

# Multi-scale modeling of powder processes: Bi-directional coupling of population balance models in gPROMS with discrete element models in STAR-CCM+

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<sup>b</sup>*Process Systems Enterprise*

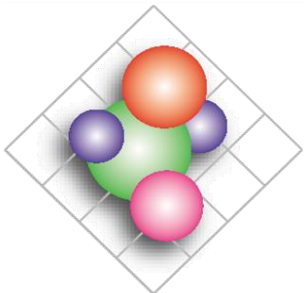
<sup>c</sup>*CD-adapco*



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## **ENGINEERING RESEARCH CENTER FOR STRUCTURED ORGANIC PARTICULATE SYSTEMS**

RUTGERS UNIVERSITY  
PURDUE UNIVERSITY  
NEW JERSEY INSTITUTE OF TECHNOLOGY  
UNIVERSITY OF PUERTO RICO AT MAYAGÜEZ



# Introduction

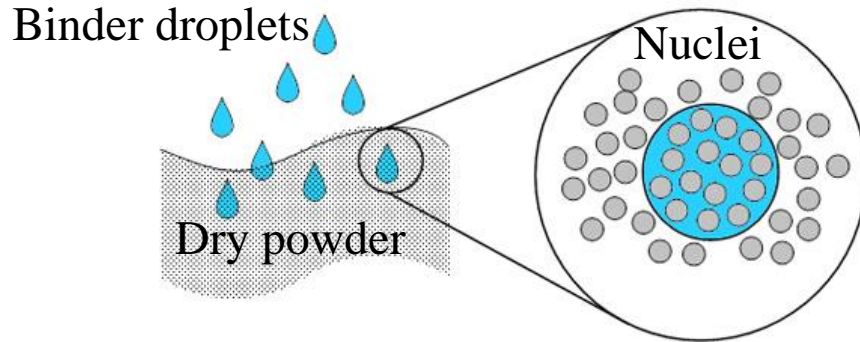
**Objective:** to develop a multi-scale, mechanistic model for wet granulation processes.

- *Process understanding and Quality-by-Design*
- *Existing approaches are insufficient*
- Outline
  - *Background and approach*
  - *Mechanistic PBM development in gPROMS*
  - *PBM-DEM coupling strategy and demonstration*
  - *Summary and future work*
- Ongoing collaboration between Rutgers University (ERC-SOPS), Process Systems Enterprise, and CD-adapco.

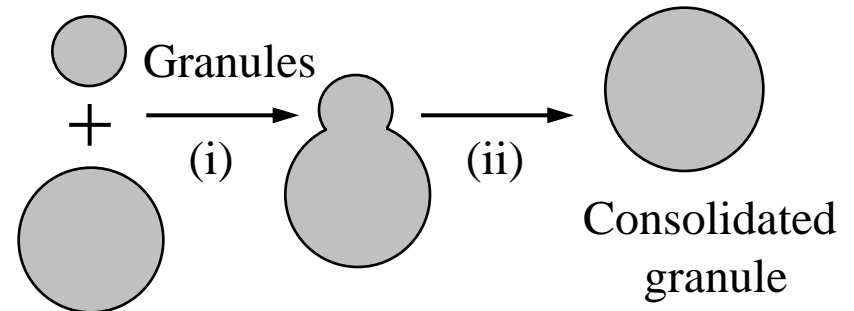


# Wet granulation

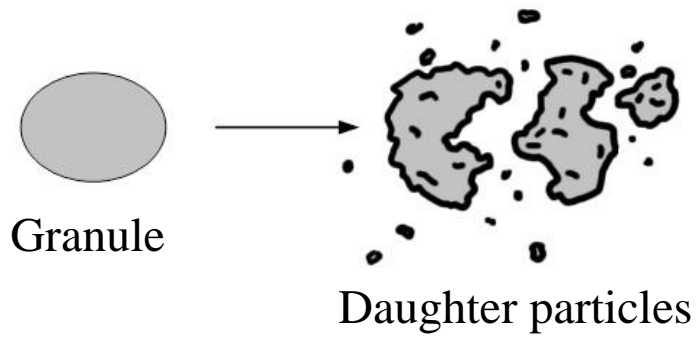
## 1 Wetting & Nucleation



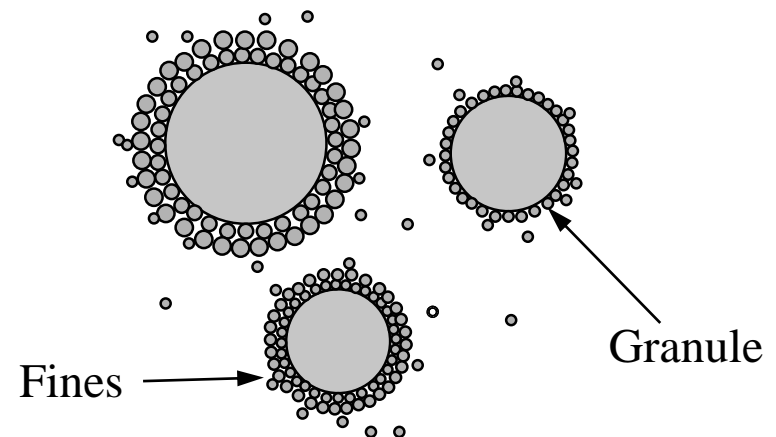
## 2 Aggregation & Consolidation



## 3 Breakage & Attrition



## 4 Layering



(Iveson *et al.*, 2001)



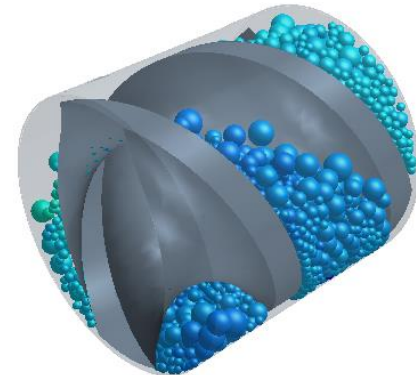
# PBM vs. DEM

## Population balance modeling:

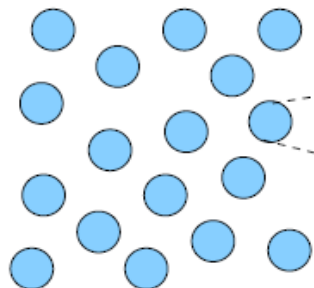
- Tracks number of particles in each size class based on rate expressions for sub-processes
  - *Typically empirical or semi-empirical*
  - *Effects of many process parameters and material properties are not accounted for*
- Spatial information is not inherent
  - *Compartmental PBMs need transfer rate data/assumptions*
  - *Inhomogeneous liquid distributions*
- Many unknown parameters must be estimated with experimental data

## Discrete element modeling:

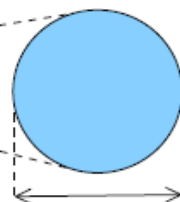
- Tracks each particle in space using laws of physics
- Can output collision, velocity, force, and spatial data at the particle scale.
- Does not inherently simulate rate processes, such as aggregation.
- Computationally intensive



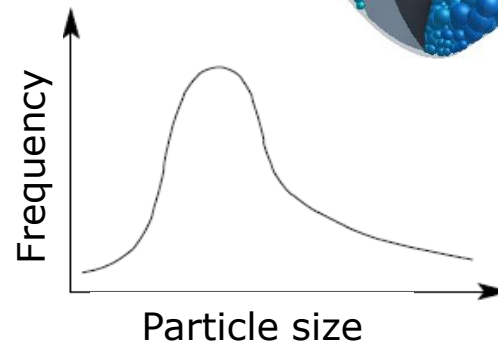
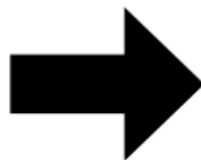
Population of granules



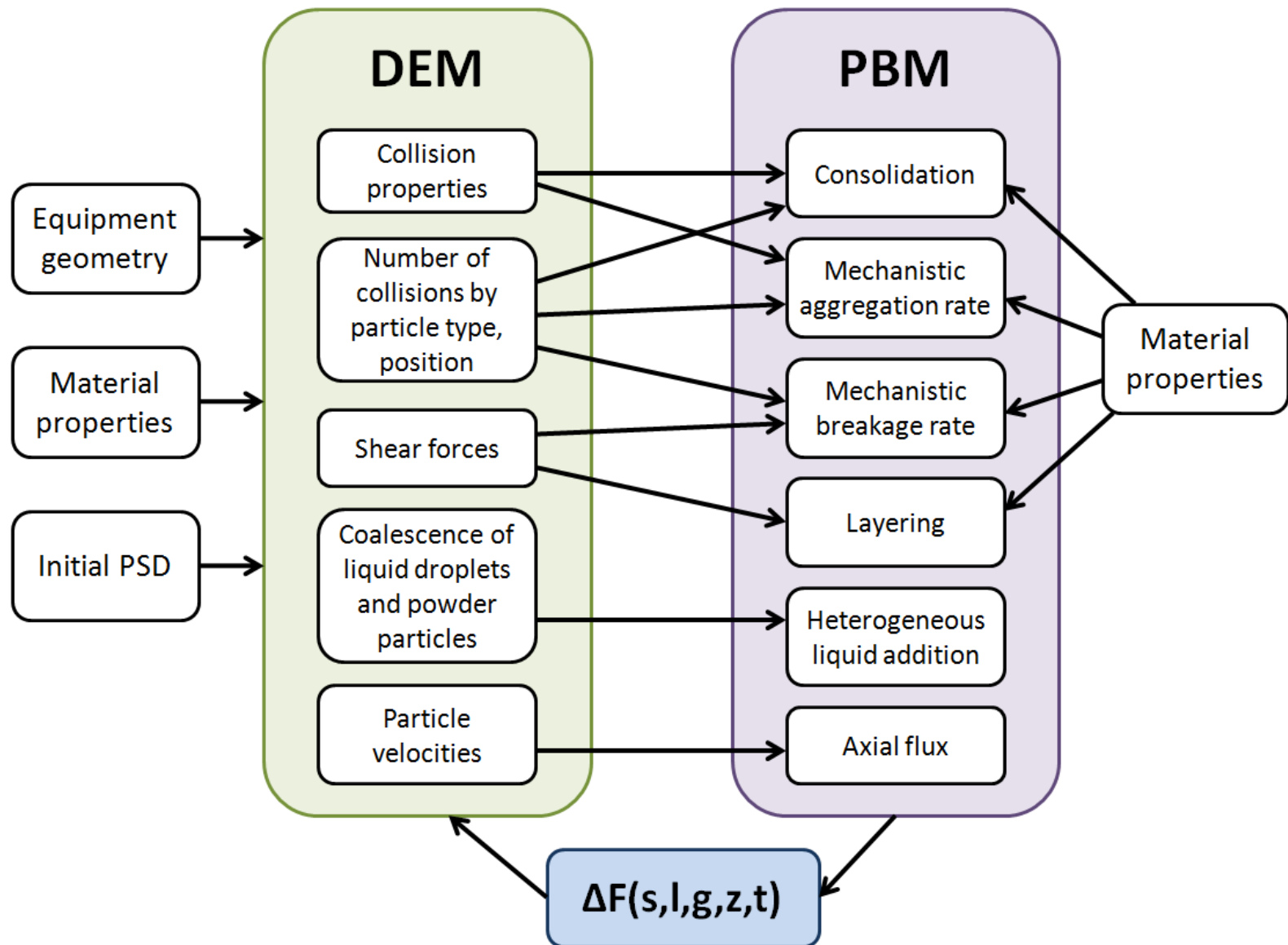
Individual granule



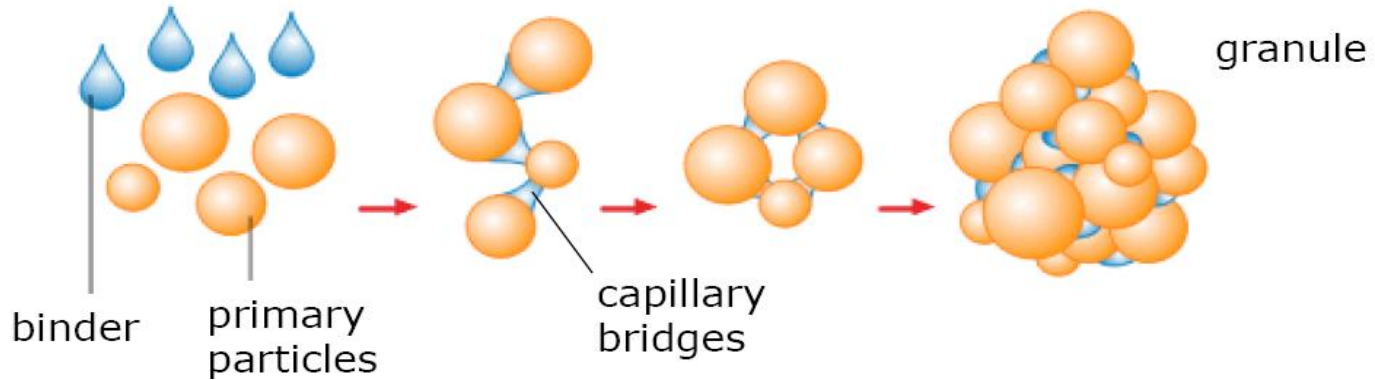
Particle size



# PBM & DEM: a multi-scale approach



# Mechanistic PBM development

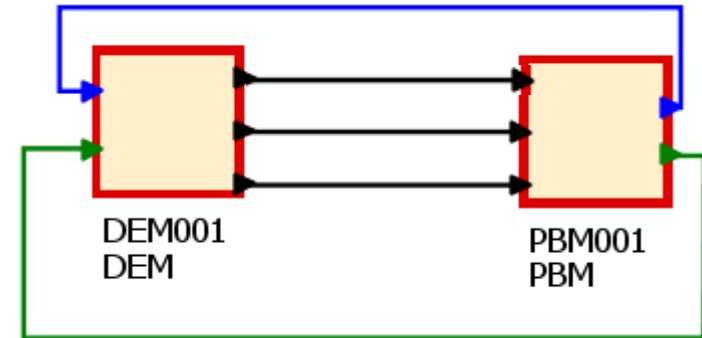


- Objective:
  - *Incorporate mechanistic and spatial details into multi-scale model.*
- Features:
  - *Mechanistic aggregation rate*
  - *Liquid addition*
  - *Porosity and consolidation*
  - *Internal vs. external liquid*
  - *Spatial compartments and particle/liquid transfer*

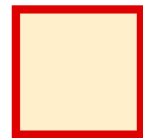


# Detailed gPROMS Model

- UNIT: Population balance model
  - *Number and properties of particles of each volume class in each spatial compartment*
  - *Number of free liquid droplets in each compartment*
  - *Uses DEM results in rate expressions for sub-processes*
- UNIT: Discrete element model
  - *Uses current PBM results to determine collision rates, relative velocities, and transfer between compartments.*
- UNIT: Universal parameters
  - *All user input settings*
- UNIT: Volume domain
  - *Sets volume grid for PBM.*
  - *Calculates cell location for colliding particles.*



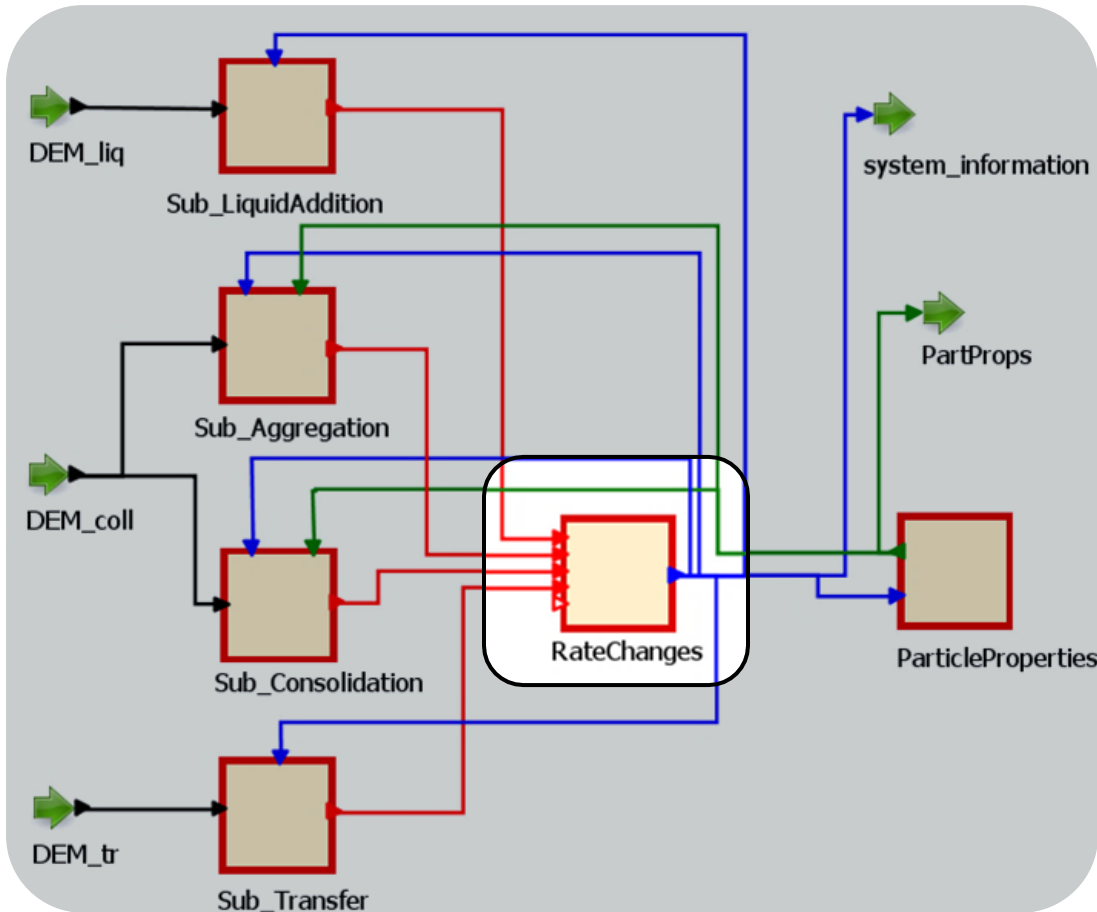
up  
UNIVERSAL\_PARAMETERS



vd  
VolumeDomain



# PBM with lumped parameters



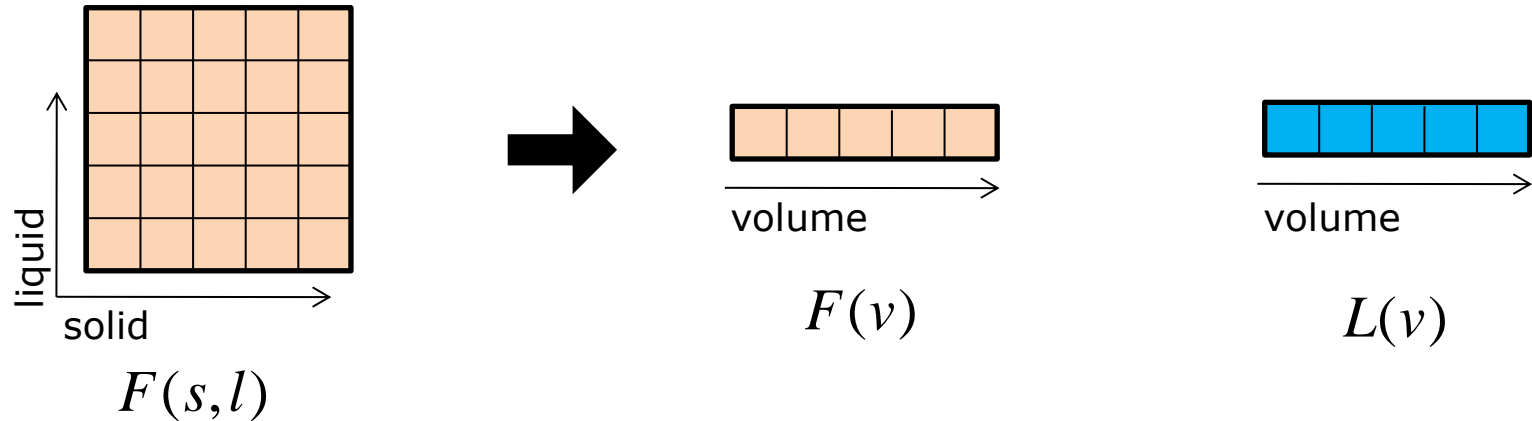
- RateChanges

- *Determines rates of change in each compartment of*
  - *Number of particles in each bin*
  - *Total liquid and pore volumes in each bin*
  - *Free liquid droplets*
- *Net rates of four sub-processes*





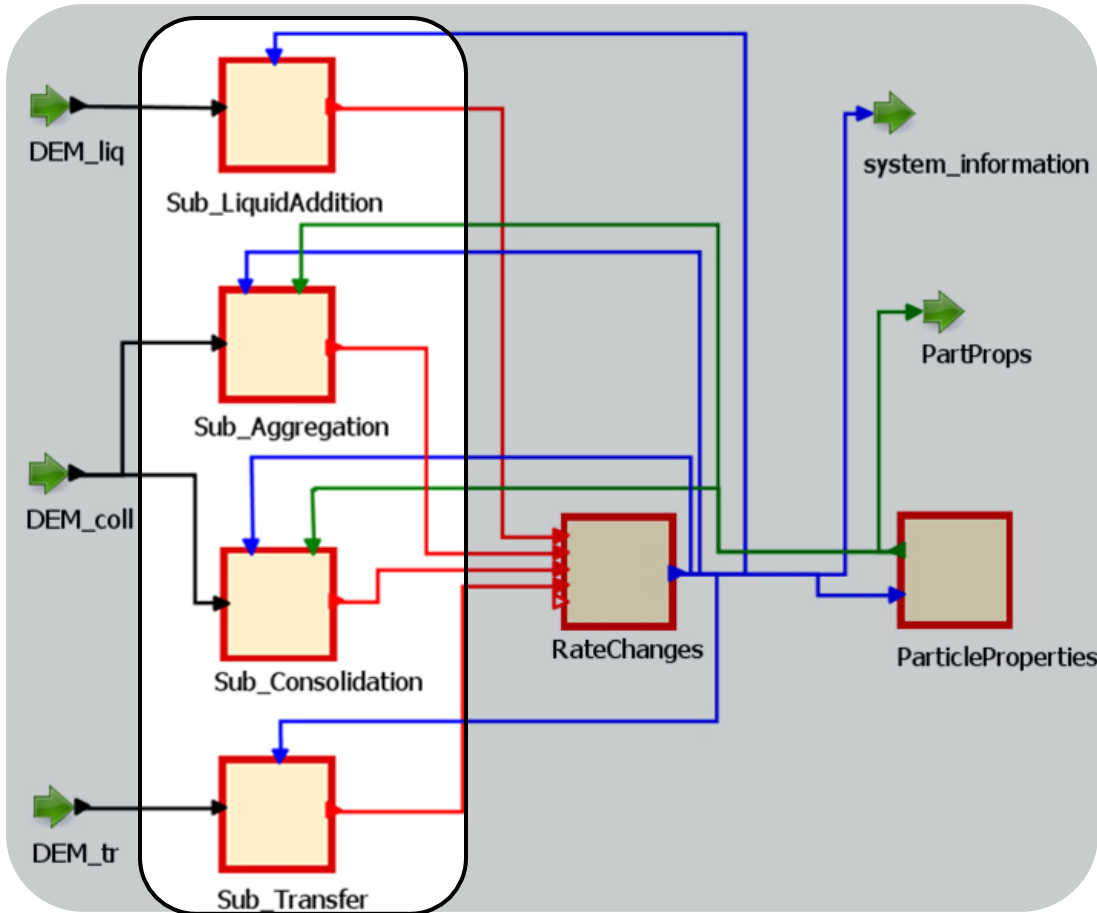
# Lumped parameter approach



- Multi-dimensional PBM tracks simultaneous distributions in multiple attributes (such as size and liquid content)
- Lumped parameter approach reduces dimensionality of distribution
  - *Assumes every particle in the same bin has the same amount of lumped parameter.*
  - *Each lumped parameter creates an additional PBM to track volume of that component in each bin.*
  - *Lumped property can change over time due to aggregation, liquid addition, and other rate processes.*
  - *Lumped property can also depend on particle size.*
  - *Using compartments, spatial inhomogeneities can still exist.*



# Sub-processes



- Sub-processes
  - *Aggregation*
  - *Liquid addition*
  - *Consolidation*
  - *Transfer*



# Mechanistic aggregation rate

$$\beta(v, v') = \overset{\text{Frequency}}{C(v, v')} \overset{\text{Efficiency}}{\Psi(v, v')} \quad \Psi(v, v') = \begin{cases} 1 & \text{for } St \leq St^* \\ 0 & \text{for } St > St^* \end{cases}$$

- Collision rate can be directly provided by DEM
- Collision efficiency depends on Stokes criterion
  - *Critical stokes number a function of thickness of surface liquid and particle surface asperity*

$$St^* = \ln \frac{\lambda_{12}}{h_a} \quad St = \frac{8\tilde{m}u_0}{3\pi\mu\tilde{d}^2}$$

- *Stokes number depends on particle masses and diameters, relative velocity, and binder viscosity*
- *Critical velocity*

$$u_{cr} = \frac{3\pi\mu\tilde{d}^2}{8\tilde{m}} \ln \frac{\lambda_{12}}{h_a}$$

- *Average relative collision velocity provided by DEM*



# Liquid addition

$$\dot{L}(v, x) = f_{drop}(v, x)F(v, x)N_{drop}(x)v_{drop}$$

- 1-D PBM with liquid volume as “lumped” parameter
- Rate of liquid addition to any bin ( $v$ ) and compartment ( $x$ ) is proportional to:
  - *Fractional rate of liquid droplet uptake*
  - *Total particles in that bin and compartment*
  - *Total number of free droplets in compartment*
  - *Droplet volume*

$$f_{drop}(v, x) = \frac{n_{drop}(v, x)}{N_{drop}(x)F(v, x)\Delta t}$$

- Fractional rate of liquid droplet uptake can be estimated using DEM
  - *Create droplets that disappear upon collision with a particle.*
  - *Count these collisions over a time interval, by particle size and compartment.*
  - *Calculate rate, per particle, per droplet, per second.*
- Liquid volume is transferred during other rate processes, such as aggregation.



# Porosity and consolidation

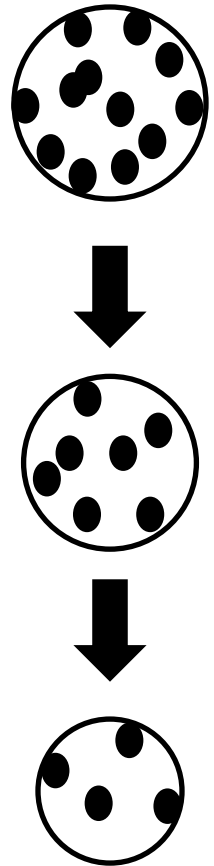
$$\varepsilon(v) = \frac{p(v)}{s + p(v)}$$

- Particle pore volume consists of internal space occupied by air or liquid.
  - *Lumped parameter approach to track pore volume of each particle in each bin and spatial compartment*
  - *As particles collide and deform, porosity decreases*
- Consolidation rate:
  - *Exponential decay in porosity approaching a minimum value*

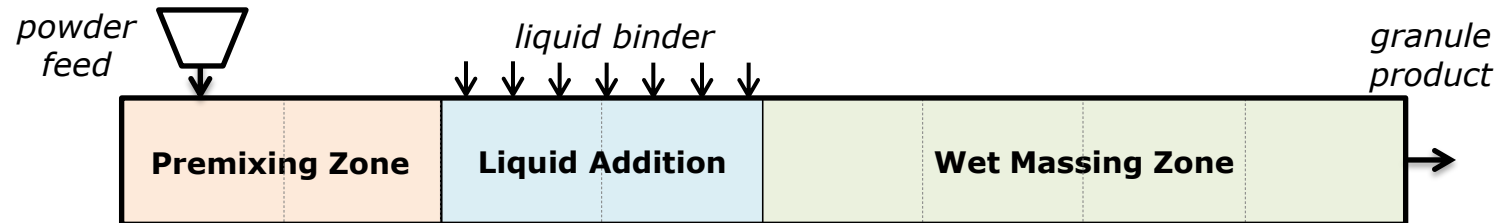
$$\dot{p}_{cons} = -c \left( \frac{1 - \varepsilon_{min}}{1 - \varepsilon} \right) \left( p - \frac{s \varepsilon_{min}}{1 - \varepsilon_{min}} \right)$$

- *Unknown rate coefficient*
- *Collision frequency (total per bin) can be included*

$$c = c_0 \dot{N}_{coll}(v)$$



# Spatial compartments



- PBM solved in each compartment
- Liquid addition region specified by user
- Transfer between compartments
  - *Fraction of particles transferred*
  - *Number of particles crossing boundaries provided by DEM, converted into rate per particle*
  - *Particles transfer can occur into and out of compartments at the same time*
  - *Compartments can be arbitrary size, shape, and position.*
- Strategy needed to define compartments

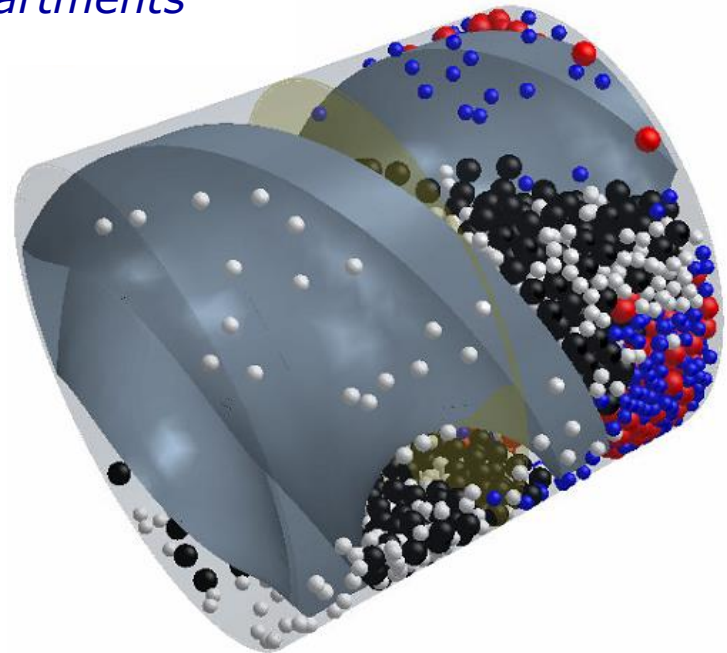
$$\frac{dF(v, x)}{dt} = \mathfrak{R}_{agg, net}(v, x) - \sum_{x'} F(v, x) \alpha(v, x, x') + \sum_{x'} F(v, x') \alpha(v, x', x)$$



# Spatial compartments

- Compartments
  - *Create compartments in STAR-CCM+*
  - *Track particle transfer between compartments*

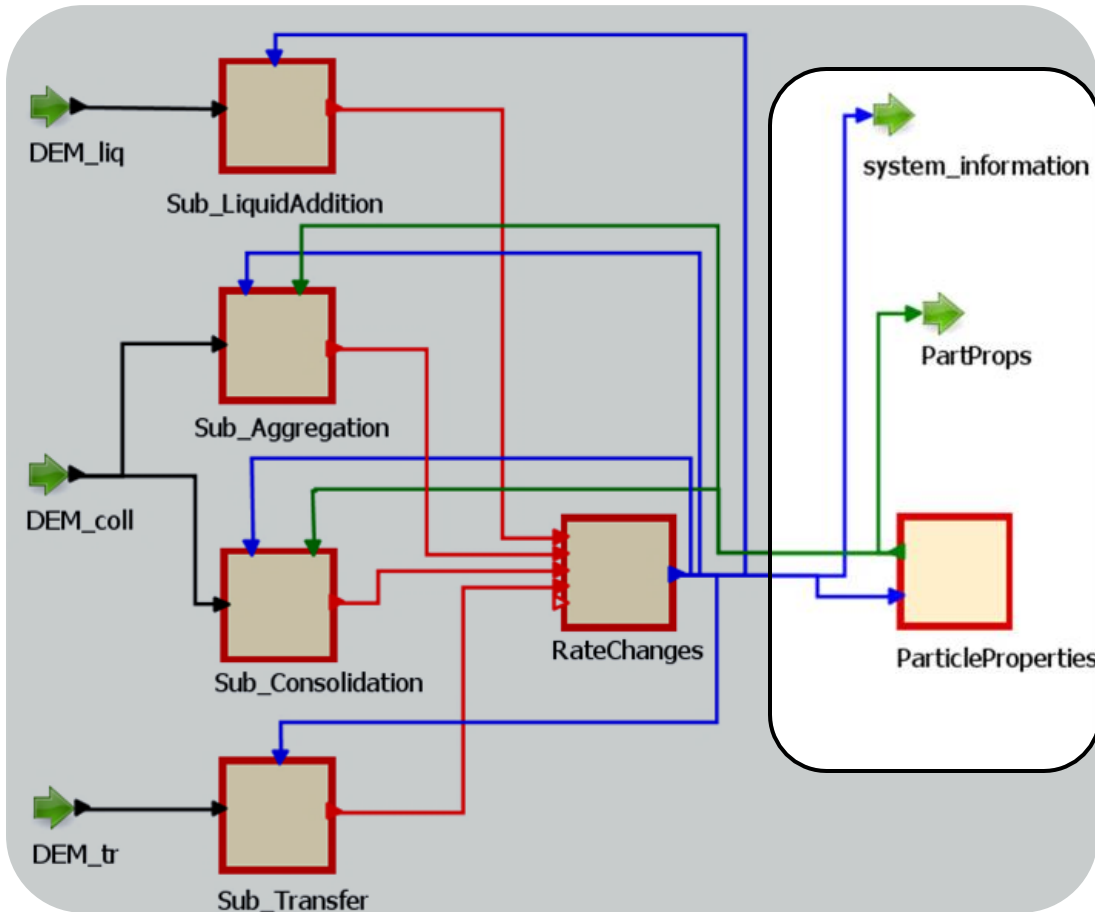
Size	Initial Region	Color
Small	Left	White
Small	Right	Blue
Large	Left	Black
Large	Right	Red



- End goal for user:
  - *Define compartments as regions of arbitrary size and shape in STAR-CCM+*
  - *Specify total the number of regions in gPROMS*
  - *Turn on or off sub-processes in each region (liquid addition, inflow/outflow)*



# Particle and bulk properties



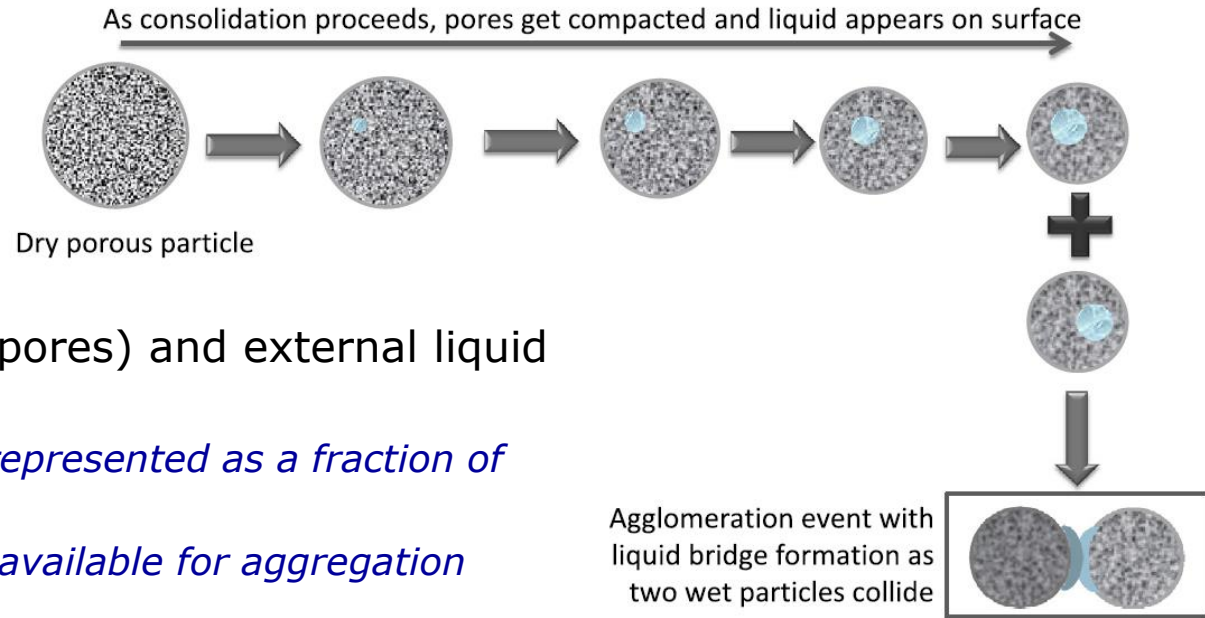
- Main granulation model
  - *Mass and volume balances*
  - *Bulk properties in each compartment and overall (d<sub>4,3</sub>, mass distributions)*
- Particle Properties model
  - *Per-particle volumes in each bin, compartment (pore, liquid)*
  - *Internal and external liquid*
  - *Total volume and diameter, wet and dry masses*
  - *Aggregation information (surface asperity, surface liquid thickness, critical Stokes number)*



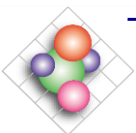


# Internal and external liquid

- Total liquid volume, per particle, calculated using lumped parameter
- Distinction between internal liquid (trapped in pores) and external liquid (on the surface)
  - *Maximum internal liquid represented as a fraction of the total pore volume*
  - *Remainder is on surface, available for aggregation*
- As porosity decreases, surface liquid increases, resulting in greater aggregation rates
- Drop penetration time
  - *Based on Washburn equation for capillary flow*
  - *Droplet volume, effective porosity and pore radius, binder viscosity, surface tension, and contact angle*
  - *Order of magnitude for small amounts of liquid:  $1e-4$  s*

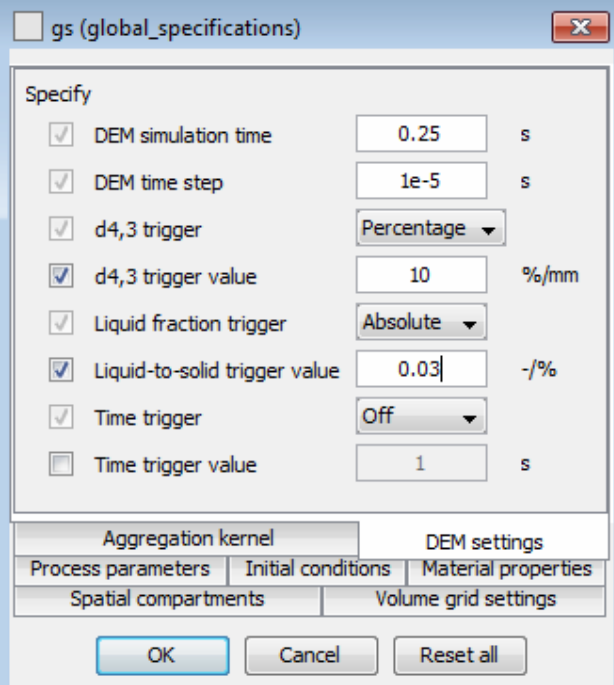


Chaudhury, et al. (2014)  
Chemical Engineering  
Science



# Summary of model

- User inputs
  - *Initial conditions*
  - *Material properties (including DEM parameters)*
  - *Process parameters (batch time, L/S ratio, screw speed)*
  - *Model settings (compartments, volume grid, kernel selection)*
  - *DEM settings (simulation time, time step, trigger)*
- From gPROMS to DEM
  - *PSD in each compartment*
  - *Particle properties*
  - *Liquid addition details*
  - *Process parameters*
  - *DEM settings*
- From DEM to gPROMS
  - *Collision rate between bins*
  - *Average relative velocity of collisions*
  - *Collision rate for each bin*
  - *Liquid uptake rate*
  - *Particle transfer rate between compartments*



gs (global\_specifications)

Specify

- ☒ DEM simulation time: 0.25 s
- ☒ DEM time step: 1e-5 s
- ☒ d4,3 trigger: Percentage
- ☒ d4,3 trigger value: 10 %/mm
- ☒ Liquid fraction trigger: Absolute
- ☒ Liquid-to-solid trigger value: 0.03 -/%
- ☒ Time trigger: Off
- ☐ Time trigger value: 1 s

Aggregation kernel      DEM settings

Process parameters    Initial conditions    Material properties

Spatial compartments    Volume grid settings

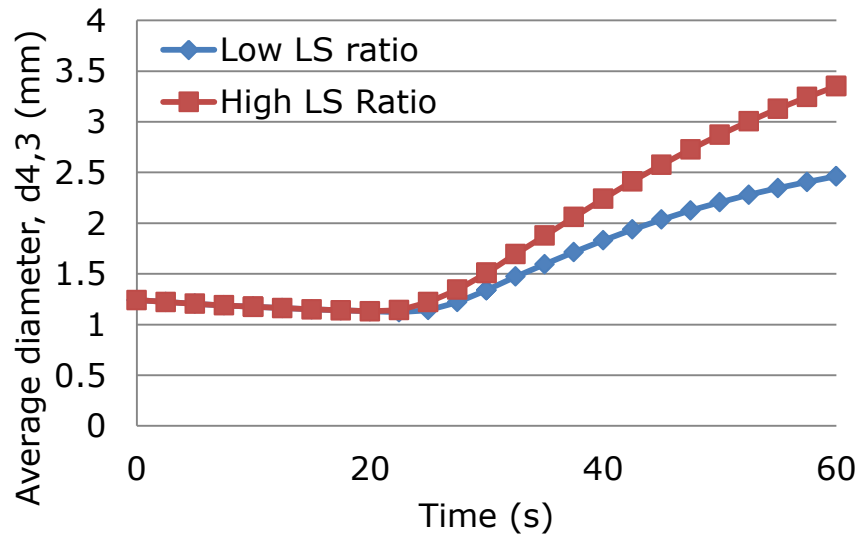
OK    Cancel    Reset all



# Results of uncoupled gPROMS model

- Higher liquid-to-solid ratio results in larger granules.
  - High: 0.35
  - Low: 0.3

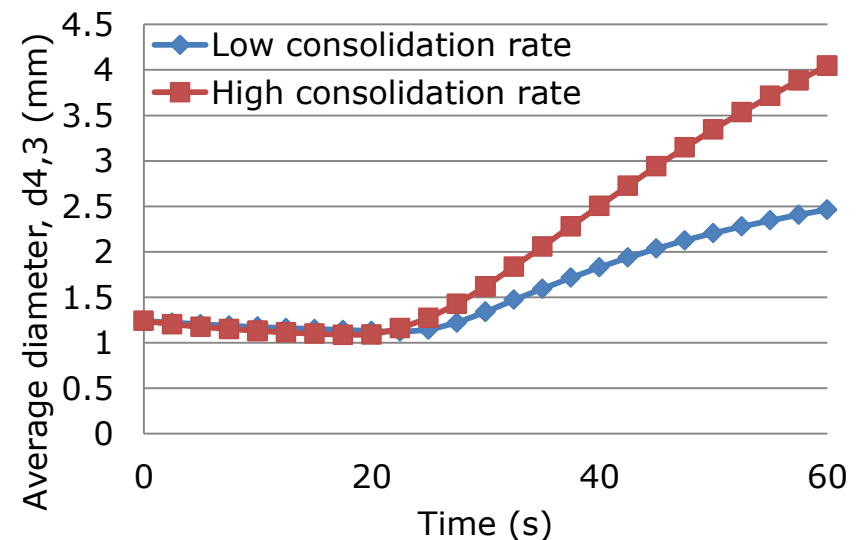
Average diameter vs. time



- Higher consolidation rate results in faster aggregation.

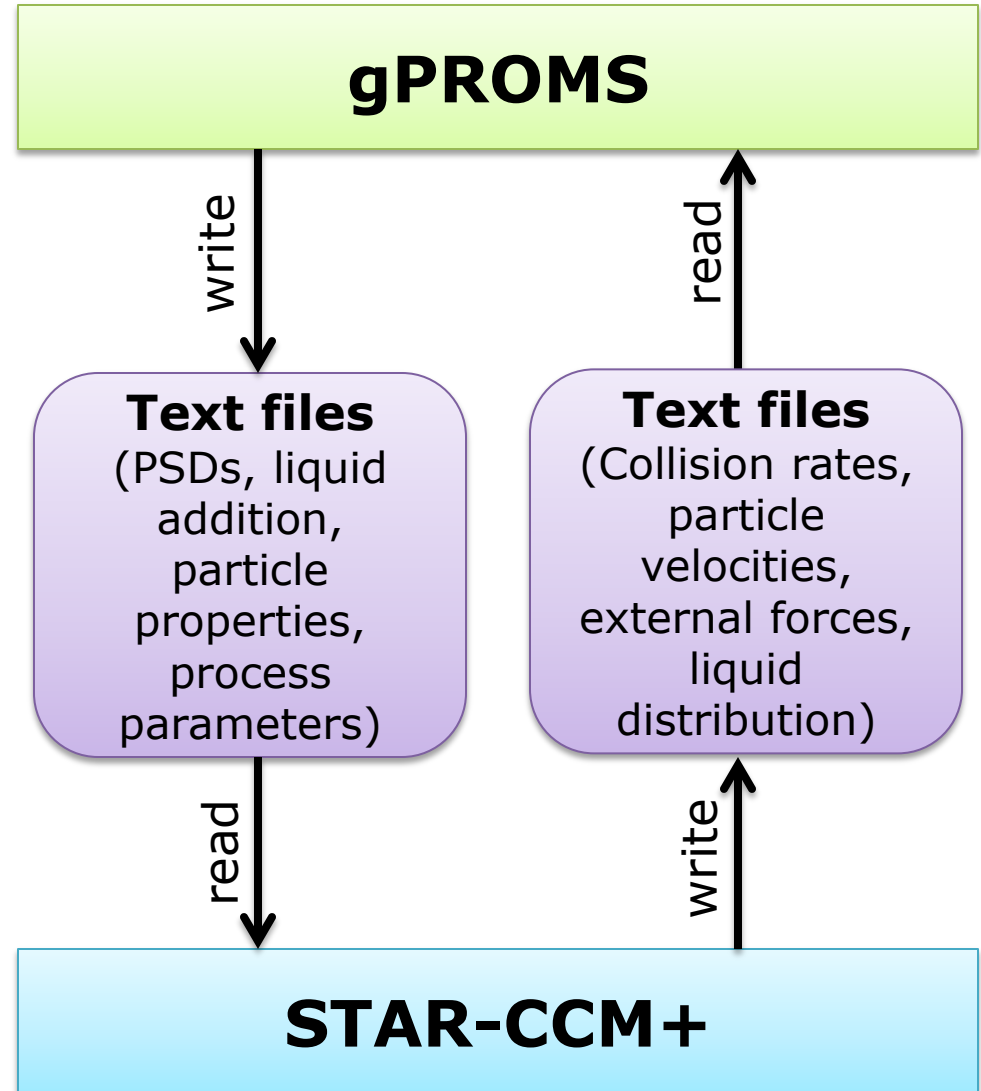
Consolidation rate constant	Percent surface liquid
5e-4/s	38%
1e-3/s	62%

Average diameter vs. time

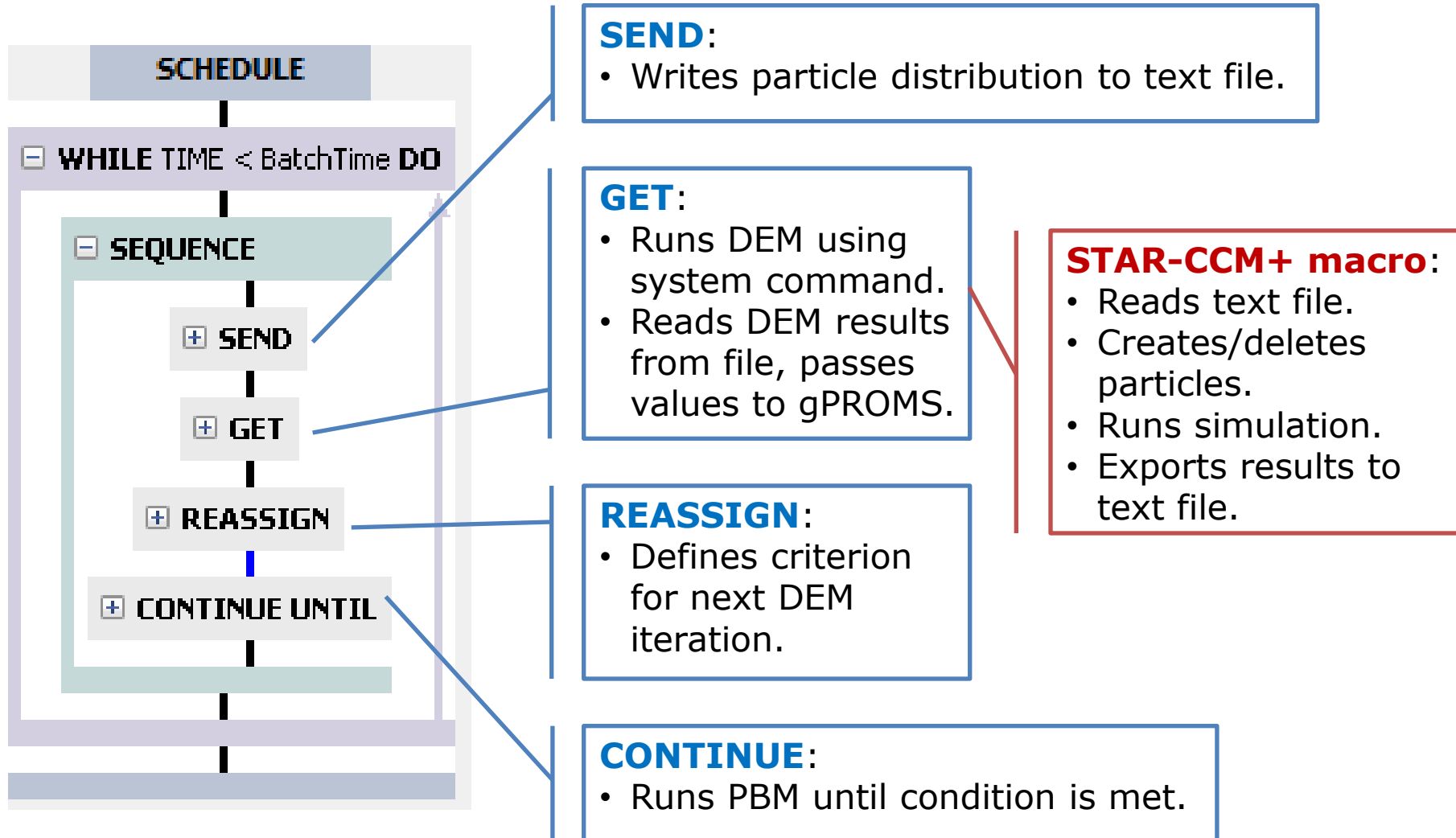


# Coupling with STAR-CCM+: approach

- gPROMS
  - Population balance, rate changes
  - Controls process parameters and problem set up (number and sizes of particles, liquid addition rates, rotational speeds, etc.)
- STAR-CCM+
  - Collision rates and forces
  - Flux and spatial behavior
  - Liquid addition
- Data transfer
  - Text files
  - DEM simulations triggered by sufficient changes to key variables



# Schedule and FPI



# gPROMS/STAR-CCM+ simulation workflow

1

- Create simulation file in **STAR-CCM+**.
  - *Define geometry (Future: define compartments).*
  - *Set model physics to turn on DEM.*
  - *Specify movement of parts (impeller or screw).*
  - *Create scenes to output images.*

2

- Specify parameters in **gPROMS** model.
  - *DEM settings (time, time step, trigger)*
  - *Volume grid size and bounds*
  - *Initial PSD, porosity, and liquid content*
  - *Process parameters and material properties*

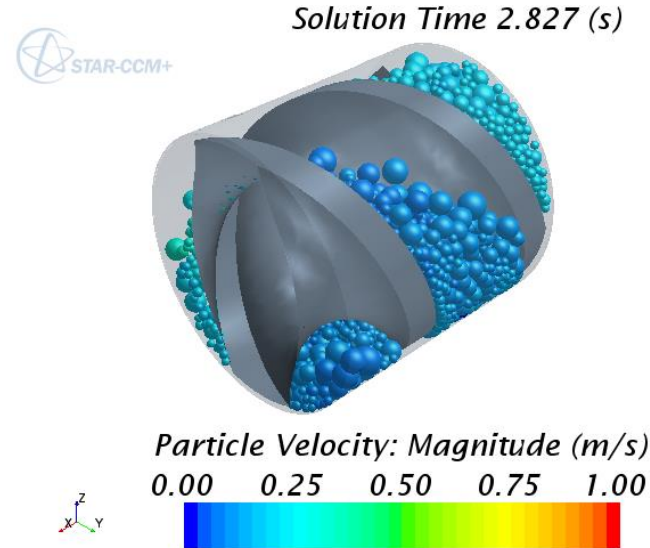
3

- Run process with **FPI** and appropriate **SCHEDULE**.
  - *Grid size and particle/collision properties are automatically read and transferred to STAR-CCM+.*
  - *STAR-CCM+ simulation is modified and executed by gPROMS during GET command.*



# gPROMS/STAR-CCM+ coupling

- Mechanistic model with one spatial compartment, only data transferred from STAR-CCM+ is collision rate.
- 20 bins (total volume)
  - *0.3-2.2 mm in diameter*
  - *Lumped solid/pore, liquid*
  - *Internal and external liquid*
  - *$L/S=0.3$ , added from 2-12 seconds*
- STAR-CCM+ called when  $d_{4,3}$  changes by more than 10% or liquid-to-solid ratio changes by more than 0.1.
- 60 s simulation
  - *Total simulation time: 4 hrs*
  - *CPU time: 18 s*

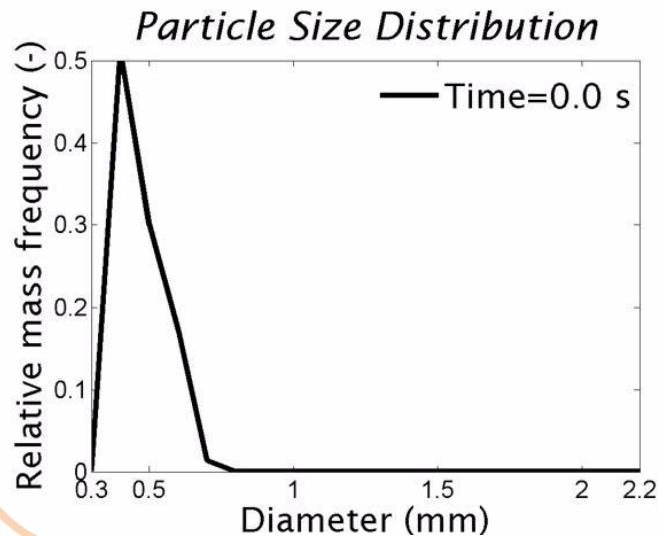
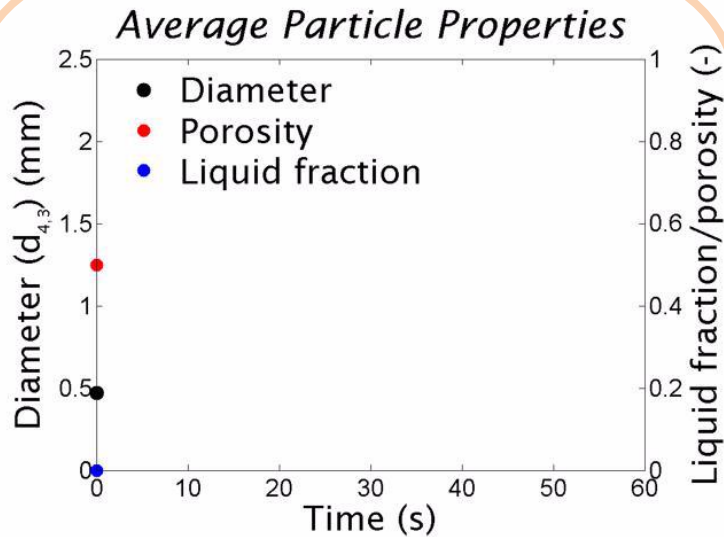


```
Execution Output (Granulation_20140313_160518)
Show messages to level 2 and update infrequently Update
STDOUT:
STDOUT: Updating interface Interface 1 between ThreadSpace:InnerCylinderSurface and Wal
STDOUT: Interface 1: Created 2097 intersection faces in 0.016s (100% of master area, 10
STDOUT: Calculating grid flux in region Volume Mesh:WallSpace
STDOUT: Calculating grid flux in region Volume Mesh:ThreadSpace
STDOUT: 358 2.558134e-01 4.822801e-02 2.823562e-01 2.607889e-01
STDOUT: TimeStep 358: Time 3.580000e-01
STDOUT: Stopping criterion Maximum Inner Iterations satisfied.
STDOUT: Resetting imprinted interface Interface 1
STDOUT: Removing 811 vertices from region ThreadSpace
STDOUT: Removing 1910 vertices from region WallSpace
STDOUT:
STDOUT: Updating interface Interface 1 between ThreadSpace:InnerCylinderSurface and Wal
STDOUT: Interface 1: Created 2010 intersection faces in 0.016s (100% of master area, 10
STDOUT: Calculating grid flux in region Volume Mesh:WallSpace
STDOUT: Calculating grid flux in region Volume Mesh:ThreadSpace
```

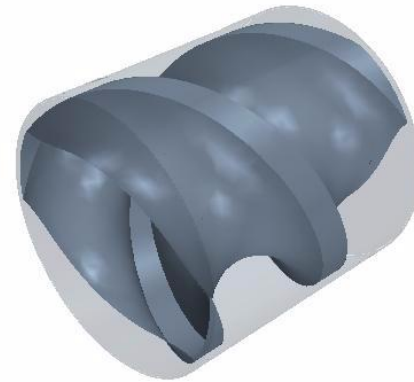
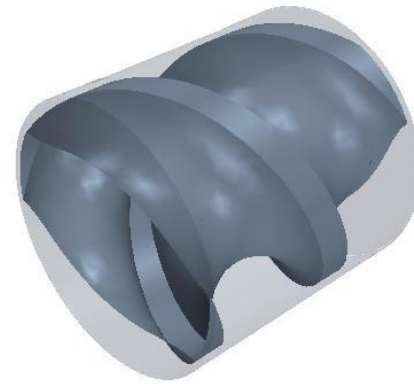
Output Topology: Granulation Stream tables: Granulation Properties

# gPROMS/STAR-CCM+ results

gPROMS



*Solution Time 0.001 (s)*



STAR-CCM+



# Summary and future work

- Modeling granulation is a multi-scale problem
  - *Developed a detailed, **mechanistic PBM** for wet granulation processes in gPROMS.*
  - *Established and demonstrated a **bi-directional coupling** technique with STAR-CCM+.*
- Ongoing and future work
  - *Expand **data transfer** from STAR-CCM+ to gPROMS (liquid addition, spatial compartments, relative velocity)*
  - *Include **additional rate processes**, such as breakage, nucleation, and layering.*
  - *Develop efficient solution techniques for **multi-dimensional PBMs** in gPROMS.*
  - ***Test and validate** multi-scale model.*



# Acknowledgements

- National Science Foundation Engineering Research Center for Structured Organic Particulate Systems (ERC-SOPS)
- Process Systems Enterprise for providing this internship opportunity.
- Jim Litster (Purdue) for his useful feedback.
- CD-adapco for their support and guidance.

Thank you.



# BACKUP SLIDES



# Customizing the DEM simulation

- Java macro reads from three text files, modifies existing simulation
  - General **simulation parameters**: total simulation time, DEM time step, number of bins, rotational speed
  - **Bin information**: Number of particles in each bin and their properties (size, Poisson ratio, density, Young's modulus)
  - **Collision information**: Contact model parameters for each bin with each other bin and the walls (coefficients of restitution, friction)

Bin Number	Diameter (mm)	Count	Density (kg/m <sup>3</sup> )	Poisson's Ratio	Young's Modulus (MPa)
1	0.4	500	2000	0.2	0.2
2	0.5	400	1750	0.2	0.2
3	0.6	300	1500	0.2	0.2
4	0.7	200	1250	0.2	0.2
5	0.8	100	1000	0.2	0.2
6	0.9	50	1000	0.2	0.2
7	1	25	1000	0.2	0.2



# Execution of Java macro

- Before simulation:
  - Changes **simulation parameters**.
  - Creates **DEM phase** (particle type) for each bin.
  - Defines **interactions** between each pair of phases.
  - Checks if particles need to be removed (when  $F$  decreases), and if so, **removes particles**.
  - Creates an **injector** for each bin.
  - Creates reports and monitors for key information we want to **output**.
- Runs simulation.
- After simulation:
  - Exports contact data over time.
  - Parses file to approximate **number of collisions, relative velocity**.
  - Creates **text file** with number of collisions between each pair of bins, number of particles in those bins, and average collision velocity.

