



Modeling in Sciences

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 $\textbf{geometry} \text{ (shapes and behaviour of particles/system)} \Longleftrightarrow \textbf{Linear Algebra}$

change (evolution with time other relevant parameters) ← **calculus**

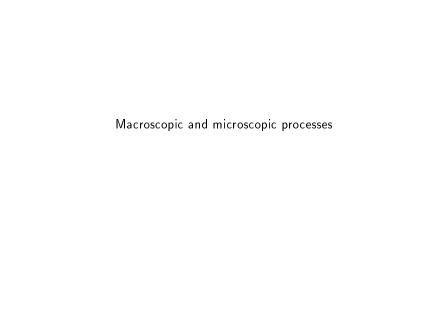
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Chance ← **Probability**



Macroscopic and microscopic processes

relevant questions :

- Why do things happen unidirectionally,
 - ▶ e.g. aging, falling of a leaf from a tree, etc.
- ▶ Is there a quantitative way of characterising spontaneity?

Microscopic Disorder ← dynamical laws:

 $\mathsf{Microscopic}\ \mathsf{Disorder}\ \Leftarrow$

dynamical laws:

classical : Newton/Lagrange/Hamilton(\dot{p}, \dot{q})

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               Grand journey from bi(multi)-nomial to Gaussian
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 molecular dynamics: monte carlo simulations
               equilibrium properties
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Thermodynamic space

Thermodynamic state: A point in the thermodynamic space is a description of a system in terms of macroscopic variables - n, $p \ V \ T$, \cdots

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physical state of a sample of a substance, its physical condition is defined by its physical properties

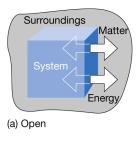
Thermodynamic space

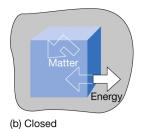
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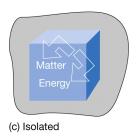
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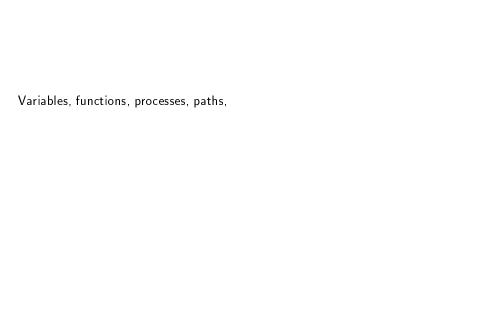
Two samples of same substance with same physical properties are in the same **state**

Thermodynamic systems:









Variables, functions, processes, paths,

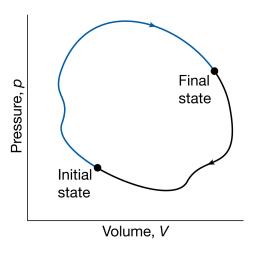
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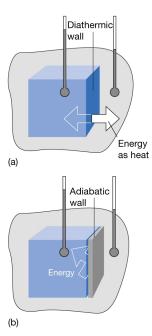
state functions

path functions

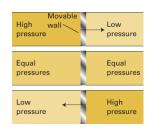
cyclic process : $\oint dX = 0$, if X is a state function



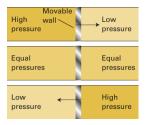
Heat flow - Diathermal and adiabatic walls :



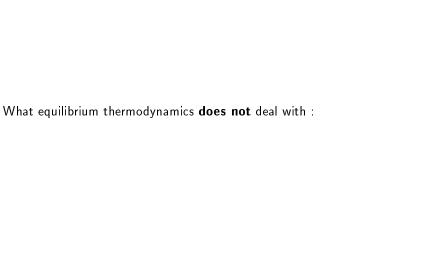
Mechanical motion - Movable and rigid walls



Mechanical motion - Movable and rigid walls



Mass flow: Permeable and impermeable walls



What equilibrium thermodynamics does not deal with :

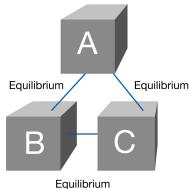
▶ time

What equilibrium thermodynamics does not deal with :

and rate at which processes occur

- ▶ time

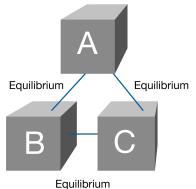
Zeroth Law of thermodynamics



If system A is in thermal equilibrium with system B and system B is in thermal equilibrium with system C then systems A and C are in thermal equilibrium with each other

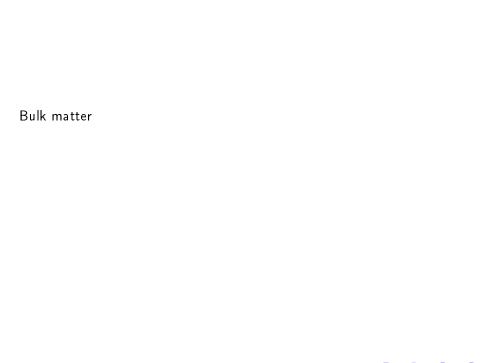
The qualitative observation is quantified by associating a parameter with each system, which is a real number, called Temperature

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The qualitative observation is quantified by associating a parameter with each system, which is a real number, called Temperature $\forall x_i \in \mathcal{R}$, if $x_A = x_B$ and $x_B = x_C \implies x_A = x_C$



Bulk matter
States of matter: solid, liquid, gas

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Properties of bulk matter: mass, volume, composition

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intensive property: independent of amount of substance present



Modeling a gas : Perfect gas: pV = nRT

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What is perfect or ideal about it?

∵it is perfect

∴ it does not exist

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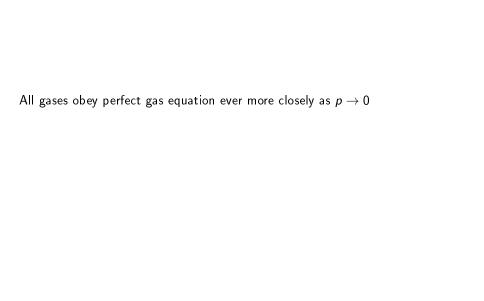
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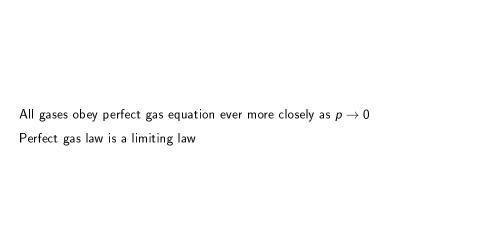
A good example of Reductionism in modern science

SATP : 298.15 K and 1 bar (exactly 10^5 Pa); $V_m = \frac{RT}{p} = 24.789$ dm 3 mol $^{-1}$

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STP : 0°C and 1 atm; molar volume of a perfect gas, $V_m=22.414 {\rm dm^3~mol^{-1}}$





All gases obey perfect gas equation ever more closely as $p o 0$
Perfect gas law is a limiting law
normal atmospheric pressure at sea level (≈ 1 atm) is already low enough for most gases to behave almost perfectly

gases

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Boyle's law applies to all gases regardless of their chemical identity (provided the pressure is low) because at low pressures the average separation of molecules is so great that they exert no influence on one another and hence travel independently

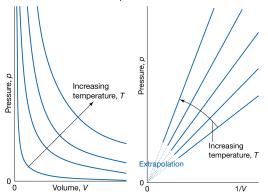
molecular explanation of Charles's law:

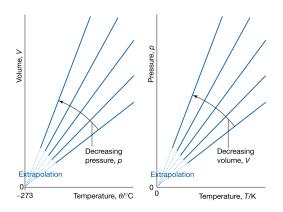
raising temperature of a gas increases average speed of molecules

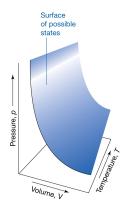
molecules collide with the walls more frequently and with greater impact

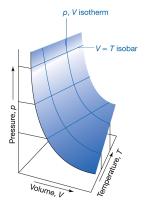
⇒ they exert a greater pressure on the walls of the container

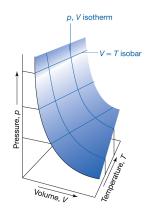
p-V-T plots : Boyle's/Charles' law and perfect gases:

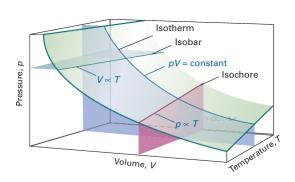




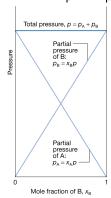




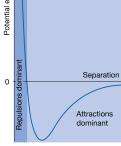




mixtures - partial pressures :



Potential energy Contact



van der Waals equation : $p=rac{nRT}{V-nb}-a\left(rac{n}{V}
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- volume excluded per molecule= $4V_{\text{molecule}}$ $\therefore b = 4V_{\text{molecule}}.N_A$

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solved problem : Estimate the molar volume of ${\rm CO_2}$ at 500 K and 100 atm by treating it as a van der Waals gas , given $\left\{ \begin{array}{l} a=3.592\,\mathrm{dm^6atmmol^{-2}}\\ b=4.257\times10^{-2}\mathrm{dm^3mol^{-1}} \end{array} \right.$

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or, $x = 0.366 \text{ dm}^3 \text{mol}^{-1} \text{ (perfect gas : } 0.41 \text{dm}^3 \text{mol}^{-1} \text{)}$

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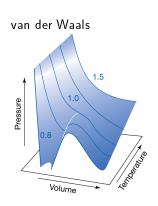
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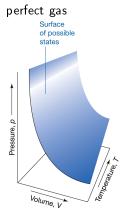
lacks allows us to draw some general conclusions about real gases

advantage:

- analytical equation
- ------

Isotherms reflect consequences of interactions





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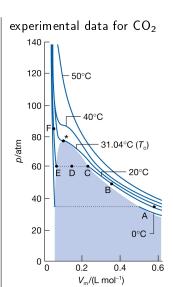
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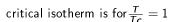
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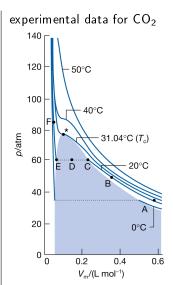
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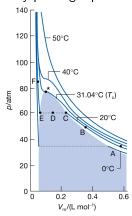
At high pressures, average separation of molecules is small, repulsive forces dominate and the gas is less compressible because now the forces help to drive the molecules apart

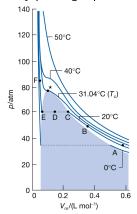


van der Waals isotherms at several values of $\frac{T}{Tc}$ 1.5 p/p_c 1.0 0.5 0 0.1 10 V/V_{c}

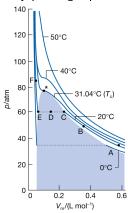






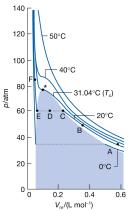


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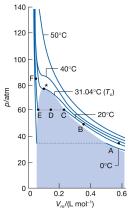
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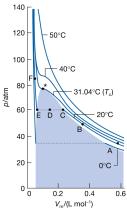


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pressure on line CDE, when both liquid and vapour are present in equilibrium, is the vapour pressure of liquid at the temperature of the experiment



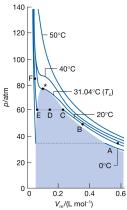
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further reduction of volume requires exertion of considerable pressure

At $T = T_{\rm C}$

At $I = I_C$ surface separating two phases does not appear and the volumes at each end of the horizontal part of the isotherm have merged to a single point \Rightarrow critical point

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The single phase that fills the entire volume when $T>T_{\it C}$ may be much denser than typical gas : supercritical fluid

features of the van der Waals eqn

(1) Perfect gas isotherms obtained at high
$$T$$
 and large V_m

$$\rho = \frac{RT}{V_m - b} - \frac{a}{V_m^2} \quad \overset{\text{high } T}{\bigvee_{m \gg b}} \quad \frac{RT}{V_m}$$

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(3) critical constants related to van der Waals coefficients

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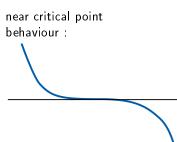
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These extrema converge as $T \to T_C$ and coincide at $T = T_C$ at the

inflexion

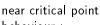
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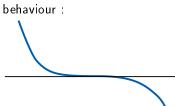


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obtain : $V_c = 3b$; $p_C = \frac{a}{27h^2}$

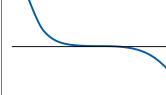
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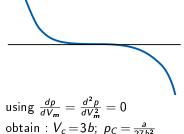
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Below a critical temperature, T_C , van der Waals isotherms show oscillations

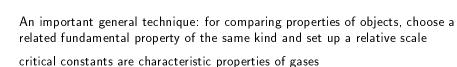


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- divide actual variable by corresponding critical constant:

$$V_r = \frac{V}{V_c}$$
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$$V_r = \frac{V}{V_c}$$
; $p_r = \frac{p}{p_c}$; $T_r = \frac{T}{T_c}$
 $p = p_r p_C$; $V = V_r V_C$; $T = T_r T_C$

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works best for gases composed of spherical molecules fails when the molecules are non-spherical or polar

The principle of corresponding states :

i ne princip	de of correspon	iding states :				
				Critical constants		
	Equation	Reduced form*	Pc	$V_{\rm c}$	$T_{\rm c}$	
Perfect gas	$p = \frac{nRT}{V}$					
van der Waals	$p = \frac{nRT}{V - nb} - \frac{n^2a}{V^2}$	$p_{\rm r} = \frac{8T_{\rm r}}{3V_{\rm r} - 1} - \frac{3}{V_{\rm r}^2}$	$\frac{a}{27b^2}$	3b	$\frac{8a}{27bR}$	
Berthelot	$p = \frac{nRT}{V - nb} - \frac{n^2a}{TV^2}$	$p_{\rm r} = \frac{8T_{\rm r}}{3V_{\rm r} - 1} - \frac{3}{T_{\rm r}V_{\rm r}^2}$	$\frac{1}{12}\left(\frac{2aR}{3b^3}\right)^{1/2}$	3b	$\frac{2}{3} \left(\frac{2a}{3bR} \right)^{1/2}$	
Dieterici	$p = \frac{nRTe^{-aRTV/n}}{V - nb}$	$p_{\rm r} = \frac{T_{\rm r} e^{2(1-1/T_{\rm r} V_{\rm r})}}{2V_{\rm r} - 1}$	$\frac{a}{4e^2b^2}$	2b	$\frac{a}{4bR}$	
Virial	$n = \frac{nRT}{1 + \frac{nB(T)}{1 + \frac$	$a^2C(T)$				

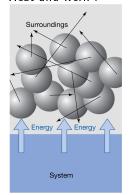
$$p = \frac{nRT}{V} \left\{ 1 + \frac{nB(T)}{V} + \frac{n^2C(T)}{V^2} + \cdots \right\}$$

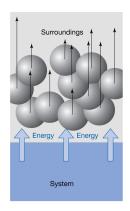


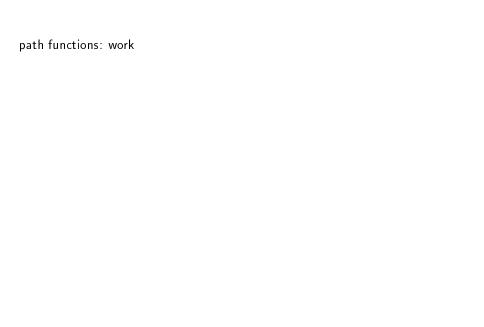
critical constants : typical values

	gas	РC	$ V_{C} $	T _C	$Z_{C} = \frac{p v_{m}}{RT}$	Τ _B
		atm	cm ³	K		K
	Ar	48.0	75.3	150.7	0.292	411.5
	CO_2	72.9	94.0	304.2	0.274	714.8
-	Не	2.26	57.8	5.2	0.305	22.64
	<u>O</u> _	50.14	78 N	154.8	0.308	<u>405 0</u>

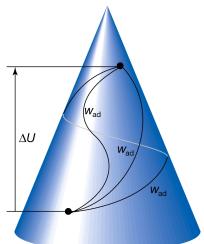
Heat and work:



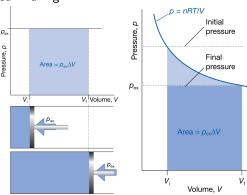




path functions: work $\Delta \textit{U} = \textit{w}_{ad}$



Calculating work:



 $\begin{aligned} \text{Heat} : \\ dU &= dq + dw_{\text{exp}} + dw_{\text{e}} \end{aligned}$

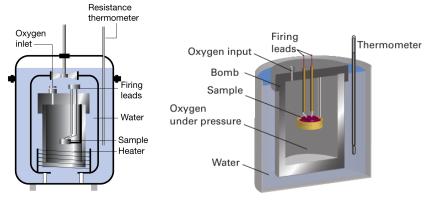
 $\begin{array}{lll} \text{Heat}: \\ dU = dq + dw_{\text{exp}} + dw_{\text{e}} \\ \uparrow & \uparrow & \uparrow \\ \text{upper lower expansion extra} \\ \text{case} \end{array}$

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 $dU = dq_V$

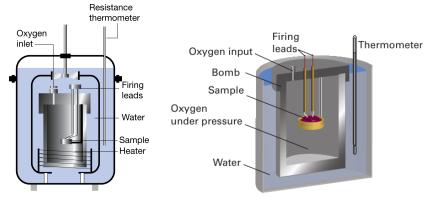
Calorimetry

- Constant volume bomb calorimeter : measurement of $q_{\it V}$



Calorimetry

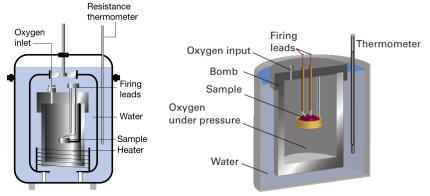
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'bomb': central vessel, strong enough to withstand high pressures To ensure adiabaticity, calorimeter is immersed in a water bath with temperature continuously readjusted to that of calorimeter at each stage of combustion

change in calorimeter temperature,	$\Delta T \propto {\sf energy}$	released or ab	sorbed in reaction

change in calorimeter temperature, $\Delta T \propto$ energy released or absorbed in reaction measuring $\Delta T \implies q_V$ and hence ΔU

Calibration: use a process of known energy output and determine calorimeter

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measuring
$$\Delta T \implies q_V$$
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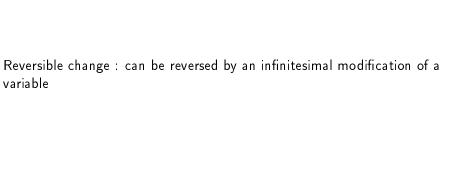
constant

 $q = C\Delta T$

Thermodynamic engine:

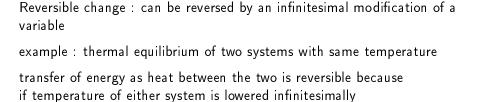


Type of work	dw	Comments	Units†
Expansion	$-p_{\rm ex} dV$	$p_{\rm ex}$ is the external pressure d V is the change in volume	Pa m³
Surface expansion	$\gamma \mathrm{d}\sigma$	γ is the surface tension ${ m d}\sigma$ is the change in area	$N m^{-1} m^2$
Extension	fdl	f is the tension dl is the change in length	N m
Electrical	ϕ d Q	ϕ is the electric potential dQ is the change in charge	V C
	$Q d\phi$	$\mathrm{d}\phi$ is the potential difference Q is the charge transferred	V C



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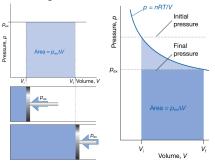
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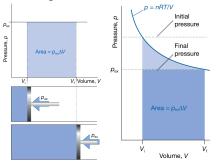
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Calculating work:



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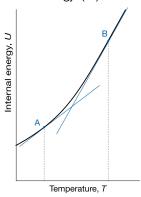
expansion =
$$V_{f}$$

$$-\int_{V_{i}}^{V_{f}} p_{\text{ext}} dV = -\int_{V_{i}}^{V_{f}} p dV$$

$$= -nRT \ln \frac{V_{f}}{V_{i}}$$

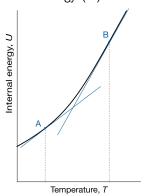
for spontaneous expansion : $work = -p_{ext} (V_f - V_i)$

Internal energy (U) as a function of temperature : U(V, T)



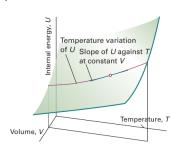
internal energy of a system increases as temperature is raised

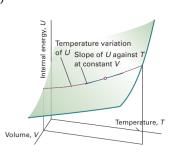
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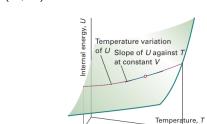
internal energy of a system increases as temperature is raised slope of tangent at any temperature =heat capacity, *C* in the Fig.,

C at A < C at B



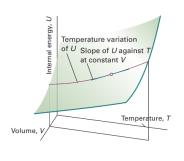


$$C_V = \left(\frac{dq}{dT}\right)_V = \left(\frac{\partial U}{\partial T}\right)_V$$



Volume, V

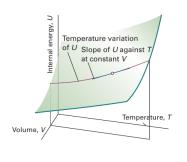
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 $\implies dU = C_V dT$
If heat capacity is independent

If heat capacity is independent of temperature over range of temperatures of interest then $\Delta U = C_V \Delta T$