

ISOTHERMAL CSTR

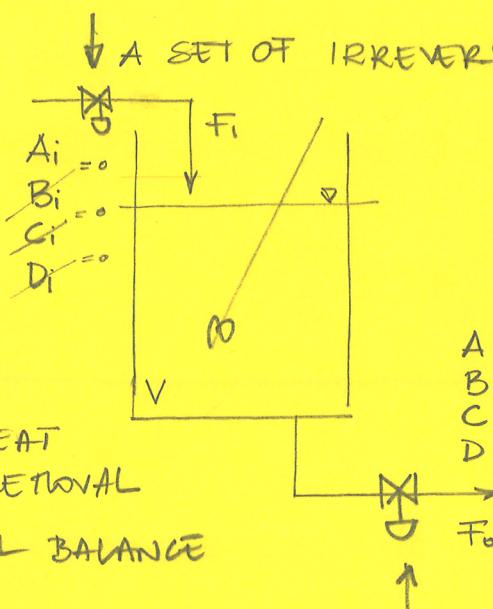


B is the product

SIMPLIFIED — NO HEAT REMOVAL

TOTAL MATERIAL BALANCE

$$\frac{dV}{dt} = F_i - F_o = 0$$



- CONSTANT DENSITY
- CONSTANT VOLUME

$$\begin{aligned} k_1 &= 5/6 \text{ min}^{-1} \\ k_2 &= 5/3 \text{ min}^{-1} \\ k_3 &= 1/6 \text{ et}(\text{mol}^{-1} \text{min}) \end{aligned}$$

RATE CONSTANTS

COMPONENT A BALANCE

$$\begin{aligned} \frac{dVCA}{dt} &= FC_{Ai} - C_A + \underbrace{Vk_1C_A - VK_3C_A^2}_{r_A} \\ \text{and } \frac{dC_A}{dt} &= \frac{F}{V}[C_{Ai} - C_A] - k_1C_A - K_3C_A^2 \end{aligned}$$

$$\begin{aligned} \frac{\text{mol}}{\text{et}} \frac{\text{mol}}{\text{et}} \left(\frac{\text{et}}{\text{mol}} \right) \\ \equiv \frac{\text{mol}}{\text{et min}} \end{aligned}$$

COMPONENT B BALANCE

$$\text{and } \frac{dC_B}{dt} = \frac{F}{V}[C_{Bi} - C_B] + \underbrace{k_1C_A - K_2C_B}_{r_B}$$

COMPONENT C BALANCE

$$\text{and } \frac{dC_C}{dt} = \frac{F}{V}[C_{Ci} - C_C] + \underbrace{K_2C_B}_{r_C}$$

COMPONENT D BALANCE

$$\text{and } \frac{dC_D}{dt} = \frac{F}{V}[C_{Di} - C_D] + \underbrace{\frac{1}{2}K_3C_A^2}_{r_D}$$

$r_{A,B,C,D}$

rate of 'generation' of
A,B,C,D per unit volume

$$\begin{aligned}K_1 &= 5/6 \\K_2 &= 5/3 \\K_3 &= 1/6\end{aligned}$$

$$F^{\text{cc}}/V = 4/7 \text{ min}^{-1}$$

$$G_{A\ddagger}^{\text{ss}} = 10 \text{ mol/l}$$

$$C_{A\text{ss}} = 3 \text{ mol/l}$$

$$C_{B\text{ss}} = 1.1140 \text{ mol/l}$$

$$C_{C\text{ss}} = 3.2580 \text{ mol/l}$$

$$C_{D\text{ss}} = 1.3125 \text{ mol/l}$$

$$\frac{dC_A}{dt} = \frac{F}{V} (C_{A_i} - C_A) - K_1 C_A - K_3 C_A^2$$

STATES

$$C_A, C_B, C_D, C_C$$

$$\frac{dC_B}{dt} = \frac{F}{V} (-C_B) + K_1 C_A - K_2 C_B$$

INPUTS

$$\frac{dC_C}{dt} = \frac{F}{V} (-C_C) + K_2 C_B$$

$$F \text{ or } F/V$$

$$\frac{dC_D}{dt} = \frac{F}{V} (-C_D) + 1/2 K_3 C_A^2$$

PARAMETERS

Assume that B is desired product and thus we measure its concentration (only)

$$K_1, K_2, K_3$$

$$y = C_B$$

STEADY STATE CONDITIONS

$$* \frac{dC_A}{dt} = 0 \Rightarrow \frac{F}{V} [C_{A_i} - C_A] - K_1 C_A - K_3 C_A^2 = 0$$

$$-K_3 C_A^2 - C_A \left[\frac{F}{V} + K_1 \right] + \frac{F}{V} C_{A_i} = 0$$

$$\tilde{K}_3 C_A^2 + \left[\frac{F}{V} + K_1 \right] C_A - \frac{F}{V} C_{A_i} = 0$$

$$\boxed{\frac{C_A^{ss}}{C_A}} = \frac{-(K_1 + \frac{F^{ss}}{V})}{2K_3} + \frac{\sqrt{(K_1 + F^{ss}/V)^2 + 4K_3(F^{ss}/V)C_{A_i}^{ss}}}{2K_3}$$

$$ax^2 + bx + c = 0$$

$$x = \frac{-b \pm \sqrt{b^2 - 4ac}}{2a}$$

$$* \frac{dC_B}{dt} \Rightarrow -C_B \left[\frac{F}{V} + K_2 \right] + K_1 C_A = 0$$

CONSIDER THE
POSITIVE ROOT

$$\left[\frac{F^{ss}}{V} + K_2 \right] C_B^{ss} - K_1 C_A^{ss} = 0$$

$$\boxed{\frac{C_B^{ss}}{C_A}} = K_1 C_A^{ss} / \left[\frac{F^{ss}}{V} + K_2 \right]$$

$$= K_1 \left[\frac{-K_1 + F^{ss}/V}{2K_3} + \frac{\sqrt{(K_1 + F^{ss}/V)^2 + 4K_3(F^{ss}/V)C_{A_i}^{ss}}}{2K_3} \right]$$

$$\left[\frac{F^{ss}}{V} + K_2 \right]$$

$$* \frac{dC_C}{dt} = 0 \rightsquigarrow -C_C [F/V] + K_2 C_B = 0$$

$$F/V C_C - K_2 C_B = 0$$

$$\boxed{C_C^{ss}} = \frac{K_2 C_B^{ss} / (F/V)}{K_2 \left[\frac{-K_1 + F^{ss}/V}{2K_3} + \frac{\sqrt{(K_1 + F^{ss}/V)^2 + 4K_3(F^{ss}/V)C_A^{ss}}}{2K_3} \right] / \left[\frac{F^{ss}/V}{K_2} + \right]}$$

$$* \frac{dC_D}{dt} = 0 \rightsquigarrow -\frac{F}{V} C_D + \frac{1}{2} K_3 C_A^2 = 0$$

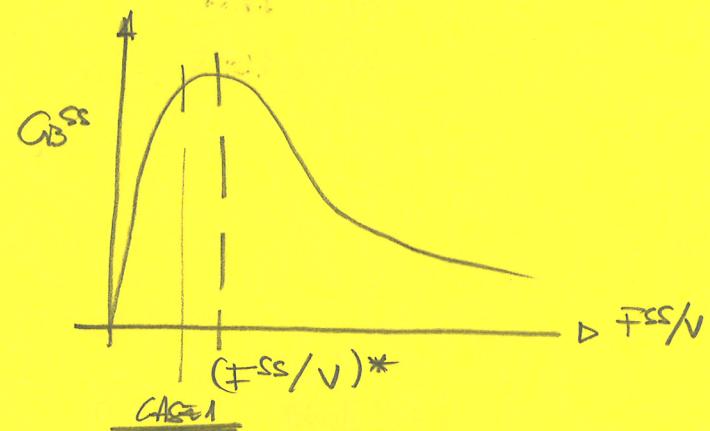
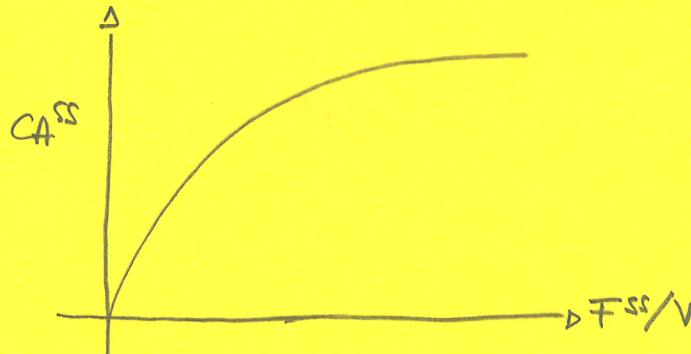
$$F/V C_D - 1/2 K_3 C_A^2 = 0$$

$$\boxed{C_D^{ss}} = \frac{1/2 K_3 C_A^{ss 2}}{(F/V)}$$

$$= \frac{1/2 K_3 \left[\quad \right]^2}{F^{ss}/V}$$

PLOT THE STEADY STATE CONCENTRATION OF C_B (C_B^{ss})
AS A FUNCTION OF THE STATE VELORITY (F^{ss}/V)

BY STUDYING THE EXPRESSION OF C_B^{ss} AS FUNCTION OF F^{ss}/V
WE CAN DERIVE THE SO-CALLED INPUT-OUTPUT CURVE



IT IS EASY TO SEE THAT THERE IS A MAXIMUM VALUE OF THE CONCENTRATION OF B

→ IF THE OBJECTIVE IS TO MAXIMIZE THE PRODUCTION OF B,
THEN THERE EXISTS AN OPTIMUM RESIDENCE TIME
($\approx 1.292 \text{ min}^{-1}$)

LINER
THE STATE SPACE MODEL OF THE NONLINEAR REPRESENTATION

$$\dot{x} = Ax + Bu$$

$$y = Cx$$

WE FIRST DEFINE THE VARIABLES

$$x = \begin{bmatrix} C_A - C_A^{ss} \\ C_B - C_B^{ss} \end{bmatrix} \quad (\begin{bmatrix} C_A - C_A^{ss} \\ C_B - C_B^{ss} \\ C_C - C_C^{ss} \\ C_D - C_D^{ss} \end{bmatrix})$$

$$u = [F/V - F^{ss}/V]$$

$$y = \begin{bmatrix} C_A - C_A^{ss} \\ C_B - C_B^{ss} \end{bmatrix}$$

$$\begin{aligned} \frac{dC_A}{dt} &= F/V (C_{A1} - C_A) - K_1 C_A - K_3 C_A^2 \\ \frac{dC_B}{dt} &= F/V (-C_B) + K_1 C_A - K_2 C_B \\ \frac{dC_C}{dt} &= F/V (-C_C) + K_2 C_B \\ \frac{dC_D}{dt} &= F/V (-C_B) + 1/2 K_3 C_A^2 \end{aligned}$$

THE DYNAMICS

$$\begin{aligned}
 x_1^{ss} &= 3 & u_1^{ss} &= 4/4 \\
 x_2^{ss} &= -1.117 & u_2^{ss} &= -10 \\
 x_3^{ss} &= -3.258 & & \\
 x_4^{ss} &= -1.3125 & &
 \end{aligned}$$

$$A = \begin{bmatrix} -2.4048 & 0 & 0 & 0 \\ 5/6 & -2.2381 & 0 & 0 \\ 0 & 5/3 & -4/4 & 0 \\ 0.5 & 0 & 0 & -4/4 \end{bmatrix}$$

$$B = \begin{bmatrix} 7 & 10 \\ -1.117 & 0 \\ -3.258 & 0 \\ -1.3125 & 0 \end{bmatrix}$$

$$\frac{dx_1}{dt} = u_1 (c_{A1} - x_1) - k_1 x_1 - k_3 x_1^2$$

$$\frac{dx_2}{dt} = u_1 (-x_2) + k_1 x_1 - k_2 x_2$$

$$\frac{dx_3}{dt} = u_1 (-x_3) + k_2 x_2$$

$$\frac{dx_4}{dt} = u_1 (-x_4) + \frac{1}{2} k_3 x_1^2$$

$$\frac{\partial f_1}{\partial x_1} = -u_1^{ss} - k_1 - 2k_3 x_1^{ss}$$

$$\frac{\partial f_1}{\partial x_2} = 0 \quad \frac{\partial f_2}{\partial x_3} = 0$$

$$\frac{\partial f_1}{\partial x_4} = 0$$

$$\frac{\partial f_2}{\partial x_1} = k_1$$

$$\frac{\partial f_2}{\partial x_2} = -u_1^{ss} - k_2 \quad \frac{\partial f_2}{\partial x_3} = 0 \quad \frac{\partial f_2}{\partial x_4} = 0$$

$$\frac{\partial f_3}{\partial x_1} = 0 \quad \frac{\partial f_3}{\partial x_2} = +k_2 \quad \frac{\partial f_3}{\partial x_3} = -u_1^{ss} \quad \frac{\partial f_3}{\partial x_4} = 0$$

$$\frac{\partial f_4}{\partial x_1} = \frac{1}{2} 2k_3 x_1^{ss} \quad \frac{\partial f_4}{\partial x_2} = -u_1^{ss} \quad \frac{\partial f_4}{\partial x_3} = 0 \quad \frac{\partial f_4}{\partial x_4} = 0$$

$$\begin{bmatrix} -u_1^{ss} - k_1 - 2k_3 x_1^{ss} & 0 & 0 & 0 \\ k_1 & -u_1^{ss} - k_2 & 0 & 0 \\ 0 & k_2 & -u_1^{ss} & 0 \\ k_3 x_1^{ss} & 0 & 0 & -u_1^{ss} \end{bmatrix}$$

$$x_1^{ss} = 3 \text{ mol/l}$$

$$x_2^{ss} = 1.117 \text{ mol/l}$$

$$x_3^{ss} = 3.218 \text{ mol/l}$$

$$x_4^{ss} = 1.3125 \text{ mol/l}$$

$$M_1^{ss} = \frac{4}{7} \text{ min}^{-1}$$

$$(x_1, x_2, x_3, x_4)^{ss}$$

$$k_1 = 516$$

$$k_2 = 513$$

$$k_3 = 116$$

$$u_2^{ss} =$$

(5)

$$C_{A_1}^{ss} = 10 \text{ mol/l}$$

$$\underbrace{\begin{bmatrix} 10-3 & 10 \\ -1117 & 0 \\ -3.258 & 0 \\ \cancel{-1.117} & 0 \\ -1.3125 \end{bmatrix}}_B$$

← 4

$$\frac{\partial f_1}{\partial x_1} = \frac{\partial f_1}{\partial (C_A - C_A^s)} = \frac{\partial f_1}{\partial C_A} = -\frac{F_{ss}}{V} - K_1 - 2K_3 C_A^{ss}$$

A₁₁

$$\frac{\partial f_1}{\partial x_2} = \frac{\partial f_1}{\partial (C_B - C_B^s)} = \frac{\partial f_1}{\partial C_B} = 0$$

A₁₂

$$\frac{\partial f_2}{\partial x_1} = \frac{\partial f_2}{\partial (C_A - C_A^s)} = \frac{\partial f_2}{\partial C_A} = K_1$$

A₂₁

$$\frac{\partial f_2}{\partial x_2} = \frac{\partial f_2}{\partial (C_B - C_B^s)} = \frac{\partial f_2}{\partial C_B} = -\frac{F_{ss}}{V} - K_2$$

A₂₂

$$\frac{\partial f_1}{\partial u_1} = \frac{\partial f_1}{\partial (F/V - F_{ss}/V)} = \frac{\partial f_1}{\partial (F/V)} = C_{Af}^{ss} - C_A^{ss}$$

B₁₁

$$\frac{\partial f_2}{\partial u_1} = \frac{\partial f_2}{\partial (F/V - F_{ss}/V)} = \frac{\partial f_2}{\partial (F/V)} = -C_{Bss}$$

B₁₂

WE OBTAIN THE FOLLOWING SYSTEM MATRICES

$$A = \begin{bmatrix} -F/V - K_1 - 2K_3 C_A^{ss} & 0 \\ K_1 & -F_{ss}/V - K_2 \end{bmatrix}$$

$$B = \begin{bmatrix} C_{Af}^{ss} - C_A^{ss} \\ -C_{Bss} \end{bmatrix}$$

The matrices can be particularised by considering different steady state operating points

CASE 1

CASE 2

CASE 3

$$K_1 = 5/6$$

$$K_2 = 5/3$$

$$K_3 = 1/6$$

$$C_A^{ss} = 3 \text{ mol/l}$$

$$C_B^{ss} = 1.140 \text{ mol/l}$$

$$C_C^{ss} = 3.1880 \text{ mol/l}$$

$$C_D^{ss} = 1.3125 \text{ mol/l}$$

-2238

-2.408

A

$$\begin{bmatrix} -\frac{1}{4} - \frac{5}{6} - \frac{2}{1} \cdot \frac{1}{6} \cdot 3 & 0 & 0 & 0 \\ \frac{5}{6} & -\frac{1}{4} - \frac{5}{3} & 0 & 0 \\ 0 & \frac{5}{3} & -\frac{1}{4} & 0 \\ \frac{1}{1} \cdot 3 & 0 & 0 & -\frac{1}{4} \end{bmatrix}$$

4

$$\frac{\partial f_1}{\partial u_1} = \frac{M_2}{C_{Ai}} - x_1$$

$$\frac{\partial f_2}{\partial u_1} = -x_2$$

$$\frac{\partial f_3}{\partial u_1} = -x_3$$

$$\frac{\partial f_4}{\partial u_1} = -x_4$$

$$B = \begin{bmatrix} \frac{M_2^{ss}}{C_{Ai}^{ss}} - x_1^{ss} & u_1^{ss} \\ -x_2^{ss} & 0 \\ -x_3^{ss} & 0 \\ -x_4^{ss} & 0 \end{bmatrix}$$

$x_1^{ss} = 3 \text{ mol/lit}$
 $x_2^{ss} = 1.114 \text{ mol/lit}$
 $x_3^{ss} = 3.258 \text{ mol/lit}$
 $x_4^{ss} = 1.3175 \text{ mol/lit}$
 $M_i^{ss} = h/4$
 $C_{Ai}^{ss} = 10 \text{ mol/lit}$
 $M_2^{ss} = 10$

$$\frac{\partial f_1}{\partial u_2} = u_1$$

$$\frac{\partial f_2}{\partial u_2} = 0$$

$$\frac{\partial f_3}{\partial u_2} = 0$$

$$\frac{\partial f_4}{\partial u_2} = 0$$

