

DESIGN OF A PID CONTROLLER FOR A MOLTEN SALT MICROREACTOR

A Thesis

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ABSTRACT

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DEDICATION

To my mother, Tammy, who planted and nurtured my love of science. To my father, Paul, who taught me how to design and build, and showed me that I am an engineer. To my cats, Babe and Bunyan, who stayed up with me all those late nights studying and writing. Thank you for your endless support.

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LIST OF CODES

1	Hello!	20
2	F strings	20

ACRONYMS

INL Idaho National Laboratory.

LTI Linear Time-Invariant.

LWR Light Water Reactor.

MIMO Multi-Input Multi-Output.

MSNB Molten Salt Nuclear Battery.

MSR Molten Salt Reactor.

MSRE Molten Salt Reactor Experiment.

NPP Nuclear Power Plant.

NRC Nuclear Regulatory Commission.

NREL National Renewable Energy Laboratory.

ORNL Oak Ridge National Laboratory.

PID Proportional-Integral-Derivative.

SISO Single-Input Single-Output.

CHAPTER 1

INTRODUCTION

The world is working to move away from fossil fuel as its main energy source [1]. National Renewable Energy Laboratory (NREL) has partnered with over 700 organizations, including large manufacturing companies, to de-carbonize supply chains [2]. Nuclear power has been well established as an alternative for base-load electrical generation with 93 facilities in the United States and 435 globally which generate on the order of 1 GWe, but there remains a need for smaller reactors to be deployed in more dynamic applications such as small remote grids (including military bases [3]), manufacturing, and power-peaking [4]. These small energy utilizers could turn to microreactors to fill their needs; to make this a reality, a robust control system for microreactors must be designed that is capable of ramping production up and down to meet demand.

1.1 MICROREACTORS

Microreactors, as the name suggests, are small nuclear reactors which are designed to be fully assembled when shipped, rather than constructed on site. This is a hot area of research in the private sector as companies are working to capitalize on the growing need for clean and dependable small scale electrical generation [5]. They aim not to replace the utility scale Nuclear Power Plants (NPPs) which handle base-load electrical generation, but the diesel or natural gas engines that are found at countless manufacturing facilities, peaking stations, military bases, islands, and other locations where on-site generation is the primary or only source of electricity.

The goal is to be able to deliver a prefabricated microreactor to a site, integrate it to the necessary power cycles and process heat applications, and meet the needs of the site for a long period of time - up to a decade - without the need for refueling or significant maintenance. This would be quite convenient compared to building a pipeline to deliver fossil fuels to the site or scheduling regular delivery. One of the biggest challenges in implementing microreactors is the transients that these applications often require. Engines handle these quite well, simply adjusting the flow rates of fuel and combustion air. Nuclear reactor load following is a bit more complicated, as the reactor must be made supercritical to ramp up power or subcritical to decrease power. This necessitates valid characterization of the reactor's criticality control & actuation system and reactivity feedback mechanisms, so an effective 'reactor-following-turbine'

controller can be tuned [6, Ch. 8].

1.2 MOLTEN SALT REACTORS

Molten salts are highly desirable in high temperature applications due to their excellent thermophysical properties [7]. Salt mixtures have been developed to have very wide liquid temperature ranges (i.e. low melting point and high vaporization point). They also have very high volumetric heat capacities compared to other high temperature coolants (which tend to be gaseous), and are able to operate at or slightly above ambient pressure. These properties combine to make molten salts excellent choices in heat transfer and thermal storage applications. Furthermore, they are extremely strong electrolytes which can be useful as solvents, catalysts, or reagents in certain chemical reactions including a pyrometallurgical method for reprocessing spent nuclear fuel [8].

Molten Salt Reactors (MSRs) are a family of nuclear reactor in which a fuel salt (containing fissile and/or fertile nuclides) is dissolved in a coolant salt [9]. The concept was proven by the Molten Salt Reactor Experiment (MSRE) at Oak Ridge National Laboratory (ORNL) in the 1960s [10]. It has yet to take off beyond the research reactor sector, but it has re-emerged as a Gen-IV reactor concept, with a team at the Shanghai Institute of Applied Physics gaining approval to operate a now fully constructed thorium breeding MSR [11]. Some of the benefits of MSRs over more conventional LWRs include:

- Higher operating temperatures allow for use in applications requiring high-grade process heat, and yield higher thermal efficiency [9];
- Lower pressure operating pressure lends itself to inherent safety, and less expensive (thinner) components [7];
- The ability to burn minor actinides supports the goal of reducing global stockpiles of high-level waste [7];
- Natural circulation of the fuel introduces an additional feedback mechanism that presents the possibility of autonomous load following of certain power demand transients [12];
- There is no concern of core melt-down as the reactor is designed for liquid fuel;
- The liquid state homogenizes nuclides throughout the core, which minimizes burn-up gradient to produce a flatter temperature and power profile within the core [13, Ch. 3]. The flowing nature also allows for online reprocessing, removing fission products and poisons during operation;

They also carry some demerits:

- Molten salts are very corrosive [14];
- The chemistry of the coolant (not only the fuel) is constantly changing due to fission, transmutation, and impurities from corrosion;
- Lithium is commonplace in molten salts, so tritium production is unavoidable (Rxn. 1.1). Off-gas systems need to be robust to handle tritium as well as radionuclide noble gasses, halides, and inter-halides [15];



1.3 MOLTEN SALT NUCLEAR BATTERY

The Molten Salt Nuclear Battery (MSNB) is a self contained design for a liquid fueled molten salt microreactor [16, 5]. It is fueled by an inorganic form of uranium, UF_4 , dissolved in a coolant salt such as $FLiNaK$ (a eutectic mixture of three alkali fluorides) or $FLiBe$ (a mixture of LiF and BeF_2) [9]. Heat is generated in the core by fission and is rejected in an integrated heat exchanger (Fig. 1.1). Criticality is manipulated using axial control drums, which may be rotated to aim either a neutron reflecting material or a neutron absorbing material towards the core. The design studied in this work is intended to produce up to 1 MWth, although larger designs of up to 50 MWth also exist.

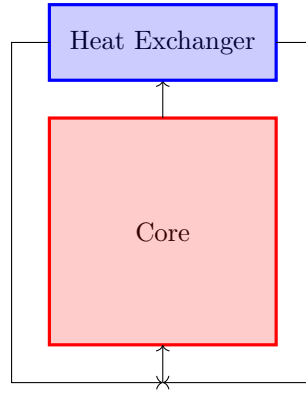


Figure 1.1: Simplified schematic drawing of an MSNB. Heat is generated in the core by fission, is transported by natural circulation of the coolant/fuel salt, and rejected to a secondary working fluid in the heat exchanger before returning to the inlet plenum through the downcomer.

1.4 SCOPE

As a developing design, work has been done on neutronics [5], thermal-hydraulics and autonomous load following [16], and corrosion concerns [17]. However, until now, little to no work has been done on the control system. First and foremost, this work details a multiphysics characterization of the MSNB required to design a feedback controller capable of matching the core power generation to the secondary power demand. In addition to the main control mode of following power transients during normal operation, specific discussion is centered around more dynamic time periods, namely: 1) initial start-up; 2) shutdown, both planned and emergency; and 3) restart;

CHAPTER 2

PROCESS CONTROL ENGINEERING

There are two main goals in process control engineering: 1) Reference tracking, where a process variable is matched to a set-point which may be changed over time; and 2) Disturbance rejection, where the process variable is held to the set-point despite outside influence upsetting it; This is usually achieved by a controller which detects the process variable using a sensor/transmitter and controls the process variable by manipulating an actuator.

2.1 FEEDBACK

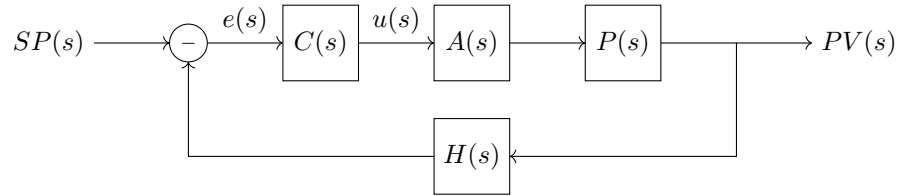


Figure 2.1: Feedback control loop. The output (PV) is measured by the transducer (H) and compared to the set-point (SP). The controller (C) uses the actuator (A) to control the process (P) based on the error (e).

The most common type of controller is a feedback controller. Figure 2.1 shows a simple feedback control loop with a sensor/transmitter (*i.e.* transducer), controller, and actuator working together to control a process. The controller takes action based on the ‘error’ (e) between the set-point (SP) and process-variable (PV) (Eqn. 2.1).

$$e(t) = PV(t) - SP(t) \quad (\text{Eqn. 2.1})$$

The action, or controller output (u) is often determined by a Proportional-Integral-Derivative (PID) equation (Eqn. 2.2), which considers the instantaneous, cumulative, and predictive error in determining the proper actuation [18, Ch. 5]. This equation has three terms:

- 1) Proportional control term. The control output is manipulated in proportion to the error defined by

the proportional gain constant (K_P). A high gain yields an aggressive controller that is prone to overshooting the set-point, while a low gain may result in steady-state offset.

- 2) Integral control term, which considers the historical cumulative error (calculated by taking the time integral of the error) in an effort to eliminate steady-state offset that a P-Only controller may exhibit. As the process variable settles around the set-point, the cumulative error approaches a constant value and the effect of the integral controller diminishes.
- 3) Derivative control term, which estimates the time rate of change of the error to dampen overshoot. This mechanism, sometimes referred to as anticipatory control, slightly reduces the proportional response to the error when the error is changing rapidly. This results in reducing the peak overshoot. A well tuned anticipatory gain can allow a more aggressive proportional gain to be used without the large overshoot.

Derivative control will be important because the controller manipulates criticality to control power generation, a highly time dependent system.

$$u(t) = \underbrace{K_P e(t)}_{\text{Proportional}} + \underbrace{K_I \int_0^t e(t) dt}_{\text{Integral}} + \underbrace{K_D \frac{de(t)}{dt}}_{\text{Derivative}} \quad (\text{Eqn. 2.2})$$

Instead of using three different gain constants, it is common for controllers to be tuned in terms of a single controller gain (K_C) plus two time constants: 1) The integral time constant (τ_I); and 2) The derivative time constant (τ_D); In this case, Eqn. 2.2 is rewritten as:

$$u(t) = K_C \left(e(t) + \tau_I^{-1} \int_0^t e(t) dt + \tau_D \frac{de(t)}{dt} \right) \quad (\text{Eqn. 2.3})$$

2.2 FEEDFORWARD

The term ‘Feedforward’ can be used to refer to any element in the control block diagram that exists outside of the feedback loop. In process control, feedforward controllers are almost always implemented alongside, not instead of feedback controllers because a standalone feedforward controller is not guaranteed to reach the set-point.

DISTURBANCE FEEDFORWARD

In many processes, the process variable is effected by phenomena other than the actuator. These other phenomena are defined as disturbances. A well-tuned feedback controller is capable of disturbance rejection, but only after the disturbance causes error. In some cases, a disturbance feedforward controller may be added to the feedback controller to cause the actuator to counteract the effect of the disturbance before it occurs [18, Ch. 10].

The most prevalent disturbances that would effect the power output of the core of a MSNB are the temperature reactivity feedback effect common to all nuclear reactors and the flow reactivity specific to natural circulation driven liquid fueled MSRs [12]. Temperature reactivity feedback is dominated by Doppler Broadening, where the microscopic radiative capture cross section resonance peaks of nuclides such as ^{238}U are depressed to cover a wider epithermal neutron spectrum [19, Ch. 6]. This results in



Figure 2.2: Feedback control loop with disturbance feedforward. It is identical to Fig. 2.1 with the addition of a disturbance (D) which effects the process variable (PV) according to the disturbance dynamics (P_D), and is measured by the disturbance transducer (H_D). The signal from H_D is sent to the disturbance feedforward controller (C_D) who's output (u_D) is combined with (u) to form the total control output (u^*).

a smaller core neutron population and less fission events, so there is a negative correlation between fuel temperature and fuel reactivity. Flow reactivity is driven by the advection of delayed neutron precursors [6, Ch. 3]. Not all fission neutrons are released promptly; sometimes an unstable nuclide which decays by neutron emission produced instead. These unstable nuclides are called delayed neutron precursors and have half-lives ranging from less than a second to over a minute [20, Ch. 7]. Since the fuel in a MSNB is flowing, there is a statistical probability that a delayed neutron precursor may leave the core by advection before the neutron is emitted in a much less reactive part of the reactor. When the temperature differential between the thermal center of the core and primary heat exchanger is increased, so too does the natural circulation flow rate. This decreases the likelihood of delayed neutrons being emitted in the core, and negatively contributes to core reactivity. Devices meant to elongate the in-core flow path may minimize delayed neutron losses [16].

Disturbance feedforward will not be utilized in the design of the controller outlined in this work. When the outlet temperature of the heat exchanger is decreased, it takes time for the cooler salt to reach the core. The disturbance transport delay is on the order of minutes. Contrastly, Doppler Broadening has a nearly instantaneous effect, so disturbance dynamics are on the order of milliseconds, governed by the mean neutron lifetime [20, Ch. 7]. The effect of control actuation are similarly prompt. Even with a temperature sensor just at the inlet of the core it would be nearly impossible to reliably predict the exact moment that control reactivity would be need to be inserted to counteract the temperature reactivity.

PRE-FILTER

The control loop for a feedback system with a pre-filter is included as Figure 2.3. Pre-filters are another type of feedforward mechanism common in control systems. They are typically first-order transfer functions such as Eqn. 2.4 function used to improve the performance of the associated feedback controller (as depicted by Figure 2.4) by 'slowing down' the rate of change of the set-point. The gain (numerator) for a pre-filter is always unity because the desire is only to reshape the input, not resize it. The time-constant (τ_F) describes how quickly the output equilibrates with the input.

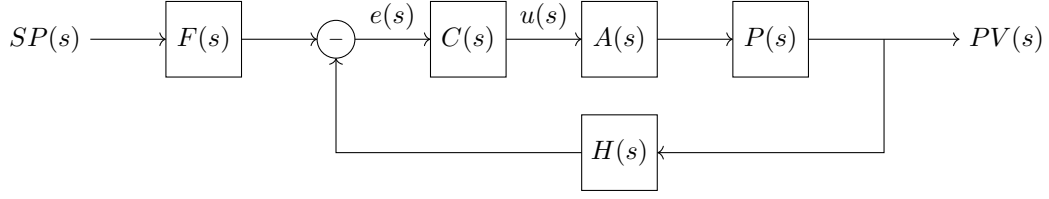


Figure 2.3: Feedback control loop with pre-filter. It is identical to Fig. 2.1 with the addition of the pre-filter (F) which reshapes changes to the set-point (SP) before calculating the error (e).

$$F(s) = \frac{1}{\tau_F s + 1} \quad (\text{Eqn. 2.4})$$

By resisting instantaneous set-point changes, or step functions, the pre-filter minimizes the instantaneous error during transients and minimizes overshoot by reducing over-actuation or actuator saturation. This is particularly useful in a control system such as the one designed in this report where the set-point is coupled to some other value. In this case, the core power generation needs to match the demand of the secondary system (*e.g.* power cycle). This method allows the secondary system to immediately change to its necessary value while giving the reactor core time to safely and effectively respond.

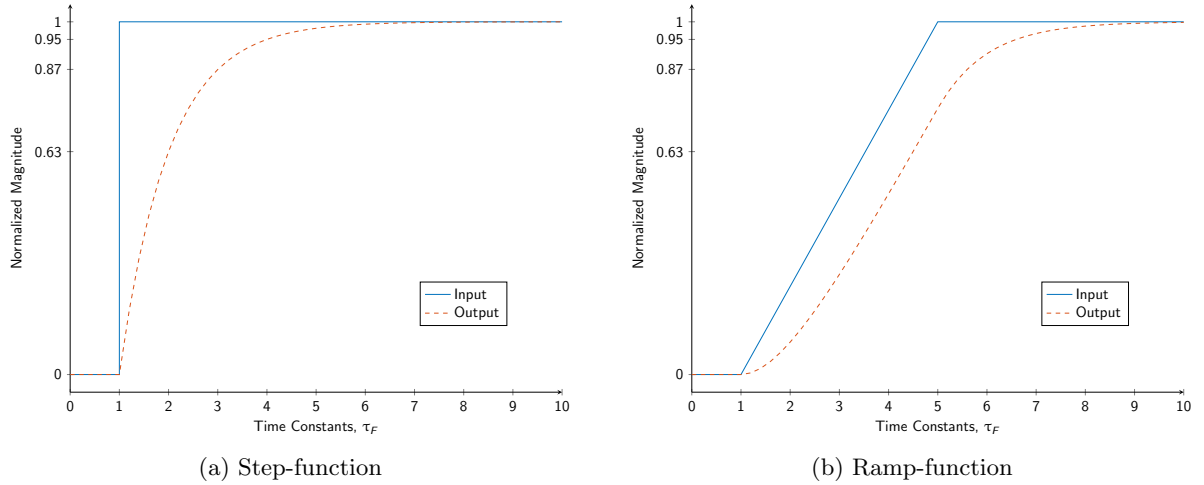


Figure 2.4: Pre-filter on step-function and ramp-function. When the pre-filter acts on a step-function, it follows an exponential curve, reaching 63.2% of the magnitude of the step in 1 time constant, 86.5% in 2 time constants, 95.0% in 3 time constants and so on. The ramp-function exhibits similar but more complicated dynamics due to the changing input.

The area between the solid blue and dashed orange curves corresponds the net amount of energy expelled from the molten salt loop following the transient. This manifests as a drop in the average salt temperature. If the reactor begins to operate near thermophysical boundaries, it may be necessary for the core to over-produce in order to bring the temperature back up. This is one example of how this controller is really a Multi-Input Multi-Output (MIMO) system, though it may be treated as Single-Input Single-Output (SISO) during the preliminary design phase. An alternative approach could be to use a slightly under-damped second-order pre-filter so the core power generation briefly overshoots the heat

exchanger power consumption to balance the energy inequality.

2.3 TRANSPORT DELAY PROBLEM

A good place to start in the design of this controller is discussing the dynamics associated with anticipated transients. The prominent factors here are the natural circulation flow mode and the transport delay separating the heat exchanger and core. Consider a step-increase in power demand to a steady-state critical MSNB where the core power generation set-point is instantaneously equal to the heat exchanger power consumption. For this thought experiment, consider an ideal controller which produces rapid load following with minimal overshoot.

Discussing the transport of cold salt and how it effects the global (flow) and local (temperature) feedback mechanism. Why we want to use a pre-filter and an actuation threshold of sorts.

IMMEDIATE RESPONSE

The heat-exchanger immediately rejects more thermal energy to the secondary loop and the core immediately generates more power. The core outlet temperature increases quite sharply, but since there is a transport delay between the core outlet and heat exchanger inlet (θ_{riser}), this hot salt does not instantaneously reach the heat exchanger, and the heat exchanger outlet temperature drops sharply.

As these hot and cold regions propagate and grow, the natural circulation driving force increases which results in a negative flow reactivity insertion. Assume this is a gradual disturbance which the ideal controller can effectively reject by a counteracting insertion of positive control reactivity.

HEAT EXCHANGER PERTURBATION

Following the response to the initial step-increase, the first notable event occurs when the hot region in the riser reaches the heat exchanger. This produces a hot ‘edge’ in the downcomer temperature profile that lags the cold edge by approximately θ_{riser} .

CORE PERTURBATIONS

The next event occurs when the cold edge reaches the core inlet, $\theta_{downcomer}$ after the step-increase, causing a rapid insertion of positive temperature reactivity which must be rejected by the controller. θ_{riser} later, the hot edge inserts negative temperature reactivity. Each of these responses cause subsequent temperature edges which rise to the heat exchanger and continue through the system. It is apparent that the ‘ideal’ controller actually inhibits the ability for the reactor to return to steady-state following a transient, instead prolonging both flow reactivity and temperature reactivity oscillations.

A pre-filter that reshapes the core set-point will make the initial hot edge more gradual. Proper tuning of the pre-filter time-constant will allow the reactivity oscillations to decay more quickly. Previous work [12] has shown that the passive feedback mechanisms (temperature and flow reactivity) are capable of autonomous load following for small transient, though not at the level of performance that may be required in certain applications. Still, this provides the opportunity to minimize fine and rapid actuation while dampening oscillations; the ‘ringing out’ of minor perturbations could be left to the passive feedback mechanisms.

2.4 TIME-VARIANCE AND NON-LINEARITY

Control Drum Angle vs. Reactivity Curve - non-linearity, Fissile depletion - time variance, the fact that we are actually controlling the criticality and not the power directly - ??

In control systems, it is typically preferred to work with Linear Time-Invariant (LTI) systems

Fissile depletion - time function parameters or look-up table to gain-schedule and turn the time variant system into a shift invariant system.

In addition to the relatively slow time variance of fissile fuel depletion during steady-state critical operation, there are specific times in a MSNB's expected operational life-cycle that exhibit a higher degree of time variance: 1) Start-up; 2) Shut-down; and 3) Re-start.

START-UP

Because microreactors are meant to be delivered in a fully or mostly assembled state, it is likely that the MSNB will be shipped with the molten fuel/coolant salt mixture frozen *in-situ*. The salt will need to be melted before initial start-up, and the heat source for melting the cannot be fission, as the MSNB requires advective heat removal caused by natural circulation; this is not possible if the flow channels between the core and heat exchanger are frozen. One possible method for salt thawing involves passing low-voltage high-current electricity through the pipes in contact with the salt, similar to how frozen water pipes are thawed [21];

Initial start-up will also require a neutron source as a seed for the fission chain reaction [19, Ch. 2]. ^{235}U undergoes spontaneous fission [22, Ch. 6], and at high enrichment may be used as the only neutron seed simply by putting the control actuators in a supercritical orientation. More commonly, a dedicated source is used, such as ^{252}Ca , which undergoes spontaneous fission much more rapidly, or a composite of a strong alpha-emitter (*e.g.* ^{238}Pu , ^{241}Am , ^{210}Po , or ^{226}Ra) and ^9Be which emits a neutron according to Rxn. 2.1 [23, Ch. 2].



Each of these systems are important considerations for the design of the MSNB and warrant further investigation, but are out of scope for this work. The main start-up consideration regarding the control system is the build-up of fission product neutron poisons.

Xenon Poisoning

^{135}Xe is the strongest known neutron poison, with a microscopic neutron capture cross-section of 2.65 Mb [20, Table II.2]. The concentration of ^{135}Xe is described by a system of differential equations which quantifies the generation, consumption, and decay of itself and its beta-precursor ^{135}I . Equations Eqn. 2.5 and Eqn. 2.6 can be used to track the concentrations of iodine-135 and xenon-135 during start-up, steady-state operation, power transients, shut-down, and dead-time [20, Ch. 7].

$$\frac{dI}{dt} = \underbrace{\gamma_I \Sigma_f^F \phi(t)}_{\text{Fission Yield}} - \underbrace{\lambda_I I(t)}_{\text{Beta Decay}} \quad (\text{Eqn. 2.5})$$

$$\frac{dXe}{dt} = \underbrace{\gamma_{Xe} \Sigma_f^F \phi(t)}_{\text{Fission Yield}} + \underbrace{\lambda_I I(t)}_{\text{Precursor Decay}} - \underbrace{\lambda_{Xe} Xe(t)}_{\text{Beta Decay}} - \underbrace{Xe(t) \sigma_a^{Xe} \phi(t)}_{\text{Radiative Capture}} \quad (\text{Eqn. 2.6})$$

Each nuclide is formed by ^{235}U fission, and removed by beta-decay. Additionally, ^{135}Xe is formed by the beta-decay of ^{135}I and removed by radiative neutron capture¹. Each nuclide builds-up in the reactor until the formation terms, i.e. fission yield and precursor decay, equilibrate with the removal terms, beta decay and radiative capture. By setting the time derivatives to zero, the neutron flux dependent equilibrium concentrations (Eqn. 2.7 and Eqn. 2.8) may be derived algebraically [20, Ch. 7] and can contribute over 2000 pcm of negative poison reactivity to the core.

$$I_{\infty}(\phi) = \frac{\gamma_I \Sigma_f^F}{\lambda_I} \phi \quad (\text{Eqn. 2.7})$$

$$Xe_{\infty}(\phi) = \frac{(\gamma_I + \gamma_{Xe}) \Sigma_f^F}{\lambda_I + \sigma_a^{Xe} \phi} \phi \quad (\text{Eqn. 2.8})$$

Samarium Poisoning

The second most important neutron poison to consider after ^{135}Xe is ^{149}Sa . ^{149}Pm is formed by fission² and decays to ^{149}Sa , which is stable, and has a large neutron capture cross-section [20, Ch. 7]. Eqn. 2.9 looks identical to Eqn. 2.5, but Eqn. 2.10 is simpler than Eqn. 2.6 as ^{149}Sa is stable and is not a direct fission product.

$$\frac{dPm}{dt} = \underbrace{\gamma_{Pm} \Sigma_f^F \phi(t)}_{\text{Fission Yield}} - \underbrace{\lambda_{Pm} Pm(t)}_{\text{Beta Decay}} \quad (\text{Eqn. 2.9})$$

$$\frac{dSa}{dt} = \underbrace{\lambda_{Pm} Pm(t)}_{\text{Precursor Decay}} - \underbrace{Sa(t) \sigma_a^{Sa} \phi(t)}_{\text{Radiative Capture}} \quad (\text{Eqn. 2.10})$$

This system too reaches an equilibrium which may be found algebraically where the time derivatives are null. Eqn. 2.11 is of the same form as Eqn. 2.7. Interestingly Eqn. 2.12 is independent of the neutron flux in the core. Because it is stable, it is only removed by the same neutron flux that forms it, and contributes a relatively constant 442 pcm of poison reactivity.

$$Pm_{\infty}(\phi) = \frac{\gamma_{Pm} \Sigma_f^F}{\lambda_{Pm}} \phi \quad (\text{Eqn. 2.11})$$

$$Sa_{\infty}(\phi) = \frac{\gamma_{Pm} \Sigma_f^F}{\sigma_a^{Sa}} \quad (\text{Eqn. 2.12})$$

Burnable Poison Control

LWRs are commonly controlled using neutron absorbing materials in two ways [6, Ch. 8]: 1) Burnable poisons (typically poisons whose daughter are neutron-transparent [19, Ch. 14]) placed in certain fuel

¹In reality, the decay chain is a bit more complicated than this. ^{135}Te , the direct beta-precursor to ^{135}I is formed by ^{235}U fission [24]. Its half-life is orders of magnitude shorter than ^{135}I , so it is common to neglect its formation and instead lump its fission yield with ^{135}I . ^{135m}Xe is also formed by ^{135}I beta-decay and is neglected for similar reasons.

²As with ^{135}I , ^{149}Pm actually comes from the decay of a much shorter lived nuclide ^{149}Nd . Because neither ^{149}Pm nor ^{149}Nd are strong neutron absorbers, the presence of ^{149}Nd may be neglected in favor of its longer lived daughter product.

rods to flatten the power profile; and 2) Soluble poisons (*i.e.* Chemical Shim) dissolved in the moderator/coolant to account for long term fission product poison build-up and fissile material depletion. In MSRs, these two concepts may be combined by adding a neutron absorber such as ^{10}B to the molten salt mixture to counter-act the poison reactivity built-up by equilibrium poisons like ^{135}Xe and ^{149}Sm . Boron could be added to the salt by dissolving BF_3 gas [25] or sodium fluoroborates such as NaBF_4 [26], either of which could be natural composition or enriched in ^{10}B . As the concentration of the fission product poisons build up, the concentration of ^{10}B depletes; unlike chemical shimming, the consumed ^{10}B would not be replenished. Making the average core reactivity equivalent upon cold-clean start-up and equilibrium would allow gain and bias scheduling to be more simple early in the fuel lifetime.

SHUT-DOWN

Planned shut-down, either for scheduled maintenance or due to a lack of demand, is quite simple. The heat exchanger load is brought to zero or very low power, and the core set-point gradually follows. Careful selection of the pre-filter time constant can alleviate potential thermal hydraulic (*e.g.* stagnation or reverse-flow) and thermophysical (*e.g.* salt precipitation, freezing, or vaporization) concerns [12]. The emergency shutdown (*i.e.* SCRAM) system must be passive. In LWRs, this is achieved by including large control rods which are actively held out of the core, so that a loss of power results in automatic insertion. Larger MSR designs may include a SCRAM tank into which the fuel/coolant salt drains in the event of power failure. These systems are often actuated by a freeze plug [27] and put the salt in a subcritical orientation by the inclusion of neutron control materials [28, Ch. 1] and high geometric buckling [20, Ch. 6]. Planned shut-down, either for scheduled maintenance or due to a lack of demand, is quite simple. The heat exchanger load is brought to zero or very low power, and the core set-point gradually follows. Careful selection of the pre-filter time constant can alleviate potential thermal hydraulic (*e.g.* stagnation or reverse-flow) and thermophysical (*e.g.* salt precipitation, freezing, or vaporization) concerns [12].

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Whether the reactor is shut down for planned purposes or in an emergency, a decay heat [13] removal system will need to be designed to keep the salt from vaporizing. The same heat exchanger used for the secondary loop could be used for this purpose, but there should also be a passive system that rejects decay heat in the event of total power failure, such as a direct contact system which removes heat through the vaporization of sodium [29]. This latent heat driven system is ideal because it minimizes the possibility of the salt freezing due to over-cooling.

RE-START

Compound dynamics in the ^{135}Xe decay chain result in the generation of a large poison reactivity in the hours following a shut-down. This can make restarting the reactor difficult or impossible for a period of approximately two days. When the reactor is shut down, each flux-containing term in the system of ODEs (Eqn. 2.5 and Eqn. 2.6) goes to zero, and the concentrations of the two nuclides are described by the Bateman equations [30], which have a readily available solution (Eqn. 2.13 and Eqn. 2.14), given some initial condition [20]. ^{135}I follows simple exponential decay. ^{135}Xe has a longer half-life than ^{135}I , as well as a lower equilibrium concentration (owing to its huge radiative capture cross-section). This causes an inverse response, where the ^{135}Xe concentration initially spikes before its population grows and the ^{135}I population shrinks to the point that the rate of ^{135}Xe decay exceeds its formation.

$$I(t) = I_0 e^{-\lambda_I t} \quad (\text{Eqn. 2.13})$$

$$Xe(t) = Xe_0 e^{-\lambda_{Xe} t} + \frac{\lambda_I I_0}{\lambda_I - \lambda_{Xe}} (e^{\lambda_{Xe} t} - e^{\lambda_I t}) \quad (\text{Eqn. 2.14})$$

This system of equations is not ideal, as it results in mandatory reactor dead time. Most nuclear reactors are not designed with enough excess control reactivity to overcome the iodine pit, so they must wait for the xenon to decay. Even if the control system does have the ability to restart during the xenon peak, it can be very unsafe to do so. When the fission chain reaction is restarted, the neutron flux increases and begins transmuting ^{135}Xe . The removal of poisons is akin to positive reactivity insertion [24]. Decreasing poison concentration increases the neutron population and therefore the rate of poison removal. This is a positive feedback system which could run away quickly if control reactivity is not removed to match.

The duration of the xenon spike may be shortened by adding an additional negative term to Eqn. 2.6. This is not physically realizable in cladded solid fuel reactors. It is however possible to remove a gaseous solvent from a liquid (such as MSR fuel) through a process called stripping [31, Ch. 10]. Helium may be bubbled through the molten salt in a sparge tube, and the xenon (as well as any other fission gasses [32]) would preferentially transport into the gaseous phase which would later be separated in a cyclone or similar apparatus [33]. This advective removal of ^{135}Xe would allow the MSNB to be restarted without having to wait for the poison to decay. ^{149}Sm is stable and strongly dissolved in the molten salt, so it is always ‘burnt off’ during restart [20, Ch. 7].

CHAPTER 3

REACTOR CHARACTERIZATION

3.1 REACTOR DESIGN SELECTION

3.2 NEUTRONICS MODELING

3.3 PROCESS SIMULATION

CHAPTER 4

CONTROLLER DESIGN

4.1 REACTOR TRANSFER FUNCTION

4.2 TUNING METHODOLOGY

CHAPTER 5

RESULTS AND ANALYSIS

CHAPTER 6

CONCLUSIONS

6.1 LIMITATIONS

6.2 FUTURE WORK

6.3 SUMMARY REMARKS

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APPENDIX A

TEST

Code 1: Hello!

```
1 print("Hello World") #comment
2 try:
3     a=2/x
4 except ZeroDivisionError:
5     print('undefined')
```

Inline codes like `import` numpy

Code 2: F strings

```
1 x = 4
2 print(f"The numeral four: {x}")
3 #comment
```

APPENDIX B

WHAT

Straight Cash Homie