

Numerical Modelling of Two-Phase Flows with moving Contact Lines

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GESAR, Rio de Janeiro, August 19, 2015



Academic Background

02.2013 - B. Sc. Mechanical Engineering, RWTH
 Thesis: FEM simulation of viscoelastic flow

- 10.2014 M. Sc. Aeronautical Engineering, RWTH
 Thesis: moving mesh implementation in FVM solver
- Since 03.2015 Ph. D. student at LTCM, EPFL
 - -Numerical simulation of two-phase flows
 - -ALE, FEM, two-phase flow simulator
 - -Contact lines, annular flow



- THERMAPOWER
- Two-Phase Flow Introduction
- Microchannel Simulation Results
- Contact Lines
- Conclusion & Further Work



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THERMAPOWER

- Thermal Management of High Power
 Microsystems Using Multiphase Flows
- Funded by European Union
- Innovative cooling systems using two-phase flow for microelectronic devices
- Partner Universities:
- ➤ University of Edinburgh, Shanghai Jiaotong, EPFL, University of Maryland, University of Nottingham and UERJ.

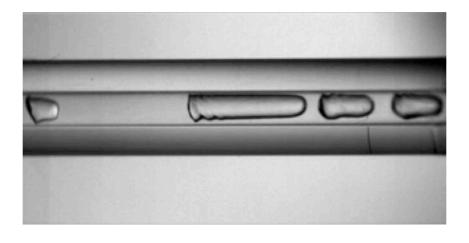


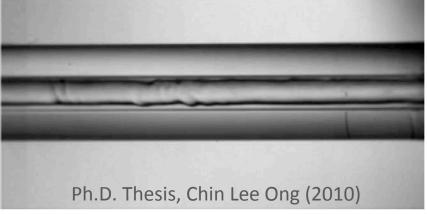
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Two-phase flow in microchannels

- Higher heat fluxes compared to single-phase cooling
- Small scales make it difficult to perform quantitative measurements
- Numerical simulation well suited
- Typical flow conditions slug or annular flow:







Governing Equations

- One fluid formulation
- Incompressible Navier-Stokes equations:

$$\begin{split} \frac{D\vec{v}}{Dt} &= \frac{\partial \vec{v}}{\partial t} + (\vec{v} - \vec{v}_{mesh}) \cdot \nabla \vec{v} = -\frac{\nabla p}{\rho} + \frac{\mu}{Re} \nabla \left(\nabla \vec{v} + (\nabla \vec{v})^T \right) + \\ & \frac{\vec{g}}{Fr^2} + \boxed{\frac{\sigma}{We} \kappa \vec{n} \delta} \quad \text{surface tension} \\ & \nabla \cdot \vec{v} = 0 \end{split}$$

$$Re = \frac{\bar{\rho}\,\bar{v}_{\infty}\,\bar{L}}{\bar{\mu}}, \quad We = \frac{\bar{\rho}\,\bar{v}_{\infty}^2\,\bar{L}}{\bar{\sigma}}, \quad Fr = \frac{\bar{v}_{\infty}}{\sqrt{\bar{g}\,\bar{L}}}$$



Governing Equations

- One fluid formulation
- Incompressible Navier-Stokes equations:

inertia / viscous

tension

inertia / surface inertia / gravity

$$Re = \frac{\bar{\rho}\,\bar{v}_{\infty}\,\bar{L}}{\bar{\mu}},$$

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$$Fr = \frac{\bar{v}_{\infty}}{\sqrt{\bar{g}\,\bar{L}}}$$

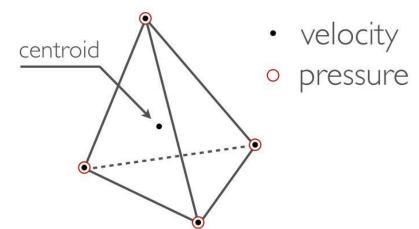


Discretization

Time derivative: Semi Lagrangian method

$$\frac{D\phi(\vec{x},t)}{Dt} \approx \frac{\phi(\vec{x},t+\Delta t) - \phi(\vec{x}-\vec{v}^n \Delta t,t)}{\Delta t}$$

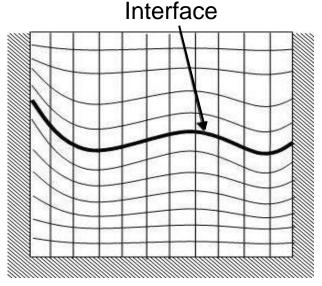
- Spatial derivatives:
- Finite Element Method (FEM)
- > LBB -> Mini Element
- Unstructured mesh
- > 2d: triangular/3d: tetrahedral elements





Interface tracking

- Arbitrary Lagrangian Eulerian (ALE)
- > Interface: Lagrangian
- Boundaries: Eulerian
- Inside: "arbitrary"
- Remeshing and smoothing operations to avoid mesh quality degradation



- sharp interface, better resolution, no additional equations like VOF, Level-Set...
- expensive mesh operations, topology changes



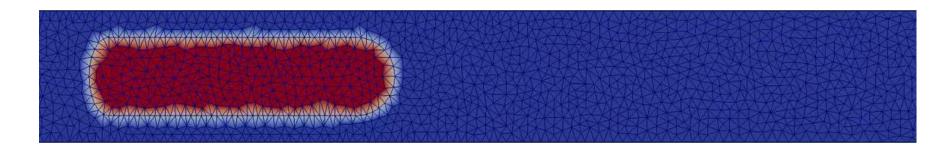
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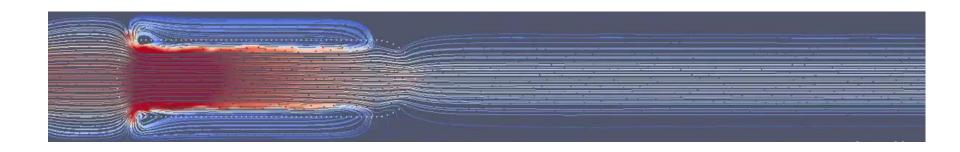


Microchannel Simulation

Single elongated air bubble in glycerol solution:

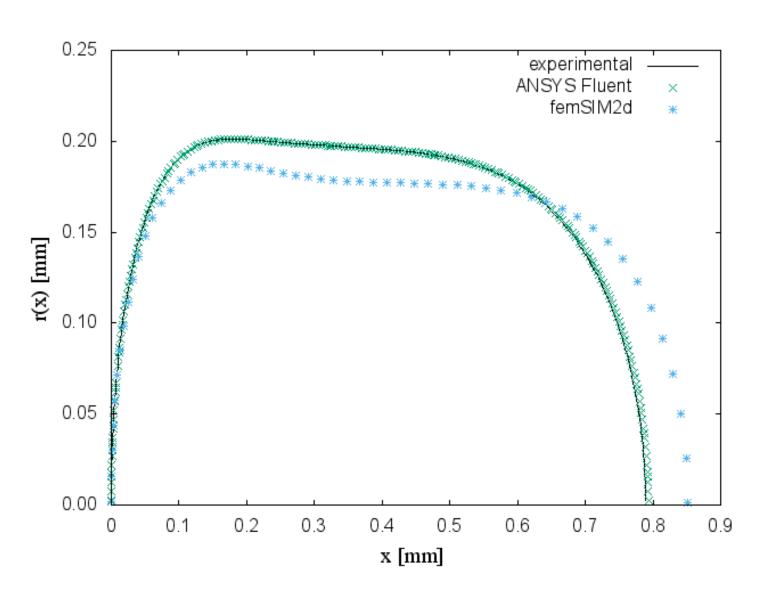
$$Re = 0.0128552, \quad We = 0.00127691, \quad \frac{\rho_{in}}{\rho_{out}} = 9.632 \cdot 10^{-4}, \quad \frac{\mu_{in}}{\mu_{out}} = 3.455 \cdot 10^{-5}$$







Microchannel Simulation



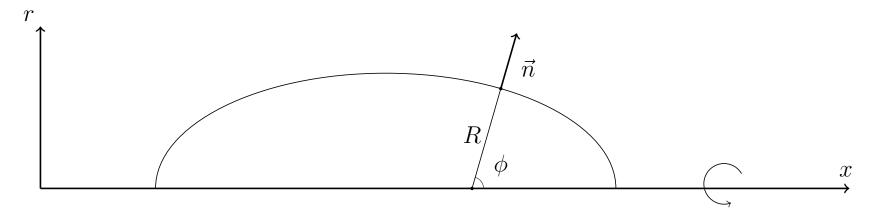


Axisymmetric Formulation

$$\rho \frac{Dv_x}{Dt} = -\frac{\partial p}{\partial x} + \mu \, \Delta v_x \qquad \frac{\partial v_x}{\partial x} + \frac{\partial v_r}{\partial r} + \frac{v_r}{r} = 0$$

$$\rho \frac{Dv_r}{Dt} = -\frac{\partial p}{\partial r} + \mu \left(\Delta v_r - \frac{v_r}{r^2} \right)$$

$$\Delta = \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial r^2} + \frac{1}{r} \frac{\partial}{\partial r}$$



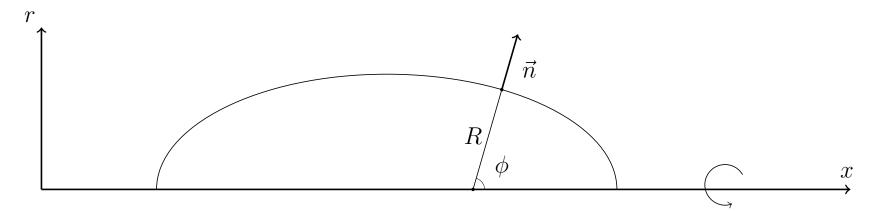


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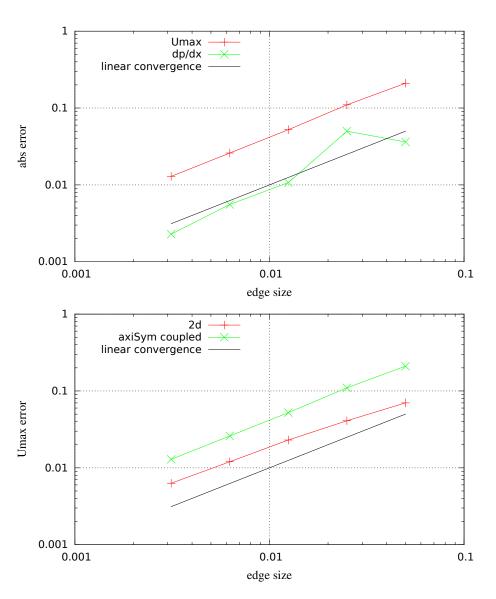
$$\Delta = \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial r^2} + \frac{1}{r} \frac{\partial}{\partial r}$$



$$\kappa_{axi} = \kappa_{2d} + \frac{1}{R} = \kappa_{2d} + \frac{\sin(\phi)}{r}$$



Convergence with Mesh Refinement





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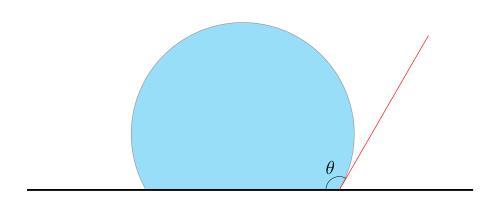
Contact Line

Region of interaction of three different materials





Contact angle



• Young's equation:
$$\sigma_{gs} = \sigma_{ls} + \sigma_{lg} \cos(\theta)$$

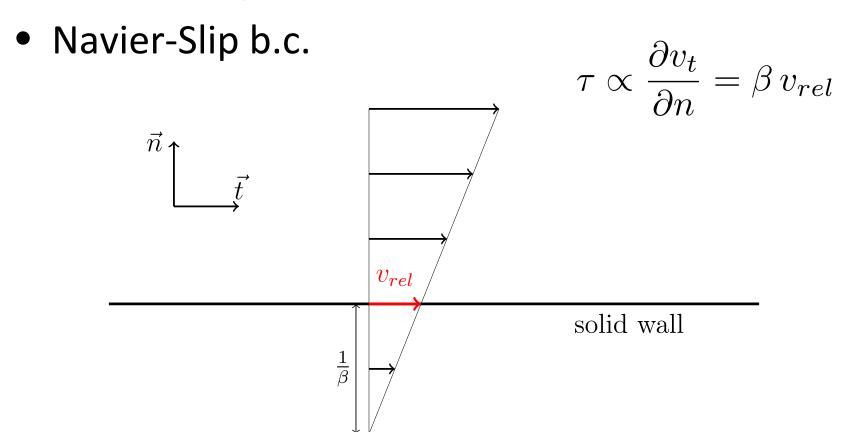






Moving Contact Lines

The moving contact line problem





Moving Contact Lines

- The moving contact line problem
- Navier-Slip b.c.

$$\vec{n} \cdot \vec{v}_{rel} = 0$$
 $\vec{t} \, \boldsymbol{\sigma}(\vec{v}, p) \, \vec{n} = \beta \, \vec{t} \cdot \vec{v}_{rel}$
 $\vec{b} \, \boldsymbol{\sigma}(\vec{v}, p) \, \vec{n} = \beta \, \vec{b} \cdot \vec{v}_{rel}$

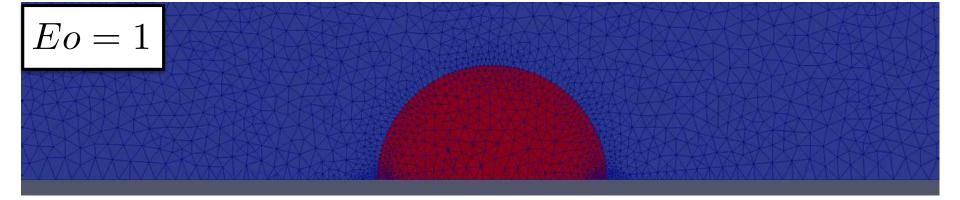
$$\vec{v}_{rel} = \vec{v} - \vec{v}_{wall}$$

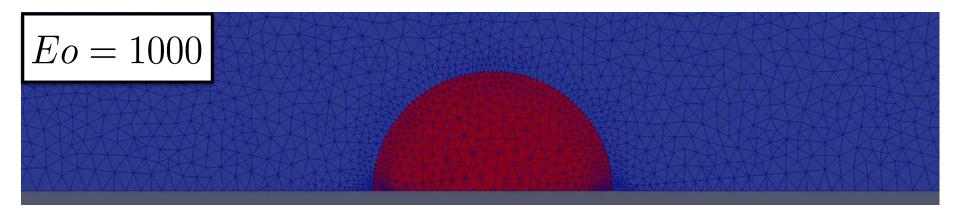


Drop Spreading on a Surface

$$\theta = 50^{\circ}, \quad \frac{\rho_{in}}{\rho_{out}} = 100, \quad \frac{\mu_{in}}{\mu_{out}} = 1.111 \qquad Eo = \frac{We}{Fr^2}$$

$$Eo = \frac{We}{Fr^2}$$







Drop Spreading on a Surface

Height of the bubble at steady-state

 \triangleright Eo >> 1:

$$h_{\infty} = 2\sqrt{\frac{\sigma}{\rho_l g}} \sin\left(\frac{\theta}{2}\right)$$

ightharpoonup **Eo** << 1: (no gravity => spherical cap)

$$h_{\infty} = R_0 \left(1 - \cos(\theta) \right) \sqrt{\frac{\pi}{2\theta - \sin(2\theta)}}$$



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Conclusion & Further Work

- For problems with rotational symmetry axisymmetric formulation is very efficient
- Moving contact lines: imposing static contact angle can already give meaningful results

Next steps:

- ➤ Navier-Slip boundary condition
- > Dynamic contact angle
- Periodic boundary conditions
- Annular flow simulation



Thank you for your attention!