

# Modeling Pyroprocessing Safeguards in Cyclus

## A Brief Summary

Advanced Reactors and Fuel Cycles Group

University of Illinois at Urbana-Champaign

January 28, 2020



**ILLINOIS**

# Outline

- 1 Background
- 2 Introduction
- 3 Methods
- 4 Pyre
- 5 Sensitivity
- 6 Conclusion
- 7 Acknowledgments

## Education



ILLINOIS

UNIVERSITY OF ILLINOIS AT URBANA-CHAMPAIGN



# Washington University



**Figure:** Dr. S. Murty Goddu - Radiation Oncology



**Figure:** Washington University's Proton Therapy

## CNEC - UIUC



- NNSA funded consortia:
  - Frequent workshops/conferences.
  - Lab interaction.
- IAEA NDA training:
  - Introduction to NDA techniques.
  - Safeguard applications - UNCL.
- Software Development - Cyclus



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# Introduction

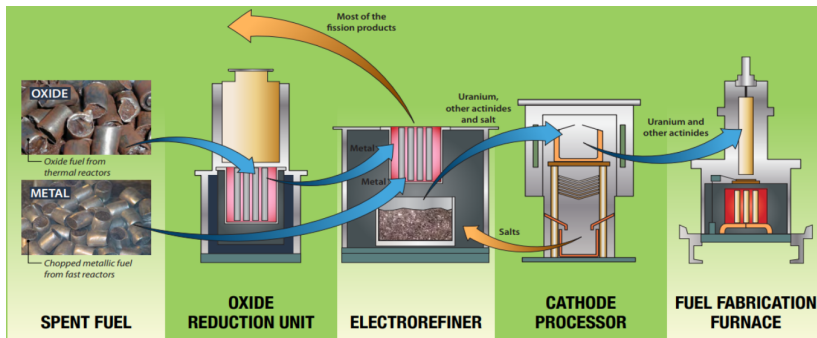


Figure: Argonne demonstration of a basic pyro plant [3].

# Motivation/Goals

## Motivation

- Safeguard by design
- Model diversion inside facilities
- Transition from LWR to SFR

## Goals

- Detect diversion using signatures and observables.
- Determine optimum detector and inspection locations in pyroprocessing
- Characterize detection sensitivities





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## Approaches to a Practical Systems Assessment for Safeguardability of Advanced Nuclear Fuel Cycles

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**Abstract** — Many nations are expanding or initiating nuclear energy programs as part of a national energy portfolio. Transitioning to advanced nuclear energy systems improves sustainability and promotes energy independence. These advanced nuclear energy systems also must be shown to enhance safety, safeguards, and security in order to be realistically deployed. This is of particular concern to non-nuclear weapons states, to assure compliance with International Atomic Energy Agency treaty obligations.

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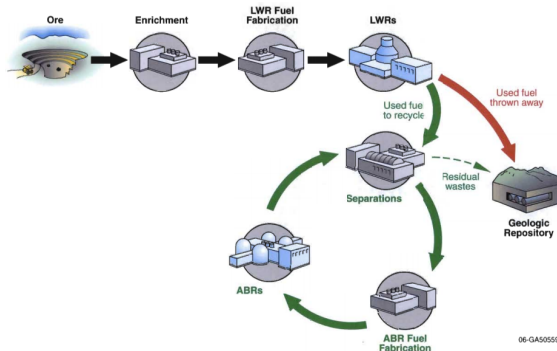
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# Cyclus



## What is Cyclus?

Cyclus is a modular agent based fuel cycle simulator for tracking commodity transactions between facilities.



## Why Cyclus?

Cyclus allows the construction of specific scenarios through the addition of archetypes. These archetypes are modular and the transactions can be tracked.

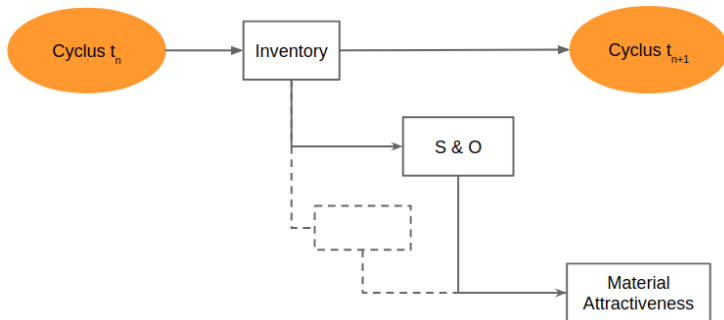


Figure: Diversion detection methods within Cyclus.

# Assumptions



## Cyclus Requirements

- Modular.
- Time step  $\geq 1$  month
- Streams must be in a trade-able form.
- Parameters are constant for the simulation.
  - Equation input toolkit under development.
- Diversion detection must be added after.



## Subprocesses - Voloxidation

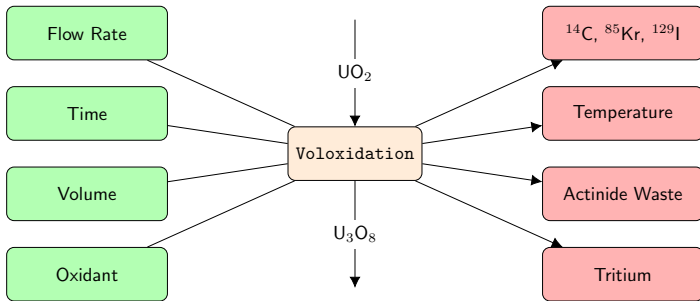


Figure: Voloxidation material balance area [1].

## Subprocesses - Electroreduction

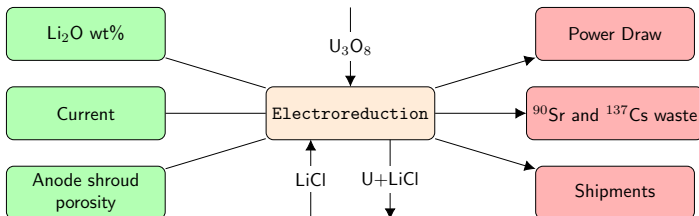
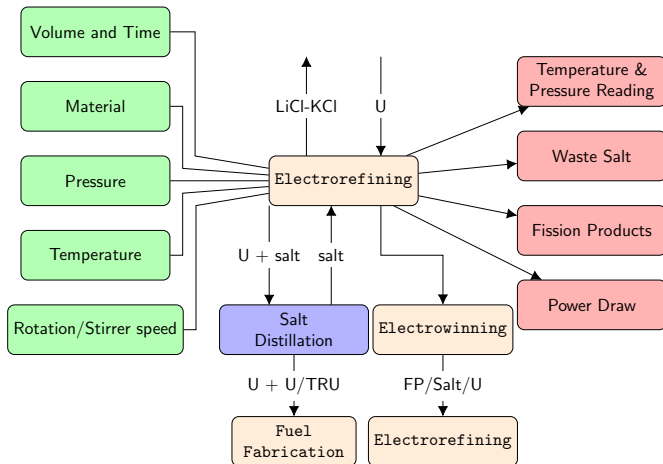


Figure: Reduction material balance area [2].

## Subprocesses - Electrorefining





## Subprocesses - Electrowinning

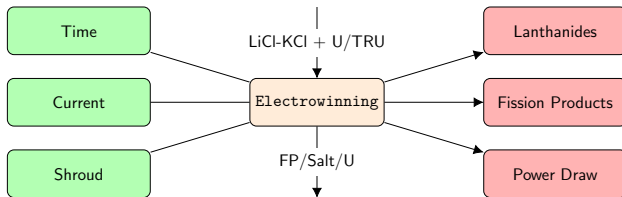


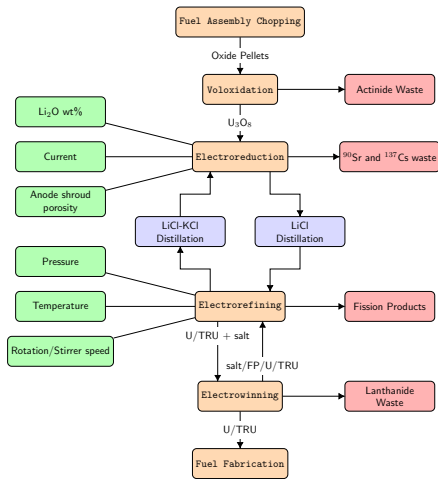
Figure: Winning material balance area.

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## Pyre Archetype

- Facility containing multiple sub-processes:
  - Separately handled.
  - Independent transactions, possibility of diversion.
- Operation setting impact efficiency.
- Generic facility:
  - Multiple types of pyro plants.
  - LWR vs SFR.



## Pyre - Diversion Options

Material diversion occurs in two different modes: **nefarious** or **operator**.

- **Nefarious Diversion** imagines diversion by a single bad actor with facility access.
- **Operator Diversion** imagines undeclared production.

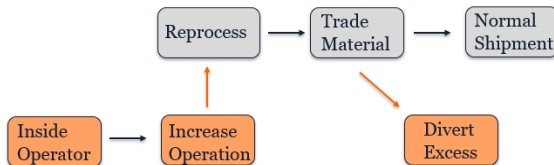


Figure: Operator vs nefarious diversion.

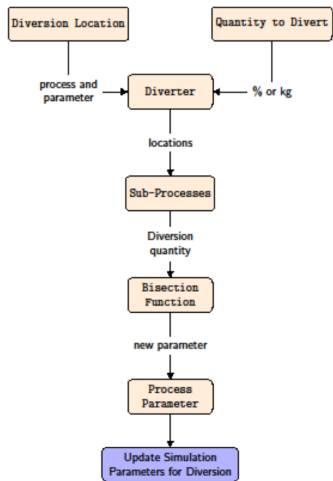
## Diverter Class

### Inputs:

- Location
  - Sub-process
  - Operation Setting
- Quantity
- Frequency
- Number of Diversions

### Purpose

The goal of a separate diverter class is to allow this method to be used by facilities other than pyre through a toolkit.



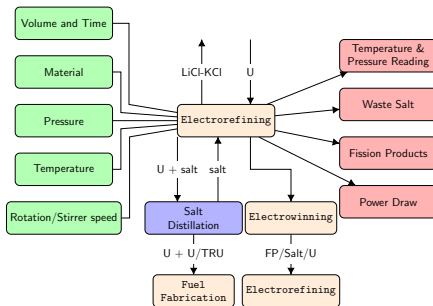
## Diversion Detection

### Diversion Detection

Material transactions are no longer a reliable method. Instead we use signatures and observables:

- Temperature, power draw, etc.

A Cumulative Sum change algorithm is used to detect any significant changes.



## Transition Scenario

A main attraction of pyroprocessing is the ability to handle LWR and SFR waste.

- To verify this capability in PyRe, we ran an EG01 – EG24 transition scenario.
- We want to observe the following:
  - Appropriate deploying of PyRe
  - Ability to meet demand of new SFRs
  - Diversion capabilities
  - Accurate transition from UOX to SFR fuels

## Transition Scenario - Setup

### Legacy:

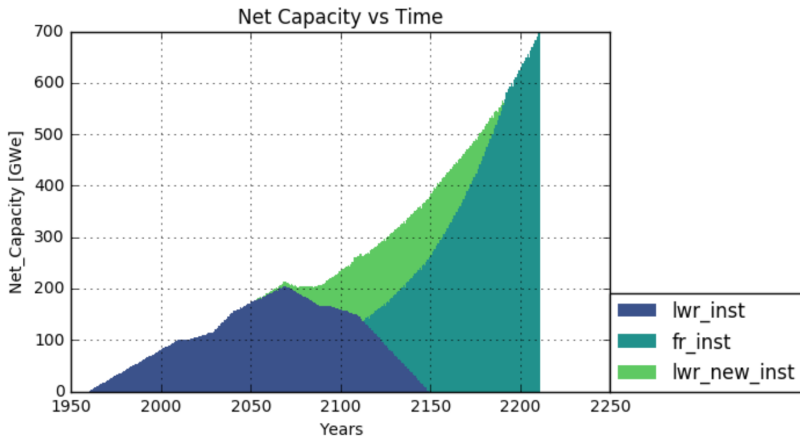
- 200 LWRs
  - 50% 60yr lifetime
  - 50% 80yr lifetime
- LWR Pyre

### Transition:

- 200 LWRs starting in 2015
  - 80yr lifetime
- SFR starts in 2050
  - 80yr lifetime
- SFR Pyre



## Transition Scenario - Results



## Diversion Settings

Two Pyre prototypes:

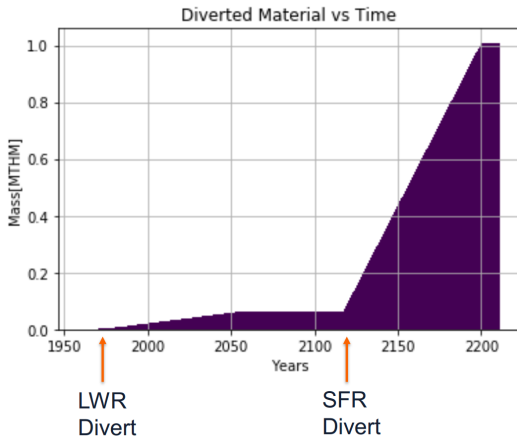
- LWR vs SFR

LWR Pyre:

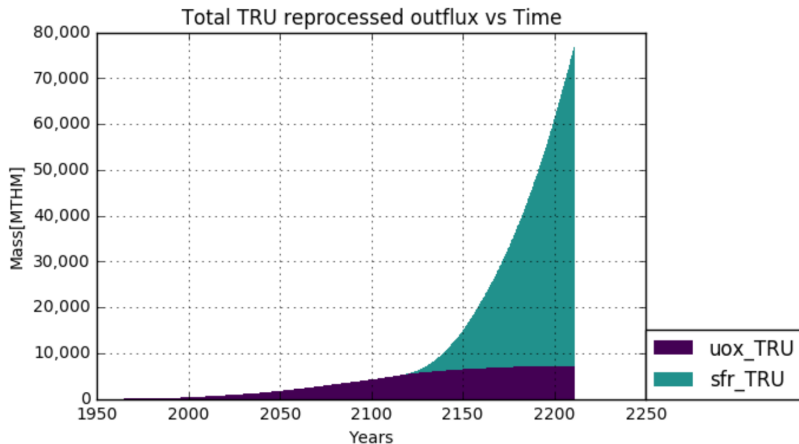
- Fewer diversions
- More material per instance
- Less frequent

SFR Pyre:

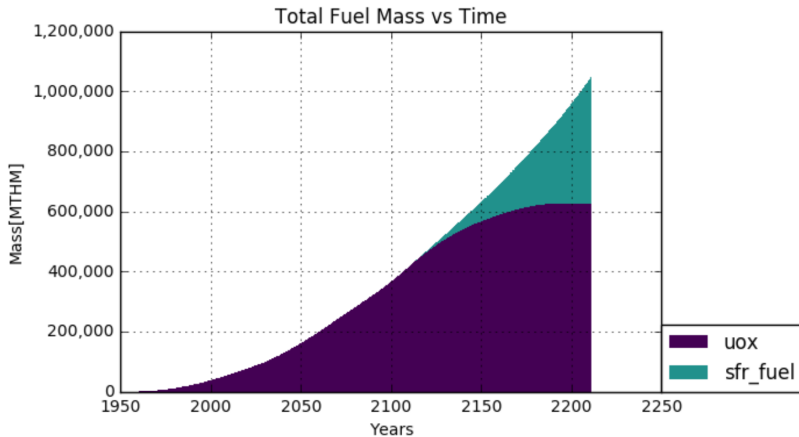
- Frequent diversion
- Small quantities



## Transition Scenario - Utilization



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## Sensitivity Analysis

Dakota was wrapped around Cyclus to randomly sample various parameters for critical sub-processes:

- Electrorefiner
- Electrowinner

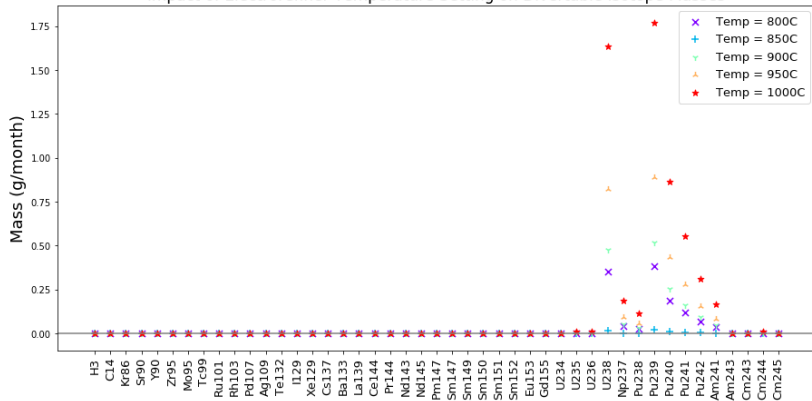
| Parameter                    | Lower Bound | Upper Bound | Units       |
|------------------------------|-------------|-------------|-------------|
| Electrorefiner Temp          | 750         | 1000        | $^{\circ}C$ |
| Electrorefiner Pressure      | 100         | 760         | mTorr       |
| Electrorefiner Stirrer Speed | 0           | 100         | rpm         |
| Electrowinner Current        | 5           | 10          | Amps        |
| Electrowinner Flow Rate      | 2           | 4.5         | cm/s        |
| Electrowinner Process Time   | 1           | 4           | hours       |

Table 4.1: Range of each sensitivity analysis parameter sample.

# Electrorefiner - Temperature



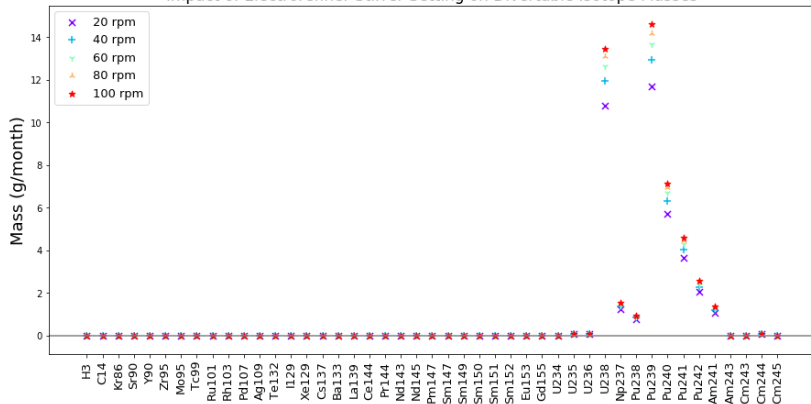
Impact of Electrorefiner Temperature Setting on Divertable Isotope Masses



# Electrorefiner - Stirrer

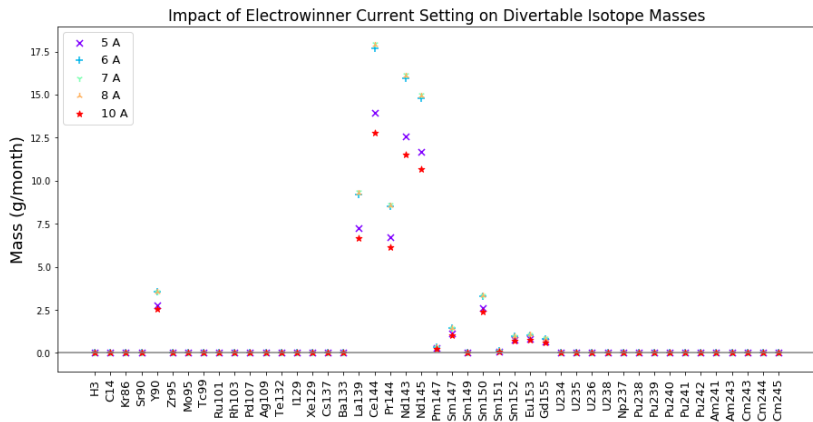


Impact of Electrorefiner Stirrer Setting on Divertable Isotope Masses





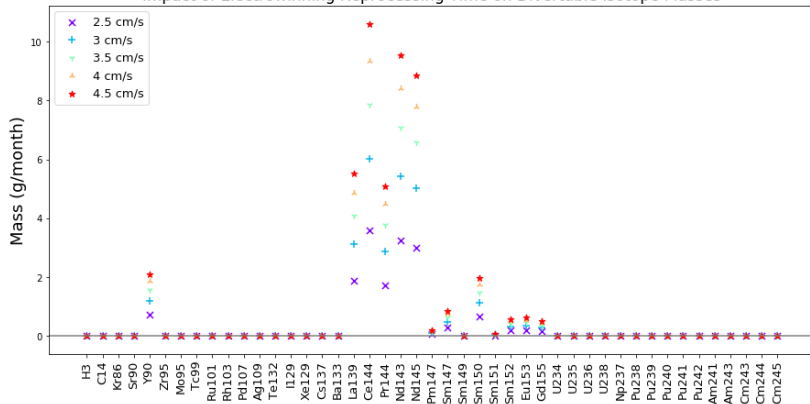
# Electrowinner - Current



# Electrorefiner - Process Time



Impact of Electrowinning Reprocessing Time on Divertable Isotope Masses



## Sensitivity Results

Parameters that influenced interaction between eutectic and waste showed more significant impact on separation efficiency.

| Sample | ER<br>Temp | ER<br>Pressure | ER<br>Stir Speed | EW<br>Current | EW<br>Flow rate | EW<br>Time |
|--------|------------|----------------|------------------|---------------|-----------------|------------|
| 1      | 0.036      | 8.589          | 30.284           | 5.684         | 3.136           | 20.030     |
| 2      | 0.715      | 13.336         | 33.542           | 7.216         | 5.699           | 33.602     |
| 3      | 0.975      | 15.393         | 35.447           | 7.308         | 7.866           | 43.879     |
| 4      | 1.672      | 15.912         | 36.799           | 7.281         | 9.743           | 52.154     |
| 5      | 3.328      | 16.047         | 37.848           | 5.202         | 11.398          | 59.080     |

Table 4.2: Comparison of operational settings' impact on divertable material (shown in % difference compared to baseline values). Where ER and EW represent electrorefiner and electrowinner, respectively.

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## Conclusions

We have developed a customizable method of diverting material from inside Cyclus facilities.

- Work has been done on the detection of two different types of diversion: Nefarious and Operator

Pyre was demonstrated to function as both LWR and SFR reprocessing method

- Generic facility capable of modeling multiple facility layouts

Key measurement points were identified with sensitivity analysis performed over the primary sub-processes.

## Future Work

This work laid the groundwork for future research into sub-facility modeling and diversion detection. Future additions to this work could include:

- Reducing time step length for higher fidelity
- Expand on operational parameter relationships with further experimental data
- Incorporate multiple data points for CUSUM detection

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