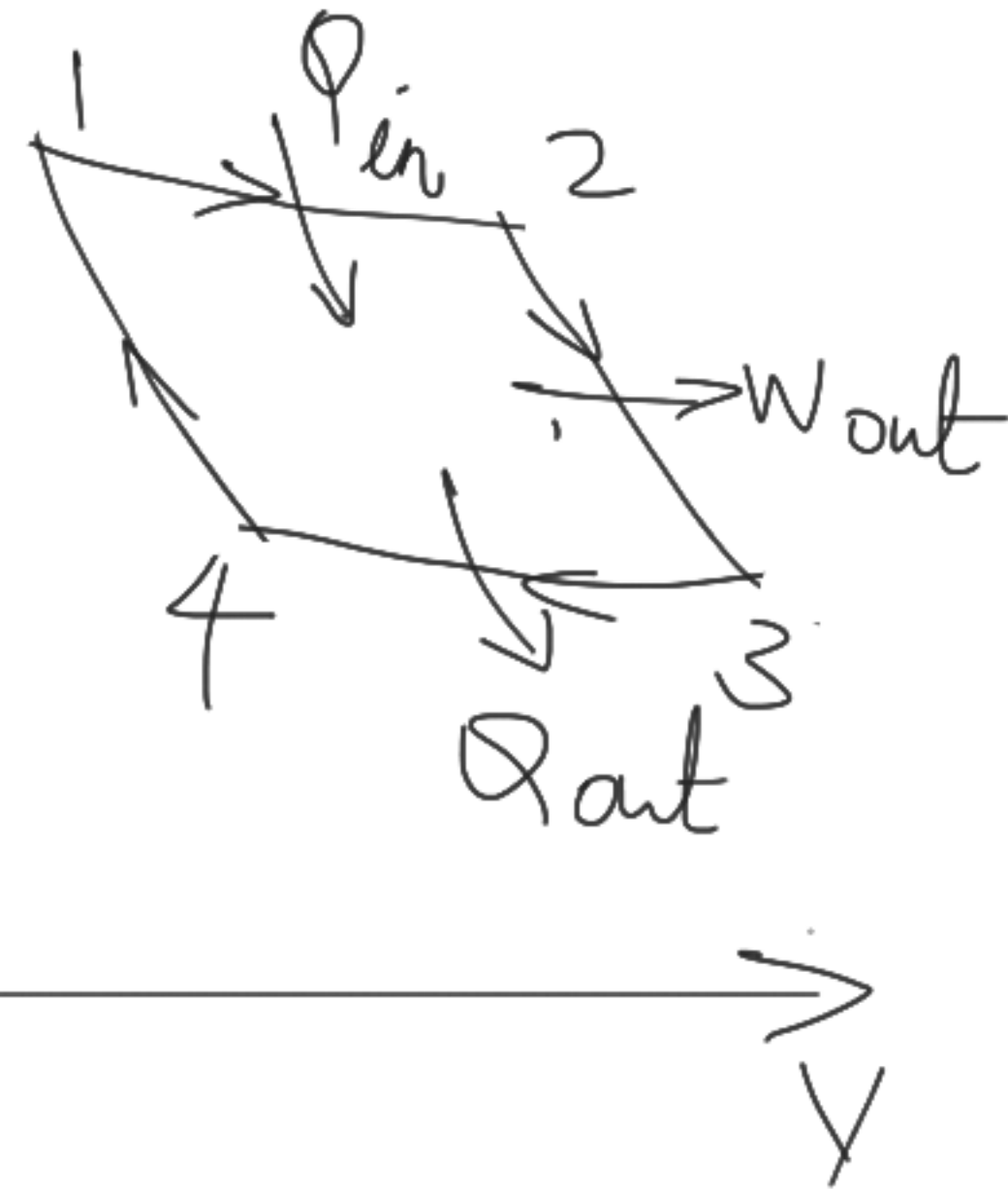


Carnot Cycle (continues ---)

04-12-'21

$$\eta = 1 - \frac{Q_R}{Q_S} = 1 - \frac{mRT_3 \ln(V_3/V_4)}{mRT_1 \ln(V_2/V_1)}$$

$$\text{u } \eta = 1 - \frac{T_3}{T_1} \frac{\ln(V_3/V_4)}{\ln(V_2/V_1)} \quad \text{--- (a)}$$



Process 2-3

V-T relation.

$$\frac{T_2}{T_3} = \left(\frac{V_3}{V_2} \right)^{\gamma-1} \quad \text{--- (i)}$$

Process 4-1

V-T relation

$$\frac{T_1}{T_4} = \left(\frac{V_4}{V_1} \right)^{\gamma-1}$$

$$\frac{T_2}{T_3} = \left(\frac{V_4}{V_1} \right)^{\gamma-1} \quad \text{--- (ii)}$$

$$T_1 = T_2$$

$$T_3 = T_4$$

Comparing (i) and (ii)

$$\Rightarrow \left(\frac{V_3}{V_2} \right)^{\gamma-1} = \left(\frac{V_4}{V_1} \right)^{\gamma-1}$$

$$\frac{V_3}{V_2} = \frac{V_4}{V_1} \quad \text{--- (iii)}$$

Adiabatic Expansion = Adiabatic Compression ratio

or $\frac{V_3}{T_4} = \frac{V_2}{T_1} \quad \text{--- (iv)}$

i.e. isothermal compression = isothermal expansion
 state state

$$\therefore \eta = 1 - \frac{T_3 \times \ln \left(\frac{V_3}{V_4} \right)}{T_1 \times \ln \left(\frac{V_2}{V_1} \right)} \quad (\text{from (i)})$$

$$= 1 - \frac{T_3 \times \ln \left(\frac{V_3}{V_4} \right)}{T_1 \times \ln \left(\frac{V_3}{V_4} \right)}$$

$$\eta = 1 - \frac{T_3}{T_1}$$

$$\eta = 1 - \frac{T_{\text{cold body}}}{T_{\text{hot body}}}$$

If T_H - temp. of hot body
 T_L - temp. of cold body.

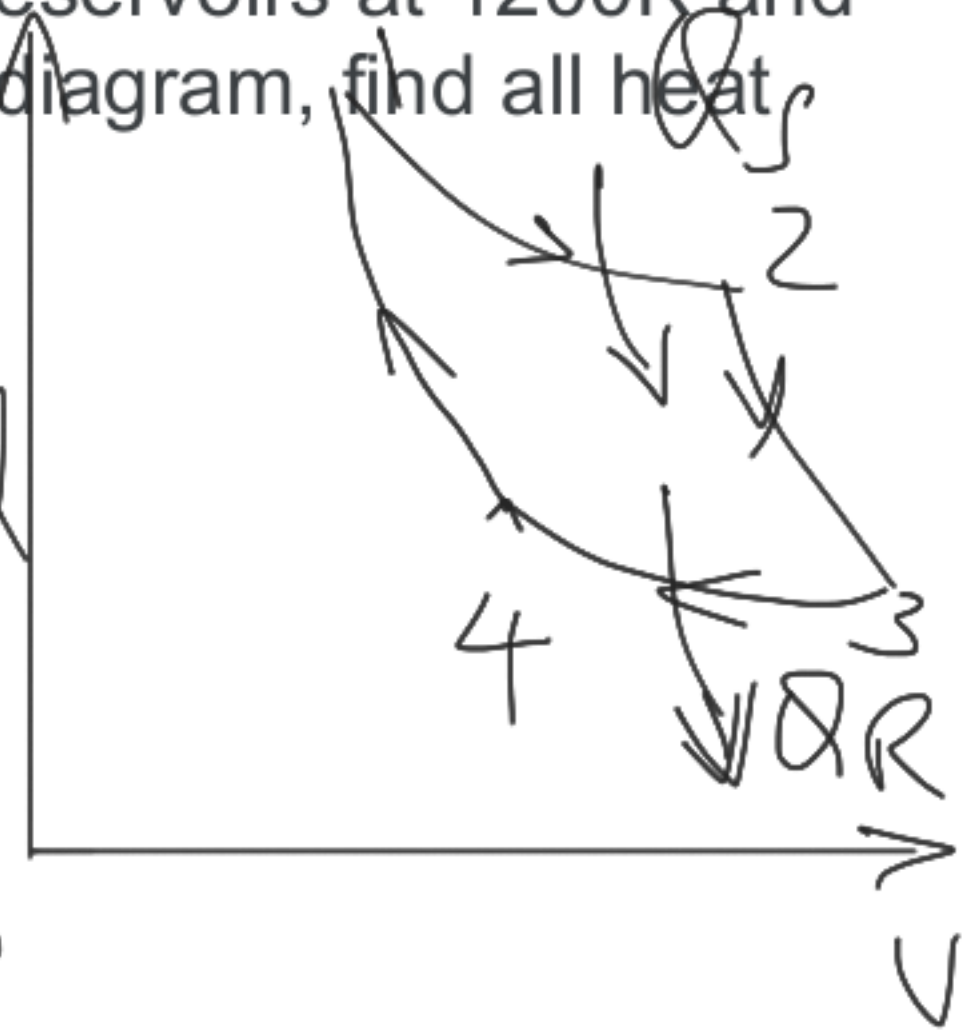
$$\eta = 1 - \frac{T_L}{T_H}$$

- Practically Carnot cycle is impossible
- of all the theoretical cycles, Carnot cycle is having maximum efficiency - to compare with other cycles

↙ Alternate isothermal & adiabatic processes are difficult to carry out.

Air undergoes a Carnot cycle inside a piston-cylinder between thermal reservoirs at 1200K and 400K. During heat addition, the volume triples. Draw the cycle on a P-v diagram, find all heat transfers in kJ/kg, and the overall cycle efficiency.

$$\begin{array}{l}
 T_1 = T_2 = 1200\text{K} \quad (\text{Source}) \\
 T_3 = T_4 = 400\text{K} \quad (\text{Sink})
 \end{array}
 \left. \vphantom{\begin{array}{l} T_1 = T_2 = 1200\text{K} \\ T_3 = T_4 = 400\text{K} \end{array}} \right\} \begin{array}{l} \text{thermal} \\ \text{energy} \\ \text{reservoirs} \end{array}$$



Heat transfers

$$Q_s = P_1 V_1 \ln(V_2/V_1) = m R T_1 \ln(V_2/V_1)$$

$$R_{\text{air}} = 287 \text{ J/kg K}$$

$$V_2 = 3V_1 \quad (\text{during heat addition})$$

$$\frac{V_2}{V_1} = 3$$

$$\therefore Q_S = 1 \times 287 \times 1250 \times \ln(3) =$$

J/kg or
kJ/kg

$$Q_R = mR T_3 \ln\left(\frac{V_3}{V_4}\right) = mR T_3 \times \ln\left(\frac{V_2}{V_1}\right)$$

$$= 1 \times 287 \times 400 \times \ln(3)$$

$$= \text{J/kg or kJ/kg}$$

$$\eta = 1 - \frac{T_3}{T_1} = 1 - \frac{400}{1200} = 1 - \frac{1}{3} = \underline{\underline{\frac{2}{3}}}$$

(or) 66.667%