

Tutorial 3

Thermodynamics

* Vapor Quality: is the % by mass of the vapor in the mixture (total).

$$X = \frac{m_{\text{vapor}}}{m_{\text{total}}}$$

* Triple Point?

Tutorial-2

Solⁿ: 1

$$\begin{aligned} 200 \text{ kPa} &= 200 \times 10^3 \text{ Pa} \\ &= 2 \times 10^5 \text{ Pa} \\ &= 2 \text{ bar} \end{aligned}$$

$$1 \text{ bar} = 10^5 \text{ Pa}$$

$$H = U + PV$$

$$U = H - PV$$

$$= 3072.1 \text{ kJ} - 2 \times 10^5 \times 1.3162 \text{ J}$$

$$= 3072.1 \text{ kJ} - \frac{2 \times 10^5 \times 1.3162 \text{ kJ}}{10^3}$$

$$\boxed{U = 2808.86 \text{ kJ}}$$

Ques:

* Latent heat of vaporization, $h_{fg} = h_g - h_f$

* Specific Volume -

$$V = X v_g + (1-X) v_f$$

$X = \text{Quality}$

* Specific Internal Energy -

$$U = H - P V$$

* Specific Enthalpy -

$$H = X h_g + (1-X) h_f$$

Ques:

2 kg of steam at $P = 5 \text{ bar}$ is produced from water at 25°C . Find the amount of heat supplied if the steam is 90% dry.

Sol:

$$X = 0.9$$

Enthalpy for 1 kg of water -

$$h_w = h_f + X h_{fg}$$

$$= 640.12 + 0.9 (h_g - h_f)$$

$$= 640.12 + 0.9 (2747.5 - 640.12)$$

$$h_w = 2536.76 \text{ kJ/kg}$$

at 25°C , Enthalpy of water, $h = 104.89 \text{ kJ/kg}$

$$\text{Heat Required} = 2 (2536.76 - 104.89)$$

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Ques: Calculate Specific Volume, Specific Enthalpy & Specific internal energy of wet steam at 18 bar, dryness fraction is 0.9.

Sol:

Turbinal 2

Sol 2:

$$2890 = 2855.1 + \left(\frac{3064.8 - 2855.1}{300 - 200} \right) \times (T - 200)$$

Sol 3:

At 90°C, from steam table -

$$P = 0.7011 \text{ bar}$$

Required Volume -

$$10 V = x V_g + (1-x) V_f$$

$$= 0.2 \times 2.3616 + 0.8 \times 0.0010361$$

$$= \text{---} \text{---} \text{---} \text{ m}^3$$

Turbinal 4

①

$$P = 50 \text{ bar} = 50 \times 10^5 \text{ Pa}$$

$$T = 500 + 273 = 773 \text{ K}$$

$$V = 1 \text{ m}^3$$

$$PV = nRT$$

$$n = \frac{50 \times 10^5 \text{ Pa} \times 1 \text{ m}^3}{8.314 \times 773} = 77.8 \text{ moles}$$

1 mole of water = 18g

$$778 \text{ moles} \rightarrow 778 \times 18 \text{ g}$$

$$= 14004 \text{ g} \\ = 14.004 \text{ kg}$$

Van der Waals EOS -

$$\left(P + \frac{an^2}{V^2}\right)(V - nb) = nRT$$

$$\left(P + \frac{an^2}{V^2}\right)\left(\frac{V}{n} - b\right) = RT$$

$$\left(50 \times 10^5 + \frac{553.667 \times n^2}{(L)^2}\right)\left(\frac{1}{n} - 0.3 \times 10^{-3}\right) = 8.314 \times 773$$

$$0.554n^2 + 50 \times 10^5 - 1500n = 6427.722n$$

$$0.554n^2 - 7962.722n + 50 \times 10^5 = 0$$

$$n = 65.8, 13715.1$$

✓ ✗

$$\text{wt.} = \frac{65.8 \times 18}{1000} = 11.844 \text{ kg}$$

Ans 2:

$$\text{Total Volume} = 3 \text{ m}^3$$

$$1 \text{ m}^3 \rightarrow \text{Sat. Liquid}$$

$$2 \text{ m}^3 \rightarrow \text{Sat. Vapor}$$

$$P = 3 \times 10^6 \text{ Pa} = 30 \text{ bar}$$

$$M_{liq.} = \frac{V_{li.}}{V_f}$$

$$M_{steam} = \frac{V_g}{V_g}$$

from Sat. Saturated Pressure Steam Table, at $P = 30 \text{ bar}$ -

$$M_{liq.} = \frac{1}{0.0012163}$$

$$M_{steam} = \frac{2}{0.06636}$$

$$M_{liq.} + M_{steam} = M_{total}$$

$$\text{Quality} = \frac{\text{Mass of Steam}}{\text{Total Mass}} = 0.03304$$

$$\text{Enthalpy} = x h_g + (1-x) h_f$$

$$h = 0.03304 \times 2802.3 + (1 - 0.03304) \times 1008.40 = 1067.67 \text{ kJ/kg}$$

$$h = u + Pv$$

$$u = h - Pv$$

$$= 1067.67 - 30 \times 10^5 \times (x v_g + (1-x) v_f)$$

Self 4:

$T \rightarrow$ Same $P \rightarrow$ Same $V \rightarrow$ Same (cylinder)

$$Pv = nRT$$

$$n_{H_2} = n_{He} \Rightarrow$$

$$\frac{7 \times 10^3}{28} = \frac{m}{28 \times 10^3}$$

$$\boxed{m = 7 \text{ kg}}$$

Sol 3:

$$\text{quality} = \frac{M_{\text{vapor}}}{M_{\text{Total mass}}} = 0.6$$

$v =$

$$P = 10^6 \text{ Pa} = 10 \text{ bar}$$

$$\Delta V = V_{\text{final}} - V_{\text{initial}}$$

from Steam Table, at $P = 10 \text{ bar}$ -

$$V_f = \underbrace{0.1943}_{V_g} \times \underbrace{0.6}_{x}$$

at 300°C (superheated) -

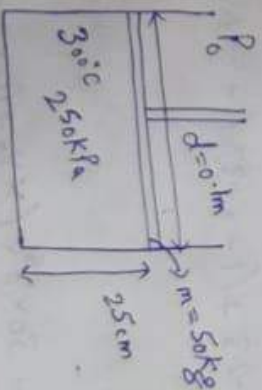
$$V_f = 0.2580 \times 0.6$$

$$\Delta V = 0.6 (0.2580 - 0.1943)$$

$$\begin{aligned} \text{Entropy Change} &= (3052.1 - 2776.2) \times 0.6 \\ &= 272.9 \times 0.6 = 163.74 \text{ kJ} \end{aligned}$$

Tutorial-3

Sol 2:



$$\begin{aligned} \text{(a)} \quad P_{\text{outside}} &= 100 \text{ kPa} + \frac{50 \times 10 \times 1}{3.14 \times 0.1^2 \times 1000} \text{ kPa} \\ &= (100 + 63.69) \text{ kPa} = 163.69 \text{ kPa} \end{aligned}$$

~~Ans: 163.69 kPa~~

$$\frac{P_{\text{outside}}}{T'} = \frac{P_{\text{inside}}}{T_{\text{inside}}}$$

$$T' = 573.13 \text{ K} \times \frac{163.69 \text{ kPa}}{250 \text{ kPa}}$$

$$= 573.13 \times 0.6547$$

$$\boxed{T' = 375.22 \text{ K}}$$

$$(b.) \quad V_1 = 0.25 \times \frac{3.14 \times 0.1 \times 0.1}{4} = ~~1.96~~ \text{ m}^3 \text{ or } 1.96 \text{ L}$$

$$T_1 = 375.22 \text{ K}$$

$$T_f = 293.13 \text{ K}$$

$$V_f = \frac{V_1}{T_1} T_f = \frac{1.96 \times 293.13}{375.22} = 1.53 \text{ L}$$

$$\Delta V = \rho \times h$$

$$h = \frac{0.43 \text{ L} \times 4}{3.14 \times 0.1 \times 0.1 \text{ m}^2} = \frac{0.43 \times 10^{-3} \text{ m}^3 \times 4}{3.14 \times 0.01 \text{ m}^2} = \frac{172}{3140}$$

$$= 0.054 \text{ m}$$

$$= 5.4 \text{ cm}$$