

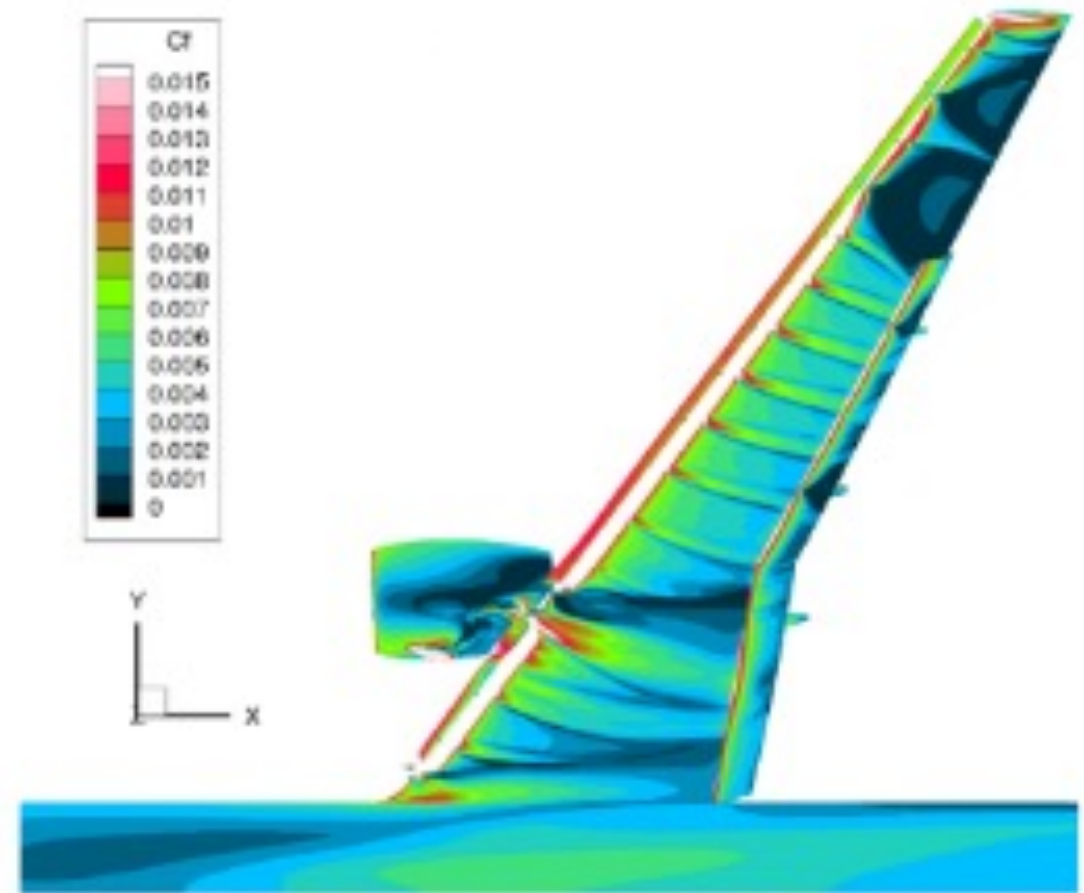


# The Basics of Turbulence Modeling

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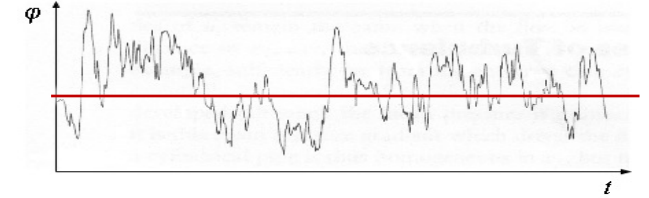
- The Reynolds-Averaged Navier-Stokes (RANS) equations
- The power and the paradox of Reynolds-Averaging and Turbulence Modeling
- The nature of a turbulence model

## State of the Art on a Complex Geometry



# The Reynolds-Averaged Navier-Stokes Equations

- The true velocity field is  $u(x, y, z, t)$
- For simplicity, assume we average it in time, giving  $U(x, y, z)$ , also called  $\bar{u}$
- Define the fluctuation  $u'(x, y, z, t) \equiv u(x, y, z, t) - U(x, y, z)$ 
  - So, “ $u = U + u'$ ” and  $\bar{u}' = 0$
- Take the incompressible Navier-Stokes equations
- The continuity condition is  $\partial u_i / \partial x_i = 0$ , and its average is  $\partial U_i / \partial x_i = 0$ : no change
- The momentum equation is (setting  $\rho = 1$ ):



$$\frac{Du_i}{Dt} = \frac{\partial u_i}{\partial t} + u_j \frac{\partial u_i}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \nu \frac{\partial^2 u_i}{\partial x_j \partial x_j}$$

- Average this equation in time:

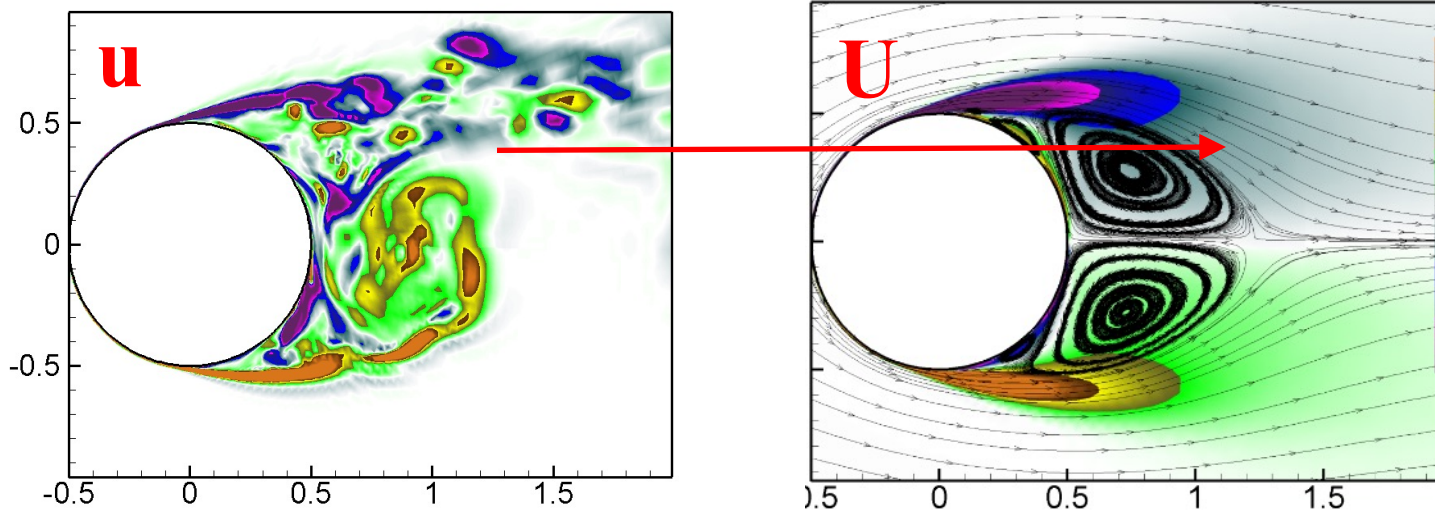
$$\frac{\overline{D}U_i}{Dt} = U_j \frac{\partial U_i}{\partial x_j} = -\frac{\partial \bar{p}}{\partial x_i} + \nu \frac{\partial^2 U_i}{\partial x_j \partial x_j} - \frac{\partial (\overline{u'_i u'_j})}{\partial x_j}$$

- The quantity  $\overline{u'_i u'_j}$  created by the nonlinearity is the “Reynolds Stress”

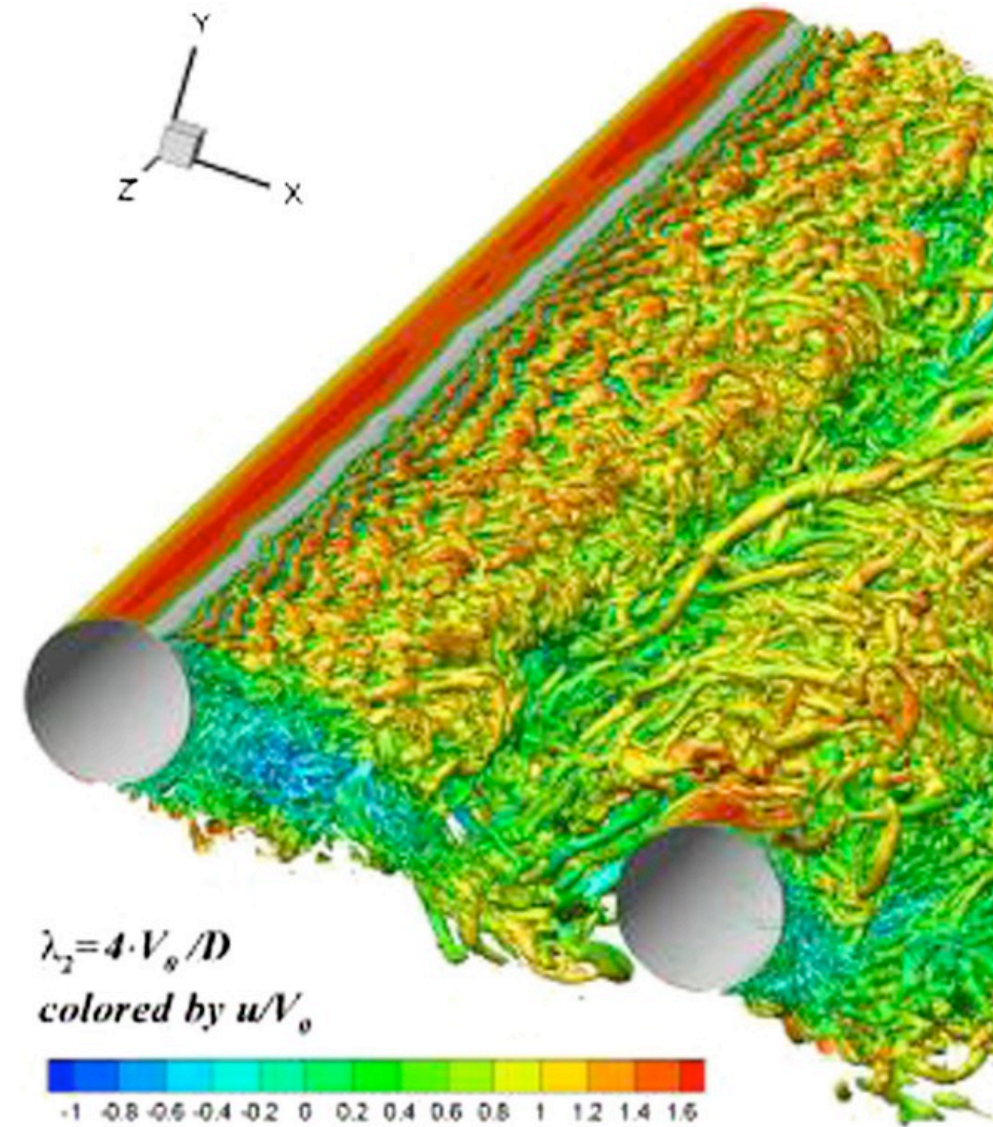


# The Power and Paradox of Turbulence Modeling

- Averaging is a valid procedure. However...



- Some very different  $u(x,y,z,t)$  conditions enter the single time-average at a given point,  $U(x,y)$
- You could describe the Reynolds-averaged flow as the flow of a fluid with “very strange” internal stresses
  - These stresses are not a property of the fluid, unlike the viscous stresses; they depend on the entire history of the flow
  - The job of a turbulence model is to give the stresses, knowing only  $U$ ! *Hoping for a rigorous approximation is not reasonable*



**Strelets work**



# The Nature of a Turbulence Model

- The clear need of CFD is to have a simple and local mathematical model of the “very strange” Reynolds stresses!
- Most common is the artificial concept of eddy viscosity  $\nu_t$ , due to Boussinesq in 1877
  - $-\overline{u'_i u'_j} = \nu_t (\partial U_i / \partial x_j + \partial U_j / \partial x_i)$
  - Very often,  $\nu_t$  is larger than  $\nu$  by orders of magnitude. It is different in every flow

- An example: the Spalart-Allmaras model of 1992 (basic form in boundary layer)

$$\frac{D\nu_t}{Dt} = c_{b1} \left| \frac{\partial U}{\partial y} \right| \nu_t - c_{w1} \left( \frac{\nu_t}{y} \right)^2 + \frac{1}{\sigma} \left[ \frac{\partial}{\partial y} \left( \nu_t \frac{\partial \nu_t}{\partial y} \right) + c_{b2} \left( \frac{\partial \nu_t}{\partial y} \right)^2 \right]$$

- Where  $y$  is the distance from the wall
- Every term is arbitrary!
- They express “Evolution = Production - Wall Confinement + Diffusion”
- The  $c$  and  $\sigma$  constants were adjusted to work in a few simple cases
- The model was inspired by Baldwin and Barth at NASA
- It shares much with the  $\nu_t$ -92 model of Secundov at TsAGI in Moscow
- Other common models have two equations, seven equations...
  - The more elaborate models have equations for six Reynolds stresses + dissipation. No  $\nu_t$ !