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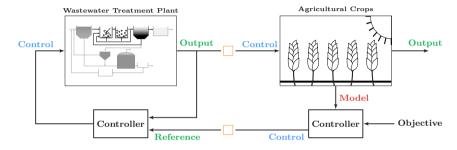
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Introduction and motivation*

- ▶ Goal: Water reuse for agricultural purposes.
 - Nitrogen-based fertigation of crops using activated sludge plants.



Motivation

We investigate the possibility to operate a common class of activated sludge plants to produce effluent wastewater of tailored quality for crop irrigation.

^{*} This study has been done within the international project Control4Reuse. We acknowledge FUNCAP and the French Research National Agency for funding the Brazilian and French part of this project, respectively.

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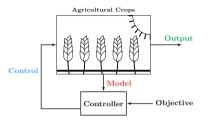
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Dynamical systems, crop growth system



We consider the model of a continuously irrigated crop

- \leadsto Modern corn cultivar grown on a silty loam type soil
- → Dynamics are described by Pelak et al (2017)[1]

$$\begin{split} \dot{x}_C(t) &= f_C(x_C(t), u_C(t)|\theta_C) \\ \text{w/} \ x_C(t) &= [C \ B \ S \ N]^\mathsf{T} \text{ and } u_C(t) = [I \ F_N]^\mathsf{T} \end{split}$$

Optimal crop growth problem

$$\begin{aligned} \max_{u_C(\cdot)} \quad & B(T) \\ \text{s.t.} \quad & \dot{x}_C(t) = f_C(x_C(t), u_C(t)|\theta_C), \\ & u_C(t) \in [0, I^{\max}] \times [0, F_N^{\max}], \\ & x_C(0) = x_0. \end{aligned}$$

Nitrogen demand for optimal crop growth

- ▶ Maximisation of final biomass production
- → Solved using dynamic programming
- ► Analysed for three different Scenarios

[1] Pelak, N., Revelli, R., Porporato, A., 2017. A dynamical systems framework for crop models: Toward optimal fertilization and irrigation strategies under climatic variability. Ecological Modelling.

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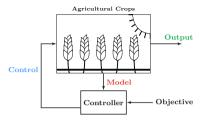
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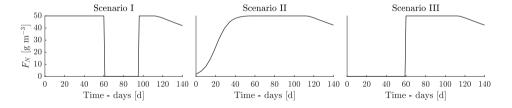
We consider the model of a continuously irrigated crop

- \leadsto Modern corn cultivar grown on a silty loam type soil
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$$\dot{x}_C(t) = f_C(x_C(t), u_C(t)|\theta_C)$$

$$\mathbf{w}/\mathbf{x}_C(t) = [C \ B \ S \ N]^\mathsf{T} \text{ and } u_C(t) = [I \ F_N]^\mathsf{T}$$

The nitrogen concentrations of the irrigation water are considered as reference trajectories



[1] Pelak, N., Revelli, R., Porporato, A., 2017. A dynamical systems framework for crop models: Toward optimal fertilization and irrigation strategies under climatic variability. Ecological Modelling.

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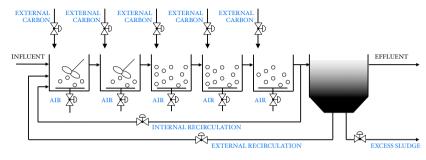
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Dynamical systems, activated sludge plants



We consider a conventional Activated Sludge Process (ASP)

► The Benchmark Simulation Model no. 1 (BSM1)^[2]

Plant layout

- → 5 sequential bio-reactors (Activated Sludge Model no. 1)
- → 1 non-reactive settler (10-layers double-exponential settling model)

^[2] Gernaey, K., Jeppsson, U., Vanrolleghem, P., Copp, J., 2014. Benchmarking of Control Strategies for Wastewater Treatment Plants. IWA.

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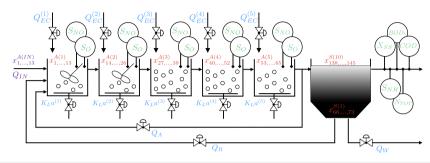
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Dynamical systems, activated sludge plants (cont.)



$$\begin{array}{c} \boldsymbol{x}(t) = [x^{A(1)} \cdots x^{A(5)} x^{S(1)} \cdots x^{S(10)}]^{\mathsf{T}} \\ \dot{\boldsymbol{x}}(t) = f(\boldsymbol{x}(t), \boldsymbol{u}(t), \boldsymbol{w}(t) | \boldsymbol{\theta}_{\boldsymbol{x}}) \\ \boldsymbol{y}(t) = g(\boldsymbol{x}(t) | \boldsymbol{\theta}_{\boldsymbol{y}}) \end{array} \qquad \begin{array}{c} \boldsymbol{x}(t) = [Q_A \ Q_R \ Q_W \ \boldsymbol{u}^{A(1)} \cdots \boldsymbol{u}^{A(5)}]^{\mathsf{T}} \\ \boldsymbol{y}(t) = [y^{A(1)} \cdots y^{A(5)} y^{S(10)}]^{\mathsf{T}} \\ \boldsymbol{y}(t) = [Q_{IN} \ x^{A(IN)}]^{\mathsf{T}} \end{array} \qquad \boldsymbol{\theta}_{\boldsymbol{x}}, \boldsymbol{\theta}_{\boldsymbol{y}} \} \text{: Model parameters}$$

▶ An "expanded model" when compared to common representations

$$\sim N_x = 5 \times 13 + 10 \times 8$$
 $\sim N_u = 3 + 5 \times 2$ $\sim N_w = 1 + 13$ $\sim N_y = 5 \times 2 + 5$ = 14 disturbances = 15 sensors

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Model predictive control, formulation

Model predictive control problem

$$\min_{\substack{u_k, \dots, u_{k+N-1} \\ \forall n \in [k, k+N-1]}} \sum_{n=k}^{k+N-1} L(x_n, u_n) + L_f(x_{k+N})$$
s.t.
$$\forall n \in [k, k+N-1]$$

$$x_{n+1} = f_{\Delta t}(x_n, u_n, \hat{w}_n | \theta_x)$$

$$x_n \in \mathcal{X}, \quad u_n \in \mathcal{U},$$

$$\Phi(x_k, x_{k+N}) = 0$$

- \longrightarrow Finite horizon of size N > 0
- Stage and terminal cost functions $L(\cdot): \mathbb{R}^{N_x} \times \mathbb{R}^{N_u} \to \mathbb{R}$

$$L_f(\cdot): \mathbb{R}^{N_x} \to \mathbb{R}$$
 \longrightarrow Path constraint sets

 $\mathcal{X} \subseteq \mathbb{R}^{N_x}, \quad \mathcal{U} \subseteq \mathbb{R}^{N_u}$

→ Initial and terminal conditions $\Phi(\cdot): \mathbb{R}^{N_x} \times \mathbb{R}^{N_x} \to \mathbb{R}^{N_\Phi}$

Discretise-then-optimise: The problem is transcribed into a NLP then solved numerically

▶ Zero-order hold of controls (given $\Delta t > 0$):

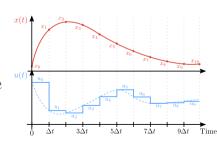
$$u(t) = u(t_n) \ (t \in [t_n, t_{n+1})), \quad t_n = n\Delta t$$

Evolution given by transition function

$$x_{n+1} = f_{\Delta t}(x_n, u_n, \hat{w}_n) = x_n + \int_{t_n}^{t_{n+1}} f(x(t), u_n, \hat{w}_n) dt$$

Fixed disturbances at each horizon (given $\Delta t_w > 0$)

$$\hat{w}_n = w_{\lfloor \frac{k\Delta t}{\Delta t_w} \rfloor} = w(\lfloor \frac{k\Delta t}{\Delta t_w} \rfloor \Delta t_w)$$



Formulation

Model predictive control, formulation (cont.)

Constrained affine quadratic regulator (c-AQR) k + N - 1

$$\begin{split} & \min_{\substack{u_k,...,u_{k+N-1}\\ v_n \in [k,k+N-1]}} & \sum_{n=k} \left(\|x_n - x_n^{sp}\|_Q^2 + \|u_n - u_n^{sp}\|_R^2 \right) + \|x_{k+N} - x_{k+N}^{sp}\|_Q^2 \\ & \text{s.t.} & \\ & x_{n+1} = z_{\Delta t}^{(k)} + A_{\Delta t}^{(k)} x_n + B_{\Delta t}^{(k)} u_n + G_{\Delta t}^{(k)} \hat{w}_n \\ & & H_x x_n \le h_x, \quad H_u u_n \le h_u, \\ & x_k = \hat{x}_k \end{split}$$

c-AQR: We consider affine dynamical constraints and quadratic cost functions

Quadratic cost functions

$$L(\cdot) = \|x_n - x_n^{sp}\|_Q^2 + \|u_n - u_n^{sp}\|_R^2$$

$$L_f(\cdot) = \|x_{k+N} - x_{k+N}^{sp}\|_Q^2$$

Linearisation of $f(\cdot)$ around $P_k := (x_k^{sp}, u_k^{sp}, w_k^{sp})$

$$x_{n+1} = z_{\Delta t}^{(k)} + A_{\Delta t}^{(k)} x_n + B_{\Delta t}^{(k)} u_n + G_{\Delta t}^{(k)} \hat{w}_n$$

Convex constraint sets

$$\mathcal{X} = \{ \mathbf{x} \in \mathbb{R}^{N_x} \mid H_x \mathbf{x} \le h_x \}$$
$$\mathcal{U} = \{ \mathbf{u} \in \mathbb{R}^{N_u} \mid H_u \mathbf{u} \le h_u \}$$

Fixed initial state (given \hat{x}_k)

$$\Phi(x_k, x_{k+N}) = x_k - \hat{x}_k$$

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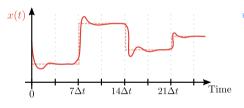
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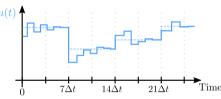
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Model predictive control, zero-offset set-point tracking

- Linearisation-based MPCs cannot ensure zero-offset with a single linearisation
- \longrightarrow **Approach:** Linearise the process around nonconstant references changing every $\Delta t_{sp} > 0$ (With each w_s^{sp} fixed to the available disturbance measurement at the k-th horizon)

$$P = \left\{ (x_m^{sp}, u_m^{sp}, w_m^{sp}) : x_m^{sp} = x^{sp} (m\Delta t_{sp}), \ u_m^{sp} = u^{sp} (m\Delta t_{sp}), \ w_m^{sp} = w \left(\lfloor \frac{k\Delta t}{\Delta t_w} \rfloor \Delta t_w \right) \right\}_{m=0}^{M}$$





▶ Affine switching system representation:

(Only the $\lfloor \frac{n\Delta t}{\Delta t_{en}} \rfloor$ -th linearisation is "active" at each n-th instant)

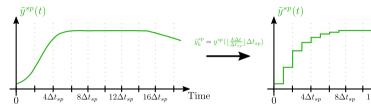
$$\boldsymbol{x_{n+1}} = \sum_{m=0}^{M} \mathbb{I}_{m=\lfloor \frac{n\Delta t}{\Delta t s p} \rfloor} \left(z_{\Delta t}^{(m)} + A_{\Delta t}^{(m)} \boldsymbol{x_n} + B_{\Delta t}^{(m)} \boldsymbol{u_n} + G_{\Delta t}^{(m)} \hat{\boldsymbol{w}_n} \right), \qquad \mathbb{I}_S = \begin{cases} 1 & \text{if S true} \\ 0 & \text{if S false} \end{cases}$$

Formulation

Model predictive control, zero-offset set-point tracking (cont.)

Usually, reference trajectories are available only for (a subset of) output variables

For continuous-time trajectories, we consider a discretisation with $\Delta t_{sp} > 0$



 \longrightarrow Each pair (x_{L}^{sp}, u_{L}^{sp}) satisfying $\tilde{y}_{L}^{sp} \in \mathbb{R}^{N_{\tilde{y}}}$ is the solution of an optimisation:

Steady-state optimisation

(We consider fixed
$$w_k^{sp}=w^{SS}$$
 and $\tilde{u}_k^{sp}=0$)

- Search for stationary point $(x_k^{sp}, u_k^{sp}, w_k^{sp})$
- The $N_{\tilde{y}} \leq N_y$ outputs of interest are selected by matrix $\underline{H} \in \{0, 1\}^{N_{\tilde{y}} \times N_y}$
- $W_{\tilde{u}}, W_u \succeq 0$ are tuning parameters

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Results, MPC simulation (Case I, Scenario I)

Model predictive control parameters

General parameters:

$$\begin{split} T &= 140 \text{ days}, & N = 21 \text{ (7 days)}, & \underset{\sim}{Q} &= C_{\Delta t}^{(k)^{\mathsf{T}}} C_{\Delta t}^{(k)} \\ R &= \text{diag}[\underbrace{10^{-4}}_{Q_A} & \underbrace{0.01}_{Q_R} & \underbrace{0.01}_{Q_W} & \underbrace{10^{-3} I_5}_{K_L a^{(k)}} & \underbrace{10^4 I_5}_{Q_{EC}^{(k)}} \end{split}$$

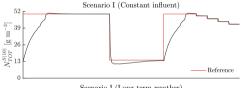
Sampling periods:

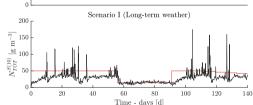
$\Delta t = (1/3)d,$

$$\Delta t_w = 1d,$$
$$\Delta t_{sp} = 7d$$

Influent conditions:

$$w = \begin{cases} \text{CONSTANT INFLUENT} \\ \text{LONG-TERM WEATHER} \end{cases}$$





Case I:
$$(W_{\tilde{y}} = 100, W_u = 0)$$

- → Constant influent: zero-offset is achieved
- → Dynamic influent: performance decreases
- ► The control strategy tracks $N_{TOT}^{S(10)}$ mainly by manipulating $NO_2^- + NO_3^-$ nitrogen

The predictive controller only partially achieves zero-offset under typical influent conditions

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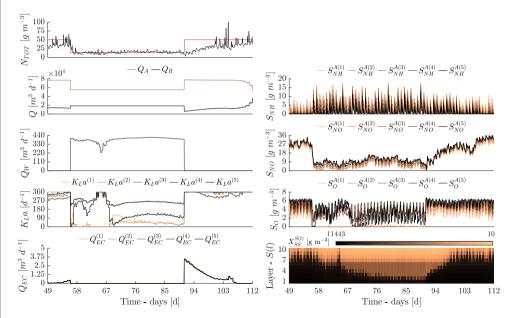
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Results, MPC simulation (Case I, Scenario I, $t \in [49, 112]$)



Simulation results

Results, MPC simulation (Case II, Scenario I)

Model predictive control parameters

General parameters:

$$\begin{split} T &= 140 \text{ days}, & N = 21 \text{ (7 days)}, & \underset{\sim}{Q} &= C_{\Delta t}^{(k)^{\mathsf{T}}} C_{\Delta t}^{(k)} \\ R &= \text{diag}[\underbrace{10^{-4}}_{Q_A} & \underbrace{0.01}_{Q_R} & \underbrace{0.01}_{Q_W} & \underbrace{10^{-3} I_5}_{K_L a^{(k)}} & \underbrace{10^4 I_5}_{Q_{EC}^{(k)}} \end{split}$$

Sampling periods:

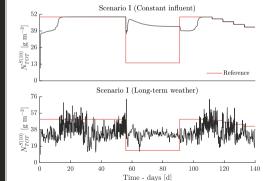
$\Delta t = (1/3)d$,

$$\Delta t_w = 1d,$$

$$\Delta t_{sp} = 7d$$

Influent conditions:

$$w = \begin{cases} \text{CONSTANT INFLUENT} \\ \text{LONG-TERM WEATHER} \end{cases}$$



Case II:
$$(W_{\tilde{y}} = 100, W_u = 0.01I_{N_u})$$

- → Constant influent: zero-offset partly achieved
- → Dynamic influent: performance decreases
- ▶ The control strategy tracks $N_{TOT}^{S(10)}$ mainly by manipulating NH₄+NH₃ nitrogen

The predictive controller partially achieves zero-offset, but is unable to recover to treatment control

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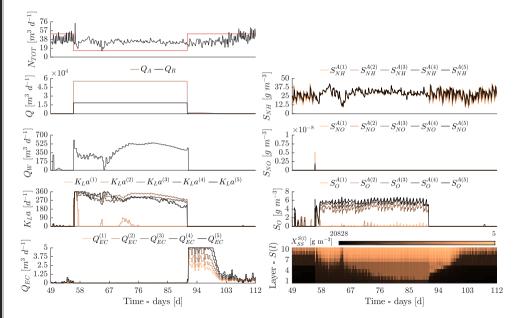
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Results, MPC simulation (Case II, Scenario I, $t \in [49, 112]$)



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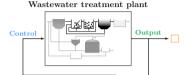
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Output MPC, formulation and estimation problem

▶ Output MPC: Initial state and disturbance (\hat{x}_k, \hat{w}_k) are not measured but rather estimated



Estimator

Moving horizon estimation problem $\min_{\substack{\hat{x}_k - N_e + 1 \\ \hat{w}_k - N_e + 1}} L_0(\hat{x}_{k-N_e+1}) + \sum_{n=k-N_e+1}^k L(\hat{x}_n, \hat{w}_n | y_n)$ s.t. $\forall n \in [k-N_e+1, k]$ $\hat{x}_n \in \mathcal{X} \quad \hat{w}_n \in \mathcal{W}$

The optimal estimation problem derives from a maximum a posteriori estimate solution

→ Stochastic state-space

Controller

$$\begin{split} &\dot{\hat{x}}(t) = f(\hat{x}(t), u(t), \hat{w}(t)|\theta_x) \\ &y(t) = g(\hat{x}(t)|\theta_y) + v(t) \end{split}$$

with
$$\hat{x}(0) \sim e^{-L_0(\hat{x}(0)|Q_{x_0})}$$

 $\hat{w}(t) \stackrel{i.i.d}{\sim} e^{-L_w(\hat{w}(t)|R_w)}$
 $v(t) \stackrel{i.i.d}{\sim} e^{-L_v(v(t)|Q_v)}$

 \triangleright Zero-order hold of disturbances: (Given the rate of measurement Δt_e)

$$\hat{w}(t) = \hat{w}(t_n) \ (t \in [t_n, t_{n+1})), \quad t_n = n\Delta t_e$$

$$\hat{x}_{n+1} = f_{\Delta t_e}(\hat{x}_n, u_n, \hat{w}_n) = \hat{x}_n + \int_{t_n}^{t_{n+1}} f(\hat{x}(t), u_n, \hat{w}_n) dt$$

Formulation

Output MPC, formulation and estimation problem (cont.)

Constrained Affine Gauss-Markov (c-AGM) estimator

$$\min_{\substack{\hat{x}_{k} - N_{e} + 1 \\ \hat{w}_{k} - N_{e} + 1 \\ v_{k} - N_{e} + 1, k}} \|\hat{x}_{k} - N_{e} + 1 - \bar{x}_{k} - N_{e} + 1}\|_{Q_{x_{0}}^{-1}}^{2} + \sum_{n = k - N_{e} + 1}^{k} \left(\|y_{n} - C_{\Delta t_{e}}^{(n)} \hat{x}_{n}\|_{Q_{v}^{-1}}^{2} + \|\hat{w}_{n} - \bar{w}_{n}\|_{R_{w}^{-1}}^{2} \right)$$
s.t.
$$\forall n \in [k - N_{e} + 1, k] \quad \hat{x}_{n+1} = z_{\Delta t_{e}}^{(n)} + A_{\Delta t_{e}}^{(n)} \hat{x}_{n} + B_{\Delta t_{e}}^{(n)} u_{n} + G_{\Delta t_{e}}^{(n)} \hat{w}_{n}$$

$$H_{x} \hat{x}_{n} \leq h_{x}, \quad H_{w} \hat{w}_{n} \leq h_{w}$$

··· c-AGM: We assume Gaussian distributions and affine dynamical models

(Given means $(\bar{x}_{k-N_e+1}, \{\bar{w}_n\}_{k-N_e+1}^k)$ as the solutions from the previous horizon)

$$\hat{\boldsymbol{x}}_{k-N_e} \sim \mathcal{N}(\bar{\boldsymbol{x}}_{k+N_e}, Q_{x_0}), \quad \hat{\boldsymbol{w}}_n \overset{i.i.d}{\sim} \mathcal{N}(\bar{\boldsymbol{w}}_n, R_w), \quad \boldsymbol{v}_n \overset{i.i.d}{\sim} \mathcal{N}(0, Q_v)$$

Linearisations of $f(\cdot)$ around each $P_n := (\hat{x}_n, u_n, \hat{w}_n)$

(Given (\bar{x}_n, \bar{w}_n) as the estimates from the previous horizon)

$$\hat{x}_{n+1} = z_{\Delta t_e}^{(n)} + A_{\Delta t_e}^{(n)} \hat{x}_n + B_{\Delta t_e}^{(n)} u_n + G_{\Delta t_e}^{(n)} \hat{w}_n$$
$$y_n = C_{\Delta t_e}^{(n)} \hat{x}_n + v_n$$

Convex support sets

$$\mathcal{X} = \{ \mathbf{x} \in \mathbb{R}^{N_x} \mid H_x \mathbf{x} \le h_x \}$$
$$\mathcal{W} = \{ w \in \mathbb{R}^{N_w} \mid H_w w \le h_w \}$$

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Results, Output MPC simulation (Case I, Scenario I)

Output model predictive control parameters*

General parameters:

$$T=140~{\rm days}, \quad N_e=12~(3~{\rm hours}),$$

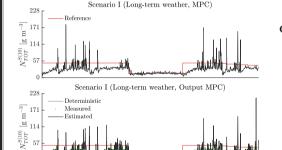
$$Q_{x_0} = \operatorname{diag}[(0.01y^{SS})^2], \ Q_v, R_w = \operatorname{diag}[\cdots]$$

Sampling periods:

$$\Delta t_e = (1/96)d$$

Influent conditions:

$$w = {\tt LONG-TERM}$$
 WEATHER



100

60 80 Time - days [d] Case I: $(W_{\tilde{y}} = 100, W_u = 0)$

- \leadsto The internal state is accurately estimated
- → Slight performance improvement

The Output MPC provides similar results to the MPC, implying accuracy in the state and disturbance estimation

^{*} The control-related parameters are the same as in the previous section. Steady-state $SS := (x^{SS}, u^{SS}, w^{SS}, y^{SS})$ is the operating point suggested by the benchmark.

Final remarks

The predictive control of activated sludge plants for water reuse was investigated

Our results show that

- ✓ Zero-offset is achieved under constant influent conditions
- × The nitrogen demand is only partially met under typical influent conditions
- An ad hoc tuning of the predictive controller leads to alternative control policies
 - I. $(W_u = 0)$: The controller favours manipulating $NO_2 + NO_3$ nitrogen
 - II. $(W_u = 0.01 I_{N_u})$: The controller favours manipulating NH₄⁺+NH₃ nitrogen

The MPC tracking accuracy is summarised by the normalized mean-squared error (NMSE)

$$J_{\text{NMSE}}(\tilde{y}, \tilde{y}^{sp}) = \frac{1}{t_f - t_0} \int_{t_0}^{t_f} ||\tilde{y}(t) - \tilde{y}^{sp}(t)||^2 / ||\tilde{y}(t)||^2 dt$$

	Case I		Case II	
	$J_{ m NMSE}$	$J_{ m NMSE}$	$J_{ m NMSE}$	$J_{ m NMSE}$
	(Constant influent)	(Dynamic influent)	(Constant influent)	(Dynamic influent)
Scenario I Scenario II Scenario III	0.1612 0.0500 0.0820	0.9797 0.4309 0.6611	0.1573 0.0159 0.0366	0.4117 0.3255 0.2531

Thank you! Questions?