

Phase coexistence in the van der Waals system

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a)

The ideal gas equation is

$$PV = nRT \quad (1)$$

where P is the pressure, V is the volume, n is the number of molecules, $R = kN_a$ is a product of Boltzmann's constant and the Avogadro's constant and T is the temperature of the gas. The *van der Waals* equation makes two modifications to the ideal gas law in equation 1, adding aN^2/V^2 to P and subtracting Nb from V . The first modification accounts for short range attraction between molecules when they're not touching and the second modification supplies the condition that the volume of the gas is greater than zero. Employing the relation $nR = Nk$ and the before-mentioned modifications gives us the van der Waals equation

$$\left(p + \frac{aN^2}{V^2}\right)(V - Nb) = NkT \quad (2)$$

The potential energy is associated with each particles interaction with its neighbour is proportional to the density of particles N/V . The total potential energy associated with all molecules' interaction must then be proportional to N^2/V , since there are N molecules.

$$U_{tot} = -\frac{aN^2}{V} \quad (3)$$

where a is simply some constant which depends on the types of molecules in the gas. Now, if one would vary the volume V slightly, while hoping the entropy S remains fixed, the relation $dU = -PdV$ holds, giving

$$p_U = -\left(\frac{dU}{dV}\right)_S = -\frac{d}{dv}\left(-\frac{aN^2}{V}\right) = \frac{aN^2}{V^2} \quad (4)$$

In absence of attractive forces, the pressure of the fluid would be $NkT/(V - Nb)$, rewriting the ideal gas law and using the effective volume. Adding this to the pressure from equation 4 we land at

$$p = \frac{NkT}{V - Nb} - \frac{aN^2}{V^2} \quad (5)$$

which is equation 2 rewritten in terms of pressure, called the equation of state for a van der Waals gas.

b)

Now, we want to make equation 5 dimensionless. This can be done by introducing the following quantities

$$\hat{p} = \frac{p}{p_c}, \quad \hat{V} = \frac{V}{V_c}, \quad \hat{T} = \frac{T}{T_c},$$

$$p_c = \frac{a}{27b^2}, \quad V_c = 3Nb, \quad kT_c = \frac{8a}{27b}$$

Applying them where needed

$$\begin{aligned} \hat{p} &= \frac{27b^2 NkT}{a(V - Nb)} - \frac{27b^2 aN^2}{aV^2} \\ &= \frac{27b^2 NkT_c \hat{T}}{a(\hat{V}V_c - \frac{1}{3}V_c)} - \frac{27b^2 N^2}{\hat{V}^2 V_c^2} \\ &= \frac{8bN\hat{T}}{\hat{V}V_c - \frac{1}{3}V_c} - \frac{3V_c^2}{\hat{V}^2 V_c^2} \\ &= \frac{8\hat{T}}{3\hat{V}^2 - 1} - \frac{3}{\hat{V}^2}. \end{aligned}$$

We have landed at a neat dimensionless expression.

c)

Figure 1 show the dimensionless pressure \hat{p} as a function of dimensionless volume \hat{V} . One can see that for temperatures $\hat{T} < 1$ the pressure value is not uniquely mapped to a single value for volume. It would therefore be impossible to find $\hat{V}(\hat{p})$.

d)

The dimensionless pressure can also be written in terms of dimensionless density $\hat{\rho}$ using the following quantities

$$\hat{\rho} = \frac{1}{\hat{V}} = \frac{\rho}{\rho_c}, \quad \rho_c = \frac{1}{3b}.$$

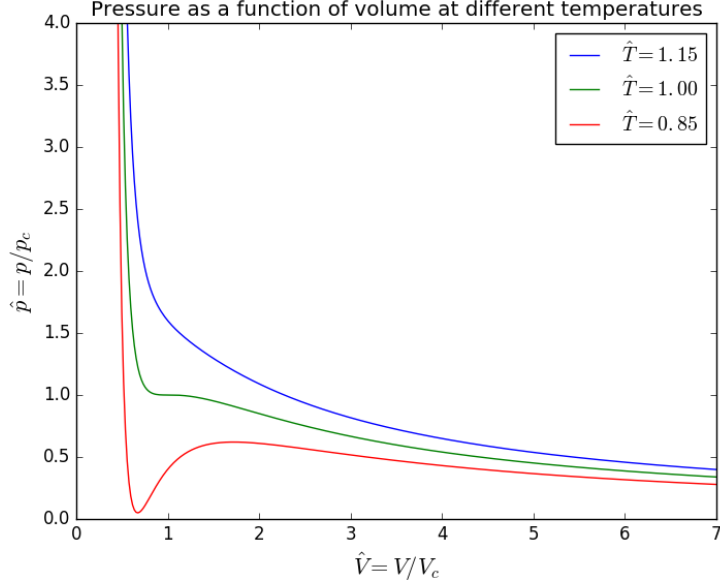


Figure 1: The dimensionless pressure \hat{p} of the system as a function of the dimensionless volume \hat{V} for different temperatures \hat{T} .

Inserting these into equation 5 where needed

$$\begin{aligned}
 \hat{p} &= \frac{27b^2NkT}{a(V-Nb)} - \frac{27b^2N^2}{V^2} \\
 &= \frac{8Nb\hat{T}}{V-Nb} - \frac{3V_c^2}{V^2}\hat{\rho}^2 \\
 &= \frac{V8\hat{\rho}\hat{T}}{V(3-\hat{\rho})} - 3\hat{\rho}^2 \\
 &= \frac{8\hat{\rho}\hat{T}}{3-\hat{\rho}} - 3\hat{\rho}^2
 \end{aligned} \tag{6}$$

Again a neat dimensionless expression.

e, f)

Figure 2 shows the dimensionless pressure \hat{p} plotted against dimensionless density $\hat{\rho}$. One can easily see that $\hat{T} > 1$ gives a unique function for pressure, i.e. $T > T_c$, as was the case for the pressure as a function of volume in the previous two problems.

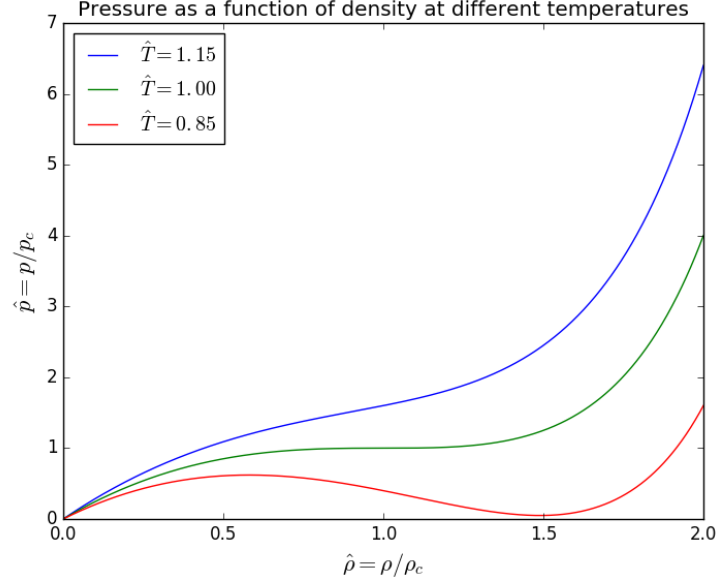


Figure 2: The dimensionless pressure \hat{p} of the system as a function of the dimensionless density $\hat{\rho}$ for different temperatures \hat{T} .

g)

Isothermic compressibility is defined as

$$\kappa = -\frac{1}{V} \left(\frac{\partial V}{\partial p} \right)_{T,N} = \frac{1}{\rho} \left(\frac{\partial \rho}{\partial p} \right)_{T,N} \quad (7)$$

One can see from figure 1 that the isothermic compressibility becomes negative whenever the pressure versus volume curve slopes upwards. This can only happen when $\hat{T} < 1$. In figure 2 the isothermic compressibility is negative when the pressure versus density curve slopes downwards. Here this can also only happen when $\hat{T} < 1$. A negative compressibility means that the system is unstable.

h)

Helmholtz free energy for a van der Waals gas is given by

$$F_{vdW} = -NkT \left(\ln \left(\frac{n_Q(V - Nb)}{N} \right) + 1 \right) - \frac{aN^2}{V}, \quad (8)$$

where $n_Q(T) = (2\pi mkT/h^2)^{3/2}$. In general Helmholtz free energy is $F = U - TS$, while Gibbs free energy is $G = U + pV - TS$ alternatively $G = F + pV$

where, in this particular case

$$pV = \frac{NkTV}{V - Nb} - \frac{aN^2}{V}, \quad (9)$$

and one can easily see that Gibbs free energy for a van der Waals gas must be

$$G_{vdW} = \frac{NkTV}{V - Nb} - \frac{2aN^2}{V} - NkT \left(\ln \left(\frac{n_Q(V - Nb)}{N} \right) + 1 \right) \quad (10)$$

i)

One can find an alternative expression for Gibbs free energy by way of the thermodynamic identity for G

$$dG = -SdT + VdP - \mu dN \quad (11)$$

For a fixed temperature and a given number of molecules this equation reduces to $dG = VdP$, dividing both sides by dV gives

$$\begin{aligned} \left(\frac{\partial G}{\partial V} \right)_{N,T} &= V \left(\frac{\partial P}{\partial V} \right)_{N,T} \\ \left(\frac{\partial G}{\partial V} \right)_{N,T} &= V \left(-\frac{NkT}{(V - Nb)^2} + \frac{2N^2}{V^3} \right) \\ \left(\frac{\partial G}{\partial V} \right)_{N,T} &= -\frac{NkTV}{(V - Nb)^2} + \frac{2N^2}{V^2} \\ G &= -NkT \ln(V - Nb) - \frac{NkT}{V - Nb} - \frac{2aN^2}{V} + c'(T) \end{aligned}$$

Once can rewrite the constant such that $c'(T) = NkTc(T)$ and insert for pV (equation 9) in order to get

$$G_{vdW} = -NkT \ln(V - Nb) - \frac{aN^2}{V} + pV + NkTc(T) \quad (12)$$

One will arrive at this expression by rewriting equation 10 directly as well.

j)

It can be beneficial to rewrite Gibbs free energy to a dimensionless expression. To do this one will need $G_c = 3kT_c/8$. Gibbs free energy per molecule is $\hat{g} = (G/G_c)/N$. I will equate one part of equation 12 at a time.

$$\begin{aligned} -NkT \ln(V - Nb) \frac{1}{G_c N} &= -\frac{8NkT}{3kT_c N} \ln(V - Nb) = -\frac{8}{3} \hat{T} \ln(V - Nb) \\ -\frac{8}{3} \hat{T} \ln(\hat{V} V_c - \frac{1}{3} V_c) &= -\frac{8}{3} \hat{T} \ln(3\hat{V} - 1) - \frac{8}{3} \hat{T} \ln(\frac{V_c}{3}) \end{aligned}$$

Since I'm only interested in terms that depend on \hat{p} and $\hat{\rho}$ I will ignore the second term. So the first term in equation 12 becomes

$$-\frac{8}{3}\hat{T}\ln\left(\frac{3}{\hat{\rho}}-1\right) \quad (13)$$

The constant only depends on T and can also be ignored. The last two parts are

$$\begin{aligned} \left(pV - \frac{aN^2}{V}\right) \frac{1}{G_c N} &= \left(\frac{NkTV}{V-Nb} - \frac{2aN}{V}\right) \frac{1}{G_c N} \\ &= \frac{8\hat{T}V}{3V-VNb} - \frac{16}{3} \frac{2aN}{kT_c V} = \frac{8\hat{T}V}{3V-\hat{\rho}V} - \frac{16}{3} \frac{27b}{8a} \frac{aN}{V} \\ &= \frac{8\hat{T}}{3-\hat{\rho}} - (2)(9) \frac{bN}{V} \end{aligned}$$

The first part is done, but the second still needs some work.

$$-(2)(9) \frac{bN}{V} = -(2)(9) \frac{bN}{\hat{V}V_c} = -(2)(9) \frac{bN}{\hat{V}3Nb} = -(2)(3) \frac{1}{V} = -(2)(3)\hat{\rho}$$

then these last two terms become

$$\frac{8\hat{T}}{3-\hat{\rho}} - 3\hat{\rho} - 3\hat{\rho}$$

which one can write, using equation 6, as

$$\frac{\hat{p}}{\hat{\rho}} - 3\hat{\rho} \quad (14)$$

combining equations 13 and 14 yields the dimensionless form of Gibbs free energy per molecule

$$\hat{g} = \frac{G/G_c}{N} = -3\hat{\rho} - \frac{8}{3}\hat{T}\ln\left(\frac{3}{\hat{\rho}}-1\right) + \frac{\hat{p}}{\hat{\rho}} \quad (15)$$

k, l)

In figure 3 are three plots. The first one shows pressure of the system as function of density, the second shows volume as a function of pressure and the last one shows Gibbs free energy for each molecule. We see from the two first plots the same instability as in the previous problems.

The third plot is rather interesting. We see that the plot skips abruptly from one point to another. This is indeed an instability, and a reasonable explanation why it is there is that the fluid goes through phase transition.

The curve rises in a regular fashion until it reaches at point and then skips downwards and to the left before rising again. This abrupt decrease in pressure

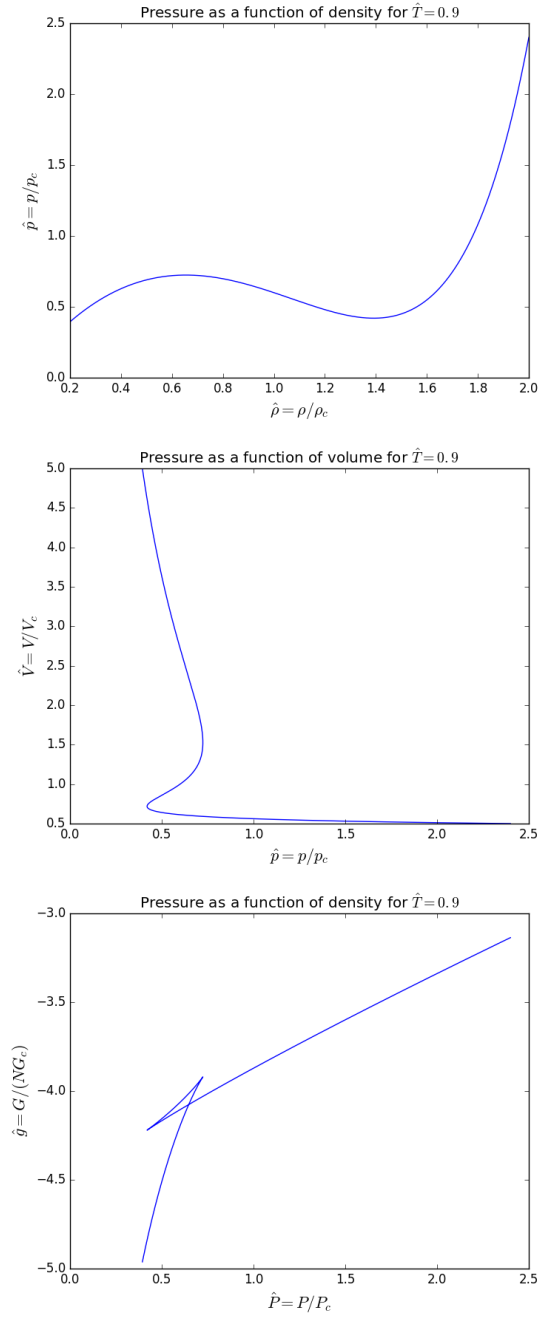


Figure 3: All figures are for $\hat{T} = 0.9$ in order to make comparison easy. From top: pressure as a function of density, volume as a function of pressure and Gibbs free energy for each molecule.

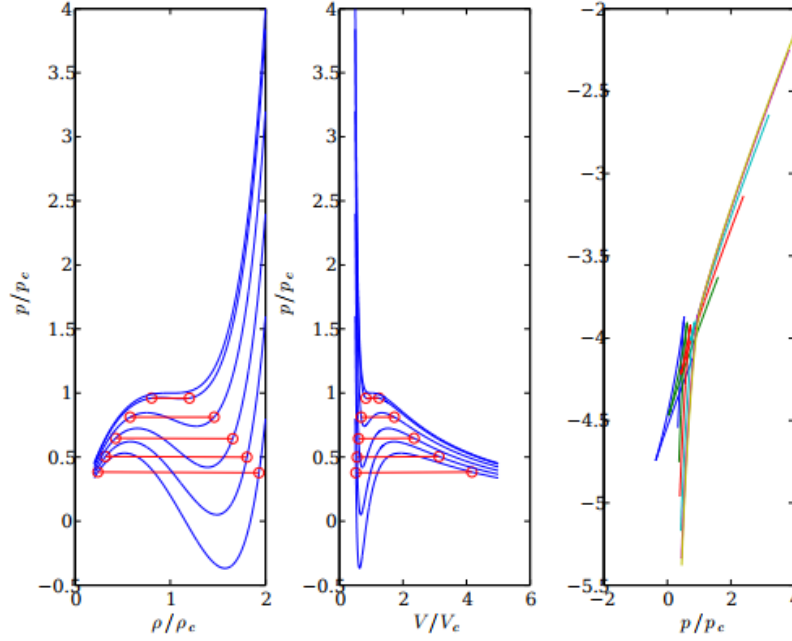


Figure 4: Maxwell Constructions for different temperatures \hat{T} .

before the energy rises again must be where the phase transition happens. The fluid goes from being a gas to a liquid.

Gibbs free energy represents how a system has “potential” left to do a net “something”. If we know where the phase transition happens, we should also know where the minimum Gibbs free energy of the system is. One does now expect a spontaneous phase transition, *ceteris paribus*¹. At the intersecting point there is always another state (gas or liquid) at the same pressure with a lower Gibbs free energy.

m, n, o)

Figure 4 shows three plots. The first two are Maxwell Constructions of the pressure-density space and the pressure-volume space, respectively. These are made using the third plot which is Gibbs free energy for different Gibbs free energies.

A necessary condition for stability is that the pressure does not increase with volume. If a liquid is contained in an expanding volume at constant temperature, at a certain point the liquid will begin to boil. The boiling liquid can be seen as being in two phases as once. If this two-phase coexistence holds as the volume

¹Everything else remaining the same.

continues to increase, the pressure remains constant. By replacing the “wavy bit” of the curves by a straight line such that the area between the wavy curve and the straight line is equal, one would remedy the situation. This is shown in figure 4.