

## SYSTEM – Methanol - Water

### Activity Coefficient Model – VAN LAAR

In this assignment, we will use modified Raoult's law with activity coefficients given by van laar equation using Matlab . We will use Antoine's equation to compute saturated pressure.

AIM- To compute -(a) isobaric T vs x, y diagram , (b) y vs x diagram (c) Comparison with the experimental results provided.

Given:-

P=760 mm hg;

A1=8.08097

A2=8.07131

B1=1582.271

B2=1730.630

C1=239.726

C2=233.426

A12=0.7715

A21=0.5775

T (in degree celcius)

P1sat, P2sat (vapour pressure of pure components 1 and 2 in mm Hg)

$$\ln \gamma_1 = (A_{12}) * ((A_{21} * x_2) / (A_{12} * x_1 + A_{21} * x_2)) * ((A_{21} * x_2) / (A_{12} * x_1 + A_{21} * x_2))$$

$$\ln \gamma_2 = (A_{21}) * ((A_{12} * x_1) / (A_{12} * x_1 + A_{21} * x_2)) * ((A_{12} * x_1) / (A_{12} * x_1 + A_{21} * x_2))$$

Antoine's equation:-

$$\log P_{1sat} = A_1 - (B_1 / (T + C_1))$$

$$\log P_{2sat} = A_2 - (B_2 / (T + C_2))$$

$$x_2 = 1 - x_1$$

$$y_2 = 1 - y_1$$

$$P = P_{1sat} * x_1 * \gamma_1 + P_{2sat} * (1 - x_1) * \gamma_2 \quad \dots\dots\dots(1)$$

Modified Raoults Law:-

$$y_1 = P_{1sat} \cdot x_1 \cdot \gamma_1 / P \quad \dots\dots\dots (2)$$

$$y_2 = P_{2sat} \cdot x_2 \cdot \gamma_2 / P$$

## DEGREE OF FREEDOM ANALYSIS

We have two equations (i.e (1) and (2)) but 3 unknowns( T ,x<sub>1</sub>,y<sub>1</sub>) so we have to specify 2 variables , out of which one is given P=760 mm of Hg.

So we need to specify one more variable(T or x<sub>1</sub> or y<sub>1</sub> ) to solve the system of equations.

T-X-Y Data(Given)

T	X <sub>1</sub>	Y <sub>1</sub>
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96.70	0.0159	0.1100
92.70	0.0476	0.2521
84.60	0.1475	0.4716
77.10	0.3515	0.6786
73.20	0.5097	0.7923
68.60	0.7595	0.8953
66.70	0.8889	0.9536
66.30	0.9408	0.9702

## Matlab code

```
P=760;
A1=8.08097;A2=8.07131;
B1=1582.271;
B2=1730.630;
C1=239.726;
C2=233.426;
A12=0.7715;
A21=0.5775;
T=linspace(50,100,51);
x1=zeros(size(T)); %Mole fraction in liquid phase of methanol
x2=zeros(size(T)); %Mole fraction in liquid phase of water
y1=zeros(size(T)); %Mole fraction in vapour phase of methanol
y2=zeros(size(T)); %Mole fraction in vapour phase of water
G1=zeros(size(T)); %activity coefficient of methanol
G2=zeros(size(T)); %activity coefficient of water
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P1sat=zeros(size(T));
P2sat=zeros(size(T));
for i=1:51
P1sat(i)=10^(A1-(B1/(T(i)+C1))); P2sat(i)=10^(A2-(B2/(T(i)+C2)));
eqn=@(x1) 760-P1sat(i)*x1*exp((A12)*((A21*(1-x1))/(A12*x1+A21*(1-x1)))*((A21*(1x1))/(A12*x1+A21*(1-x1))))-P2sat(i)*(1-x1)*exp((A21)*((A12*x1)/(A12*x1+A21*(1x1)))*((A12*x1)/(A12*x1+A21*(1-x1))));
x1(i)=fzero(eqn,0);
x2(i)=1-x1(i);

G1(i)=exp((A12)*((A21*x2(i))/(A12*x1(i)+A21*x2(i)))*((A21*x2(i))/(A12*x1(i)+A21*x2(i))));
G2(i)=exp((A21)*((A12*x1(i))/(A12*x1(i)+A21*x2(i)))*((A12*x1(i))/(A12*x1(i)+A21*x2(i))));
y1(i)=P1sat(i)*x1(i)*G1(i)/P;
y2(i)=P2sat(i)*x2(i)*G2(i)/P;
end

%% Graph plotting and comparison from the given data
Tpoints=[96.70,92.70,84.60,77.10,73.20,68.60,66.70,66.30];
xpoints=[0.159,0.476,0.1475,0.3515,0.5097,0.7595,0.8889,0.9408];
ypoints=[0.1100,0.2521,0.4716,0.6786,0.7923,0.8953,0.9536,0.9702];
tiledlayout(1,2);
nexttile;
plot(x1,y1);
hold on
plot(xpoints,ypoints,'--or');
hold off
xlim([0,1])
ylim([0,1])
nexttile;
plot(x1,T);
hold on
plot(y1,T);
hold on
plot(xpoints,Tpoints,'--or')
hold on
plot(ypoints,Tpoints,'--or')
hold off
xlim([0,1])

```

Results-

