MXB326 Group Project - Reservoir Simulation

 $\begin{array}{c} {\rm MXB326_23se1~Computational~Methods~2} \\ {\rm Due~26-05-2023} \end{array}$

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1 Introduction

Oil is a natural resource which is used abundantly in modern society. Necessary for the creation of fuels which transport us around the world, to materials in products we use hundreds of times a day, and many applications in between, it is no stretch to say that civilisation as we know it relies on oil. But the production of oil can be a slow and costly process. One method commonly used in the oil industry to improve production is called water-flooding. This processes uses the injection of water into the porous rock structure of an oil reservoir to increase the pressure, driving more oil out. Modelling this process mathematically is a key interest of a field of research known as reservoir engineering, and is of vital importance to ensure that the process of water-flooding runs smoothly.

This modelling, involving the simultaneous flow of two viscous fluids through a horizontal reservoir in three dimensions, is quite complex. Fortunately, the model can be substantially simplified when considering a homogeneous, one-dimensional reservoir. This simplification in turn reduces what would be a coupled system of partial differential equations into a single, one-dimensional PDE. To describe the mechanics of the system, the conservation of mass of oil and water assuming immiscibility and incompressibility, are given by the transport equations:

$$\phi \frac{\partial S_w}{\partial t} + \frac{\partial q_w}{\partial x} = 0 \tag{1}$$

$$\phi \frac{\partial S_o}{\partial t} + \frac{\partial q_o}{\partial x} = 0 \tag{2}$$

In this system, ϕ indicates how porous the medium of the reservoir is, and S_w and q_w , S_o and q_o indicate the saturation and flow rate of the water and oil respectively. We relate the pressure in each fluid as the capillary pressure: $P_c = p_o - p_w$, and assume that the capillary pressure is positive. Furthermore, the saturations of the oil and water can be related as $S_w + S_o = 1$, allowing a single saturation, $S = S_o$ to be the sole variable to be modelled. Also defined are the minimum, irreducible saturations S_{or} and S_{wr} .

For a comprehensive description of the mathematical system, it is also necessary to define the conditions at the boundaries of the domain. Figure 1 demonstrates the domain of the problem.

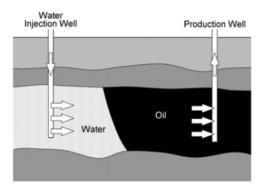


Figure 1: Schematic of the oil injection process.

Assuming a constant injection of water at x = 0 at rate q:

$$q_w(0,t) = q$$
 and $q_o(0,t) = 0$ (3)

And assuming oil saturation begins at its maximum value:

$$S(x,0) = 1 - S_{wr} (4)$$

Finally, assuming a semi-infinite reservoir:

$$\lim_{x \to \infty} S(x, t) = 1 - S_{wr} \tag{5}$$

For an efficient and cost-effective water-flooding operation, it is critical to prevent the water from mixing with the oil in the well-bore (extraction point). We thus define the breakthrough time as $T_B = 1 - S_{or} - S_{wr}$, the time taken for the water to reach the well-bore during the water-flooding. Specification of a suitable injection rate q is capable of preventing this issue from arising.

This report contains a pilot study of the simplified system above, including a mathematical model with a semi-analytic solution and a numerical solution. These solutions will be analysed thoroughly, with the goal of demonstrating the capability of a fully detailed study in the future.

2 Mathematical Model

It is possible to derive an exact solution for the system described above using methods from Fokas and Yortsos, in the case of constant injection rates when the water to oil viscosity ratio F has the form

$$F = \frac{1 - S_{wr} + \frac{\gamma}{\beta}}{S_{or} + \frac{\gamma}{\beta}} \tag{6}$$

Applying this, the following one-dimensional initial boundary value problem can be derived for the oil saturation:

$$\frac{\partial S}{\partial t} = \frac{\partial}{\partial x} \left[g(S) \frac{\partial S}{\partial x} + f(S) \right], \tag{7}$$
$$S(x,0) = 1 - S_{wr}, \tag{8}$$

$$S(x,0) = 1 - S_{wr}, (8)$$

$$\frac{\partial S}{\partial x}(0,t) = \frac{\alpha}{\beta}(\beta S(0,t) + \gamma) + \frac{\omega}{\beta}(\beta S(0,t) + \gamma)^2, \tag{9}$$

$$\lim_{x \to \infty} S(x, t) = 1 - S_{wr}. \tag{10}$$

By specifying $S_{wr}, S_{or}, F, \text{and}\beta$, the remaining parameters can be determined from (6) as well as the relations

$$\frac{\alpha}{\beta^2} = -\frac{\left(S_{or} + \frac{\gamma}{\beta}\right)\left(1 - S_{wr} + \frac{\gamma}{\beta}\right)}{1 - S_{wr} - S_{or}},\tag{11}$$

$$\omega = \beta - \frac{\alpha}{\beta - \beta S_{wr} + \gamma}. (12)$$

Using these equations, γ can be found with equation (6), α with γ and equation (11), and ω using the other two parameters with equation (12). This process has been implemented in the function paramsFunc.

Furthermore, the functions f(S) and g(S), called the capillary-hydraulic properties of the fluidporous system are given by

$$f(S) = \frac{\alpha}{\beta^2} \left[\frac{1}{1 - S_{wr} + \frac{\gamma}{\beta}} - \frac{1}{S + \frac{\gamma}{\beta}} \right], \quad g(S) = \frac{1}{(\beta S + \gamma)^2}.$$

These functions allow for an exactly solvable PDE (7), and also correspond to a physically meaningful model.

3 Semi-Analytical Solution

A semi-analytical solution for (7) can be derived at discrete space x_i and time t_n by applying the spacial transformation

$$\tilde{x} = \int_0^x (\beta S(\xi, t) + \gamma) d\xi + \omega t, \tag{13}$$

This linearises the equation and yields the solution for S:

$$S(x,t) = \frac{1}{\beta} \left[\frac{\alpha e^{\alpha x}}{\frac{\partial \phi}{\partial \tilde{x}}(\tilde{x},t)} - \gamma \right], \tag{14}$$

where \tilde{x} is the solution of $\phi(\tilde{x},t)=e^{\alpha x}$ for a given x and t. The solution of the nonlinear equation must be obtained using MATLAB's fzero function. The MATLAB documentation for this function indicates that it is used to find the roots of nonlinear function. Specifically, for some input x = fzero(func, x0), x will return a point where func(x) = 0. The fzero function requires an initial guess x_0 such that $func(x_0) \approx 0$. An appropriate guess for each i = 1..N and n = 1..M can be found by evaluating (13) at $x = x_i$ and $t = t_{n-1}$. Let \hat{x} indicate the approximate initial guess. Thus we have:

$$\hat{x}_{i,n} = (\beta S(x_i, t_{n-1}) + \gamma) x_i + \omega t_{n-1}$$
(15)

This results in an iterative process for the semi-analytical solution: for each t_n , solve for all x_i using $S(x_i, t_{n-1})$. For the initial guess at $t = t_1$, the initial condition (8) is applied. This provides \hat{x} for all x_i at $t = t_1$:

$$\hat{x}_{i,1} = [\beta(1 - S_{wr}) + \gamma] x_i \tag{16}$$

With an iterative solution defined and appropriate initial conditions, the solution can be straightforwardly determined using MATLAB. This solution is implemented in the MATLAB script semianalytic.m, and produces the following result:

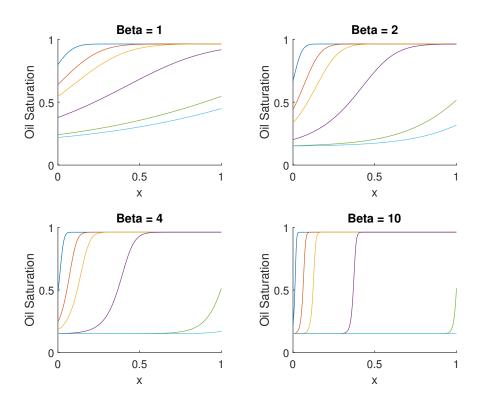


Figure 2: The semi analytical solution, plotted from x = 0 to x = 1 at t = 0.01, 0.05, 0.1, 0.3, 0.8125, 1, for $\beta = 1, 2, 4, 10$.

4 Numerical Solution

5 Analysis and Findings

- 5.1 Comparison of semi-analytical solution and numerical solution
- 5.2 Average reservoir oil saturation
- 5.3 Computational efficiency analysis
- 5.4 Buckley-Leverett solution analysis

For large β , the capillary forces are negligible when compared to the viscous forces. As a result, the method of characteristics can be used to obtain a simplified solution. The solution exhibits Buckley-Leverett shock front behaviour given by

$$S(x,t) = \begin{cases} S_{or}, & x < vt, \\ 1 - S_{wr}, & x > vt. \end{cases}, \text{ where } v = \frac{1}{1 - S_{wr} - S_{or}}$$
 (17)

This is implemented in MATLAB as the function BuckleyLeverett.m. Plotting the Buckley-Leverett shock front against the semi-analytical solution with $\beta = 10$, it can be seen that the semi-analytical solution does exhibit the shock front behaviour:

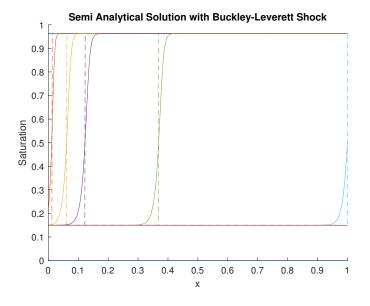


Figure 3: The semi-analytical solution with $\beta = 10$ plotted against the Buckley-Leverett shock front.

Similarly for the numerical solution:

As has been observed in the plots previously, increases of β correspond to increases of the slope of the front between the phases. As such, the shock front behaviour of becoming perfectly vertical as $\beta \to \infty$ is reasonable.

5.5 Impact of different injection rates

- 6 Conclusions
- 7 References