

NS Cahn-Hilliard description

$$\rho \frac{D\mathbf{u}}{Dt} = -\nabla p + \mu \nabla^2 \mathbf{u} + \phi \nabla C$$

$$\nabla \cdot \mathbf{u} = 0$$

$$\frac{DC}{Dt} = \kappa \nabla^2 \phi$$

$$\phi = \frac{\sigma}{\varepsilon} f'(C) - \sigma \varepsilon \nabla^2 C$$

Standard choice

$$f(C) = (1 - C)^2 (1 + C)^2 / 4$$

$$g(C) = (2 + 3C - C^3) / 4$$

Wetting boundary condition

$$\varepsilon \mu_f \frac{\partial C}{\partial t} = -\sigma \varepsilon \nabla C \cdot \mathbf{n} + (\gamma_1 - \gamma_0) g'(C)$$

$$\mathbf{u}_s = 0$$

Solve for: \mathbf{u}, p, C

Parameters:

$$\mu_f, \rho, \mu, \gamma (= \sigma \frac{2\sqrt{2}}{3} = \text{surface tension})$$

$$(\gamma_1 - \gamma_0) / \gamma = \cos \theta_e$$

ε, κ : interface width, mobility – treat as numerical parameters

NS Cahn-Hilliard description

$$\frac{D\mathbf{u}}{Dt} = -\nabla p + \frac{1}{Re} \nabla^2 \mathbf{u} + \frac{1}{We} \phi \nabla C$$

$$\nabla \cdot \mathbf{u} = 0$$

$$\frac{DC}{Dt} = \frac{1}{Pe} \nabla^2 \phi$$

$$\phi = f'(C) - Cn^2 \nabla^2 C$$

Standard choice

$$f(C) = (1 - C)^2 (1 + C)^2 / 4$$

$$g(C) = (2 + 3C - C^3) / 4$$

Wetting boundary condition

$$Ca_f Cn \frac{\partial C}{\partial t} = -\frac{3}{2\sqrt{2}} Cn \nabla C \cdot \mathbf{n} + \cos\theta_e g'(C)$$

$$\mathbf{u}_s = 0$$

Solve for: \mathbf{u}, p, C

Parameters:

Re, We, Pe, Ca_f, Cn

$$\frac{DC}{Dt} = \kappa \nabla^2 \phi$$

$$\phi = \frac{\sigma}{\varepsilon} f'(C) - \sigma \varepsilon \nabla^2 C$$

Standard choice

$$f(C) = (1 - C)^2 (1 + C)^2 / 4$$

$$g(C) = (2 + 3C - C^3) / 4$$

A two component mixture

Chemical potential phi may seem a bit mystical

But

Away from the interface, where $C \approx \pm 1$:

$$C = 1 + c, \quad c \ll 1$$

Eqns become:

$$\frac{Dc}{Dt} = 2\alpha \nabla^2 c$$

Regular Fickian mass diffusion

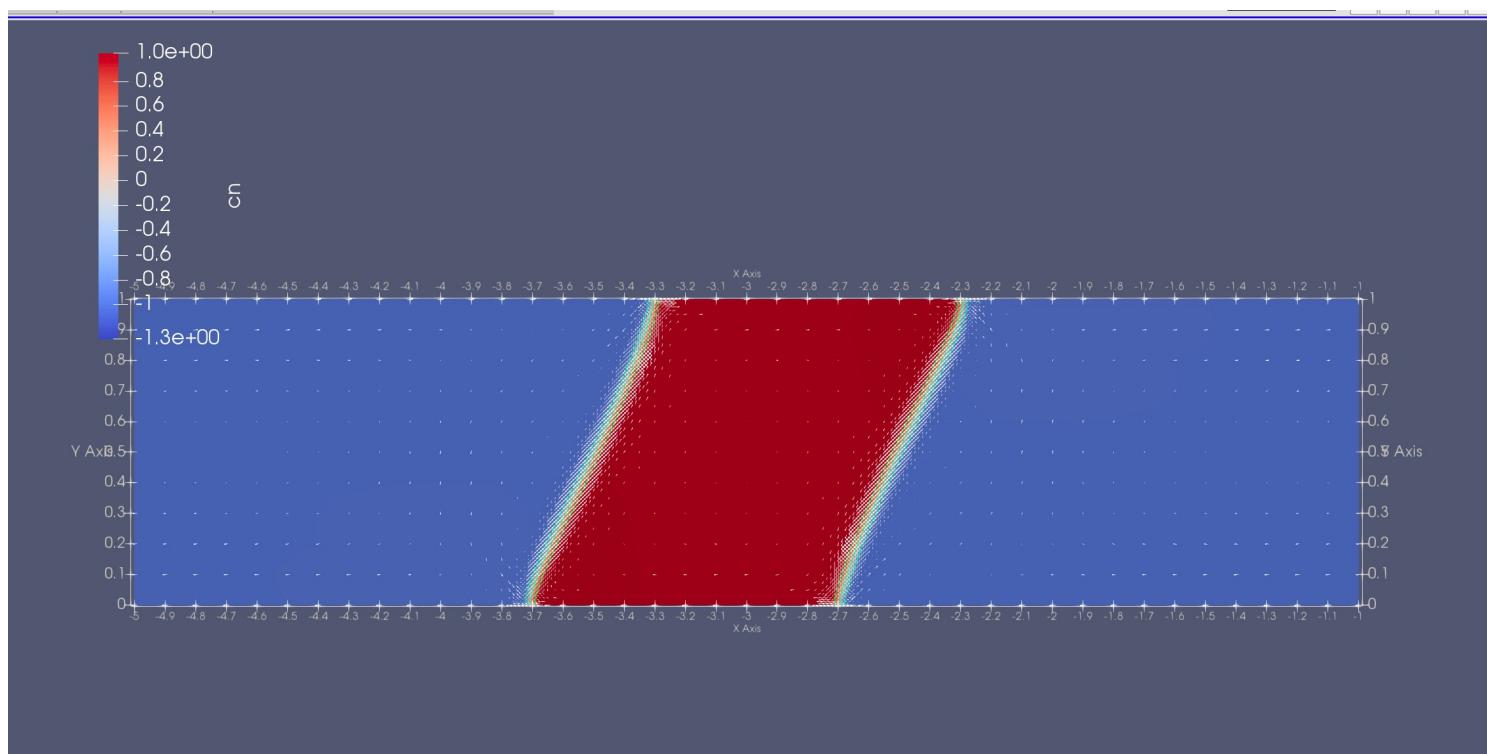
$$\alpha = \frac{3}{2\sqrt{2}} \frac{\kappa \gamma}{\varepsilon}$$


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##### GENERAL INFORMATION #####
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empty      < plotfiles/tmpSave1    < infile
1E-11     < GMRES-tolerance
1E-11     < CG-tolerance
5000      < max of loop in cg
0.004     < dt
30        < endtime
0.1       < time to print out information
0.1       < time to save results to disk
0.02      < time to check stop flag (define in femlego.stop)
0         < time limit (minute: 0=nolimit)
##### ADAPTIVE INFORMATION #####
0.0001      < errLow
0.0004      < errHi
0.002       < adaptHmin
0.001       < adaptive time
##### USER's PARAMETERS #####
3.978      < Reno
0.01        < Cahn
1.06       < Ca
100.0      < Pe
0.0         < Bo
0.0       < cos_theta
0.010      < eps_p
0.0        < eps_phi
0.0       < eps_c
1.040      < rad
0.01       < xi
100.0      < errfcn
0.99       < a
0.01       < rhom
0.01       < vism
0.0        < ksmt
1.0        < coupl
10.        < errcrf1
1000.0     < errcrf2
0.3        < dr
0.05      < ui   use as wall speed
0.0        < A
1000.0     < fric, controls slip
0.0        < lnk
0.0        < muf

```

/Users/gustava2/prog/paradapt-2.4/Couette_wetting/P100_cn01
Wall speed = +- 0.05
Ca= $1.06 \times 0.02 = 0.053$

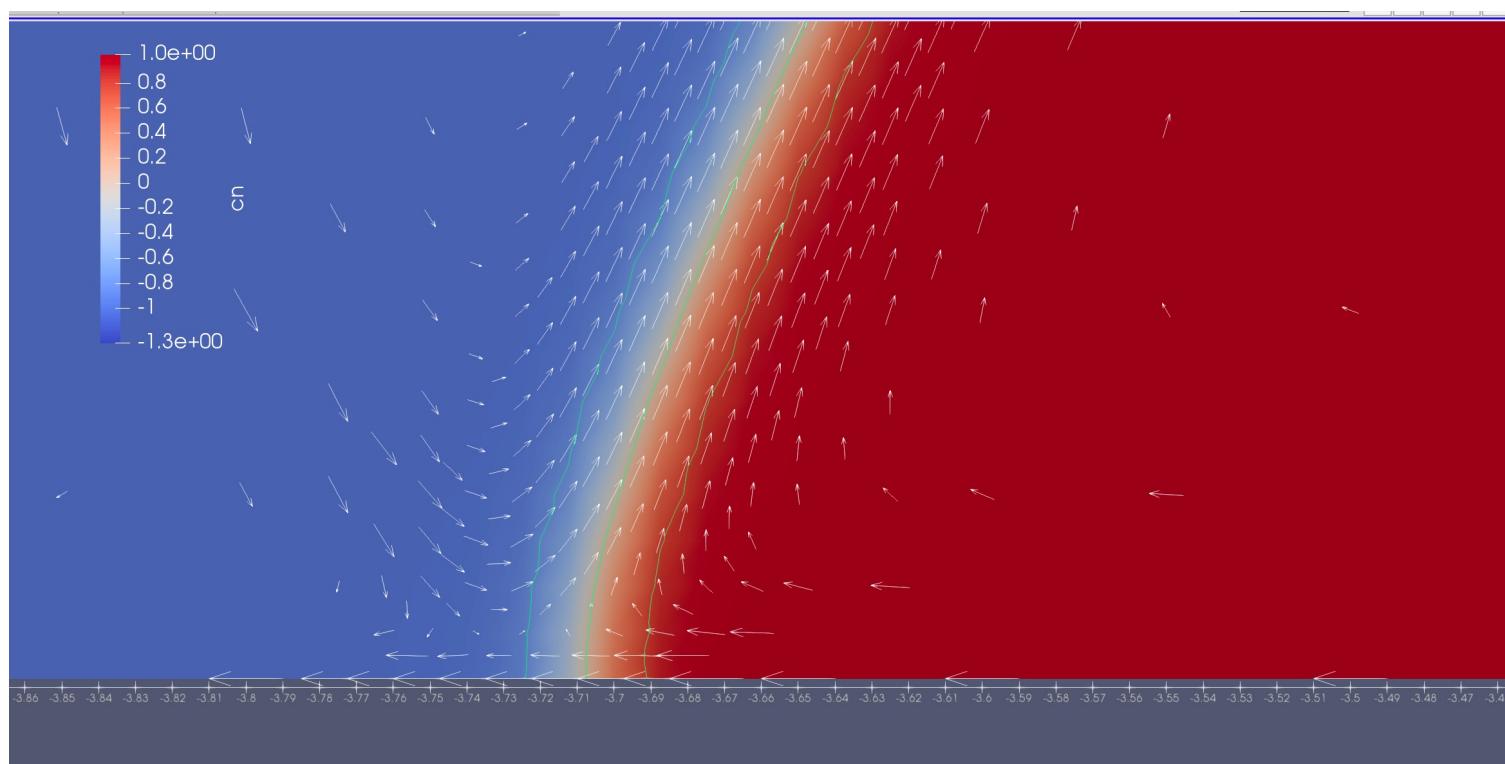


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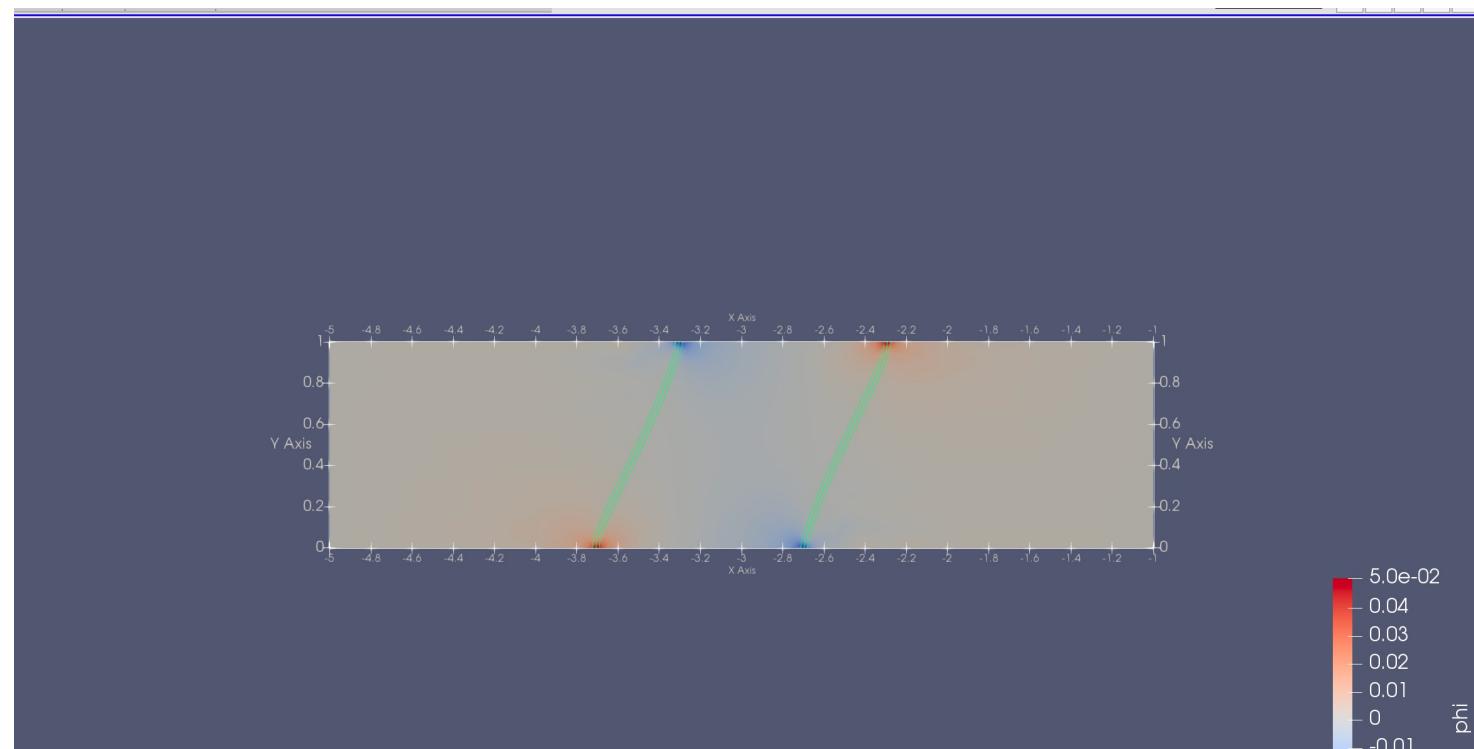


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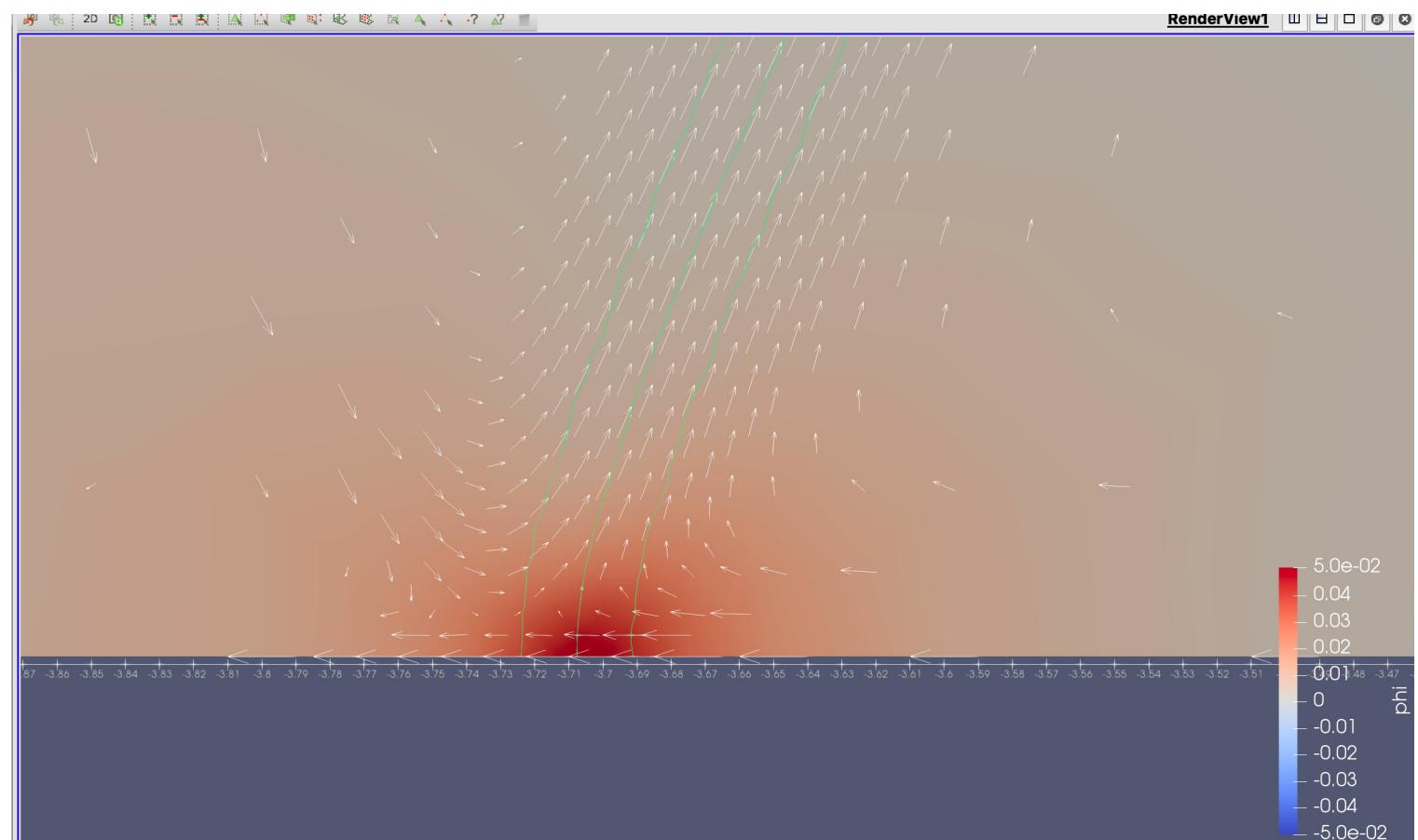


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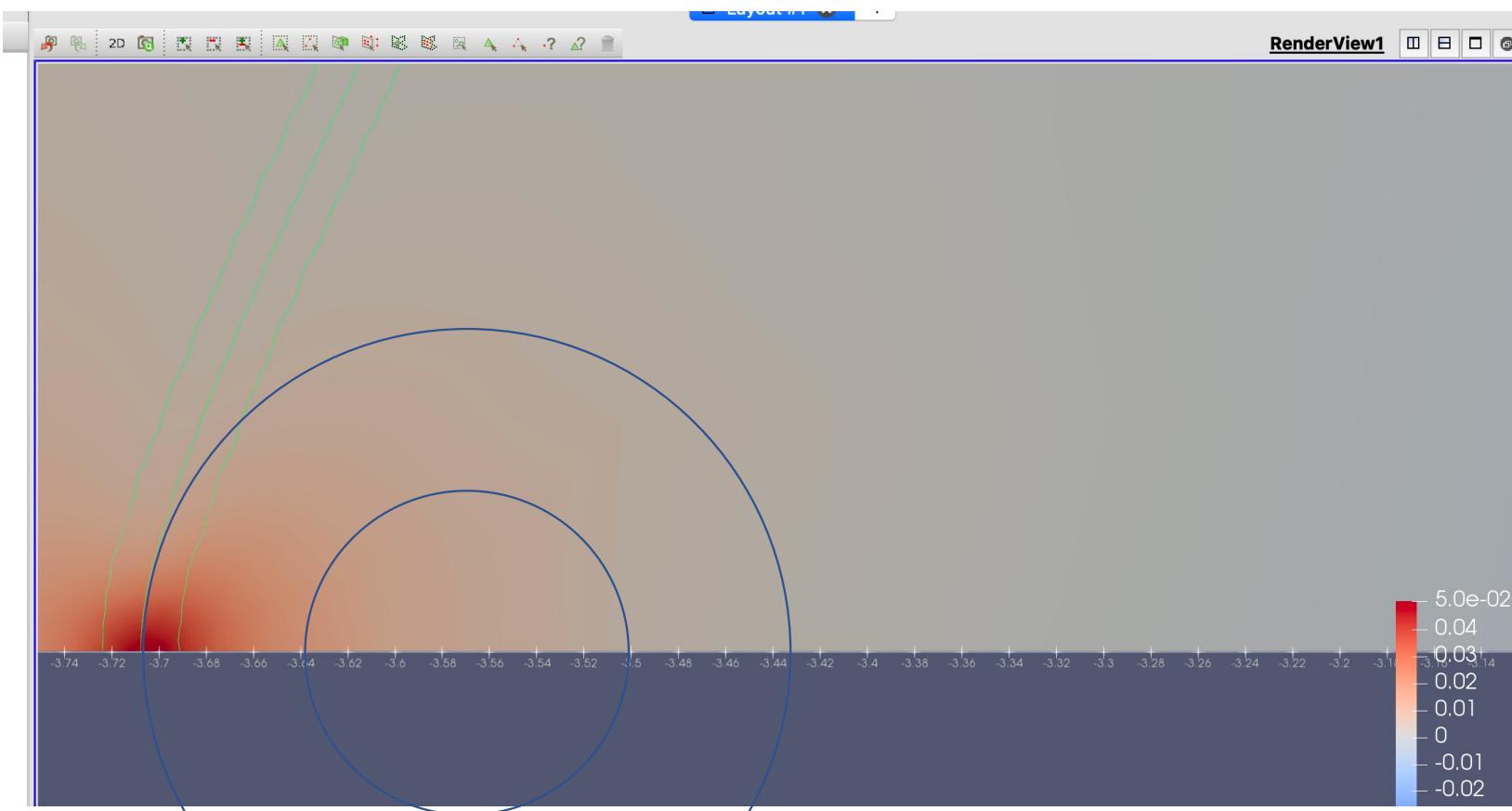


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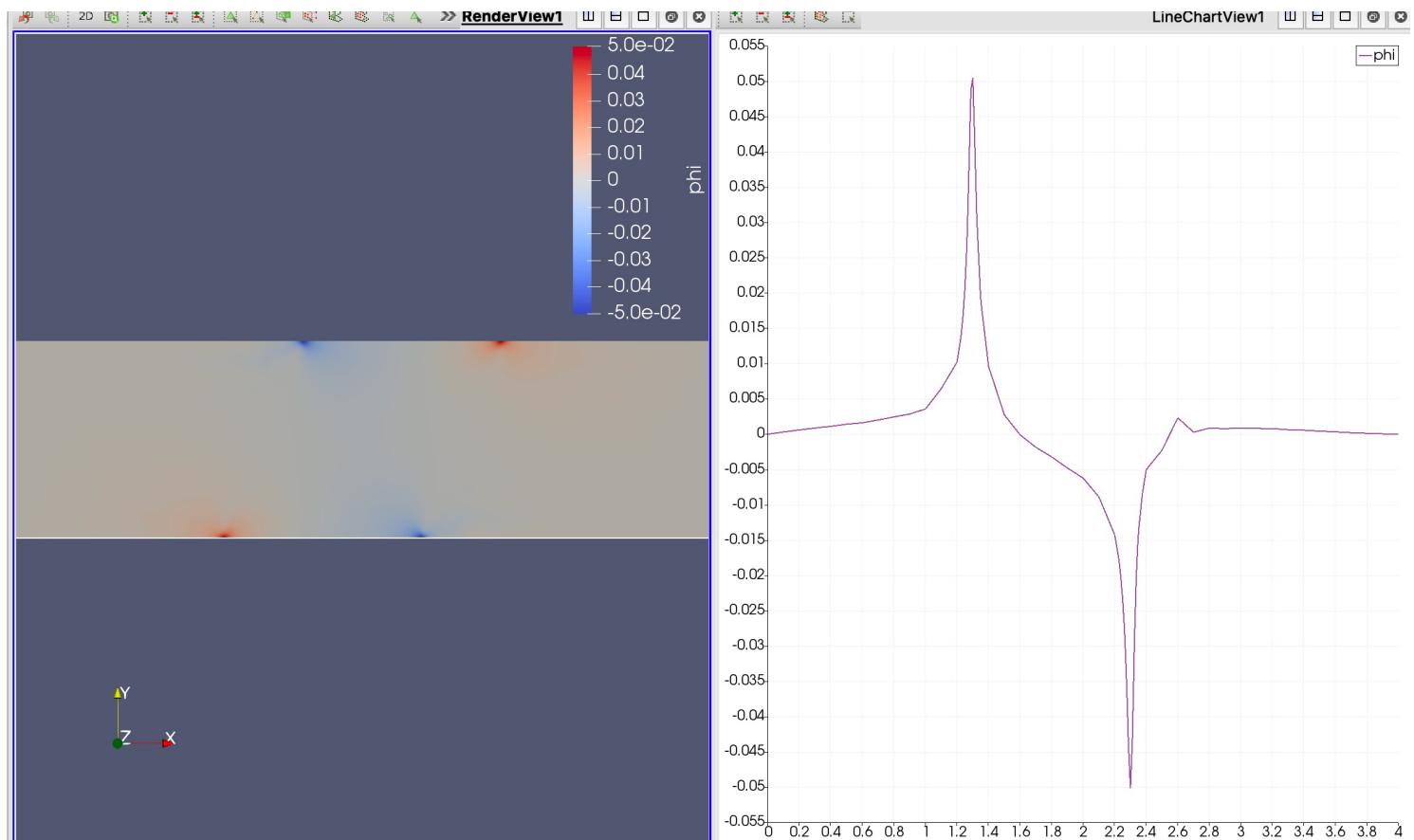
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 Wall speed = +- 0.05
 $Ca = 1.06 * 0.02 = 0.053$



Cn	Pe	
0.04	30	Made a number of simulations for Ca=0.053
0.02	30	
0.01	30	
0.005	30	Evaluated max chem pot value phi, and local curvature at the contact line
0.04	100	
0.02	100	
0.01	100	
0.005	100	
0.04	300	
0.02	300	
0.01	300	
0.005	300	
0.005	50	
0.01	100	
0.02	200	
0.04	400	
0.1	160	
0.04	160	
0.02	160	
0.01	160	
0.005	160	

Mass diffusion moves the contact line right at the wall.

Try to relate the chemical potential to interface curvature and massflux of one species

Curved interface at equilibrium:

Result for radius of curvature R

$$\phi = \frac{1}{2} \frac{2\sqrt{2}}{3} \frac{Cn}{R}$$

$\Phi = -\nabla C + (c^2 - 1)C$

$\nabla^2 C = \frac{\partial^2 C}{\partial r^2} + \frac{1}{r} \frac{\partial C}{\partial r} \approx \frac{\partial^2 C}{\partial \xi^2} + \frac{1}{R} \frac{\partial C}{\partial \xi}$

perturbation expansion in $c = c_0 + c_1$, $c_1 \ll c_0$.

$c_0: 0 = \frac{\partial^2 c_0}{\partial \xi^2} + (c_0^2 - 1)c_0$

$\Rightarrow c_0 = \tanh(\xi/\sqrt{2})$

$c_1: \Phi_1 = -\frac{\partial^2 c_1}{\partial \xi^2} - \frac{1}{R} \frac{\partial c_0}{\partial \xi} + c_1 \cdot f''(c_0)$

($\Phi = 0 + \Phi_1 \dots$, assume $\Phi_1 = \text{const.}$)

$\int \Phi_1 c_0 d\xi = (\dots) - \frac{1}{R} \int c_0^2 d\xi$

$\Rightarrow \boxed{\Phi_1 = \frac{1}{2} \cdot \frac{2R^2}{3} \cdot \frac{1}{R}}$

Mass diffusion moves the contact line right at the wall.

Try to relate the chemical potential to interface curvature and massflux of one species

Massflux?
A more daring attempt!

Mimick the scaling of YZF.

$$u \cdot c_x = M D^2 \phi$$

$$\sigma - \mu \frac{u}{\delta^2} + \phi \cdot c_x$$

$$\textcircled{1} \quad \frac{u}{\delta} \sim M \frac{1}{\delta^2} \cdot \phi, \quad u = \frac{M \phi}{\delta}$$

$$\textcircled{2} \quad \frac{\mu u}{\delta^2} \sim \phi \cdot \frac{1}{\delta}, \quad \frac{\mu u}{\delta} = \phi$$

$$\therefore \mu = \frac{M}{\delta} \cdot \frac{\phi}{\delta} \Rightarrow \delta^2 \sim M \mu. \quad (\text{YZF})$$

u undetermined.

$$\textcircled{3} \quad 8 \cdot Pe \cdot \int R \cdot R_{SS} \cdot u d\zeta = - \frac{1}{R} \int \frac{\partial u}{\partial \zeta} d\zeta$$

$$\textcircled{4} \quad b = -\delta \cdot (P_f - P_i) + \frac{1}{Re} \cdot L \cdot (C_x - C_i) - \frac{1}{We} \cdot g \cdot S_{Ca} \cdot \frac{\partial u}{\partial \zeta} d\zeta$$

~~\int_a^b~~ \int_a^b

$$Re \cdot R \approx \frac{u}{\delta} \cdot a, \quad \int R \cdot R_{SS} \cdot u d\zeta$$

$$\textcircled{5} \quad 8 \cdot Pe \cdot u \cdot 0.8679 = \frac{1}{R} \cdot \frac{2\sqrt{2}}{3} \quad (u=1!)$$

$$\textcircled{6} \quad Re \cdot a \cdot \frac{u}{\delta} \sim \frac{1}{R} \frac{2\sqrt{2}}{3} \cdot \frac{1}{We}$$

$$8 \cdot Pe \cdot u \cdot 0.8679 = We \cdot \frac{1}{Re} \cdot a \cdot \frac{u}{\delta} = \frac{1}{R} \frac{2\sqrt{2}}{3}$$

$$\boxed{\delta = \frac{1}{0.8679} \cdot \sqrt{\frac{We \cdot a}{Pe \cdot Re}}}$$

Actually the non dim form of YZF

Mass diffusion moves the contact line right at the wall.

Try to relate the chemical potential to interface curvature and massflux of one species

Massflux?

A more daring attempt!

$$-U \cdot c_{\xi} \cdot Pe = \frac{\partial^2}{\partial \xi^2} \left(-\frac{\partial \psi}{\partial z} + f(\xi) - \frac{1}{R} \frac{\partial \psi}{\partial z} \right)$$

$$c = c_0 + c_1, \quad c_1 \ll 1$$

$$Pe = \frac{U \varepsilon}{\alpha} = \left(\varepsilon = \text{L width} \right) \ll 1$$

$$c_0 = \ln \frac{h(\xi)}{h_0}$$

c_1 ? Rhind a similar Redholm alternative?

introduce $R = \int \delta \phi_0 d\xi$:

$$\frac{\partial R}{\partial \xi} \approx \phi_0$$

$$\Rightarrow \delta \int R (+U \cdot Pe \cdot \delta \phi_0) d\xi = \int \phi_0 \left(\frac{1}{R} \frac{\partial \phi_0}{\partial \xi} \right) d\xi - \int \frac{1}{R} \cdot R \cdot Pe \delta \phi_0 d\xi$$

$$\Rightarrow \boxed{\delta U_{el} \cdot Pe \cdot \frac{2\pi}{3} (1 - \ln 2) = \frac{2\pi}{3} \cdot \frac{1}{R}}$$

or $\boxed{-U_{el} \delta Pe \cdot 0,8679 = \frac{1}{R} \cdot 0,9428}$

or $-U_{el} \delta Pe \cdot 0,8679 = \frac{1}{R_w} \cdot 0,9428$

$$Pe_w = \frac{Uw}{\alpha}, \quad R_w = \frac{R}{w}$$

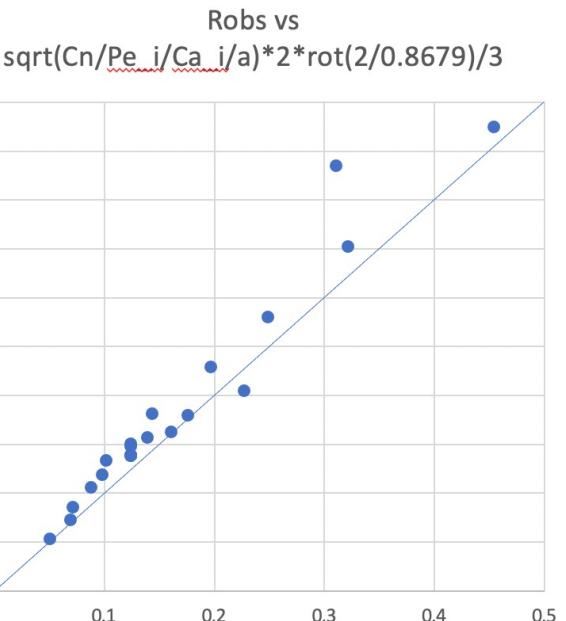
Mass diffusion moves the contact line right at the wall.

Try to relate the chemical potential to interface curvature and massflux of one species

End result:

Local curvature at CL as a function of parameters

$$R = \frac{2\sqrt{2}}{3} \frac{1}{\sqrt{0.8679}} \sqrt{\frac{Cn}{Pe Ca a}}$$



Geometry factor for the viscous flow
 $a = 2.5$
 Could/should depend on the static contact angle

Mass diffusion moves the contact line right at the wall.

Try to relate the chemical potential to interface curvature and massflux of one species

$$Cn = \frac{\varepsilon}{W}$$

End result:

Local curvature at CL as a function of parameters

$$Pe = \frac{UW}{\alpha}$$

$$Ca = \frac{\mu U}{\gamma}$$

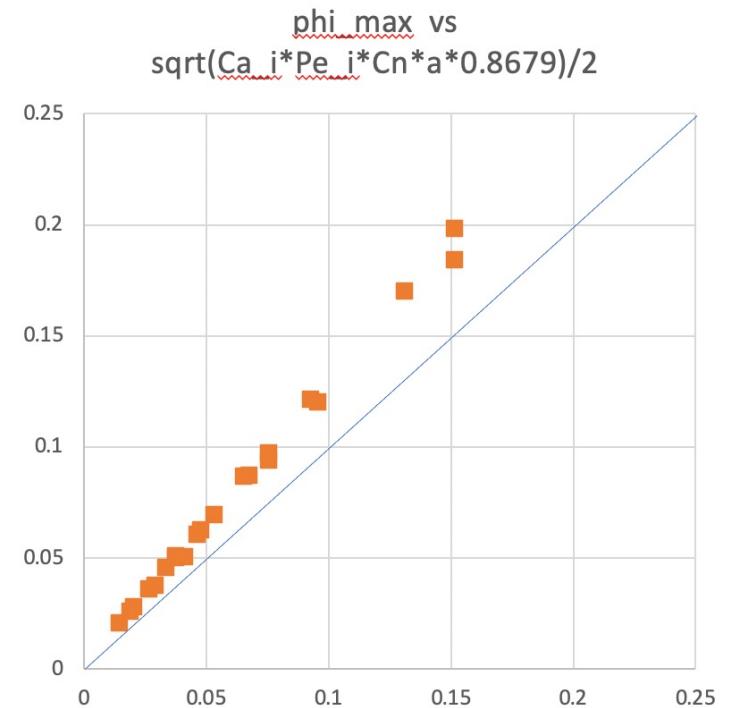
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Chemical potential:

$$\phi = \frac{\sqrt{0.8679}}{2} \sqrt{Pe_W Ca Cn a}$$



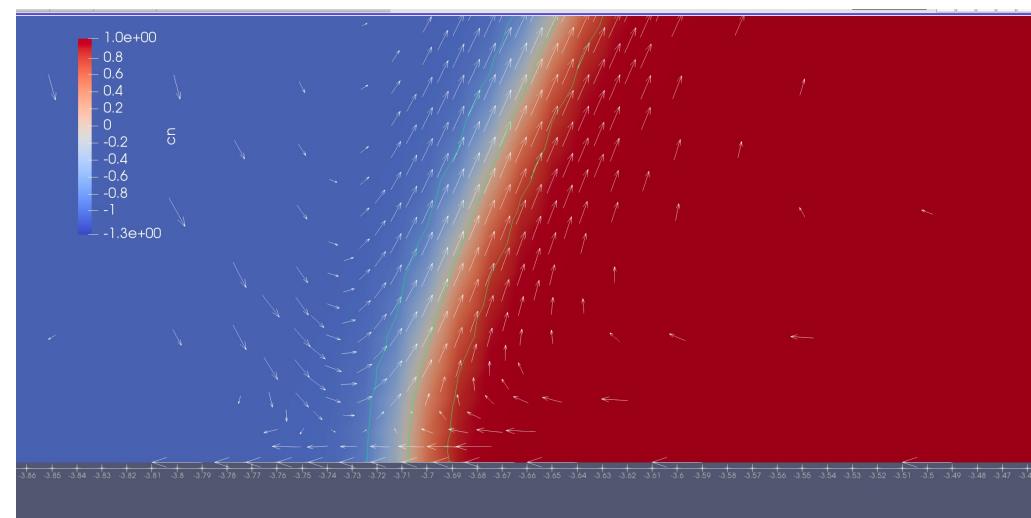
Toy model that mimicks PF (at lower cost?)

Sharp-interface limit of the Cahn-Hilliard
model for moving contact lines

Yue, Zhou, Feng JFM 2010

Scaling gives

Stagnation point at $\sqrt{\kappa\mu}$
PF mobility and viscosity.
Independent of interface width.
 $\sqrt{\kappa\mu}$ works as a slip length



Toy model that mimicks PF (at lower cost?)

Use as slip length

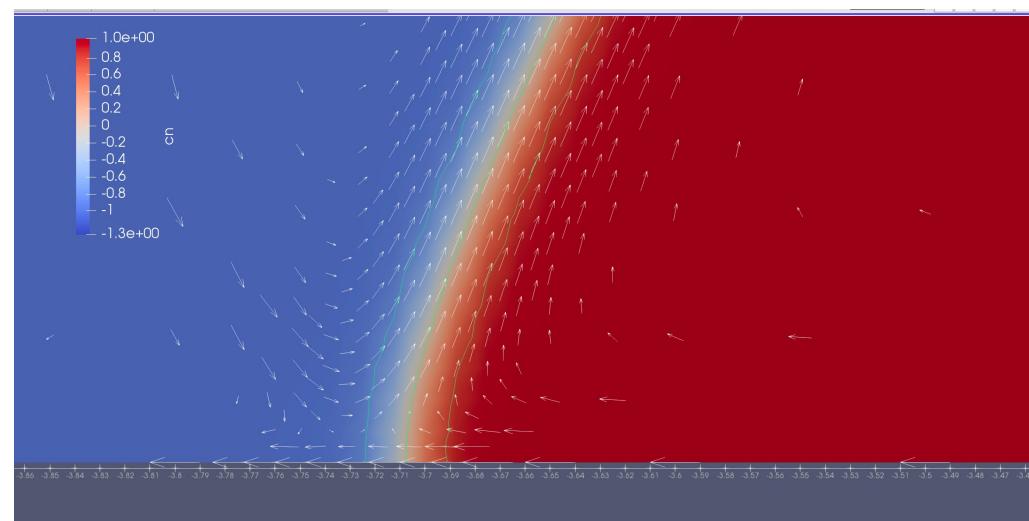
$$\delta = \frac{1}{\sqrt{0.8679}} \sqrt{\frac{Ca Cn a}{Pe}}$$

And an apparent contact angle

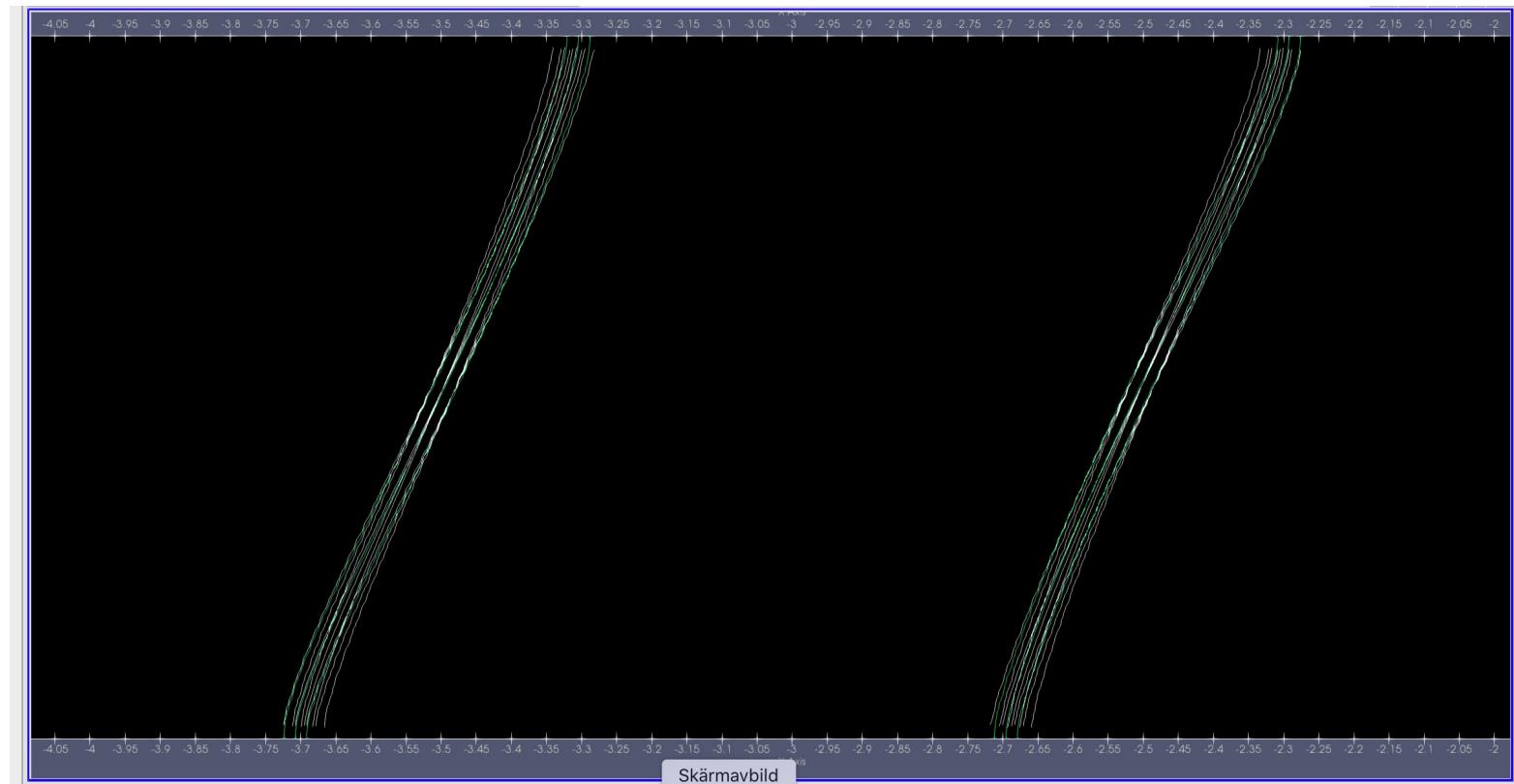
$$\cos\theta_a = \cos\theta_s + \frac{3}{2\sqrt{2}} Ca a$$

(Obtained from local curvature

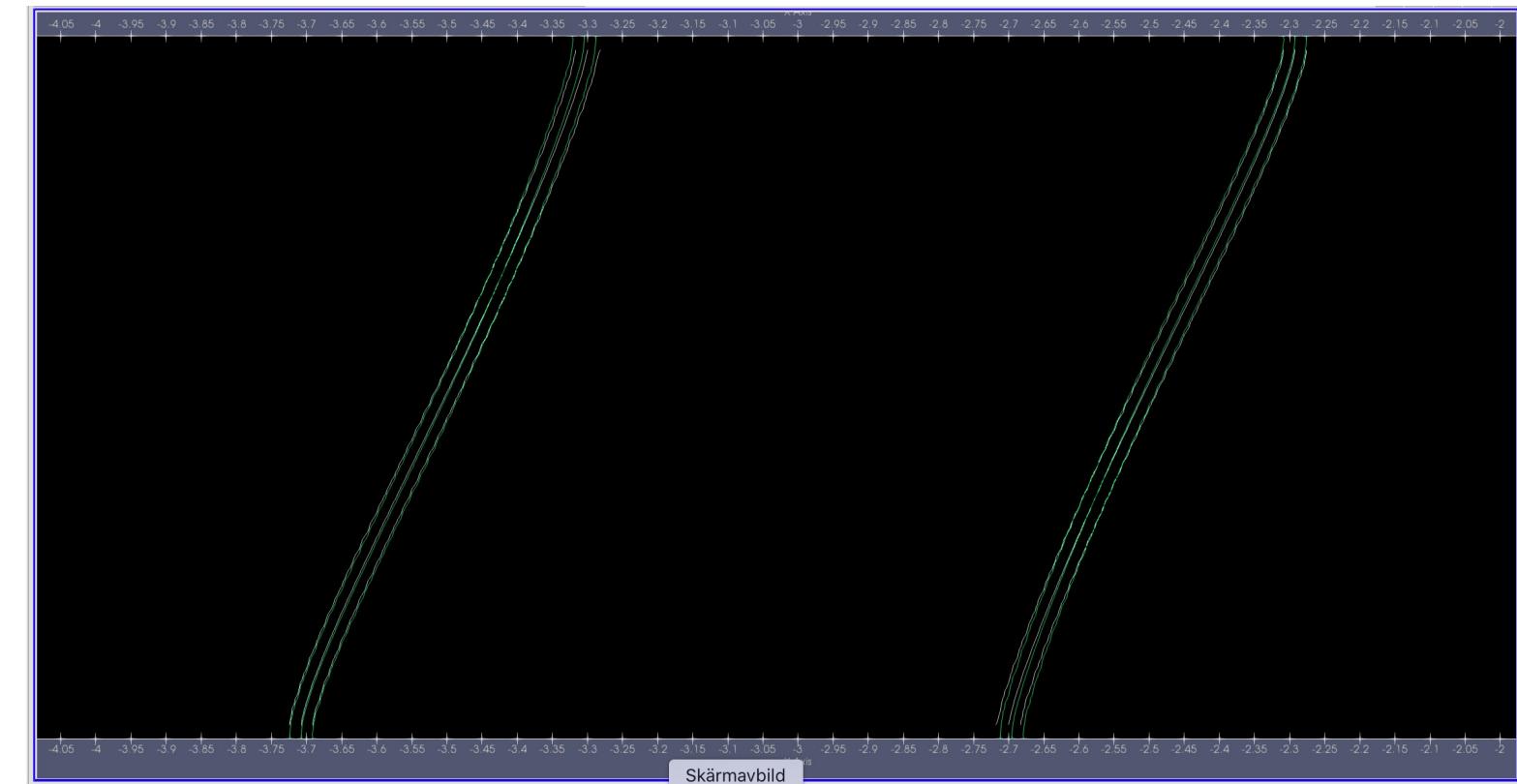
$$R = \frac{2\sqrt{2}}{3} \frac{1}{\sqrt{0.8679}} \sqrt{\frac{Cn}{Pe Ca a}}$$



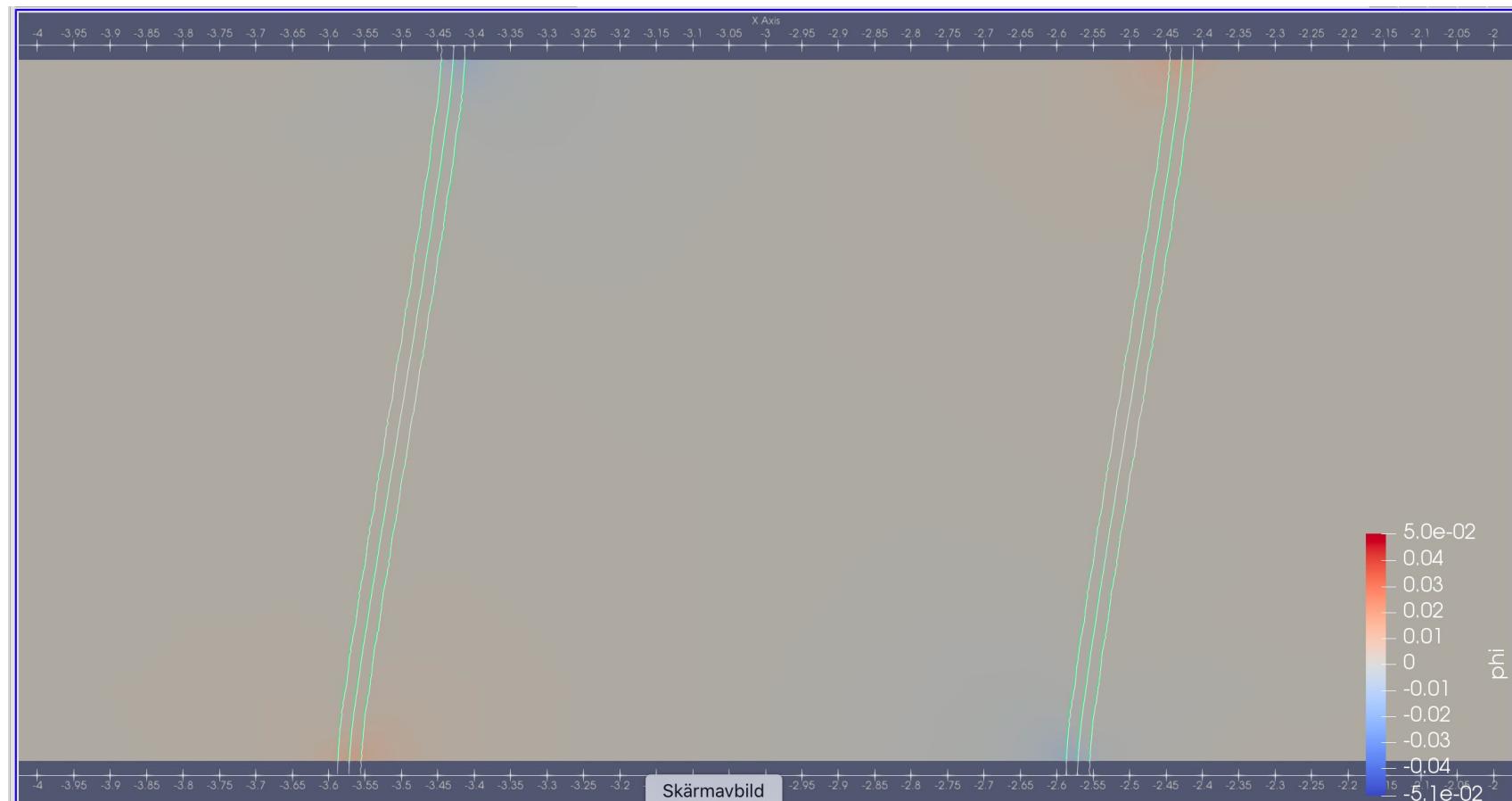
P100_cn01 full PF
toyP100_01_a2 a=2.0
toyP100_01 a=2.5
toyP100_01_a3 a=3.0



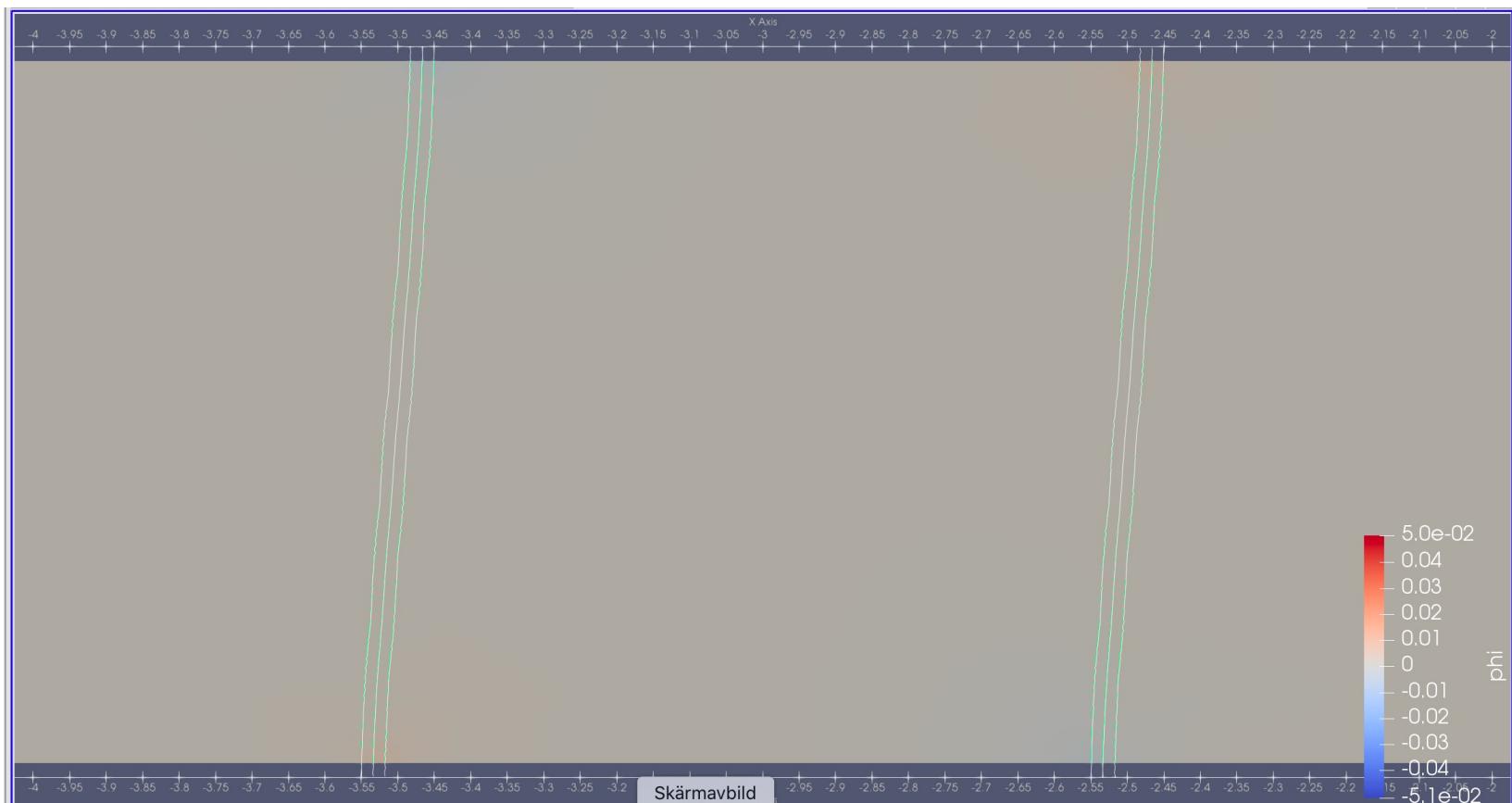
P100_cn01 full PF
toyP100_01_a2 a=2.0
toyP100_01 a=2.5
toyP100_01_a3 a=3.0 best fit



P1c1_Ca02
t1c1_Ca02

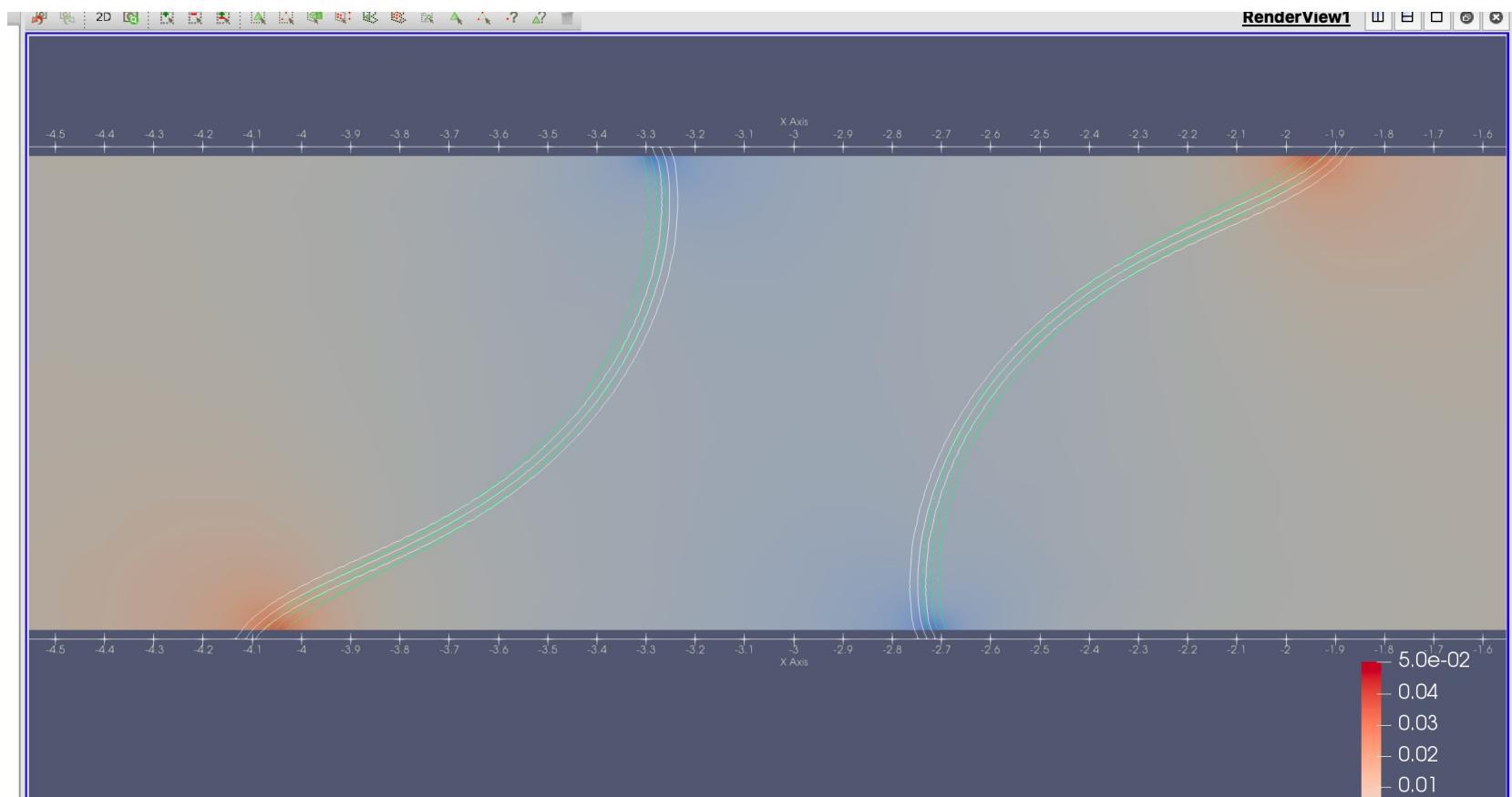


P1c1_Ca01
t1c1_Ca01



P1c1_Ca05_th60
t1c1_Ca05_th60 a=3

Ca =0.053
theta_s = 60 deg



P1c1_Ca02_th60

t1c1_Ca02_th60

a=3

Ca =0.0212

theta_s = 60 deg

