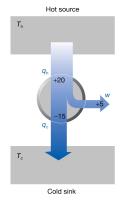
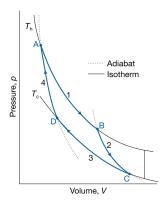
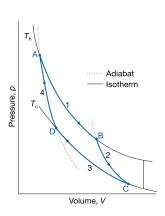
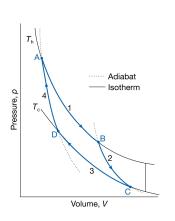
Example of a Carnot engine



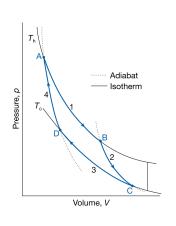


 $q_h = nRT_h \ln rac{V_B}{V_A}; \quad q_c = nRT_c \ln rac{V_D}{V_C}$





 $q_h = nRT_h \ln \frac{V_B}{V_A};$ $q_c = nRT_c \ln \frac{V_D}{V_C}$ adiabats: $V_A T_h^c = V_D T_c^c$ (exponent $c = \frac{C_V}{nR}$) and $V_C T_c^c = V_B T_h^c$

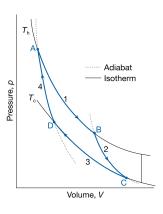


$$\begin{split} q_h &= nRT_h \ln \frac{V_B}{V_A}; \quad q_c = nRT_c \ln \frac{V_D}{V_C} \\ \text{adiabats: } V_A T_h^c &= V_D T_c^c \text{ (exponent } c = \frac{C_V}{nR} \text{)} \\ \text{and} \qquad V_C T_c^c &= V_B T_h^c \\ \text{obtain: } V_A V_C T_h^c T_c^c &= V_D V_B T_h^c T_c^c \end{split}$$

and
$$\therefore \frac{V_A}{V_B} = \frac{V_D}{V_C} \Longrightarrow q_C = -nRT_C \ln \frac{V_B}{V_A}$$

 $\cdot q_b = -T_b$

$$\therefore \frac{q_h}{q_c} = -\frac{T_h}{T_c}$$



$$q_h = nRT_h \ln rac{V_B}{V_A}; \quad q_c = nRT_c \ln rac{V_D}{V_C}$$

and $V_C T_c^c = V_B T_h^c$

obtain :
$$V_A V_C T_h^c T_C^c = V_D V_B T_h^c T_c^c$$

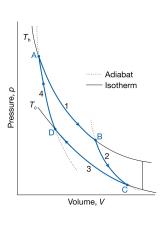
and $\therefore \frac{V_A}{V_B} = \frac{V_D}{V_C} \Longrightarrow q_c = -nRT_c \ln \frac{V_B}{V_A}$

adiabats: $V_A T_h^c = V_D T_c^c$ (exponent $c = \frac{C_V}{nR}$)

$$\therefore \frac{q_h}{q_c} = -\frac{T_h}{T_c}$$
work performed

efficiency,
$$\eta = \frac{\text{work performed}}{\text{heat absorbed}} = \frac{|w|}{q_h}$$

$$= \frac{q_h + q_c}{q_h} = 1 + \frac{q_c}{q_h} = 1 - \frac{T_c}{T_h}$$



 $q_h = nRT_h \ln rac{V_B}{V_A}; \quad q_c = nRT_c \ln rac{V_D}{V_C}$

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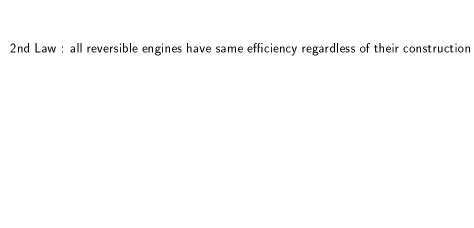
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$$V_A V_C T_h^c T_C^c = V_D V_B T_h^c T_C^c$$

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$$\therefore \frac{q_h}{q_c} = -\frac{T_h}{T_c}$$

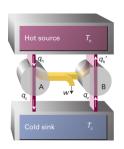
efficiency,
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 $= rac{q_h + q_c}{q_h} = 1 + rac{q_c}{q_h} = 1 - rac{T_c}{T_h}$

$$\Delta S = \frac{q_h}{T_h} + 0 + \frac{q_c}{T_c} + 0 = 0$$



Equivalent to Kelvin-Planck statement : Proof by contradiction

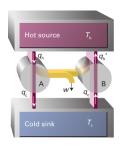
Let $\eta_A > \eta_B$ engine A takes heat q_h from hot source and dumps q_c in cold reservoir



Equivalent to Kelvin-Planck statement : Proof by contradiction

Let $\eta_A>\eta_B$ engine A takes heat q_h from hot source and dumps q_c in cold reservoir

Reverse engine B



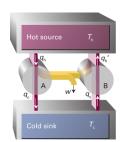
Equivalent to Kelvin-Planck statement : Proof by contradiction

Hot source

Let $\eta_A>\eta_B$ engine A takes heat q_h from hot source and dumps q_c in cold reservoir

Reverse engine B engine B acquires energy heat q_c from cold reservoir and releases $q_h' < q_h$ to the hot end

Equivalent to Kelvin-Planck statement : Proof by contradiction

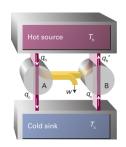


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Form composite engine C : A+B

► Equivalent to Kelvin-Planck statement : Proof by contradiction



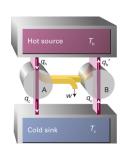
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C takes heat $q_h - q'_h$ from hot source and converts it completely into work

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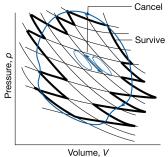
C takes heat $q_h - q'_h$ from hot source and converts it completely into work

⇒ violation of Kelvin-Planck statement of second law



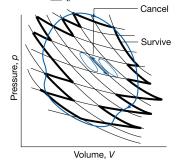
any reversible cycle \approx collection of Carnot cycles \oint (arbitrary path)

$$=\sum \oint$$
 (each cycle)



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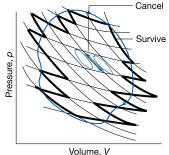
$$=\sum \phi$$
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 ΔS along an individual path inside is cancelled by ΔS along the path it shares with neighbouring cycle

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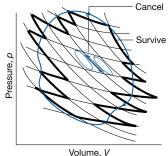


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The approxmn. becomes exact as individual cycles become infinitesimal $\phi(\text{arbitrary path}) = \sum \phi \text{ (each cycle)} = 0$

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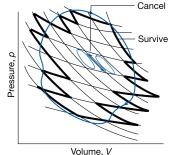
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... all entropy changes cancel except for those along perimeter of the overall cycle

$$\sum_{\mathsf{all}} \frac{q_{\mathsf{rev}}}{T} = \sum_{\mathsf{perimeter}} \frac{q_{\mathsf{rev}}}{T} = 0$$

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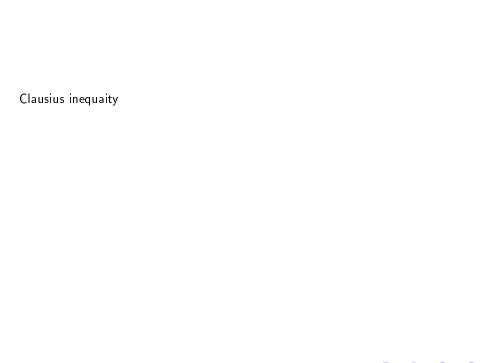
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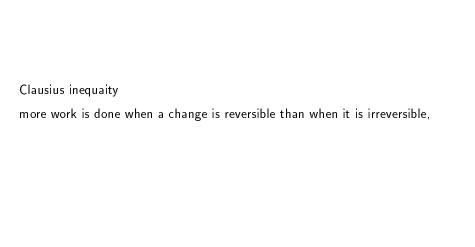
∴ all entropy changes cancel except for those along perimeter of the overall cycle

$$\sum_{\mathsf{all}} rac{q_{\mathsf{rev}}}{T} = \sum_{\mathsf{perimeter}} rac{q_{\mathsf{rev}}}{T} = 0$$

In the limit of infinitesimal cycles, the non-cancelling edges of Camot cycles match the overall cycle exactly, and the sum becomes an integral

 \implies dS is exact differential and S is state function





Clausius inequaity	

i.e.,, $|dw_{rev}| \ge |dw|$

more work is done when a change is reversible than when it is irreversible,

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$$dU = dq + dw = dq_{rev} + dw_{rev}$$

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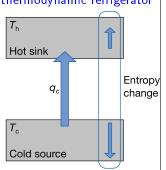
 $dq_{\mathsf{rev}} \ge dq, :: \Delta S = \int \frac{dq_{\mathsf{rev}}}{T} \ge \int \frac{dq}{T}$

Consider transfer of energy as heat from one system - hot source-at T_h

to another system - the cold sink- at T_c

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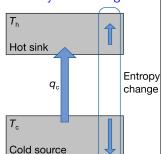
thermodynamic refrigerator



energy removed from cool source at temp. T_c = $\frac{|q_c|}{T}$

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thermodynamic refrigerator



energy removed from cool source at temp. T_c = $\frac{|q_c|}{T_c}$

and deposited in warmer sink at temp. T_h

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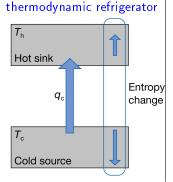
thermodynamic refrigerator $T_{\rm h}$ Hot sink Entropy q_c change Cold source

energy removed from cool source at temp. T_c $=\frac{|q_c|}{T}$

and deposited in warmer sink at temp. T_h

$$\Delta S = -rac{|q_c|}{T_c} + rac{|q_c|}{T_h} < 0 \implies$$
 not spontaneous

Consider transfer of energy as heat from one system - hot source-at \mathcal{T}_h to another system - the cold sink- at \mathcal{T}_c

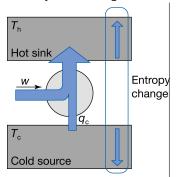


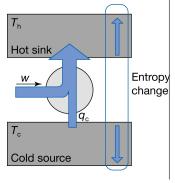
energy removed from cool source at temp. T_c = $\frac{|q_c|}{T_c}$

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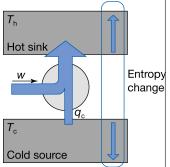
$$\Delta S = -rac{|q_e|}{T_e} + rac{|q_e|}{T_h} < 0 \implies$$
 not spontaneous

to generate more entropy, energy must be added to the stream that enters the warm sink. task: find minimum energy to be supplied



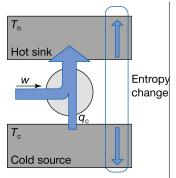


coefficient of peformance, $c = \frac{\text{energy transferred as heat}}{\text{energy transferred as work}} = \frac{|q_c|}{|w|}$

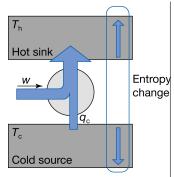


coefficient of peformance,
$$c = \frac{\text{energy transferred as heat}}{\text{energy transferred as work}} = \frac{|q_c|}{|w|}$$

The less the work required to achieve a given transfer, greater is \boldsymbol{c}

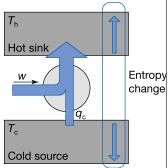


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coefficient of peformance, $c = \frac{\text{energy transferred as heat}}{\text{energy transferred as work}} = \frac{|q_c|}{|w|}$ The less the work required to achieve a given transfer, greater is c and more efficient the refrigerator. $\frac{1}{c} = \frac{|q_h| - |q_c|}{|q_c|} = \frac{|q_h|}{|q_c|} - 1$

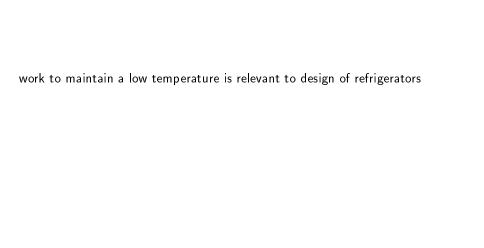
Thermodynamic refrigerator



coefficient of peformance,
$$c = \frac{\text{energy transferred as heat}}{\text{energy transferred as work}} = \frac{|q_c|}{|w|}$$
The less the work required to achieve a given transfer, greater is c and more efficient the refrigerator.

using $\frac{q_h}{q_c} = -\frac{T_h}{T_c}$, we get, $c = \frac{T_c}{T_h - T_c}$

 $\frac{1}{c} = \frac{|q_{h}| - |q_{c}|}{|q_{c}|} = \frac{|q_{h}|}{|q_{c}|} - 1$



work to maintain a low temperature is relevant to design of refrigerators
No thermal insulation is perfect there is always a flow of energy as heat into the sample at a rate $\propto \Delta T$

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If rate at which energy leaks = $A(T_h - T_c)$ where A depends on sample size and insulation then minimum power, P, required to maintain original ΔT by pumping out energy by heating surroundings

$$P = \frac{1}{c} A (T_h - T_c) = \frac{A(T_h - T_c)^2}{T_c} \propto (\Delta T)^2$$

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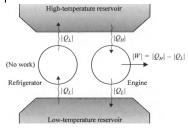
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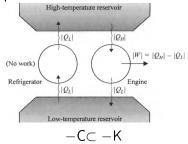
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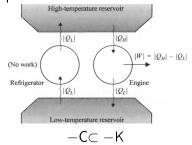
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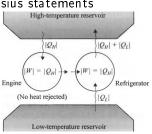
power increases as $(\Delta T)^2$

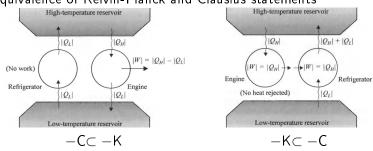
: air-conditioners more expensive to run on hot days than on mild days



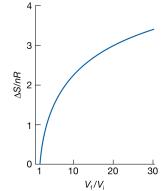


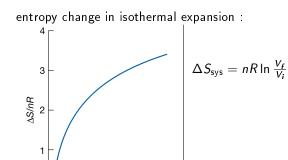






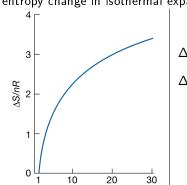
entropy change in isothermal expansion :





 $V_{\rm f}/V_{\rm i}$

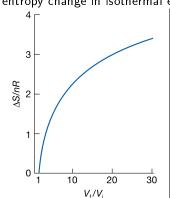
entropy change in isothermal expansion :



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 $\Delta S_{
m sys} = nR \ln rac{V_f}{V_i}$ $\Delta S_{
m surr\ (rev)} = -\Delta S_{
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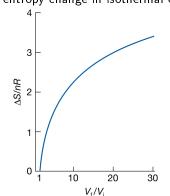


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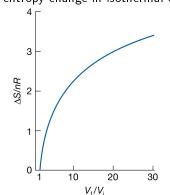
$$\Delta U = 0$$

∴ If isothermal expansion occurs freely, $w_{\text{surr}} = 0$ and irreversibly, then q = 0

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$$\therefore$$
 If isothermal expansion occurs freely, $w_{\text{surr}} = 0$ and irreversibly, then $q = 0$

$$\therefore \Delta \textit{S}_{\text{surr (irrev)}} = 0$$

$$S_{\text{total}(\text{rev})} = 0 \text{ rev}$$

 $> 0 \text{ irred}$

Phase transition : $\Delta_{\mathsf{trs}} \mathcal{S} = \frac{\Delta_{\mathsf{trs}} \mathcal{H}}{T_{\mathsf{trs}}}$

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Trouton's rule:

wide range of liquids have approx. same $\Delta_{\text{vap}} S$ ($\approx 85 \text{ J K}^{-1} \text{ mol}^{-1}$)

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Ex. liq. Br₂:

- no complexity like hydrogen bonding in liquid Br₂ there is no unusual behaviour in the gas phase - safe to use Trouton's rule

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- boils at 59.2°C, $\Delta_{\rm vap} H^{\odot} = T_b \times 85 \rm J~mol^{-1}$ = 332.4 \times 85 = 28kJ mol⁻¹

Phase transition : $\Delta_{trs}S = \frac{\Delta_{trs}H}{T_{trans}}$

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 $\mathsf{Ex.}\ \mathsf{liq.}\ \mathsf{Br}_2 \colon$

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- safe to use Trouton's rule

- boils at 59.2°C,
$$\Delta_{\rm vap}H^{\odot}=T_b\times 85\rm J~mol^{-1}$$
 = 332.4 \times 85 = 28kJ mol $^{-1}$

experimental value : $29.45 \text{ kJ mol}^{-1}$

entropy change as a function of temperature (varying heat capacity) :

$$S(T_f) = S(T_i) + \int_{T_i}^{T_f} \frac{dq_{rev}}{T}$$

entropy change as a function of temperature (varying heat capacity):

Solution of temperature (varying heat capacity):
$$S(T_f) = S(T_i) + \int_{T_i}^{T_f} \frac{dq_{rev}}{T}$$

$$const. \ p(V): S(T_f) = S(T_i) + \int_{T_i}^{T_f} \frac{C_{p(V)}dT}{T}$$

$$= S(T_i) + C_{p(V)} \ln \frac{T_f}{T_i}$$
 | label: heat capacity

solved problem : Calculate ΔS when 0.500 dm³ of Ar at 25°C and 1.00 bar expands to 1.000 dm³ and is simultaneously heated to 100°C

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S is a state function

... choose a convenient path from initial state

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S is a state function

 $0.5~dm^3~Ar;~25^{\circ}C \xrightarrow[sotherma]{rev.~expansion} 1~dm^3~Ar;~25^{\circ}C \xrightarrow[const.~V]{heat} 1~dm^3~Ar;~100^{\circ}C$

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$$0.5~dm^3~Ar;~25^{\circ}C \xrightarrow[isothermal]{rev.~expansion} 1~dm^3~Ar;~25^{\circ}C \xrightarrow[const.~V]{heat} 1~dm^3~Ar;~100^{\circ}C$$

$$\Delta S_{l} = nR \ln \frac{V_{f}}{V_{i}} = \frac{p_{i}V_{i}}{T_{i}} \ln \frac{V_{f}}{V_{i}};$$

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$$0.5~\text{dm}^3~\text{Ar};~25^{\circ}\text{C} \xrightarrow[\text{isothermal}]{\text{rev. expansion}} 1~\text{dm}^3~\text{Ar};~25^{\circ}\text{C} \xrightarrow[\text{const. V}]{\text{heat}} 1~\text{dm}^3~\text{Ar};~100^{\circ}\text{C}$$

$$\Delta S_{\rm I} = nR \ln \frac{V_f}{V_c} = \frac{p_i V_i}{T_c} \ln \frac{V_f}{V_c}; \qquad \Delta S_{\rm II} = C_V \ln \frac{T_f}{T_c}$$

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$$\begin{split} \Delta S &= \Delta S_{\mathsf{I}} + \Delta S_{\mathsf{II}} = nR \left(\ln \frac{V_f}{V_i} + \frac{3}{2} \ln \frac{T_f}{T_i} \right) = \frac{p_i V_i}{T_i} \ln \left(\frac{V_f}{V_i} \left[\frac{T_f}{T_i} \right]^{\frac{3}{2}} \right) \\ &= \frac{10^5 \operatorname{Pa} \times 0.5 \times 10^{-3} \operatorname{m}^3}{298} \ln \left(\frac{1}{0.5} \left[\frac{373}{298} \right]^{\frac{3}{2}} \right) \end{split}$$

$$= \frac{10^{5} \, \text{Pa} \times 0.5 \times 10^{-3} \, \text{m}^{3}}{298} \, \text{ln} \left(\frac{1}{0.5} \left[\frac{373}{298} \right]^{\frac{3}{2}} \right) = 0.173 \, \text{JK}^{-1}$$

solved problem : Calculate ΔS when 0.5 dm³ of Ar at 25°C and 1.00 bar is

compressed to $0.05~\mathrm{dm^3}$ and is simultaneously cooled to $-25^{\circ}\mathrm{C}$

solved problem : Calculate ΔS when 0.5 dm³ of Ar at 25°C and 1.00 bar is compressed to 0.05 dm^3 and is simultaneously cooled to -25°C

0.5 dm³ Ar; 25°C $\xrightarrow[\text{isothermal}]{\text{erev. expansion}}$ 0.05dm³ Ar; 25°C $\xrightarrow[\text{const. V}]{\text{const. V}}$ 0.05dm³ Ar; -25°C

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compressed to 0.05 dm^3 and is simultaneously cooled to -25°C

0.5 dm³ Ar; 25°C
$$\xrightarrow[\text{isothermal}]{\text{rev. expansion}} 0.05$$
dm³ Ar; 25°C $\xrightarrow[\text{cool}]{\text{const. V}} 0.05$ dm³ Ar; -25°C

 $\Delta S_{\mathsf{I}} = nR \ln \frac{V_f}{V_i} = \frac{p_i V_i}{T_i} \ln \frac{V_f}{V_i};$

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compressed to 0.05 dm³ and is simultaneously cooled to
$$-25^{\circ}$$
C

0.5 dm³ Ar; 25°C $\xrightarrow{\text{rev. expansion}}$ 0.05dm³ Ar; 25°C $\xrightarrow{\text{cool}}$ 0.05dm³ Ar; -25° C

 $\Delta S_{\text{I}} = nR \ln \frac{V_f}{V_c} = \frac{p_i V_i}{T_c} \ln \frac{V_f}{V_c}; \qquad \Delta S_{\text{II}} = C_V \ln \frac{T_f}{T_c}$

solved problem: Calculate ΔS when 0.5 dm³ of Ar at 25°C and 1.00 bar is

compressed to 0.05 dm³ and is simultaneously cooled to
$$-25^{\circ}$$
C

0.5 dm³ Ar: 25°C rev. expansion 0.05 dm³ Ar: 25°C $\frac{\text{cool}}{2}$ 0.05 dm³ Ar: -25° C

0.5 dm³ Ar; 25°C
$$\xrightarrow{\text{rev. expansion}}_{\text{isothermal}}$$
 0.05dm³ Ar; 25°C $\xrightarrow{\text{cool}}_{\text{const. V}}$ 0.05dm³ Ar; -25°C $\Delta S_{\text{II}} = nR \ln \frac{V_f}{V} = \frac{p_i V_i}{V} \ln \frac{V_f}{V}$; $\Delta S_{\text{II}} = C_V \ln \frac{T_f}{V}$

0.5 dm³ Ar; 25°C
$$\xrightarrow[\text{isothermal}]{\text{even}}$$
 0.05dm³ Ar; 25°C $\xrightarrow[\text{cool}]{\text{cool}}$ 0.05dm³ Ar; -25°C $\Delta S_{\text{I}} = nR \ln \frac{V_f}{V_i} = \frac{p_i V_i}{T_i} \ln \frac{V_f}{V_i}$; $\Delta S_{\text{II}} = C_V \ln \frac{T_f}{T_i}$

 $\Delta S = \Delta S_{\mathsf{I}} + \Delta S_{\mathsf{II}} = nR \left(\ln \frac{V_f}{V_i} + \frac{3}{2} \ln \frac{T_f}{T_i} \right) = \frac{p_i V_i}{T_i} \ln \left(\frac{V_f}{V_i} \left\lceil \frac{T_f}{T_i} \right\rceil^{\frac{3}{2}} \right)$

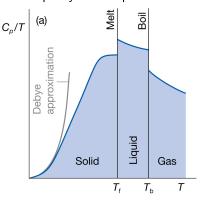
 $=\frac{10^5 \text{Pa} \times 0.5 \times 10^{-3} \text{m}^3}{298} \ln \left(\frac{0.05}{0.5} \left[\frac{248}{298} \right]^{\frac{3}{2}} \right) =$

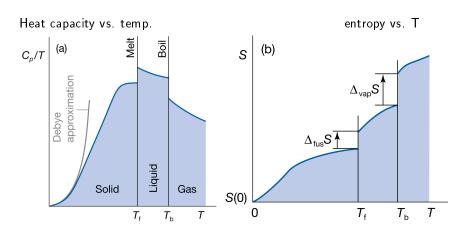
0.5 dm³ Ar; 25°C
$$\xrightarrow{\text{rev. expansion}}_{\text{isothermal}}$$
 0.05dm³ Ar; 25°C $\xrightarrow{\text{cool}}_{\text{const. V}}$ 0.05dm³ Ar; -25°C $\xrightarrow{\text{cool}}_{\text{const. V}}$ 0.05dm³ Ar; -25°C $\xrightarrow{\Delta S_{\text{II}}} = nR \ln \frac{V_f}{V_i} = \frac{p_i V_i}{T_i} \ln \frac{V_f}{V_i}$; $\Delta S_{\text{II}} = C_V \ln \frac{T_f}{T_i}$

 $= -0.44 = -0.44 \text{ IK}^{-1}$

Heat capacity vs. temp.

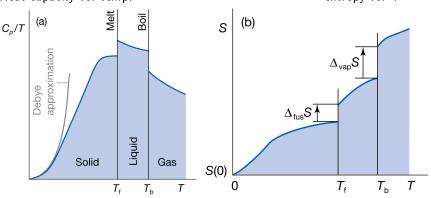




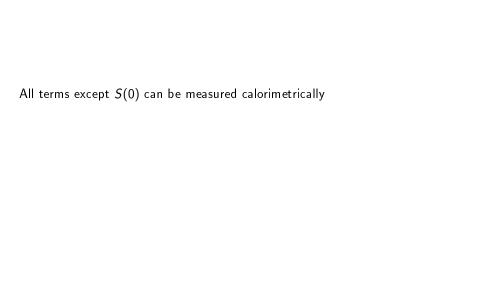


Heat capacity vs. temp.

entropy vs. T



$$S(T) = S(0) + \int_{0}^{T_f} \frac{C_{p}(s)dT}{T} + \frac{\Delta_{\text{fus}}H}{T_{\text{fus}}} + \int_{T_1}^{T_b} \frac{C_{p}(l)dT}{T} + \frac{\Delta_{\text{vap}}H}{T_{\text{vap}}} + \int_{T_1}^{T} \frac{C_{p}(g)dT}{T}$$

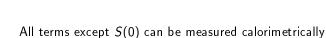


and meeglating analytically			

integrals can be evaluated either graphically or by fitting a polynomial to the data

All terms except S(0) can be measured calorimetrically

and integrating analytically



 $\therefore \frac{dT}{T} = d \ln T$, one can evaluate area under a plot of C_p against $\ln T$

integrals can be evaluated either graphically or by fitting a polynomial to the data

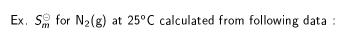
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 $\therefore \frac{dT}{T} = d \ln T$, one can evaluate area under a plot of C_p against $\ln T$. Debye extrapolation : $\mathcal{L}t_0C_p \longrightarrow aT^3$



Ex. S_m^{\odot} for N₂(g) at 25°C calculated from following data : $|S_m^{\odot}/\text{J K}^{-1}\text{mol}^{-1}|$

Ex. S_m^{\odot} for N₂(g) at 25°C calculated from following data :

	$S_m^{\odot}/J K^{-1} mol^{-1}$
Debye extrapolation	1.92
	I

Ex. S_m^{\odot} for $N_2(g)$ at 25°C calculated from following data :

	$S_m^{\odot}/J\;K^{-1}mol^{-1}$
Debye extrapolation	1.92
35.61	25.25

Е.,	C⊝ for N (~)	at 250C adjaulat.	- d fuana fa	عجمام مسابيين	
ĽX.	S_m° for $N_2(g)$	at 25°C calculate	ed from 10	nowing data	

	$S_m^{\odot}/J\;K^{-1}mol^{-1}$
Debye extrapolation	1.92
35.61	25.25
Phase transition: 35.61K	6.43

Ex. S_m^{\odot} for N₂(g) at 25°C calculated from following data :

=x: om ::: ::2(8) as =s & carearassa :::::: : ::::::::::::::: : : ::::::::		
	$S_m^{\odot}/J\;K^{-1}mol^{-1}$	
Debye extrapolation	1.92	
35.61	25.25	
Phase transition: 35.61K	6.43	
63.14	23.38	

Ex. S_m^{\odot} for N₂(g) at 25°C calculated from following data :

111 = (0)	O
	$S_m^{\odot}/J\;K^{-1}mol^{-1}$
Debye extrapolation	1.92
35.61 \int 10	25.25
Phase transition: 35.61K	6.43
63.14	23.38
Fusion: 63.14K	11.42

Ex. S_m^{\odot} for N₂(g) at 25°C calculated from following data :

	$\mid S_m^{\odot} / J \; K^{-1} mol^{-1}$
Debye extrapolation	1.92
35.61	25.25
Phase transition: 35.61K	6.43
63.14	23.38
Fusion : 63.14K	11.42
77.32	11.41

Ex. S_m^{\odot} for $N_2(g)$ at 25°C calculated from following data :

	$\mid S_m^{\circleddash} / J \; K^{-1} mol^{-1}$
Debye extrapolation	1.92
35.61	25.25
Phase transition: 35.61K	6.43
63.14	23.38
Fusion: 63.14K	11.42
77.32	11.41
Vaporization: 77.32K	72.13
	,

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$S_m^{\odot}/J\;K^{-1}$ mol $^{-1}$
1.92
25.25
6.43
23.38
11.42
11.41
72.13
39.20

Ex. S_m^{\odot} for N₂(g) at 25°C calculated from following data :

	$ S_m^{\odot}/J\;K^{-1}mol^{-1} $
Debye extrapolation	1.92
35.61	25.25
Phase transition: 35.61K	6.43
63.14	23.38
Fusion: 63.14K	11.42
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Vaporization: 77.32K	72.13
298.15	39.20
Correction for gas imperfection	0.92

Ex. S_m^{\odot} for N2(g) at 25°C calculated from following data :

	$\mid S_m^{\odot} / J \; K^{-1} mol^{-1}$
Debye extrapolation	1.92
35.61	25.25
Phase transition: 35.61K	6.43
63.14	23.38
Fusion: 63.14K	11.42
77.32	11.41
Vaporization: 77.32K	72.13
298.15	39.20
Correction for gas imperfection	0.92
Total	192.06

Ex. S_m^{\odot} for $N_2(g)$ at 25°C calculated from following data : $S_m^{\odot}/J \text{ K}^{-1} \text{mol}^{-1}$ Debye extrapolation 1.92 35.61 25 25

J 10	23.23
Phase transition: 35.61K	6.43
63.14	23.38
Fusion: 63.14K	11.42
77.32	11.41
Vaporization: 77.32K	72.13
298.15	39.20
	0.00

0.92 Correction for gas imperfection Total 192.06

 $S_m(298.15 \,\mathrm{K}) = S_m(0) + 192.06 \,\mathrm{J} \,\mathrm{K}^{-1} \mathrm{mol}^{-1}$

Nernst heat theorem : $\mathop{\mathcal{L}t}_{T o 0}\Delta S\longrightarrow 0$ for any transformation provided all

substances involved are perfectly crystalline

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The entropy of all perfect crystalline substances is zero at T=0

3rd law (?) :

Nernst heat theorem : $\underset{T \to 0}{\mathcal{L}t} \Delta S \longrightarrow 0$ for any transformation provided all

 $\Omega=\#$ ways the molecules can be arranged in a crystalline form

Boltzmann formula : $S = k_B \ln \Omega$

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Boltzmann formula : $S = k_B \ln \Omega$

$$\Omega = \#$$
ways the molecules can be arranged in a crystalline form

In most cases, $\underset{T\to 0}{\mathcal{L}t}\Omega=1,$ $\therefore \underset{T\to 0}{\mathcal{L}t}S=0$ when $\Omega\neq 0$, then S=S(0), residual entropy

Ice-I_h: each H atom can lie either close to or far from its 'parent' O atom

total # of arrangements in sample of N H_2O molecules with 2N H atoms = 2^{2N} lce-l_h:
each H atom can lie either close to or far from its 'parent' O atom
total # of arrangements in sample of NH₂O molecules with 2N H atoms = 2^{2N} consider a single central O atom.

total number of arrangements of locations of H atoms around central O atom of one H_2O molecule is $2^4=16$

lce-l $_{\rm h}$: each H atom can lie either close to or far from its 'parent' O atom total # of arrangements in sample of N H $_2$ O molecules with 2N H atoms = 2^{2N} consider a single central O atom.

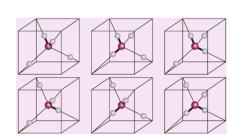
total number of arrangements of locations of H atoms around central O atom of one H_2O molecule is $2^4=16$ Of these , only 6 correspond to two

short and two long bonds

Ice-I_h:

each H atom can lie either close to or far from its 'parent' O atom total # of arrangements in sample of N H_2O molecules with 2 N H atoms = 2^{2N} consider a single central O atom. total number of arrangements of locations of H atoms around central O atom of one H_2O molecule is $2^4 = 16$ Of these, only 6 correspond to two short and two long bonds only $\frac{6}{16} = \frac{3}{8}$ of all arrangements are possible, and for N molecules only

 $(3/8)^N$ of all arrangements are possible

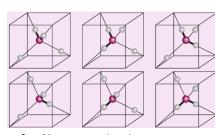


Ice-Ih:

each H atom can lie either close to or far from its 'parent' O atom total # of arrangements in sample of N H₂O molecules with 2N H atoms = 2^{2N} consider a single central O atom. total number of arrangements of locations of H atoms around central O

atom of one H_2O molecule is $2^4 = 16$ Of these, only 6 correspond to two

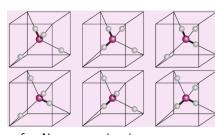
short and two long bonds only $\frac{6}{16} = \frac{3}{8}$ of all arrangements are possible, and for N molecules only $(3/8)^N$ of all arrangements are possible



∴ for N water molecules # of possible configurations = $2^{2N}(3/8)^N = (\frac{3}{2})^N$

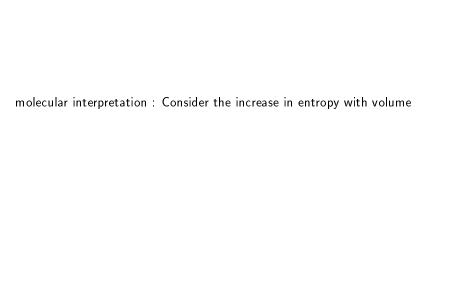
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∴ for N water molecules # of possible configurations = $2^{2N}(3/8)^N = \left(\frac{3}{2}\right)^N$

$$S(0) = Nk_B \ln \left(\frac{3}{2}\right) = 3.37 \text{ J mol}^{-1} \text{K}^{-1}$$



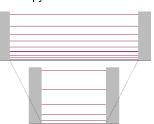
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molecular	Interpretation	(onci	dar tha	Increase	ın	ontrony	with	VALUMA
IIIOIECUIAI	interpretation	COLISI	uei tile	IIICI Case	111	CILLIODA	WILLI	volulle

As the system size increases energy levels move closer together and more become accessible to the molecules

molecular interpretation: Consider the increase in entropy with volume

As the system size increases energy levels move closer together and more become accessible to the molecules

ways of achieving same energy (Ω) increases



Maxwell's demon: a thought experiment

Open the tab and gas in first chamber expands to fill both chambers

A gas initially in one chamber, connected via a closed tap to a second chamber

containing only vacuum

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Maxwell's demon: a thought experiment

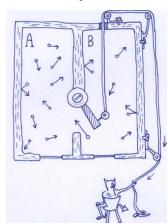
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Maxwell imagined that the tap was operated by a microscopic intelligent creature. If it sees a molecule heading from the second chamber back into the first, it opens the tap and then shuts it, just letting the molecule through. If it sees a molecule heading from the first chamber back into the second chamber, it keeps the tap closed



Maxwell's demon: a thought experiment

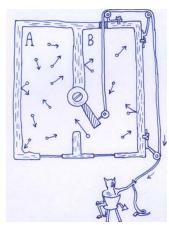
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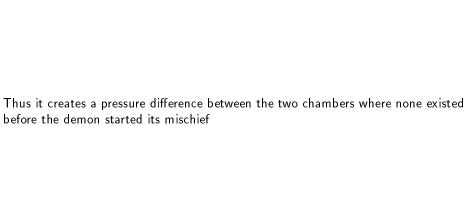
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Demon does no work and yet it makes molecules in second chamber all go back into the first chamber



Thus it	creates	a pressure	difference	between	the two	chambers	where none	existed

as if the demon could therefore cause entropy to decrease in a system with no

before the demon started its mischief

consequent increase in entropy anywhere else

► Conventional explanation : All observations and measurements require energy consumption and the demon is no exception

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- It is possible to design a computational process that proceeds entirely reversibly, and therefore has no increase in entropy associated with it
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- Erasing information has an associated increase in entropy Maxwell's demon can operate reversibly therefore, but only if it has a large
- enough hard disc that it doesn't ever need to clear space to continue operating.

The Landauer principle: "information is physical" and it has an e	energy

quantifies the thermodynamic cost of the recording/erasure of one bit of

equivalent

information,

The Landauer principle: "information is physical" and it has an energy equivalent

quantifies the thermodynamic cost of the recording/erasure of one bit of information.

Erasure of one bit of information requires a minimum energy cost equal

to $k_B T \ln 2 \approx 0.018$ eV, where T is the temperature of a thermal

reservoir used in the process.

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- electrical or optical signals.

 ➤ ∴ it must obey the laws of physics and, first and foremost, the laws of thermodynamics.

system or its environment

(1) any logically irreversible process must result in an entropy increase in the non-information-bearing degrees of freedom of the information-processing

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• an amount of energy equal to $k_B T \ln 2$ ($k_B T = \text{thermal noise per unit}$ bandwidth) is needed to transmit a bit of information, and more if quantized

channels are used with photon energies $h\nu > kT$