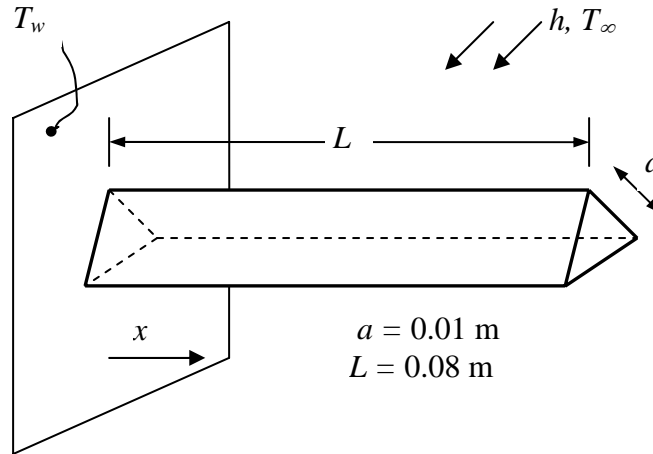


Solutions - Problem Set # 4

Problem 1:



Given: $k_{rod} = 138.56 \text{ W/m-K}$; $T_w = 118^\circ\text{C}$; $h = 20 \text{ W/m}^2\text{-K}$ and $T_\infty = 18^\circ\text{C}$

Assumption: i) SS, 1-D heat conduction problem with constant properties: ii) compensated length approach is adequate.

This is case 2 (convection from the tip surface); however, using compensated length approach, the solution to the problem can be approximated using the results for Case 3 (insulated tip).

a) Estimate the tip temperature

We use the corrected length:

$$L_c = L + \Delta L \cong L + \frac{A_{c.s.tip}}{P_{c.s.tip}}$$

$$A_{c.s.tip} = \frac{a^2}{4} \tan(60^\circ) = \frac{0.01^2}{4} \sqrt{3} = 4.33 \times 10^{-5} \text{ m}^2$$

$$P_{c.s.tip} = 3a = 0.03 \text{ m}$$

$$L_c = L + \frac{4.33 \times 10^{-5}}{0.03} = 0.08 + 1.443 \times 10^{-3} = 0.081443 \text{ m}$$

Solution to Case 3 (insulated tip) using L_c

$$\frac{\theta}{\theta_{Base}} = \frac{T - T_\infty}{T_{Base} - T_\infty} = \frac{\cosh[m(L_c - x)]}{\cosh[mL_c]}$$

$$\rightarrow T_{tip} = T_{x=L_c} = T_{\infty} + (T_{Base} - T_{\infty}) \frac{1}{\cosh[mL_c]}$$

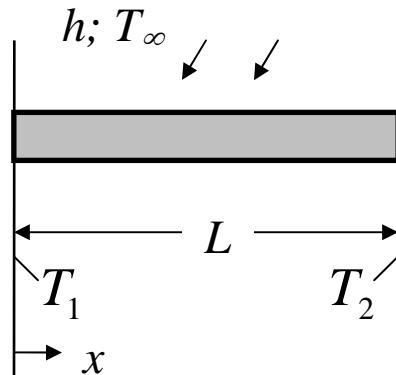
$$m = (hP_{c.s.} / k_s A_{c.s.})^{0.5} = \left(\frac{20 \times 0.03}{138.56 \times 4.33 \times 10^{-5}} \right)^{0.5} = 10 \text{ m}^{-1}$$

$$T_{tip} = T_{x=L_c} = 18 + (118 - 18) \frac{1}{\cosh[10 \times 0.081443]} = 92.05^{\circ}\text{C}$$

b) Calculate the fin efficiency

$$\eta_{Fin, Case3} = \frac{\tanh[mL_c]}{(mL_c)} = \frac{\tanh[10 \times 0.081443]}{(10 \times 0.081443)} = 0.825$$

Problem 2:



Given:

$$T_{\infty} = 38^{\circ}\text{C}; T_1 = 200^{\circ}\text{C}; T_2 = 93^{\circ}\text{C}$$

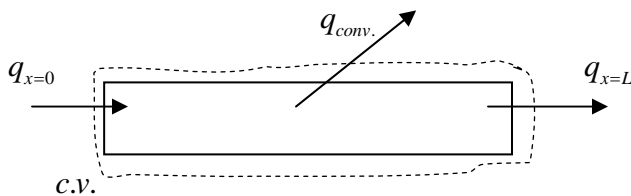
$$h = 17 \text{ W/m}^2\text{-K}; k = 395 \text{ W/m-K}$$

$$L = 30 \text{ cm}; D = 12.5 \text{ mm}$$

a)

Assumptions: classical fin theory applies; 1-D, SS; excellent thermal contact Wall-Base, $R_{th, contact} = 0$

Energy balance on the rod:



$$q_{conv.} = q_{x=0} - q_{x=L}$$

$$q_{x=0} = -k_s \left. \frac{dT}{dx} \right|_{x=0} A_{c.s.}; q_{x=L} = -k_s \left. \frac{dT}{dx} \right|_{x=L} A_{c.s.}$$

Case 4 (prescribed temperature)

The solution for temperature distribution for this case is given in handout #3. You can also drive this by solving the general solution presented and by applying BCs.

$$\frac{\theta}{\theta_{Base}} = \frac{T - T_{\infty}}{T_{Base} - T_{\infty}} = \frac{(\theta_L / \theta_{Base}) \sinh[mx] + \sinh[m(L-x)]}{\sinh[mL]}$$

$$T = T_{\infty} + \frac{(T_{Base} - T_{\infty})}{\sinh[mL]} \left\{ \frac{(T_L - T_{\infty})}{(T_{Base} - T_{\infty})} \sinh[mx] + \sinh[m(L-x)] \right\}$$

$$\frac{dT}{dx} = \frac{(T_{Base} - T_{\infty})}{\sinh[mL]} m \left\{ \frac{(T_L - T_{\infty})}{(T_{Base} - T_{\infty})} \cosh[mx] - \cosh[m(L-x)] \right\}$$

$$\left. \frac{dT}{dx} \right|_{x=0} = \frac{(T_{Base} - T_{\infty})}{\sinh[mL]} m \left\{ \frac{(T_L - T_{\infty})}{(T_{Base} - T_{\infty})} - \cosh[mL] \right\}$$

$$\left. \frac{dT}{dx} \right|_{x=L} = \frac{(T_{Base} - T_{\infty})}{\sinh[mL]} m \left\{ \frac{(T_L - T_{\infty})}{(T_{Base} - T_{\infty})} \cosh[mL] - 1 \right\}$$

$$\left. \frac{dT}{dx} \right|_{x=0} - \left. \frac{dT}{dx} \right|_{x=L} = \frac{(T_{Base} - T_{\infty})}{\sinh[mL]} m \left\{ \frac{(T_L - T_{\infty})}{(T_{Base} - T_{\infty})} - \cosh[mL] - \frac{(T_L - T_{\infty})}{(T_{Base} - T_{\infty})} \cosh[mL] + 1 \right\}$$

$$\left. \frac{dT}{dx} \right|_{x=0} - \left. \frac{dT}{dx} \right|_{x=L} = m \frac{(1 - \cosh[mL])}{\sinh[mL]} \{T_L + T_{Base} - 2T_{\infty}\}$$

$$q_{conv.} = q_{x=0} - q_{x=L} = -kA_{cs} \left[\left. \frac{dT}{dx} \right|_{x=0} - \left. \frac{dT}{dx} \right|_{x=L} \right]$$

after arranging terms:

$$q_{conv.} = -kA_{cs} m \frac{(1 - \cosh[mL])}{\sinh[mL]} \{T_L + T_{Base} - 2T_{\infty}\}$$

$$R_{th-contact} = 0 \rightarrow T_{Base} = T_1 \text{ and } T_L = T_2$$

$$m = (hP_{c.s.} / k_s A_{c.s.})^{0.5} = \left(\frac{17 \times \pi 12.5 \times 10^{-3}}{395 \times \pi (12.5 \times 10^{-3})^2 / 4} \right)^{0.5} = 3.711 \text{ m}^{-1}$$

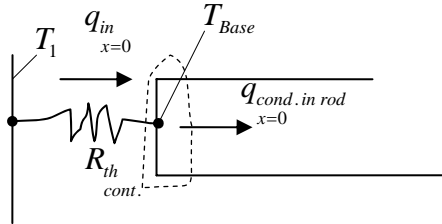
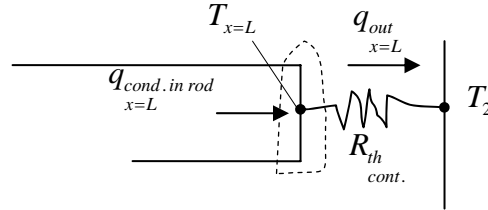
$$q_{conv.} = -395 \left(\pi (12.5 \times 10^{-3})^2 / 4 \right) 3.711 \frac{(1 - \cosh[3.711 \times 0.3])}{\sinh[3.711 \times 0.3]} (200 + 93 - 2 \times 38)$$

$$q_{conv.} = 19.73 \text{ W}$$

(b)

$$A_{cs} = \frac{\pi}{4} \times (12.5 \times 10^{-3})^2 = 1.2272 \times 10^{-4} \text{ m}^2$$

$$R_{th, cont.} = 1 / (h_{cont} A_{cs}) = 1 / [1000 \times 1.2272 \times 10^{-4}] = 8.149 \text{ } ^\circ\text{C/W}$$

at $x = 0$ at $x = L$ at $x = 0$

$$q_{in, x=0} = q_{cond, rod, x=0}$$

$$\frac{T_1 - T_{Base}}{R_{th, cont.}} = -kA_{cs} \left. \frac{dT}{dx} \right|_{x=0}$$

at $x = L$

$$q_{cond, rod, x=L} = q_{out, x=L}$$

$$\frac{T_{x=L} - T_2}{R_{th, cont.}} = -kA_{cs} \left. \frac{dT}{dx} \right|_{x=L}$$

* at $x = 0$

$$\frac{T_1 - T_{Base}}{R_{th, cont.}} = -kA_{cs} \frac{(T_{Base} - T_\infty)}{\sinh[mL]} m \left\{ \frac{(T_L - T_\infty)}{(T_{Base} - T_\infty)} - \cosh[mL] \right\}$$

$$\frac{200 - T_{Base}}{8.149} = -395 \times 1.2272 \times 10^{-4} \frac{(T_{Base} - 38)}{\sinh[3.711 \times 0.3]} 3.711 \left\{ \frac{(T_L - 38)}{(T_{Base} - 38)} - \cosh[3.711 \times 0.3] \right\}$$

$$\Rightarrow 2.82T_{Base} - 1.0794T_L = 228.16 \quad (1)$$

* at $x = L$

$$\frac{T_L - T_2}{R_{th, cont.}} = -kA_{cs} \frac{(T_{Base} - T_\infty)}{\sinh[mL]} m \left\{ \frac{(T_L - T_\infty)}{(T_{Base} - T_\infty)} \cosh[mL] - 1 \right\}$$

$$\frac{T_L - 93}{8.149} = -395 \times 1.2272 \times 10^{-4} \frac{(T_{Base} - 38)}{\sinh[3.711 \times 0.3]} 3.711 \left\{ \frac{(T_L - 38)}{(T_{Base} - 38)} \cosh[3.711 \times 0.3] - 1 \right\}$$

$$\Rightarrow -1.0794T_{Base} + 2.82T_L = 121.16 \quad (2)$$

$$(1) \text{ and } (2) \Rightarrow T_{Base} = 114.1^\circ\text{C}$$

$$T_L = 86.62^\circ\text{C}$$

at $x = 0$

$$q_{in, x=0} = \frac{T_1 - T_{Base}}{R_{th, cont.}}$$

$$q_{in, x=0} = \frac{200 - 114.1}{8.149} = 10.54 \text{ W}$$

at $x = L$

$$q_{out, x=L} = \frac{T_{x=L} - T_2}{R_{th, cont.}}$$

$$q_{out, x=L} = \frac{86.62 - 93}{8.149} = -0.783 \text{ W} \quad (\text{thus, heat is conducted in})$$

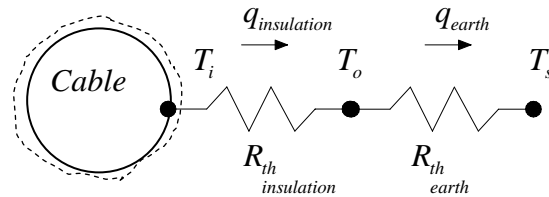
$$q_{conv.} = 10.54 - (-0.783) = 11.3 \text{ W}$$

Problem 3:

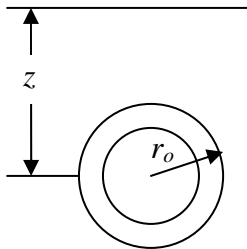
a)

S.S. E-Bal. on the Cable:

$$q_{generation, cable} = q_{insulation} = q_{earth}$$



$$q_{generation, cable} = \frac{T_i - T_s}{R_{th, insul.} + R_{th, Earth}}$$



$$R_{th, Earth} = \frac{1}{Sk_{earth}} = \frac{\ln(z/r_o)}{2\pi k_{earth} L} \quad (z > 3r_o) \quad \text{Table 3-1 in Holman, 2002.}$$

Please note that for this system, other textbooks have provided a different

$$\text{Shape factor: } S = \frac{2\pi L}{\ln(2z/r_o)} \quad (\text{e.g., Incropera and DeWitt, 1994})$$

When $I_{cable} = I_{max}$, $T_i = T_{ins, max} = 80^\circ\text{C}$

$$q_{generation, cable, MAX} = \frac{80 - 10}{\frac{\ln(r_o/r_i)}{2\pi k_{ins} L} + \frac{\ln(z/r_o)}{2\pi k_{earth} L}} = \frac{80 - 10}{\frac{\ln(0.015/0.01)}{2\pi \times 5} + \frac{\ln(0.3/0.015)}{2\pi \times 0.5}} L$$

$$\text{Thus, } q_{generation, cable, MAX} = \frac{70}{0.0129 + 0.95} L = 72.4L$$

$$q_{generation, cable, MAX} = I_{MAX}^2 R_e = 72.4L$$

$$\rightarrow I_{MAX}^2 \times (5 \times 10^{-4} \times L) = 72.4L \Rightarrow I_{MAX} = 380.5 \text{ A}$$

b)

under the operating condition in part (a) $S_{in\ cable} = \frac{q_{generation}}{Volume} = \frac{72.4L}{\left[\pi(0.02)^2 / 4\right]L} = 230456.35 \text{ W/m}^3$

With constant S inside the cable, the temperature profile was developed in handout #2. Thus,

$$T - T_i = \frac{1}{4} \frac{S_{cable}}{k_{cable}} r_i^2 \left[1 - \left(\frac{r}{r_i} \right)^2 \right] \text{ and } T_{\max} = T_{r=0}$$

$$T_{\max} = T_i + \frac{1}{4} \frac{S_{cable}}{k_{cable}} r_i^2 = 80 + \frac{1}{4} \times \frac{230456.35}{200} (0.01)^2 = 80.029^\circ\text{C}$$