

# Implementation of a Reduced System Model to a Continuous Direct Compression Manufacturing Process

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# Continuous Manufacturing of Drug Product

- Shift in processing times
  - Days → Minutes
- Less material handling
- Lean manufacturing
- Small footprint
- Accelerated development

# Model Based Design

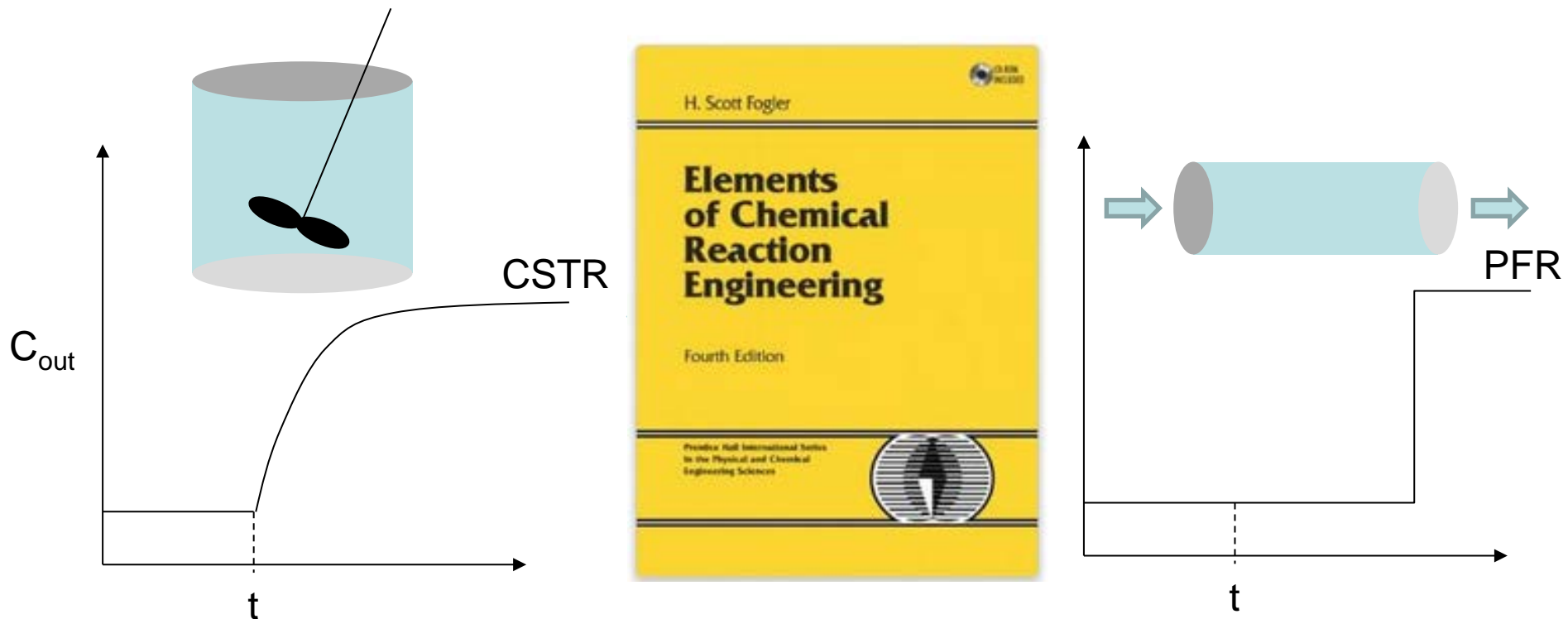
- Process Design:

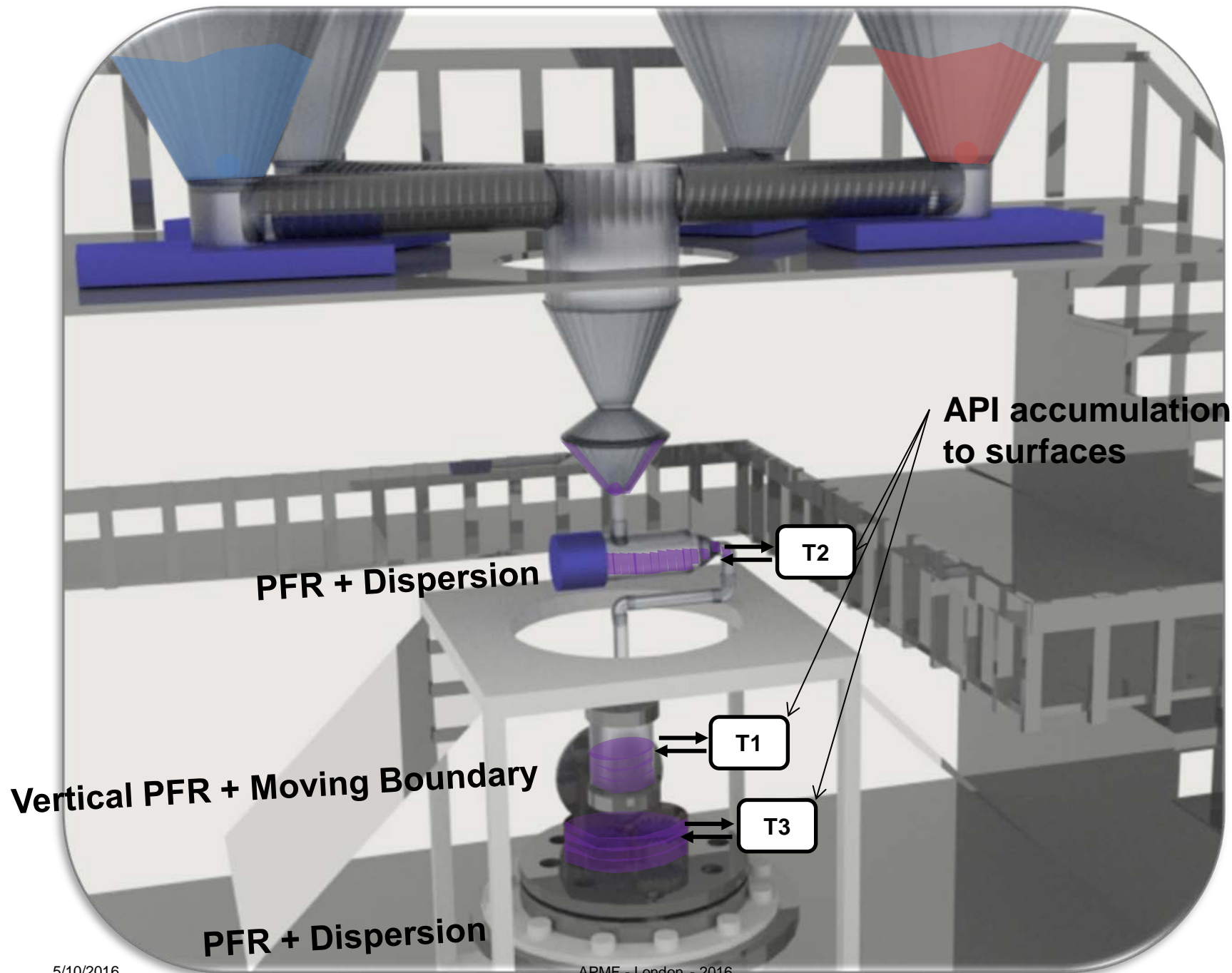
The study of continuous flow of material and it's mixing is a **very well** understood science

- Some adjustments need to be done for powders, but the major points still apply.

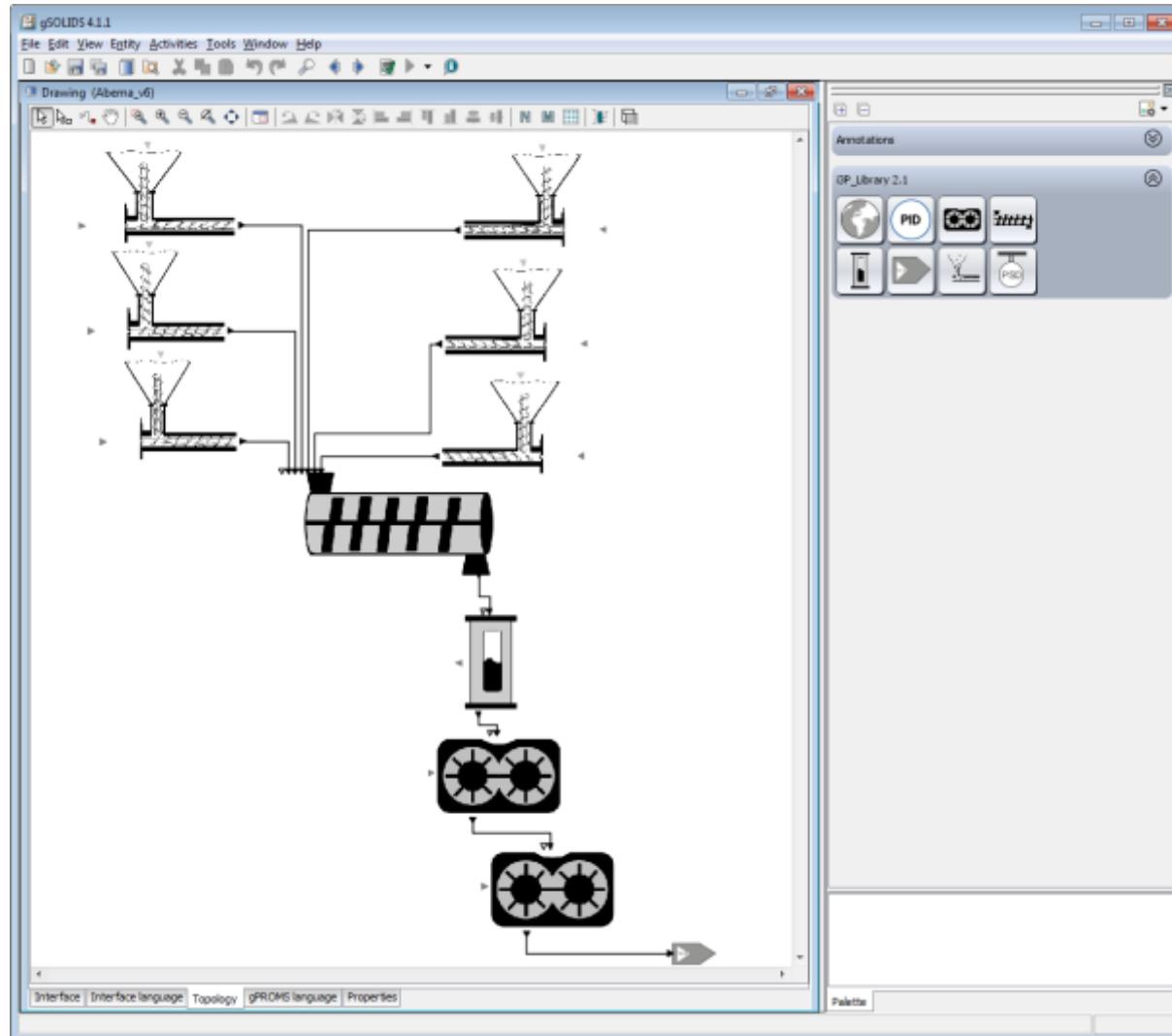
# Model Based Design

- Continuous mixing is a very well understood principle in chemical engineering



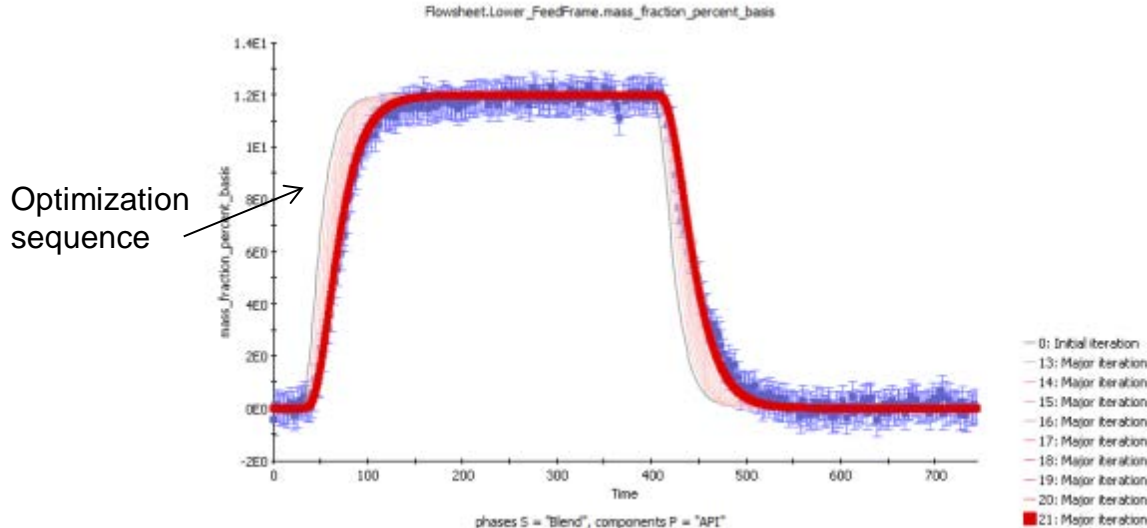


# gPROMS implementation



# Parameter Estimation

- System components are characterized by introducing step tests



## Lack of Fit Test

Weighted Residual	$\chi^2$ -Value (95%)	Comment
528.663	580.463	Good fit: weighted residual less than $\chi^2$ -Value



# Current Solution – Reduced System Model

- Knowing expected dispersion and noise sequence for a given new formula this model can be used (among other uses) to :

1. Aid Product Development

1. On-Line Model Based Application !

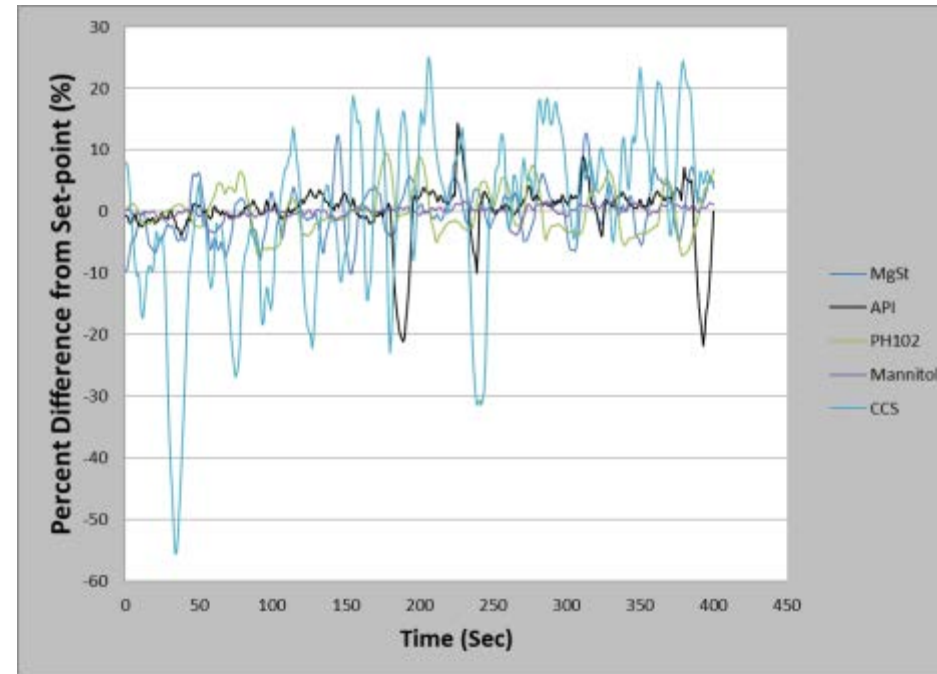
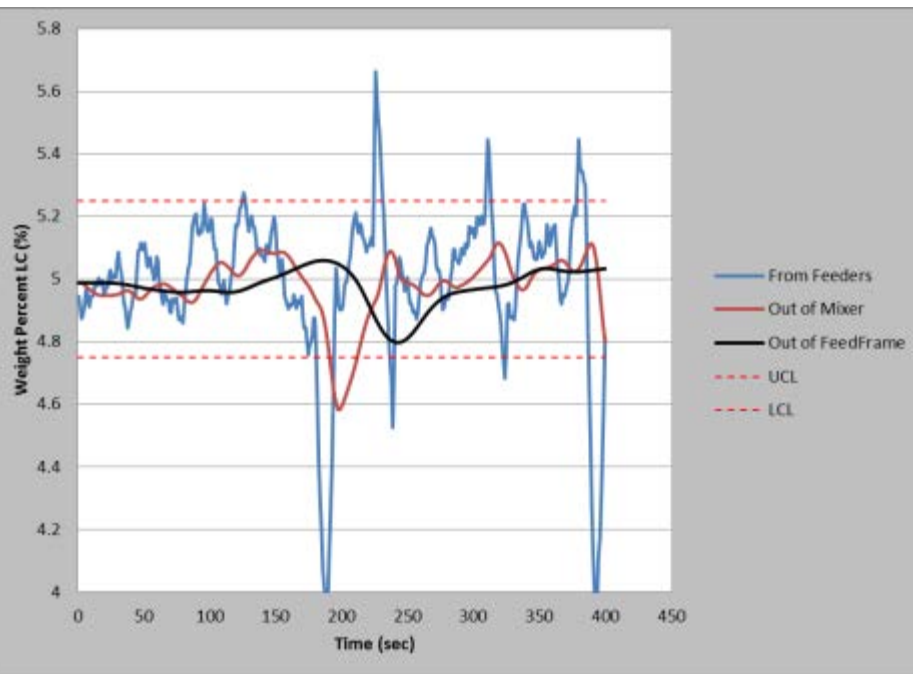
- Moving Horizon Estimation



# Disturbance rejection study

- Can system reject disturbances from feeders for a given compound/formulation?

Yes, integration across system successfully rejects disturbances for this case.



# Current Solution – Reduced System Model

- Knowing expected dispersion and noise sequence for a given new formula this model can be used (among other uses) to :

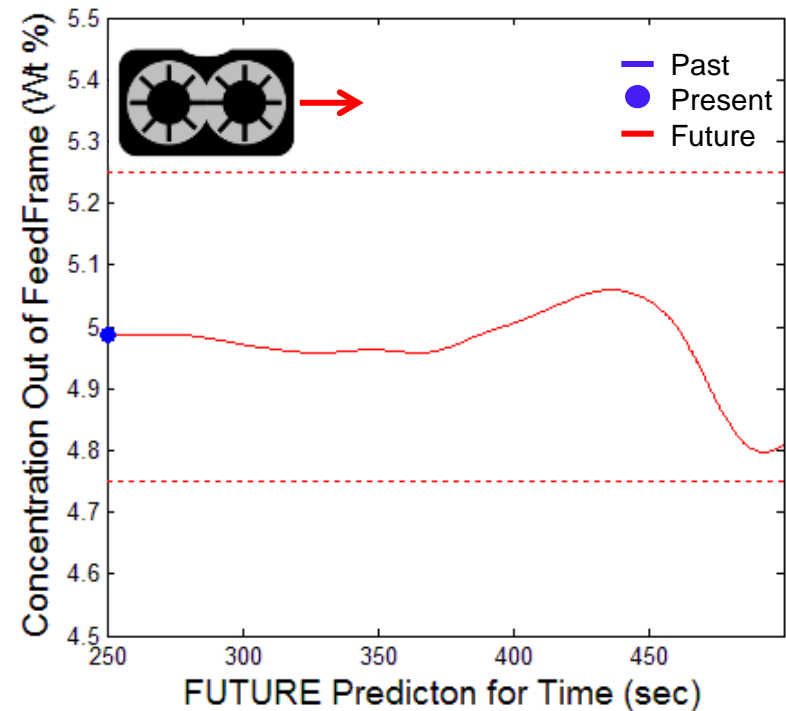
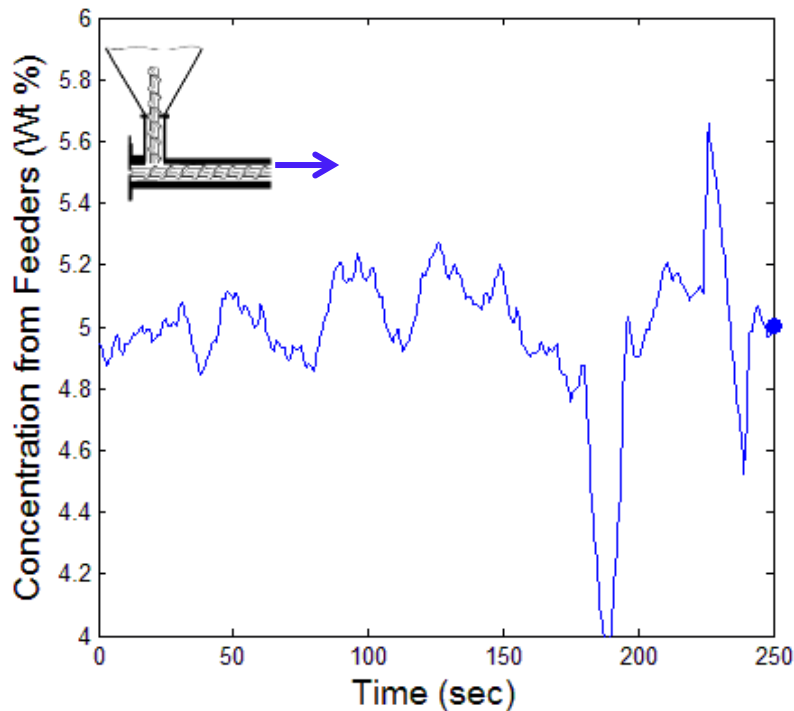
## 1. Aid Product Development

### 1. On-Line Model Based Application !

- Moving Horizon Estimation

# Desired solution – Non Linear State Estimation

- On-line, non-linear state estimation and prediction of downstream impact.

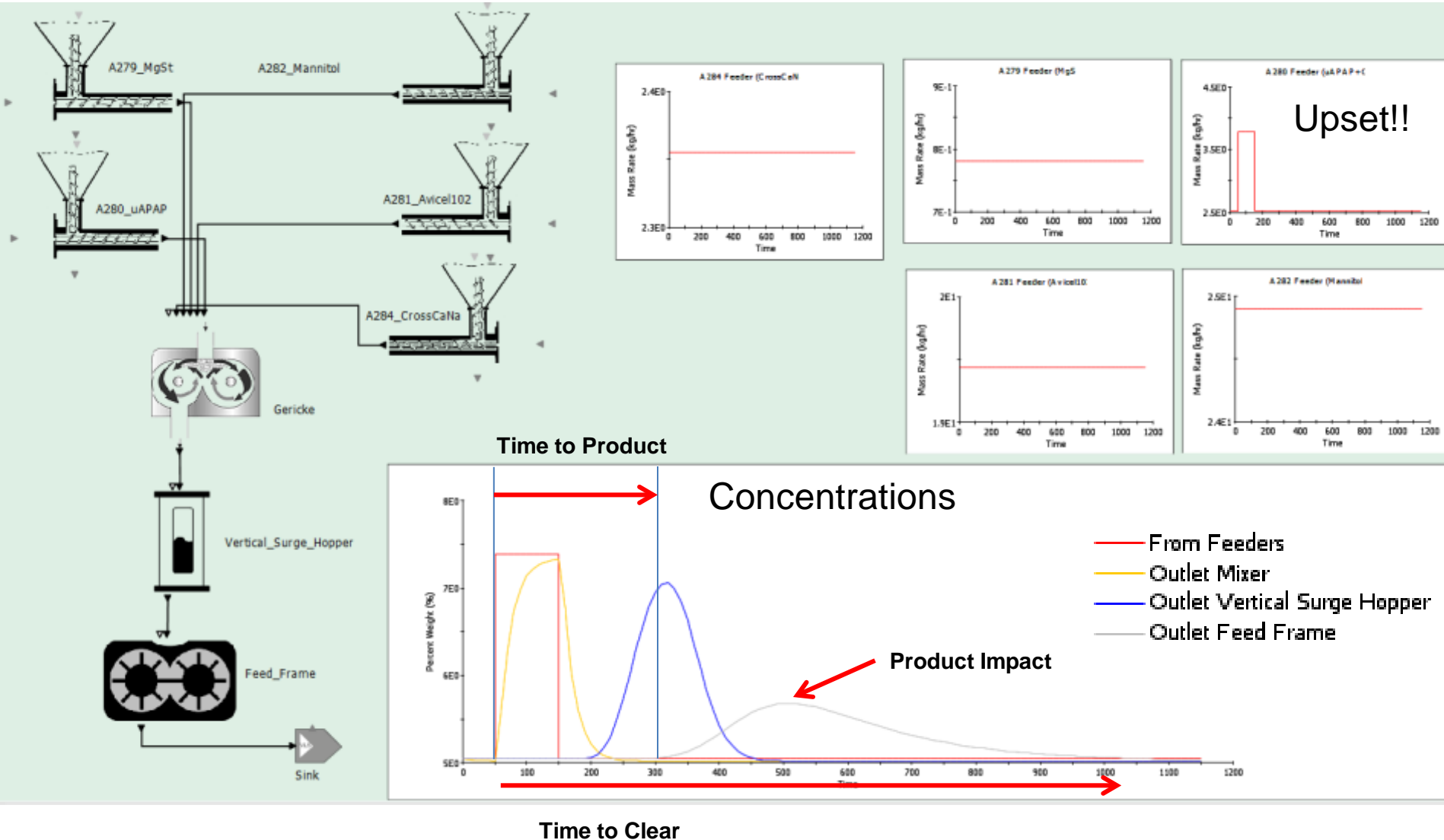


- Working towards this, but not there today
  - Computationally intense

# Current Solution – Reduced System Model

- Knowing expected dispersion and noise sequence for a given new formula this model can be used (among other uses) to :
  1. Aid product development
  2. For the conditions chosen, what is the **Impact to Product, Time to Product** and **Time to Clear** for a disturbance in the feeders to enter/leave the system.

# Product Impact, Time to Product and Time to Clear



# TASKS and SCHEDULE

- Implementation is laborious and complex to transfer to a new owner

```
g50025411
File Edit View Entity Activities Tools Window Help
Generate_FFConc_B100 (Abema_v6)

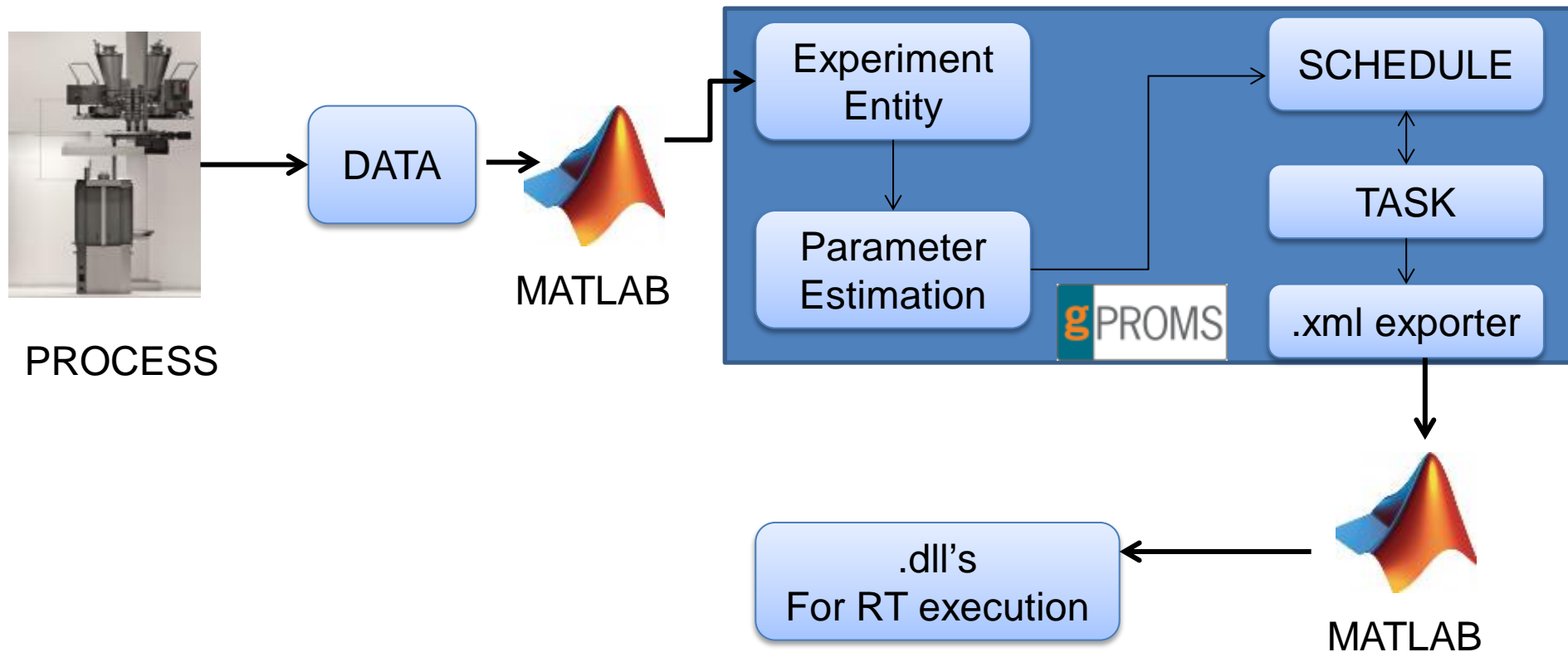
1. PARAMETER
2 System AS MODEL B100_Abema_Gocrip_200kg #Set to model being studied
3 SH_HT_SP AS REAL
4 SH_HT_MAX AS REAL
5 PID_OUTMAX AS REAL
6 PID_GAIN_SP AS REAL
7 API_FLOW_SP AS REAL
8 API_MASS_FRAC_SP AS REAL
9 AMPLITUDE_FRACTION_INCREMENT AS REAL
10 AMPLITUDE_MIN AS REAL
11 AMPLITUDE_MAX AS REAL
12 DURATION_INCREMENT AS REAL
13 DURATION_MAX AS REAL
14 DURATION_MIN AS REAL
15
16
17 # ParameterValue AS INTEGER (1 REAL 1) LOGICAL
18 # ParameterValue AS INTEGER_EXPRESSION (1 REAL_EXPRESSION 1) LOGICAL_EXPRESSION
19 # ParameterValue AS MODEL_ModelName
20
21 VARIABLE
22 AMPLITUDE AS REAL
23 DURATION AS REAL
24 COUNTER AS INTEGER
25
26 SCHEDULE
27 SEQUENCE #Main Sequence
28 RESET System.PID_controller001.maximum_output := PID_OUTMAX; END
29 RESET System.PID_controller001.gain := PID_GAIN_SP; END
30 RESET System.PID_controller001.set_point := SH_HT_SP; END
31 RESET System.Surge_Hopper.initial_height := SH_HT_SP / SH_HT_MAX; END
32 SAVE "InitialCondition"
33 COUNTER := 1;
34 AMPLITUDE := AMPLITUDE_MIN;
35 WHILE AMPLITUDE <= (AMPLITUDE_MAX + 0.05) DO
36     SEQUENCE #1
37     DURATION := DURATION_MIN;
38     WHILE DURATION <= (DURATION_MAX + 0.05) DO
39         SEQUENCE #2
40         RESTORE "InitialCondition"
41         REINITIAL System.Run_Number WITH System.Run_Number = COUNTER; END
42         #Perform the step to AMPLITUDE for DURATION
43         CONTINUE FOR 100
44         RESET System.FFG_Abema.mass_flowrate_S_kg_hr := AMPLITUDE * API_FLOW_SP; END
45         CONTINUE FOR DURATION
46         RESET System.FFG_Abema.mass_flowrate_S_kg_hr := API_FLOW_SP; END
47         CONTINUE FOR 200 #100 for 18.2 kg/h, 200 for 36.3 kg/h
48         CONTINUE UNTIL AND((System.FFG_Abema.mass_flowrate_percent_basis("B100", "API") - API_MASS_FRAC_SP) < 0.002-2
49         DURATION := DURATION + DURATION_INCREMENT;
50         COUNTER := COUNTER + 1;
51     END #2
52 END #1
53
```

```
SCHEDULE
#Continue for 5000
# SEQUENCE
# CONTINUE FOR 100
# REASSIGN
# Flowsheet.FDR6_Abema.mass_flowrate_S_kg_hr := 0;
# END
# CONTINUE FOR 2000
# END

# Generate_T2P (System is Flowsheet,
#
# PID_OUTMAX is 1000, #Typical value for 100mg is 10000 when not generating T2P
# PID_GAIN is 50, #Typical value for 100mg is 50 when not generating T2P
# VSH_HT_SP_INCREMENT is 0.031, #Steps of +10% Level
# VSH_HT_SP_MIN is 0.031, #Height a 10% fill
# VSH_HT_SP_MAX is 0.31, #Max. for angled hopper
# FLOW_RT_MULT_INCREMENT is 0.05, #Based on 35.71% / 6
# FLOW_RT_MULT_MIN is .90, # 90% of flow as min
# FLOW_RT_MULT_MAX is 1.1, # 110% of flow as max
# FDR1_MASSFLOW_SP is 0.5184, #For 36.3 kg/h B100
# FDR2_MASSFLOW_SP is 2.0736, #For 36.3 kg/h B100
# FDR3_MASSFLOW_SP is .9072, #For 36.3 kg/h B100
# FDR4_MASSFLOW_SP is 6.3504, #For 36.3 kg/h B100
# FDR5_MASSFLOW_SP is 1.8144, #For 36.3 kg/h B100
# FDR6_MASSFLOW_SP is 6.48, #For 36.3 kg/h B100
# API_MASS_FCNF_SP is 35.714058)

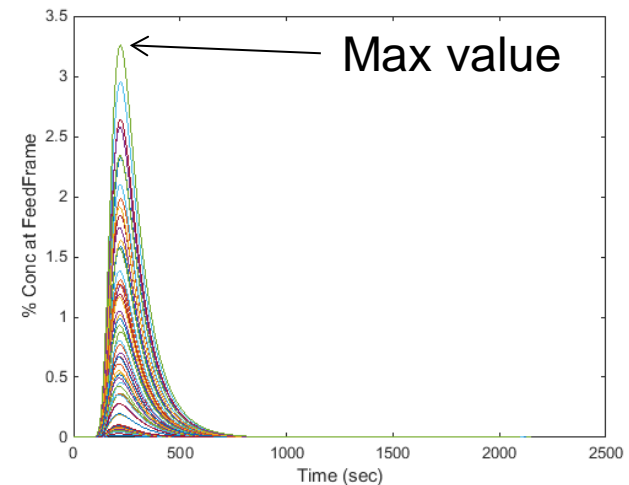
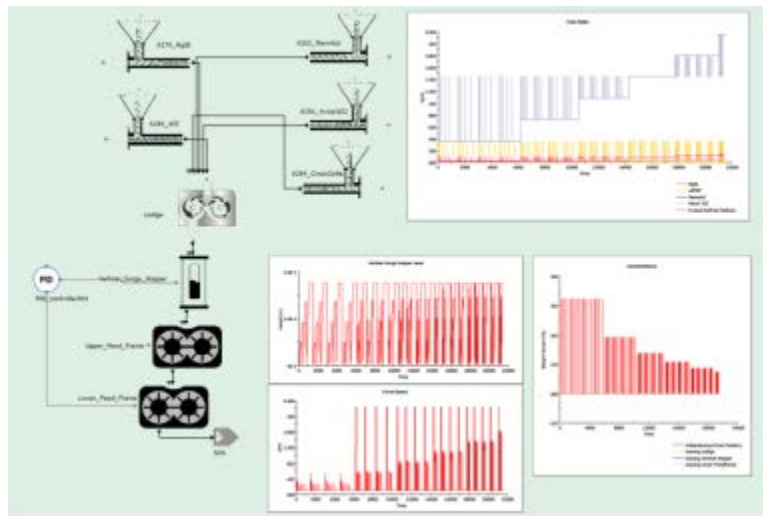
Generate_FFConc (System is Flowsheet,
SH_HT_SP is 0.1319, #Surge hopper height at 50%
SH_HT_MAX is 0.307986315, #Surge hopper maximum height
PID_OUTMAX is 500, #PID Controller maximum output
PID_GAIN_SP is 50, #PID Controller gain setpoint
AMPLITUDE_FRACTION_INCREMENT is 0.1,
AMPLITUDE_MIN is 1,
AMPLITUDE_MAX is 2,
DURATION_INCREMENT is 20,
DURATION_MIN is 120,
DURATION_MAX is 180,
API_FLOW_SP is 6.48, #For 18 kg/h
API_MASS_FRAC_SP is 35.714058)
```

# Current implementation



# Construction of a Reduced System Model - Impact to Product

- Simulated dispensed disturbances – THOUSANDS!
  - Spans from minute to large in both severity and duration
  - Example for Impact to Product:

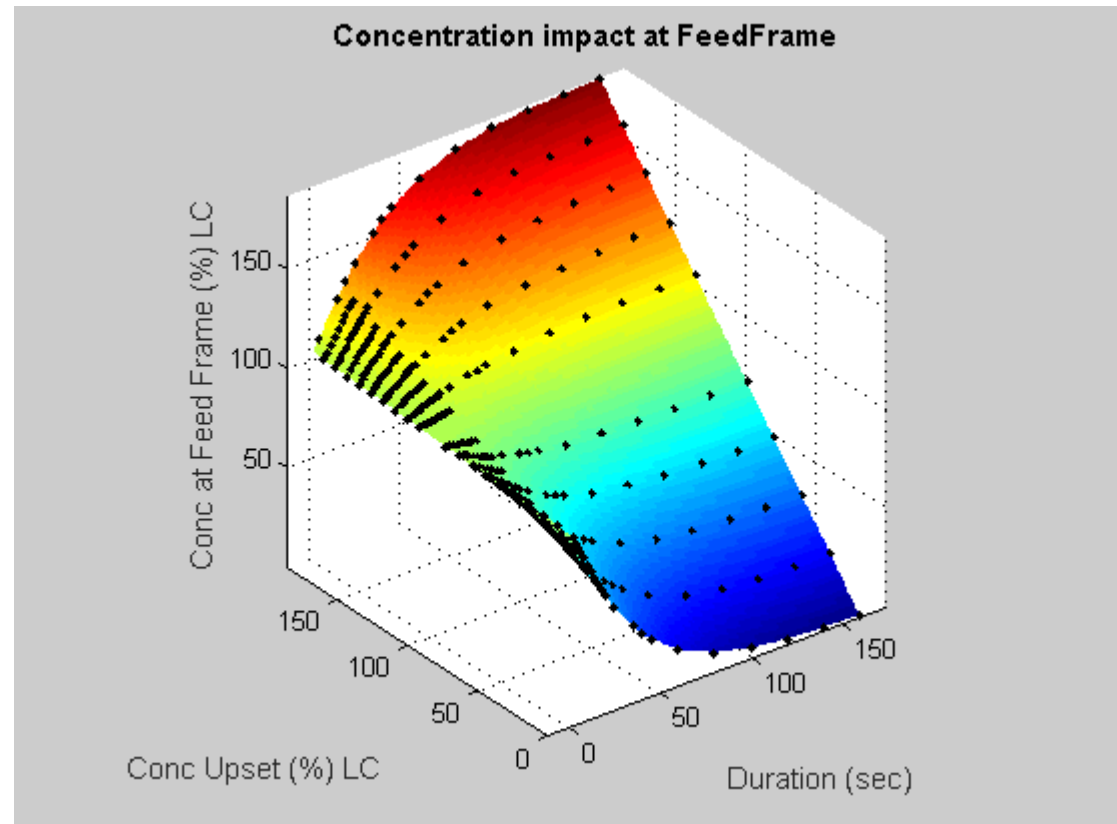


- Peak of concentration upset is worst case



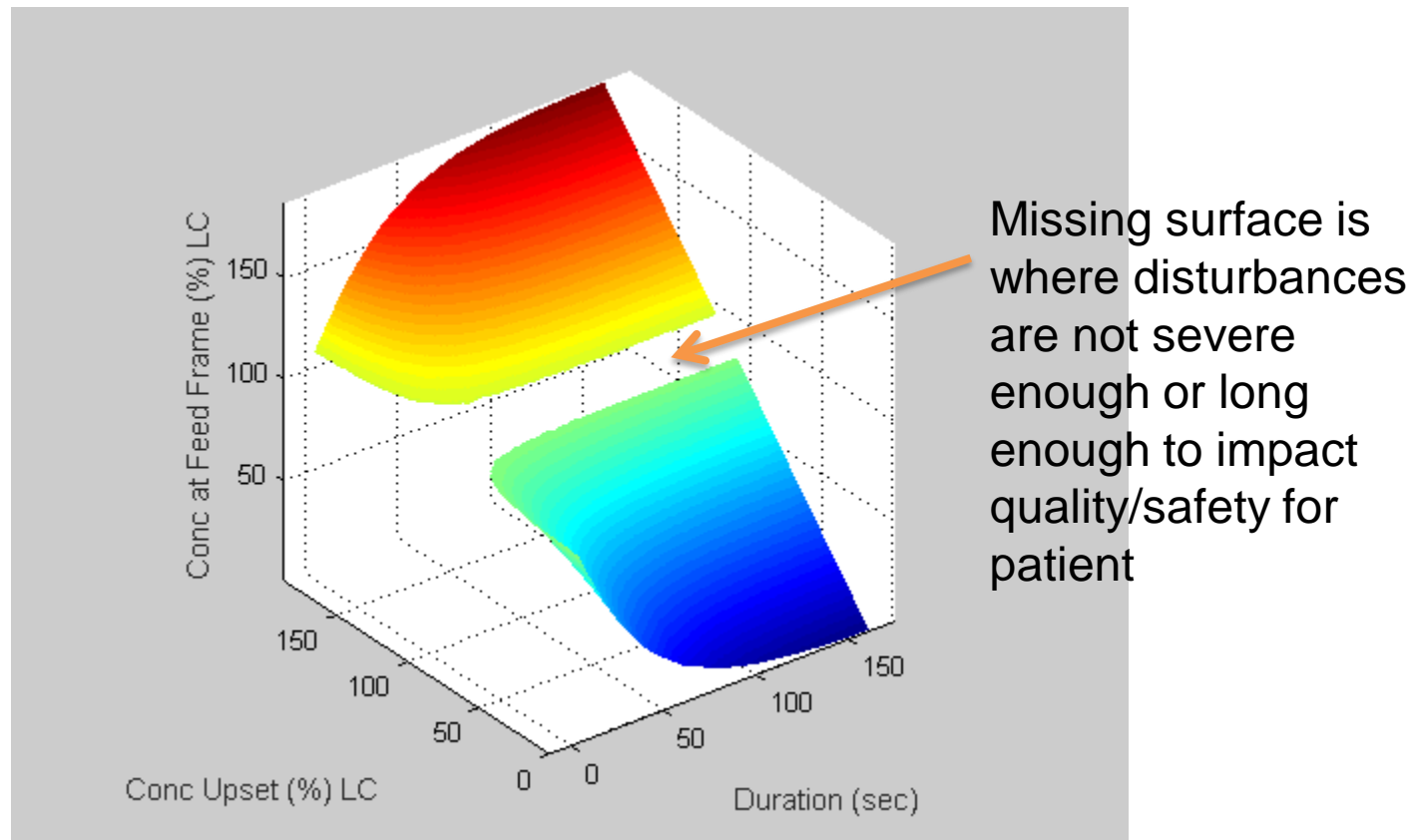
# Construction of a Reduced System Model - Impact to Product

- Resulting surface encompasses output of digital experiments
- Practical execution would take days and consume large amounts of API



# Construction of a Reduced System Model - Impact to Product

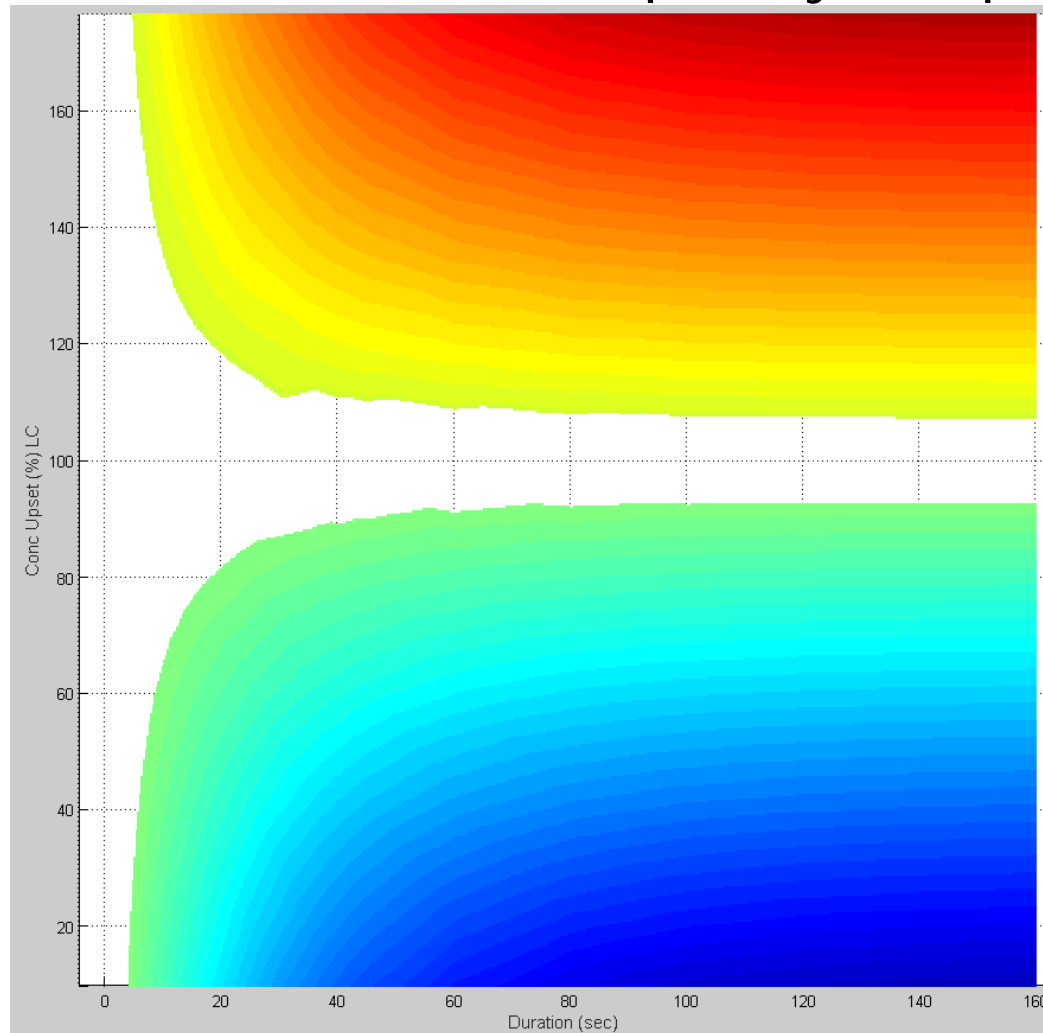
- Removing portion where disturbances do not impact product quality



# Construction of a Reduced System Model - Impact to Product

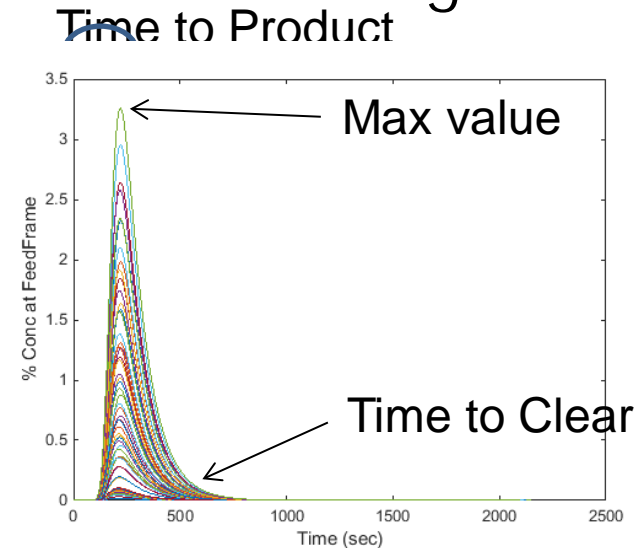
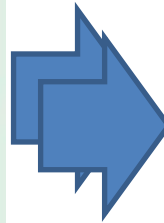
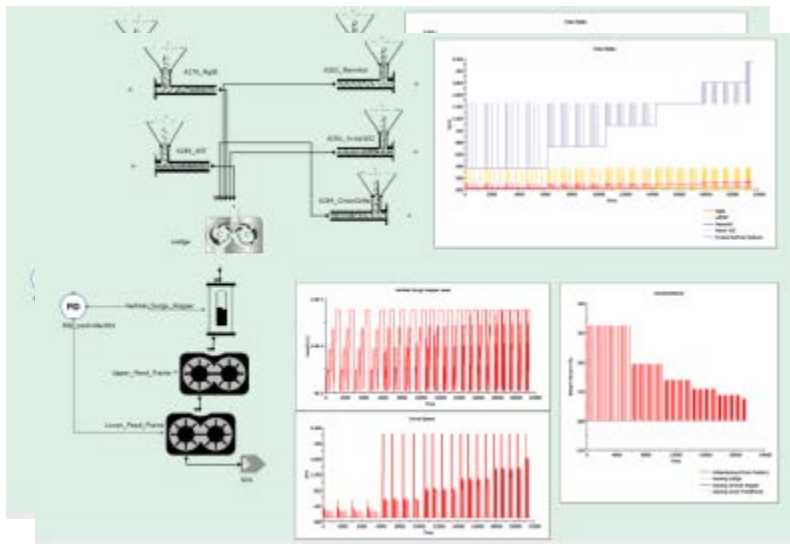
- X-Y projection (done for simplicity of upset testing)

## The “Funnel” Plot



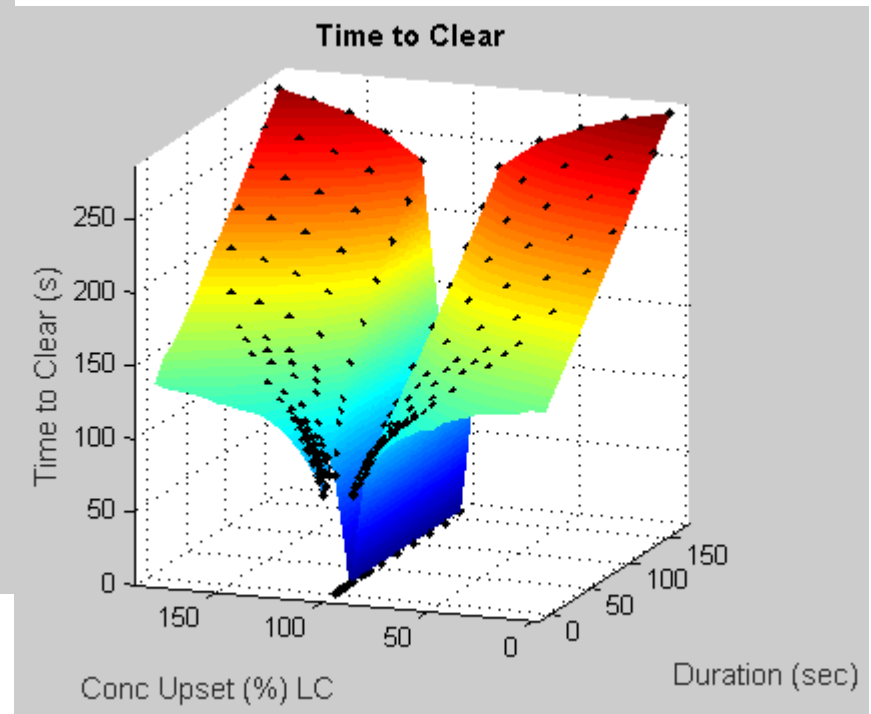
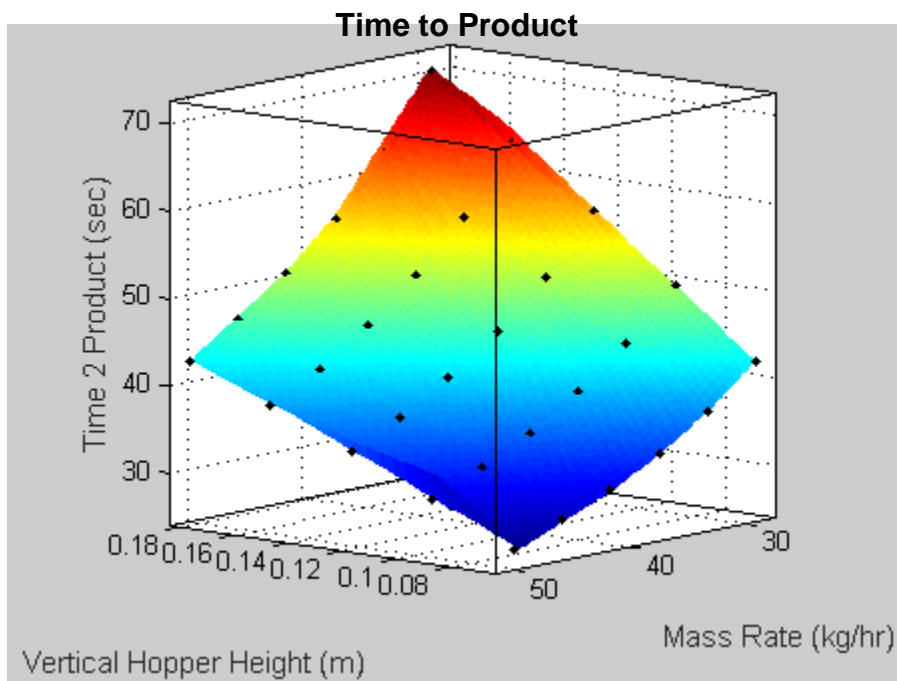
# Construction of a Reduced System Model – Time to Product/Clear

- Again, digital experiment in the Thousands
- Patient safety a core focus!
  - Looking for earliest sign of drift from target



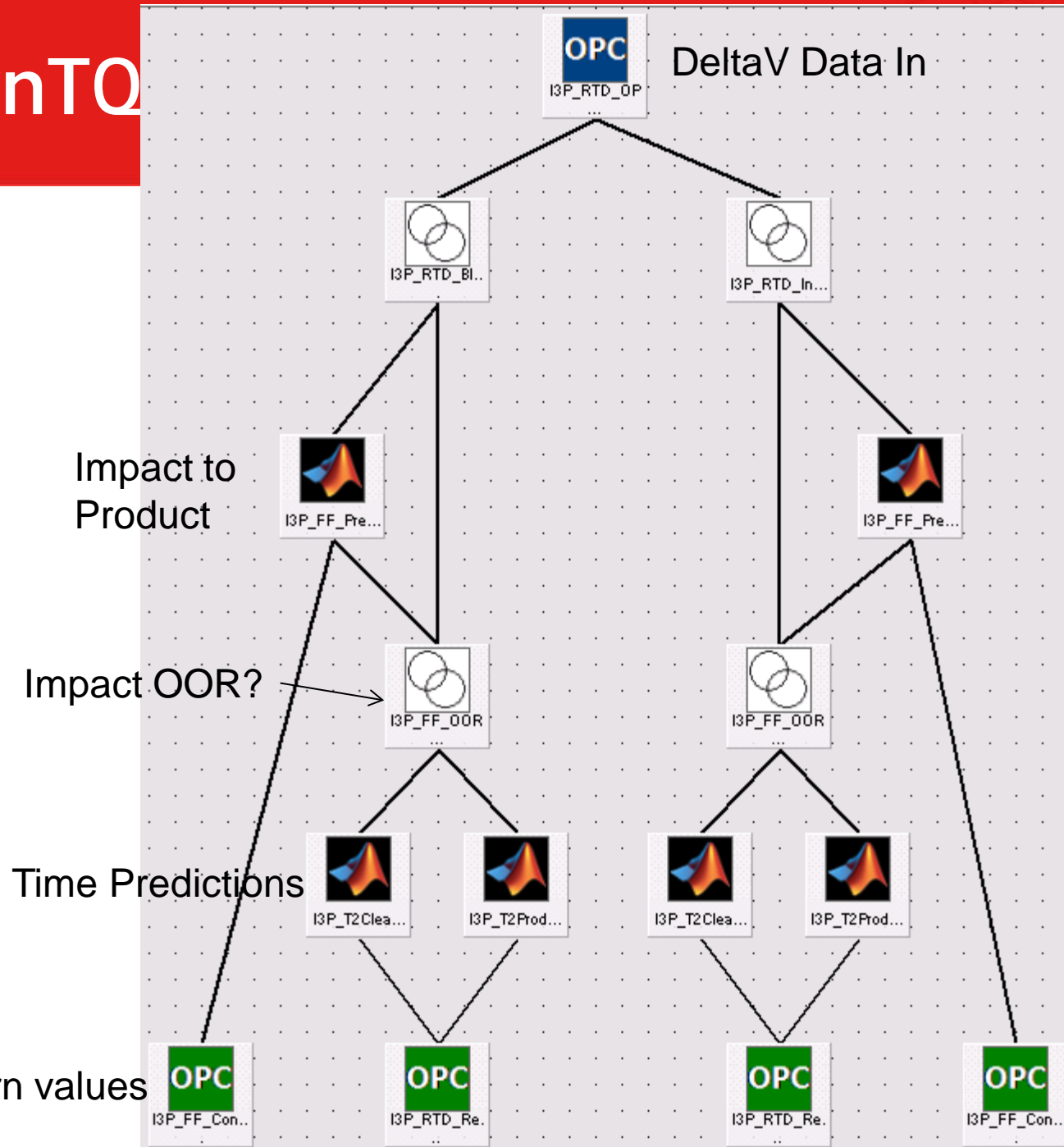
# Time to Product Module

- Reduction of temporal element of deterministic model to simple surface



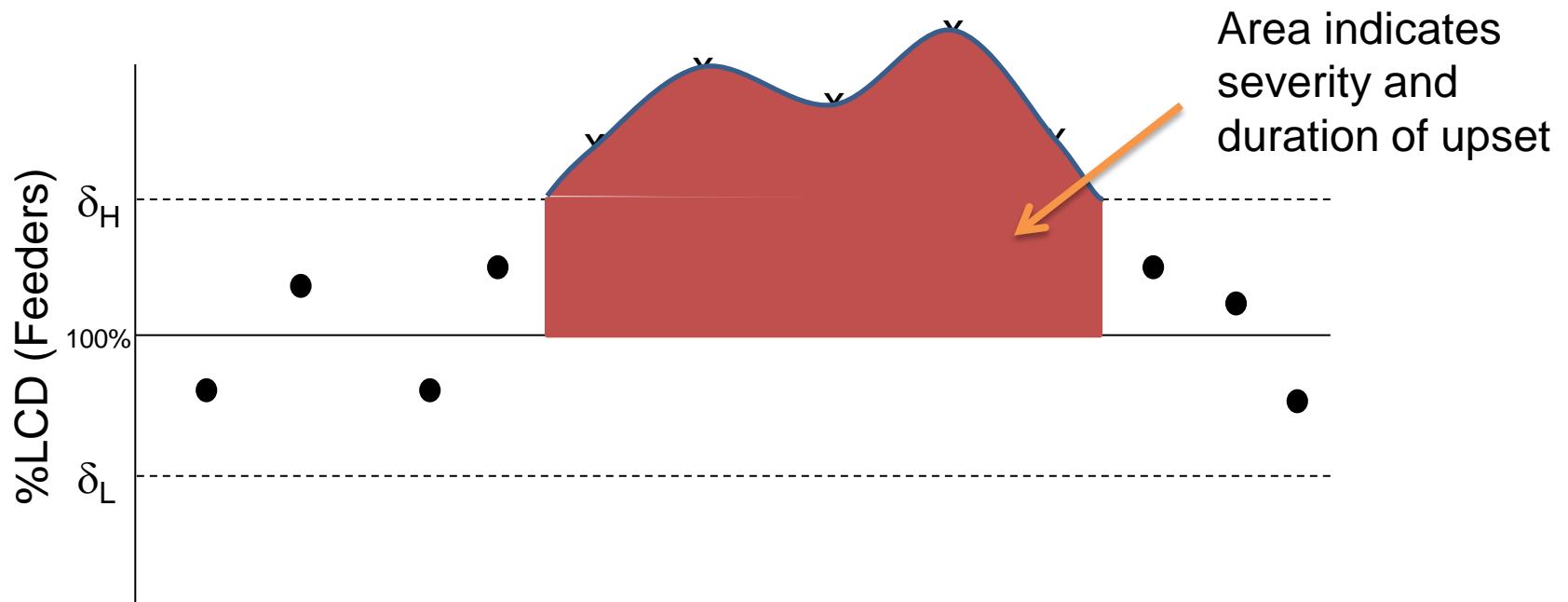
# Matlab Interpolants

- Surfaces become interpolants in Matlab
  - Feed Frame Conc Prediction
  - Time to Product (Time to Reject)
  - Time to Clear (Time to Accept)
- Compiled in Matlab to DLLs and ran on the SynTQ server under a Matlab execution, as needed
  - Pass DV data to Matlab DLLs in SynTQ
  - Return predictions, calculate times within DV



# Characterizing Disturbance

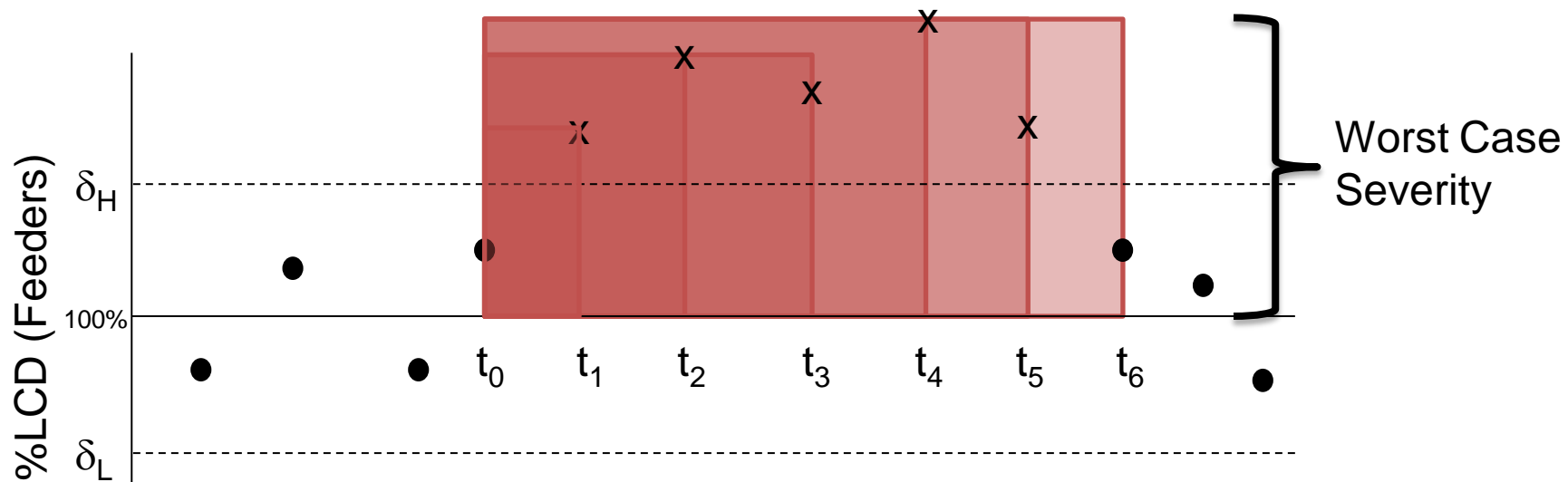
- Easy in a retrospective, post-mortum analysis
  - Given the following disturbance:





# Characterizing Disturbance

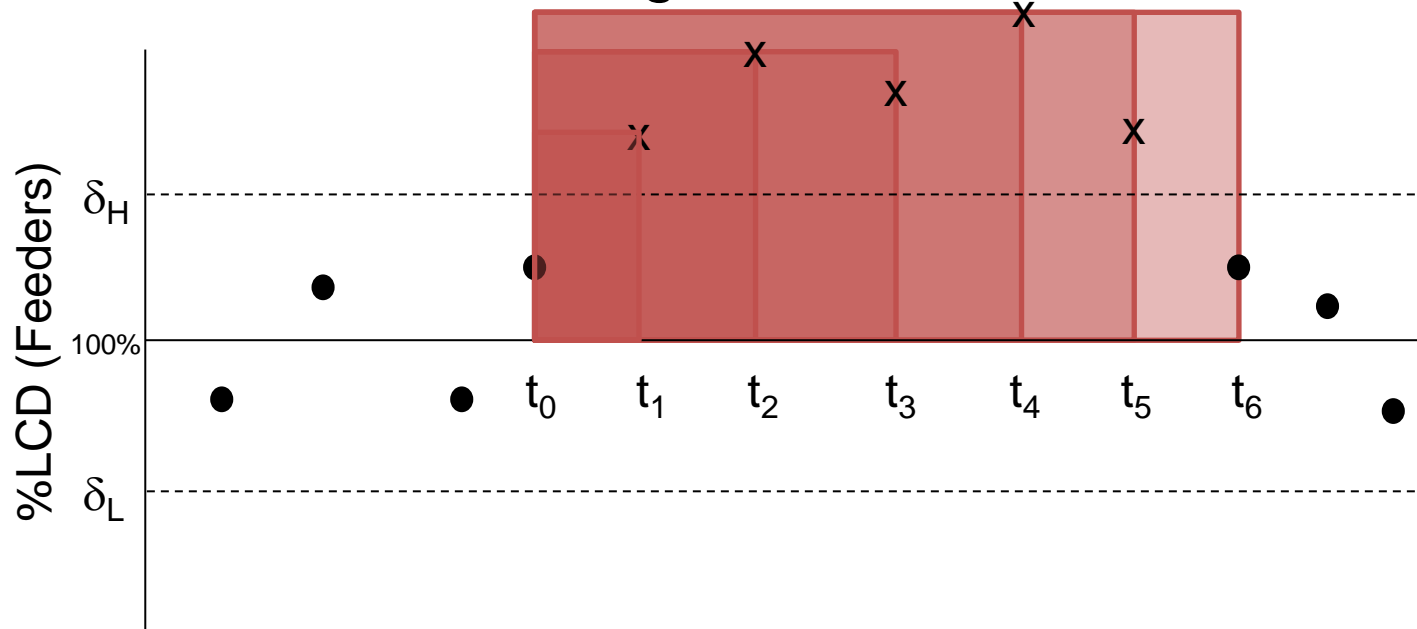
- Real time – future trending unknown
  - Given the following disturbance:



- Product impact for disturbance  
 $f(\max|\%LCD - 100\%|, \max t)$

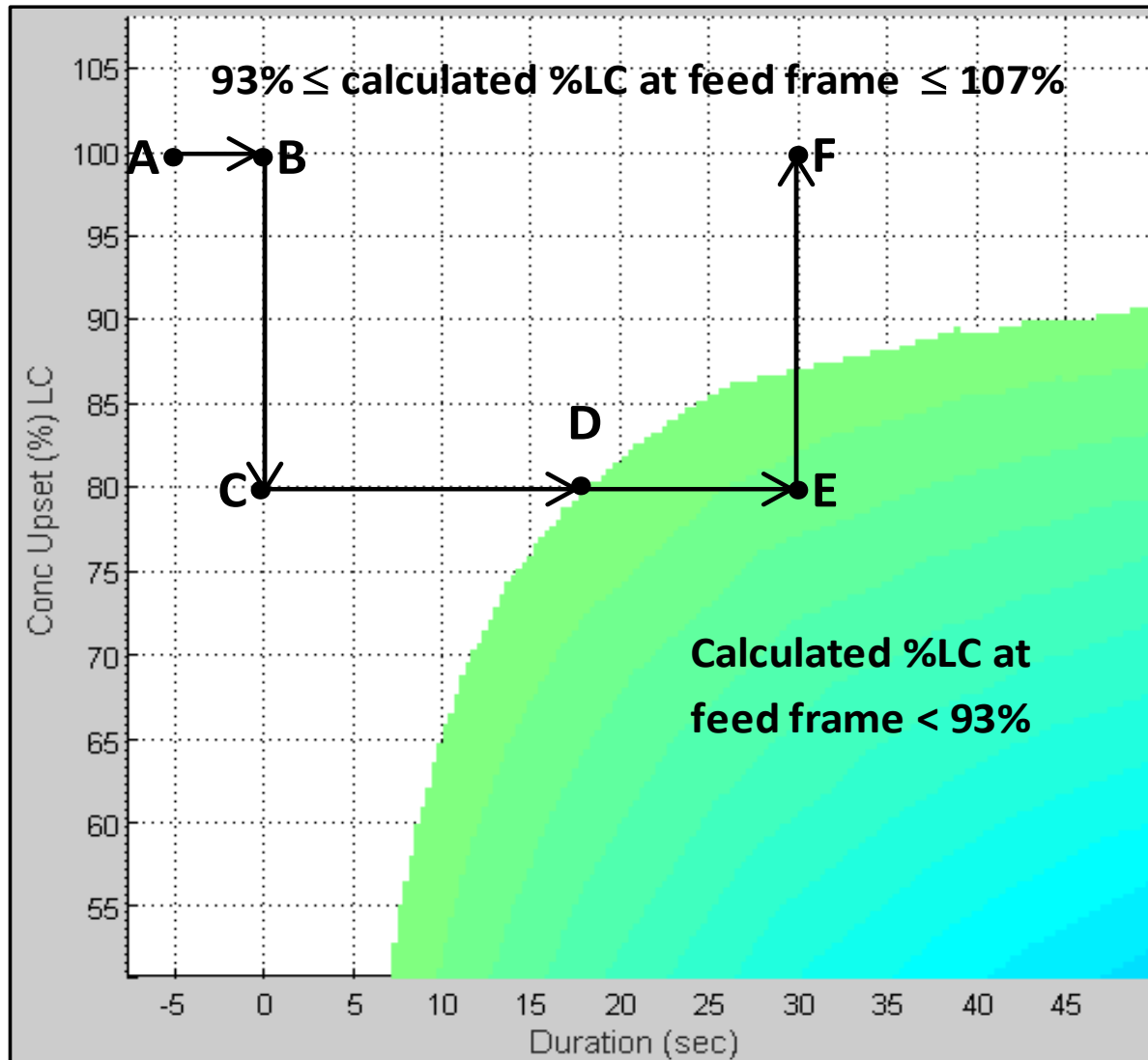
# Characterizing Disturbance

- Time to Product/Clear
  - Given the following disturbance:

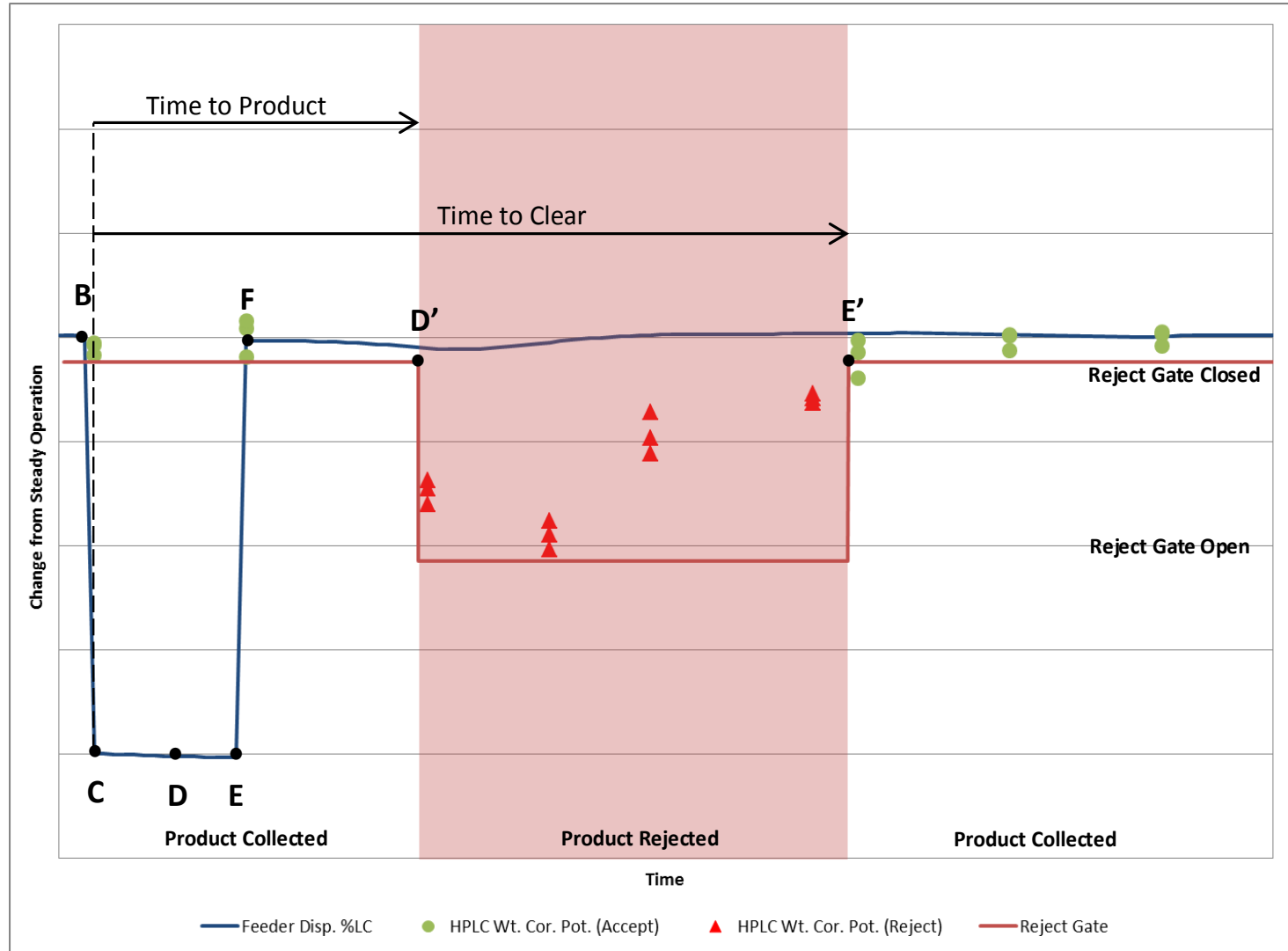


- $T2P_i = \min(T2P_{i-1}, T2P(VSH, MF))$
- $T2C_i = \max(T2C_{i-1}, T2C(\max|\%LCD - 100\%|, \max t))$
- Again, erring on patient safety

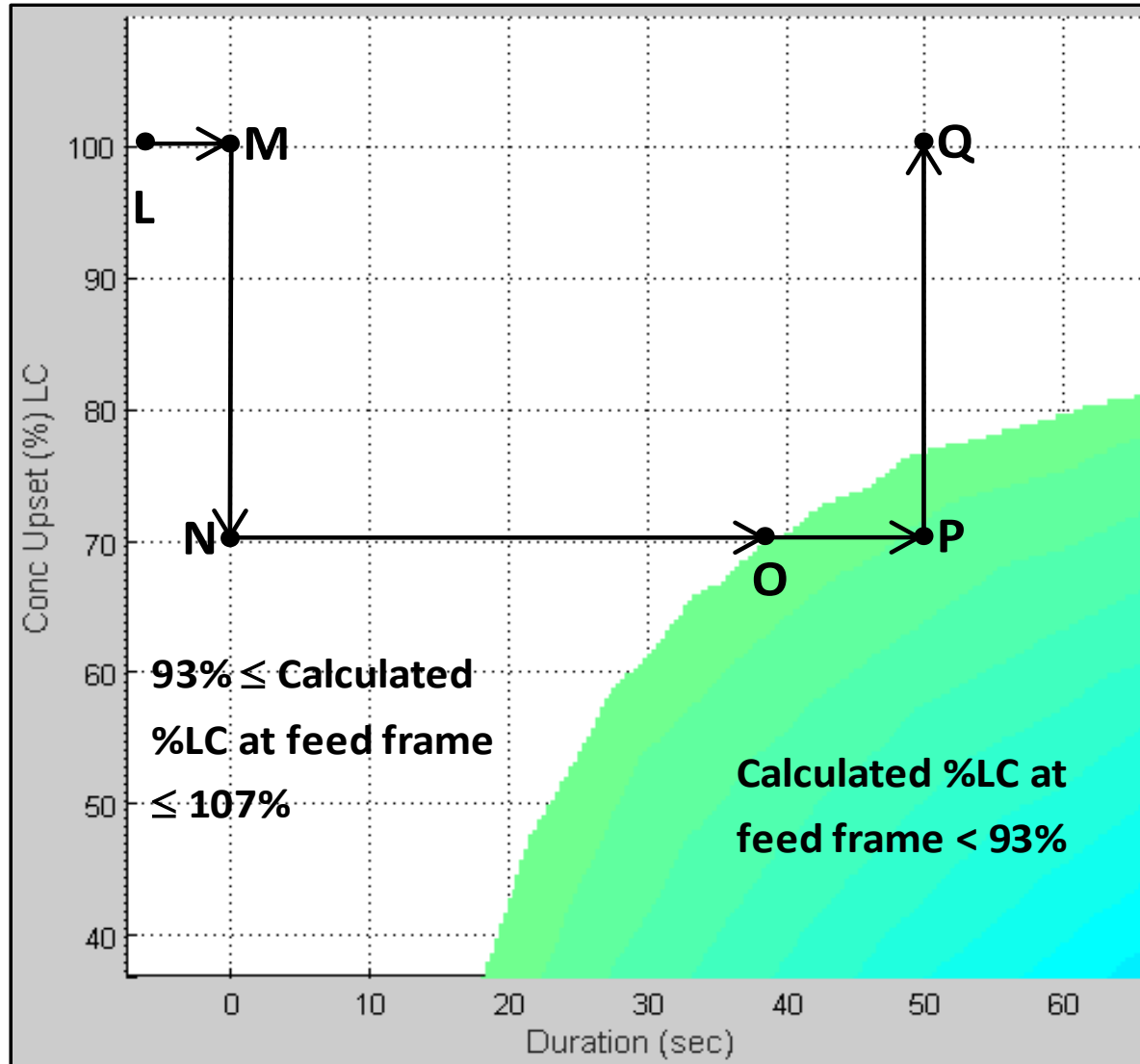
# Funnel Plot for LY1 (20 mg) Challenge



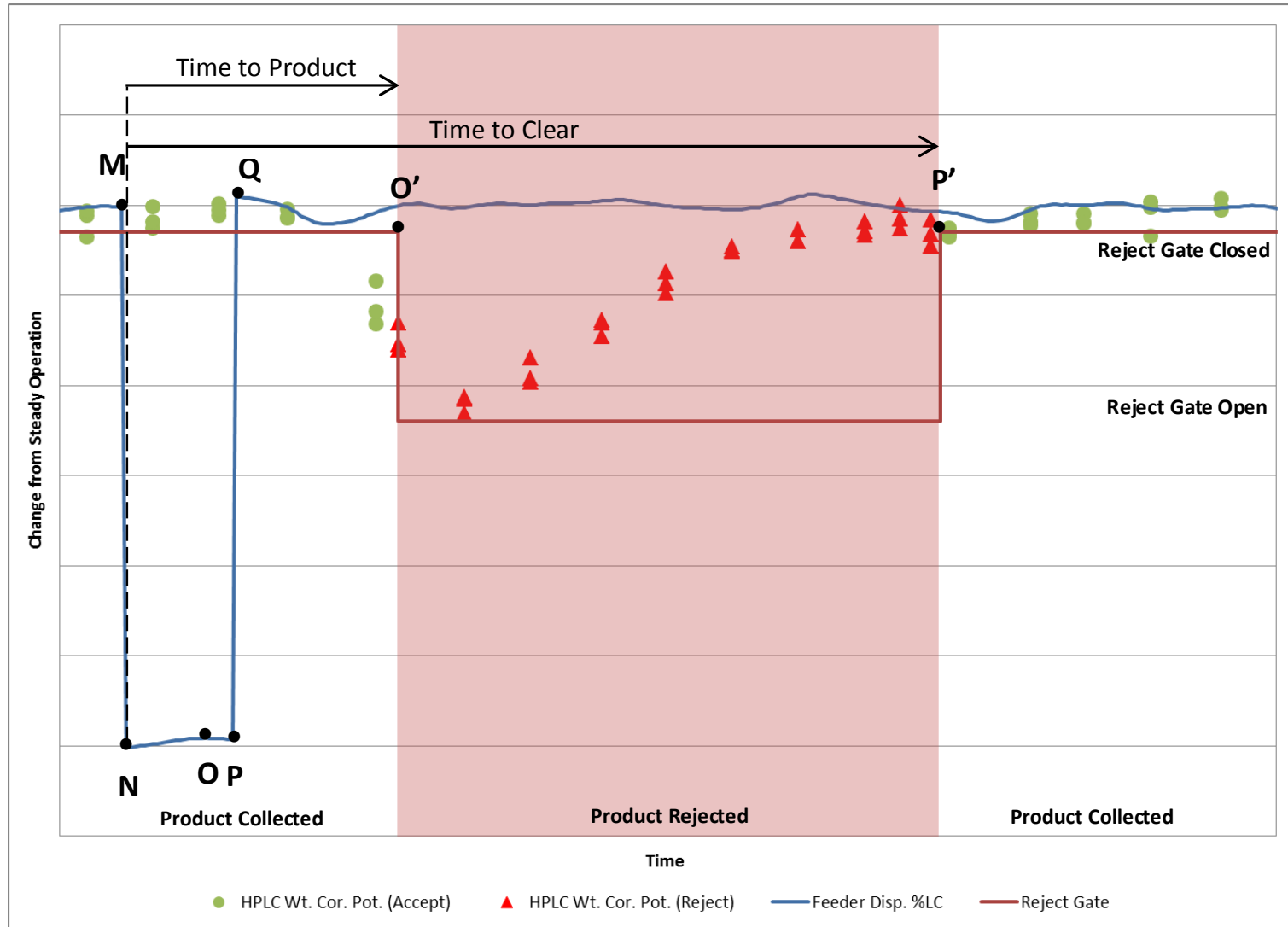
# LY1 (20 mg) Challenge



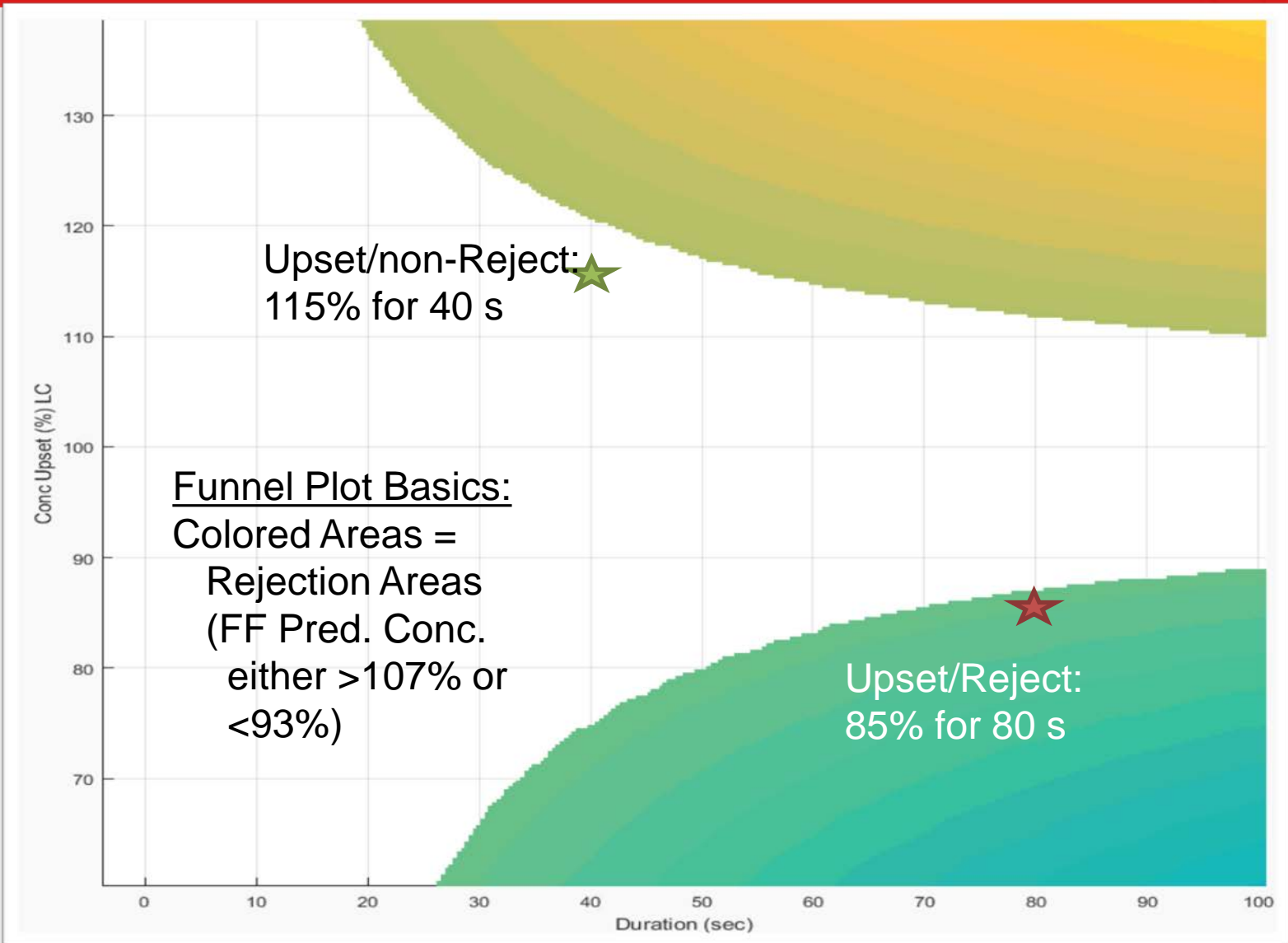
# Funnel Plot for LY1 (10 mg) Challenge



# LY1 (10 mg) Challenge



# Funnel Plot for LY2 (150 mg) Challenge

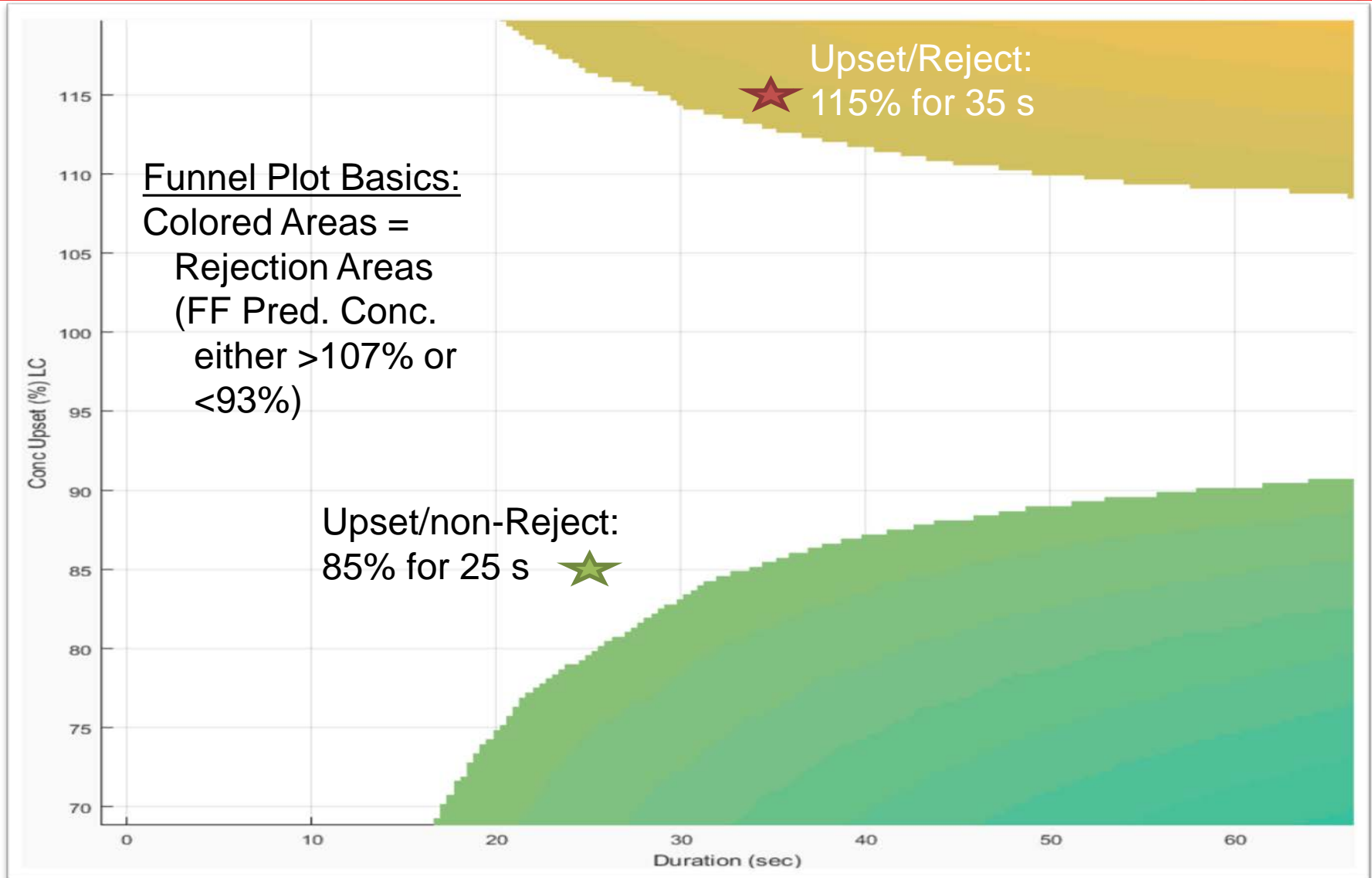


## 150 mg Challenge

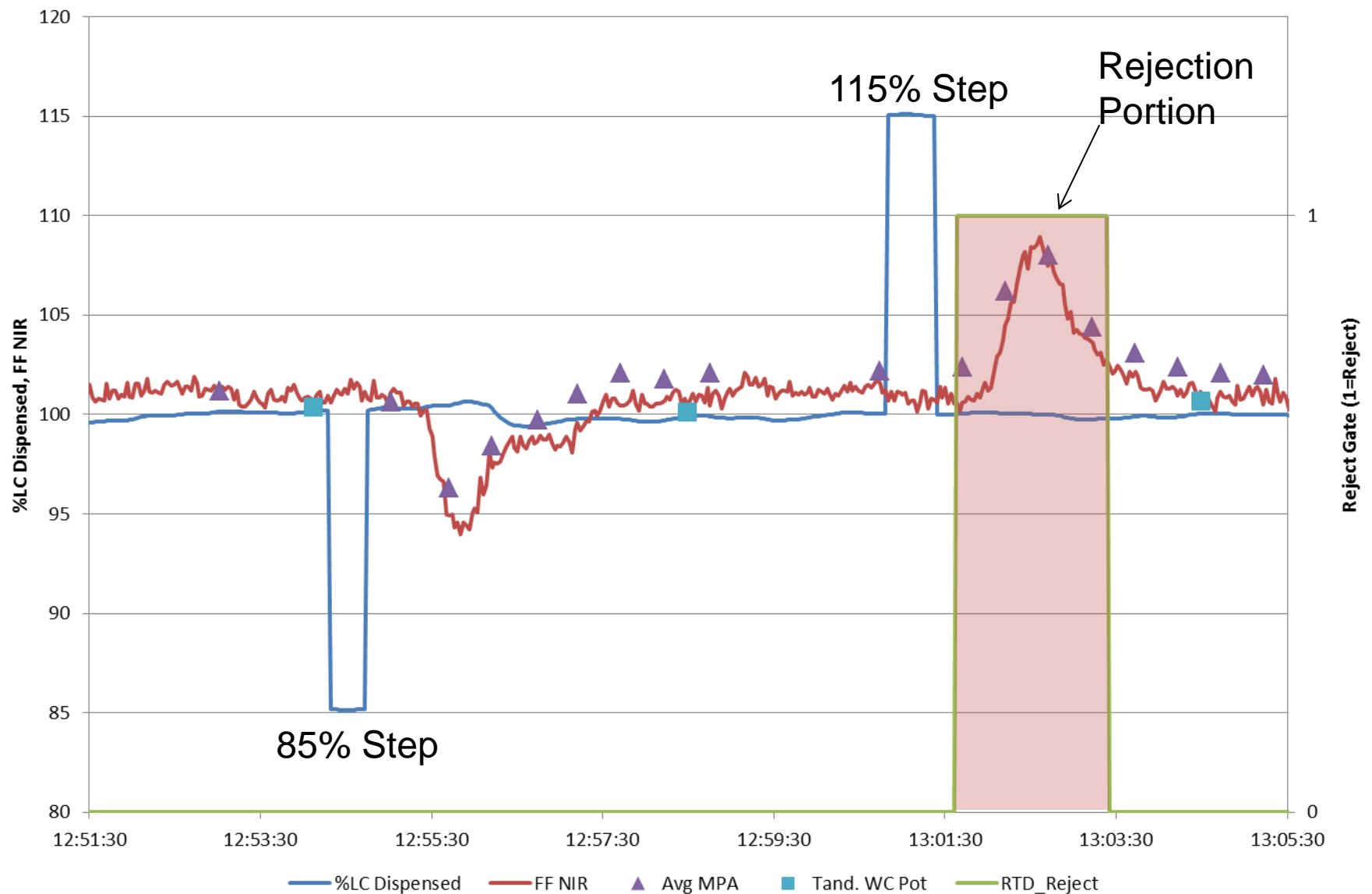




# Funnel Plot for LY2 (200 mg) Challenge



## 200 mg Challenge



# Final Remarks

- An adequate model for the drug product continuous manufacturing process was built and implemented in gPROMS.
- Observability continues to be an issue in a powder manufacturing line.
- Real-time implementation of a reduced system model is done by pre-computing key actionable indexes from the full model.
- Such a scheme is part of the control strategy for the process.
- Real-time non-linear state estimation continues to be the goal.