

Isothermal CSTR



B is the product

SIMPLIFIED — NO HEAT RETENTION

TOTAL MATERIAL BALANCE

$$\frac{dV}{dt} = F_i - F_o = 0$$

COMPONENT A BALANCE

$$\frac{dC_A}{dt} = F C_{Ai} - r_A - V k_1 C_A - V k_3 C_A^2$$

$$\text{and } \frac{dC_A}{dt} = \frac{F}{V} [C_{Ai} - C_A] - k_1 C_A - k_3 C_A^2$$

COMPONENT B BALANCE

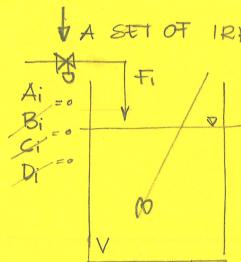
$$\text{and } \frac{dC_B}{dt} = \frac{F}{V} [C_{Bi} - C_B] + r_B$$

COMPONENT C BALANCE

$$\text{and } \frac{dC_C}{dt} = \frac{F}{V} [C_{Ci} - C_C] + r_C$$

COMPONENT D BALANCE

$$\text{and } \frac{dC_D}{dt} = \frac{F}{V} [C_{Di} - C_D] + \frac{1}{2} k_3 C_A^2$$



A SET OF IRREVERSIBLE REACTIONS

- CONSTANT DENSITY
- CONSTANT VOLUME

$K_1 = 5/6$	min^{-1}
$K_2 = 5/3$	min^{-1}
$K_3 = 1/6$	$\text{lit}(\text{mol}^{-1} \text{min}^{-1})$

RATE CONSTANTS

$$\begin{aligned} & \frac{\text{mol}}{\text{lit min}} \cdot \frac{\text{mol}}{\text{lit min}} \cdot \frac{\text{mol}}{\text{lit min}} \\ & \equiv \frac{\text{lit mol}}{\text{lit min}} \end{aligned}$$

$r_{A,B,C,D}$

rate of 'generation' of
 A, B, C, D per unit volume

$$F^{ss}/V = 4/7 \text{ min}^{-1}$$

$$C_{A,f}^{ss} = 10 \text{ mol/l}$$

$$\left| \begin{array}{l} K_1 = 5/6 \\ K_2 = 5/3 \\ K_3 = 1/6 \end{array} \right.$$

$$C_{A,ss} = 3 \text{ mol/l}$$

$$C_{B,ss} = 1.1140 \text{ mol/l}$$

$$C_{C,ss} = 3.2580 \text{ mol/l}$$

$$C_{D,ss} = 1.3125 \text{ mol/l}$$

$$\frac{dC_A}{dt} = \frac{F}{V} (C_{A_i} - C_A) - K_1 C_A - K_2 C_A^2$$

$$\frac{dC_B}{dt} = \frac{F}{V} (-C_B) + K_1 C_A - K_2 C_B$$

$$\frac{dC_C}{dt} = \frac{F}{V} (-C_C) + K_2 C_B$$

$$\frac{dC_D}{dt} = \frac{F}{V} (-C_D) + \frac{1}{2} K_3 C_A^2$$

Assume that B is desired product and thus we measure its concentration (only)

$$y = C_B$$

STATES

C_A, C_B, C_D, C_C

INPUTS

F or F/V

PARAMETERS

K_1, K_2, K_3

STEADY STATE CONDITIONS

$$* \frac{dC_A}{dt} = 0 \Rightarrow \frac{F}{V} [C_{A_i} - C_A] - K_1 C_A - K_3 C_A^2 = 0$$

$$-K_3 C_A^2 - C_A \left[\frac{F}{V} + K_1 \right] + \frac{F}{V} C_{A_i} = 0$$

$$\tilde{K}_3 C_A^2 + \left[\frac{F}{V} + K_1 \right] C_A - \frac{F}{V} C_{A_i} = 0$$

$$\boxed{C_A^{ss}} = \frac{-\left(K_1 + \frac{F^{ss}}{V}\right)}{2K_3} + \frac{\sqrt{\left(K_1 + F^{ss}/V\right)^2 + 4K_3(F^{ss}/V)} C_{A_i}^{ss}}{2K_3}$$

$$* \frac{dC_B}{dt} \Rightarrow -C_B \left[\frac{F}{V} + K_2 \right] + K_1 C_A = 0$$

$$\left[\frac{F^{ss}}{V} + K_2 \right] C_B^{ss} - K_1 C_A^{ss} = 0$$

$$\boxed{C_B^{ss}} = \frac{K_1 C_A^{ss}}{\left[\frac{F^{ss}}{V} + K_2 \right]} / \left[\frac{F^{ss}}{V} + K_2 \right]$$

$$= K_1 \left[\frac{-K_1 + F^{ss}/V}{2K_3} + \frac{\sqrt{\left(K_1 + F^{ss}/V\right)^2 + 4K_3(F^{ss}/V)} C_{A_i}^{ss}}{2K_3} \right] / \left[\frac{F^{ss}}{V} + K_2 \right]$$

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$$* \frac{dC_c}{dt} = 0 \rightsquigarrow -C_c [F/V] + K_2 C_B = 0$$

$$F/V C_c - K_2 C_B = 0$$

$$\boxed{C_c^{ss}} = \frac{K_2 C_B^{ss} / (F/V)}{K_2 \left[\frac{-K_1 + F^{ss}/V}{2K_3} + \frac{\sqrt{(K_1 + F^{ss}/V)^2 + 4K_3(F^{ss}/V) C_A^{ss}}}{2K_3} \right] / \left[\frac{F^{ss}/V}{K_2} + \right]}$$

$$* \frac{dC_D}{dt} = 0 \rightsquigarrow -\frac{F}{V} C_D + \frac{1}{2} K_3 C_A^2 = 0$$

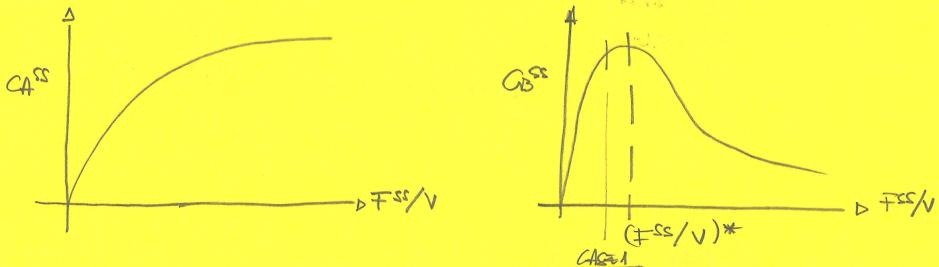
$$F/V C_D - 1/2 K_3 C_A^2 = 0$$

$$\boxed{C_D^{ss}} = \frac{\frac{1}{2} K_3 C_A^{ss 2}}{(F/V)}$$

$$= \frac{1/2 K_3}{F^{ss}/V} \left[\quad / \quad \right]^2$$

PLOT THE STEADY STATE CONCENTRATION OF C_B (C_B^{ss}) AS A FUNCTION OF THE STATE VELOCITY (F^{ss}/V)

BY STUDYING THE EXPRESSION OF C_B^{ss} AS FUNCTION OF F^{ss}/V
WE CAN DERIVE THE SO-CALLED INPUT-OUTPUT CURVE



IT IS EASY TO SEE THAT THERE IS A MAXIMUM VALUE OF THE CONCENTRATION OF B

→ IF THE OBJECTIVE IS TO MAXIMIZE THE PRODUCTION OF B,
THEN THERE EXISTS AN OPTIMUM RESIDENCE TIME
($\approx 1.292 \text{ min}^{-1}$)

LINER STATE SPACE MODEL OF THE NONLINEAR REPRESENTATION

$$\dot{x} = Ax + Bu$$

$$y = Cx$$

WE FIRST DEFINE THE VARIABLES

$$x = \begin{bmatrix} C_A - C_A^{ss} \\ C_B - C_B^{ss} \end{bmatrix} \quad (\begin{bmatrix} C_A - C_A^{ss} \\ C_B - C_B^{ss} \\ C_C - C_C^{ss} \\ C_D - C_D^{ss} \end{bmatrix})$$

$$u = [F/V - F^{ss}/V]$$

$$y = \begin{bmatrix} C_A - C_A^{ss} \\ C_B - C_B^{ss} \end{bmatrix}$$

$$\begin{aligned} \frac{dC_A}{dt} &= F/V(C_A - C_A) - k_1 C_A - K_3 C_A^2 \\ \frac{dC_B}{dt} &= F/V(-C_B) + k_1 C_A - k_2 C_B \\ \frac{dC_C}{dt} &= F/V(-C_C) + k_2 C_B \\ \frac{dC_D}{dt} &= F/V(-C_D) + 1/2 K_3 C_A^2 \end{aligned}$$

THE DYNAMICS

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$$\begin{aligned} x_1^{ss} &= 3 & u_1^{ss} &= 4/4 \\ x_2^{ss} &= 1.117 & u_2^{ss} &= 10 \\ x_3^{ss} &= 3.258 \\ x_4^{ss} &= 1.3125 \end{aligned}$$

$$A = \begin{bmatrix} -2.4048 & 0 & 0 & 0 \\ 5/6 & -2.2381 & 0 & 0 \\ 0 & 5/3 & -4/4 & 0 \\ 0.5 & 0 & 0 & -4/4 \end{bmatrix}$$

$$B = \begin{bmatrix} 7 & 10 \\ -1.117 & 0 \\ -3.258 & 0 \\ -1.3125 & 0 \end{bmatrix}$$

$$\frac{dx_1}{dt} = u_1 (C_{A1} - x_1) - k_1 x_1 - k_3 x_1^2$$

$$\frac{dx_2}{dt} = u_1 (-x_2) + k_1 x_1 - k_2 x_2$$

$$\frac{dx_3}{dt} = u_1 (-x_3) + k_2 x_2$$

$$\frac{dx_4}{dt} = u_1 (-x_4) + \frac{1}{2} k_3 x_1^2$$

$$\frac{\partial f_1}{\partial x_1} = -u_1^{ss} - k_1 - 2k_3 x_1^{ss}$$

$$\frac{\partial f_1}{\partial x_2} = 0 \quad \frac{\partial f_2}{\partial x_3} = 0 \quad \frac{\partial f_1}{\partial x_4} = 0$$

$$\frac{\partial f_2}{\partial x_1} = k_1$$

$$\frac{\partial f_2}{\partial x_2} = -u_1^{ss} - k_2 \quad \frac{\partial f_2}{\partial x_3} = 0 \quad \frac{\partial f_2}{\partial x_4} = 0$$

$$\frac{\partial f_3}{\partial x_1} = 0 \quad \frac{\partial f_3}{\partial x_2} = +k_2 \quad \frac{\partial f_3}{\partial x_3} = -u_1^{ss} \quad \frac{\partial f_3}{\partial x_4} = 0$$

$$\frac{\partial f_4}{\partial x_1} = \frac{1}{2} \cdot 2k_3 x_1^{ss} \quad \frac{\partial f_4}{\partial x_2} = -u_1^{ss} \quad \frac{\partial f_4}{\partial x_3} = 0 \quad \frac{\partial f_4}{\partial x_4} = 0$$

$$\begin{bmatrix} -u_1^{ss} - k_1 - 2k_3 x_1^{ss} & 0 & 0 & 0 \\ k_1 & -u_1^{ss} - k_2 & 0 & 0 \\ 0 & k_2 & -u_1^{ss} & 0 \\ k_3 x_1^{ss} & 0 & 0 & -u_1^{ss} \end{bmatrix}$$

$$(x_1, x_2, x_3, x_4)^{ss}$$

$$\begin{aligned} k_1 &= 5/6 \\ k_2 &= 5/3 \\ k_3 &< 1/6 \end{aligned}$$

$$u_1^{ss} =$$

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$$C_{A1}^{ss} = 10 \text{ mol/l}$$

$$\begin{bmatrix} B \\ 10 - 3 & 10 \\ -1.117 & 0 \\ -3.258 & 0 \\ -1.114 & 0 \\ -1.3125 \end{bmatrix}$$

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$$\frac{\partial f_1}{\partial x_1} = \frac{\partial f_1}{\partial (C_A - C_A)} = \frac{\partial f_1}{\partial C_A} = -\frac{F_{ss}}{V} - K_1 - 2K_3 C_A^{ss}$$

$$\frac{\partial f_1}{\partial x_2} = \frac{\partial f_1}{\partial (C_B - C_B)} = \frac{\partial f_1}{\partial C_B} = 0$$

$$\frac{\partial f_2}{\partial x_1} = \frac{\partial f_2}{\partial (C_A - C_A)} = \frac{\partial f_2}{\partial C_A} = K_1$$

$$\frac{\partial f_2}{\partial x_2} = \frac{\partial f_2}{\partial (C_B - C_B)} = \frac{\partial f_2}{\partial C_B} = -\frac{F_{ss}}{V} - K_2$$

A₁₁A₁₂A₂₁A₂₂

$$\frac{\partial f_1}{\partial u_1} = \frac{\partial f_1}{\partial (\dot{V}_1 - \dot{V}_{ss})} = \frac{\partial f_1}{\partial (\dot{V}_1)} = C_A^{ss} - C_A^{ss}$$

$$\frac{\partial f_2}{\partial u_1} = \frac{\partial f_2}{\partial (\dot{V}_1 - \dot{V}_{ss})} = \frac{\partial f_2}{\partial (\dot{V}_1)} = -C_B^{ss}$$

B₁₁B₂₁

WE OBTAIN THE FOLLOWING SYSTEM MATRICES

$$A = \begin{bmatrix} -\frac{F}{V} - K_1 - 2K_3 C_A^{ss} & 0 \\ K_1 & -\frac{F}{V} - K_2 \end{bmatrix}$$

$$B = \begin{bmatrix} C_A^{ss} - C_A^{ss} \\ -C_B^{ss} \end{bmatrix}$$

The matrices can be particularised by considering different steady state operating points

CASE 1CASE 2CASE 3

$$\begin{cases} K_1 = 5/6 \\ K_2 = 5/3 \\ K_3 = 1/6 \end{cases}$$

$$C_A^{ss} = 3 \text{ mol/lit}$$

$$C_B^{ss} = 1.140 \text{ mol/lit}$$

$$C_C^{ss} = 3.2880 \text{ mol/lit}$$

$$C_D^{ss} = 1.3125 \text{ mol/lit}$$

-2238

$$\begin{array}{c} -2.408 \\ \downarrow \\ \begin{bmatrix} -1/4 - 5/6 - 2\sqrt{1/6 \cdot 3} & 0 & 0 & 0 \\ 5/6 & -4/4 - 5/3 & 0 & 0 \\ 0 & 5/3 & -4/4 & 0 \\ 1/6 \cdot 3 & -0 & 0 & -4/4 \end{bmatrix} \end{array}$$

4

(5)^a

$$\frac{\partial f_1}{\partial u_1} = \frac{M_2}{C_{A1} - x_1}$$

$$\frac{\partial f_2}{\partial u_1} = -x_2$$

$$\frac{\partial f_3}{\partial u_1} = -x_3$$

$$\frac{\partial f_4}{\partial u_1} = -x_4$$

$$B = \begin{bmatrix} M_2^{ss} & C_{A1}^{ss} - x_1^{ss} & u_1^{ss} \\ -x_2^{ss} & 0 & \\ -x_3^{ss} & 0 & \\ -x_4^{ss} & 0 & \end{bmatrix}$$

$$x_1^{ss} = 3 \text{ mol/lit}$$

$$x_2^{ss} = 1.114 \text{ mol/lit}$$

$$x_3^{ss} = 3.258 \text{ mol/lit}$$

$$x_4^{ss} = 1.5175 \text{ mol/lit}$$

$$M_1^{ss} = h/4$$

$$C_{A1}^{ss} = 10 \text{ kg/lit}$$

$$M_2^{ss} = 10$$

$$\frac{\partial f_1}{\partial u_2} = u_1$$

$$\frac{\partial f_2}{\partial u_2} = 0$$

$$\frac{\partial f_3}{\partial u_2} = 0$$

$$\frac{\partial f_4}{\partial u_2} = 0$$

⑥