Project 2

April 2, 2022

Gabe Morris

[1]:
```python
from scipy.interpolate import interp1d
from scipy.optimize import fsolve
from msu_esd import cross_flow_unmixed
import numpy as np
import matplotlib.pyplot as plt
import pandas as pd
import warnings
from IPython.display import display, Latex

warnings.filterwarnings('ignore', category=FutureWarning)

plt.style.use('../maroon.mplstyle')
```

Contents

1 Given

The preliminary design of a recovery heat exchanger for a Solar Turbines Centaur 50 is to be accomplished. The heat exchanger is to be used to heat water from the turbine exhaust for process use. Surface 8.0-3/8T or surface 9.29-0.737-SR is to be used. More information on the Centaur 50 may be found here.

The requirements are:

Property	Gas Side	Water Side
$\dot{m}\,(\frac{lbm}{hr})$	151,410	36,000
$T_{in}\,(^{\circ}F)$	910	70
$T_{out}\,(^{\circ}F)$	400	?
P_{in}	atmospheric	atmospheric

The heat exchanger can have necessary width, but the gas inlet side must be such that the Reynolds number inside the finned-tube is about 1000. Water flows through the tubes, which are manifolded together in such a fashion that the water velocity is 3 ft/sec in order to ensure turbulent flow. The properties of the exhaust gas from the heat recovery are close to the properties of air at the same temperature.

2 Find

Select the better surface based on economy of the operation by calculating (a) the heat exchanger width and volume for both surfaces, (b) the gas side pressure drop for both surfaces, and (c) the operating costs for both surfaces for 8760 hr/yr operation. Electricity costs $\frac{\$0.05}{kW\,hr}$ for usage and $\frac{\$9}{kW}$ for demand (per month). The fan is 75% efficient.

The surface selected must be clearly indicated in the report. A sketch of the selected configuration, with dimensions indicated should be included.

3 Solution

3.1 Properties

The first step is to acquire the properties of the air and water. The properties may be taken at the average temperature between the inlet and exiting temperatures.

3.1.1 Air

The average temperature of the air is $655\,^{\circ}F$. The following properties may be obtained from Table B-2 in the text: $\rho = 0.03554\,\frac{lbm}{ft^3}$, $c_p = 0.25165\,\frac{Btu}{lbm\,^{\circ}F}$, $\mu = 2.077 \cdot 10^{-5}\,\frac{lbm}{ft\,sec}$, $Pr = 0.68775$.

3.1.2 Water

For water, the exit temperature is not known, but it may be solved for using an iterative process. First, the rating must be solved for using the known values for the air properties.

```
[2]: # Input parameters of air
mdot_a = 151_410  # lbm/hr
Tin_a = 910  # F
Tout_a = 400  # F
cp_a = 0.25165  # btu/(lbm F)

# Getting the rating
q = mdot_a*cp_a*(Tin_a - Tout_a)
q  # Btu per hour
```

```
[2]: 19432186.514999997
```

Now the exiting temperature may be solved using some python magic.

```
[3]: # Input parameters of water
mdot_w = 36_000  # lbm/hr
Tin_w = 70  # F

# We can get cp as a function of temperature using an interpolation function␣
 ↪from scipy
# From the book,
T_values = [80, 90, 100, 150, 200, 250, 300, 350, 400, 450, 500, 550, 600]
cp_values = [0.998, 0.997, 0.998, 1, 1, 1.01, 1.03, 1.05, 1.08, 1.12, 1.19, 1.
 ↪31, 1.51]

cp_w_lamb = interp1d(T_values, cp_values, fill_value='extrapolate')
```

Now `cp_w_lamb` may take in arguments at any temperature. This feature will be used later when accessing the database. For instance, the heat capacity should be between 1.08 and 1.12 for 410 $^{\circ}F$

```
[4]: float(cp_w_lamb(410))  # adding float() because it returns an array
```

```
[4]: 1.088
```

Now `fsolve` may be used to iteratively find the outlet temperature.

```
[5]: # Getting the outlet temperature
def get_T(Tout_water):
    T_avg = (Tout_water + Tin_w)/2
    cp_water = float(cp_w_lamb(T_avg))
    return q - mdot_w*cp_water*(Tout_water - Tin_w)  # expression equal to zero

Tout_w = fsolve(get_T, np.array([500, ]))[0]
Tout_w  # F
```

```
[5]: 588.2044624423871
```

With the average temperature of the water being 329.10223 $^{\circ}F$, the properties from Table B-2 are: $\rho = 56.31\,\frac{lbm}{ft^3}$, $c_p = 1.0416\,\frac{Btu}{lbm\,^{\circ}F}$, $\mu = 0.114 \cdot 10^{-3}\,\frac{lbm}{ft\,sec}$, $Pr = 1.087$, $k_w = 0.393\,\frac{Btu}{hr\,ft\,^{\circ}F}$.

3.2 Heat Exchanger Conductance

The heat exchanger conductance may be calculated using the NTU method.

[6]:
```
# Calculating the conductance
cp_w = 1.0416  # Btu/(lbm F)

Cc = mdot_w*cp_w  # Btu/(hr F)
Ch = mdot_a*cp_a  # Btu/(hr F)
C_min, C_max = min([Cc, Ch]), max([Cc, Ch])
C = C_min/C_max
print(f'C: {C:.3f}')
q_max = C_min*(Tin_a - Tin_w)  # Btu/hr
eff = q/q_max
print(f'Effectiveness: {eff:.3f}')
ntu = cross_flow_unmixed(eff, C)
UA = ntu*C_min  # Btu/(hr F)
print(f'UA: {UA:.3f} Btu/(hr F)')
```

```
C: 0.984
Effectiveness: 0.617
UA: 74166.055 Btu/(hr F)
```

The conductance of the iteration for the heat exchangers need to match the one calculated above as well as possible.

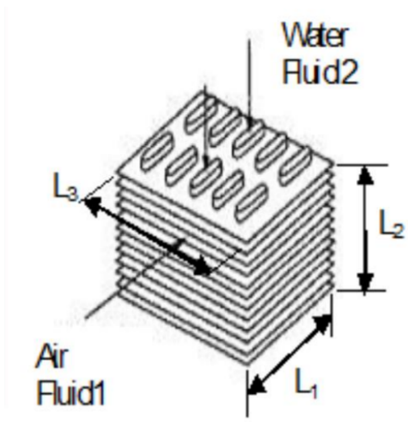


Figure 1: Fin-Tube Heat Exchanger

The conductance for an iteration depending on the geometry of the heat exchanger may be obtained by calculating the resistances for the air side and water side portions of the heat exchanger. The following relationship is,

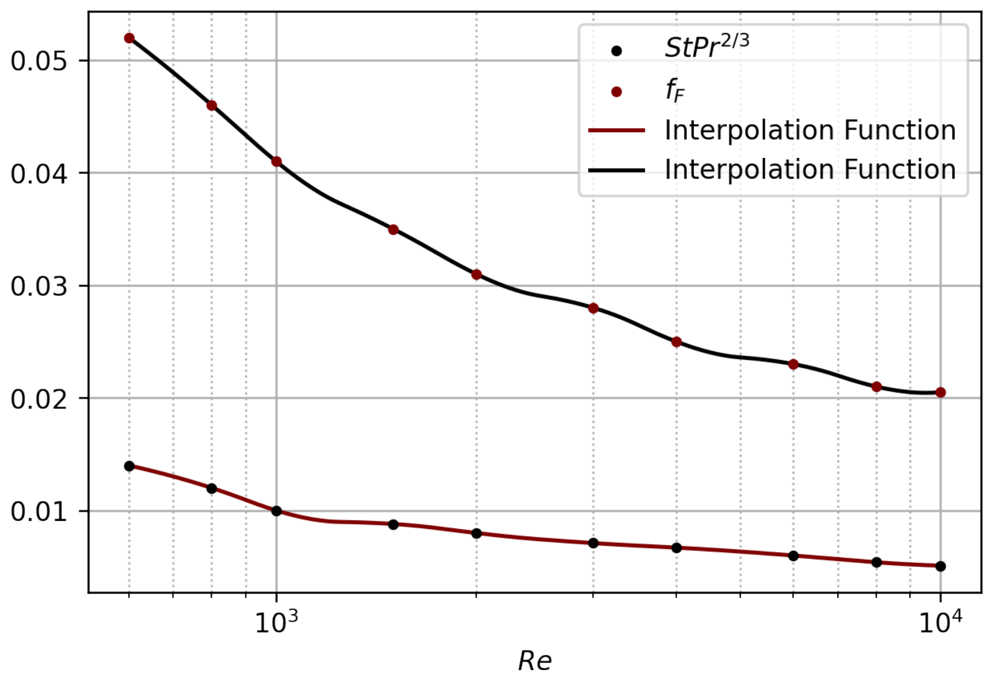
$$UA_{iter} = \frac{1}{R_a + R_w}$$

3.3 Surface 9.29-0.737-SR

A graphical representation of the relationship between Re and $StPr^{2/3}$ may be acquired from the database. This relationship will be used to obtain the heat convection coefficient for the airside.

[7]:
```
# Getting graph
Re = np.array([600, 800, 1000, 1500, 2000, 3000, 4000, 6000, 8000, 10_000])
hts = np.array([0.014, 0.012, 0.01, 0.0088, 0.008, 0.0071, 0.0067, 0.006, 0.
↪0054, 0.0051])
fF = np.array([0.052, 0.046, 0.041, 0.035, 0.031, 0.028, 0.025, 0.023, 0.021, 0.
↪0205])
hts_lamb = interp1d(Re, hts, kind='quadratic')
fF_lamb = interp1d(Re, fF, kind='quadratic')
Re_values = np.linspace(Re[0], Re[-1], 1000)

plt.scatter(Re, hts, label='$StPr^{2/3}$', zorder=3, marker='.', color='black')
plt.scatter(Re, fF, label='$f_F$', zorder=3, marker='.', color='maroon')
plt.plot(Re_values, hts_lamb(Re_values), label='Interpolation Function',␣
↪zorder=2)
plt.plot(Re_values, fF_lamb(Re_values), label='Interpolation Function',␣
↪zorder=2)
plt.xscale('log')
plt.xlabel('$Re$')
plt.grid(which='minor', ls=':')
plt.legend()
plt.show()
```



Property	Value
Fin Pitch	9.29 per inch
Hydraulic Diameter (D_h)	0.01352 ft
Fin Thickness (Copper)	0.004 in
Free flow area/frontal area (σ)	0.788
Total heat transfer/total volume (α)	228 $\frac{ft^2}{ft^3}$
Fin area/total area	0.814

3.3.1 Airside

For the airside (fins), the resistance may be found using,

$$R_a = \frac{1}{\eta_t A h_a}$$

The first step is to calculate Re and making sure that it is around 1000.

[8]:
```
# Air properties
rho_a = 0.03554 # lbm/ft^3
mu_a = 2.077e-5 # lbm/(ft sec)
cp_a = 0.25165 # Btu/(lbm F)
Pr_a = 0.68775
mdot_a = 151_410/3600 # lbm/sec

# Find the velocity of the air then use that to find Re
N1, N2, N3 = 9, 629, 129
L1 = N1*0.79/12  # ft
L2 = N2*0.112/12  # ft
L3 = N3*0.55/12  # ft
vol = L1*L2*L3 # ft^3
print(f'L1: {L1*12:.3f} in')
print(f'L2: {L2*12:.3f} in')
print(f'L3: {L3*12:.3f} in')
print(f'Volume: {vol:.3f} ft^3')
Da = 0.01352 # ft (from database)
sigma = 0.788 # from database
Va = mdot_a/(L2*L3*sigma*rho_a) # ft/sec
print(f'Velocity: {Va:.3f} ft/s')
G = Va*rho_a
Re_a = G*Da/mu_a
print(f'Re: {Re_a:.3f}')
L1_list, L2_list, L3_list = ['$L_1$ ($in$)', f'{L1*12:.3f}'], [r'$L_2$ ($in$)',
↪f'{L2*12:.3f}'], [r'$L_3$ ($in$)', f'{L3*12:.3f}']
vol_list = ['Volume ($ft^3$)', f'{vol:.3f}']
air_vel_list = [r'Air Velocity ($\frac{ft^3}{s}$)', f'{Va:.3f}']
```

```
air_re_list = ["Airside Reynold's", f'{Re_a:.3f}']
```

```
L1: 7.110 in
L2: 70.448 in
L3: 70.950 in
Volume: 20.566 ft^3
Velocity: 43.266 ft/s
Re: 1000.939
```

With Re known, the convection may now be solved using,

$$StPr^{2/3} = \frac{h}{G \cdot c_{p,a}} Pr^{2/3} \rightarrow h = \frac{StPr^{2/3} \cdot G \cdot c_{p,a}}{Pr^{2/3}}$$

[9]:
```
h_a = hts_lamb(Re_a)*G*cp_a/(Pr_a**(2/3))
h_a  # Btu/(s ft^2 F)
```

[9]:
```
0.004962771472598979
```

The total fin efficiency may be determined using,

$$\eta_t = 1 - \frac{A_{fin}}{A_{tot}}(1 - \eta_{fin})$$

[10]:
```
alpha = 228 # ft^2/ft^3
A_ratio = 0.814
A = alpha*vol # ft^2
L_fin = 0.01875 # ft
k_fin = 221/3600 # Btu/(sec ft F)
t_fin = 0.004/12 # ft
m = np.sqrt(h_a*2/(k_fin*t_fin))
eta_fin = np.tanh(m*L_fin)/(m*L_fin)
print(f'Fin Efficiency: {eta_fin:.3f}')
eta_t = 1 - A_ratio*(1 - eta_fin)
print(f'Total Efficiency: {eta_t:.3f}')
R_fin = 1/(eta_t*A*h_a)
print(f'Resistance: {R_fin:.3f} sec F/Btu')
```

```
Fin Efficiency: 0.947
Total Efficiency: 0.957
Resistance: 0.045 sec F/Btu
```

3.3.2 Waterside

The resistance from the waterside may be acquired by using,

$$R_w = \frac{1}{h_w A_c}$$

Re may be found first after acquiring the hydraulic diameter, then that could be used to calculate Nu. The convection coefficient can then be found using,

$$h_w = \frac{Nu \cdot k_w}{D_h}$$

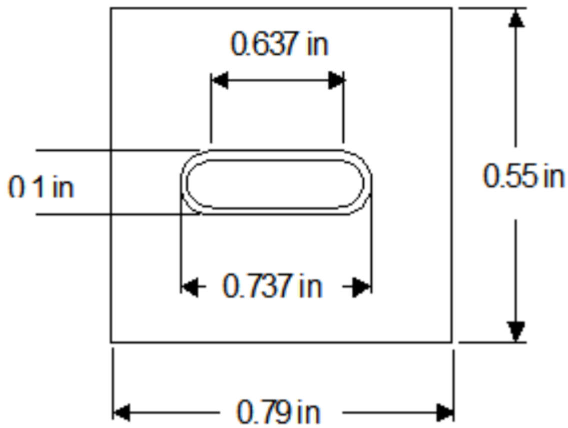


Figure 2: Known Tube Geometry

[11]:
```
# Water properties
rho_w = 56.31  # lbm/ft^3
cp_w = 1.0416  # btu/(lbm F)
mu_w = 0.114e-3  # lbm/(ft sec)
Pr_w = 1.087
k_w = 0.393/3600  # btu/(sec ft F)

Dc = 4*0.00306  # ft (from example 3-3)
alpha_c = 42.1  # ft^2/ft^3 (from example 3-3)
sigma_c = 0.129
Vw = 3  # ft/sec
Gw = Vw*rho_w  # lbm/(s ft^2)
Re_w = Gw*Dc/mu_w
print(f"Re: {Re_w:.3f}")
water_re_list = [f'{Re_w:.3f}']
```

```
Re: 18137.747
```

[12]:
```
# Since the flow is turbulent,
Nu = 0.023*Re_w**0.8*Pr_w**0.333
print(f'Nu: {Nu:.3f}')
h_w = Nu*k_w/Dc
print(f'h: {h_w:.3f} Btu/(s ft^2 F)')
Ac = alpha_c*vol
print(f'Ac: {Ac:.3f} ft^2')
Rw = 1/(Ac*h_w)
print(f'Resistance: {Rw} F*sec/Btu')
```

```
Nu: 60.347
h: 0.538 Btu/(s ft^2 F)
Ac: 865.823 ft^2
Resistance: 0.002145869904262943 F*sec/Btu
```

[13]:
```
# Solving for UA_iter
UA_iter = 1/(Rw + R_fin)*3600
print(f'UA_iter: {UA_iter:.3f} Btu/(hr F)')
print(f'UA_iter/UA: {UA_iter/UA:.3f}')
```

```
UA_iter: 76490.886 Btu/(hr F)
UA_iter/UA: 1.031
```

Thus, the final dimensions of the heat exchanger are $L_1 = 7.110\,in$ (width), $L_2 = 70.448\,in$, and $L_3 = 70.950\,in$. One important criteria to consider when determining the lengths is that the number of fins and tubes have to be an integer because part of a fin or tube cannot exist. This means that N in the relationships below for L_1, L_2, and L_3 must be an integer.

$$0.79 \cdot N_1 = L_1$$

$$0.112 \cdot N_2 = L_2$$

$$0.55 \cdot N_3 = L_3$$

The 0.112 for the second equation above comes from adding the thickness of the fins and the distance between the fins, which is the repeating pattern in the L_2 direction. If the pitch is 9.29 per inch,

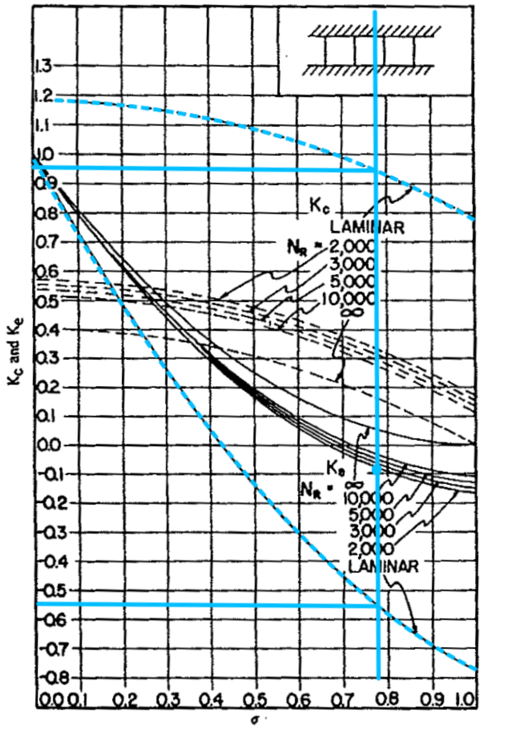
$$\frac{1}{9.29} + 0.004 = 0.112\,in$$

The distances calculated above do follow this physical limitation. This limitation also means that L_2 can never be equal to L_3 because $N = 0$ is the only solution to that system.

3.3.3 Airside Pressure Drop

The relationship for the pressure drop is,

$$\Delta P = \frac{G^2}{2\rho_{a,in}}\left[(K_c + 1 - \sigma^2) + 2\left(\frac{\rho_{a,in}}{\rho_{a,out}} - 1\right) + f_F \frac{A}{A_c}\frac{\rho_{a,in}}{\rho_{a,mean}} - (1 - \sigma^2 - K_e)\frac{\rho_{a,in}}{\rho_{a,out}}\right]$$



(c) Entrance and exit pressure loss coefficients for a multiple-square-tube heat exchanger core with abrupt-contraction entrance and abrupt-expansion exit.

Figure 3: K_c and K_e

The constants K_c and K_e may be acquired from Figure 3. Although the curves above are for square tube geometry, the assumption is that surface 9.29-0.737-SR is similar.

[14]:
```python
# Obtain air properties
rho_a_in = 0.0289  # lbm/ft^3 at 910 F
rho_a_out = 0.046  # lbm/ft^3 at 400 F
rat = rho_a_in/rho_a_out

# From figure above
Kc, Ke = 0.95, -0.55

x1 = Kc + 1 - sigma**2
x2 = 2*(rat - 1)
x3 = float(fF_lamb(Re_a))*A/(L2*L3*sigma)*rho_a_in/rho_a
x4 = (1 - sigma**2 - Ke)*rat

del_P = G**2/(2*rho_a_in)*(x1 + x2 + x3 - x4)/32.174
pressure_list = [r'$\Delta P$ ($\frac{lbf}{ft^2}$)', f'{del_P:.3f}']
del_P  # lbf/ft^2
```

[14]: 7.266053573200167

Thus, the pressure drop across the airside is around 7.27 $\frac{lbf}{ft^2}$.

3.3.4 Power Consumption

The power consumption for the fan may be calculating using,

$$power = \frac{Q\Delta P}{\eta}$$

where η is the efficiency and $Q = \frac{\dot{m}}{\rho}$.

[15]:
```
# Calculating the power
eta = 0.75
Q_a = mdot_a/rho_a   # ft^3/s
power = Q_a*del_P/eta
power_kW = power*0.00135581795
print(f'Power: {power:.3f} ft*lbf/s = {power/550:.3f} hp = {power_kW:.3f} kW')
power_list = ['Airside Power ($hp$)', f'{power/550:.3f}']
```

```
Power: 11464.945 ft*lbf/s = 20.845 hp = 15.544 kW
```

The relationship for power and cost is,

$$cost\ per\ year = \frac{\$0.05}{kW\ hr}\frac{8760\,hr}{yr} \cdot power + \frac{\$9}{kW\ mo}\frac{12\,mo}{yr} \cdot power$$

where the power is in kilowatts.

[16]:
```
# Calculating the cost per year
cost_per_year = 0.05*8760*power_kW + 9*12*power_kW
print(f'Cost Per Year: ${cost_per_year:.2f}/year')
cost_list = ['Annual Cost', f'{cost_per_year:.2f}']
```

```
Cost Per Year: $8487.23/year
```

The operating cost of the 9.29-0.737-SR surface is \$8487.23/year.

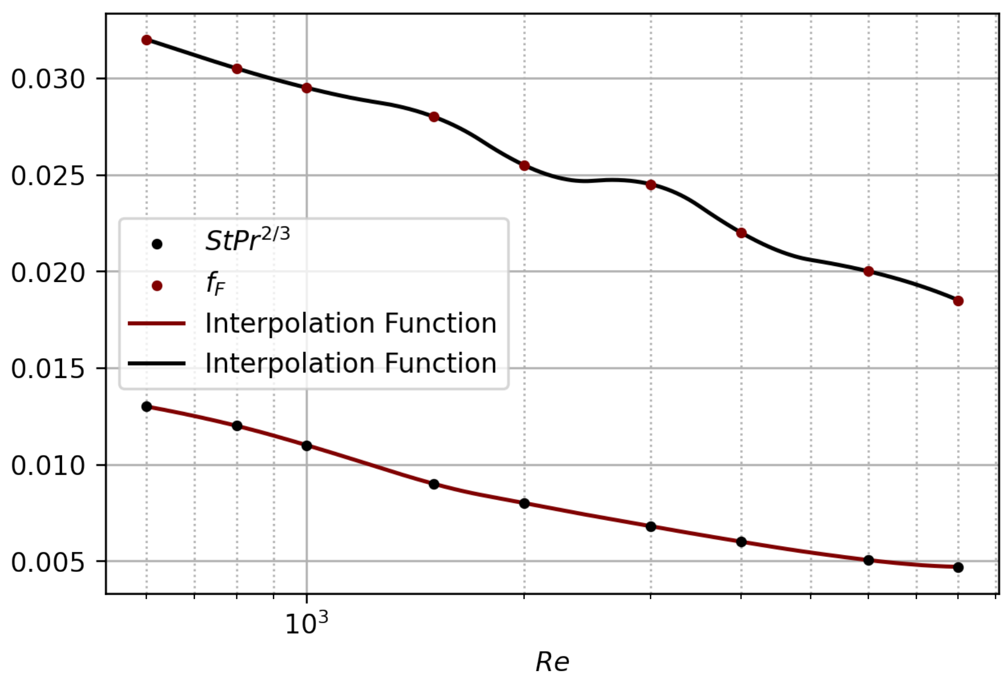
3.4 Surface 8.0-3/8T

The process above may be copied with different values from the database.

[17]:
```
# Getting graph
Re = np.array([600, 800, 1000, 1500, 2000, 3000, 4000, 6000, 8000])
hts = np.array([0.013, 0.012, 0.011, 0.009, 0.008, 0.0068, 0.006, 0.00505, 0.
↪0047])
fF = np.array([0.032, 0.0305, 0.0295, 0.028, 0.0255, 0.0245, 0.022, 0.02, 0.
↪0185])
hts_lamb = interp1d(Re, hts, kind='quadratic')
fF_lamb = interp1d(Re, fF, kind='quadratic')
Re_values = np.linspace(Re[0], Re[-1], 1000)

plt.scatter(Re, hts, label='$StPr^{2/3}$', zorder=3, marker='.', color='black')
```

```python
plt.scatter(Re, fF, label='$f_F$', zorder=3, marker='.', color='maroon')
plt.plot(Re_values, hts_lamb(Re_values), label='Interpolation Function',␣
 ↪zorder=2)
plt.plot(Re_values, fF_lamb(Re_values), label='Interpolation Function',␣
 ↪zorder=2)
plt.xscale('log')
plt.xlabel('$Re$')
plt.grid(which='minor', ls=':')
plt.legend()
plt.show()
```



Property	Value
Tube outside diameter	0.402 in
Fin Pitch	8 per inch
Hydraulic Diameter (D_h)	0.01192 ft
Fin Thickness (Copper)	0.013 in
Free flow area/frontal area (σ)	0.534
Total heat transfer/total volume (α)	179 $\frac{ft^2}{ft^3}$
Fin area/total area	0.913

3.4.1 Airside

[18]:
```python
# Find the velocity of the air then use that to find Re
N1, N2, N3 = 7, 582, 81
L1 = 0.866*N1/12  # ft
L2 = 0.138*N2/12  # ft
L3 = 1.000*N3/12  # ft
vol = L1*L2*L3 # ft^3
print(f'L1: {L1*12:.3f} in')
print(f'L2: {L2*12:.3f} in')
print(f'L3: {L3*12:.3f} in')
print(f'Volume: {vol:.3f} ft^3')
Da = 0.01192 # ft (from database)
sigma = 0.534 # from database
Va = mdot_a/(L2*L3*sigma*rho_a) # ft/sec
print(f'Velocity: {Va:.3f} ft/s')
G = Va*rho_a
Re_a = G*Da/mu_a
print(f'Re: {Re_a:.3f}')
L1_list.append(f'{L1*12:.3f}')
L2_list.append(f'{L2*12:.3f}')
L3_list.append(f'{L3*12:.3f}')
vol_list.append(f'{vol:.3f}')
air_vel_list.append(f'{Va:.3f}')
air_re_list.append(f'{Re_a:.3f}')
```

```
L1: 6.062 in
L2: 80.316 in
L3: 81.000 in
Volume: 22.822 ft^3
Velocity: 49.053 ft/s
Re: 1000.520
```

[19]:
```python
h_a = hts_lamb(Re_a)*G*cp_a/(Pr_a**(2/3))
h_a  # Btu/(s ft^2 F)
```

[19]:
```
0.006192366863039942
```

[20]:
```python
alpha = 179 # ft^2/ft^3
A_ratio = 0.913
A = alpha*vol # ft^2
L_fin = (1 - 0.402)/2/12 # ft
k_fin = 221/3600 # Btu/(sec ft F) assuming copper
t_fin = 0.013/12 # ft
m = np.sqrt(h_a*2/(k_fin*t_fin))
eta_fin = np.tanh(m*L_fin)/(m*L_fin)
print(f'Fin Efficiency: {eta_fin:.3f}')
eta_t = 1 - A_ratio*(1 - eta_fin)
```

```
print(f'Total Efficiency: {eta_t:.3f}')
R_fin = 1/(eta_t*A*h_a)
print(f'Resistance: {R_fin:.3f} sec F/Btu')
```

```
Fin Efficiency: 0.963
Total Efficiency: 0.966
Resistance: 0.041 sec F/Btu
```

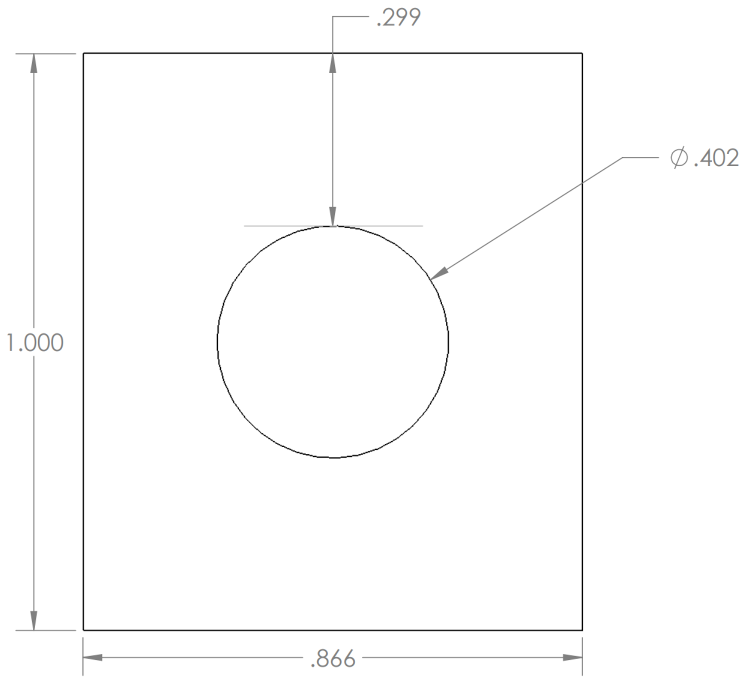


Figure 4: Surface 8.0-3/8T Tube Geometry

Assuming that the thickness of the tube is negligible, the hydraulic diameter of the tube is the diameter $D_c = 0.402\,in$, since the geometry is circular. The contraction ratio, σ, is the cross-sectional area divided by the repeating pattern area.

$$\sigma_c = \frac{\frac{\pi}{4} \cdot 0.402^2}{1 \cdot 0.866} = 0.147$$

The heat transfer area is $A_c = \alpha_c \cdot V$, where α_c is the surface area density, which is the surface area inside the tubes divided by the repeating pattern volume. If a $1\,in$ chunk of the pattern is considered, the surface area density is,

$$\alpha_c = \frac{\pi \cdot 0.402\,in \cdot 1\,in}{1\,in \cdot 0.866\,in \cdot 1\,in} = 1.458\,\frac{in^2}{in^3} = 17.5\frac{ft^2}{ft^3}$$

3.4.2 Waterside

[21]:
```
Dc = 0.402/12  # ft
alpha_c = 17.5  # ft^2/ft^3
# sigma_c = (np.pi/4*0.402**2)/0.866
Vw = 3  # ft/sec
Gw = Vw*rho_w  # lbm/(s ft^2)
Re_w = Gw*Dc/mu_w
print(f"Re: {Re_w:.3f}")
water_re_list.append(f'{Re_w:.3f}')
```

```
Re: 49641.711
```

[22]:
```
# Since the flow is turbulent,
Nu = 0.023*Re_w**0.8*Pr_w**0.333
print(f'Nu: {Nu:.3f}')
h_w = Nu*k_w/Dc
print(f'h: {h_w:.3f} Btu/(s ft^2 F)')
Ac = alpha_c*vol
print(f'Ac: {Ac:.3f} ft^2')
Rw = 1/(Ac*h_w)
print(f'Resistance: {Rw} F*sec/Btu')
```

```
Nu: 135.042
h: 0.440 Btu/(s ft^2 F)
Ac: 399.390 ft^2
Resistance: 0.0056896789401672575 F*sec/Btu
```

[23]:
```
# Solving for UA_iter
UA_iter = 1/(Rw + R_fin)*3600
print(f'UA_iter: {UA_iter:.3f} Btu/(hr F)')
print(f'UA_iter/UA: {UA_iter/UA:.3f}')
```

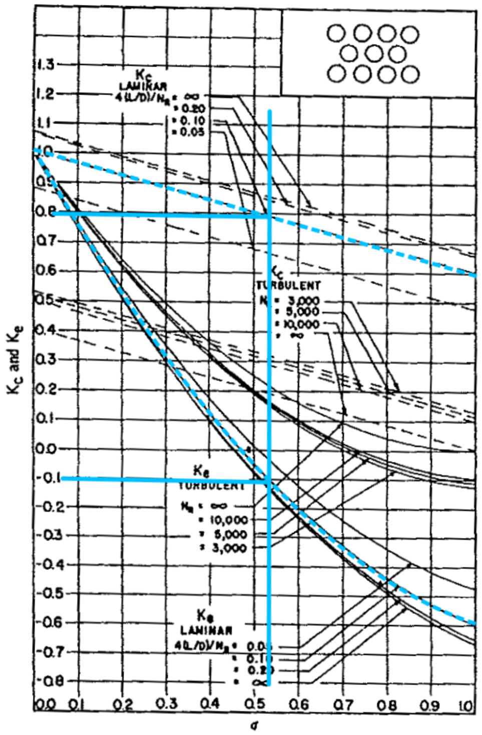
```
UA_iter: 77260.220 Btu/(hr F)
UA_iter/UA: 1.042
```

Thus, the final dimensions of the heat exchanger are $L_1 = 6.062\,in$, $L_2 = 80.316\,in$, and $L_3 = 81\,in$. Looking at Figure 4, the limitations are,

$$0.866 \cdot N_1 = L_1$$
$$0.138 \cdot N_2 = L_2$$
$$1.000 \cdot N_3 = L_3$$

3.4.3 Airside Pressure Drop

An important part of calculating the pressure drop is determining the K_c and K_e values. According to W.M. Kays and A.L. London's *Compact Heat Exchangers*, the less developed the fluid should have K_c values that are lower than K_c values for a fully developed flow (meaning viscous effects are present), and K_e values should be higher for the less developed flows (p. 110). The entrance length for this scenario is $L_H = 0.05(1000)(0.01192) = 0.596\,ft = 7.152\,in$, which is greater than the width for which the air travels (L_1). This means that the flow is not fully developed.



(a) Entrance and exit pressure loss coefficients for a multiple-circular-tube heat exchanger core with abrupt-contraction entrance and abrupt-expansion exit.

Figure 5: K_c and K_e for Circular Tubes

Because the flow is in the inviscid region, a less conservative line from the plot in Figure 5 was chosen.

[24]:
```
# From figure above
Kc, Ke = 0.8, -0.1

x1 = Kc + 1 - sigma**2
x2 = 2*(rat - 1)
x3 = float(fF_lamb(Re_a))*A/(L2*L3*sigma)*rho_a_in/rho_a
x4 = (1 - sigma**2 - Ke)*rat

del_P = G**2/(2*rho_a_in)*(x1 + x2 + x3 - x4)/32.174
pressure_list.append(f'{del_P:.3f}')
del_P   # lbf/ft^2
```

[24]:
```
7.0623039585879255
```

Thus, the pressure drop across the airside is $7.06\,\frac{lbf}{ft^2}$.

3.4.4 Power Consumption

[25]:
```
# Calculating the power
eta = 0.75
Q_a = mdot_a/rho_a  # ft^3/s
power = Q_a*del_P/eta
power_kW = power*0.00135581795
print(f'Power: {power:.3f} ft*lbf/s = {power/550:.3f} hp = {power_kW:.3f} kW')
power_list.append(f'{power/550:.3f}')
```

```
Power: 11143.453 ft*lbf/s = 20.261 hp = 15.108 kW
```

[26]:
```
 # Calculating the cost per year
cost_per_year = 0.05*8760*power_kW + 9*12*power_kW
print(f'Cost Per Year: ${cost_per_year:.2f}/year')
cost_list.append(f'{cost_per_year:.2f}')
```

```
Cost Per Year: $8249.24/year
```

Thus, the operating cost of the 8.0-3/8T surface is $8249.24/year.

4 Results and Discussion

[27]:
```
# Generating table
data = [
    L1_list,
    L2_list,
    L3_list,
    vol_list,
    air_vel_list,
    air_re_list,
    pressure_list,
    power_list,
    cost_list
]
index = [row[0] for row in data]
df = pd.DataFrame([row[1:] for row in data], columns=['9.29-0.737-SR', '8.0-3/
 ↪8T'], index=index)
# df
display(Latex(fr'\begin{{center}}{df.to_latex(escape=False)}\end{{center}}'))
```

	9.29-0.737-SR	8.0-3/8T
L_1 (in)	7.110	6.062
L_2 (in)	70.448	80.316
L_3 (in)	70.950	81.000
Volume (ft^3)	20.566	22.822
Air Velocity $(\frac{ft^3}{s})$	43.266	49.053
Airside Reynold's	1000.939	1000.520
ΔP $(\frac{lbf}{ft^2})$	7.266	7.062
Airside Power (hp)	20.845	20.261
Annual Cost	8487.23	8249.24

The table above shows a summary of the calculated results. Some key takeaways are,

1. The volume for the 8.0-3/8T heat exchanger is greater than the 9.29-0.737-SR, thus, taking up more space overall.
2. The 8.0-3/8T heat exchanger has the smaller width, L_1.
3. The 8.0-3/8T heat exchanger is more cost-efficient.

Given the following above, the heat exchanger to select should be the 8.0-3/8T because it is thinner and more cost-efficient by almost 3%. Although the cost savings may not be substantial enough to justify the selection alone, the real advantage is that it can fit in narrower spaces. This, however, is only useful if the space has a length long enough to fit the 81" × 80.316" square surface, which is assumed to be present along the Centaur 50 given the size of the system shown in Figure 6.

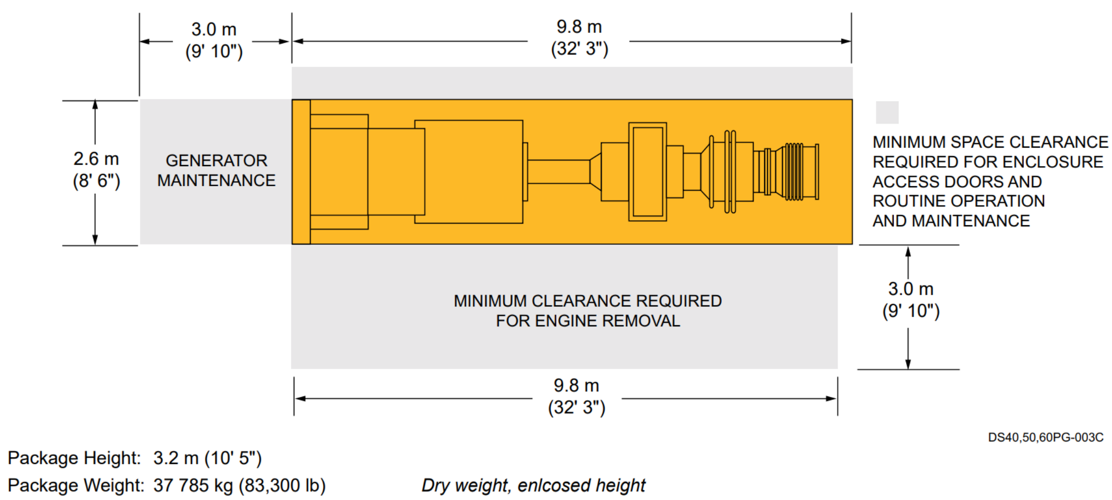


Figure 6: Enclosure Access and Maintenance Space

From Figure 6, notice that the height of the system is 10'5", and the width is 8'6". This is sufficient space to fit the larger 81" × 80.316" square of the 8.0-3/8T heat exchanger.