Fluid Dynamics

Chapter 3

Conservation Laws for Mass and Energy

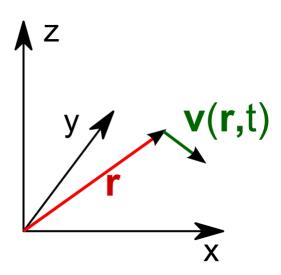
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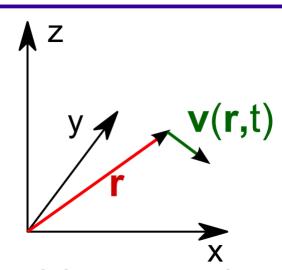
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- Consideration of fluid flows
- Movement of a fluid is in general dependent on
 - the place (x,y,z-coordinates or radius r)
 - the time t
- Approaches for description of fluid flow
 - Euler's definition
 - Lagrange definition



- Euler's definition
 - In a given coordinate system with space coordinates r the velocity v(r,t) is given at every point



- Lagrange definition
 - At a starting time t_0 , the starting position \mathbf{r}_0 and velocity \mathbf{v}_0 are noted
 - At a later time, the current place $\mathbf{r}(\mathbf{r}_0, \mathbf{v}_0, \mathbf{t})$ and time $\mathbf{v}(\mathbf{r}_0, \mathbf{v}_0, \mathbf{t})$ can be pictured as a function of the starting values for every fluid element

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- Euler's definition is from a mathematical point of view easier to implement than the Lagrange definition. That is why the Euler definition is commonly used.
- However, thinking about how we are observing flows, we notice that our eyes are following a moving reference point of a flow. This method complies with the Langrange definition.

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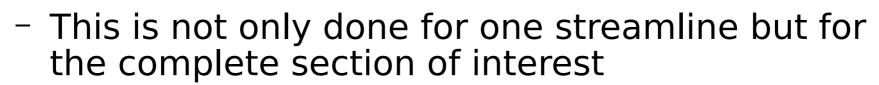
- Steady flows
 - The fluid elements change their position with time but the velocity field (and other physical properties) itself stays constant at every place and experiences no temporal change
- Unsteady flows
 - The velocity changes at one or more places within the flow field with time

Streamlines and Pathlines

Streamlines

 For a given point in time, curves can be constructed within the flow so that the tangent to these curves are the velocity vectors of the





 Streamlines indicate where a fluid element is going to move in the next moment

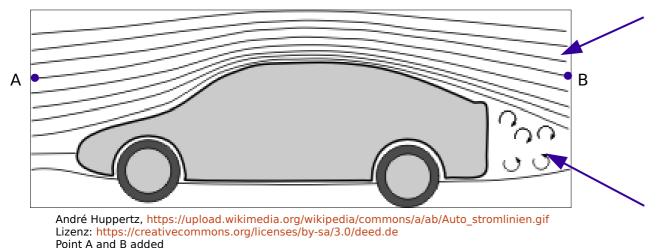
Streamlines and Pathlines

Pathlines

- A pathline is the curve in space that is defined by the movement of a specific fluid element within a specified time interval
- Pathlines are what we see while we are watching a moving reference point in a flow
 - e.g. a leaf on a river
- For steady flows, streamlines and pathlines are identical
- For unsteady flows streamlines and pathlines are different

Streamlines and Pathlines: Examples

Streamlines around a car:



In this area the flow is steady, which means it is constant over time

In this area of the vortexes, the flow is unsteady. It changes constantly over time

- Per definition a streamline is only defined for one point in time. But if the flow is steady, which means constant over time, the streamline applies to every point in time.
- In case of steady flow, a fluid element starting in point A moves step by step on a particular streamline. The streamline is also the pathline for this fluid element.
- Result: the fluid element does not leave the streamline and arrives in point B

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Streamlines and Pathlines: Examples

... and in the experiment:



Deutsches Zentrum für Luft und Raumfahrt, https://upload.wikimedia.org/wikipedia/commons/1/10/Schl%C3%B6rwagen_Windkanal_Modell.jpg Lizenz:https://creativecommons.org/licenses/by/3.0/deed.de

 ...and a simulation: https://www.youtube.com/watch?v=09tVUvtyOmk

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Conservation of Mass - Continuity Equation

- The mass of a fluid is not altered by a flow
- This is described by the continuity equation
- We are considering the continuity equation just for steady flows
- We are using the mass flow rate to balance the mass in a flow:
 - Mass flow \dot{m} is the mass per time interval that flows through an cross sectional area
 - The unit is kg/s

Conservation of Mass - Mass Flow

- How can the mass flow be calculated?
- Given is a fluid with density ρ and velocity v vertical on the area A
- Let's consider the fluid elements that are on the area A at starting time
- After a time Δt they moved the distance $\Delta x = v \cdot \Delta t$
- In the same time interval further fluid elements moved to the area A. The so defined volume $\Delta x \cdot A$ is filled with the mass of the fluid that moved through the area A. The fluid has the density ρ . The mass Δm in this volume is:

$$\Delta m = \rho \cdot \Delta x \cdot A = \rho \cdot v \cdot \Delta t \cdot A \quad \Rightarrow \quad \dot{m} = \frac{\Delta m}{\Delta t} = \rho \cdot v \cdot A$$

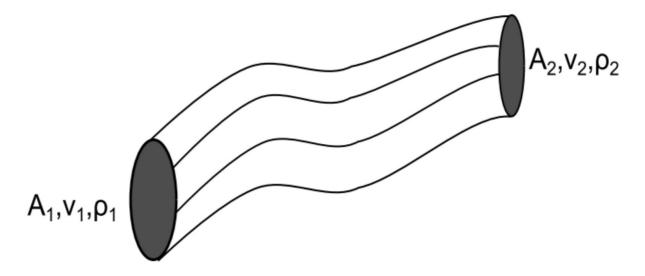
Mass flow through area A

 $\Delta x = v \cdot \Delta t$

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Conservation of Mass - Continuity Equation

- Motivation of the continuity equation for steady flows
- Consideration of a stream pipe:



- Areas A₁ and A₂ vertical to the streamlines
- Streamlines crossing A1 and A2 form the stream pipe
- Shell surface: streamlines that cross the border of the areas A₁ and A₂

Conservation of Mass- Continuity Equation

- Consideration of the mass flow trough the flow pipe
 - The mass flowing into the stream pipe through area A₁ cannot escape trough the shell surface because fluid elements always move with the streamlines in case of steady flow
 - The mass leaves the pipe trough area A_2 . The mass flowing through the two areas is the same:

$$\dot{m}_1 = \dot{m}_2$$

 If density and velocity are constant over the area, the continuity equation is formed

$$\rho_1 \mathbf{v}_1 \mathbf{A}_1 = \rho_2 \mathbf{v}_2 \mathbf{A}_2$$

Conservation of Mass - Continuity Equation

 For incompressible flows with constant density the continuity equation can be simplified even more:

$$\rho v_1 A_1 = \rho v_2 A_2$$

$$v_1 A_1 = v_2 A_2$$

$$\dot{V}_1 = \dot{V}_2$$

• We introduce the volume flow rate \dot{V} :

$$\dot{V} = v \cdot A \implies \dot{m} = \rho \cdot \dot{V}$$

- The volume flow has the unit [volume per time] and is a useful quantity for incompressible fluids
 - e.g. liter/hour
- The general continuity equation for compressible unsteady flows can be found in chapter 6

Conservation of Energy - Bernoulli Equation

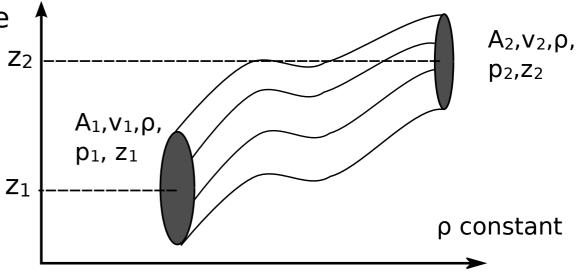
- Energy is maintained no creation or destruction
- But: energy can be transformed from one form to another. For example kinetic energy to potential energy
- And: energy can be transported over system boundaries in both directions
- Relevant forms of energy in this lecture:
 - Kinetic and potential energy
 - Mechanical energy (e.g. pressure)
- We do not consider: thermal and chemical energy
- Restriction to
 - isothermal,
 - frictionless ("ideal"),
 - steady and
 - incompressible flows (ρ constant)
- Energy balance of these flows: Bernoulli equation

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Conservation of Energy- Bernoulli Equation Derivation 1

restrictions: see slide before!

Balance area is a flow pipe



- Inlet with area A₁ at height z₁
 with constant quantities:
 - Density ρ
 - Velocity v₁
 - Pressure p₁
- Similarly outlet with area A₂

Important:

The z-axis is pointing **upwards!**

- Energy content within stream pipe depends on inflow through A₁ and outflow through A₂
- Flow is given by volume flow \dot{V} and mass flow \dot{m}
- For the balance, we need the energy rate of change (energy change per unit time interval)
- kinetic energy $\frac{1}{2}mv^2$
 - Rate of change due to mass flow $\frac{1}{2}\dot{m}v$
- potential energy mgz
 - Rate of change due to mass flow $\dot{m}gz$
- Work against pressure in the pipe
 - Rate of change due to volume flow

$$F \Delta s = p A \Delta s$$

$$p A \frac{\Delta s}{\Delta t} = p A v = \underline{p \dot{V}}$$

 "Steady" means the flow does not change in time in the stream pipe. That means the energy outflow is the equal to the inflow.

$$\dot{m}\frac{v_1^2}{2} + \dot{m}gz_1 + p_1\dot{V}_1 = \dot{m}\frac{v_2^2}{2} + \dot{m}gz_2 + p_2\dot{V}_2$$

• Using $\dot{m} = \rho \dot{V}$ gives:

$$\rho \dot{V}_{1} \frac{v_{1}^{2}}{2} + \rho \dot{V}_{1} g z_{1} + p_{1} \dot{V}_{1} = \rho \dot{V}_{2} \frac{v_{2}^{2}}{2} + \rho \dot{V}_{2} g z_{2} + p_{2} \dot{V}_{2}$$

 Since the density is constant ('incompressible') the continuity equation applies in the following form:

$$\dot{V}_1 = \dot{V}_2$$

• We divide both sides by volume flow rate \dot{V} :

$$\rho \frac{v_1^2}{2} + \rho g z_1 + p_1 = \rho \frac{v_2^2}{2} + \rho g z_2 + p_2$$

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• There is no special requirement for the position of the areas A_1 , A_2 . We can place them anywhere in the stream pipe. But the equality always applies:

$$\rho \frac{v_1^2}{2} + \rho g z_1 + p_1 = \rho \frac{v_2^2}{2} + \rho g z_2 + p_2$$

 In other words, the total energy of the fluid is constant (friction is ignored!):

$$p+\rho\frac{v^2}{2}+\rho gz=\text{const.}$$

- This is the **Bernoulli Equation**
 - In general, the upper form of the eq. is used, in order to calculate the energy at one point of the flow as function of another point.

• In this form, the Bernoulli Equation has the unit of pressure: v^2

 $p+\rho \frac{v^2}{2}+\rho gz=\text{const.}$

 If the eq. Is divided by pg, the Bernoulli equation has the form

$$\frac{p}{\rho g} + \frac{1}{2g}v^2 + z = \text{const.}$$

- In this form, all terms have the dimension of a height z
- Important for both forms: The z-axis points upwards, because the potential energy E_{pot}=mgz is only correct for this case!

Example of transformation of energy

 Kinetic energy is larger at z₂:

$$v_1 A_1 = v_2 A_2$$

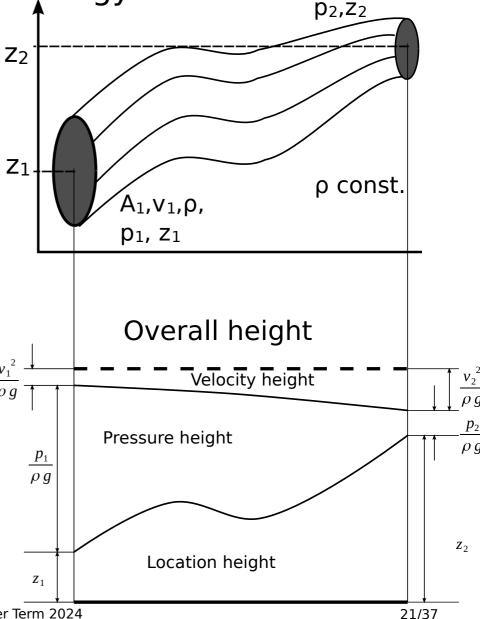
$$A_1 > A_2 \Rightarrow v_1 < v_2$$

 Potential energy is larger at z₂ because:

$$Z_1 \leq Z_2$$

 Higher kinetic and potential energy at z₂ implies lower pressure energy content. Thus:

$$p_1 > p_2$$

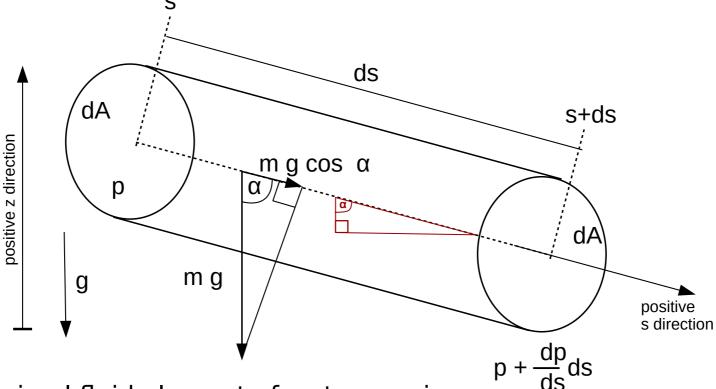


 A_2, V_2, ρ

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Conservation of Energy - Bernoulli Equation Derivation 2

Restrictions as before: isothermal, steady, incompressible, ideal flow



- · Infinitesimal fluid element of a stream pipe
 - Position given by the length s
 - Constant cross section dA
 - Inclination α against the vertical line
 - Mass of a fluid element: $m = \rho dA ds$

 We want to determine the forces in s direction and set up the equation of motion (Newton's 2nd law) for a fluid element

Forces:

- Pressure force at point s: p(s)dA = pdA
- Pressure force at point s+ds from Taylor series for pressure

$$p(s+ds) \approx p(s) + \frac{dp(s)}{ds} ds = p + \frac{dp}{ds} ds$$

$$\Rightarrow p(s+ds) dA \approx p dA + \frac{dp}{ds} ds dA$$

- Gravity force: $mg\cos(\alpha)$
- All together ... next page

- Before we derive the equation of motion (Newton's 2nd law) for a fluid element, we have to clarify the signs:
 - The pressure force at point s acts in the direction of s
 ⇒ positive
 - The pressure force at point s+ds on the fluid element acts in the opposite direction of s ⇒ negative
 - Gravity acts in the direction of s ⇒ positive
- Together

$$m\frac{dv}{dt} = \rho \, dA \, ds \, \frac{dv}{dt} = p \, dA - (p \, dA + \frac{dp}{ds} \, ds \, dA) + \rho \, ds \, dA \, g \cos(\alpha)$$

$$\rho \, \frac{dv}{dt} = -\frac{dp}{ds} + \rho \, g \cos(\alpha) \qquad (*)$$

- In the last step, we canceled dA.

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A positive change in s causes a negative change in z.
 From the red triangle in the illustration of the fluid element on page 22 before we get:

$$\cos(\alpha)ds = -dz \implies \cos(\alpha) = -\frac{dz}{ds}$$

 The flow is steady. The speed does not depend on the time, it depends on the position s: v(s). But the position s changes for our flowing fluid element: s=s(t). For the speed we get v(s(t)). Therefore:

$$\frac{dv}{dt} = \frac{dv}{ds} \frac{ds}{dt}$$
 (Derivative Chain Rule)

 The change of the position s(t) by time is the speed itself:

$$\frac{ds}{dt} = v \implies \frac{dv}{dt} = \frac{dv}{ds}v = v\frac{dv}{ds}$$

We put that into (*):

$$\rho \frac{dv}{dt} = -\frac{dp}{ds} + \rho g \cos(\alpha) \qquad | \cos(\alpha) = -\frac{dz}{ds}$$

$$\Rightarrow \rho \frac{dv}{dt} = -\frac{dp}{ds} - \rho g \frac{dz}{ds} \qquad | \frac{dv}{dt} = v \frac{dv}{ds}$$

$$\Rightarrow \rho v \frac{dv}{ds} = -\frac{dp}{ds} - \rho g \frac{dz}{ds}$$

Two more tricks:

- It is
$$\frac{d}{ds} \left(\frac{1}{2} v^2 \right) = v \frac{dv}{ds}$$

- Because g and ρ are constant: $\rho g \frac{dz}{ds} = \frac{d}{ds} (\rho g z)$

$$\rho g \frac{dz}{ds} = \frac{d}{ds} (\rho g z)$$

This gives:

$$\rho \frac{d}{ds} \left(\frac{1}{2} v^2 \right) = -\frac{dp}{ds} - \frac{d}{ds} (\rho g z)$$

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With that we get the following:

$$\rho \frac{d}{ds} \left(\frac{1}{2} v^2 \right) = -\frac{dp}{ds} - \frac{d}{ds} (\rho g z) \qquad \qquad \rho = \text{const.}$$

$$\Rightarrow \frac{d}{ds} \left(\rho \frac{v^2}{2} \right) = -\frac{dp}{ds} - \frac{d}{ds} (\rho g z) \qquad \qquad | \text{All terms on one side}$$

$$\Rightarrow \frac{d}{ds} \left(\rho \frac{v^2}{2} \right) + \frac{dp}{ds} + \frac{d}{ds} (\rho g z) = 0 \qquad \qquad | \text{All terms derivatives by s.}$$

$$\Rightarrow \frac{d}{ds} \left(\rho \frac{v^2}{2} + p + \rho g z \right) = 0$$

$$\Rightarrow \frac{d}{ds} \left(\rho \frac{v^2}{2} + p + \rho g z \right) = 0$$

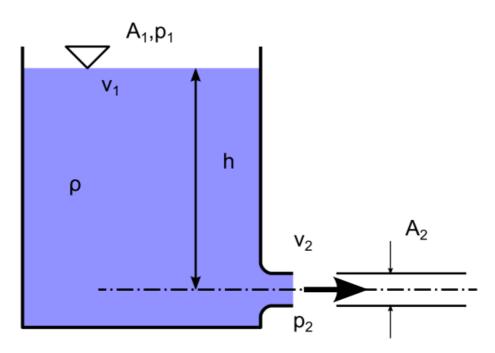
 If the derivative is zero, the term is constant. From this we get again the <u>Bernoulli-Equation</u>:

$$\rho \frac{v^2}{2} + p + \rho g z = \text{const.}$$

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Usage of the Bernoulli Equation Flow from a Water Tank

- Water flows out of a tank through a small outlet.
- Assumption: frictionless, stationary, incompressible
- Looking for: outlet speed v₂
- Approach: We are looking at a streamline between the water surface (z_1) and the outlet (z_2) .



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Usage of the Bernoulli equation Flow from a Water Tank

Calculation of v₂ with Bernoulli and Conti.-Equ.

$$\rho \frac{v_{1}^{2}}{2} + \rho g z_{1} + p_{1} = \rho \frac{v_{2}^{2}}{2} + \rho g z_{2} + p_{2}$$

$$\Rightarrow \rho \frac{v_{1}^{2}}{2} + \rho g z_{1} = \rho \frac{v_{2}^{2}}{2} + \rho g z_{2}$$

$$\Rightarrow \rho \frac{\left(\frac{v_{2} A_{2}}{A_{1}}\right)^{2}}{2} + \rho g z_{1} = \rho \frac{v_{2}^{2}}{2} + \rho g z_{2}$$

$$\Rightarrow 2g z_{1} - 2g z_{2} = v_{2}^{2} - \left(\frac{A_{2}}{A_{1}}\right)^{2} v_{2}^{2}$$

$$\Rightarrow v_{2} = \sqrt{\frac{2gh}{1 - \left(\frac{A_{2}}{A_{2}}\right)^{2}}} \Rightarrow v_{2} = \sqrt{2gh} \text{ (Torricelli)}$$

 $p_1=p_2=$ ambient pressure, counteract.

Conti.-Equ.:
$$\rho v_1 A_1 = \rho v_2 A_2$$

$$\Rightarrow v_1 = \frac{v_2 A_2}{A_1}$$

times 2, divide by ρ , then sort

$$h = z_1 - z_2$$
 and dissolve by v_2

The last simplification uses $A_2 / A_1 \ll 1$, if the outflow is much smaller than that water surface in the tank

- Separate parts of pressure in a fluid
 - Static pressure

$$p_s$$

- Dynamic pressure

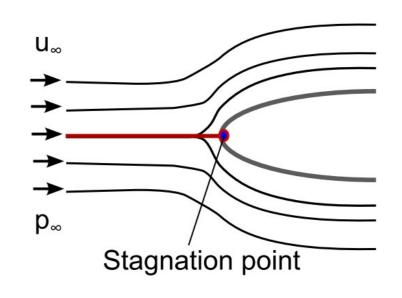
$$p_d = \rho \frac{v^2}{2}$$

Total pressure

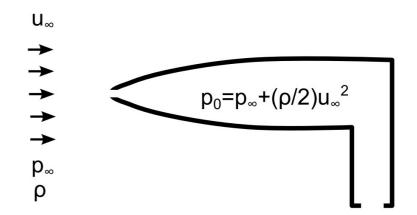
$$p_t = p_s + p_d + \rho g z$$

- Bernoulli:
 The total pressure is constant on a streamline.
- Stagnation point
 - Static pressure: maximum
 - Kinetic energy: minimum
- Stagnation pressure:

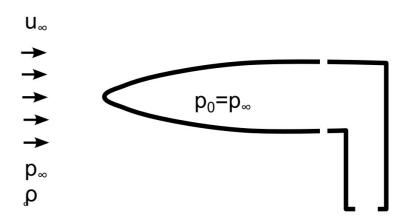
$$p_{\text{stagnation}} = p_s + p_d = p_{\infty} + \rho \frac{u_{\infty}^2}{2}$$



- Pitot tube
 - Measurement of total pressure
 - Static pressure unknown



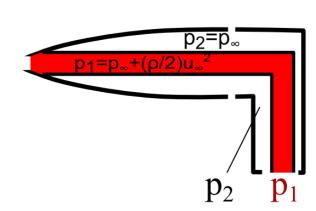
- Pressure probe
 - Measurement of static pressure



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- Prandtl probe
 - Assumption: close streamlines have the same total pressure
 - That's why: Difference in height is negligible

→ → → p_∞ρ



With that the flow rate can be determined:

$$p_1 - p_2 = p_\infty + \rho \frac{u_\infty^2}{2} - p_\infty = \rho \frac{u_\infty^2}{2} \Rightarrow u_\infty = \sqrt{\frac{2(p_1 - p_2)}{\rho}}$$

- Use for this device: Measurement of the speed of airflow around aircraft
 - Attention: That is not the speed above ground!

Airplane Pitot Tubes

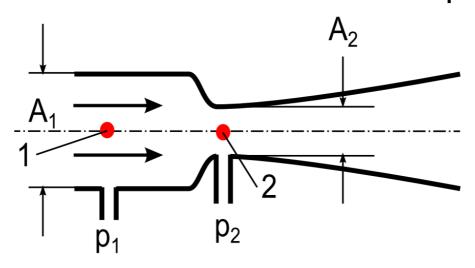






https://en.wikipedia.org/wiki/Pitot_tube

- Venturi nozzle
 - Measurement of volume flow in a pipe



 Determination of volume flow with Bernoulli and continuity equation

$$p_1 + \rho \frac{v_1^2}{2} + \rho g z_1 = p_2 + \rho \frac{v_2^2}{2} + \rho g z_2$$
 $|z_1 = z_2|$

Determination of volume flow (continued)

$$p_{1}+\rho \frac{v_{1}^{2}}{2}=p_{2}+\rho \frac{v_{2}^{2}}{2}$$

$$\Rightarrow p_{1}+\rho \frac{\left(\frac{v_{2}A_{2}}{A_{1}}\right)^{2}}{2}=p_{2}+\rho \frac{v_{2}^{2}}{2}$$

$$\Rightarrow 2\frac{\Delta p}{\rho}=v_{2}^{2}-\left(\frac{A_{2}}{A_{1}}\right)^{2}v_{2}^{2}$$

$$\Rightarrow v_{2}=\sqrt{\frac{2\Delta p}{\rho\left(1-\left(\frac{A_{2}}{A_{1}}\right)^{2}\right)}}$$

$$\Rightarrow \dot{V}=v_{2}\cdot A_{2}$$

Conti.-Equ.:
$$\rho v_1 A_1 = \rho v_2 A_2$$

$$\Rightarrow v_1 = \frac{v_2 A_2}{A_1}$$

- times 2, divide by ρ, then sort
- use $\Delta p = p_1 p_2$

Separate for v₂

Volume flow at point 2. Because it is constant, it is the volume flow through the pipe.

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- Important for usage in reality:
 - Consideration of the friction of real fluids
- Coefficient C_d comes as manufacturer information for any particular Venturi nozzle
- From consideration:

$$\dot{V} = v_2 A_2 \quad \Rightarrow \quad \dot{V} \propto A_2 \sqrt{\left(\frac{2\Delta p}{\rho}\right)}$$

we get

$$\dot{V} = C_d A_2 \sqrt{\left(\frac{2\Delta p}{\rho}\right)}$$

• The factor $1/\sqrt{(1-(A_2/A_1)^2)}$ containing the geometry information is included in the coefficient C_d

 A quick question of comprehension: Which of the following illustrations is right and which is wrong?

