# Prediction of ignition delay using data-driven framework for straight chain alkanes

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### **Abstract**

Ignition delay is important global combustion property. Ignition delay time(IDT) is generally measured using Shock-tube and RCM experiments. Calculation of IDT from simulation is computationally expensive and time consuming process. To obtain IDT faster and accurately, shock tube experimental data has been used to predict IDT using error based clustering regression. For that, IDT correlation is Arrhenius type in its nature which includes activation energy and reformulated using bond energy to avoid uncertainty and dependency of experimental parameters. To predict IDT, models are created using error based clustering algorithm. For that dataset is divided into recursively into sub-dataset using relative error between predicted and actual ignition delay using multiple regression and hypothesis testing. Result obtained using framework and correlation shows excellent agreement with experimental result.

# Keywords:

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Ignition delay prediction, Machine learning, Data-Driven ,Fuel, Error based clustering, IDT correlation, Framework

#### 1. Introduction:

Combustion process is mainly characterized by transport processes and chemical reactions.

When fluid undergoes chemical reaction, it liberates heat without external source of energy such sustainable process is called as Ignition. Ignition comprises series of coincidental physical and

chemical processes which have different characteristic time scale, which is called as ignition delay.

Ignition delay gives important information about fuel reactivity. It is one of the major global physio-chemical combustion property. Ignition delay is mainly comprised of two parts: physical ignition delay and chemical ignition delay. Physical ignition delay depends on certain physical phenomena such as heating, fuel atomization, penetration of spray, and evaporation rate of fuel for different temperature range. Whereas, chemical ignition delay is mainly function of chemical characteristics of fuel, molecular structure, equivalence ratio, etc. Chemical ignition delay is main focus of this study which will be referred as ignition delay time(IDT or ID).

Ignition delay is crucial factor for design of combustor. Right amount of ignition delay is required for proper functioning of combustor. Ignition delay are generally calculated using reacting flow simulation which involves large number species and thousands of reaction including broad range of chemical and flow time scale. Calculation of IDT for various fuel and wide range of conditions is complicated and time consuming process. Ignition delay calculation using realistic-detail chemical mechanism requires full-scale numerical solvers which are computationally intensive.[1]

Taking motivation from such complications, acquired results gives simplified, accurate correlations along with efficient framework which is applicable over variety of fuels and wide range of 20 conditions.

#### 1.1. Literature review:

Substantial work has been done by researchers to calculate and correlate the ignition delay. 23 Major ignition delay models are of Arrhenius-type. 24

## **Notations:**

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P = PressureT = Temperature

 $\tau$  = Ignition Delay Time  $\phi$  = Equivalence Ratio  $X_{Oxi}$  = Oxidizer mole fraction  $X_{Fuel}$  = Fuel mole fraction  $E_a$  = Activation Energy  $\delta H$  = Change in enthalpy

R = Gas constantA = Scaling factorIDT = Ignition delay time C = Constant

**Horning et al.** [2] has conducted study of different hydrocarbon at high-temperature to observe 26 auto ignition and thermal decomposition. For n-alkanes at  $\phi = 1$  follows obtained ignition delay correlation is given as-1, 28

$$\tau = 9.40 * 10^{-6} P^{-0.55} X_{Oxi}^{0.63} C^{-0.5} e^{46500/RT}$$
 (1)

Where C is number of carbon atoms in the molecules. Correlation suggest that, ignition delay is not only function of pressure, temperature but it also depends on chemical characteristics of fuel. Such Arrhenius-type equations are constrained by certain physical condition. In parametric uncertainty [2], he has also mentioned that activation energy is very sensitive to ignition temperature.

In recent study of distillate fuels, Fethi and Amir [3] has obtained ignition delay correlation for gasoline and jet fuels using modified Arrhenius expression which applicable over wide range of conditions [P = 10-80 bar,  $\phi = 0.5$ -2]. By statistical methods and numerical simulation obtained correlation are mentioned as [2],

$$\tau_{gasoline} = 6.76 * 10^{-7} \frac{P}{20}^{-1.01} \phi^{1.13 - \frac{(17.59)}{T}} \exp \frac{29.39}{RT}$$
 (2)

for 
$$T > \frac{1000}{-0.073ln(\frac{P}{P_0}) + \phi^{-0.0338} + 0.0938}$$
 (3)

$$\tau_{JetFuel} = 4.76 * 10^{-7} \frac{P}{20}^{-1.21} \phi^{2.04 - \frac{(29.56)}{T}} \exp \frac{29.33}{RT}$$
for  $T > \frac{1000}{-0.0371 ln(\frac{P}{P_0}) + \phi^{-0.00727} + 0.0995}$ 
(5)

for 
$$T > \frac{1000}{-0.0371 ln(\frac{P}{P_0}) + \phi^{-0.00727} + 0.0995}$$
 (5)

Such correlations are useful for modeling of the fuel surrogates. But they are either fuel specific 37 or constrained by physical conditions.

**Goldsborough** has also suggested traditional Arrhenius-based, power law formulation for iso-octane [4]:

$$\tau = A\phi^{\alpha}P^{\beta}X_{O_{\gamma}}^{\gamma}exp(\lambda) \tag{6}$$

where,  $\alpha$ ,  $\beta$ ,  $\gamma$  are third order polynomials, to capture changes in functionality across different ignition delay regimes.  $\lambda$  is overall activation energy which is expressed by addition of two quadratic expression which also includes pressure terms in it.

**Zhao et al.** [5] has developed two ignition delay model for hydrogen/air mixtures using High Dimensional Model Representation (HDMR). Piece-wise correlation gives alternative for full kinetic mechanism. For that 2000 data points were obtained by random sampling of uniform distribution from given range parameter.

$$\frac{1}{1600} < \frac{1}{T_0} < \frac{1}{800}, -1 < \log_{10} P < 2, \log_{10} 0.2 < \log_{10} \phi < 1 \tag{7}$$

Obtained conditioned were used to run SENKIN(chemkin) simulation to obtain ignition delay values. Thus complete data-set of 2000 data points was used to generate correlation. Rather than generating single correlation, 2000 data points were divided into six segments based on pressure and temperature. All piece-wise models gives  $R^2 > 0.95$ .

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Upper NTC turnover points of n-butane, n-heptane and iso-octane exhibits typical kinetic and thermodynamic properties under different pressures. **Weiqi Ji et al.** [6] showed that, the ignition delay at the turnover states exhibits an Arrhenius dependence on the temperature and approximately inverse quadratic power law dependency on the pressure which implies that the temperature and pressure at turnover states are not independent and can be correlated as  $\ln P \propto \frac{1}{T}$ .

To predict auto-ignition and flame properties of multi-component fuel, **Neel et al.** [7] has used two machine learning algorithm random forest and neural network. For that, ignition delay data of toluene primary reference fuel [TPRF] extracted from kinetic simulation. While training the model, he has observed that the major concern of over-representative data as it does overfitting. Removal of under-representative data points predicted the IDT with better accuracy.

For prediction global combustion behavior, **Dussan et al.** [8] have used chemical functional group for analytical formulation of IDT.  $CH_2$ ,  $CH_3$  and benzyl-type functional group are used to represent n-alkyl, iso-alkyl and aromatics. High temperature formulation was generated using Scheff $\ddot{e}$  simplex polynomial(first order) with natural logarithm, considering temperature dependency of each functional group's mass fraction. The low temperature correlation was obtained by third order polynomial. Study concludes that molecular structure governs the combustion chemical kinetic behavior.

Apart from formulation, clustering of data also plays important role in generation of appropriate ignition delay model. **Chinta et al.** [9] have proposed clustering of parameter rather than clustering of data. He has also used statistical testing for removal of redundant parameters. The obtained piece-wise models gives better control in non-isothermal continuous stirred tank reactor.

From above discussion, concluded major affecting parameters i.e temperature, pressure, fuel mass fraction and molecular structure is utilized for model development. Also taking motivation from piece-wise cluster, rather than generating single cluster, error-based recursive clustering tree has been implemented. **The goal** of present study is to find out correlation which generalize, efficient, applicable over wide range physical condition and variety of fuel. To obtain this, it is necessary to modify Arrhenius-type equation. Formulation of ignition delay is discussed in next

73 sections.

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74 1.2. Ignition delay formulation:

Arrhenius-type ignition delay correlation has limitation of fuel specificity and are also bounded by constrain of affecting parameters. Major affecting parameters also carries uncertainty in results. To remove such complication, ignition delay correlation has to be reformulated.

In chemical reactions, the most sensitive parameter in ignition delay correlation is activation energy. Activation energy describes overall transformation of reaction and it only gives macroscopic information about reaction as intermediate species are not considered in any reaction. More microscopic information about the single step reaction can be obtained using the Eyring equation [10].

$$k = \kappa \left(\frac{k_B T}{h}\right) e^{\frac{\Delta S^{\ddagger}}{R}} e^{\frac{-\Delta H^{\ddagger}}{RT}} \tag{8}$$

Where,  $k_B$  = Boltzmann constant, T = absolute temperature, h = Planck's constant,  $\Delta S^{\ddagger}$  = Activation Entropy,  $\Delta H^{\ddagger}$  = Activation Enthalpy.

Eyring's equation is based on statistical and mechanical rationale of transition state theory whereas Arrhenius equation is empirical. These both equation are different in its nature. Relation between these two equations is possible when elementary reaction is as uni-molecular or bi-molecular. In such case, activation energy or energy barrier can be defined in terms of enthalpy of activation [10] which is closely related to bond energy.

$$E_a = \Delta H^{\ddagger} + nRT \tag{9}$$

According to transition state theory, when molecules with enough kinetic energy collides in certain orientation, it may generate activated complex. Bond structure of activated complex is different from reactants bond structure.  $\Delta H^{\ddagger}$  plays critical role in bond formation or breakage. So, enthalpy of activated complex is related to enthalpy of reaction.

In combustion, heat of combustion ( $\Delta H_{combustion}$ ) or heat of reaction ( $\Delta H_{reaction} = -\Delta H_{combustion}$ ) is directly related to bond dissociation energy [11] which can be expressed as,

$$\Delta H_{combustion} = H_{reactants} - H_{products}$$

$$\approx \text{Bond energy of Reactants} - \text{Bond energy of Products}$$
(10)

Being point function, enthalpy of activation ( $\Delta H^{\ddagger}$ ) for forward reaction can be expressed as difference between reactant state and activation state,

$$\Delta H^{\ddagger} = H_{reactant} - H^{\ddagger} \tag{11}$$

from equation-(10) & (11),

$$\Delta H^{\ddagger} = \Delta H_{combustion} + H_{products} - H^{\ddagger} \tag{12}$$

In IDT equation-(1) Horning et al. has showed that IDT depends on the number of carbons. So, Arrhenius-type ignition delay can be reformulated using equation-(9) and (12).

$$\tau = A \cdot \phi^{\alpha} \cdot P^{\beta} \cdot X_{O_{2}}^{\gamma} \cdot \exp\left(\frac{E_{a}}{RT}\right) \\
= A \cdot \phi^{\alpha} \cdot P^{\beta} \cdot X_{O_{2}}^{\gamma} \cdot \exp\left(\frac{\Delta H^{\ddagger} + nRT}{RT}\right) \\
= A \cdot \phi^{\alpha} \cdot P^{\beta} \cdot X_{O_{2}}^{\gamma} \cdot \exp\left(\frac{\Delta H_{combustion} + H_{products} - H^{\ddagger}}{RT}\right) \exp\left(\frac{nRT}{RT}\right) \\
= A \cdot \exp(n) \cdot \phi^{\alpha} \cdot P^{\beta} \cdot X_{O_{2}}^{\gamma} \cdot \exp\left(\frac{\Delta H_{combustion} + H_{products} - H^{\ddagger}}{RT}\right) \\
= C \cdot \phi^{\alpha} \cdot P^{\beta} \cdot X_{O_{2}}^{\gamma} \cdot \exp\left(\frac{\Delta H_{combustion} + H_{products} - H^{\ddagger}}{RT}\right) \\
= C \cdot \phi^{\alpha} \cdot P^{\beta} \cdot X_{O_{2}}^{\gamma} \cdot \exp\left(\frac{\Delta H_{combustion} + H_{products} - H^{\ddagger}}{RT}\right)$$

From-(10), it clear that enthalpy of combustion depends on the type of bond and bond energy.
Enthalpy being point function, it can be treated as constant term so, formulation can be rewritten as:

$$\tau \propto \phi^{\alpha} \cdot P^{\beta} \cdot X_{O_{2}}^{\gamma} \cdot \exp\left(\frac{\text{Fuel Bond Energy Term} + \text{Constant Energy Term}}{RT}\right)$$

$$\propto \phi^{\alpha} \cdot P^{\beta} \cdot X_{O_{2}}^{\gamma} \cdot \exp\left(\frac{1}{T} \cdot \left\{\frac{\text{Constant Energy Term}}{R} + \frac{\text{Fuel Bond Energy Term}}{R}\right\}\right) \tag{14}$$

Now, by dimensional analysis of Arrhenius exponent term,

$$\frac{E_{a}}{RT} \sim \left[\frac{\frac{KJ}{mol}}{\frac{KJ}{mol \cdot K} \cdot K}\right]$$

$$\frac{E_{a}}{R} \cdot \frac{1}{T} \sim \left[\frac{\frac{KJ}{mol}}{\frac{KJ}{mol \cdot K} \cdot K}\right]$$

$$\sim \left[\frac{\frac{KJ}{mol}}{\frac{KJ}{mol}}\right] \left[\frac{1}{K}\right]$$

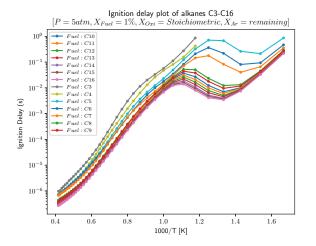
$$\sim \left[\frac{\frac{KJ}{mol} \cdot K}{\frac{KJ}{mol}}\right] \left[\frac{1}{K}\right]$$
Units of temprature
$$\sim \underbrace{(\alpha_{0} \cdot T_{0} + \alpha_{1} \cdot T_{0})}_{term - B} \cdot \frac{1}{T} \quad \text{where, } T_{0} - \text{Refrence Temprature}.$$

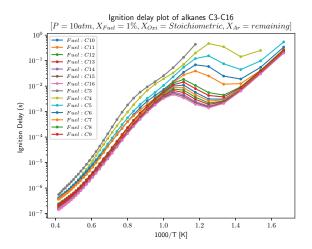
Now, comparing term-A in (14) and term-B in (15),

$$\left\{ \underbrace{\frac{\text{Constant Energy Term}}{R} + \frac{\text{Fuel Bond Energy Term}}{R}}_{term-A} \right\} \sim \underbrace{(\alpha_0 \cdot T_0 + \alpha_1 \cdot T_0)}_{term-B}$$
(16)

From comparison, it is clear that  $\beta_1$  contains information regarding types of bond. But it is difficult to obtain direct relationship between those parameters which can be obtained using chemical kinetic simulations of different fuels.

Chemical kinetic simulation of Propane-[12], Butane-[13], Pentane-[14], Hexane-[15], Heptane-[16], and Octane to Hexa-Decane-[17] fuel has been conducted using constant volume reactor at condition of P=5atm and 10 bar,  $X_{Fuel} = 1\%$ ,  $X_{Oxygen}$ =According to stochiometry,  $X_{Ar}$  =remaining, T=600 to 2400 K by increment of 50K using ChemKin-18.1. From obtained result mentioned in fig-1(a) & 1(b), it clear that from 2400 K (higher temperature) to around 1000K curve follows almost linear relationship. Slope of linear fit slope gives  $\frac{E_a}{R}$ .





- (a) Ignition delay result of C3-C16 alkanes at 5atm
- (b) Ignition delay result of C3-C16 alkanes at 10atm

Figure 1: Ignition delay result of C3 - C16 alkanes at P= 5atm and 10atm,  $X_{Fuel} = 1\%$ ,  $X_{Oxygen} = According$  to stochiometry,  $X_{Ar} = Remaining$ , T= 600 to 2400 K.

Obtained  $\frac{E_a}{R}$  values for different fuels are shown in figure-4(a) and 4(b). All blue points shows  $\frac{E_a}{R}$  value obtained by performing regression over simulation result. Plotting the  $\frac{E_a}{R}$  against number of secondary carbon-hydrogen bonds- $C_{SH}$  gives hidden information regarding relationship between two parameters. Detail of  $C_{SH}$  bonds are illustrated in fig-2 by taking example of pentane.

In figure-3(a) and 3(b), points shows  $\frac{E_a}{R}$  values obtained by regression considering data within temperature range of 1800 to 1250 K. Each data point of  $\frac{E_a}{R}$  is associated with each fuel. Same way, points in figure-4(a) and 4(b) were obtained by performing regression considering all data from T= 600 to 2400 K. By looking at trend of data points, intuitively it looks obvious that  $\frac{E_a}{R}$  data follows nearly inversely proportional relationship with  $C_{SH}$ .

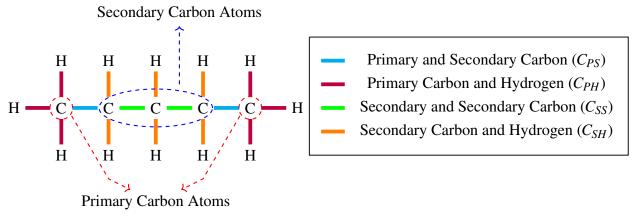


Figure 2: Different type of bonds in straight alkane (Pentane)

To verify the relationship between  $\frac{E_a}{R}$  and  $C_{SH}$ - (Number of secondary carbon-hydrogen bonds) used hypothesis is mentioned below:

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$$\frac{E_a}{R} \propto \frac{1}{C_{SH}}$$

$$\frac{E_a}{R} \propto \beta_0 + \beta_1 \cdot \frac{1}{C_{SH}}$$

$$\frac{E_a}{R} \propto \beta_0 + \beta_1 \cdot C_{SH}^{-1}$$
(17)

By inverting  $C_{SH}$  data and performing simple linear regression. Obtained regression coefficient and  $R^2$  valued are mentioned in respective plots. All the values in fig-3(a), 4(a), 3(b), 4(b) shows promising results in favor of hypothesis with  $R^2 > 0.84$  for different cases.

To maintain dimensionality, temperature term is used as proportionality constant.

$$\frac{E_a}{R} = T_0 \cdot \beta_0 + \beta_1 \cdot \frac{T_0}{C_{SH}} \tag{18}$$

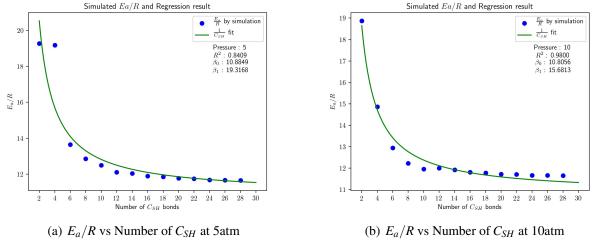


Figure 3:  $E_a/R$  (using data ranges from 600 to 2400K) vs number  $C_{SH}$  bonds and also its regression fit

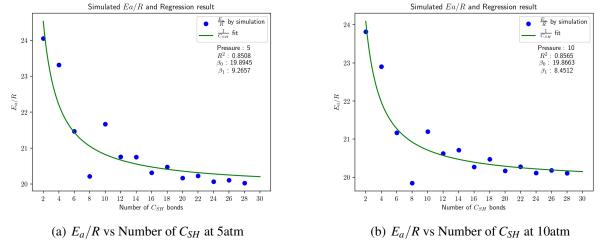


Figure 4:  $E_a/R$  (using data ranges from 1250 to 1800K) vs number  $C_{SH}$  bonds and also its regression fit

From equation- (16) and (18) the obtain term can be written as,

$$\left\{\underbrace{\frac{\text{Constant Energy Term}}{R} + \frac{\text{Fuel Bond Energy Term}}{R}}_{term-A}\right\} \sim \underbrace{\left(\alpha_0 \cdot T_0 + \alpha_1 \cdot T_0\right)}_{term-B} \sim \underbrace{\left(T_0 \cdot \beta_0 + \beta_1 \cdot \frac{T_0}{C_{SH}}\right)}_{term-C}$$
(19)

Replacing term-A of formulation-14 with term-C mentioned above, gives final formulation for ignition delay with replacement of activation energy with bond details - 20.

$$\tau \propto \phi^{\alpha} \cdot P^{\beta} \cdot X_{O_2}^{\gamma} \cdot \exp\left(\frac{1}{T} \cdot \left\{ T_0 \cdot \beta_0 + \beta_1 \cdot \frac{T_0}{C_{SH}} \right\} \right)$$
 (20)

This formulation gives clear indication regarding, ignition delay dependency on the fuel bonds. To make quantities independent of unit, some terms in the formulation is normalized with unit quantities. Considering all the possible affecting parameters in above formulation-20, the functional form it can be expressed as:

$$\tau = f(T, P, \phi, X_{Fuel}, X_{O_2}, X_{Dilutant}, C_{SH})$$
(21)

But it is known that,

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$$X_{Fuel} + X_{O_2} + X_{Dilut6ant} = 1 \quad \& \quad \phi = \frac{\left(\frac{X_{fuel}}{X_{O_2}}\right)_{act}}{\left(\frac{X_{fuel}}{X_{O_2}}\right)_{stochio}}$$
(22)

As Fuel composition is already known, from stoichiometry equation,  $\left(\frac{X_{fuel}}{X_{O_2}}\right)_{stochio}$  is attainable.

It is possible to obtain  $\phi$  from  $X_{fuel}$  and  $X_{O_2}$ , which is also true for  $X_{Diluant}$ .

Removing redundant function formulation can be re-written as,

$$\tau = f(T, P, X_{Fuel}, X_{O_2}, C_{SH}) \tag{23}$$

$$\tau \propto \left(\frac{P}{P_0}\right)^b \cdot X_{Fuel}^c \cdot X_{O_2}^d \cdot exp\left(\beta_0 \cdot \frac{T_0}{T} + \beta_1 \cdot \frac{T_0}{T \cdot C_{SH}}\right)$$

$$= C' \cdot \left(\frac{P}{P_0}\right)^b \cdot X_{Fuel}^c \cdot X_{O_2}^d \cdot exp\left(\beta_0 \cdot \frac{T_0}{T} + \beta_1 \cdot \frac{T_0}{T \cdot C_{SH}}\right)$$
(24)

Formulation can simplified by taking natural log on both side,

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$$ln(\tau) = ln(C') + b \cdot ln(\frac{P}{P_0}) + c \cdot ln(X_{Fuel}) + d \cdot ln(X_{O_2}) + \beta_0 \cdot \frac{T_0}{T} + \beta_1 \cdot \frac{T_0}{T \cdot C_{SH}}$$

$$ln(\tau) = C + b \cdot ln(\frac{P}{P_0}) + c \cdot ln(X_{Fuel}) + d \cdot ln(X_{O_2}) + \beta_0 \cdot \frac{T_0}{T} + \beta_1 \cdot \frac{T_0}{T \cdot C_{SH}}$$
(25)

where, C, b, c, d,  $\beta_0$ ,  $\beta_1$  are coefficients, which is attainable from ignition delay data using multiple regression. It was assumed that ignition delay correlation depends on all the parameters which can be refined using hypothesis testing. To obtain models, multiple regression was used with error based clustering, which explained in further discussion. The fundamental step of whole process is to collect the data and make of processable, which is discussed in next section.

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