1 and our maximum flow speed

$$Re = \frac{UL\rho}{\mu} \approx \frac{6.66 \cdot 10^{-3} \cdot 2.5 \cdot 10^{-3} 2.5}{24 \cdot 10^{-3}} \approx 1.6 \cdot 10^{-3} \ll 1$$
 (2.1)

In order to study the dynamics of particles, a channel made from PDMS and bonded onto a glass slide. A fluid containing the triaxial glass particles that can be seen in fig re REF HERE is pumped at a constant rate through the channel using a INSERT THE PUMP NAME HERE. To observe the particles, the channel is placed upon a confocal microscope connected to a INSERT CAMERA MODEL HERE. The channel is then moved using a INSERT STEP ENINE NAME HERE controlled from a computer. A mroe detailed description of the setup can be seen in figure REF to SETUP IMAGE THAT I MAKE

2.2 The particles

Previously the particles used in the experiment were polymeric made by swirling an apoxy solution in a vortex. This produces rod like particles of different lengths, but very often included noticeable defects such as being bent, small lumps etc.

To improve results glass particles from Nippon Glass company in Japan were brought in. As they are mainly manufactured to serve as spacing rods in LCD screens they have a very well determined width but then broken at varying lengths. These breaking points are the only real visible point of imperfection of the rods. The specification of length and width can be seen in figure ??

While the glass rods are far more regular in terms of size and shape, they do have on major problem. The density of the glass is $2.57 \, \rm ^g/cm^3$, significantly higher than water which has a density of around $1 \, \rm g/cm$ at 20 degrees C and glycerol which has a density of DENSITY OF GLYCEROL. And so the particles sink very quickly in any mix of water and glycerol.

The solution is to use Sodium Metatungstate, a water soluble mineral which gives the resulting mix a maximum density of around $3\,\mathrm{g/cm}$ which is more than sufficient to keep the particles suspended. However the viscocity of only water and Sodium Metatungstate is only around SOMETHING OR OTHER

First the viscosity of the mix is significantly lower than the glycerol and water mix used previously (a 1:4 mix of glycerol and water was commonly used) which means the system is more sensitive to noise. Second the density of the solution changes when the water mixed in evaporates. As the ratio of water to mineral is relatively high, clearly more than 1:1 by weight, a small percentage of water evaporating will result in significant change in density

2.2.1 Density matching

I guess we use sodium meta tungstate. But does this really need a whole section? Seems like overdoing it... but what THE EQUATION FOR MODIFYING VISCOCITY

$$\rho_a = \frac{m_a}{V_a} = \frac{V_b \rho_b + V_{mix} \rho_{mix}}{V_b + V_{mix}} \tag{2.2}$$

So if we want to find V_{mix} we get

$$V_{mix} = \frac{V_b(\rho_b - \rho_a)}{\rho_a - \rho_{mix}} \tag{2.3}$$

TODO: READ UP ON THE EFFICIENCY OF THE CANNY EDGE DETECTION TAKE AN IMAGE OF THE STATIC NOISE REDUCTION (DOES IT ACTUALLY WORK?!) GET AN IMAGE OF BEFORE AND AFTER SMOOTHING, PREFERABLY INCLUDE A CANNY EDGE DETECTION OF BOTH WRITE ABOUT THE TIME IT TAKES TO DO VARIOUS STUFFS (IS THIS NEEDED?) GET MORE SOURCES IN THE THEORY SECTION IN PARTICULAR: Looking up reynolds number sources, "creeping motion" might be a relevant term Add our measured visc and add it to citations, maybe add Dag how to cite that?

JEFFREY ORBIT STUFF: Make a picture illustrating the various angles Have a picture of some jeffrey orbits

EXPERIMENTAL SETUP STUFF: Include images of the particles Include the distribution of lengths, either measured or from nippon Add the citation for Nippon glass

2.2.2 Noise Reduction

The first step in tracking a particle is to correctly identify it in the image given. To do this we want to eliminate as much noise from the image as we can. The first type of noise we will eliminate is static noise, this is noise present in every image and results from dirt or scratches on the lens of the camera or microscope. The easiest solution to such noise would of course be to clean the instruments, but despite numerous attempts of carefully cleaning every surface a noticeable of static noise would always remain.

This means one must use algorithmic noise reduction methods to remove this noise. The method employed is a simple averaging that takes N pictures at different positions in the channel to generate an average image where any particular features of the channel would disappear and only the static noise remain. This can be seen in figure STATIC NOISE REDUCTION IMAGE,

2.2.3 Canny Edge Detection

The Canny Edge invented by John Canny in his 2011 paper the canny of cane [?]detection is generally considered the most advanced and best performing edge detection of the simple filter functions. Without going in to the finer details, given an image matrix \mathbf{I} where each value corresponds to the light intensity $i_{x,y}$ of that pixel at index x,y the Canny edge detector will try to find the cohesive pixels $E=\{e_1,e_2...e_n\}$ where there is a noticeable change in intensity. In other words, what we call an "edge" an image.

This is accomplished in two steps. First a Sobel Filter edge image is computed by looking at the change in intensity at every pixel from 3 possible directions and averaging these.

S = MATHEMATICS OF SOBEL We then consider a Then, a pixel $p_{x,y} \in EifS(x,y) > T_{high}$ where T_{high} is a predetermined threshold value.

Secondly we recursively check all pixels neighbouring an edge MATH?

if they are higher than some threshold value T_low . if they are, they are also considered part of the edge. This is repeated until no more pixels are added. An image illustrating this process can be seen in figure FIG. The benefit of the Canny edge detection over the simpler Sobel is that it is much easier to detect cohesive objects that vary in intensity without getting a lot of other noise in the image. The only real drawback of the Canny Edge detection is the computation time, and thus the implementation from the Open Computer Vision (OCV) was used, as this is a heavily optimized routine written in C++ with real time uses in mind. Thanks to this the computing for the Canny Edge of a 260x260 Image takes about X ms and thus is of little importance in the overall time per frame.

After noise reduction the Canny Edge Detection is used to find the most significant edges in the image.

2.3 Contour detection and selection

Once an edge image has been generated, the OCV package has another useful function, Contours which returns a list of every contiguous group of edge pixels. If we have chosen the threshold values to the edge detection correctly, this should include the particle or a good approximation of it.

In order to find the correct contour, a few techniques are used to find the correct contour.

First particles whose total size is less than some minimum value, n_{min} or larger than some maximum value n_{max} are ignored. Then the position pP_i of each contour $C_i = p_1, p_2...p_n$ is calculated as the average pixel position

$$P_i = \sum_{j=1}^{n} p_j / n$$

This position is compared to the expected position of the Kalman filter, which the very first frame is the middle position.

Finally a 'thinness value' is calculated according to eq 2.4

$$w_{thin} \left(\frac{n}{d_{max}^2}\right)^2 \tag{2.4}$$

. where w_{thin} is a weighting constant, n is the number of pixels in the contour and d_{max} is the longest distance between two pixels in the where I am not really sure I should do this now that I have so few particles, but I do it none the less!

2.4 Kalman Filter

When the particle is at constant motion in the channel the equations of motion give us

$$\begin{bmatrix} x_n \\ v_{x,n} \\ y_n \\ v_{y,n} \end{bmatrix} = \begin{bmatrix} x_{n-1} & +v_{x,n-1} \\ v_{x,n-1} & \dots \\ y_{n-1} & +v_{y,n-1} \\ v_{y,n-1} \end{bmatrix} + \begin{bmatrix} 0 \\ c_{xn} \\ 0 \\ c_{yn} \end{bmatrix} y_n v_{yn}$$
(2.5)

We can rewrite this in matrix form as

$$\begin{bmatrix} x_n \\ v_{x,n} \\ y_n \\ v_{y,n} \end{bmatrix} = \begin{bmatrix} 1 & \Delta t & 0 & 0 \\ 0 & 1 & 0 & 0 \\ 0 & 0 & 1 & \Delta t \\ 0 & 0 & 0 & 1 \end{bmatrix} \cdot \begin{bmatrix} x_{n-1} \\ v_{x,n-1} \\ y_{n-1} \\ v_{y,n-1} \end{bmatrix} + \begin{bmatrix} 0 & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 \\ 0 & 0 & 0 & 0 \\ 0 & 0 & 0 & 1 \end{bmatrix} \cdot \begin{bmatrix} 0 \\ c_{x,n-1} \\ 0 \\ c_{y,n-1} \end{bmatrix}$$

Now if we want to transform this to the measured data we have to simply multiply by a constant pixel-to-meter constant, which has been measured to be around $1/940=1.06\cdot 10^{-3}$

$$Q = \begin{bmatrix} 0 & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 \\ 0 & 0 & 0 & 0 \\ 0 & 0 & 0 & 1 \end{bmatrix}$$
 (2.7)

Which we can easily re-write as a Kalman filter

$$\hat{\mathbf{x}}_n = \mathbf{A}_n \mathbf{x}_{n-1} + \mathbf{B}_n \mathbf{u}_n + \mathbf{w}_n \tag{2.8}$$

$$\hat{\mathbf{P}}_n = \mathbf{F}_n \mathbf{P}_{n-1} \mathbf{F}_n^T + \mathbf{Q}_n \tag{2.9}$$

with

$$\mathbf{x}_n = \left[x_n v_{x,n} y_n v_{y,n}\right]^T \tag{2.10}$$

$$\mathbf{A} = \begin{bmatrix} 1 & \Delta t & 0 & 0 \\ 0 & 1 & 0 & 0 \\ 0 & 0 & 1 & \Delta t \\ 0 & 0 & 0 & 1 \end{bmatrix}$$

$$(2.10)$$

$$\mathbf{B}_{n} = \begin{bmatrix} 0 & 0 & 0 & 1 \\ 0 & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 \\ 0 & 0 & 0 & 0 \\ 0 & 0 & 0 & 1 \end{bmatrix}$$
 (2.12)

$$\mathbf{u}_n = \begin{bmatrix} 0 \\ c_{x,n-1} \\ 0 \\ c_{y,n-1} \end{bmatrix}$$
 (2.13)

and we add the update part as

$$\mathbf{K}_n = \hat{\mathbf{P}}_n \mathbf{H}_n^T (\mathbf{H}_n \hat{\mathbf{P}}_n \mathbf{H}_n^T) \tag{2.14}$$

$$\mathbf{x_n} = \hat{\mathbf{x}}_n + \mathbf{K}_n(\mathbf{y} - \mathbf{H}_n \hat{\mathbf{x}}_n) \tag{2.15}$$

$$\mathbf{P} = (\mathbf{I} - \mathbf{K}_n \mathbf{H}_n) \hat{\mathbf{P}}_n \tag{2.16}$$

2.5 Stabilizing the tracking

Once a state estimation has been made, we want to adjust the speed of the step engine to, as best as possible, match that of the particle. This is done by looking both the position and velocity of the particle and going through the conditional statements shown in figure CONDITIONAL CORRECTION VECTOR.

The goal is to limit the amount of corrections made, as changing the velocity is rather time intensive as discussed in section 2.6, as well as keeping the particle stable. There is also no point in trying to completely eliminate movement

2.6 Time Considerations

A higher FPS will allow the particle detection to be better, improve the position saving and allow the particle tracking to be more stable as well. So maximizing the FPS, ie reducing the computational time of each task, is a clear goal for a good automated tracking. A list of the different tasks and their average execution times can be seen in table 2.6

Task	Average time	Std deviation
Capture screen	1000	200
Find edges	200	20

We can clearly see that FPS is limited primarily by three routines: The screen capture routine, the change velocity routine and finally the save position routine. The first and last are unavoidable and must be done every frame by definition if we are interested in knowing the particles position as well as possible. This means we simply want to use the velocity correction as little as possible. Since the time constraint is in the communication with the step engine, there is not any optimization to be done here, at least not within the scope is this thesis.

Experimental Setup

Results

Discussion

Appendix A

Raw data

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