

Sum of all losses along the steamline "Verlustlishe" "head loss"

Pressure loss due to friction
$$\Delta p_{L} = \lambda + \frac{1}{2} V^{2} \Rightarrow \Delta h_{L} = \frac{\Delta p_{L}}{3g} = \lambda + \frac{V^{2}}{2g}$$

Pressure loss due to sudden expansion

$$\Delta P_{L} = S \stackrel{?}{=} V^{2}, S = (1 - \frac{A_{1}}{A_{L}})^{2} \Rightarrow \Delta h_{1} = \frac{\Delta P_{L}}{S_{1}^{2}} = S \stackrel{?}{=} V^{2}$$

zeta Ch.5, p.58

Zeta 2

Pressure loss due to a constriction

$$\Delta P_{L} = S \stackrel{?}{=} V^{2} \qquad S = \left(\frac{1-4}{4}\right)^{2} \Rightarrow \Delta h_{L} = \frac{\Delta P_{L}}{S_{0}^{2}} = S \stackrel{V^{2}}{=} S \stackrel{V^{2}}{$$

Chap5, Supplement (cont'd) 2g (V1-V2) + 5g (P1-P2) + Z1-Z2 = 5 Ahr Sum of all individual losses of all sorts of equipment $= \sum_{z_f} \frac{\sqrt{z}}{z_f}$ basically a parabola V ~ characteristic Systembernhinie for average velocities system characteristic => That is a lot of work to compute! All cletails in pipe system water!

Sharpedge rounded edge

Chap 5 Supplement (ont'd)

Pumps required to provide the volume flow rate. Potentially many pumps, potentially spread over the outier system.

To operate pumps (economically) efficiently, pumps should meet the requirements.

Our example of tadial pumps is just one special single Case.

Typically pumps behave like this

characteristic:

this curve is for a

fixed tpm.

Yes Very V transported

Volume flow rate

pipe end closed

wo opposing pressure

maximum pressure

haximum flow rate

of very small









