

# Linking Process Engineering to Product Performance

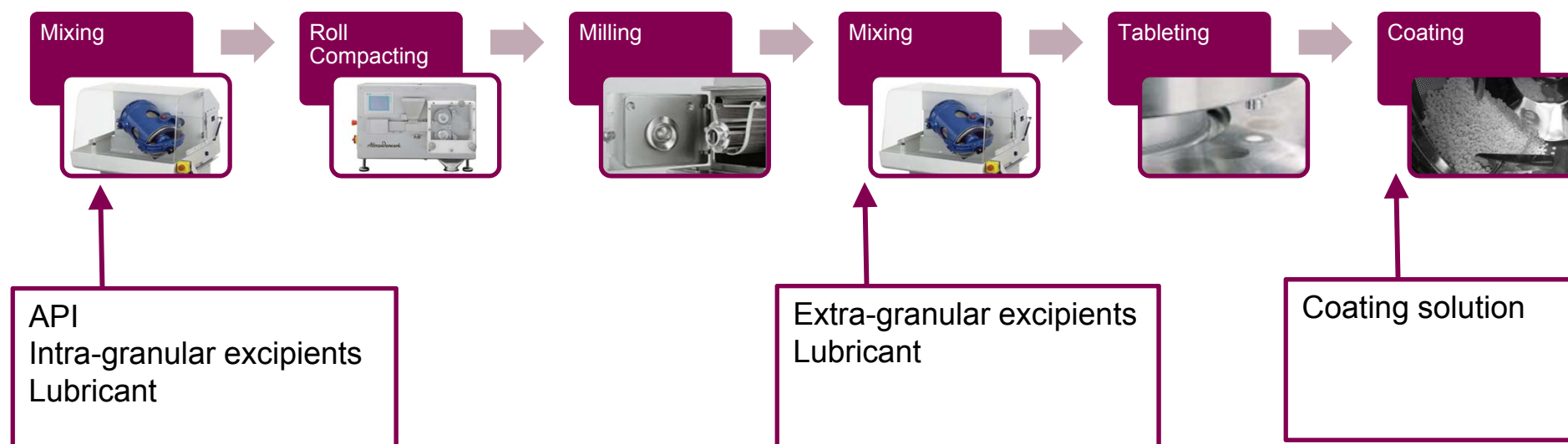
## A roll compaction case study

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# (One way) to make a tablet



# What is important (for a tablet)?

It depends, but often...



Dissolution



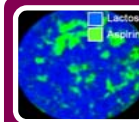
Assay



Hardness



Appearance

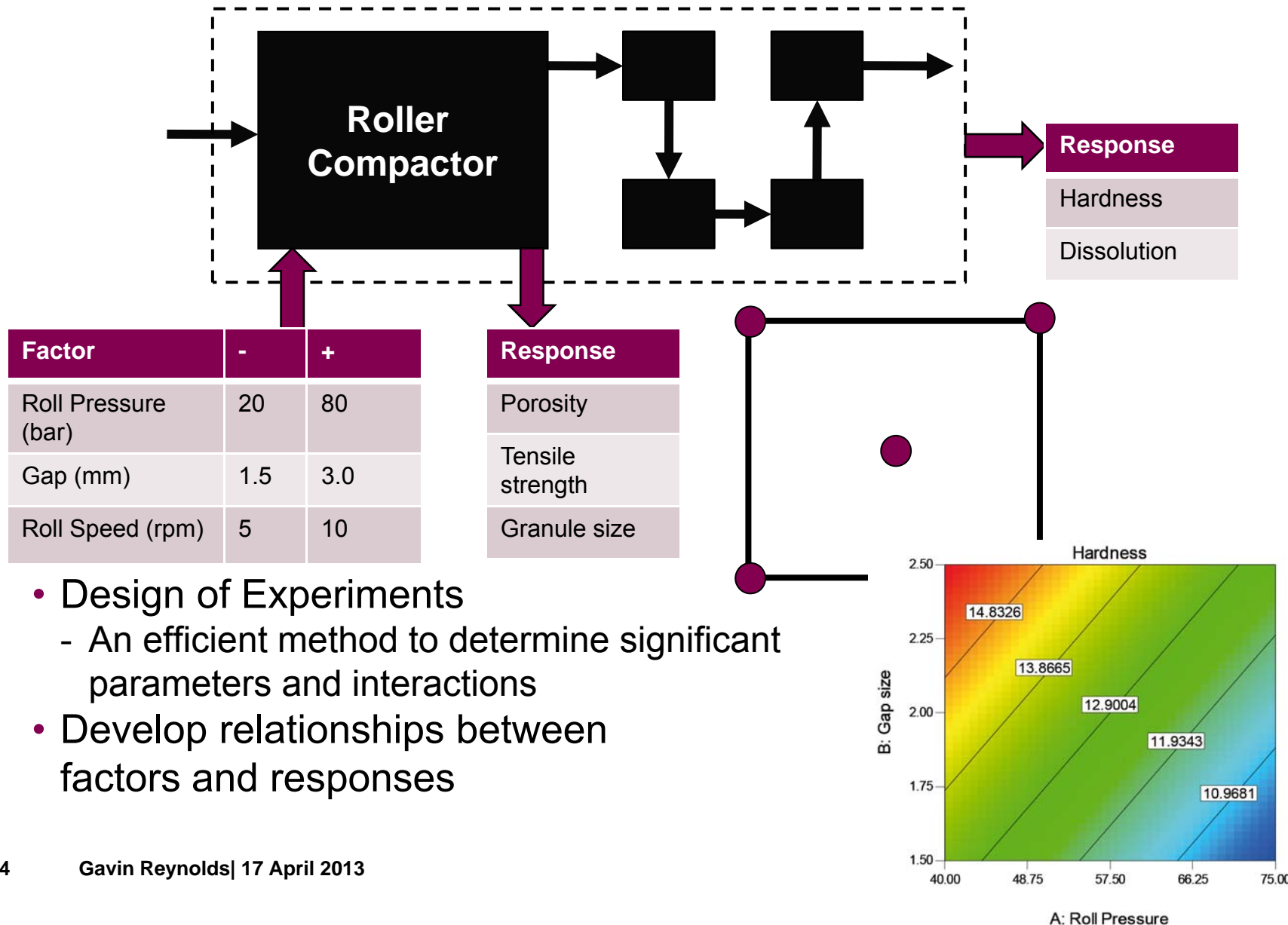


Content Uniformity

... and others

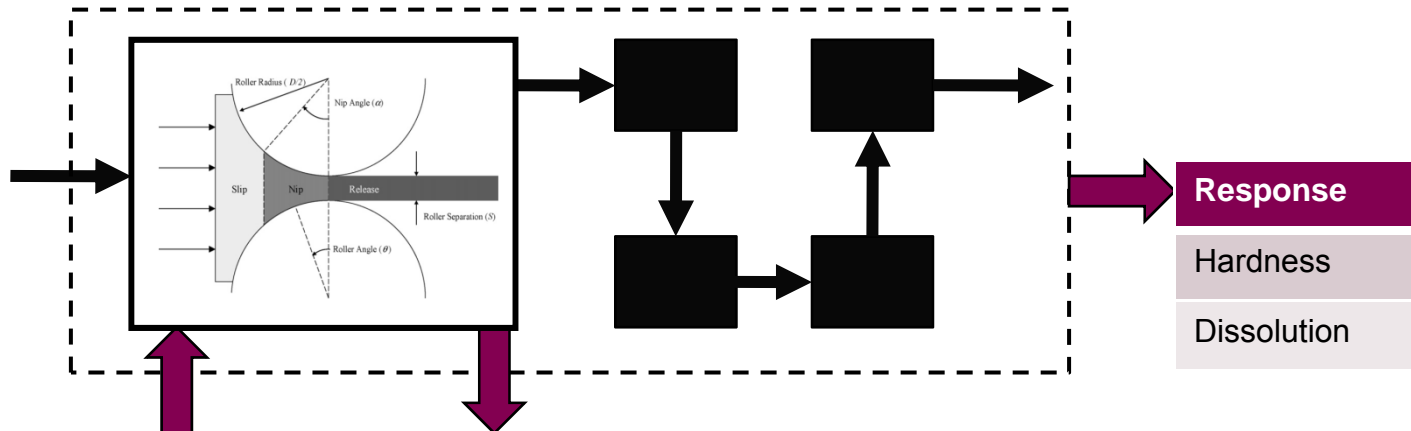


# Typical 'black box' experimental approach



- Design of Experiments
  - An efficient method to determine significant parameters and interactions
- Develop relationships between factors and responses

# What can we model? – unit operations



Factor	-	+	Response
Roll Pressure (bar)	20	80	Porosity
Gap (mm)	1.5	3.0	Tensile strength
Roll Speed (rpm)	5	10	Granule size

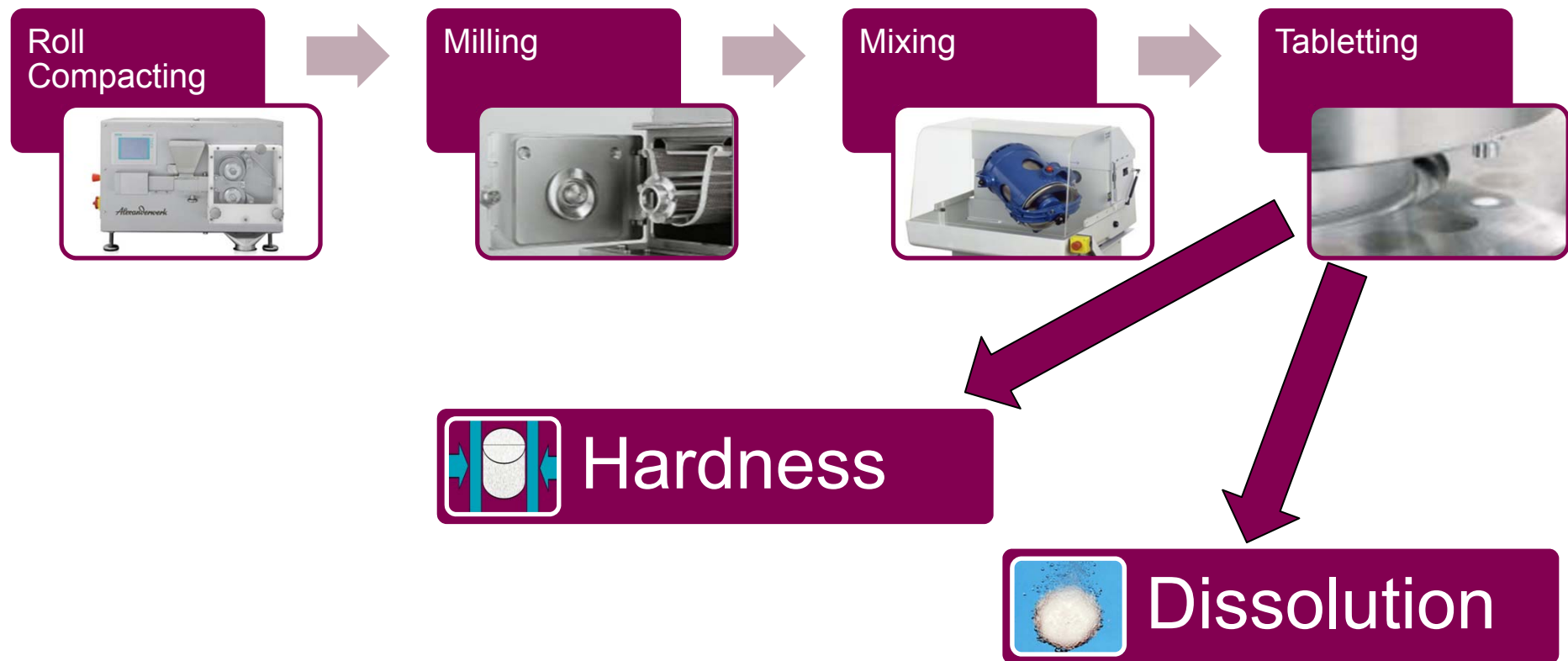
$$\gamma_R = \gamma_0 \left( \frac{2R_f}{WD \int_{\theta=0}^{\theta=\alpha(\delta_E, \phi_W, K)} \left[ \frac{(S/D)}{(1 + S/D - \cos \theta) \cos \theta} \right]^K \cos \theta d\theta} \right)^{1/K}$$

- We can develop models for individual unit operations, for example RC
- Useful to predict porosity for scale-up and process understanding
- However, what we really want to know is how each process parameter and unit operation impacts on product quality and performance



# A systems-based approach

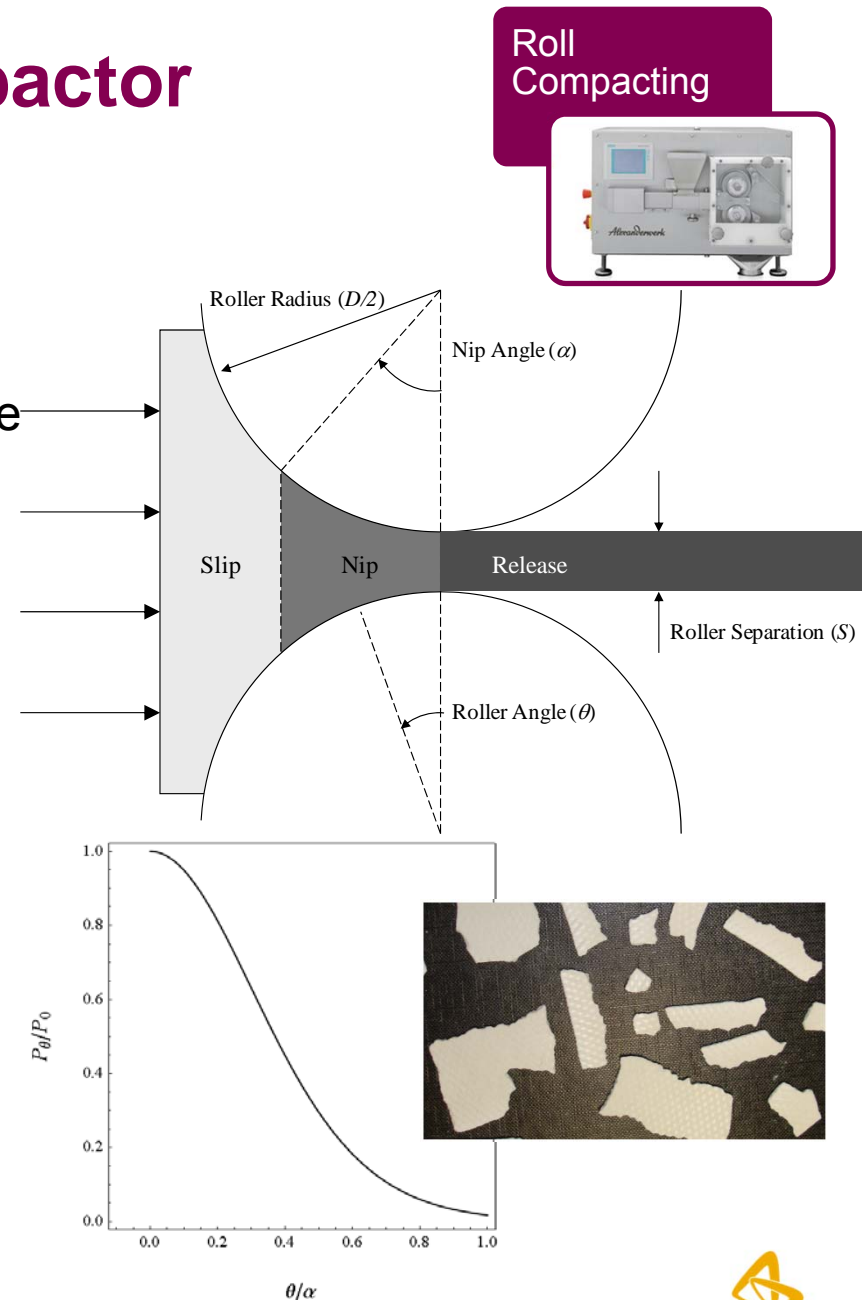
Develop unit operation models and link to product performance



# Unit Operation – Roll Compactor

## Developing a model

- The material properties of the ribbon will be related to the peak pressure exerted within the roll compactor.
- In practise the peak pressure is not known
  - Total pressing force
  - OR hydraulic pressure
- Models can be developed to describe the pressure distribution within the roll compactor and therefore the peak pressure
- Material assumed to be isotropic, frictional, cohesive and compressible, obeying effective yield function of Jenike and Shield (1959).
- Boundary conditions based on determining the nip angle as proposed by Johanson (1965).



# Unit Operation – Roll Compactor

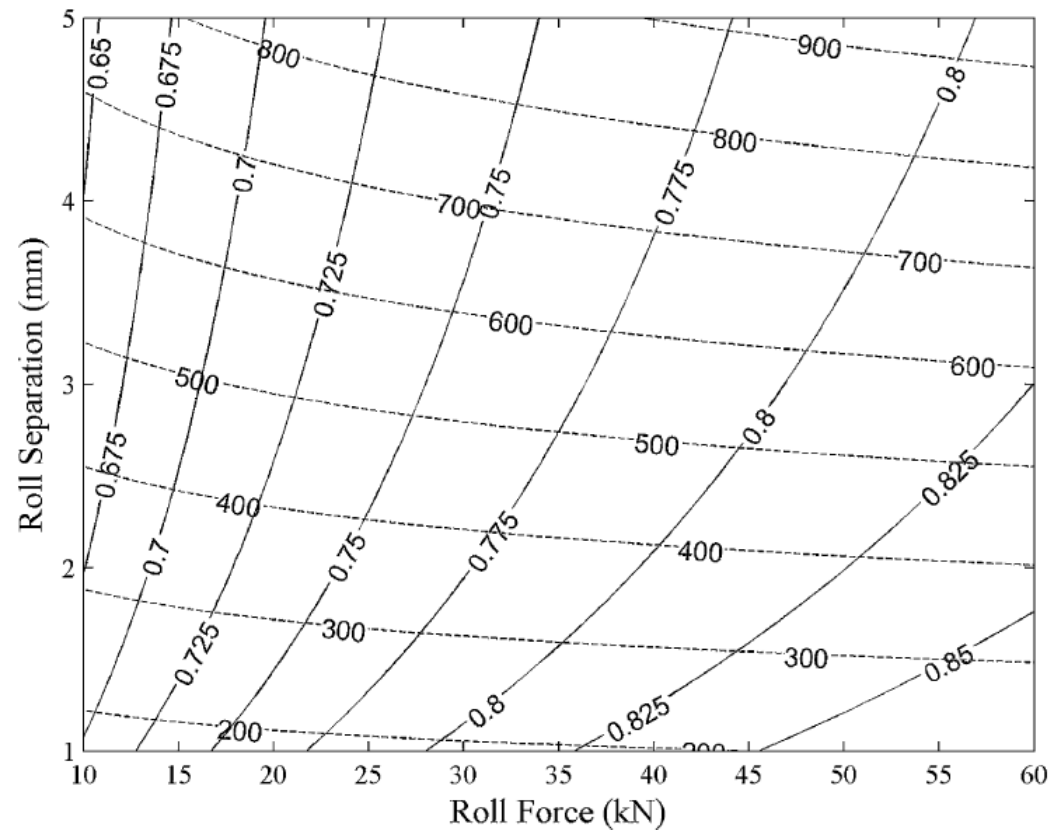
## Developing a model

Roll  
Compacting



$$\gamma_R = \gamma_0 (2R_f)^{1/K} \left( WD \int_{\theta=0}^{\theta=\alpha(\delta_E, \phi_W, K)} \left[ \frac{c_S N_S}{\pi \rho_{\text{true}} \gamma_R WD^2 N_R (1 + c_S N_S / \pi \rho_{\text{true}} \gamma_R WD^2 N_R - \cos \theta) \cos \theta} \right]^K \cos \theta d\theta \right)^{-1/K}$$

- Powder mechanics model allows the key intermediate attribute of **ribbon relative density or porosity** to be related to **process parameters** (roller pressure, gap size, screw speed) based on **material compaction properties** (compressibility) and **equipment geometry** (diameter, width).



Reynolds (2010), *Comp. Chem. Eng.* 34, 1049

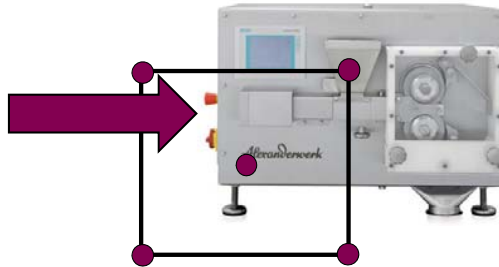




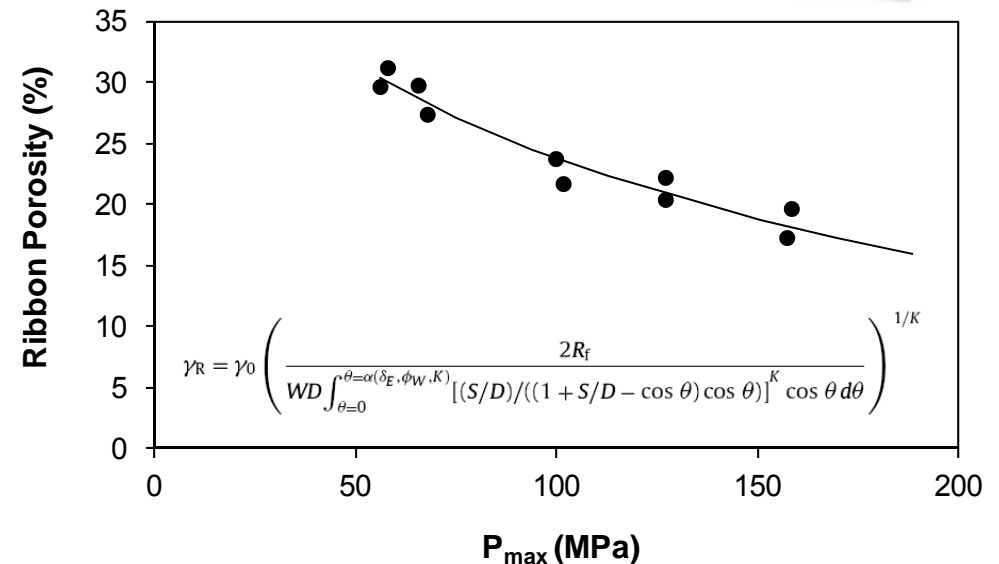
# Unit Operation – Roll Compactor

## Calibrating a model

Roll Compacting



- The powder compaction properties are calibrated to RC experimental data.
- $P_{\max}$  is dependent on these parameters, so the model needs to be solved iteratively to determine  $\gamma_0$  and  $K$ .



# Unit Operation – Milling

## Developing a model

### Milling



- The roll compactor is followed by a screening mill. This is modelled by coupling a mill model with a classification model.

- The mill model uses the breakage kernel of Vogel and Peukert (2005).

- Breakage probability

$$P_B = 1 - \exp\left\{f_{Mat} x k (W_{m,kin} - W_{m,min})\right\}$$

Material strength parameter

Number of impacts

Mass specific impact energy

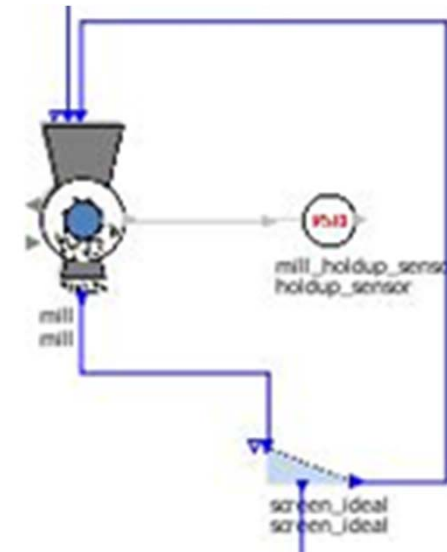
Threshold energy for particle of size x

- Fragment size distribution

$$B = \left(\frac{x}{y}\right)^q \frac{1}{2} \left\{ 1 + \tanh\left(\frac{y - y'}{y'}\right) \right\}$$

Minimum particle size limit

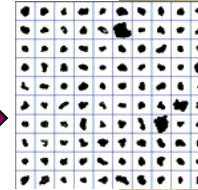
Power law exponent



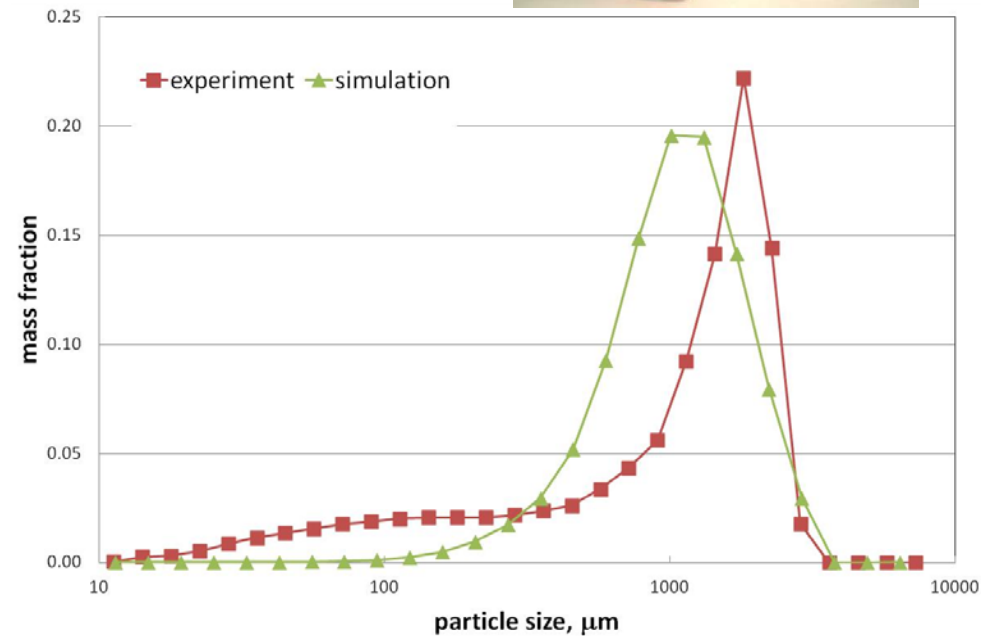
# Unit Operation – Milling

## Calibrating a model

Milling



- The six parameters of the breakage kernel are determined by fitting the predicted granule size distribution to experimental data.
- In this case the mill model was only able to approximate the granule size distribution
  - The sharpness of the large mode is not captured
  - No fines are predicted



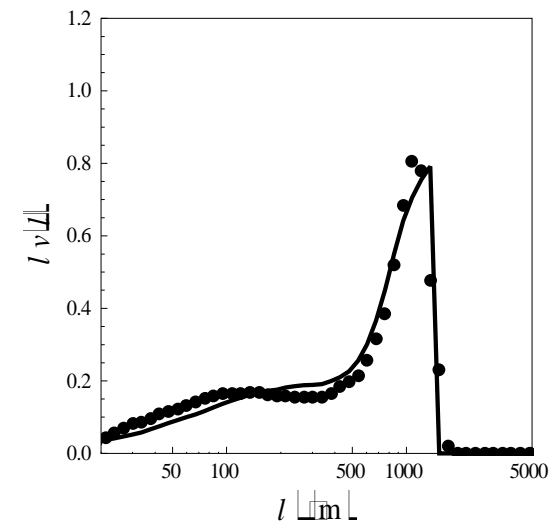
# Unit Operation – Milling

## Improving a model

### Milling



- Typically granular material exhibits a bimodal breakage mechanism
- The accuracy of the predicted granule size distribution could be improved by incorporating a bimodal fragment size distribution
- However, the approximated distribution was considered sufficient for the initial system model.



$$b(v, v) = \frac{u z}{3k_v^{1/3} v^{2/3}} \frac{2}{\sqrt{2\pi \ln \sigma_1}} \frac{\exp \left[ - \left( \frac{\ln \left( v^{1/3} / k_v^{1/3} \mu_1 \right)}{\sqrt{2 \ln \sigma_1}} \right)^2 \right]}{1 + \operatorname{erf} \left[ \frac{\ln u^{1/3} / k_v^{1/3} \mu_1}{\sqrt{2 \ln \sigma_1}} \right]} + (1-z) \frac{p}{u} \frac{\left( \frac{v}{u} \right)^{-1} \left( 1 - \left( \frac{v}{u} \right) \right)^r}{B(q, r)}$$

Fragmentation

Disintegration

Reynolds (2010), Chem. Eng. J. 164, 383

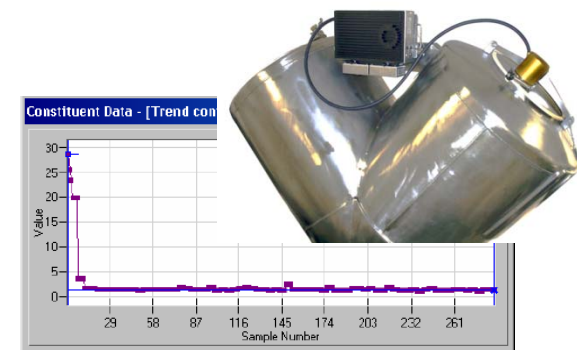
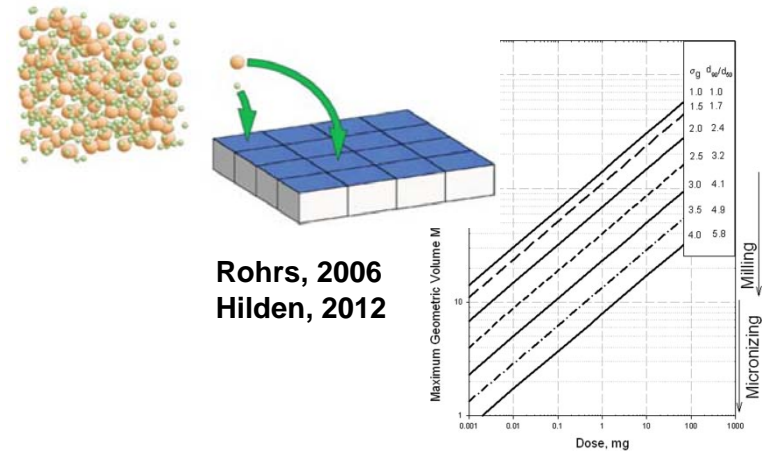


# Unit Operation – Mixing

## Developing a model

- To simplify the construction of the system model, the mixing unit operation was not modelled (i.e. the stream was considered well-mixed)
- Various approaches can be envisaged ranging from well-mixed models to empirical exponential decay models.
- One practical challenge would be considering how 'degree of mixedness' would propagate downstream to subsequent unit operations and product properties.

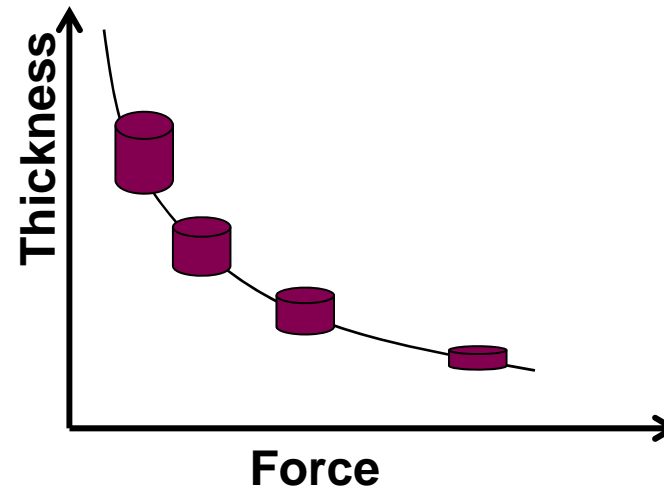
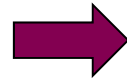
### Mixing



# Unit Operation – Tableting

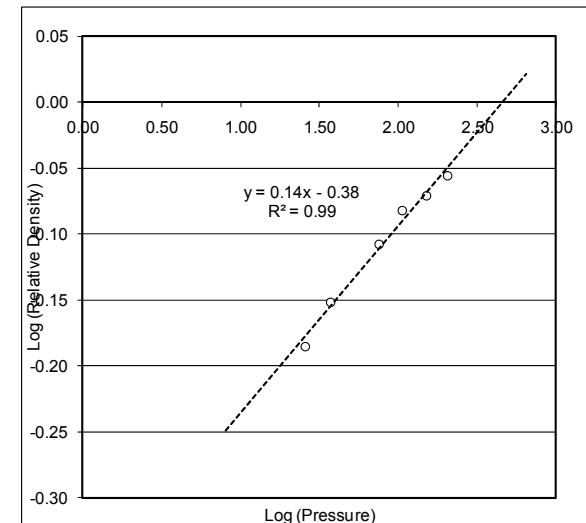
## Developing a model

Tableting



- A simple compaction model is implemented to determine tablet porosity from the tablet dimensions and punch force.

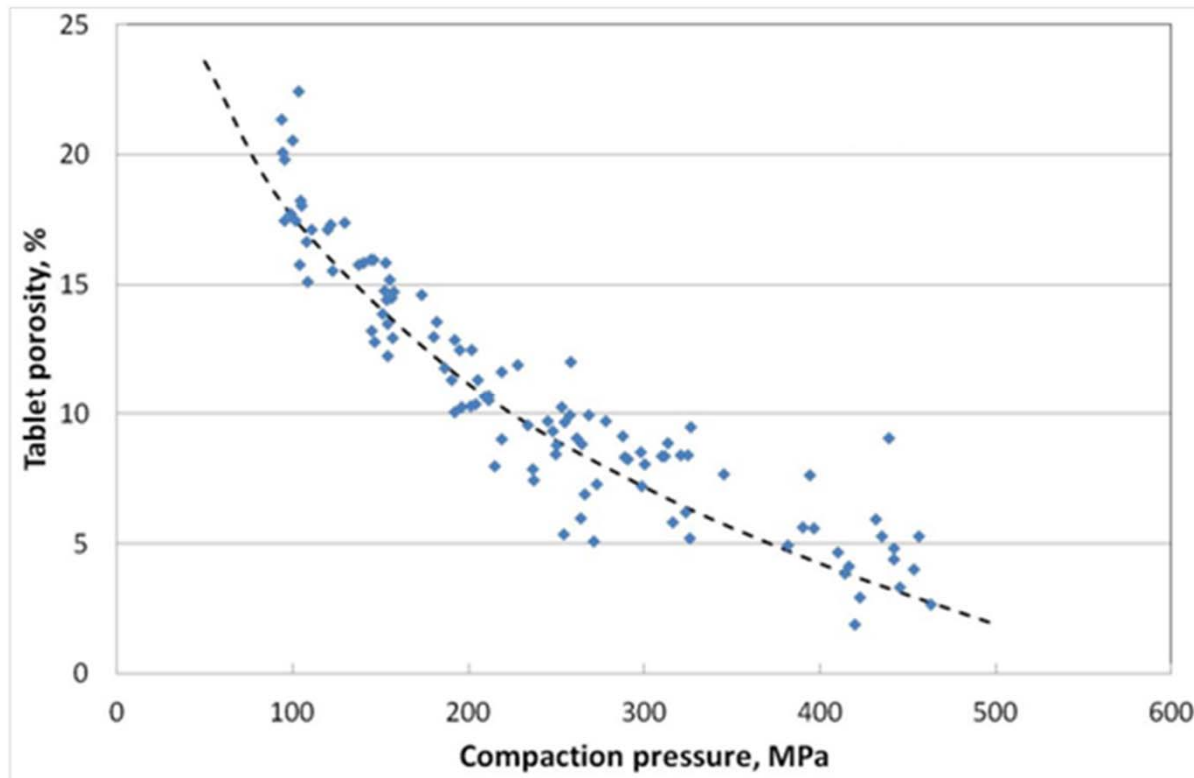
$$P = \frac{F}{A} \quad \gamma = \gamma_0 P^{1/K}$$



# Unit Operation – Tableting

## Calibrating a model

Tableting



- This simple model assumes that only the formulation composition influences the relationship, and not upstream processes (e.g. roll compaction). In this case, a single relationship across all the experiments seems to be a reasonable approximation.





# Performance – Hardness

## Developing a model



## Hardness

- Tensile strength (hardness) can be related to tablet porosity using the Ryshkewitch-Duckworth equation

$$T = \bar{T} e^{-k_b \varepsilon}$$

Tensile strength at zero porosity

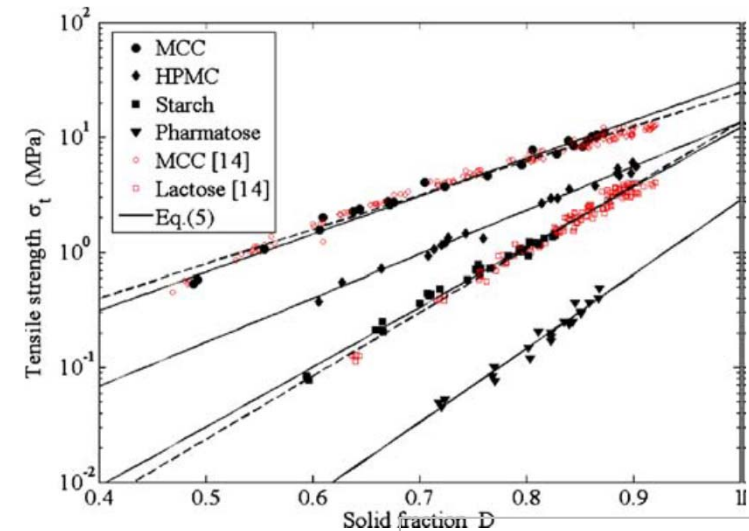
Bonding capacity

- In general it is observed that roll compaction typically reduces the apparent tablet tensile strength. This 'loss of compressibility' can be approximated by subtracting the tensile strength generated during roll compaction from the final tablet tensile strength.

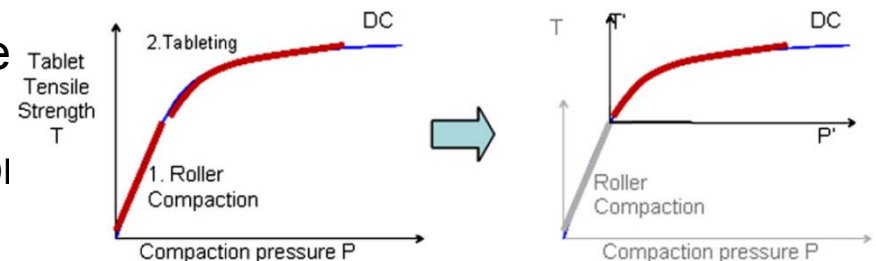
$$T_{\text{tablet}} = \bar{T} e^{-k_b \varepsilon_{\text{tablet}}} - \bar{T} e^{-k_b \varepsilon_{\text{ribbon}}}$$

Tablet porosity

Ribbon porosity



Wu (2006), Pharm. Res. 23, 1898



Farber (2008), Int. J. Pharm. 346, 17



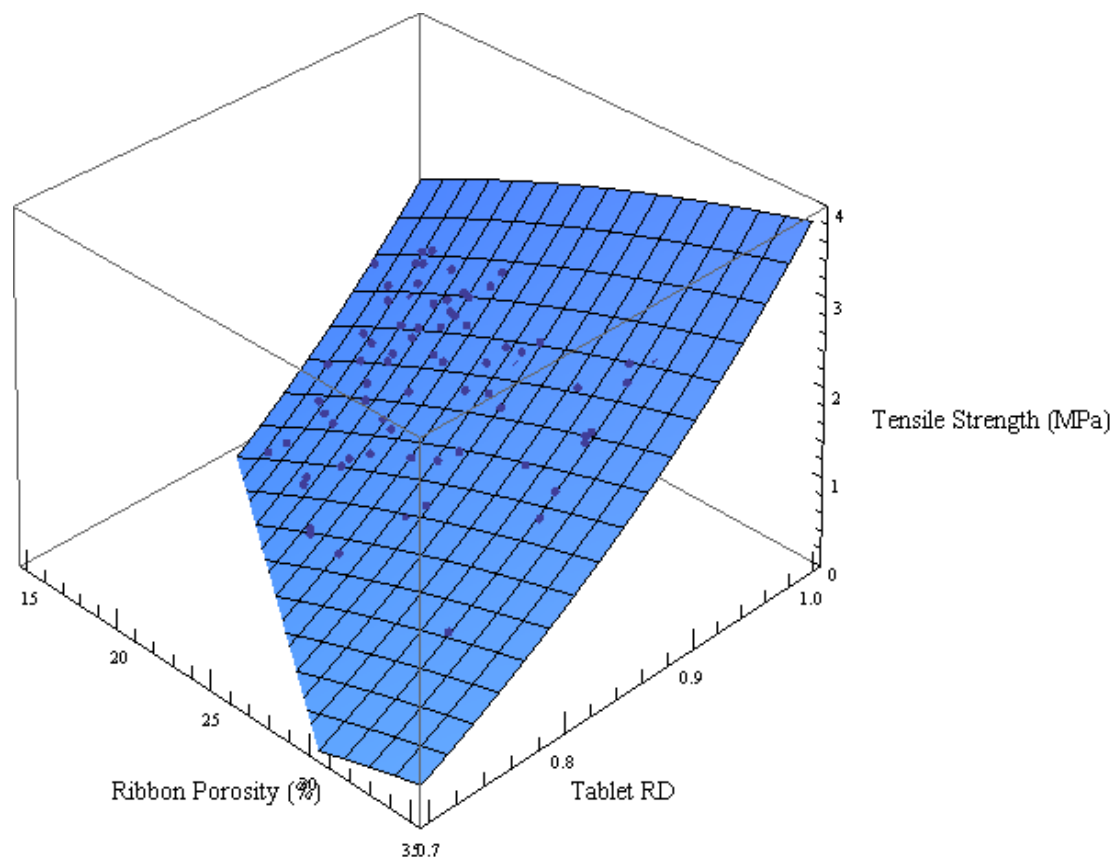


# Performance – Hardness

## Calibrating a model



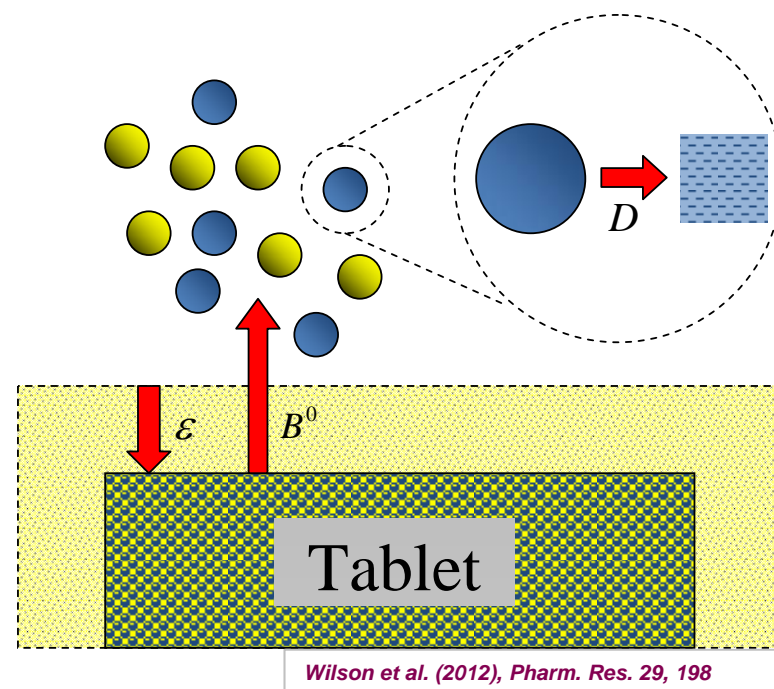
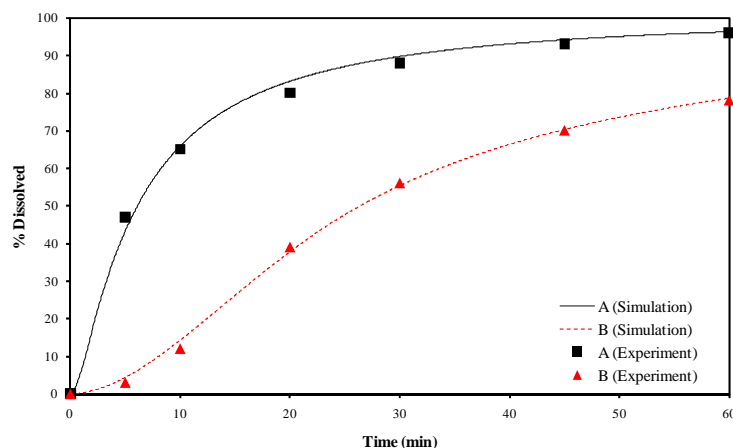
- A single set of material parameters was estimated by fitting the compaction model to experimental data.
- This single set of parameters were able to be used across all the process conditions (i.e. related to formulation composition rather than upstream processing such as roller compaction).



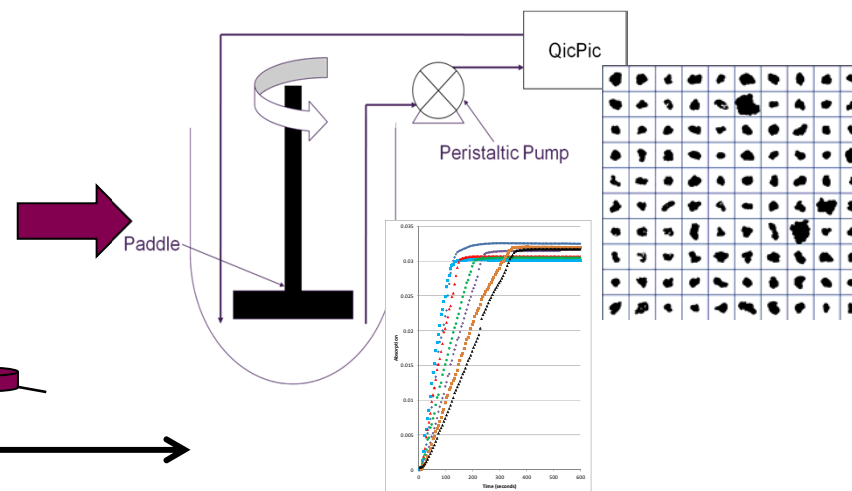
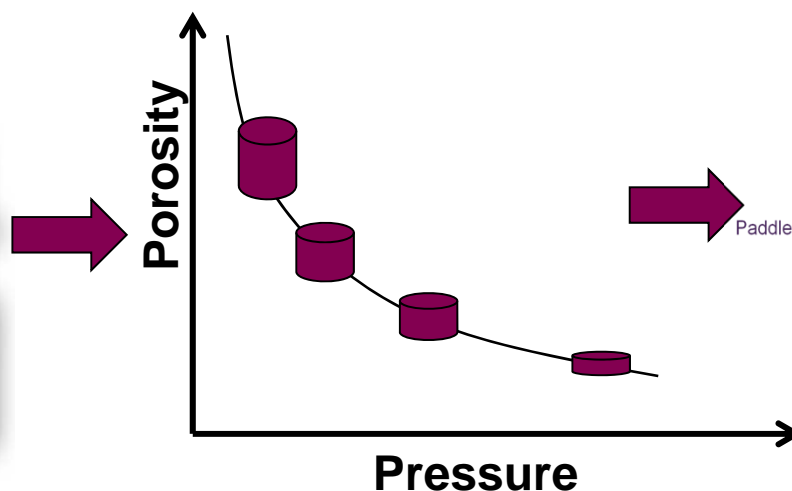
# Performance – Dissolution

## Developing a model

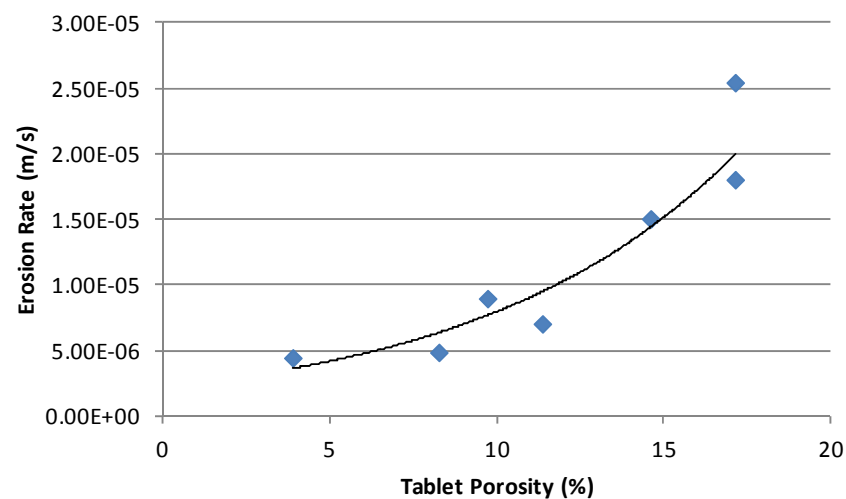
- A relatively simple model to describe tablet disintegration and dissolution was developed.
- Here, particles are released into suspension as a result of erosion of the tablet. The API is then dissolved into solution by mass transfer from the suspended particles.
- The model is based on that presented by Wilson et al. (2012).



# Performance – Dissolution Calibrating a model

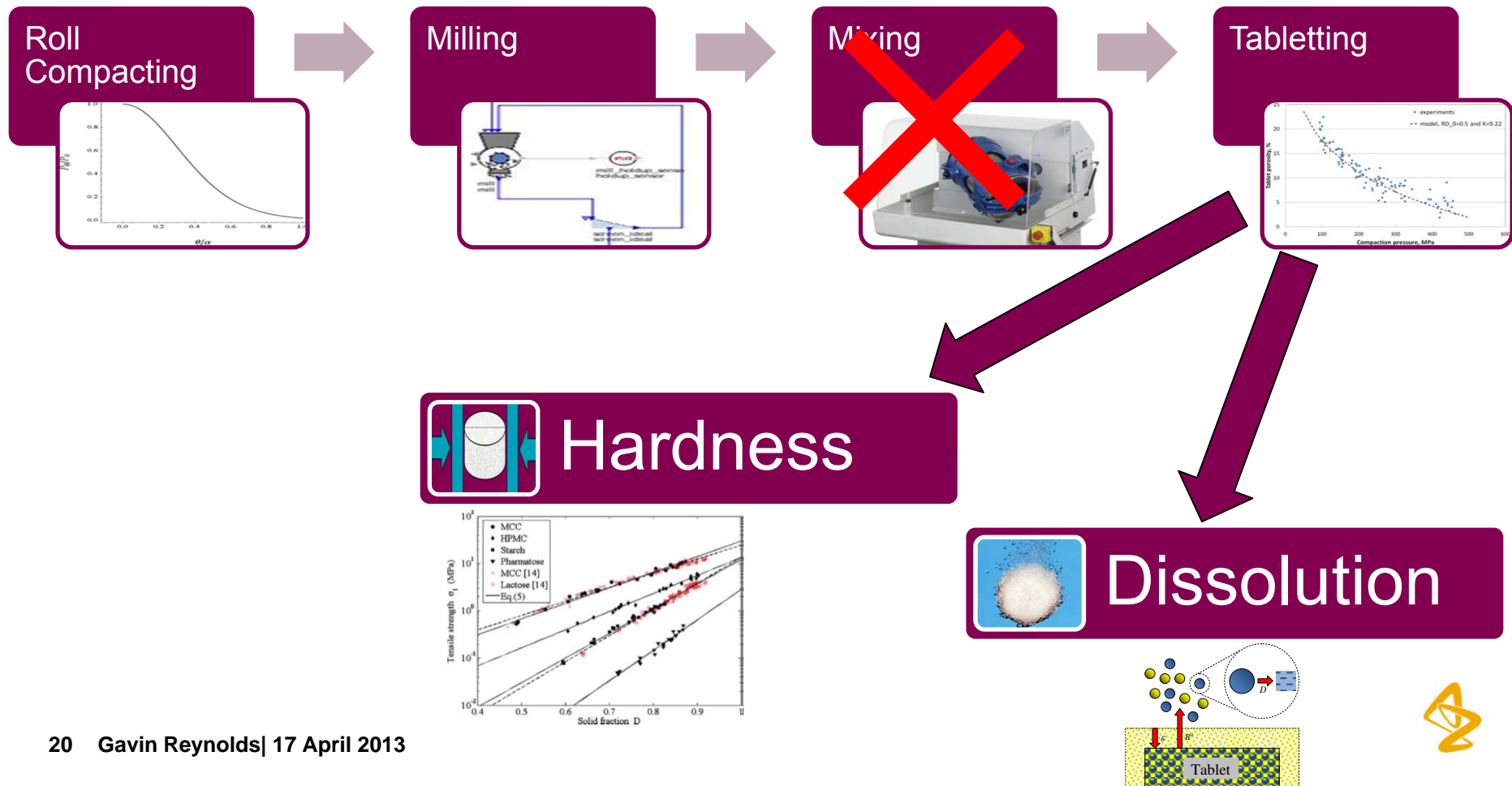


- Experimental data was fitted in order to determine the erosion rate.
- An exponential relationship was used to describe the link between erosion rate and tablet porosity.



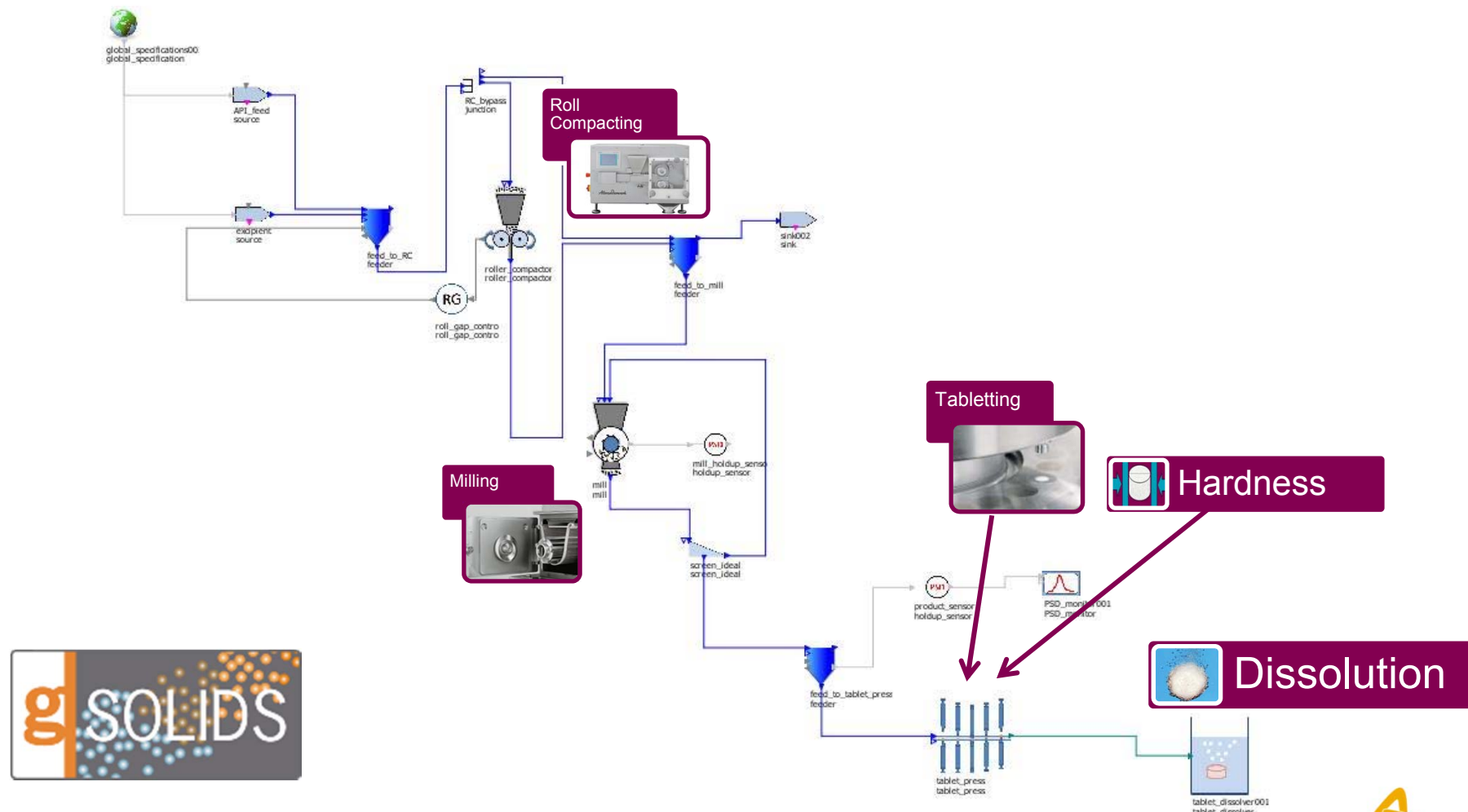
# A systems-based approach

Develop unit operation models and link to product performance



# Putting it all together

## Implementing the system in gSolids



# Results

## Experimental parameters

- **Typical immediate release tablet formulation**

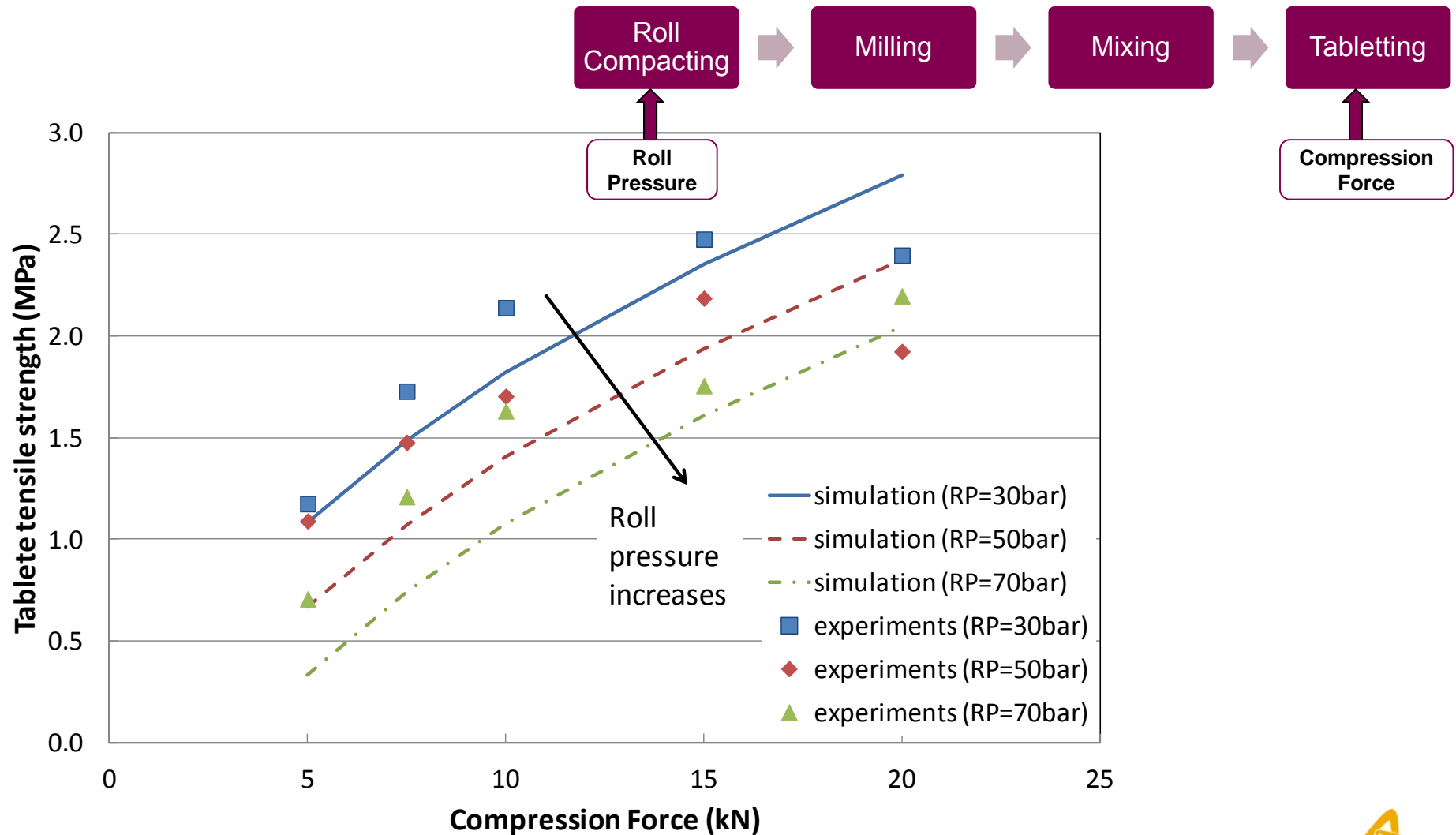
- 15% API
- Mixture of brittle and ductile fillers
- Lubricant

Factor	Range
Roll Pressure	30 – 70 bar
Mill Screen	1.25 – 2.0 mm
Compaction Force	5 – 20 kN
Number of runs	19



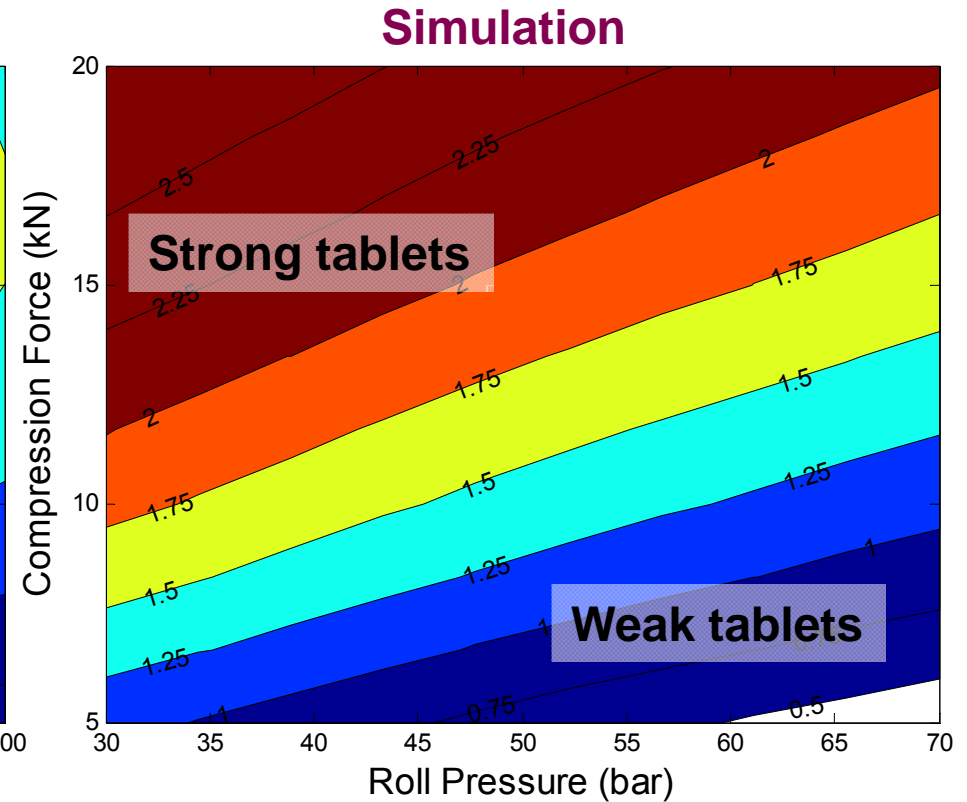
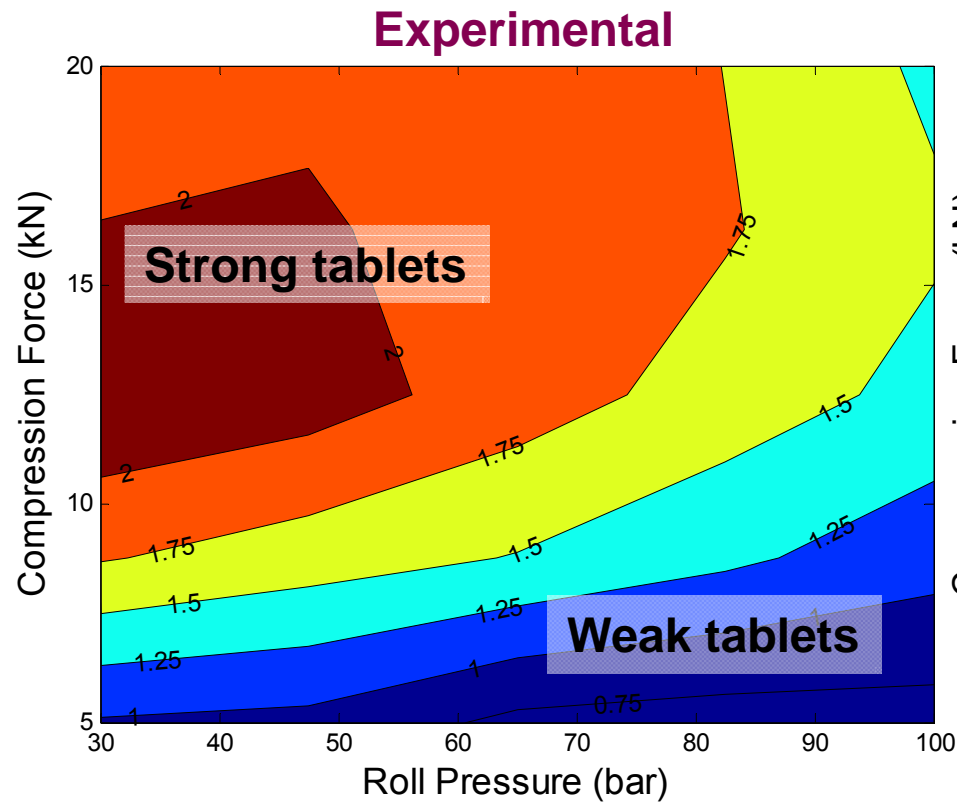
# Results

## Roller Pressure and Tablet Tensile Strength



# Results

## Roller Pressure and Tablet Tensile Strength



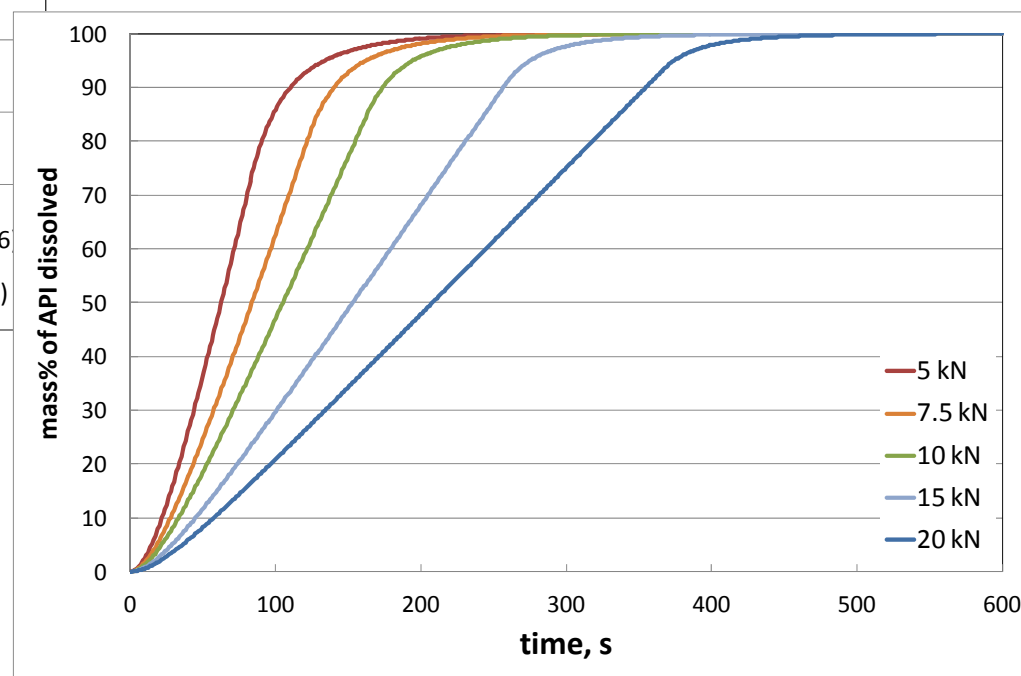
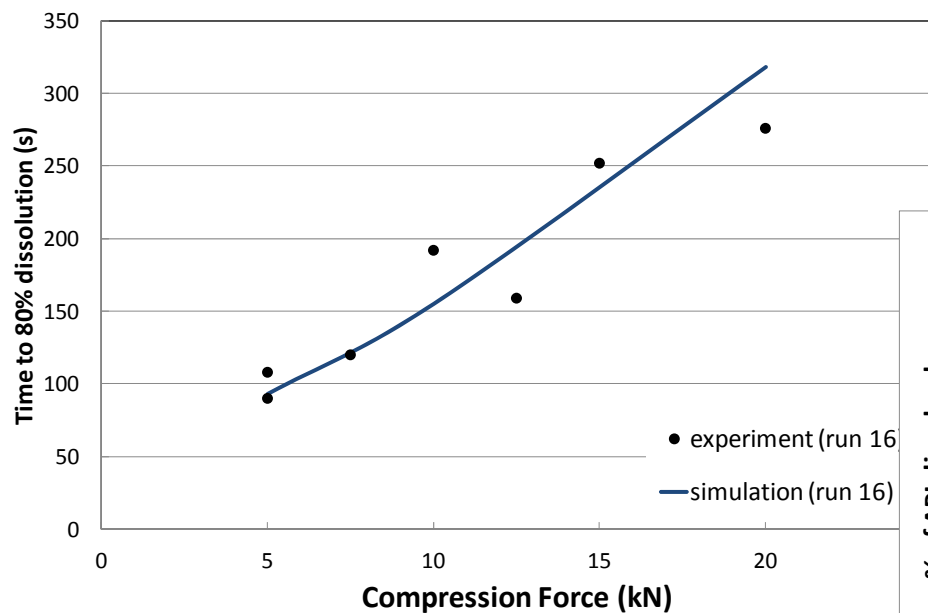
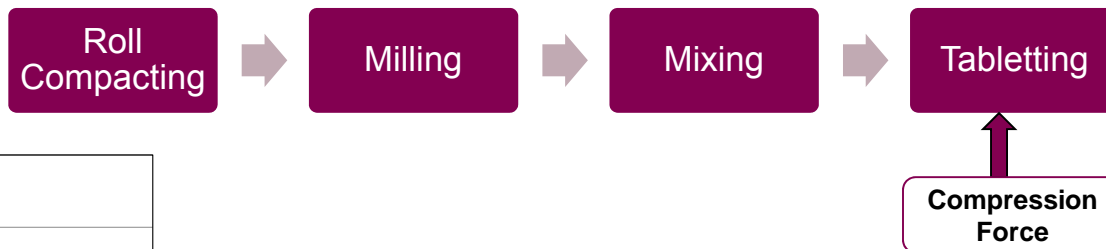
- General qualitative and quantitative trends captured
- Some non-linear behaviour at high compression forces not captured





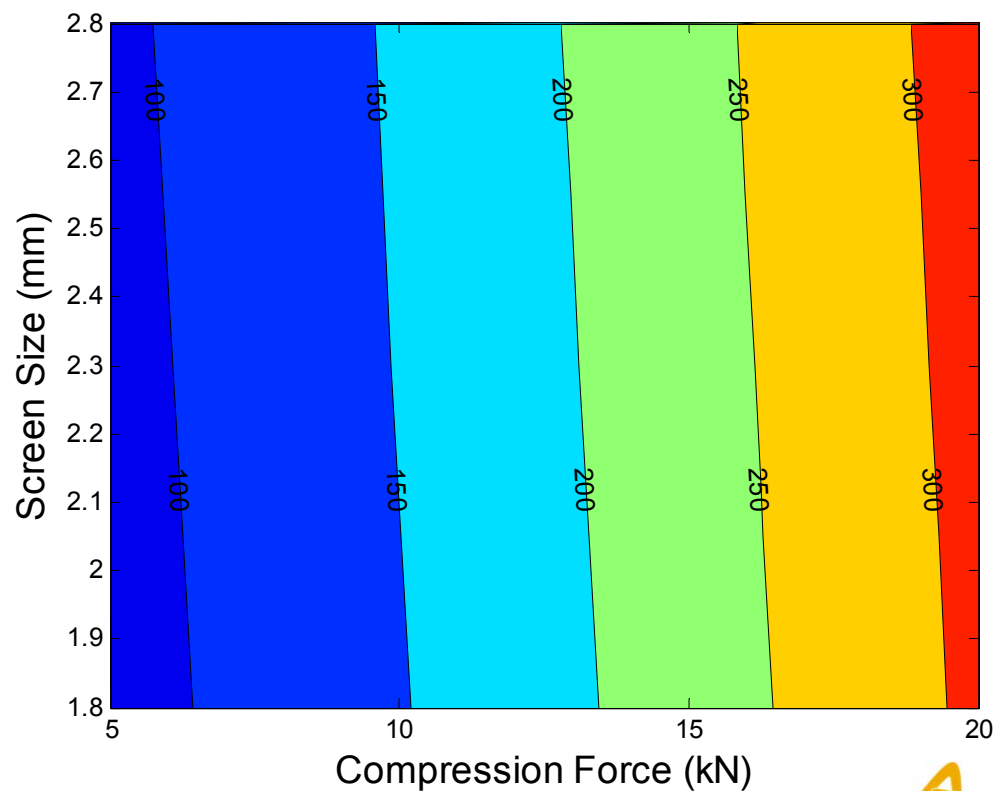
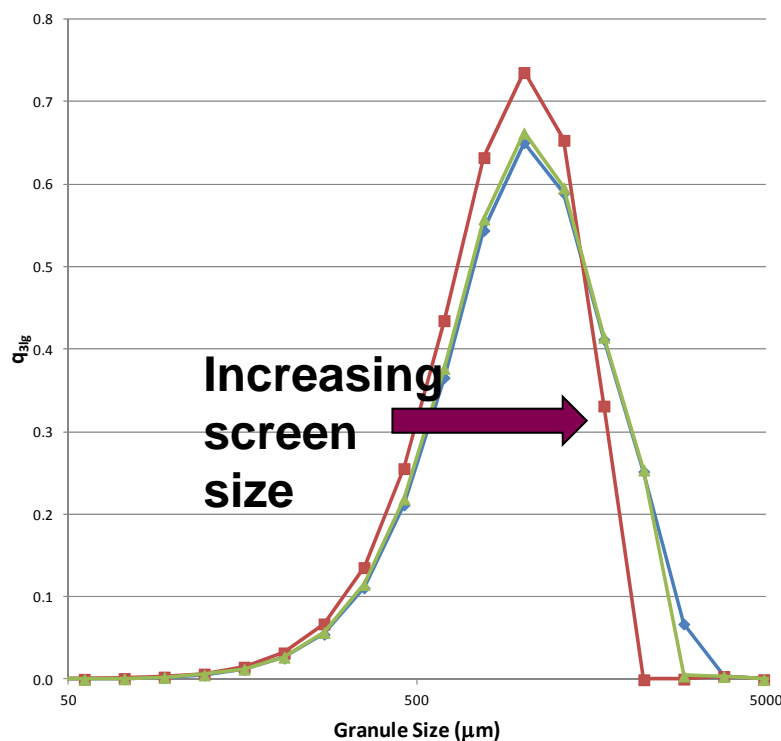
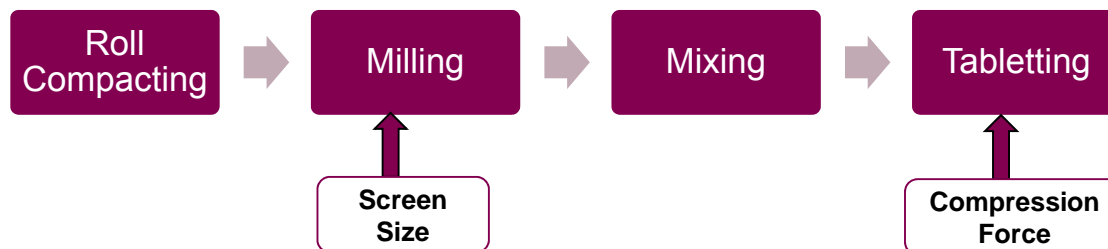
# Experimental Validation

## Tablet Compression Force and Dissolution



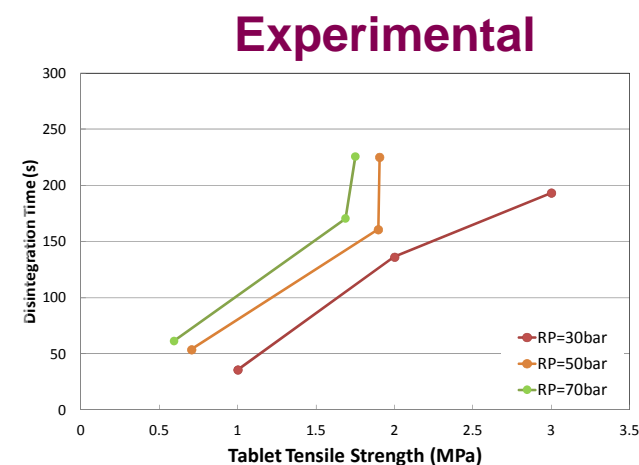
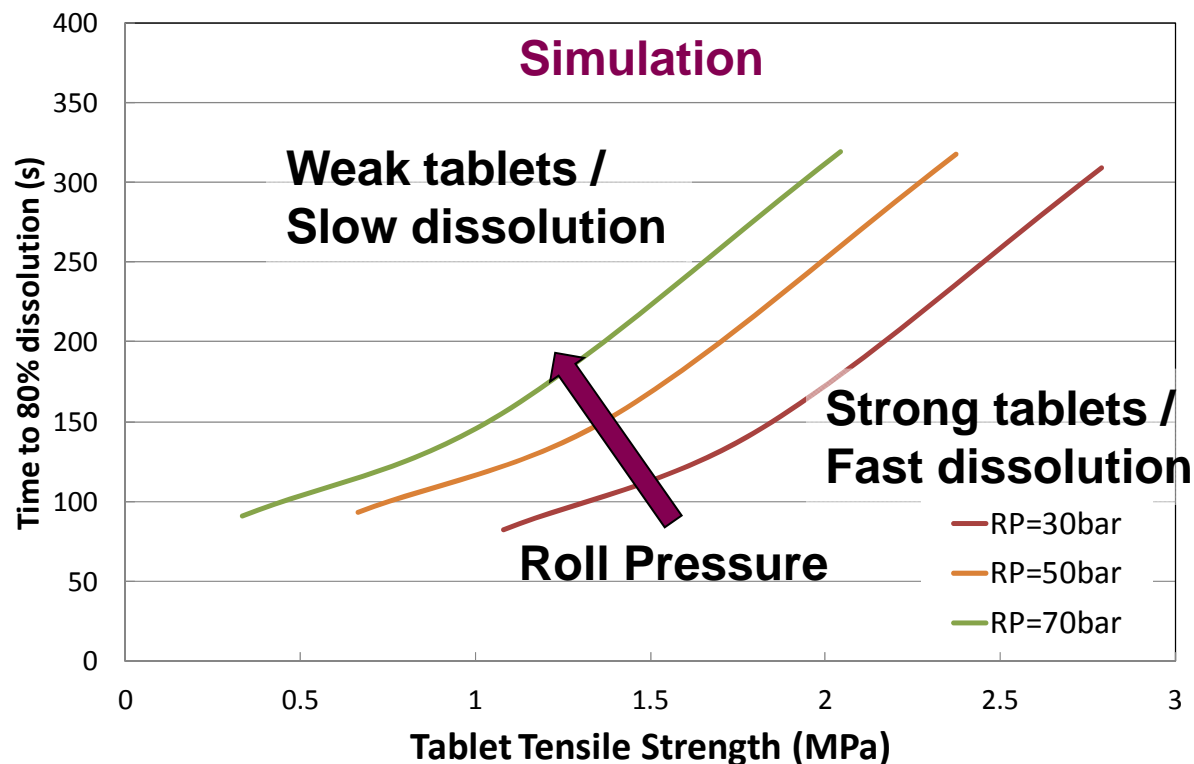
# Experimental Validation

## Tablet Compression Force and Dissolution



# Experimental Validation

## Tablet Tensile Strength and Dissolution



- Predicted dissolution performance in qualitative agreement with experimental disintegration time.



# Conclusions

- **Demonstrated constructing a system model linking tablet manufacture to performance.**
- **Relatively simple unit operation models link together to provide qualitatively and in some cases quantitatively excellent predictions of effects and interactions between process parameters and product quality attributes.**
- **This provides an excellent basis for**
  - Improving product and process understanding
  - Education
  - Supporting process optimisation
  - Building control or RTRT models
  - Implementing improved unit operation or product performance models (e.g. in-vivo absorption)
  - Support a move towards continuous manufacture



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