

Linearisation of nonlinear models: Example CHEM-E7190 (was E7140), 2022

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Example II

Example II Linearisation of nonlinear models

Example II

We consider two irreversible chemical reactions in a perfectly mixed chemical reactor

- $A \longrightarrow B \longrightarrow C$
- $2A \longrightarrow D$

The two reactions compete to convert species A, species B is the desired product

The chemical reactor operates in liquid-phase

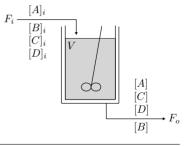
- \leadsto Assume constant volume, $V \neq V(t)$
- \rightarrow Assume constant density, $\rho \neq \rho(t)$

Assume constant temperature

$$\rightarrow$$
 $T(t) \neq T(t)$

Volumetric flow-rates

$$\rightarrow$$
 $F_i(t)$ and $F_o(t)$



Our interest is in understanding the dynamics of the concentrations inside the reactor $\frac{1}{2}$

- \rightarrow The concentration of species A, B, C and D, as a function of time
- [A](t), [B](t), [C](t), and [D](t) (molar concentrations, [mol lt⁻¹])

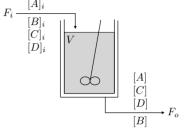
Example II

Reaction rate constants (per unit volume)

$$A \xrightarrow{k_1} B \xrightarrow{k_2} C$$
$$2A \xrightarrow{k_3} D$$

Assume that only component A is fed

- $[B]_i(t), [C]_i(t), [D]_i(t) = 0$
- $\bullet \ [A]_i(t) \neq 0$



The total material balance, under the assumption of a constant volume in the tank

Total mass balance

$$\frac{\mathrm{d}V(t)}{\mathrm{d}t} = F_i(t) - F_o(t) = 0$$

As a result, we simplify notation

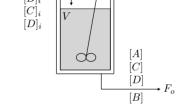
- V(t) = constant = V
- $F_i(t) = F_o(t) = F(t)$

Example II

$$A \xrightarrow{k_1} B \xrightarrow{k_2} C$$

$$2A \xrightarrow{k_3} D$$

- $[B]_i(t), [C]_i(t), [D]_i(t) = 0$
- $[A]_i(t) \neq 0$



Mass balance for component A

$$\frac{\mathrm{d}}{\mathrm{d}t}V[A](t) = F(t)[A]_i(t) - F(t)[A](t) - Vk_1[A](t) - Vk_3[A]^2(t)$$

$$= \frac{F(t)}{V}\Big([A]_i(t) - [A](t)\Big) - k_1[A](t) - k_3[A]^2(t)$$

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Example II

$$A \xrightarrow{k_1} B \xrightarrow{k_2} C$$

$$2A \xrightarrow{k_3} D$$

• $[B]_i(t), [C]_i(t), [D]_i(t) = 0$

• $[A]_i(t) \neq 0$

Mass balance for component B, C, and D $\frac{\mathrm{d}}{\mathrm{d}t}[B](t) = \frac{F(t)}{V} \left(\underbrace{[B]_{\tau}(t)}_{\tau} - [B](t) \right) + k_1[A](t) - k_2[B](t)$

$$\frac{V}{V} \left(\underbrace{[B]_{\tau}(t)}_{=0} - [B](t) \right) + k_1[A](t)$$

$$= 0$$

$$V \left(\underbrace{[C]_{\tau}(t)}_{=0} - [C](t) \right) + k_2[B](t)$$

$$\frac{d}{dt}[C](t) = \frac{F(t)}{V} \left(\underbrace{[C]_{\tau}(t)}_{=0} - [C](t) \right) + k_2[B](t)$$

$$\frac{d}{dt}[D](t) = \frac{F(t)}{V} \left(\underbrace{[D]_{\tau}(t)}_{=0} - [D](t) \right) + \frac{1}{2}k_3[A]^2(t)$$

Example II

Example II (cont.)

$$A \xrightarrow{k_1} B \xrightarrow{k_2} C$$
$$2A \xrightarrow{k_3} D$$

• $[B]_i(t), [C]_i(t), [D]_i(t) = 0$

• $[A]_i(t) \neq 0$

Putting things together, we get the dynamics of the state-space model of the reactor

$$\frac{\mathrm{d}}{\mathrm{d}t}[A](t) = \frac{F(t)}{V} \Big([A]_i(t) - [A](t) \Big) - k_1[A](t) - k_3[A]^2(t)$$

$$\frac{\mathrm{d}}{\mathrm{d}t}[B](t) = -\frac{F(t)}{V}[B](t) + k_1[A](t) - k_2[B](t)$$

$$k_3[A]^-(t)$$

 $k_1 = 5/6 \text{ [min}^{-1}]$
 $k_2 = 5/3 \text{ [min}^{-1}]$

$$\frac{d}{dt}[C](t) = -\frac{F(t)}{V}[C](t) + k_2[B](t)$$

$$\frac{d}{dt}[D](t) = -\frac{F(t)}{V}[D](t) + \frac{1}{2}k_3[A]^2(t)$$

$$= 5/6 \text{ [min}^{-1}]$$

 $k_3 = 1/6 \left[lt(mol^{-1}min^{-1}) \right]$

Example II

$$\begin{split} \frac{\mathrm{d}}{\mathrm{d}t}[A](t) &= \frac{F(t)}{V} \Big([A]_i(t) - [A](t) \Big) - k_1 [A](t) - k_3 [A]^2(t) \\ \frac{\mathrm{d}}{\mathrm{d}t}[B](t) &= -\frac{F(t)}{V} [B](t) + k_1 [A](t) - k_2 [B](t) \\ \frac{\mathrm{d}}{\mathrm{d}t}[C](t) &= -\frac{F(t)}{V} [C](t) + k_2 [B](t) \\ \frac{\mathrm{d}}{\mathrm{d}t}[D](t) &= -\frac{F(t)}{V} [D](t) + \frac{1}{2} k_3 [A]^2(t) \end{split}$$

 \rightarrow State variables, x(t)

$$x(t) = \begin{bmatrix} [A](t) \\ [B](t) \\ [C](t) \\ [D](t) \end{bmatrix} = \begin{bmatrix} x_1(t) \\ x_2(t) \\ x_3(t) \\ x_4(t) \end{bmatrix}$$

Example II

$$\frac{d}{dt}[A](t) = \frac{F(t)}{V} ([A]_i(t) - [A](t)) - k_1[A](t) - k_3[A]^2(t)
\frac{d}{dt}[B](t) = -\frac{F(t)}{V}[B](t) + k_1[A](t) - k_2[B](t)
\frac{d}{dt}[C](t) = -\frac{F(t)}{V}[C](t) + k_2[B](t)
\frac{d}{dt}[D](t) = -\frac{F(t)}{V}[D](t) + \frac{1}{2}k_3[A]^2(t)$$

$$\rightsquigarrow$$
 Input variables, $u(t)$

$$u(t) = \begin{bmatrix} F_i(t) \\ [A]_i(t) \end{bmatrix} = \begin{bmatrix} u_1(t) \\ u_2(t) \end{bmatrix}$$

Example II

$$\frac{d}{dt}[A](t) = \frac{F(t)}{V} \Big([A]_i(t) - [A](t) \Big) - k_1 [A](t) - k_3 [A]^2(t)$$

$$\frac{d}{dt}[B](t) = -\frac{F(t)}{V}[B](t) + k_1 [A](t) - k_2 [B](t)$$

$$\frac{d}{dt}[C](t) = -\frac{F(t)}{V}[C](t) + k_2 [B](t)$$

$$\frac{d}{dt}[D](t) = -\frac{F(t)}{V}[D](t) + \frac{1}{2}k_3 [A]^2(t)$$

 \rightsquigarrow Parameters, θ_x

$$\theta_x = \begin{bmatrix} k_1 \\ k_2 \\ k_3 \\ V \end{bmatrix} = \begin{bmatrix} \theta_{x,1} \\ \theta_{x,2} \\ \theta_{x,3} \\ \theta_{x,4} \end{bmatrix}$$

Example II (cont.)

$$\frac{d}{dt}[A](t) = \frac{F(t)}{V} ([A]_i(t) - [A](t)) - k_1[A](t) - k_3[A]^2(t)$$

$$\frac{d}{dt}[B](t) = -\frac{F(t)}{V}[B](t) + k_1[A](t) - k_2[B](t)$$

$$\frac{d}{dt}[C](t) = -\frac{F(t)}{V}[C](t) + k_2[B](t)$$

$$\frac{d}{dt}[D](t) = -\frac{F(t)}{V}[D](t) + \frac{1}{2}k_3[A]^2(t)$$

Using the control notation, we get

$$\frac{dx_1(t)}{dt} = \frac{u_1(t)}{\theta_{x,4}} \left(u_2(t) - x_1(t) \right) - \theta_{x,1} x_1(t) - k_3 x_1^2(t)
\frac{dx_2(t)}{dt} = -\frac{u_1(t)}{\theta_{x,4}} x_2(t) + \theta_{x,1} x_1(t) - \theta_{x,2} x_2(t)
\frac{dx_3(t)}{dt} = -\frac{u_1(t)}{\theta_{x,4}} x_3(t) + \theta_{x,2} x_2(t)
\frac{dx_4(t)}{dt} = -\frac{u_1(t)}{\theta_{x,4}} x_4(t) + \frac{1}{2} \theta_{x,3} x_1^2(t)$$

Example II

$$\frac{dx_{1}(t)}{dt} = \underbrace{\frac{u_{1}(t)}{\theta_{x,4}}}_{f_{1}(x,u|\theta_{x})} \left(u_{2}(t) - x_{1}(t) \right) - \theta_{x,1}x_{1}(t) - k_{3}x_{1}^{2}(t) \right)_{f_{1}(x,u|\theta_{x})}$$

$$\frac{dx_{2}(t)}{dt} = \underbrace{-\frac{u_{1}(t)}{\theta_{x,4}}}_{f_{2}(x,u|\theta_{x})} x_{2}(t) + \theta_{x,1}x_{1}(t) - \theta_{x,2}x_{2}(t) \right)_{f_{2}(x,u|\theta_{x})}$$

$$\frac{dx_{3}(t)}{dt} = \underbrace{-\frac{u_{1}(t)}{\theta_{x,4}}}_{f_{3}(x,u|\theta_{x})} x_{3}(t) + \theta_{x,2}x_{2}(t)$$

$$\underbrace{\frac{dx_{4}(t)}{dt}}_{f_{3}(x,u|\theta_{x})} = \underbrace{-\frac{u_{1}(t)}{\theta_{x,4}}}_{f_{4}(x,u|\theta_{x})} x_{4}(t) + \underbrace{\frac{1}{2}\theta_{x,3}x_{1}^{2}(t)}_{f_{4}(x,u|\theta_{x})}$$

$$\Rightarrow$$
 $\dot{x}(t) = f(x(t), \frac{u(t)|\theta_x}{\theta_x})$

Example II

$$\frac{dx_1(t)}{dt} = \frac{u_1(t)}{\theta_{x,4}} \left(u_2(t) - x_1(t) \right) - \theta_{x,1} x_1(t) - k_3 x_1^2(t)
\frac{dx_2(t)}{dt} = -\frac{u_1(t)}{\theta_{x,4}} x_2(t) + \theta_{x,1} x_1(t) - \theta_{x,2} x_2(t)
\frac{dx_3(t)}{dt} = -\frac{u_1(t)}{\theta_{x,4}} x_3(t) + \theta_{x,2} x_2(t)
\frac{dx_4(t)}{dt} = -\frac{u_1(t)}{\theta_{x,4}} x_4(t) + \frac{1}{2} \theta_{x,3} x_1^2(t)$$

Suppose that we are capable of measuring the concentration of B, we then also have

$$\mathbf{y(t)} = \underbrace{\begin{bmatrix} 0 & 1 & 0 & 0 \end{bmatrix}}_{C} \begin{bmatrix} x_1(t) \\ x_2(t) \\ x_3(t) \\ x_4(t) \end{bmatrix} + \underbrace{\begin{bmatrix} 0 & 0 \end{bmatrix}}_{D} \begin{bmatrix} \mathbf{u_1(t)} \\ \mathbf{u_2(t)} \end{bmatrix}}_{g(x(t), \mathbf{u(t)} | \theta_x)}$$

Example II

Example II (cont.)

The dynamics are a set of nonlinear equations, the measurement equation is linear

$$\begin{bmatrix} \dot{x}_1(t) \\ \dot{x}_2(t) \\ \dot{x}_3(t) \\ \dot{x}_4(t) \end{bmatrix} = \begin{bmatrix} \frac{u_1(t)}{\theta_{x,4}} (u_2(t) - x_1(t)) - \theta_{x,1} x_1(t) - k_3 x_1^2(t) \\ -\frac{u_1(t)}{\theta_{x,4}} x_2(t) + \theta_{x,1} x_1(t) - \theta_{x,2} x_2(t) \\ -\frac{u_1(t)}{\theta_{x,4}} x_3(t) + \theta_{x,2} x_2(t) \\ -\frac{u_1(t)}{\theta_{x,4}} x_4(t) + \frac{1}{2} \theta_{x,3} x_1^2(t) \end{bmatrix}$$

$$\mathbf{y}(t) = \begin{bmatrix} 0 & 1 & 0 & 0 \end{bmatrix} \begin{bmatrix} x_1(t) \\ x_2(t) \\ x_3(t) \\ x_4(t) \end{bmatrix} + \begin{bmatrix} 0 & 0 \end{bmatrix} \begin{bmatrix} u_1(t) \\ u_2(t) \end{bmatrix}$$

To be able to proceed with the tools of linear systems theory, we need to linearise

- Approximate nonlinearities with first-order Taylor series expansions
- About some convenient steady-state point, (x^{SS}, u^{SS})

Example II (cont.)

How to determine the steady-state point associated to a desirable operating conditions?

- By simulation, integrate the model until stationarity is reached
- By optimisation, solve f(x, u) = 0 with respect to x and u

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Example II (cont.)

Sometimes, it can also be worked out from the model equations at steady-state (x_{SS}, u_{SS})

At steady-state all derivative are zero, for component [A] we thus have

$$\frac{d[A](t)}{dt} = \frac{F_i^{SS}}{V} \left([A]_i^{SS} - [A](t) \right) - k_1 [A](t) - k_3 [A]^2(t)$$

$$= -k_3 [A]^2(t) - [A](t) \left(\frac{F_i^{SS}}{V} + k_1 \right) + \frac{F_i^{SS}}{V} [A]_i^{SS}$$

$$= 0$$

We get the second-order equation in the variable [A](t),

$$k_3[A]^2(t) + \left(\frac{F_i^{SS}}{V} + k_1\right)[A](t) - \frac{F_i^{SS}}{V}[A]_i = 0$$

Second-order equation:
$$ax^2 + bx + c = 0$$
 with solutions $x_{1,2} = \frac{-b \pm \sqrt{b^2 - 4ac}}{2a}$

Example II (cont.)

$$\underbrace{k_3[A]^2(t)}_{ax^2} + \underbrace{\left(\frac{F_i^{SS}}{V} + k_1\right)[A](t)}_{bx} - \underbrace{\frac{F_i^{SS}}{V}[A]_i}_{-c} = 0$$

The steady-state values for [A], given F_i^{SS} and $[A]_i^{SS}$

$$[A]_{1,2}^{SS} = \frac{-\left(k_1 + \frac{F_i^{SS}}{V}\right)}{2k_3} \pm \sqrt{\frac{\left(k_1 + \frac{F_i^{SS}}{V}\right)^2 + 4k_3 \frac{F_i^{SS}}{V} [A]_i^{SS}}{2k_3}}$$

We need to consider only the root where [A] is positive,

$$[A]^{SS} = \frac{-\left(k_1 + \frac{F_i^{SS}}{V}\right)}{2k_3} + \sqrt{\frac{\left(k_1 + \frac{F_i^{SS}}{V}\right)^2 + 4k_3 \frac{F_i^{SS}}{V}[A]_i^{SS}}{2k_3}}$$

Proceeding similarly for component [B], we can write

$$\frac{d[B](t)}{dt} = -[B](t) \left(\frac{F_i^{SS}}{V} + k_2 \right) + k_1 \underbrace{[A](t)}_{[A]^{SS}}$$

$$= 0$$

We get the first-order equation in [B](t)

$$[B](t)\left(\frac{F_i^{SS}}{V} + k_2\right) - k_1[A]^{SS} = 0$$

The steady-state value for [B],

$$[B]^{SS} = \frac{k_1[A]^{SS}}{\left(\frac{F^{SS}}{V} + k_2\right)}$$

given F_i^{SS} , $[A]_i^{SS}$, and $[A]^{SS}$

Example II

Substituting $[A]^{SS}$, we get

$$[B]^{SS} = \frac{k_1[A]^{SS}}{\left(\frac{F^{SS}}{V} + k_2\right)}$$

$$= k_1 \left(\frac{-\left(k_1 + \frac{F_i^{SS}}{V}\right) + \sqrt{\left(k_1 + \frac{F_i^{SS}}{V}\right)^2 + 4k_3 \frac{F_i^{SS}}{V}[A]_i^{SS}}}{2k_3} - \frac{2k_3}{V}\right)$$

Example II

For component [C], we have

$$\frac{\mathrm{d}[C](t)}{\mathrm{d}t} = -[C](t) \left(\frac{F_i^{SS}}{V}\right) + k_2 \underbrace{[B](t)}_{[B]^{SS}}$$
$$= 0$$

We get the equation,

$$\left(\frac{F_i^{SS}}{V}\right)[C](t) - k_2[B]^{SS} = 0$$

The steady-state value for [C],

$$[C]^{SS} = \frac{k_2[B]^{SS}}{\left(\frac{F_i^{SS}}{V}\right)}$$

given F_i^{SS} , $[A]_i^{SS}$, $[A]^{SS}$, and $[B]^{SS}$

Example II

Substituting $[B]^{SS}$, we get

$$[C]^{SS} = \frac{k2[B]^{SS}}{\left(\frac{F_i^{SS}}{V}\right)}$$

$$k_1 \left(\frac{-\left(k_1 + \frac{F_i^{SS}}{V}\right) + \sqrt{\frac{\left(k_1 + \frac{F_i^{SS}}{V}\right)^2 + 4k_3 \frac{F_i^{SS}}{V}[A]_i^{SS}}{2k_3}}{\left(\frac{F^{SS}}{V} + k_2\right)}\right)$$

$$= k_2 \frac{\left(\frac{F_i^{SS}}{V}\right)}{\left(\frac{F_i^{SS}}{V}\right)}$$

Example II

Example II (cont.)

Finally, for component [D] we have

$$\frac{\mathrm{d}[D](t)}{\mathrm{d}t} = -[D](t) \left(\frac{F_i^{SS}}{V}\right) + \frac{1}{2}k_3 \underbrace{[A]^2(t)}_{([A]^{SS})^2}$$
$$= 0$$

We get the equation,

$$\left(\frac{F_i^{SS}}{V}\right)[D](t) - \frac{1}{2}k_3([A]^{SS})^2 = 0$$

The steady-state value for [D],

$$[D]^{SS} = \frac{\frac{1}{2}k_3([A]^{SS})^2}{\left(\frac{F_i^{SS}}{V}\right)}$$

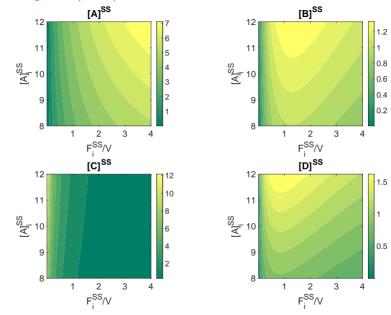
given F_i^{SS} , $[A]_i^{SS}$, $[A]^{SS}$, and $[B]^{SS}$

Substituting $[A]^{SS}$, we get

$$[D]^{SS} = \frac{1}{2}k_3 \frac{\left(-\left(k_1 + \frac{F_i^{SS}}{V}\right) + \sqrt{\frac{\left(k_1 + \frac{F_i^{SS}}{V}\right)^2 + 4k_3\frac{F_i^{SS}}{V}[A]_i^{SS}}{2k_3}}\right)^2}{\left(\frac{F_i^{SS}}{V}\right)}$$

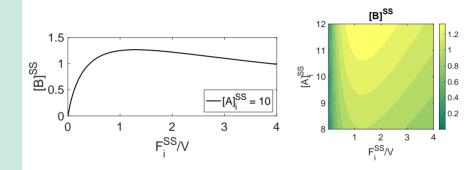
Example II

Example II (cont.)

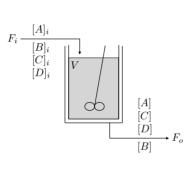


Example II (cont.)

Where would you operate the reactor if told that the feed composition is $[A]_i^{SS} = 10$?



Example II



We could define desirable operating conditions

$$\begin{split} u^{SS} &= \begin{bmatrix} \frac{F_i^{SS}}{V} = \frac{4}{7} \, \text{min}^{-1} \\ [A]_i^{SS} &= 10 \, \, \text{mol} \, \, \text{l}^{-1} \end{bmatrix} = \begin{bmatrix} F_i^{SS} \\ [A]_i^{SS} \end{bmatrix} \\ & \rightsquigarrow \begin{bmatrix} u_1^{SS} \\ u_2^{SS} \end{bmatrix} \end{split}$$

Then, determine the corresponding fixed point

Note that we replaced the first input variable (the feed flow-rate, $F_i(t)$)

- We will use the space-velocity $F_i(t)/V$, instead
- \bullet No difference, as the volume V is constant

Given a steady-state point $((x_1^{SS},x_2^{SS},x_3^{SS},x_4^{SS}),(u_1^{SS},u_2^{SS})),$ we linearise the model

We start by defining the deviation variables, for both state- and input variables

• For the state variables, we have

$$x'(t) = \begin{bmatrix} x_1(t) - x_1^{SS} \\ x_2(t) - x_2^{SS} \\ x_3(t) - x_3^{SS} \\ x_4(t) - x_4^{SS} \end{bmatrix} = \begin{bmatrix} [A](t) - [A]^{SS} \\ [B](t) - [B]^{SS} \\ [C](t) - [C]^{SS} \\ [D](t) - [D]^{SS} \end{bmatrix}$$

• For the input variables, we have

$$u'(t) = \begin{bmatrix} u_1(t) - u_1^{SS} \\ u_2(t) - u_2^{SS} \end{bmatrix} = \begin{bmatrix} F_i(t)/V - F_i^{SS}/V \\ [A]_i(t) - [A]_i^{SS} \end{bmatrix}$$

Then proceed by computing the Jacobians of dynamics at steady-state (x_{SS}, u_{SS})

 \rightarrow State matrix A and input matrix B

$$\Rightarrow \dot{x'}(t) = Ax'(t) + Bu'(t)$$

Example II (cont.)

 $\begin{bmatrix} \dot{x_1}(t) \\ \dot{x_2}(t) \\ \dot{x_3}(t) \\ \dot{x_4}(t) \end{bmatrix} = \begin{bmatrix} \underbrace{u_1(t) \left(u_2(t) - x_1(t)\right) - \theta_{x,1} x_1(t) - \theta_{x,3} x_1^2(t)}_{f_1} \\ \underbrace{-u_1(t) x_2(t) + \theta_{x,1} x_1(t) - \theta_{x,2} x_2(t)}_{f_2} \\ \underbrace{-u_1(t) x_3(t) + \theta_{x,2} x_2(t)}_{f_3} \\ \underbrace{-u_1(t) x_4(t) + \frac{1}{2} \theta_{x,3} x_1^2(t)}_{f_4} \end{bmatrix}$

$$\begin{bmatrix} \frac{\partial f_1}{\partial x_1} & \frac{\partial f_1}{\partial x_2} & \frac{\partial f_1}{\partial x_3} & \frac{\partial f_1}{\partial x_4} \\ \frac{\partial f_2}{\partial f_2} & \frac{\partial f_2}{\partial x_2} & \frac{\partial f_2}{\partial x_3} & \frac{\partial f_2}{\partial x_4} \\ \frac{\partial f_3}{\partial x_1} & \frac{\partial f_3}{\partial x_2} & \frac{\partial f_3}{\partial x_3} & \frac{\partial f_3}{\partial x_4} \\ \frac{\partial f_4}{\partial x_1} & \frac{\partial f_4}{\partial x_2} & \frac{\partial f_4}{\partial x_3} & \frac{\partial f_4}{\partial x_4} \end{bmatrix}_{SS} = \begin{bmatrix} -u_1 - \theta_{x,1} - 2\theta_{x,3}x_1 & 0 & 0 & 0 & 0 \\ \theta_{x,1} & -u_1 - \theta_{x,2} & 0 & 0 & 0 \\ \theta_{x,2} & -u_1 & 0 & 0 & -u_1 \end{bmatrix}_{SS}$$

Example II

Example II (cont.)

We get,

$$A = \begin{bmatrix} -u_1 - \theta_{x,1} - 2\theta_{x,3}x_1 & 0 & 0 & 0 \\ \theta_{x,1} & -u_1 - \theta_{x,2} & 0 & 0 \\ 0 & \theta_{x,2} & -u_1 & 0 \\ \theta_{x,3}x_1 & 0 & 0 & -u_1 \end{bmatrix}_{SS}$$

$$= \begin{bmatrix} -u_1^{SS} - \theta_{x,1} - 2\theta_{x,3}x_1^{SS} & 0 & 0 & 0 \\ \theta_{x,1} & -u_1^{SS} - \theta_{x,2} & 0 & 0 \\ 0 & \theta_{x,2} & -u_1^{SS} & 0 \\ \theta_{x,3}x_1^{SS} & 0 & 0 & -u_1^{SS} \end{bmatrix}$$

$$= \begin{bmatrix} -(4/7) - (5/6) - 2 \times (1/6) \times 3 & 0 & 0 & 0 \\ (5/6) & -(4/7) - (5/3) & 0 & 0 \\ 0 & (5/3) & (-4/7) & 0 \\ (1/6) \times 3 & 0 & 0 & -(4/7) \end{bmatrix}$$

We used
$$\theta_x = \begin{bmatrix} \theta_{x,1} & \theta_{x,2} & \theta_{x,3} \end{bmatrix}^T = \begin{bmatrix} k_1 & k_2 & k_3 \end{bmatrix}^T = \begin{bmatrix} (5/6) & (5/3) & (1/6) \end{bmatrix}^T$$
 and
$$x^{SS} = \begin{bmatrix} x_1^{SS} \\ x_2^{SS} \\ x_3^{SS} \\ x_4^{SS} \end{bmatrix} = \begin{bmatrix} [A]_{SS} \\ [B]_{SS} \\ [C]_{SS} \\ [D]_{SS} \end{bmatrix} = \begin{bmatrix} 3.0000 \\ 1.1170 \\ 3.2580 \\ 1.3125 \end{bmatrix}$$

$$egin{pmatrix} 0 \\ 0 \\ -u_1^{SS} \\ 0 \\ -0 \\ 7)-(5/3) \end{pmatrix}$$

$$\begin{pmatrix} & & 0 \\ & & 0 \\ & & 0 \\ /7) & 0 \\ & & -(4/7) \end{pmatrix}$$

$$x^{SS} = \begin{bmatrix} x_1^{SS} \\ x_2^{SS} \\ x_3^{SS} \\ x_4^{SS} \end{bmatrix} = \begin{bmatrix} [A]^{SS} \\ [B]^{SS} \\ [C]^{SS} \\ [D]^{SS} \end{bmatrix} = \begin{bmatrix} 3.0000 \\ 1.1170 \\ 3.2580 \\ 1.3125 \end{bmatrix}$$
$$u^{SS} = \begin{bmatrix} u_1^{SS} \\ u_2^{SS} \end{bmatrix} = \begin{bmatrix} F_{iS}^{SS} / V \\ AI^{SS} \end{bmatrix} = \begin{bmatrix} 4/7 \\ 10 \end{bmatrix}$$

Example II

$$\begin{bmatrix} \dot{x_1}(t) \\ \dot{x_2}(t) \\ \dot{x_3}(t) \\ \dot{x_4}(t) \end{bmatrix} = \begin{bmatrix} \underbrace{u_1(t) \left(u_2(t) - x_1(t) \right) - \theta_{x,1} x_1(t) - \theta_{x,3} x_1^2(t) \right)}_{f_1} \\ \underbrace{-u_1(t) x_2(t) + \theta_{x,1} x_1(t) - \theta_{x,2} x_2(t) }_{f_2} \\ \underbrace{-u_1(t) x_3(t) + \theta_{x,2} x_2(t) }_{f_3} \\ \underbrace{-u_1(t) x_4(t) + \frac{1}{2} \theta_{x,3} x_1^2(t) }_{f_4} \end{bmatrix}$$

$$\rightarrow B = \begin{bmatrix} \frac{\partial f_1}{\partial u_1} & \frac{\partial f_1}{\partial u_2} \\ \frac{\partial f_2}{\partial f_2} & \frac{\partial f_2}{\partial g_2} \\ \frac{\partial f_3}{\partial u_1} & \frac{\partial f_3}{\partial u_2} \\ \frac{\partial f_4}{\partial u_1} & \frac{\partial f_4}{\partial u_2} \end{bmatrix}_{SS} = \begin{bmatrix} u_2 - x_1 & u_1 \\ -x_2 & 0 \\ -x_3 & 0 \\ -x_4 & 0 \end{bmatrix}_{SS}$$

Example II (cont.)

We get,

Example II

$$B = \begin{bmatrix} u_2 - x_1 & u_1 \\ -x_2 & 0 \\ -x_3 & 0 \\ -x_4 & 0 \end{bmatrix}_{SS}$$

$$= \begin{bmatrix} u_2^{SS} - x_1^{SS} & u_1^{SS} \\ -x_2^{SS} & 0 \\ -x_3^{SS} & 0 \\ -x_4^{SS} & 0 \end{bmatrix}$$

$$= \begin{bmatrix} 10 - 3 & (4/7) \\ -1.1170 & 0 \\ -3.2580 & 0 \\ -1.3125 & 0 \end{bmatrix}$$

We used,

$$x^{SS} = \begin{bmatrix} x_1^{SS} \\ x_2^{SS} \\ x_3^{SS} \\ x_4^{SS} \end{bmatrix} = \begin{bmatrix} [A]^{SS} \\ [B]^{SS} \\ [C]^{SS} \\ [D]^{SS} \end{bmatrix} = \begin{bmatrix} 3.0000 \\ 1.1170 \\ 3.2580 \\ 1.3125 \end{bmatrix}$$
$$u^{SS} = \begin{bmatrix} u_1^{SS} \\ u_2^{SS} \end{bmatrix} = \begin{bmatrix} F_i^{SS}/V \\ [A]_i^{SS} \end{bmatrix} = \begin{bmatrix} 4/7 \\ 10 \end{bmatrix}$$