

Process simulation of complex metallurgical Systems

Advanced Process Modelling Forum 2013

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“Process simulation of complex metallurgical systems”

Bernd Weiss/Ironmaking Technology
APM Forum 2013

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Portfolio

- Part of Siemens Industry Sector
- Technology, mechanical engineering, automation and electrical engineering for metallurgical plants in the areas of
 - New plants
 - Modernisation
 - Service

Mining



Blast furnaces



Smelting/Direct reduction



Steel plants



Mini mills



Continuous casting



Hot/Plate mills



Cold band



Long rolling



Metallurgical services



Electrics Automation



Ironmaking processes

- Business segment of business unit Siemens VAI Metals Technologies
- Competence for
 - Agglomeration, pelletising, sinter technologies
 - Conventional iron making
 - Blast furnace
 - Alternative iron making
 - Corex®
 - Finex®
 - Midrex®/DR
 - Finmet®

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Ironmaking processes

Raw Materials for ironmaking



Fine ore



Concentrate



Coal > Coke



Lump ore



Fine ore

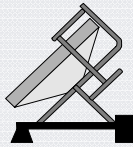


Pellets

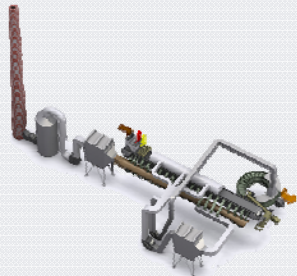


Sinter

Preparation



Pellet Plant



Sinter Plant

Ironmaking Processes



Blast
Furnaces



FINEX®



COREX®



DR Plants/
MIDREX®

Products



Hot Metal



Hot Briquetted Iron



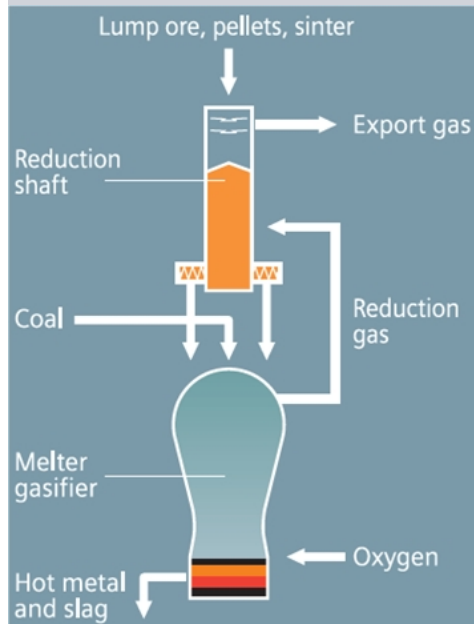
Direct Reduced Iron

Steelmaking
Market

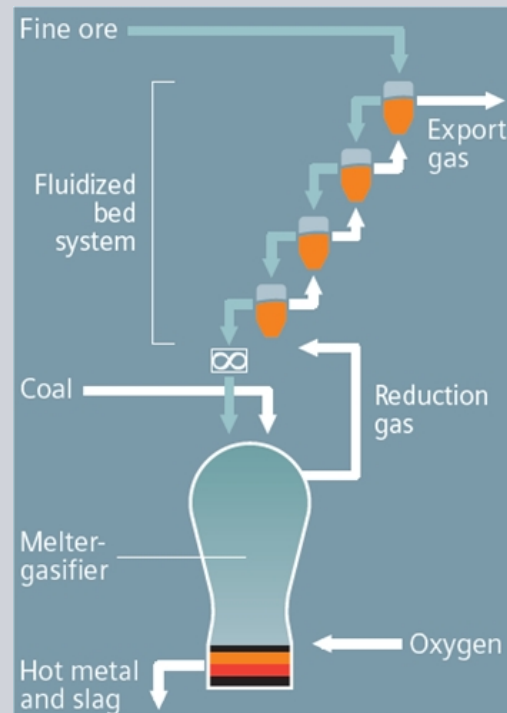
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Ironmaking processes

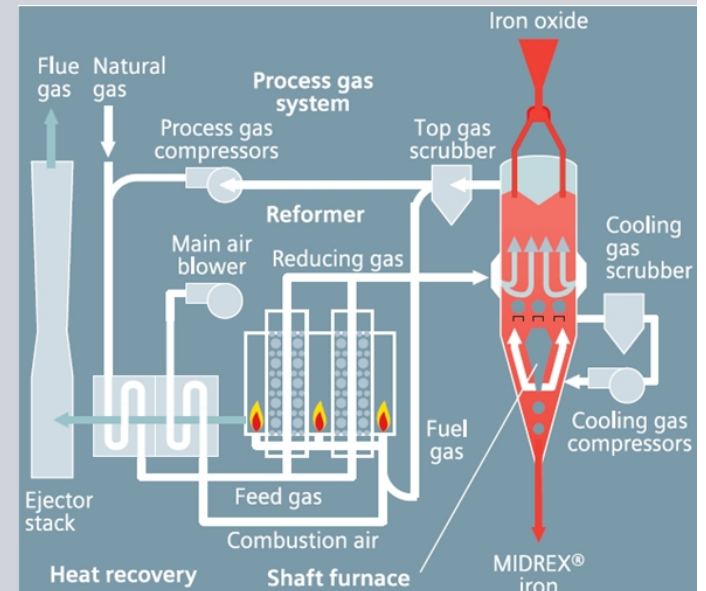
- Processes besides conventional blast furnace iron making route:



Corex®



Finex®

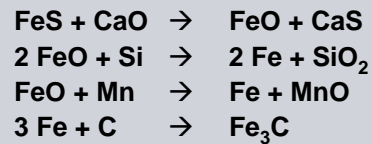


Midrex®

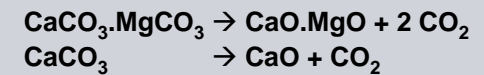
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Chemical challenge - melter gasifier

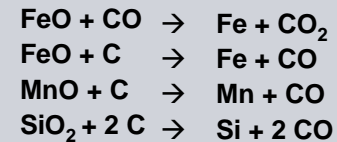
• Metallurgy



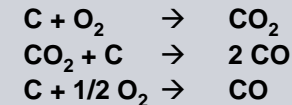
• Calcination



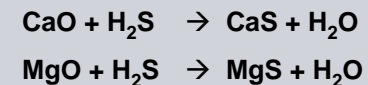
• Reduction



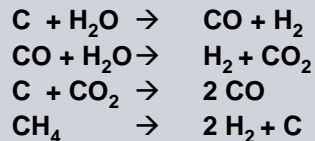
• Gasification



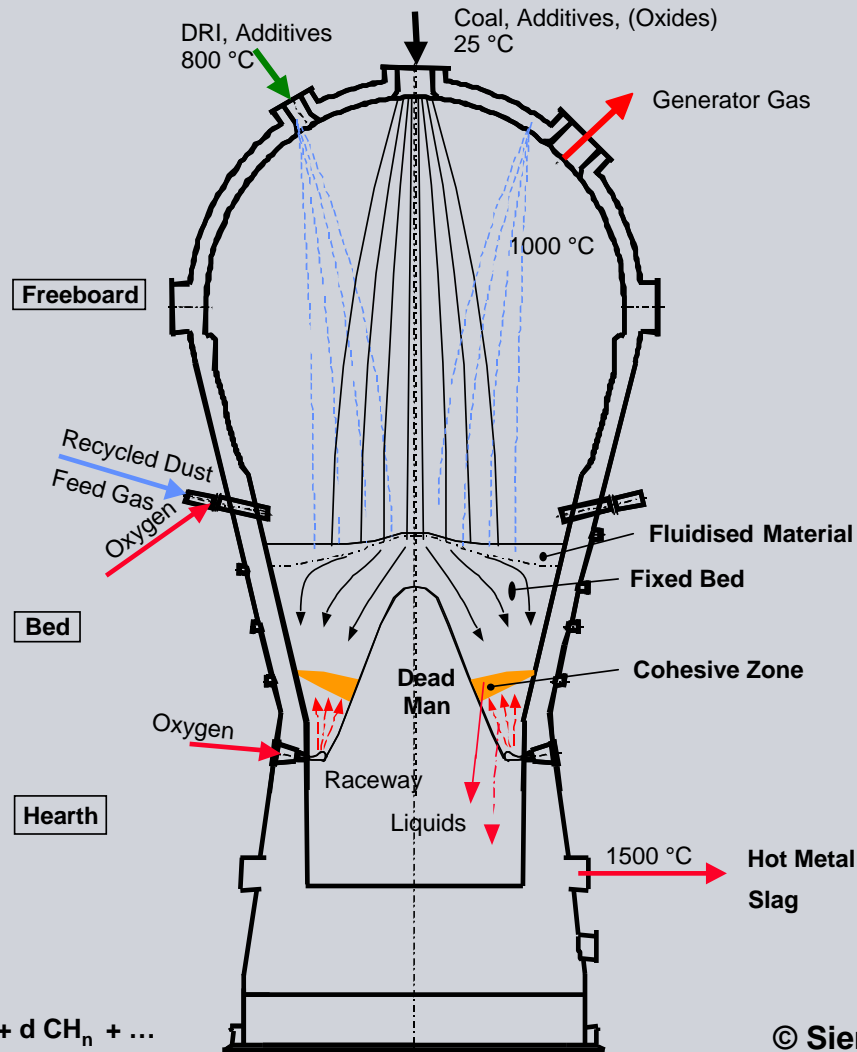
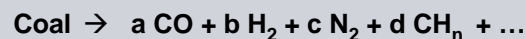
• Sulphur



• Gas Reactions



• Coal Pyrolysis

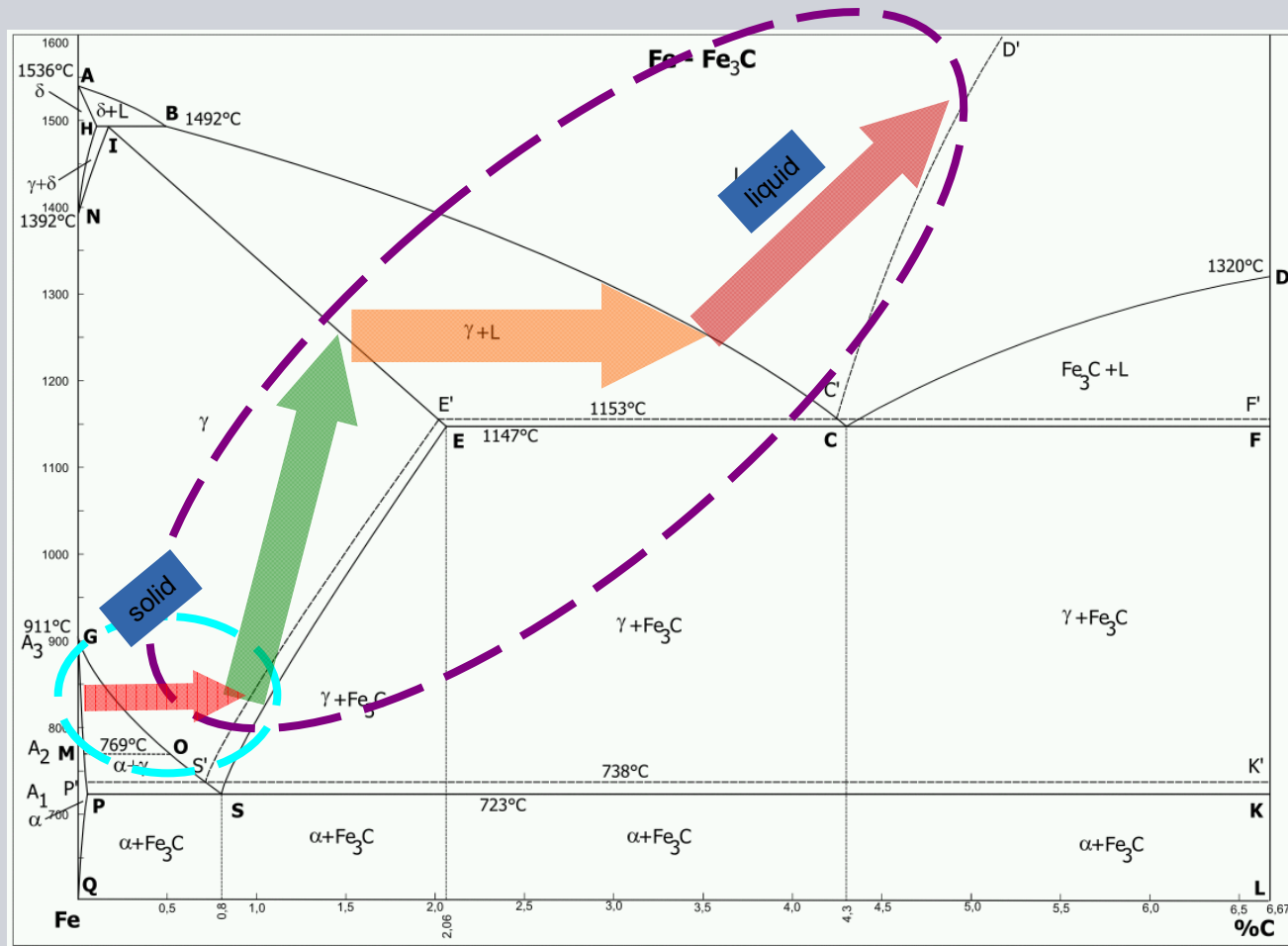


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Chemical challenge

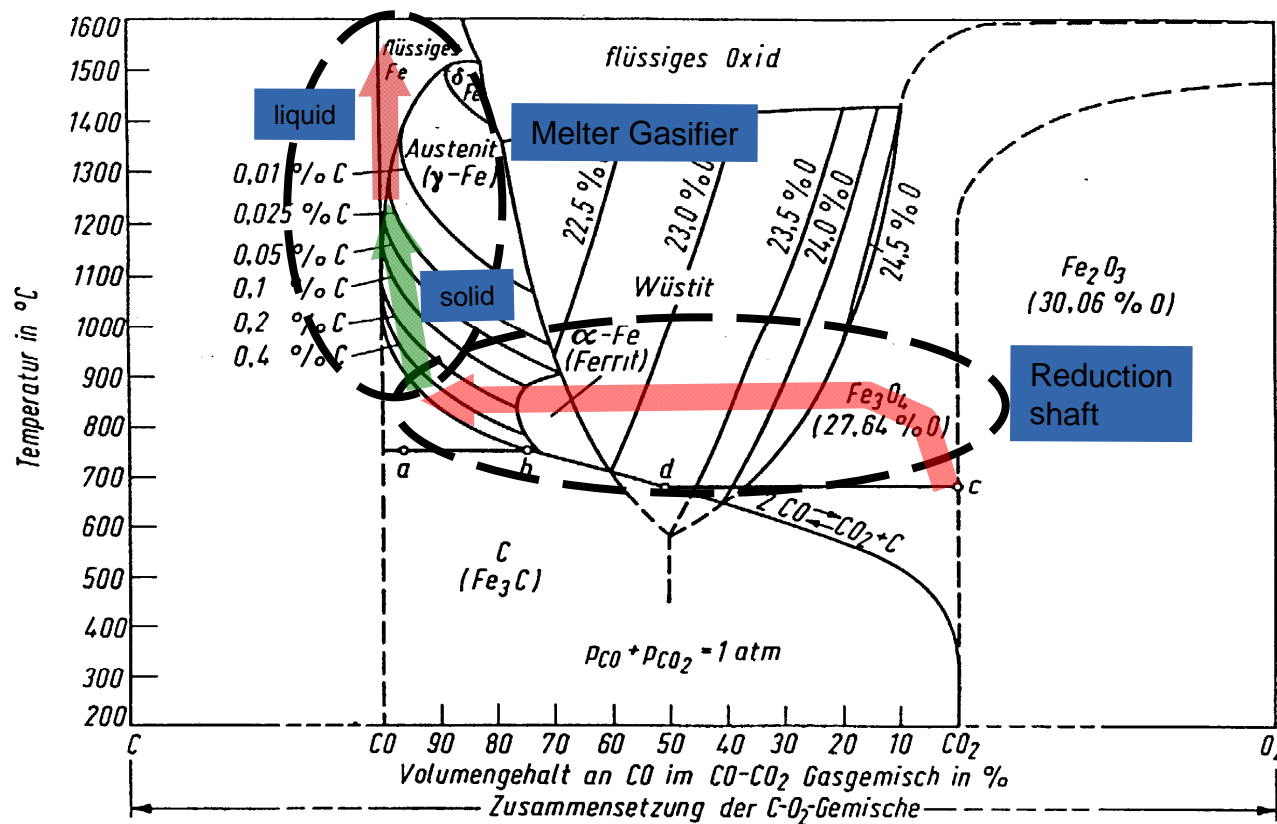
Melter Gasifier

Reduction Shaft



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Chemical challenge



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Approach to gPROMS

Motivation

- Increased complexity of process development
- Increased flexibility for process setup on customer demands
- Additionally:
 - No standardized thermodynamics, flow sheeting

Approach to gPROMS

- Evaluations on state of the art in process simulation
 - Internal, external, guided with PSE
- Outcome: no standard process simulation tool suitable
 - Lack of thermodynamics
 - Unit operations
- Decision for gPROMS due to its flexibility, customizability and functionality

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Development approach

Two parallel implementations

- Low fidelity approach
 - Based on existing internal routines
 - Substitution of MS Excel implementations
 - Utilisation for “every day” project work
 - Global aim - implementation of overall iron and steelmaking routes
 - Conventional (sinterplant, pelletising plant, coking plant, blast furnace, converter)
 - Alternative (sinterplant, pelletising plant, Corex, Finex, converter)
- High fidelity approach
 - Only for selected unit operations
 - Extended thermodynamic routines by using an interface to ChemApp
 - Utilisation for scientific investigations

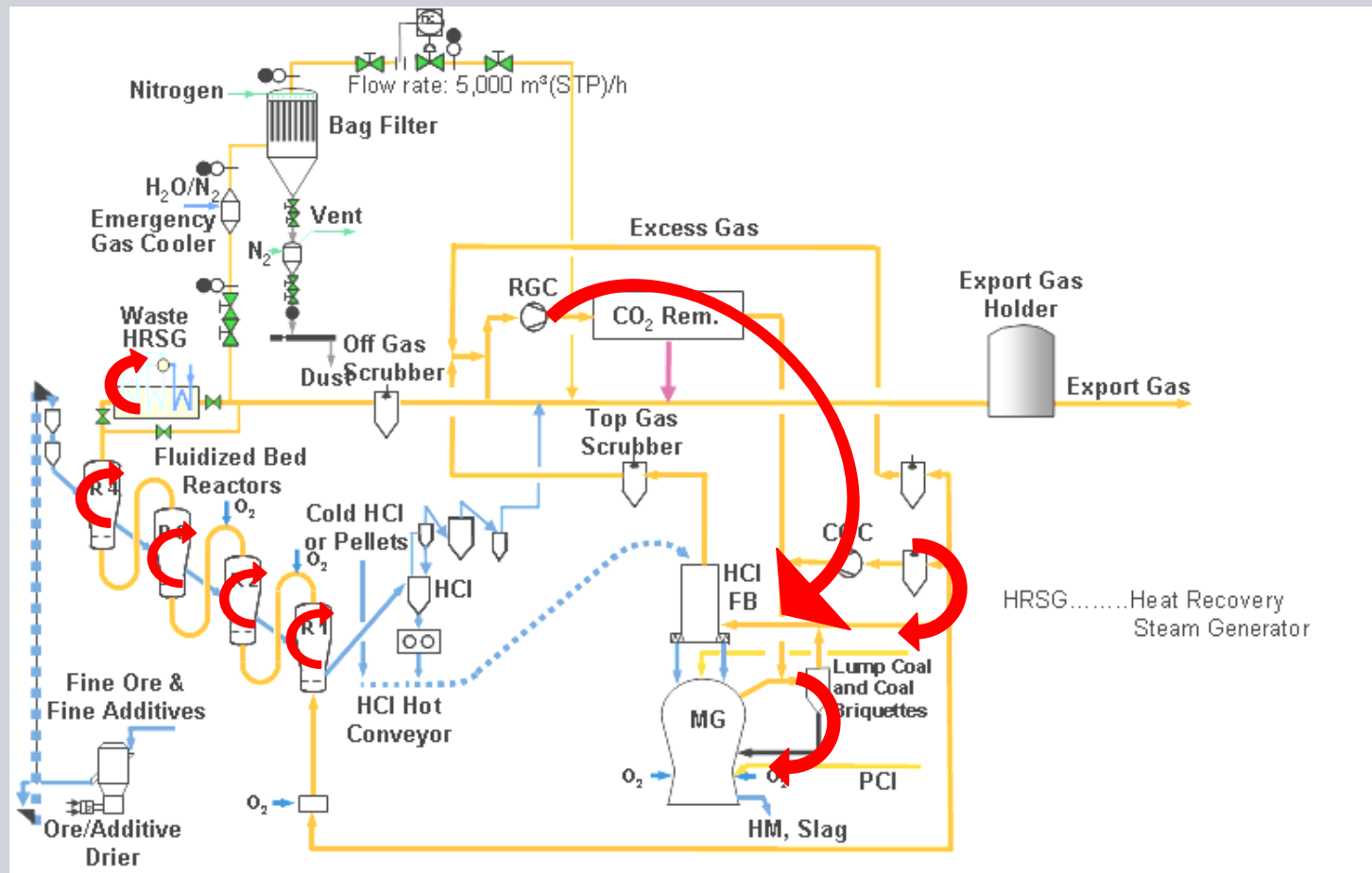
Low Fidelity Approach

- Full capable metallurgic unit operation library building large flow sheets
- Based on conversion and distribution coefficient calculations as complex chemistry was not available
- Utilization of:
 - FO look up table for enthalpy calculations (based on HSC Chemistry 6.0)
 - IAPWS95 for steam parameters
 - Multiflash gibbs equilibrium for combustion calculations
 - MS Excel interface for results export
 - Linkage to MS Access ore/coal data base for raw material data import
- Challenges:
 - Process abstraction => MS Excel tool move to flow sheeting tool
 - Initialisation procedures (recycles, non linear equation systems)

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Low Fidelity Approach

Initialisation - Recycles



Low Fidelity Approach - Status

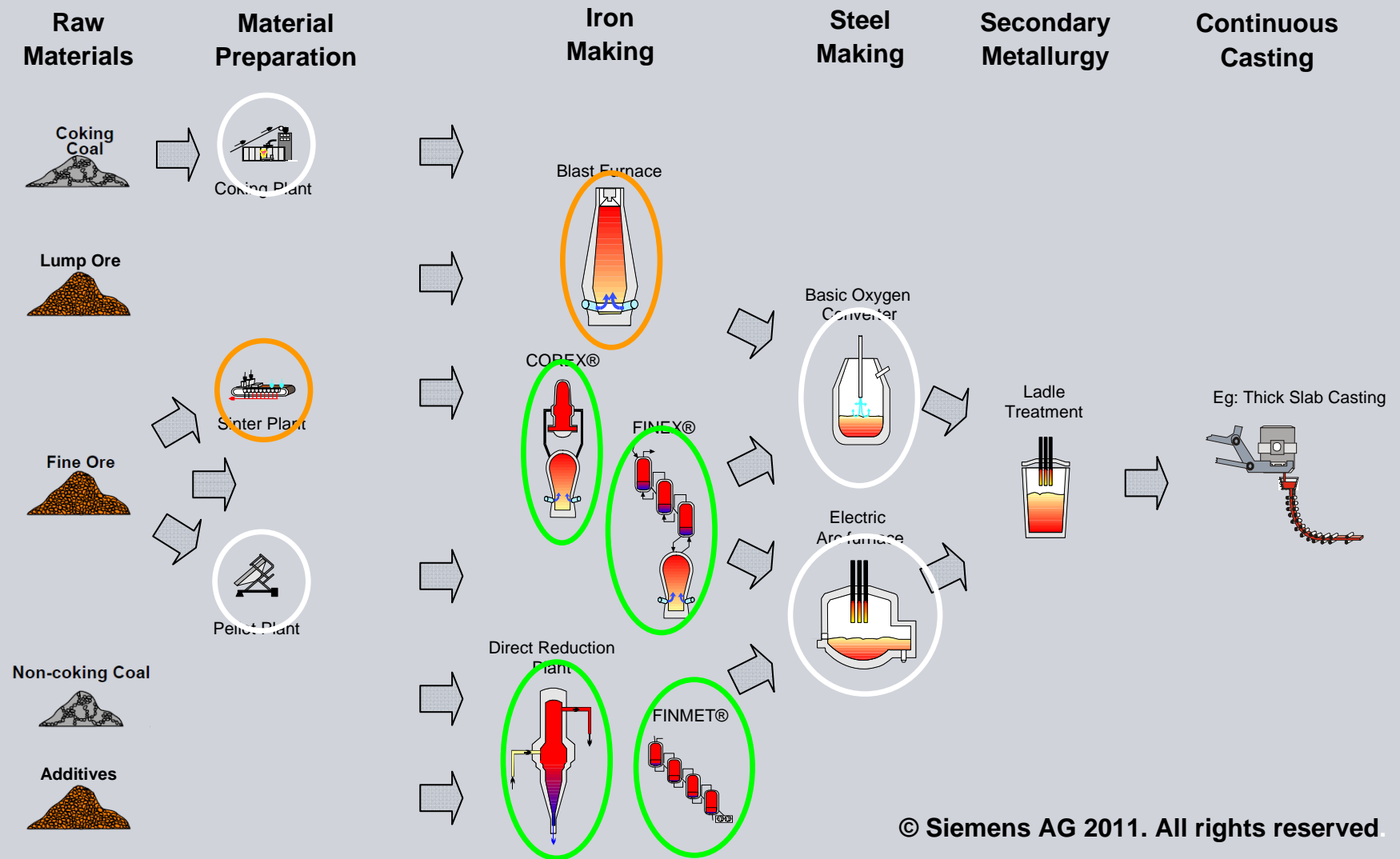
- Blast furnace ironmaking route
 - Sinter machine pending
 - Blast furnace started
 - Hot blast stoves + slag granulation envisaged

- Alternative ironmaking route
 - Corex® finished
 - Finex® finished
 - Midrex® + Corex gas based Midrex® process pending

- Outlook
 - Steelmaking:
 - BOF
 - EAF
 - Additionally:
 - Air separation unit
 - Power plants

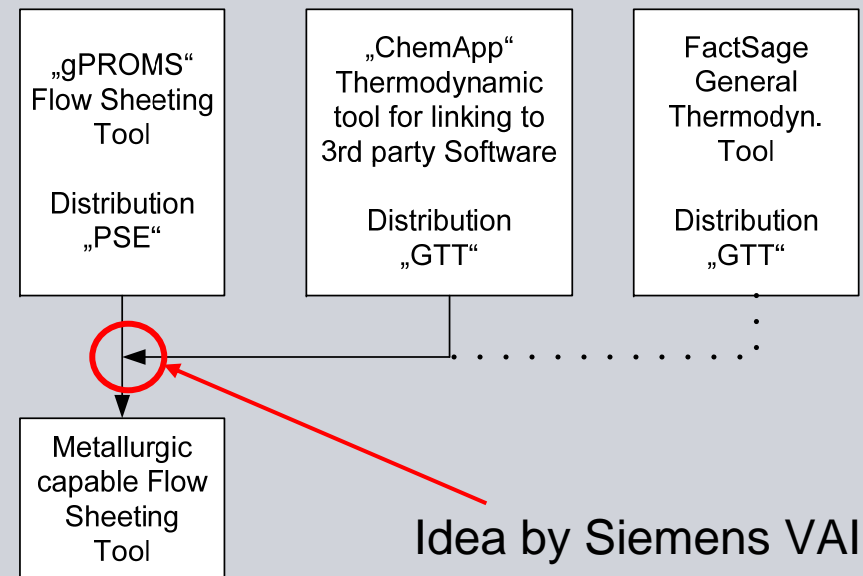
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Low Fidelity Approach - Status



High Fidelity Approach

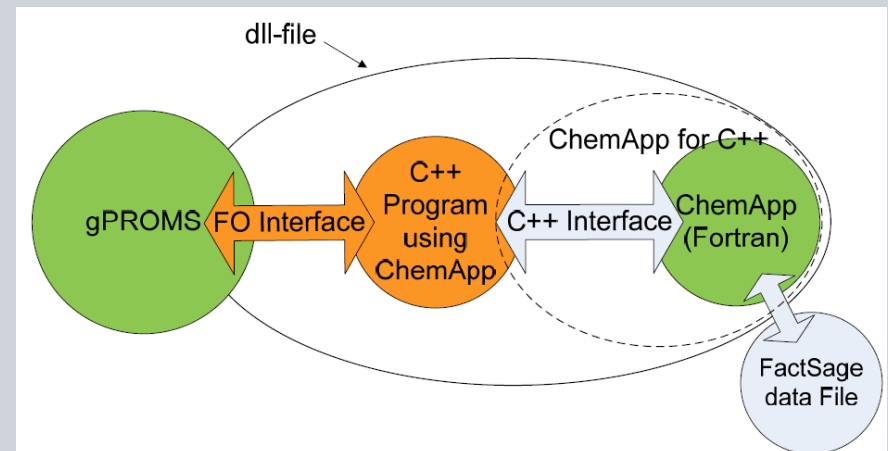
- Idea: full thermodynamic implementation of selected unit operations for scientific investigations
- Basis: FactSage + ChemApp
 - **FactSage**: provides thermo chemical data and tools for thermodynamic calculations incl. GUI with fully capable metallurgic libraries
 - **ChemApp**: Calculation engine linkable to 3rd party software containing a rich set of subroutines for complex, multiphase chemical equilibria. It has to be fed with species data provided by FactSage
- Precondition: Interface gPROMS - ChemApp
 - Linkage as a dynamic link library
 - Input file on chemical system from FactSage
 - Preselection of phase information/settings in FactSage



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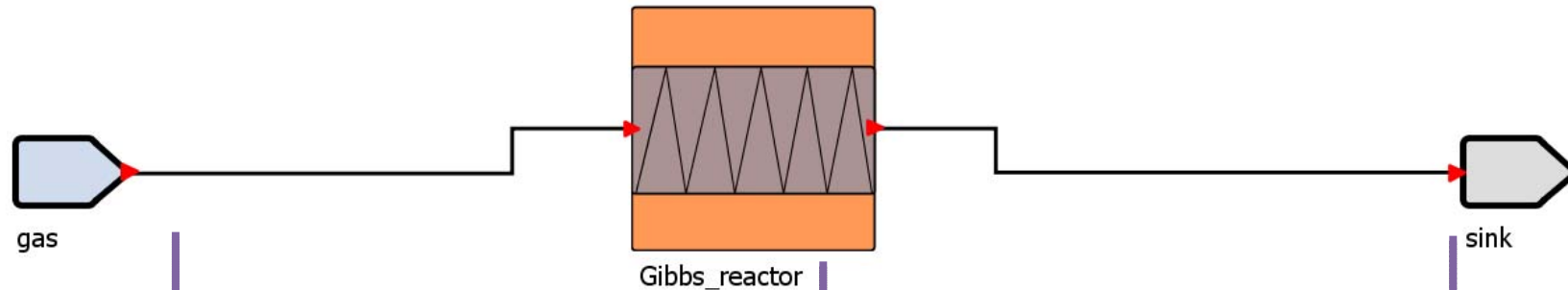
High Fidelity Approach

- Procedure
 - **FactSage:** .dat/.cst file is created based on all elements/species of the problem statement and expected solutions
 - **ChemApp:** installed
 - **Interface ChemApp - gPROMS:** .dll file stored in fo-folder in installation directory
 - **gPROMS:** .dat/.cst file stored under miscellaneous files



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High Fidelity Approach



```

non_equilibrium_CS_mass_percent("Fe2O3_hematite(s)#Fe2O3_hematite(s)") = normalised_inlet_mass_percent("Fe2O3");
non_equilibrium_CS_mass_percent("Fe3O4_magnetite(s)#Fe3O4_magnetite(s)") = normalised_inlet_mass_percent("Fe3O4");
non_equilibrium_CS_mass_percent("K2O_solid(s)#K2O_solid(s)") = normalised_inlet_mass_percent("K2O");
  
```

gas (source_gas)

Temperature units: Degrees Celsius
Pressure units: barg
Composition specification: mol %
Flowrate specification: mol/h

Specify

☒ Temperature: 25 degrees Celsius
☒ Pressure: 5.3 barg
☐ Composition: Uniform for entire array ☐ Per element

Component	mol %
H2	19.1139363
H2O_gas	5.3771925
H2S	0
O2	0
CO	46.2610203
CO2	28.2483506
CH4	0
C6H6	0
N2	0

Flow rate: 614.58742 mol/h

OK Cancel Reset All

VARIABLE RESULTS

Flowsheet.gas.outlet.mass_percent

Time ... 0.0 Actual ...

components	mol %
FeCO3	0.0
Fe2O3_H2O	0.0
H2O_liq	0.0
H2	1.431225
H2O_gas	4.267083
H2S	0.0
O2	0.0
CO	48.12723
CO2	46.17446
CH4	0.0
C6H6	0.0
N2	0.0
C_vol_coal	0.0
C_vol_coke	0.0
H_vol	0.0
N_vol	0.0
O_vol	0.0
S_vol	0.0

Table Graph Properties

VARIABLE RESULTS non_equilibrium_CS_mass...

Flowsheet.Gibbs_reactor.non_equilibrium_CS_mass_percent

Time [0.0 .. 0.0] Fixed at 0.0 Actual = 0.0

phase_constit...

phase constituents	mol %
CaO_liquid(liq)#CaO_liquid(liq)	0.0
Mn_liquid(liq)#Mn_liquid(liq)	0.0
Fe_liquid(liq)#Fe_liquid(liq)	0.0
Na2O_liquid(liq)#Na2O_liquid(liq)	0.0
Al2O3_liquid(liq)#Al2O3_liquid(liq)	0.0
K2O_liquid(liq)#K2O_liquid(liq)	0.0
TiO2_liquid(liq)#TiO2_liquid(liq)	0.0
MnO_liquid(liq)#MnO_liquid(liq)	0.0
P_liquid(liq)#P_liquid(liq)	0.0
S_liquid(liq)#S_liquid(liq)	0.0

Table Graph Properties

VARIABLE RESULTS

Flowsheet.gas.outlet.mass_percent

Time ... 0.0 Actual ...

components	mol %
FeCO3	0.0
Fe2O3_H2O	0.0
H2O_liq	0.0
H2	1.431225
H2O_gas	4.267083
H2S	0.0
O2	0.0
CO	48.12723
CO2	46.17446
CH4	0.0
C6H6	0.0
N2	0.0
C_vol_coal	0.0
C_vol_coke	0.0
H_vol	0.0
N_vol	0.0
O_vol	0.0
S_vol	0.0

Table Graph Properties

```

# Equilibria calculation
equilibrium_CS_mass_percent = phys_prop_CS.EquilibriumAmount(temperature , pressure , non_equilibrium_CS_mass_percent() ) ;
  
```

```

outlet.mass_percent("FeO") = equilibrium_CS_mass_percent("FeO_wustite(s)#FeO_wustite(s)");
outlet.mass_percent("Fe2O3_H2O") = equilibrium_CS_mass_percent("Fe2O3(H2O)_solid(s)#Fe2O3(H2O)_solid(s)");
outlet.mass_percent("FeCO3") = equilibrium_CS_mass_percent("FeCO3_siderite(s)#FeCO3_siderite(s)");
  
```

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High Fidelity Approach

- Problems
 - Phase and solution systems selection in FactSage prior to .cst/.dat file
 - Model abstraction: equilibria not reached in real processes
 - “distance to equilibrium” approach
 - Temperature approach
 - Further evaluations on possible solution systems selection to be used from FactSage

Contact



Bernd Weiss

Iron Making Technology
I I S M T I R T Y D R

Turmstrasse 44
4031 Linz

Phone: 0043 - 732 6592 74829
Fax: 0043 - 732 6980 6466
Mobile: 0043 664 8844 8330

E-mail: bernd.weiss@siemens.com



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