

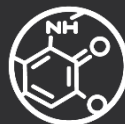


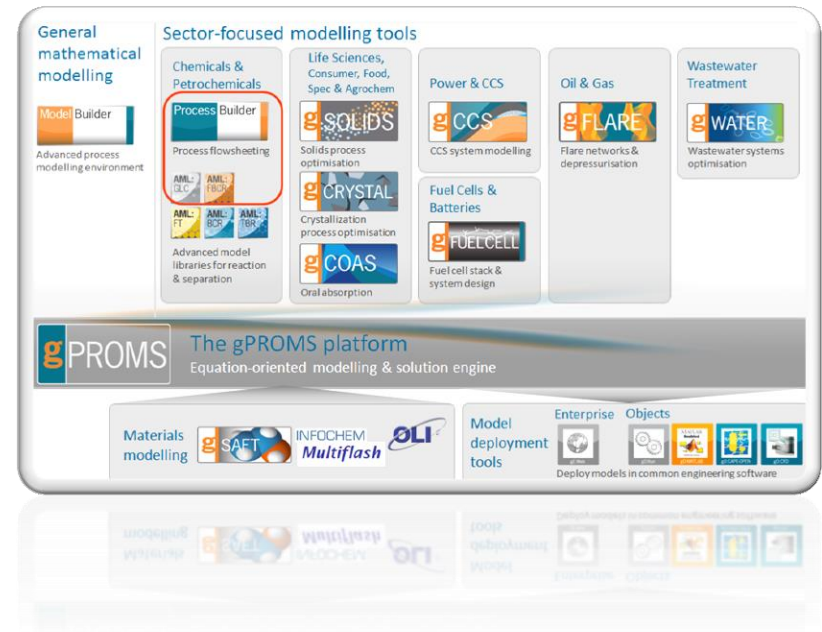
# ADVANCED PROCESS MODELLING FORUM **2014**

## gPROMS ProcessBuilder

Advanced Process Simulation for Chemicals & Petrochemicals

Maarten Nauta – Senior Consultant





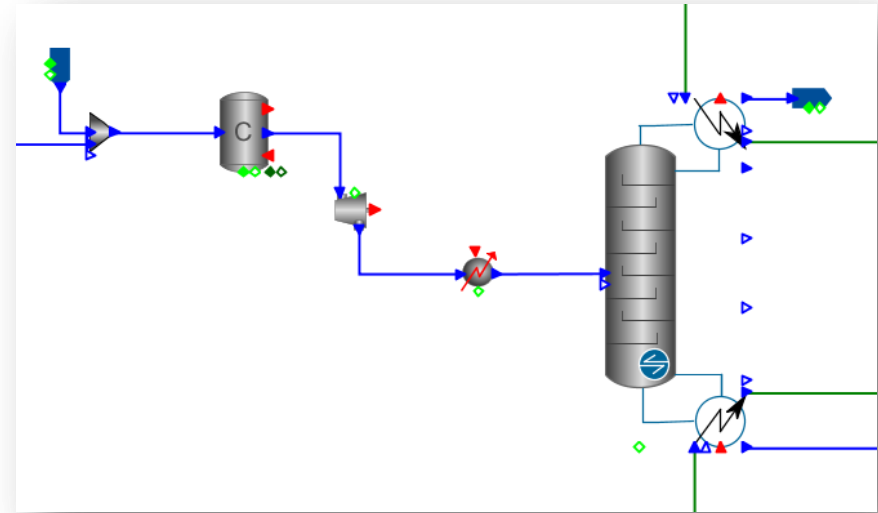
A new product

...based on the gPROMS Platform

...for the **Chemicals & Petrochemicals** sector

...delivering new levels of functionality, usability & efficiency

- Drag-and-drop flowsheeting
- Comprehensive library of unit operation models
- Custom modelling
- Advanced thermodynamics
- Steady-state & dynamic simulation
  - ...and transition from one to the other
- Process optimisation



- **Overview**
  - Dr Maarten Nauta
  
- **Distillation/absorption**
  - Dr Charles Brand
  
- **Pressure Swing Adsorption (PSA)**
  - Dr Mayank Patel
  
- **gSAFT physical properties**
  - Dr Tom Lafitte
  
- **Conclusion & perspective**
  - Prof C.C. Pantelides



- Content
  - Model libraries
- Workflow
  - Steady-state flowsheeting
  - From steady state to dynamics
- Advanced capabilities for flowsheet simulation

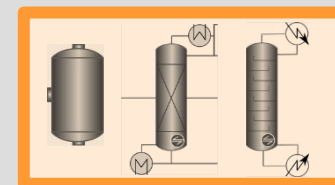
# gPROMS ProcessBuilder Model libraries

Separations – Fluid-Fluid	Steady-state	Dynamic
Component splitter	<input checked="" type="checkbox"/>	
Flash drum	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Decanter	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
3-phase separator	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Distillation column (tray, equilibrium)	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Distillation column (packed-bed, HETP)	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Distillation column (packed-bed, 1D rate-based)	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Distillation column (packed-bed, 2D rate-based)	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Distillation column (reactive)	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>

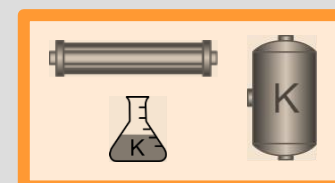
Separations – Adsorption	Steady-state	Dynamic
Adsorption bed		<input checked="" type="checkbox"/>
Schedule for periodic processes (PSA, TSA)		<input checked="" type="checkbox"/>
Schedule for self-interacting bed approach		<input checked="" type="checkbox"/>

Separations – Membranes	Steady-state	Dynamic
Membrane module	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>

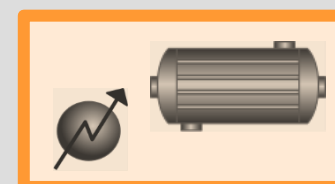
## Separation



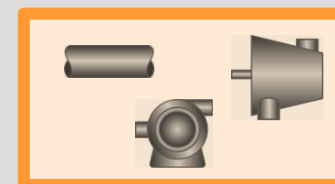
## Reaction



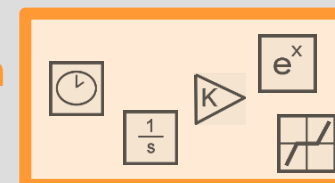
## Heat exchange



## Flow transportation

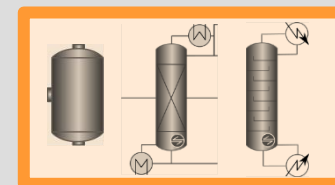


## Instrumentation and control

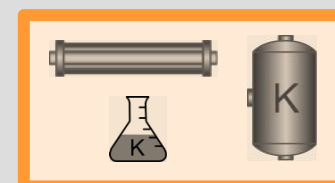


Reaction	Steady-state	Dynamic
Conversion reactor	<input checked="" type="checkbox"/>	
Gibbs reactor	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
CSTR (kinetic & equilibrium reactions)	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
PFR (kinetic & equilibrium reactions)	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Fixed-bed catalytic reactor (1D)	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Fixed-bed catalytic reactor (2D)	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Fixed-bed catalytic reactor (2D + intra-particle)	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Reaction mechanisms:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
<ul style="list-style-type: none"> <li>Arrhenius</li> <li>Langmuir-Hinshelwood</li> <li>Michaelis-Menten</li> <li>User specified</li> </ul>		

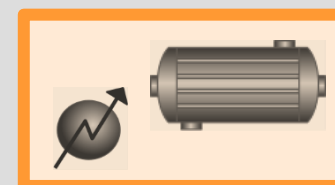
## Separation



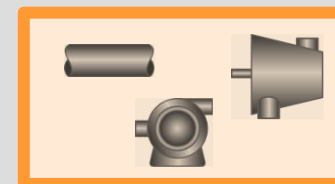
## Reaction



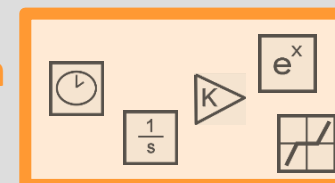
## Heat exchange



## Flow transportation



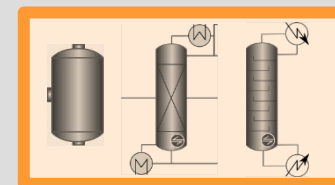
## Instrumentation and control



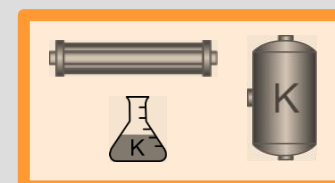


Heat exchange	Steady-state	Dynamic
Heater	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Cooler	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Two-stream heat exchanger	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Multi-stream heat exchanger	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>

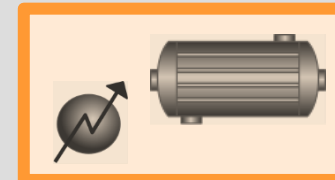
## Separation



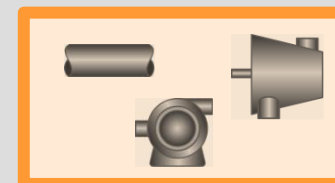
## Reaction



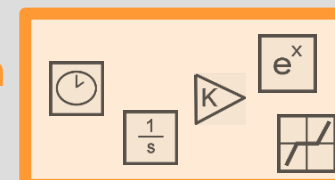
## Heat exchange



## Flow transportation



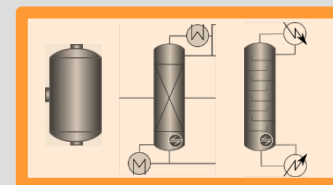
## Instrumentation and control



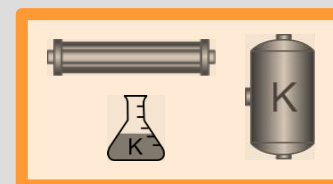
Flow transportation	Steady-state	Dynamic
Pipe	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Pump	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Valve	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>

Compression	Steady-state	Dynamic
Compressor	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Expander	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Compressor section	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Electric drive	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Surge valve	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>

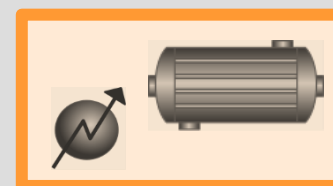
## Separation



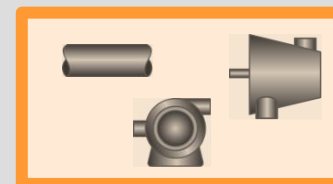
## Reaction



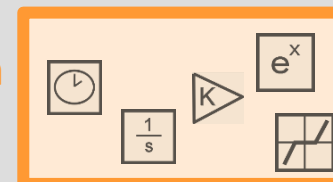
## Heat exchange



## Flow transportation

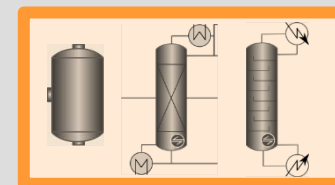


## Instrumentation and control

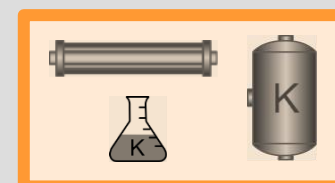


Instrumentation and control	Steady-state	Dynamic
<b>Controllers</b> <ul style="list-style-type: none"> <li>Gain, PID, delays</li> </ul>	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
<b>Logic</b> <ul style="list-style-type: none"> <li>Switches</li> </ul>	<input checked="" type="checkbox"/>	
<b>Linear systems</b> <ul style="list-style-type: none"> <li>Transfer function, state-space model</li> </ul>		<input checked="" type="checkbox"/>
<b>Discrete</b> <ul style="list-style-type: none"> <li>Dead zone, hysteresis, saturation</li> </ul>	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
<b>Mathematics</b> <ul style="list-style-type: none"> <li>Functions, basic operations</li> </ul>	<input checked="" type="checkbox"/>	
<b>Signal Sources</b> <ul style="list-style-type: none"> <li>Constant, ramp, step signal, function generator, time signal</li> </ul>	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
<b>Signal Sinks</b> <ul style="list-style-type: none"> <li>Display, plot, X-Y plot</li> </ul>	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
<b>Data</b> <ul style="list-style-type: none"> <li>Lookup table, file read, file write</li> </ul>	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
<b>Functionality</b> <ul style="list-style-type: none"> <li>System identification, linearisation,</li> <li>Mixed-integer optimisation</li> </ul>	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>

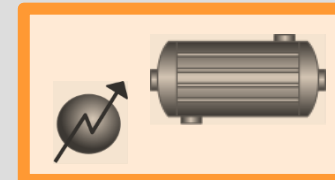
## Separation



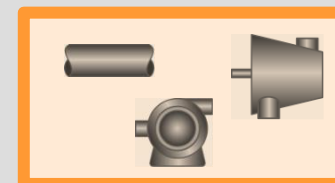
## Reaction



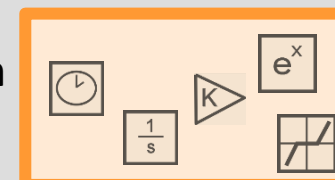
## Heat exchange



## Flow transportation



## Instrumentation and control



## I. Separation

- fluid/fluid: distillation, absorption
- fluid/solid: adsorption, membrane

## II. Reaction

## III. Heat exchange

## IV. Flow transportation

## V. Instrumentation & control

## VI. Custom models & model libraries

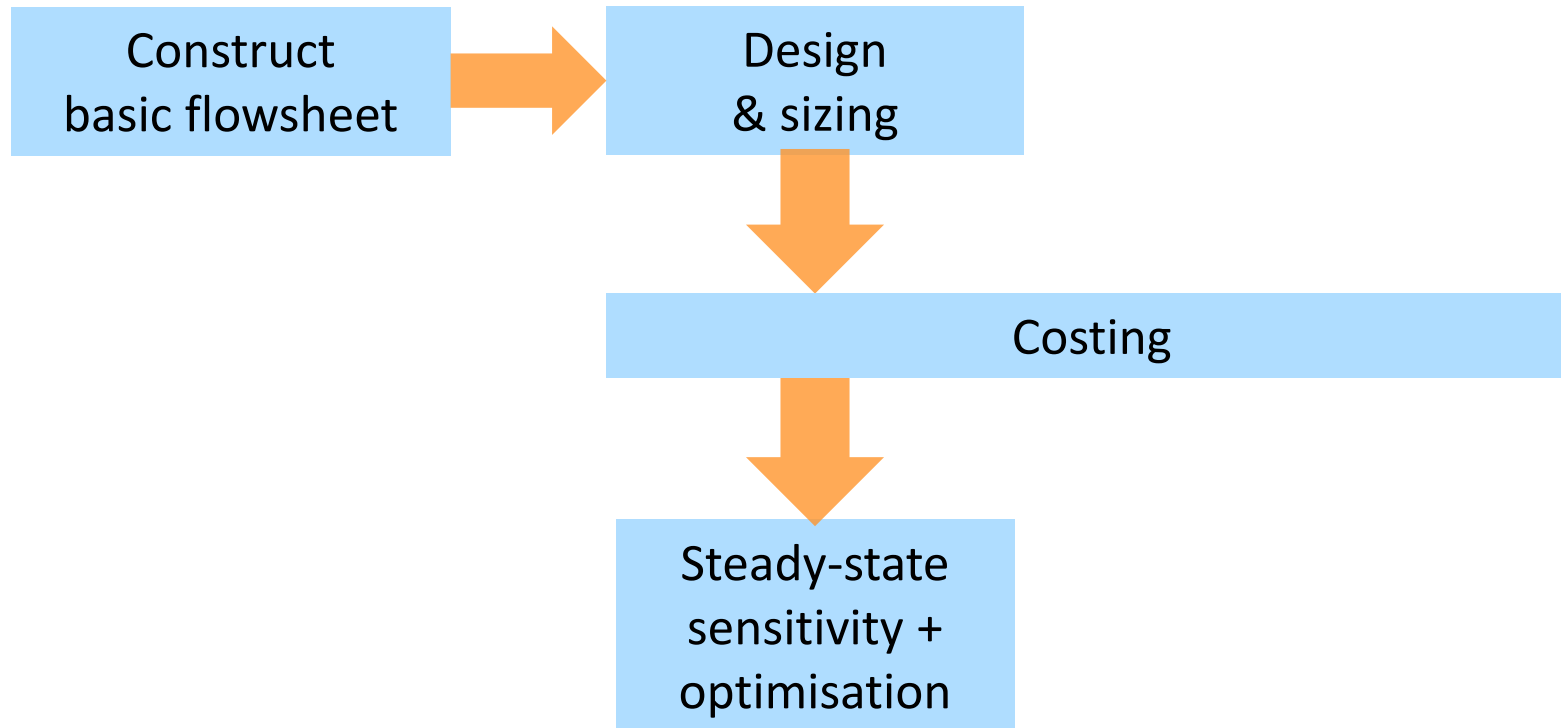
- proprietary, third-party, ....



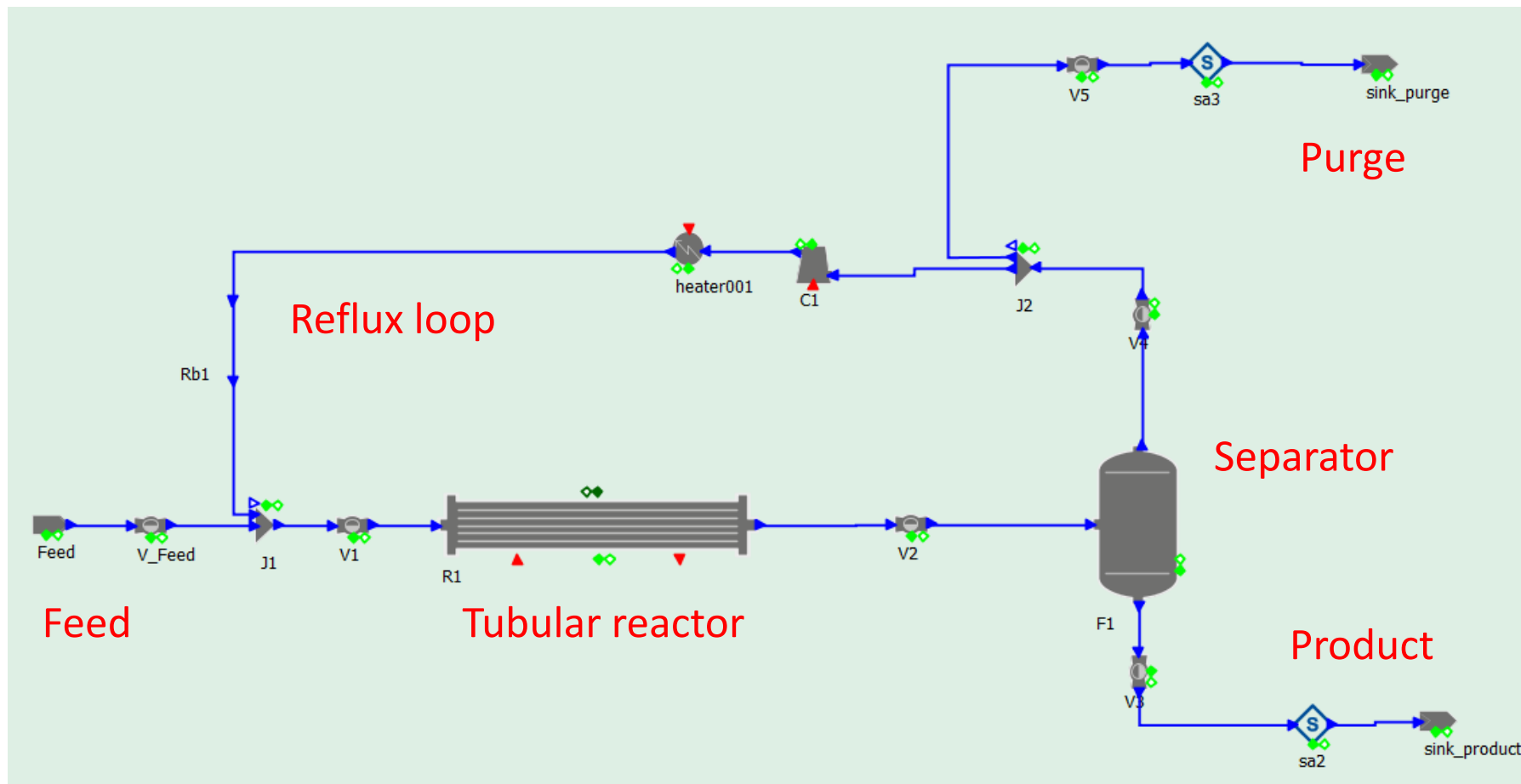
# gPROMS ProcessBuilder

## Steady-state flowsheeting





# Example: Methanol production

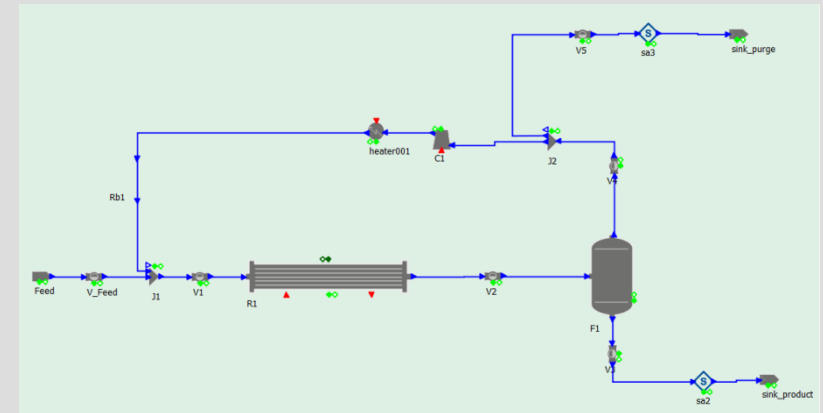


# 1. Basic mass & energy balances

- Drag & drop models on the flowsheet
- Enter output specifications for model in dialogs



- Determine process mass & energy balances
- [Video](#)



V1 (JT\_Valve)

Specify

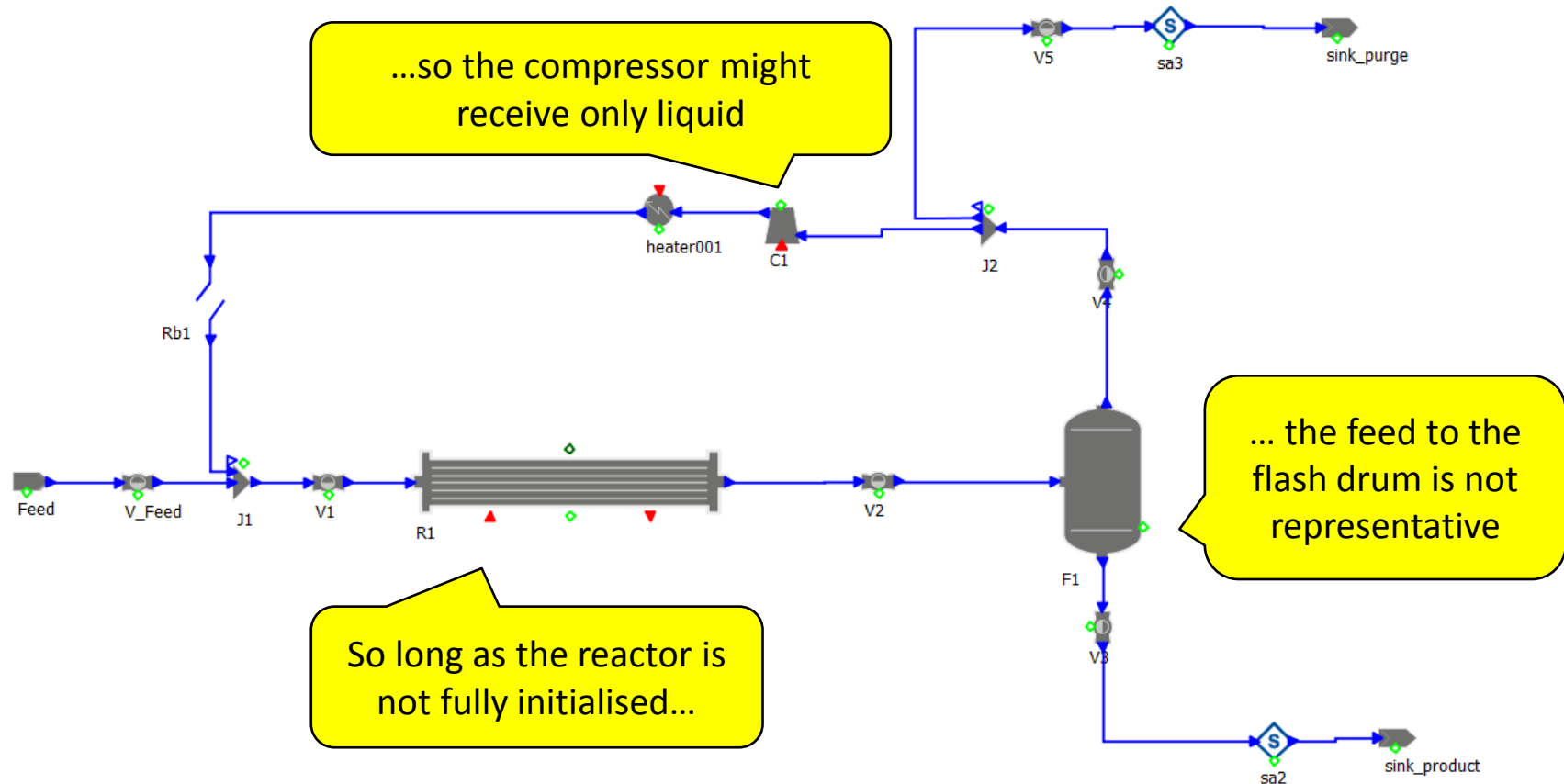
Outlet specification: Pressure

☒ Pressure: 148 bar

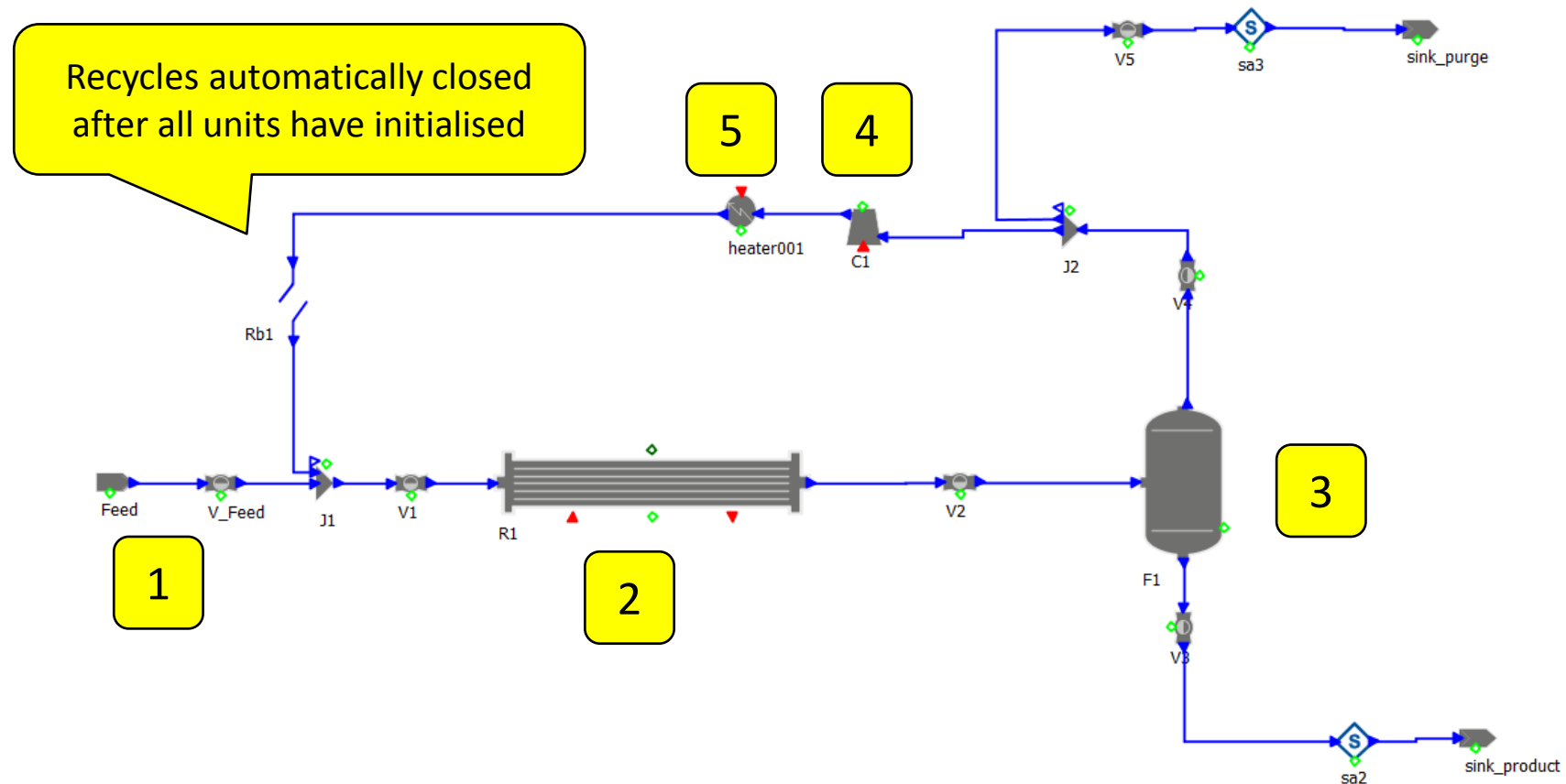
Main | Design | Operation | Dynamics | Reporting | Numerics

OK Cancel Reset all

**Problem:** In equation-based flowsheet model initialisation, during the first steps, unit operation models are sometimes “fed” with a non-physical feed



## Solution: initialise flowsheet sequentially





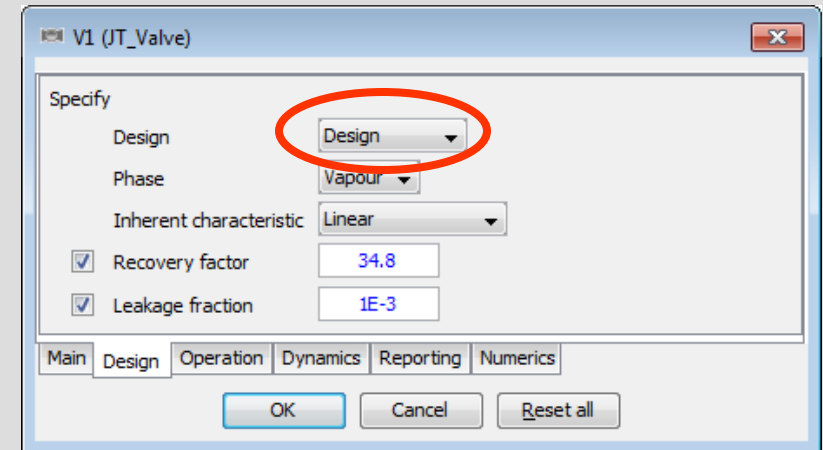
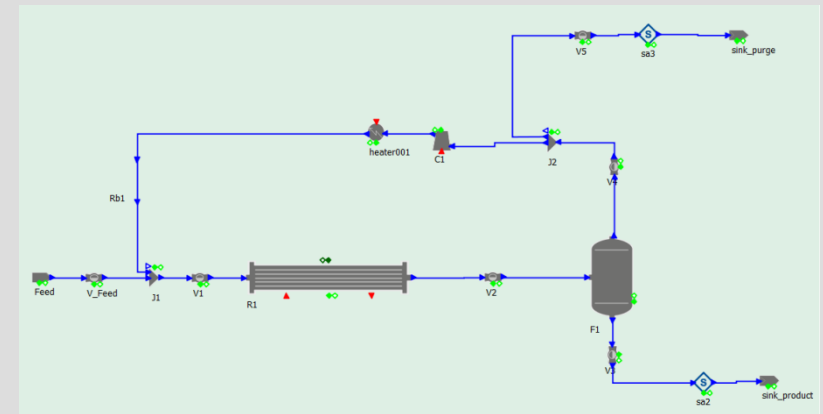
## 2. Sizing

- Switch unit operations to *design* mode
- Refine unit specifications
  - e.g. choose specific type of equipment
- Impose performance specs
  - e.g. separation to be achieved



- Determine
  - sizing
  - operating point

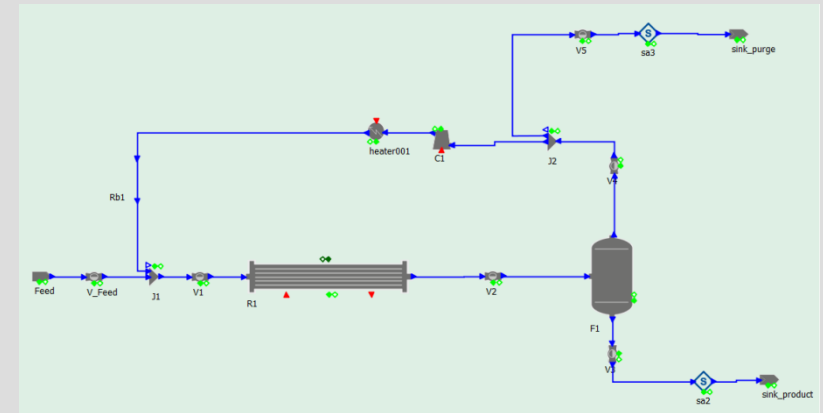
- Video



- Switch unit operations to *performance* mode



- Determine process performance for given input specifications



V1 (JT\_Valve)

Specify

Design **Performance**

Phase Vapour

Inherent characteristic Linear

☒ Vapour valve coefficient 200  $\text{m}^3 \text{s}^{-1} \text{Pa}^{-0.5}$

☒ Recovery factor 34.8

☒ Leakage fraction 1E-3

Main Design Operation Dynamics Reporting Numerics

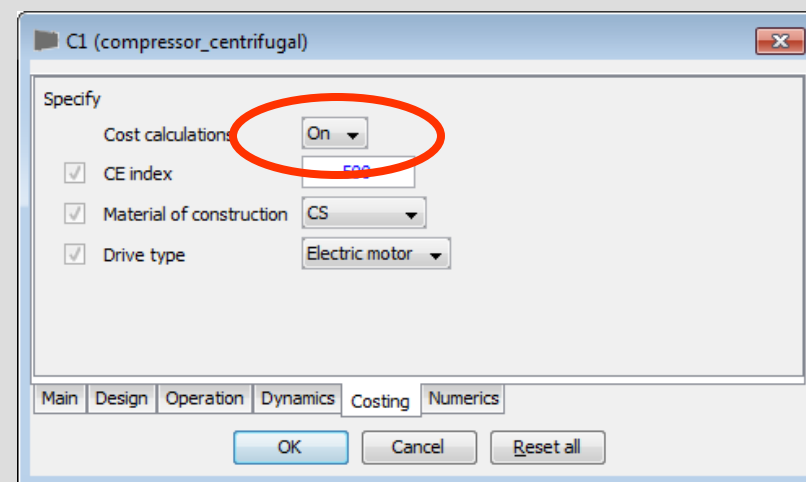
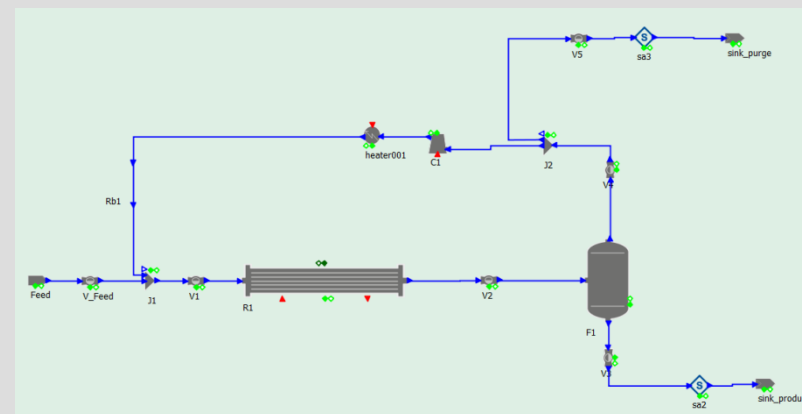
OK Cancel Reset all

## 4. Costing

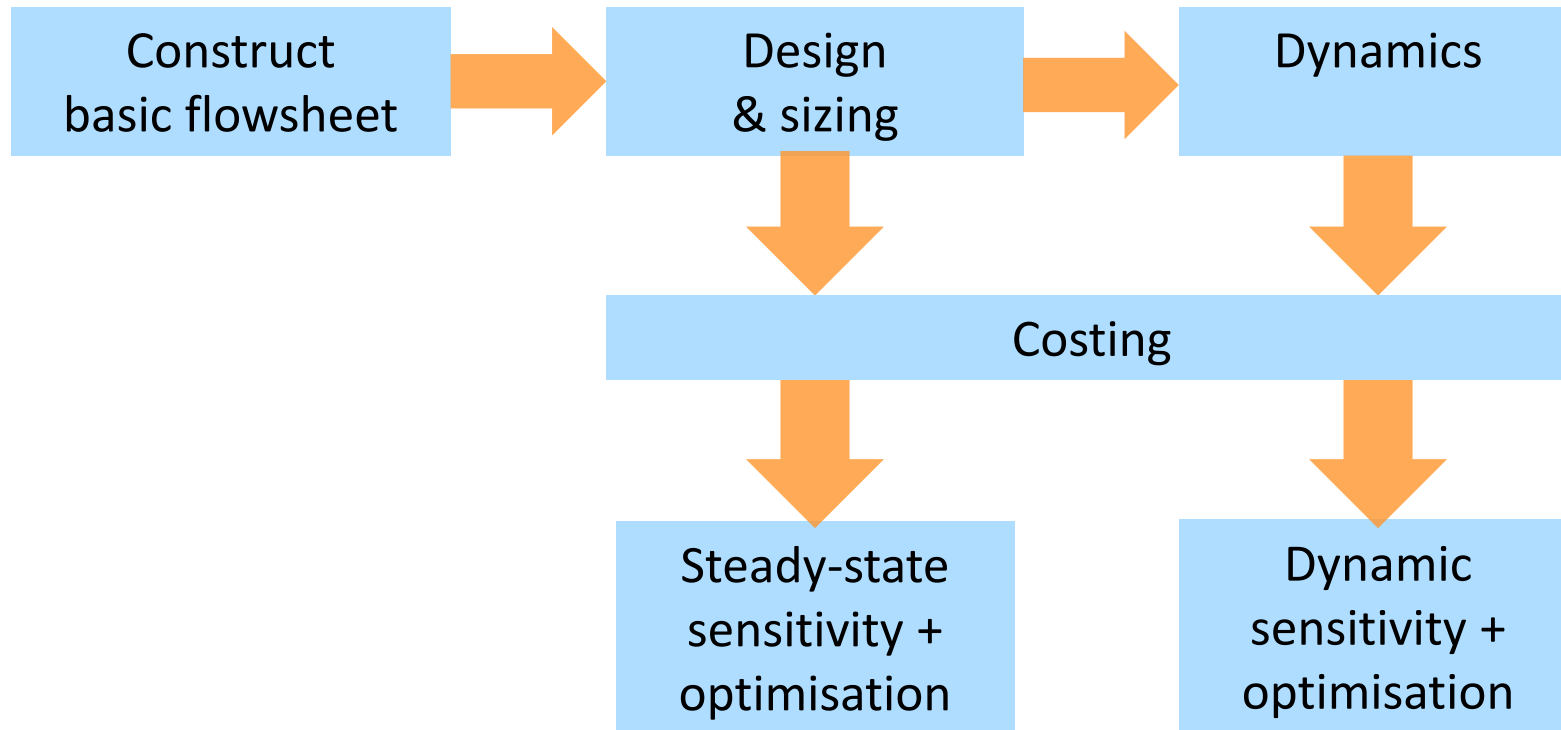
- Switch unit operations to *costing* mode
  - models incorporate fixed & variable cost calculations



- Simulation: Compute cost for given specifications
- Optimisation: minimise cost by adjusting process design and operation parameters



# From steady state to dynamics

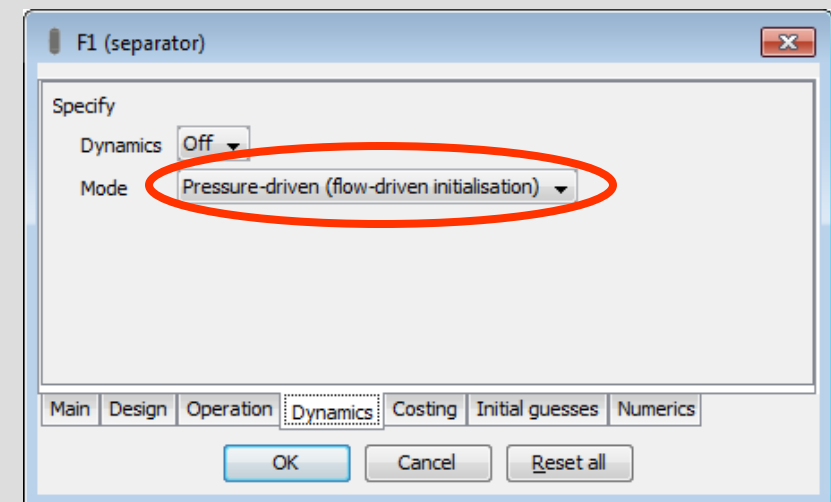
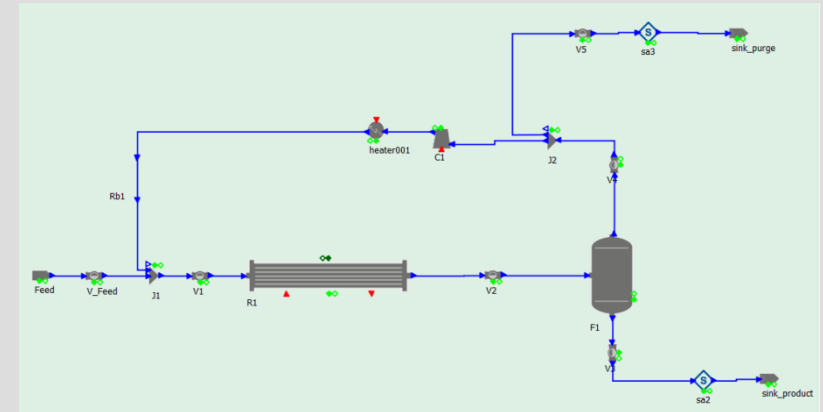




- Switch all units to *pressure-driven* mode
- Specify downstream pressures



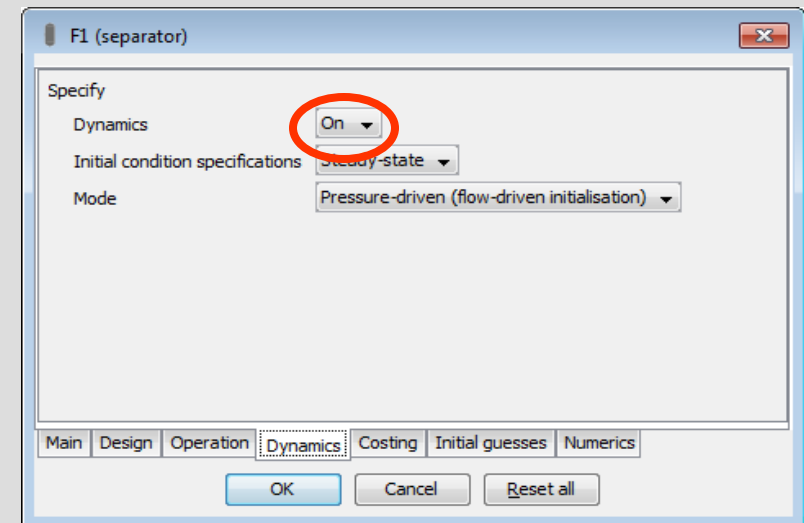
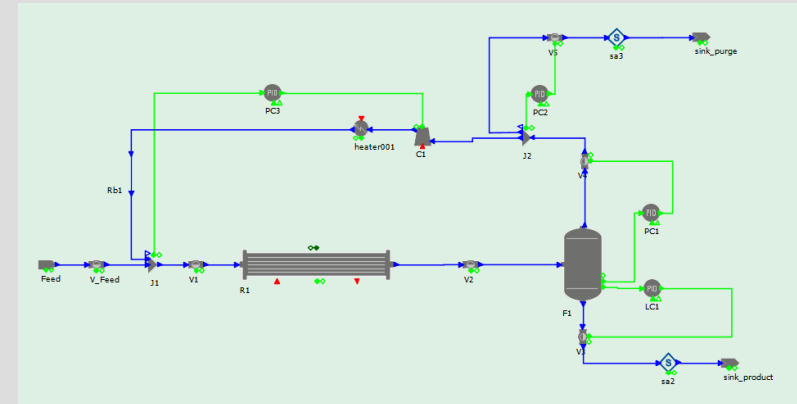
- Determine pressure-driven steady-state operating point
- Video



- Switch all units to *dynamic* mode
- Add controllers to enforce unit outlet specifications



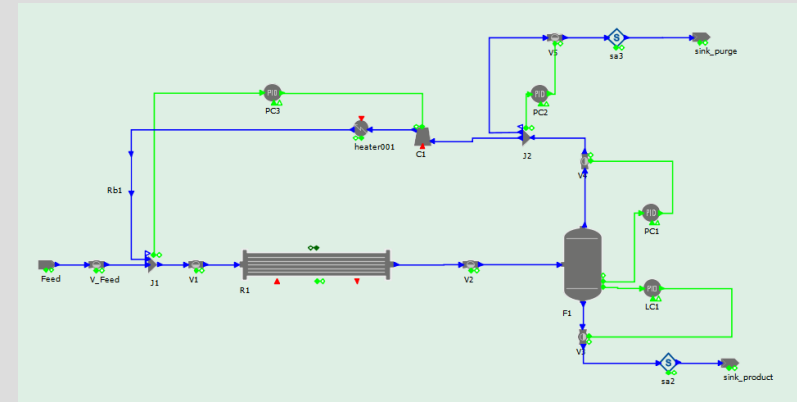
- Fully dynamic flowsheet
  - use steady state as default initial condition...
- Video dynamic no control
- Video dynamic control



- Switch all units to *dynamic* mode
- Add controllers to enforce unit outlet specifications



- Fully dynamic flowsheet
  - use steady state as default initial condition...
  - ...or specify initial condition via dialog



F1 (separator)

Specify

Dynamics: On

Initial condition specifications: Dynamic

Initial holdup: Composition (w) and intensive variable (P,T,H)

Mode: Flow-driven

Intensive variable specification: Temperature

Holdup specification: Mass

Initial thermal specification: Pressure

☒ Temperature: 300.0 K

☒ Pressure: 1.0 bar

☒ Mass fraction: ☐ Uniform for entire array ☒ Per element

Components	
HYDROGEN	
CARBONMONOXIDE	
METHANOL	

kg/kg

Main Design Operation Dynamics Costing Initial guesses Numerics

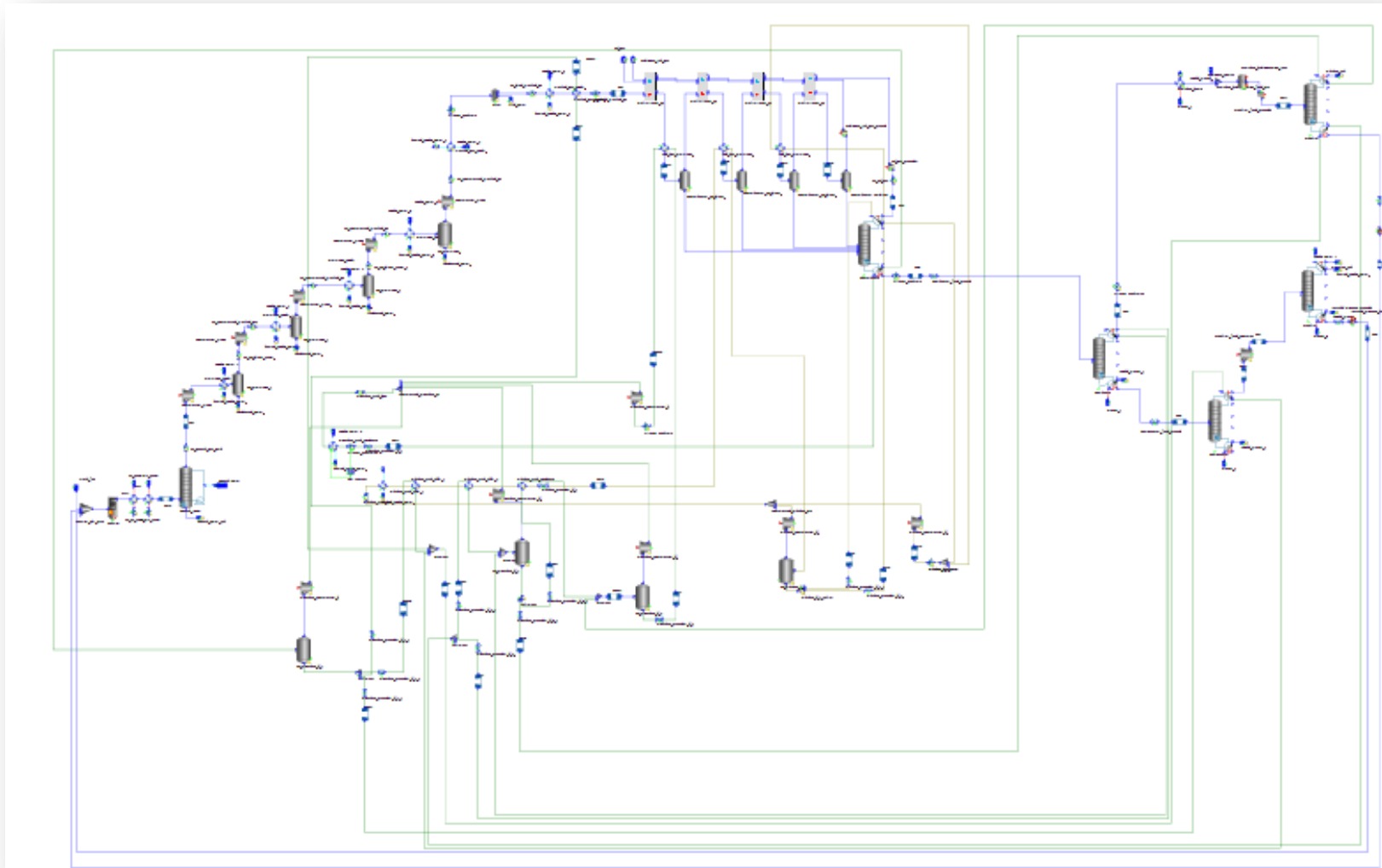
OK Cancel Reset all

# gPROMS ProcessBuilder

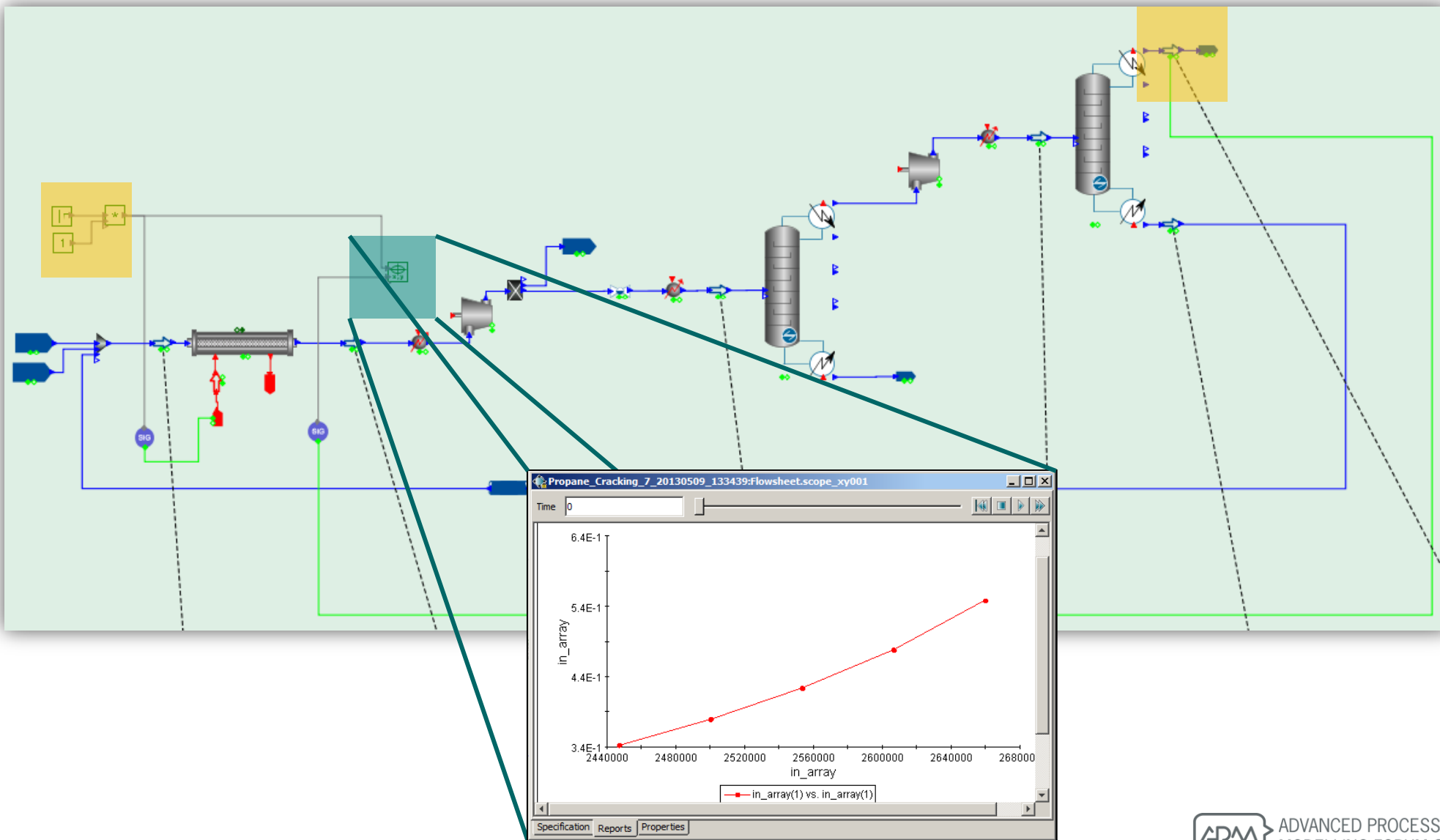
## Advanced capabilities for flowsheet simulation

# Complex flowsheets with multiple recycles

- Ethylene plant model with refrigeration, 70k+ equations

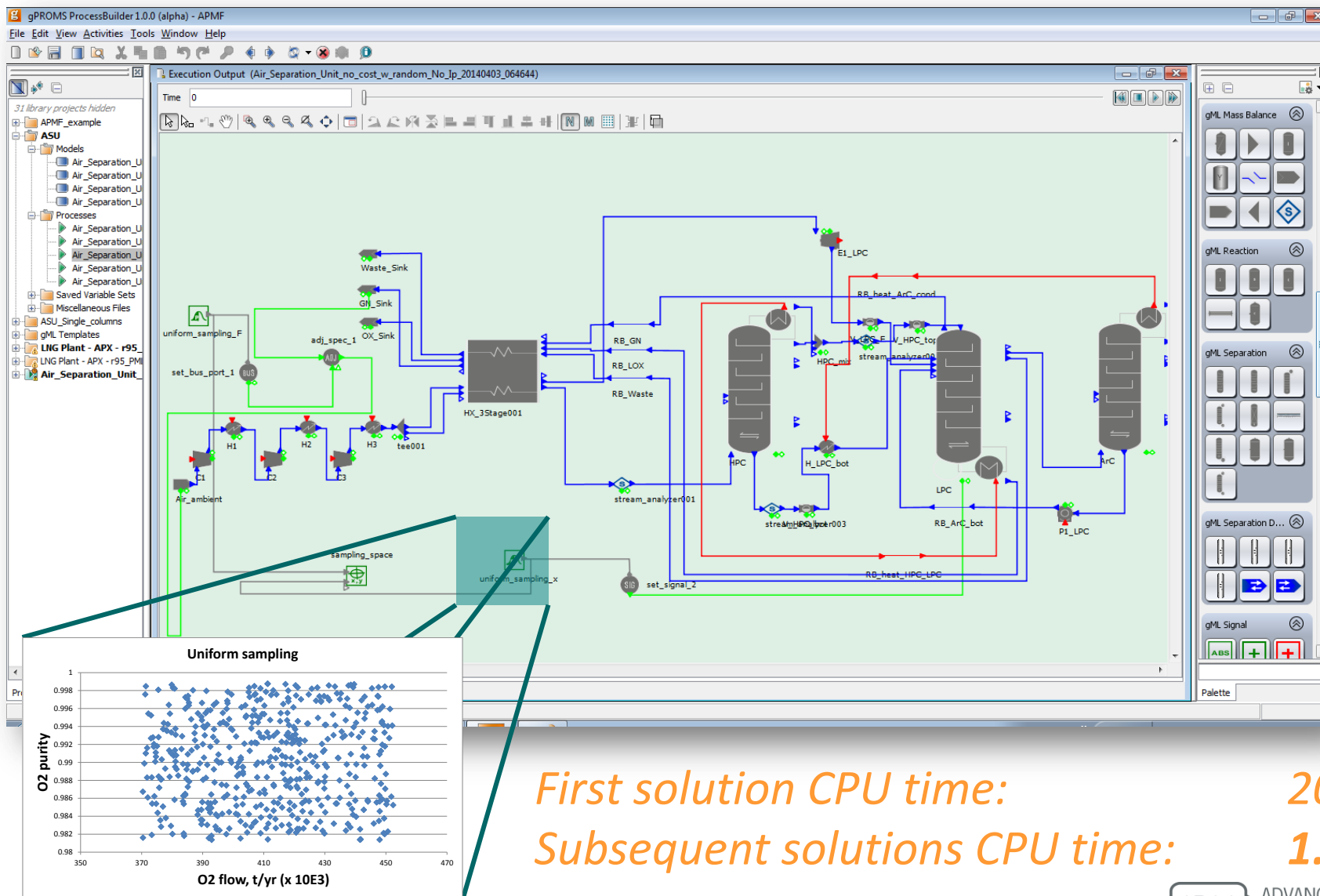






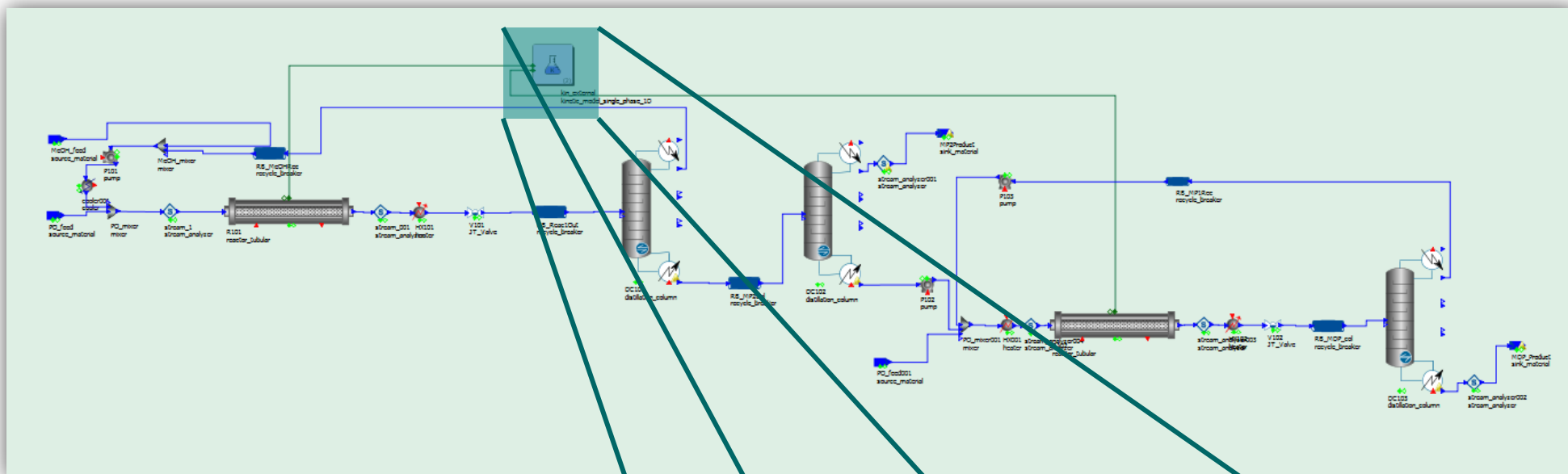
# gPROMS ProcessBuilder Sensitivity studies – II

Process Builder



# gPROMS ProcessBuilder Integration with custom models

Process Builder



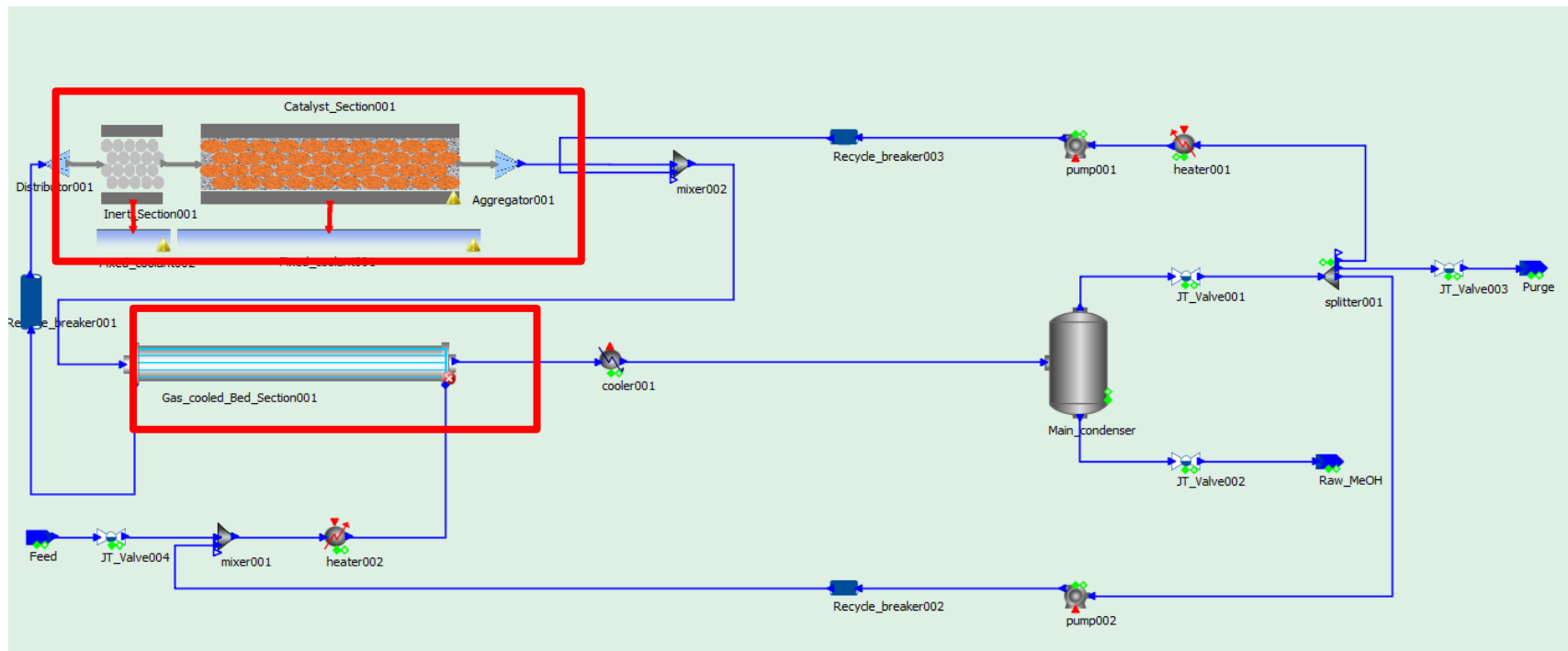
*Add custom models easily using the  
gPROMS language*

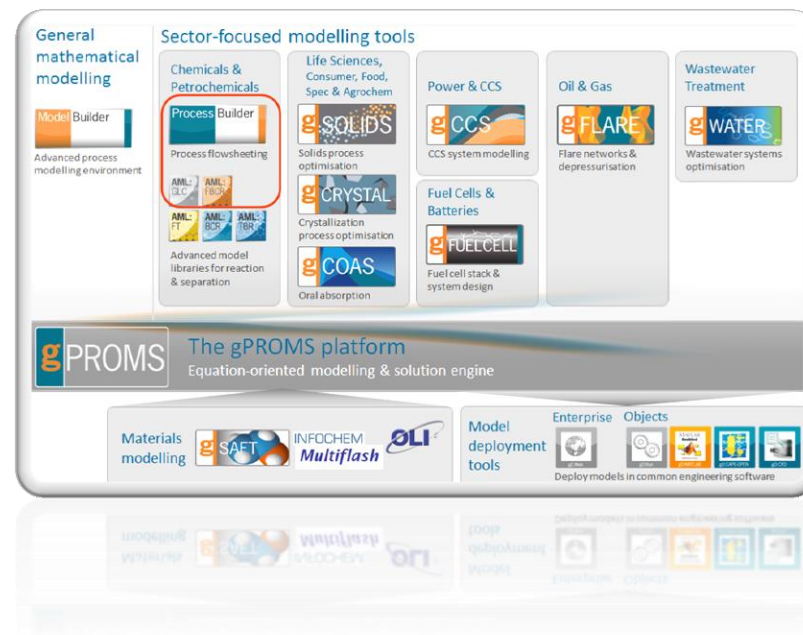
*Templates for constructing  
ProcessBuilder -compliant  
custom models  
provided*

```
kinetic_model_single_phase_1D (PML-SS Components Reaction)
END # FOR z := 0 TO 1 DO
# Equilibrium reactions
#---
FOR z := 0 TO 1 DO
CASE equilibrium_constants_spec OF
WHEN concentration:
CASE reaction_rate_base_eq OF
WHEN molar_mode:
FOR j IN Reactions_equilibrium DO
CASE reaction_switch OF
WHEN reactions_off:
Reaction_rate(j,z) = 0 ; # mol/m3/s
WHEN reactions_on:
(1/eq_const_scale) * Equilibrium_constants(j,z) = (1/eq_con
END # CASE initialisation_mode OF
END # FOR j IN Reactions DO
WHEN mass_mode:
FOR j IN Reactions_equilibrium DO
CASE reaction_switch OF
WHEN reactions_off:
```

*Advanced Model Libraries now integrated within ProcessBuilder*

- *AML:FBCR*
- *AML:GLC*





A new product

...based on the gPROMS Platform

...for the **Chemicals & Petrochemicals** sector

...delivering new levels of functionality, usability & efficiency



- Overview
  - Dr Maarten Nauta
  
- **Distillation/absorption**
  - **Dr Charles Brand**
  
- Pressure Swing Adsorption (PSA)
  - Dr Mayank Patel
  
- gSAFT physical properties
  - Dr Tom Lafitte
  
- Conclusion & perspective
  - Prof C.C. Pantelides

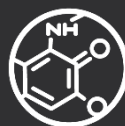




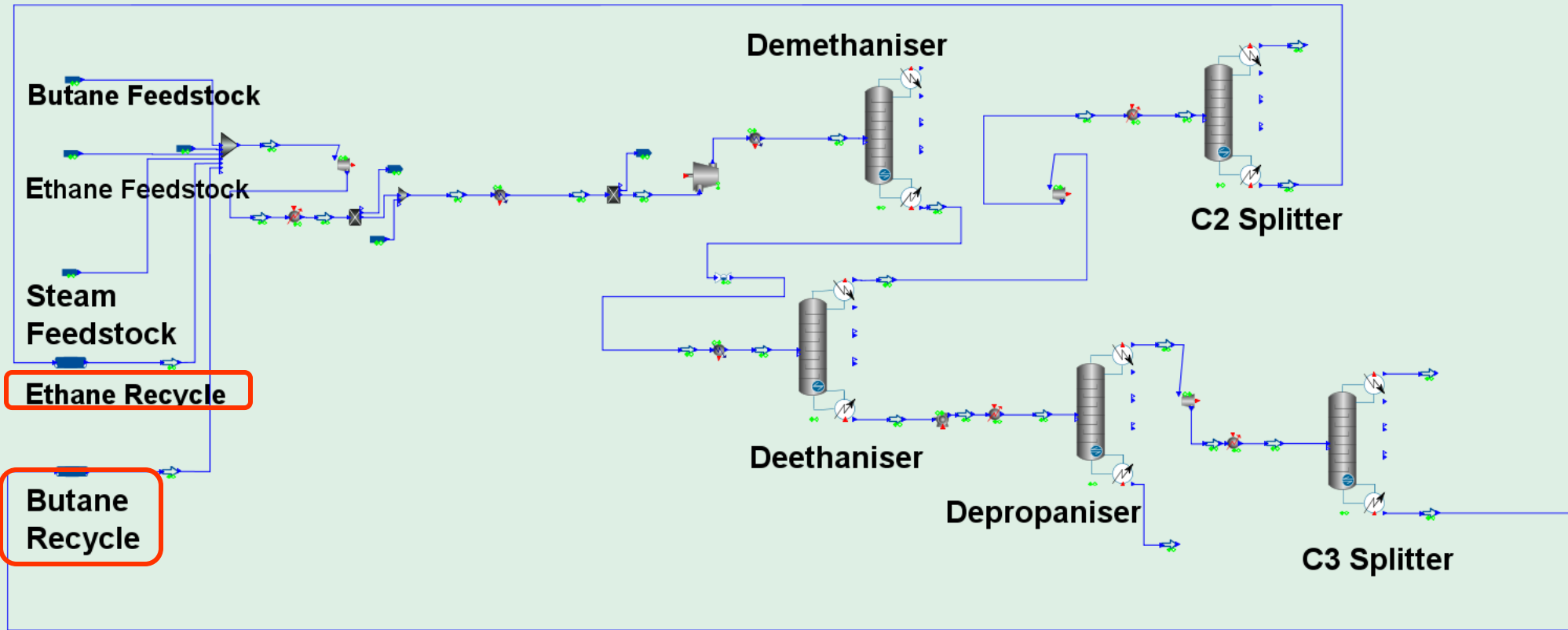
ADVANCED PROCESS  
MODELLING FORUM **2014**



Thank you



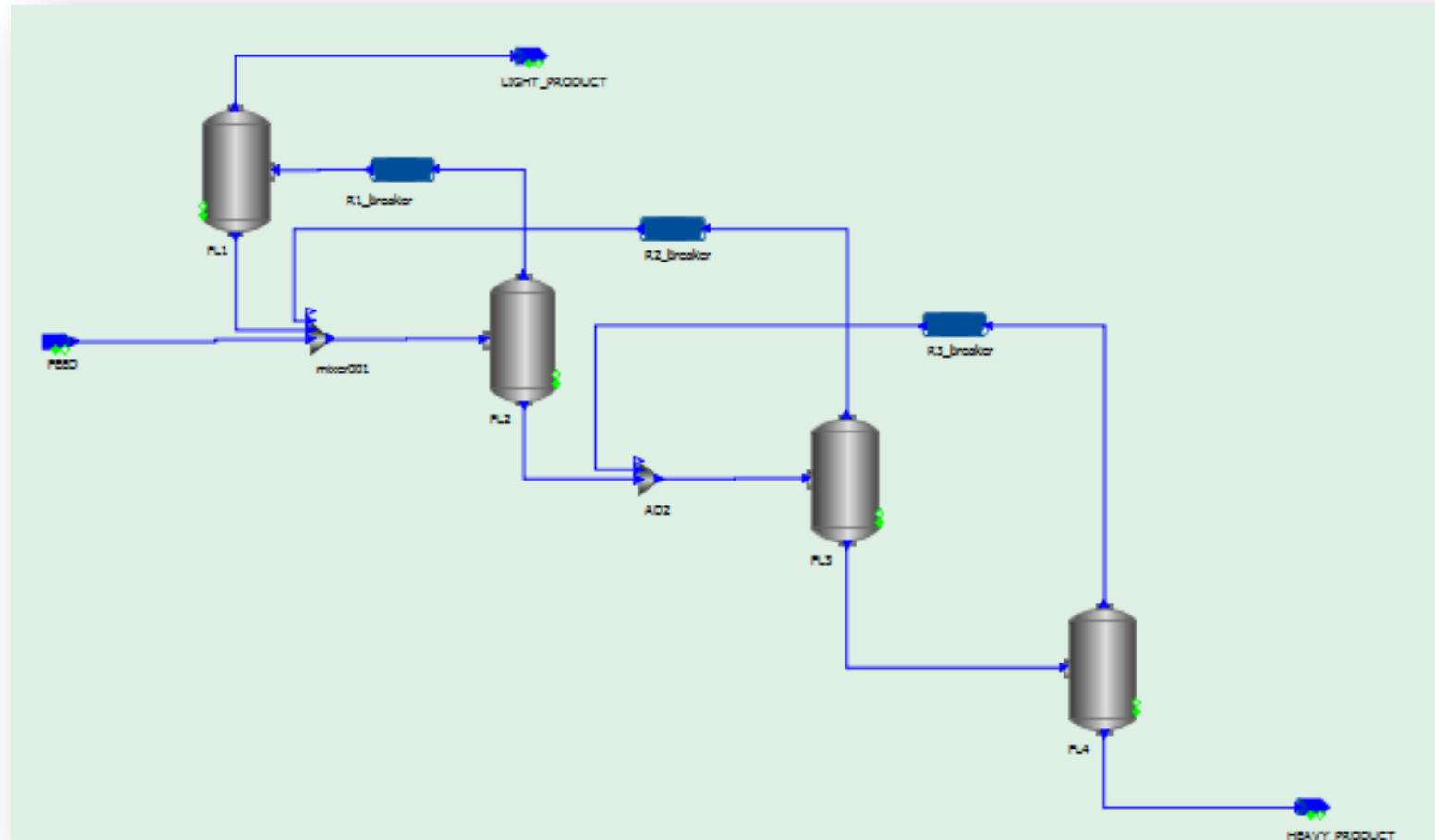
- Solution time with no user-provided initial guesses: 37 CPU s (Intel i7 laptop)



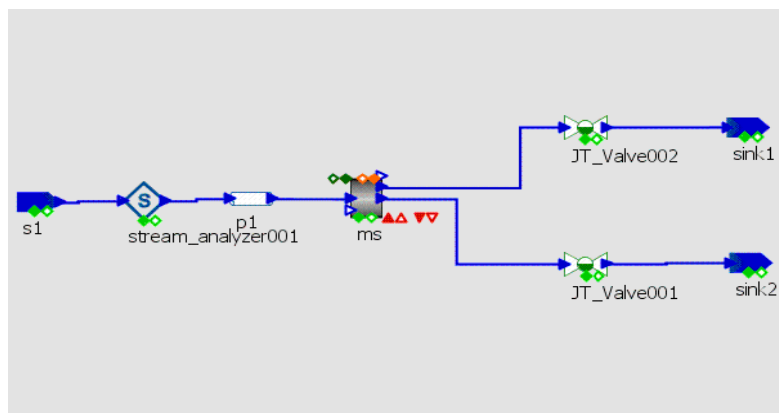
K. Y. Cheung, *Site-wide and supply chain optimisation for continuous chemical processes*,  
PhD thesis, Imperial College, 2008

# Basic steady-state flowsheeting

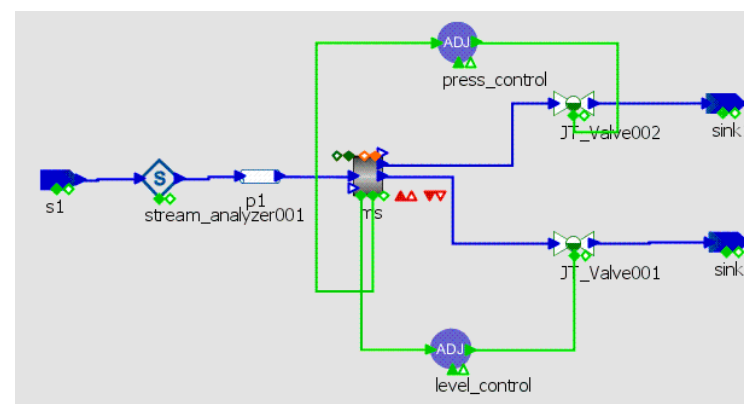
## ■ Cavett problem



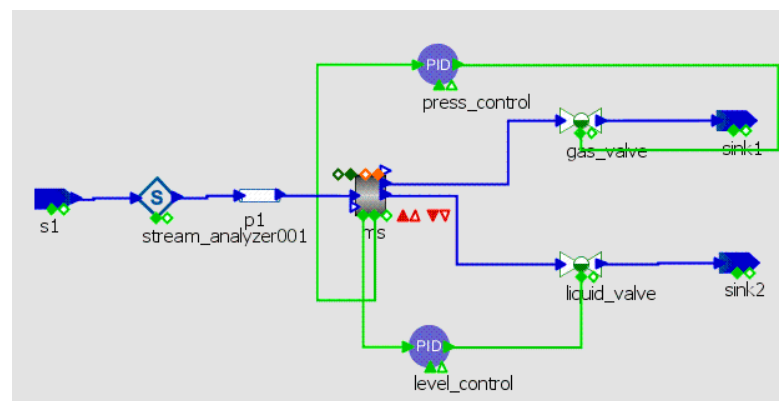
## Transition from steady-state to dynamics



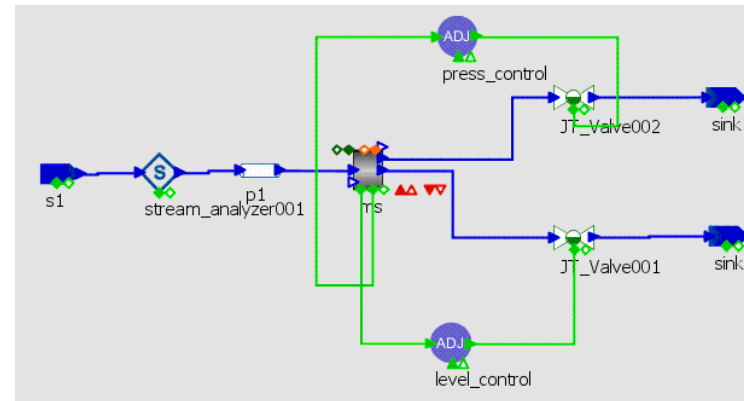
Flow-driven steady-state flowsheet



Flow-driven steady-state flowsheet with design specifications



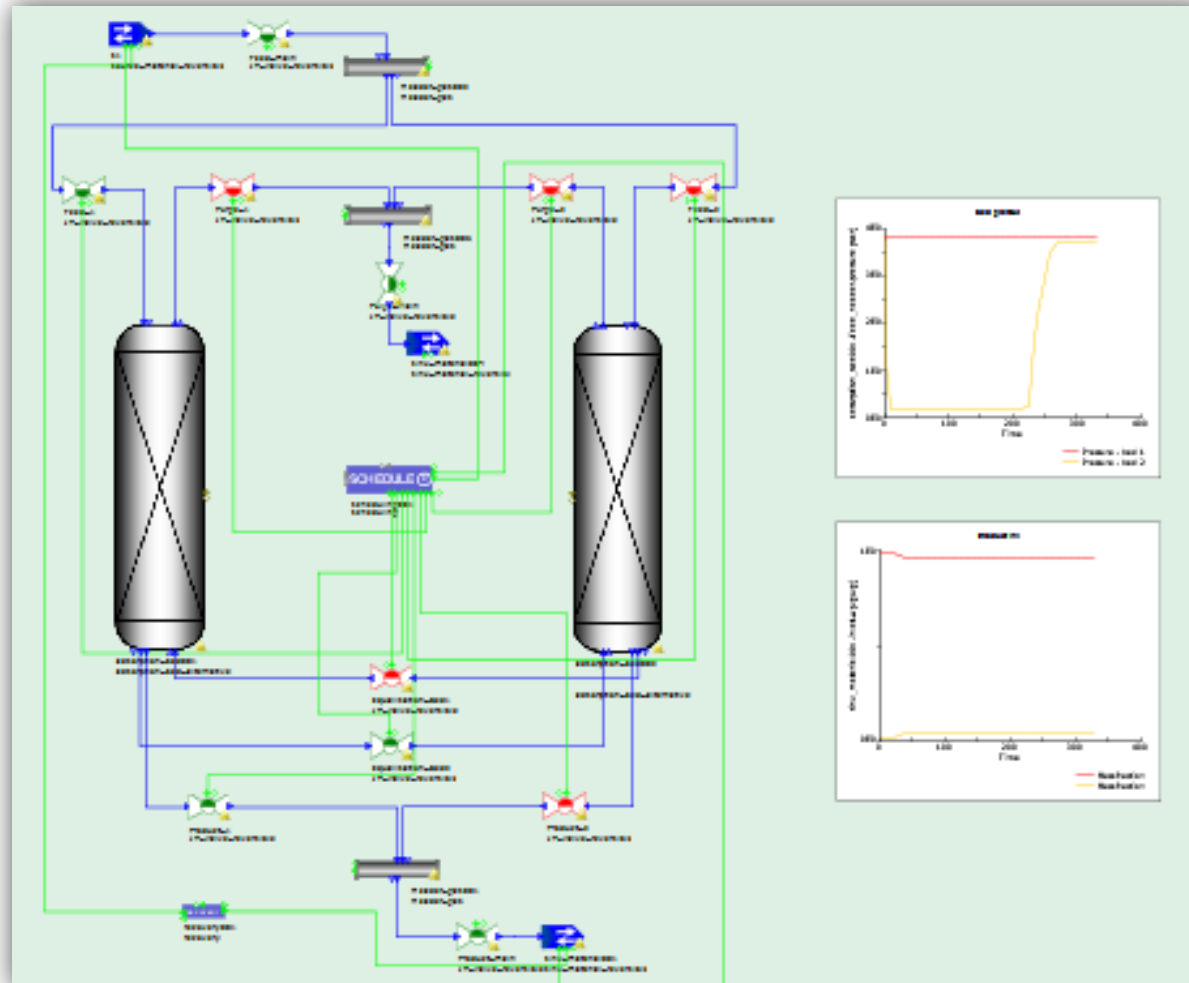
Pressure-driven **dynamic** flowsheet at **steady-state** with control



Pressure-driven steady-state flowsheet with design specifications

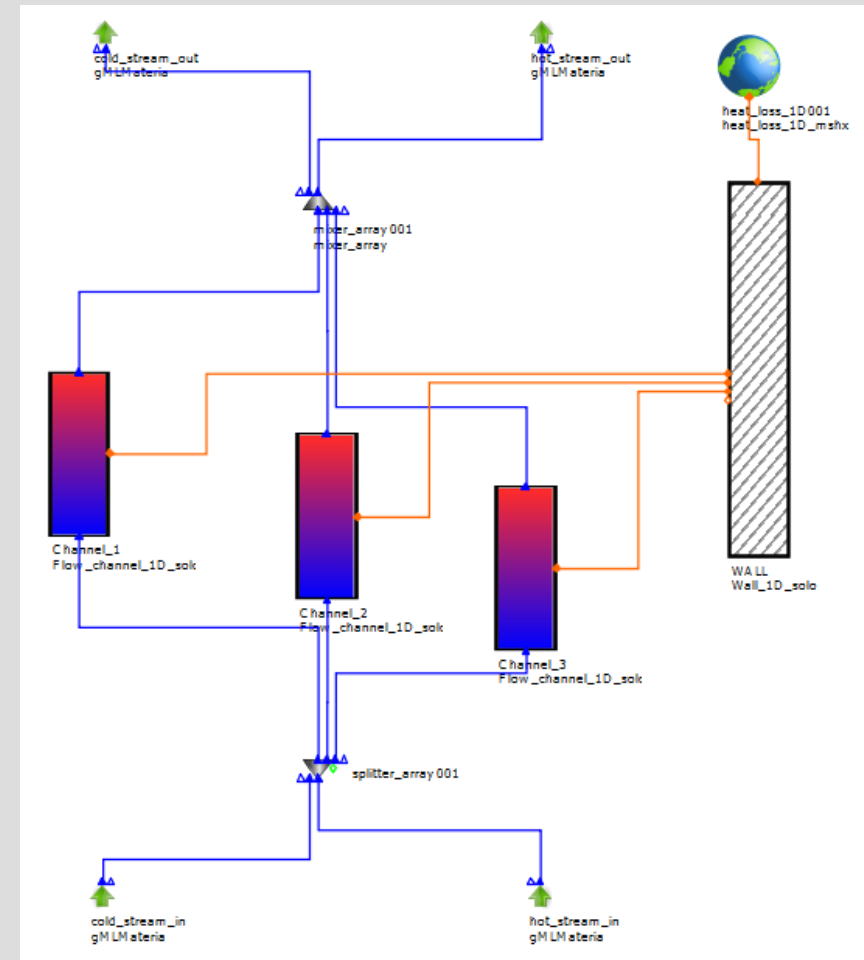


## Dynamic applications, Pressure Swing Adsorption (PSA)

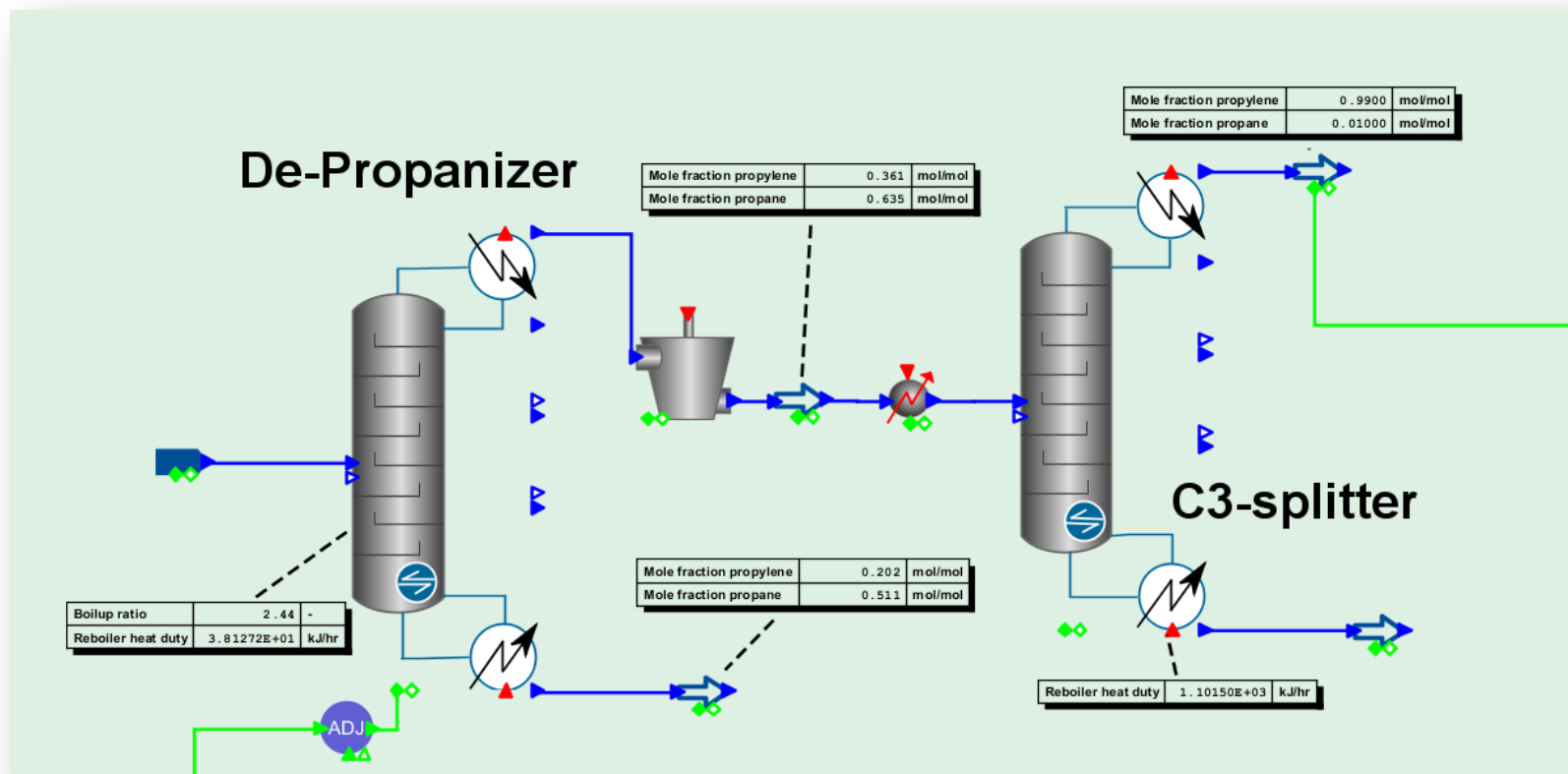


## ■ Detailed design of individual unit operations using flowsheeting

- Multistream heat exchanger
- Multilayer adsorption bed
- Fixed bed-catalytic reactor configurations
- Custom distillation column configurations







adj\_spec001 (adj\_spec)

Specify

Target variable type: Ordered set

Value for target variable: Specified here

☒ Target variable: Molar Fraction

☒ Target variable element index: PROPYLENE

☒ Target value: 0.99

Target Adjust (Initial guesses) Numerics

OK Cancel Reset all

adj\_spec001 (adj\_spec)

Specify

Adjusted variable type: Scalar

☒ Adjust signal variables: Boilup molar ratio

☒ Adjusted variable initial guess: 3

Target Adjust (Initial guesses) Numerics

OK Cancel Reset all

adj\_spec001 (adj\_spec)

Specify

Operation mode: Initialisation procedure

Initialisation procedure: Automatic (Robust)

☐ Typical values for target variable: 1

☐ Typical value for adjusted variable: 1

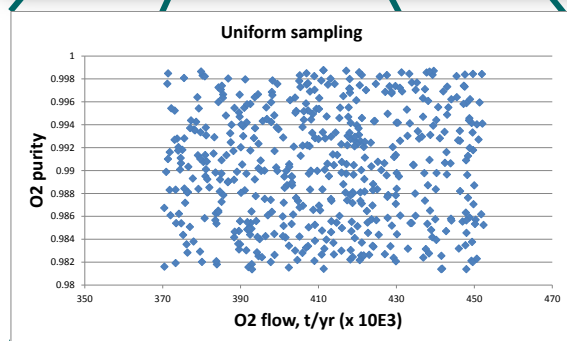
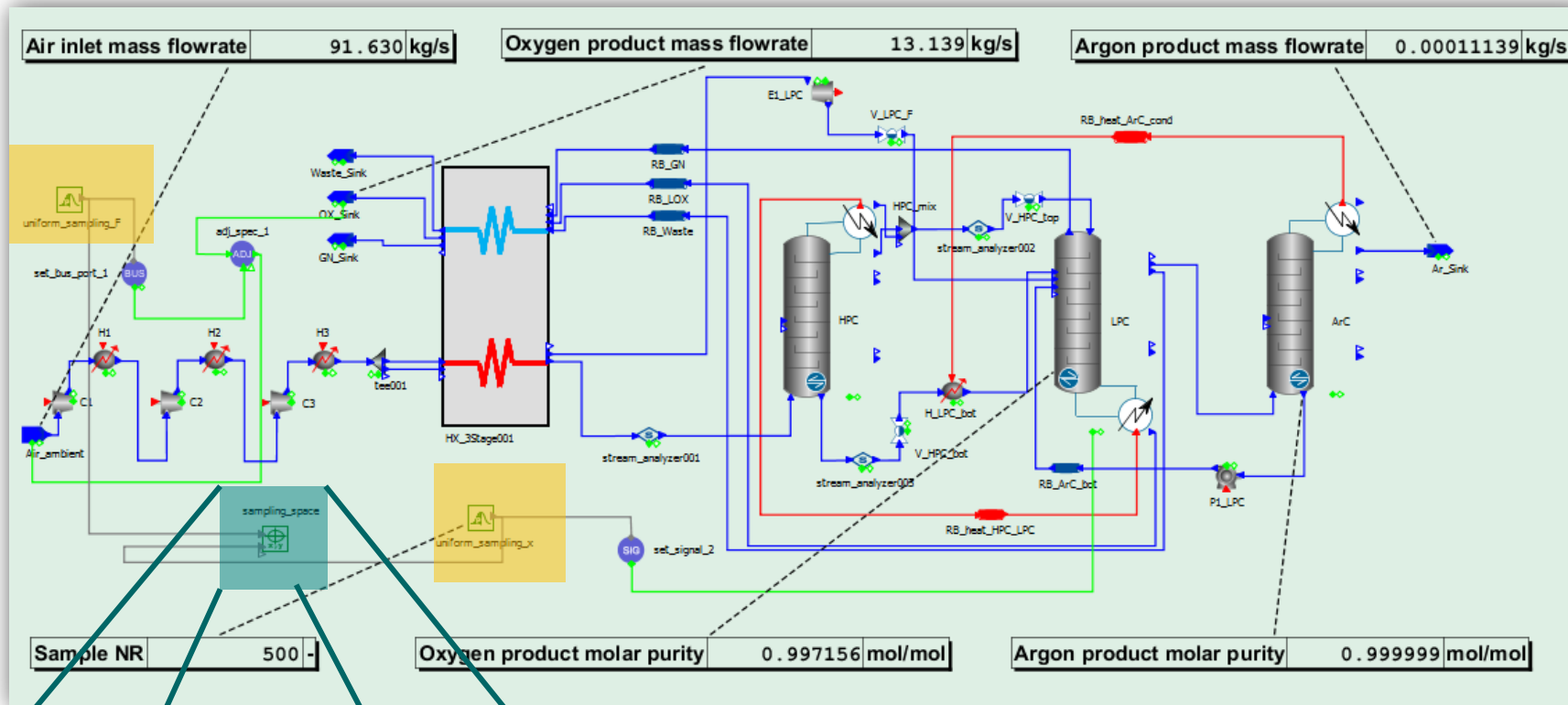
Target Adjust (Initial guesses) Numerics

OK Cancel Reset all

# gPROMS ProcessBuilder

## Sensitivity studies – II

Process Builder



First solution CPU time:

200 sec

Subsequent solutions CPU time:

1.5 sec

# ProcessBuilder key benefits

- Rapidly construct flowsheet models of a wide array of chemical processes
  - Drag-and-drop construction of flowsheets
  - Easy configuration of unit models
- Built-in optimisation capability
- Seamless integration with custom modelling
  - Processes with custom unit operations
  - Detailed characterisation of kinetics, mass transfer, isotherms....
  - Custom cost calculations
- Steady-state and dynamic simulation using a single library
- Only “true equation oriented” flowsheeting tool
  - Rapid convergence of process flowsheets, even with multiple recycles
  - Full exploitation of recent developments on Model Initialisation Procedures
    - Ensure robustness of solution with little/no user intervention

# ProcessBuilder Roadmap

- Flowsheet diagnostics
- Batch processes and plant start-up
- Extend number of distillation column initialisation algorithms
- Documentation, testing and quality control