

ASSIGNMENT-1

MODEL- SOLUTION

(CHE221A)

18-3] Given; $P_A = 0.2 \text{ MPa}$, $V_A = 0.01 \text{ m}^3$
 $U = 2.5 PV + \text{constant} \quad \text{--- (1)}$

→ For A → B;

$$\Delta W_{AB} = -P \Delta V$$
$$= -(0.2 \times 10^6)(0.03 - 0.01)$$

$$\boxed{W_{AB} = -4000 \text{ J}}$$

$$U_A = (2.5)(0.2 \times 10^6)(0.01) + C$$

[Using (1)]

$$\boxed{U_A = 5000 + C}$$

$$U_B = (2.5)(0.2 \times 10^6)(0.03)$$

$$\boxed{U_B = 15000 + C}$$

$$\therefore \Delta U_{AB} = U_B - U_A$$

$$\boxed{\Delta U_{AB} = 10000 \text{ J}}$$

(3)

→ Using 1st Law of Thermodynamics, --

$$Q_{AB} = \Delta U_{AB} - W_{AB}$$

$$\boxed{Q_{AB} = 14000 \text{ J}}$$

→ For B → C;

W_{BC} = Area under BC segment in PV diagram

$$\boxed{W_{BC} = 7000 \text{ J}}$$

$$U_C = 2.5 \times (0.5 \times 10^6) \times 0.01 + C$$

$$\boxed{U_C = 12500 + C}$$

$$\Delta U_{BC} = U_C - U_B$$

$$\boxed{\Delta U_{BC} = -2500 \text{ J}}$$

$$\Delta U_{BC} = Q_{BC} + W_{BC}$$

$$\Rightarrow \boxed{Q_{BC} = -9500 \text{ J}}$$

→ For C to A:-

$$\Delta W_{CA} = 0$$

From 1st law of Thermodynamics

$$\Delta U_{CA} = \Delta Q_{CA}$$

$$\therefore \boxed{\Delta Q_{CA} = -7500 \text{ J}}$$

→ Given; $P = 10^5 + (V - 0.02)^2 \times 10^9$

$$W_{AB} = - \int P dV$$

$$= - \int_{V_A}^{V_B} [10^5 + 10^9 (V - 0.02)^2] dV$$

$$= - \left\{ 10^5 [V]_{0.01}^{0.03} + \left[\frac{(V - 0.02)^3}{3} \right]_{0.01}^{0.03} \times 10^9 \right\}$$

$$= - \{ 2000 + 666.67 \}$$

$$\boxed{W_{AB} = -2666.67 \text{ J}}$$

8-4

Given,

$$U = 2.5 PV + \text{constant}$$

$$\therefore dU = 2.5 PdV + 2.5 VdP \quad \text{--- (1)}$$

→ From 1st Law of Thermodynamics;

$$dU = dQ + dW$$

For adiabatic,

$$dQ = 0$$

$$\therefore dU = dW$$

From (1)

$$2.5 PdV + 2.5 VdP = -PdV$$

~~$$2.5 PdV = -3.5 PdV$$~~

$$2.5 VdP = -3.5 PdV$$

$$\frac{dP}{P} = -\frac{7}{5} \frac{dV}{V}$$

$$[\because dW = -PdV]$$

Integrating;

$$\int_{P_1}^{P_2} \frac{dP}{P} = -\frac{7}{5} \int_{V_1}^{V_2} \frac{dV}{V}$$

$$[\ln(P)]_{P_1}^{P_2} = -\frac{7}{5} [\ln(V)]_{V_1}^{V_2}$$

$$\Rightarrow P_1^5 V_1^7 = P_2^5 V_2^7$$

Hence;

Equation of adiabatic is as below:-

$$P^5 V^7 = K$$

1.8-7

Given; $U = APV^2$, $N = 2$

TO get U in terms of P , V & N we write

$$U = APV^2 \cdot f(N)$$

Here $f(N) = aN^m$;

Moreover; $f(2) = a \cdot 2^m$

$$\therefore 1 = a \cdot 2^m$$

→ Rewriting in terms of P ;

$$P = \frac{U}{(AV^2) \cdot (a2^m)} \quad \text{--- (1)}$$

→ If we ~~increase~~ double the system then;

$$P = \frac{2U}{A(4V^2) \cdot a4^m} \quad \text{--- (2)}$$

→ Since P does not change (1) = (2)

$$\therefore \frac{2U}{A(4V^2)(4^m)} = \frac{U}{AV^2(2^m)}$$

$$2^m = 2 \cdot 4^m$$

$$m \ln(2) = \ln(2) + m \ln(4)$$

$$\Rightarrow \boxed{m = -1} \quad \& \quad \boxed{a = 2}$$

$$\therefore U = APV^2 \cdot a(2)^{-1}$$

$$\boxed{U = \frac{2aAPV^2}{2N}}$$

[1.10-1]

$$(f) S = NR \ln(UV/N^2 R \theta_0)$$

Let: $NR = A$ & $\frac{UV}{N^2 R \theta_0} = B$

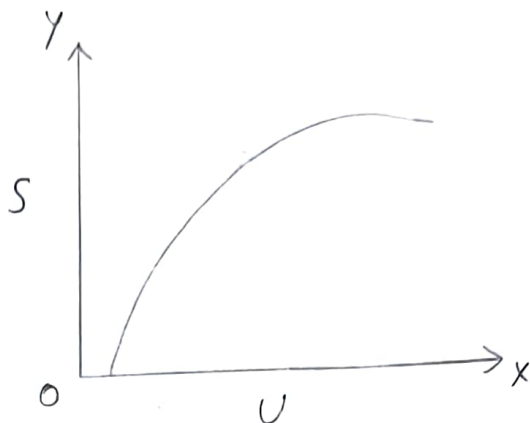
$$\therefore S = A \ln(UB)$$

→ Rewriting in terms of U we get;

$$U = \frac{1}{B} e^{S/A}$$

$$\rightarrow \left(\frac{\partial U}{\partial S}\right)_{V,N} = \frac{1}{B} e^{S/A} \cdot \frac{1}{A}$$

$$\left(\frac{\partial U}{\partial S}\right)_{V,N} = \frac{1}{AB} e^{S/A}$$



Moreover,

$$\left(\frac{\partial U}{\partial S}\right)_{V,N} = T$$

$$\therefore \frac{1}{AB} e^{S/A} = T$$

→ As LHS term can become zero only when

$S \rightarrow -\infty$, but this violates 4th postulate of Thermodynamics which says at zero absolute temp. entropy of system is also zero.

Given

$$\frac{1}{T^{(1)}} = \frac{3}{2} R \frac{N^{(1)}}{U^{(1)}}, \quad N^{(1)} = 2$$

$$\frac{1}{T^{(2)}} = \frac{5}{2} R \frac{N^{(2)}}{U^{(2)}}, \quad N^{(2)} = 3$$

$$U_{\text{Total}} = 2.5 \times 10^3 \text{ J}$$

\therefore The wall is diathermal, the system will achieve thermal eqb when

$$\frac{1}{T^{(1)}} = \frac{1}{T^{(2)}}$$

(4)

$$\frac{3}{2} R \frac{N^{(1)}}{U^{(1)}} = \frac{5}{2} R \frac{N^{(2)}}{U^{(2)}}$$

putting the value of $N^{(1)} = 2$ & $N^{(2)} = 3$

$$\Rightarrow \frac{6}{U^{(1)}} = \frac{15}{U^{(2)}}$$

$$\boxed{15 U^{(1)} - 6 U^{(2)} = 0} \quad \text{--- (1)}$$

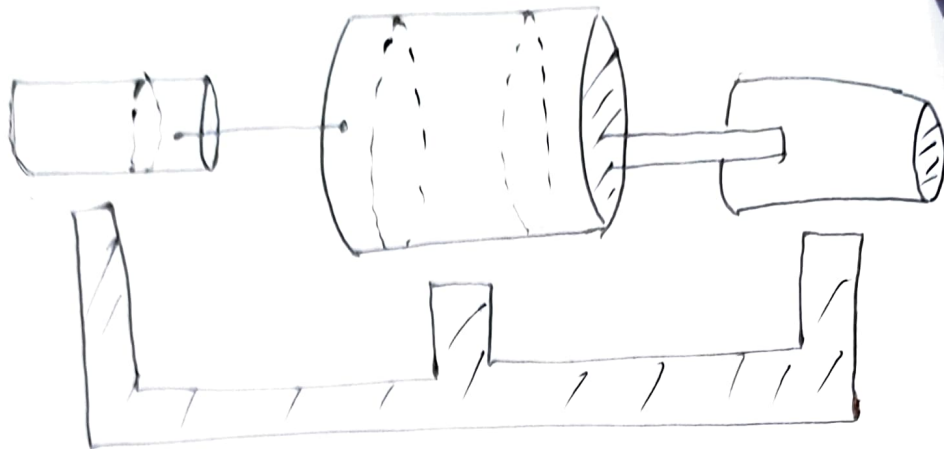
we also have

$$U_{\text{Total}} = U^{(1)} + U^{(2)} = 2500 \text{ J} \quad \text{--- (2)}$$

on solving equation (1) & (2)

$$\boxed{\begin{aligned} U^{(1)} &= 714.29 \text{ J} \\ U^{(2)} &= 1785.714 \text{ J} \end{aligned}}$$

2.7-1



$$dV^{(1)} = A_1 dl_1, \quad dV^{(2)} = A_2 dl_2, \quad dV^{(3)} = A_3 dl_3$$

$$\boxed{dU = dU^{(1)} + dU^{(2)} + dU^{(3)} = 0}$$

$$dV^{(3)} = -3dV^{(1)} - \frac{3}{2}dV^{(2)} \quad (\because A_1 : A_3 : A_2 = 1 : 3 : 2)$$

Now,

$$dS = \frac{1}{T^{(1)}} dU^{(1)} + \frac{p^{(1)}}{T^{(1)}} dV^{(1)} + \frac{1}{T^{(2)}} dU^{(2)} + \frac{p^{(2)}}{T^{(2)}} dV^{(2)} \\ + \frac{1}{T^{(3)}} dU^{(3)} + \frac{p^{(3)}}{T^{(3)}} dV^{(3)}$$

at eq⁶ $ds = 0$

$$\left(\frac{1}{T^{(1)}} - \frac{1}{T^{(3)}} \right) dU^{(1)} + \left(\frac{1}{T^{(2)}} - \frac{1}{T^{(3)}} \right) dU^{(2)} + \left(\frac{p^{(1)}}{T^{(1)}} - \frac{3p^{(3)}}{T^{(3)}} \right) dV^{(1)} \\ + \left(\frac{p^{(2)}}{T^{(2)}} - \frac{3}{2} \frac{p^{(3)}}{T^{(3)}} \right) dV^{(2)} = 0$$

$$\text{So, } \boxed{\frac{1}{T^{(1)}} = \frac{1}{T^{(2)}} = \frac{1}{T^{(3)}}}$$

$$p^{(1)} = 3p^{(3)}$$

$$p^{(2)} = \frac{3}{2}p^{(3)}$$

$$\boxed{\text{Ratio of pressure} = 1 : \frac{1}{2} : \frac{1}{3}}$$

$$\therefore P = \text{Force} \times \text{Area}$$

$$p^{(1)} = F \times A^{(1)}$$

$$\therefore A_1 : A_3 : A_2 = 1 : 3 : 2$$

As we know

$$U = U(s, v, x_1, x_2, \dots)$$

Taking total differential of equation we get, where $x_i = \frac{N_i}{N}$

$$du = \left(\frac{\partial U}{\partial s} \right)_{v, x_1, x_2, \dots} ds + \left(\frac{\partial U}{\partial v} \right)_{s, x_1, x_2, \dots} dv + \sum_i \left(\frac{\partial U}{\partial x_i} \right)_{s, v, x_{i \neq j}} dx_i$$

Also, we know

$$\left(\frac{\partial U}{\partial v} \right)_{s, x_1, x_2, \dots} = -p \quad \left(\frac{\partial U}{\partial s} \right)_{v, x_1, x_2, \dots} = T \quad \left(\frac{\partial U}{\partial x_i} \right)_{s, v, x_{i \neq j}} = \mu_i$$

So,

$$\boxed{du = Tds - pdv + \sum_j^r \mu_j dx_j} \quad \text{--- (1)}$$

$$du = Tds - pdv + \sum_{j=1}^{r-1} \mu_j dx_j + \mu_r dx_r$$

$$\therefore x_1 + x_2 + x_3 + \dots + x_r = 1$$

$$\Rightarrow dx_1 + dx_2 + dx_3 + \dots + dx_r = 0$$

$$\left(\sum_{j=1}^{r-1} dx_j \right)$$

$$\Rightarrow dx_r = - \sum_{j=1}^{r-1} dx_j \quad \text{--- (2)}$$

putting dx_r in eqn (2)

$$du = Tds - pdv + \sum_{j=1}^{r-1} \mu_j dx_j + \mu_r \sum_{j=1}^{r-1} -dx_j$$

$$\boxed{du = Tds - pdv + \sum_{j=1}^{r-1} (\mu_j - \mu_r) dx_j}$$

proved

2.2-1

As we have

$$U = \left(\frac{V_0 \theta}{R^2} \right) \frac{s^3}{NV}$$

So, equation of state in ^{term of} temperature (we know):-

$$\left(\frac{\partial U}{\partial S} \right)_{N,V} = T$$

$$\Rightarrow \boxed{T = \frac{3s^2 V_0 \theta}{R^2 NV} = \left(\frac{V_0 \theta}{R^2} \right) \frac{3s^2}{NV}}$$

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Equation of state in term of pressure is as follow:-

$$P = - \left(\frac{\partial U}{\partial V} \right)_{S,N} = - \frac{V_0 \theta}{R^2} \left(\frac{-s^3}{NV^2} \right)$$

$$\boxed{P = + \left(\frac{V_0 \theta}{R^2} \right) \frac{s^3}{NV^2}}$$

Equation of state in term of chemical potential is as follow:-

$$\mu = \left(\frac{\partial U}{\partial N} \right)_{S,V} = \frac{V_0 \theta}{R^2} \left(\frac{-s^3}{N^2 V} \right)$$

$$\boxed{\mu = - \left(\frac{V_0 \theta}{R^2} \right) \frac{s^3}{N^2 V}}$$

For Equation of state to be homogeneous zero order

we replace $S \rightarrow KS, N \rightarrow KN, V \rightarrow KV$
(S, V, N):

where K is arbitrary constant

$$\text{Let's take } T' = \left(\frac{V_0 \theta}{R^2} \right) \frac{3K^2 s^2}{(KN) \cdot (KV)}$$

$$\boxed{T' = \left(\frac{V_0 \theta}{R^2} \right) \frac{3s^2}{NV} = T}$$

Similarly, we get

$P' = P$ & $\mu' = \mu$ proved.

2.8-1

$$S = NA + NR \ln \left(\frac{U^{3/2} V}{N^{5/2}} \right) - N_1 R \ln \left(\frac{N_1}{N} \right) - N_2 R \ln \left(\frac{N_2}{N} \right)$$

$$N = N_1 + N_2$$

$$\boxed{\frac{\partial S}{\partial U} = \frac{3}{2} \frac{NR}{U}}$$

Given data

$$V_T = 10L$$

$$N_1^{(1)} = 0.5, N_2^{(1)} = 0.75, V^1 = 5L, T^{(1)} = 300K$$

$$N_1^{(2)} = 1, N_2^{(2)} = 0.5, V^2 = 5L, T^{(2)} = 250K$$

For eq

$$\boxed{\frac{U_1^{(1)}}{T^{(1)}} = \frac{U_2^{(2)}}{T^{(2)}}},$$

$$\boxed{\frac{1}{T^{(1)}} = \frac{1}{T^{(2)}}}$$

$$\Rightarrow \frac{\partial S}{\partial U} = \frac{1}{T} = \frac{3}{2} \frac{NR}{U}$$

$$\frac{1}{T^{(1)}} = \frac{3}{2} \frac{N^{(1)} R}{U^{(1)}}, \quad \frac{P^{(1)}}{T^{(1)}} = R \frac{N^{(1)}}{V^{(1)}}$$

$$\frac{U_1^{(1)}}{T^{(1)}} = A + R \ln \left[\frac{U^{(1)3/2} V^{(1)}}{N^{(1)5/2}} \right]$$

$$- \frac{5}{2} R - R \ln \left(\frac{N_1'}{N_1} \right)$$

$$\frac{1}{300} = \frac{3}{2} \times 8.3 \times \frac{1.25}{U^{(1)}}, \quad \frac{1}{250} = \frac{3}{2} \times 8.3 \times \frac{1.5}{U^{(2)}}$$

$$\therefore U^{(1)} = 4668.75 J \quad \& \quad U^{(2)} = 4668.75 J$$

$$U_T = U^{(1)} + U^{(2)} = 9337.5 \text{ J}$$

for eq.

$$\frac{1}{T^{(1)}} = \frac{1}{T^{(2)}} \quad , \quad \frac{U_1^{(1)}}{T^{(1)}} = \frac{U_1^{(2)}}{T^{(2)}}$$

so we have,

$$\frac{N_1^{(1)} + 0.75}{U^{(1)}} = \frac{N_1^{(2)} + 0.5}{U^{(2)}}$$

$$\frac{[U^{(1)}]^{3/2}}{(N_1^{(1)} + 0.75)^{3/2} N_1^{(1)}} = \frac{[U^{(2)}]^{3/2}}{(N_1^{(2)} + 0.5)^{3/2} N_1^{(2)}}$$

\therefore we have

$$\frac{1}{N_1^{(1)}} = \frac{1}{N_1^{(2)}}$$

$$\text{or } N^{(1)} = N^{(2)}$$

$$\therefore N = N^{(1)} + N^{(2)} = 1.5$$

$$\text{so, } N^{(1)} = N^{(2)} = 0.75$$

The final internal energy can be calculated using,

$$U^{(1)} = \left(\frac{0.75 + 0.75}{0.75 + 0.75} \right) U^{(2)}$$

$$U^{(1)} + U^{(2)} = 9337.5$$

So,

$$U^{(1)} = 5093.18 \quad , \quad U^{(2)} = 4244.32$$

Thus the final eq^b temperature is,

$$\frac{1}{T} = \frac{3}{2} R \times \frac{N^{(1)}}{U^{(1)}} = \frac{3}{2} \times 8.3 \times \frac{1.5}{5093.18}$$

giving $T = 272.73$, the pressure can then be calculated by using

$$p^{(1)} = \frac{N^{(1)} R T^{(1)}}{V} = \frac{1.5 \times 8.31 \times 272.3}{5}$$

$$= 679.1 \text{ Pa}$$

~~679.1 Pa~~
~~679.1 Pa~~

$$p^{(2)} = \frac{N^{(2)} R T^{(2)}}{V} = 565.9 \text{ Pa}$$

~~565.9 Pa~~
~~565.9 Pa~~