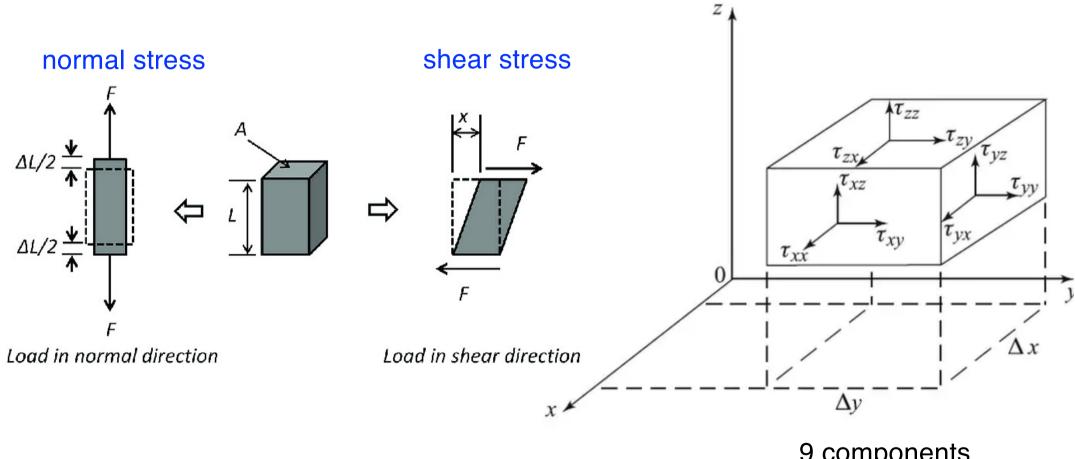
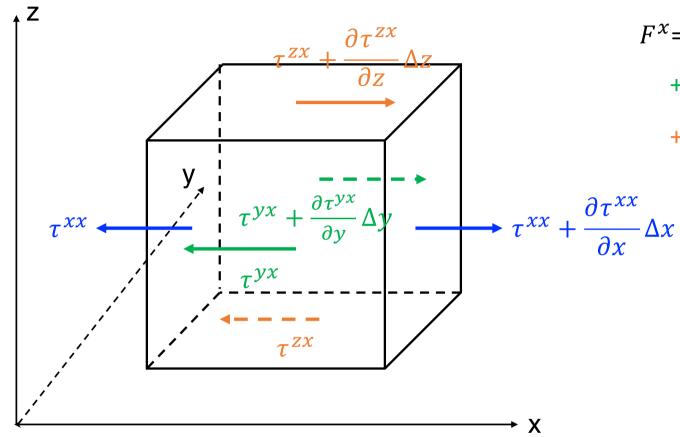
### Frictional force term

# **Stress** – second-order tensor (N m<sup>-2</sup>)



9 components



$$F^{x} = (\tau^{xx} + \frac{\partial \tau^{xx}}{\partial x} \Delta x) \Delta y \Delta z - \tau^{xx} \Delta y \Delta z$$
$$+ (\tau^{yx} + \frac{\partial \tau^{yx}}{\partial y} \Delta y) \Delta x \Delta z - \tau^{yx} \Delta x \Delta z$$
$$+ (\tau^{zx} + \frac{\partial \tau^{zx}}{\partial z} \Delta z) \Delta x \Delta y - \tau^{zx} \Delta x \Delta y$$

For per unit volume

$$F^{x} = \frac{\partial \tau^{xx}}{\partial x} + \frac{\partial \tau^{yx}}{\partial y} + \frac{\partial \tau^{zx}}{\partial z}$$

For Newtonian fluids, viscous stress is:  $\tau^{zx} = \mu \frac{\partial u}{\partial z}$ 

Assumption: μ is constant

$$F^{x} = \frac{\partial \tau^{xx}}{\partial x} + \frac{\partial \tau^{yx}}{\partial y} + \frac{\partial \tau^{zx}}{\partial z}$$

$$= \frac{1}{\partial x} \left( \mu \frac{\partial u}{\partial x} \right) + \frac{1}{\partial y} \left( \mu \frac{\partial u}{\partial y} \right) + \frac{1}{\partial z} \left( \mu \frac{\partial u}{\partial z} \right)$$

$$= \mu \nabla^{2} u$$

$$F^{y} = \frac{\partial \tau^{xy}}{\partial x} + \frac{\partial \tau^{yy}}{\partial y} + \frac{\partial \tau^{zy}}{\partial z}$$

$$= \frac{1}{\partial x} \left( \mu \frac{\partial v}{\partial x} \right) + \frac{1}{\partial y} \left( \mu \frac{\partial v}{\partial y} \right) + \frac{1}{\partial z} \left( \mu \frac{\partial v}{\partial z} \right)$$

$$= \mu \nabla^{2} v$$

$$F^{Z} = \frac{\partial \tau^{xz}}{\partial x} + \frac{\partial \tau^{yz}}{\partial y} + \frac{\partial \tau^{zz}}{\partial z}$$

$$= \frac{1}{\partial x} \left( \mu \frac{\partial w}{\partial x} \right) + \frac{1}{\partial y} \left( \mu \frac{\partial w}{\partial y} \right) + \frac{1}{\partial z} \left( \mu \frac{\partial w}{\partial z} \right)$$

$$= \mu \nabla^{2} w$$

 $\mu$ : dynamic viscosity coefficient

Laplacian operator

$$\nabla^2 = \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2} + \frac{\partial^2}{\partial z^2}$$

$$\frac{F^{x}}{\rho} = \frac{\mu}{\rho} \nabla^{2} u$$
$$= \nabla^{2} u$$

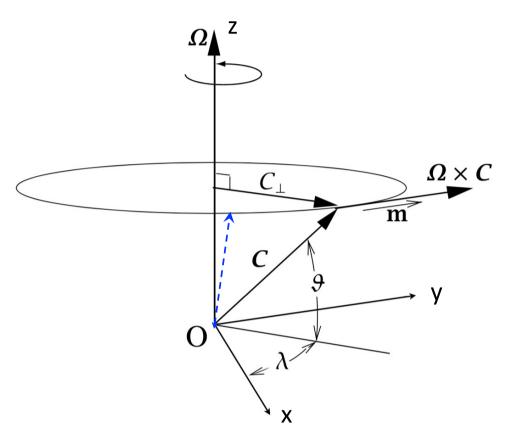
ν: kinematic viscosity coefficient

	$\mu  ( \mathrm{kg}  \mathrm{m}^{-1}  \mathrm{s}^{-1})$	$\nu$ ( $\mathrm{m^2s^{-1}}$ )
Air	$1.8 \times 10^{-5}$	$1.5 \times 10^{-5}$
Water	$1.1 \times 10^{-3}$	$1.1 \times 10^{-6}$
Mercury	$1.6  imes 10^{-3}$	$1.2\times10^{-7}$

### The momentum equations

x direction: 
$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + v \frac{\partial u}{\partial y} + v \frac{\partial u}{\partial z} + v \frac{\partial v}{\partial z} + v \frac{\partial w}{\partial z} + v \frac{\partial w}{\partial$$

Expressions for the force terms are given in the inertial frame. So is the acceleration term.



**Fig. 2.1** A vector C rotating at an angular velocity  $\Omega$ . It appears to be a constant vector in the rotating frame, whereas in the inertial frame it evolves according to  $(dC/dt)_I = \Omega \times C$ .

### **Coriolis Force**

The change in  $\mathcal{C}$  in  $\delta t$  with respect to the Intertial frame

$$\delta C = |C| \cos \theta \, \delta \lambda \, m,$$

$$\delta \lambda = |\Omega| \delta t$$

Let 
$$\hat{\theta} = (\pi/2 - \theta)$$
 
$$\delta C = |C| |\Omega| \sin \hat{\theta} \, m \, \delta t = \Omega \times C \, \delta t.$$

$$\left(\frac{\mathrm{d}\boldsymbol{C}}{\mathrm{d}t}\right)_{I} = \boldsymbol{\Omega} \times \boldsymbol{C}$$

#### Non-constant vector in the rotating frame **B**

The change of **B** in the inertial frame:

$$(\delta \mathbf{B})_I = (\delta \mathbf{B})_R + (\delta \mathbf{B})_{rot}$$

With  $(\delta B)_{rot} = \Omega \times B \, \delta t$ 

$$\delta \mathbf{C} = \mathbf{\Omega} \times \mathbf{C} \, \delta t$$

$$\left(\frac{\mathrm{d}\mathbf{C}}{\mathrm{d}t}\right)_{I} = \mathbf{\Omega} \times \mathbf{C}$$

 $\mathbf{v}_I = \mathbf{v}_R + \mathbf{\Omega} \times \mathbf{r}$   $\left(\frac{\mathrm{d}\mathbf{v}_R}{\mathrm{d}t}\right)_I = \left(\frac{\mathrm{d}\mathbf{v}_R}{\mathrm{d}t}\right)_R + \mathbf{\Omega} \times \mathbf{v}_R$ 

$$\left(\frac{\mathrm{d}}{\mathrm{d}t}(\boldsymbol{v}_{I}-\boldsymbol{\Omega}\times\boldsymbol{r})\right)_{I}=\left(\frac{\mathrm{d}\boldsymbol{v}_{R}}{\mathrm{d}t}\right)_{R}+\boldsymbol{\Omega}\times\boldsymbol{v}_{R}$$

Centrifugal acceleration

$$\left(\frac{dv_I}{dt}\right)_I = \left(\frac{dv_R}{dt}\right)_R + 2\Omega \times v_R + \Omega \times (\Omega \times r)$$

Coriolis acceleration

### The Coriolis acceleration

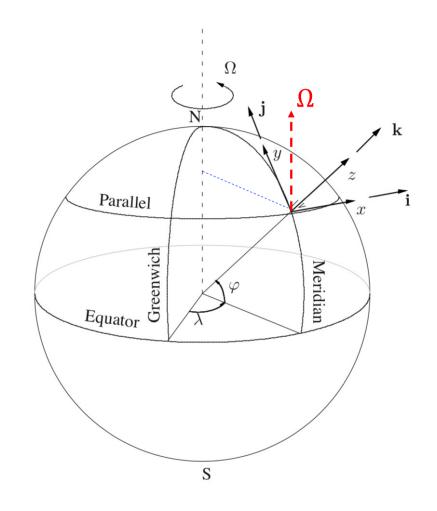
$$2\Omega \times v_R$$

$$\mathbf{\Omega} = \Omega \, \cos \varphi \, \mathbf{j} \, + \, \Omega \, \sin \varphi \, \mathbf{k}$$

x: 
$$2\Omega \cos \varphi w - 2\Omega \sin \varphi v$$

y:  $2\Omega \sin \varphi u$ 

z:  $-2\Omega \cos \varphi u$ .



$$f = 2\Omega \sin \varphi$$

$$f_* = 2\Omega \cos \varphi$$

f: Coriolis parameter

## The momentum equations

$$\left(\frac{dv_I}{dt}\right)_I = \left(\frac{dv_R}{dt}\right)_R + 2\Omega \times v_R + \Omega \times (\Omega \times r) = \text{force terms}$$

Nonlinear advection term Coriolis term Pressure gradient term

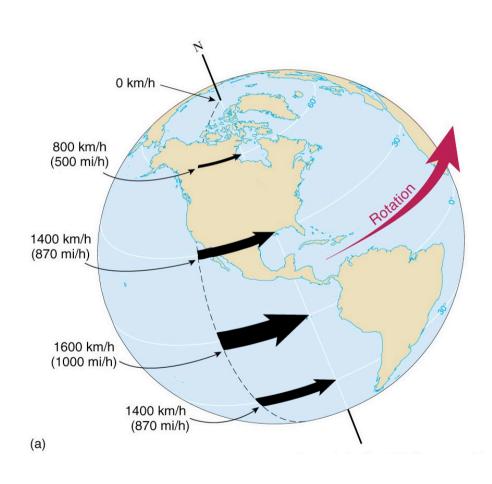
x direction: 
$$\frac{\partial \mathbf{u}}{\partial \mathbf{t}} + \mathbf{u} \frac{\partial \mathbf{u}}{\partial \mathbf{x}} + \mathbf{v} \frac{\partial \mathbf{u}}{\partial \mathbf{y}} + \mathbf{w} \frac{\partial \mathbf{u}}{\partial \mathbf{z}} - \frac{f \mathbf{v} + f_* \mathbf{w}}{\partial \mathbf{z}} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \frac{\mathbf{v} \nabla^2 u}{\partial \mathbf{v}} + \cdots$$
Viscosity term

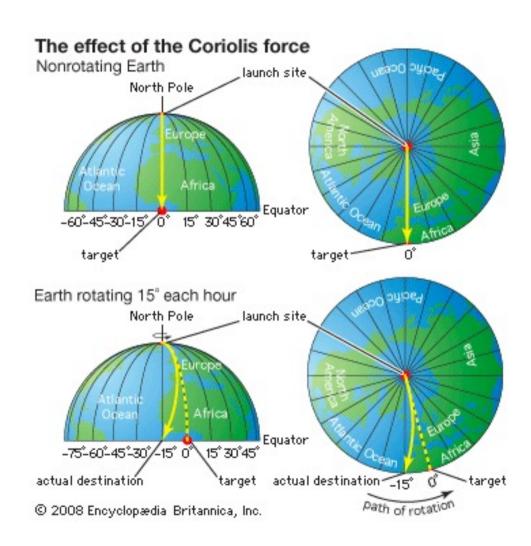
Local acceleration

y direction: 
$$\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} + \underline{fu} = -\frac{1}{\rho} \frac{\partial p}{\partial y} + \underline{v} \nabla^2 v + \cdots$$

z direction: 
$$\frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} - \underline{f_* u} = -\frac{1}{\rho} \frac{\partial p}{\partial z} + \underline{v} \nabla^2 \underline{w} + \cdots$$

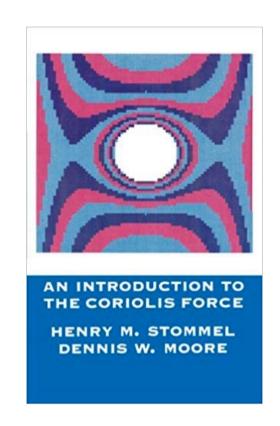
### The Coriolis Force





# References about Coriolis force

- An introduction to the Coriolis Force, H.M. Stommel and D.W. Moore, 1989
- Persson (2000). What is the Coriolis force? Weather, 55, 165–170.
- Persson (1998). *How to understand the Coriolis force?* Bulletin of the American Meteorological Society, 79(7), 1373–1385.

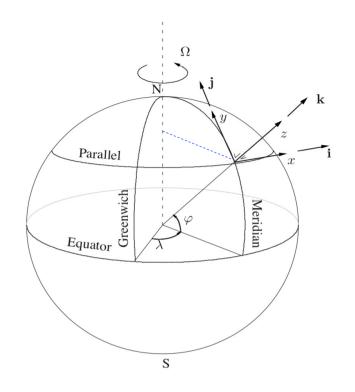


# f-plane and $\beta$ -plane

$$f = 2\Omega \sin \varphi = 2\Omega \left( \sin \varphi_0 + \cos \varphi_0 (\varphi - \varphi_0) \right)$$
$$f_0$$

If  $\varphi - \varphi_0$  is small:

*f*-plane:  $f = f_0$  is a constant.



If  $\varphi - \varphi_0$  cannot be neglected:

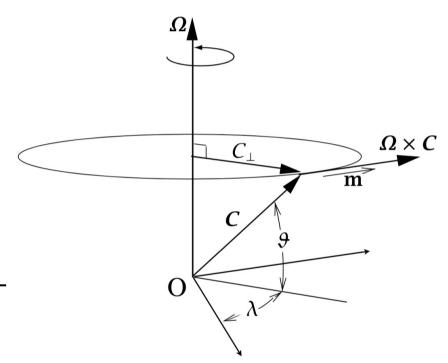
β-plane: 
$$f = f_0 + 2\Omega cos \varphi_0 (\varphi - \varphi_0) = f_0 + \frac{2\Omega cos \varphi_0}{a} y$$

# Centrifugal force term



### Substitute C with r:

$$=-\Omega imes(\Omega imes r_{\perp})$$
 $=-(\Omega\cdot r_{\perp})\Omega+(\Omega\cdot\Omega)r_{\perp}$ 
 $=\Omega^2r_{\perp}$ 



# Gravity force term

The Gravity Term in the Momentum Equation The gravitational attraction of two masses  $M_1$  and m is:

$$\mathbf{F}_g = \frac{G \, M_1 \, m}{R^2}$$

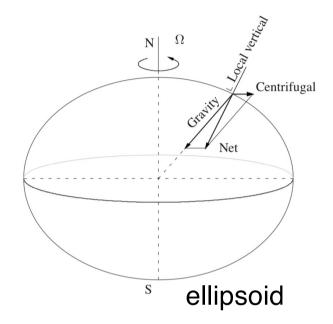
where R is the distance between the masses, and G is the gravitational constant. The vector force  $\mathbf{F}_g$  is along the line connecting the two mases.

The force per unit mass due to gravity is:

$$\frac{\mathbf{F}_g}{m} = \mathbf{g}_f = \frac{GM_E}{R^2} \tag{7.15}$$

where  $M_E$  is the mass of Earth. Adding the centrifugal acceleration to (7.15) gives gravity **g** (Figure 7.5):

effective gravity 
$$\mathbf{g} = \mathbf{g}_f - \mathbf{\Omega} \times (\mathbf{\Omega} \times \mathbf{R})$$
 (7.16)



# The momentum equations

Nonlinear advection term Coriolis term Pressure gradient term

$$x \ direction: \quad \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} - f v + f_* w = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \nabla^2 u$$
 Viscosity term

Local acceleration

y direction: 
$$\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} + \frac{fu}{dz} = -\frac{1}{\rho} \frac{\partial p}{\partial y} + v \frac{\partial^2 v}{\partial z}$$

z direction: 
$$\frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} + \underline{f_* u} = -\underline{\frac{1}{\rho}} \frac{\partial p}{\partial z} + \underline{v \nabla^2 w} - \underline{g}$$
gravity term

# Continuity equation

fluid loss = 
$$\int_{S} \rho \boldsymbol{v} \cdot d\boldsymbol{S} = \int_{V} \nabla \cdot (\rho \boldsymbol{v}) dV$$
 Divergence (Gaussian) theorem

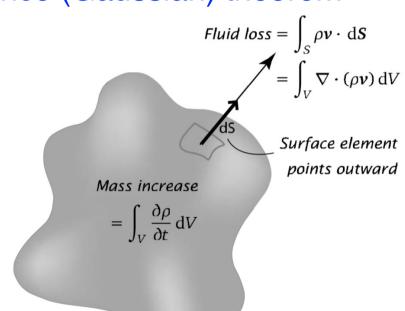
Vallis (Eq. 1.19)
$$-\frac{dM}{dt} = -\frac{d}{dt} \int_{v}^{\infty} \rho \, dV = -\int_{v}^{\infty} \frac{\partial \rho}{\partial t} \, dV$$

$$\int_{V} \left[ \frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \boldsymbol{v}) \right] dV = 0$$

For any arbitrary volume *V*,

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{v}) = 0 \quad \text{or} \quad \frac{d\rho}{dt} + \rho \nabla \cdot \mathbf{v} = \mathbf{0}$$
For incompressible fluids  $(\frac{d\rho}{dt} = 0)$ 

$$\nabla \cdot \mathbf{v} = 0$$



# The thermodynamic equation

1<sup>st</sup> Law of Thermodyamics (energy conservation, and for per unit mass):

$$\frac{dI}{dt} = Q - W$$
 *I:* internal energy   
 Q: rate of heat gain

*W*: rate of work done by pressure force

onto surrounding fluids

 $C_{v}$ : specific heat capacity  $I = C_{v}T$ 

Fourier's Law of heat conduction:

$$Q = \frac{k_T}{\rho} \nabla^2 T$$

Rate of work done by pressure force:

specific volume

$$W = p \frac{d\alpha}{dt} \qquad \boxed{\alpha = 1/\rho}$$

$$C_{v} \frac{dT}{dt} = \frac{k_{T}}{\rho} \nabla^{2}T - p \frac{d\alpha}{dt}$$

$$= \frac{k_{T}}{\rho} \nabla^{2}T + \frac{p}{\rho^{2}} \frac{d\rho}{dt}$$

$$\alpha = 1/\rho$$

From the continuity equation:

$$\frac{d\rho}{dt} = -\rho \nabla \cdot \boldsymbol{v}$$

$$C_{\boldsymbol{v}}\frac{dT}{dt} = \frac{k_T}{\rho} \nabla^2 T - \frac{p}{\rho} \nabla \cdot \boldsymbol{v}$$

For incompressible fluids:

 $K_T$ : thermal diffusivity coefficient

$$\frac{dT}{dt} = \frac{k_T}{\rho C_D} \nabla^2 T \qquad \qquad \frac{dS}{dt} = K_S \nabla^2 S$$