$$- YA = k_1 CA - k_2 CB = k_1 CAO (1-XA) - k_2 (CAO XA)$$

$$t = \frac{GAO XA}{GAO [k_1 (1-XA) - k_2 XA]}$$

$$k_1$$
 at $280 \text{ K}:- 10^3 \text{ exp} \left(\frac{-2500}{280}\right) \text{ s}^{-1} = 0.1325 \text{ s}^{-1}$

$$K = 7.8 = \frac{k_1 \text{ at } 280 \text{ K}}{k_2 \text{ at } 280 \text{ K}}$$

$$T = \frac{XA}{0.1325(1-XA)-0.0169XA}$$

Von't Hoff equation :-

$$\ln\left(\frac{k_2}{K_1}\right) = \frac{-\Delta H_{syn}}{R} \left[\frac{1}{T_2} - \frac{1}{T_1}\right]$$

$$\ln \left(\frac{K(\tau)}{K_{280}} \right) = \frac{10 \text{ Rcal}}{8.314 \text{ J/wolk}} \left[\frac{1}{480} - \frac{1}{280} \right]$$

$$\Delta H_{800} = -\frac{10 \text{ Kcel}}{\text{mol}} = -\frac{10 \times 4.184 \times 1000 \text{ J/wo}}{1000}$$

$$\ln\left(\frac{K_T}{K_{280}}\right) = \frac{+41840}{8.314} \left[\frac{-1}{672}\right] = -7.488$$

$$k_1$$
 at $480K = 10^3 exp \left(\frac{-2500}{480} \right) = 5.47 s^{-1}$

$$K_T = \frac{k_1}{k_2} = 0.0043$$

$$k_2 = \frac{5.47}{0.0043} = 1272.09 \text{ s}^{-1} \text{ at } 480\text{ K}$$

$$t = 600 = \frac{XA}{R_1(1-XN) - R_2(XA)}$$

Energy bolonce:

$$\frac{CPS}{G_{00}} = 0.2 \frac{Kcal}{Wol.K}$$

$$0 = \dot{Q} + f_{A0} \times 0.2 \times 10^{3} (320 - 280)$$
$$- (-10^{4}) \times f_{A0} \times 0.877$$

$$\dot{Q} = -f_{A0} \left[8000 + 8770 \right] F$$

$$\dot{Q} = -\frac{CAOV}{T} \times 16770$$

$$\frac{Q}{V} = -139.75 \frac{\text{col}}{\text{Lis}}$$

Q = -139.75 Cal Heat romoved per liter of reactor volume to maintain at 280 K operating temperature.