

1. All cylinders are identical (except for gas in them)
Same cross-sectional area A .
Pistons each have mass M .
Each piston is in Mechanical equilibrium.

$$F_{\text{down}} = F_{\text{up}} \quad \text{pressure of ideal gas.}$$
$$Mg + P_0 A = P A$$

(external pressure

In all 3 cylinders, F_{down} is the same

So $P_A = P_B = P_C$ which answers parts (a) & (b)

2. Thermodynamic system: Helium; treat it as ideal gas
($M_g = 4 \text{ g/mol}$)

State a: $T_a = 1100 \text{ K}$ $V_a = 0.5 \times 10^{-3} \text{ m}^3$

State b: $T_b = 1100 \text{ K}$ $P_b = 1.0 \times 10^5 \text{ Pa}$

State c: $T_c = 300 \text{ K}$

$a \rightarrow b$ isothermal ($T_a = T_b$)

$b \rightarrow c$ isochoric ($V_b = V_c$)

$c \rightarrow a$ isobaric ($P_c = P_a$)

$N = \text{const}$ - need to find N to determine mass of He present

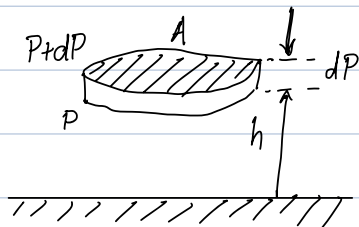
$$\begin{aligned}
 N &= \frac{P_a V_a}{RT_a} \\
 &= \frac{P_c V_a}{RT_a} \\
 &= \frac{T_c P_b}{T_b} \frac{V_a}{RT_a} \qquad V_b = V_c, \quad \frac{P_c}{T_c} = \frac{P_b}{T_b}
 \end{aligned}$$

$$= \frac{300 (1 \times 10^5) (0.5 \times 10^{-3})}{(1100) (8.314) (1100)}$$

$$= 1.49 \times 10^{-3} \text{ moles}$$

$$\begin{aligned}
 M_{He} &= N \times M_g \\
 &= 1.49 \times 10^{-3} \text{ moles} (4 \text{ g/mol}) \\
 &= 5.96 \times 10^{-3} \text{ g} \\
 &\approx 6 \text{ mg.}
 \end{aligned}$$

3. a) Show that $\frac{dP}{dh} = -\rho g$



Mechanical equilibrium $\Rightarrow F_{\text{down}} = F_{\text{up}}$

$$\begin{aligned}
 F_{\text{down}} &= dm g + (P + dP) A \\
 &= (P A dh) g + (P + dP) A
 \end{aligned}$$

$$F_{\text{up}} = P A$$

$$\Rightarrow (PA dh)g + \cancel{PA} + dPA = \cancel{PA}$$

$$\Rightarrow \boxed{\frac{dP}{dh} = -\rho g} \quad \text{--- (1)}$$

b) Assume isothermal ideal gas to show $\left(\frac{\partial P}{\partial p}\right)_T = \frac{Mg}{RT}$

$$\text{Since } N = \frac{m}{Mg} \quad \& \quad \rho = \frac{m}{V}$$

$$PV = NRT$$

$$\Rightarrow P = \frac{PRT}{Mg}$$

$$\Rightarrow dP = \frac{RT}{Mg} dp + \frac{PR}{Mg} dT$$

$$\text{Const } T \Rightarrow dT = 0$$

by definition of partial diffs

$$dP = \left(\frac{\partial P}{\partial p}\right) dp + \left(\frac{\partial P}{\partial T}\right) dT$$

$$\Rightarrow \boxed{\left(\frac{\partial P}{\partial p}\right)_T = \frac{Mg}{RT}} \quad \text{for const } T \quad \text{--- (2)}$$

c) from (1) & (2) obtain $\left(\frac{\partial P}{\partial h}\right)_T$

$$\frac{dP}{dh} = \frac{dP}{dP} \frac{dP}{dh}$$

$$\begin{aligned} \text{at const } T \\ \left(\frac{\partial P}{\partial h} \right)_T &= \frac{dP}{dh} \left(\frac{\partial P}{\partial P} \right)_T \\ &= - \frac{\rho g M_g}{RT} \end{aligned}$$

Since g & T are constant

$$\frac{dP}{P} = - \frac{g M_g}{RT} dh$$

Integrate both sides

$$\int_{P_0}^P \frac{dP}{P} = \int_0^h - \frac{g M_g}{RT} dh$$

$$\Rightarrow \ln \left(\frac{P}{P_0} \right) = - \frac{g M_g}{RT} h \quad h_0 = 0$$

$$\Rightarrow P = P_0 \exp \left(- \frac{g M_g h}{RT} \right)$$

$$d) \quad h_0 = \frac{RT}{g M_g}$$

$$\text{Taking } T = 293 \text{ K}, \quad M_g = 28.96 \times 10^{-3} \text{ kg/mol}$$

$$\begin{aligned} h_0 &= \frac{(8.314)(293)}{(9.8)(28.96 \times 10^{-3})} \\ &= 8.58 \times 10^3 \text{ m} \\ &\sim 8.6 \text{ km.} \end{aligned}$$

Sea level: $h_{sl} = 0$ $P_{sl} = 1.01 \times 10^5 \text{ Pa}$ $T_{sl} = 20^\circ\text{C} = 293 \text{ K}$

top of Bannaby mountain: $h_B = 1200 \text{ feet}$ (from city of Bannaby)
 $= 367 \text{ m}$

Peak of Whistler: $h_W = 2182 \text{ m}$ (www.tourismwhistler.com)

$$P_{sl} = \frac{N}{V} = \frac{P_{sl}}{RT}$$

$$N = \frac{m}{M_g}$$

$$= \frac{(1.01 \times 10^5 \text{ Pa})}{(8.314 \text{ J/mol}\cdot\text{K})(293)}$$

$$= 41.46 \text{ moles/m}^3 \times (28.96 \times 10^{-3} \text{ kg/mol})$$

$$= 1.2 \text{ kg/mol}$$

$$P_B = P_{sl} \exp\left(-\frac{g M_g h_B}{RT}\right)$$

$$= 41.46 \exp\left(-\frac{(9.8)(28.96 \times 10^{-3})(367)}{(8.314)(293)}\right)$$

$$= 40 \text{ moles/m}^3$$

$$P_W = 32 \text{ moles/m}^3$$

$$P_B = RT P_B$$

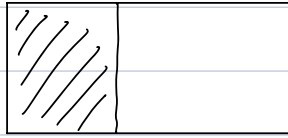
$$= 9.7 \times 10^4 \text{ Pa}$$

$$= 0.96 \text{ atm}$$

$$P_W = 7.8 \times 10^4 \text{ Pa}$$

$$\sim 0.77 \text{ atm.}$$

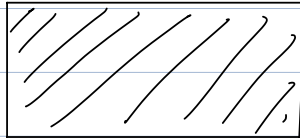
4. state a :



$$T_a = 300 \text{ K} \quad P_a = 10^5 \text{ Pa}$$

$$V_a = 1 \times 10^{-3} \text{ m}^3$$

state b :



$$T_b = ? \quad P_b = ? \quad V_b = 3 \times 10^{-3} \text{ m}^3$$

a) $\Delta U = 0$

Since $\Delta U = \frac{3}{2} N R \Delta T$

$$\Delta T = 0$$

$$T_b = T_a = 300 \text{ K}$$

b) $N = \text{const}$ so

$$\frac{P_a V_a}{T_a} = \frac{P_b V_b}{T_b}$$

$$P_b = \frac{V_a}{V_b} P_a$$

$$= \frac{10^{-3}}{3 \times 10^{-3}} 10^6$$

$$= 3.3 \times 10^4 \text{ Pa}$$

$$= 33 \text{ kPa}$$

if you used $V_b = 2 \times 10^{-3} \text{ m}^3$
you got $P_b = 50 \text{ kPa}$.

5. System is an ideal gas
process is quasistatic \Rightarrow quasistatic work.

Fig 3.3 : $W_{ab} = - \int_{V_a}^{V_b} P dV$ (isochoric compression)

I don't know what P is but I know it's constant

$$\begin{aligned}\Rightarrow W_{ab} &= -P(V_b - V_a) \\ &= P(V_a - V_b) \\ &= 300 \times 10^3 \text{ Pa} (2 - 0.5) \text{ m}^3 \\ &= +450 \text{ kJ}\end{aligned}$$

Fig 3.4. : $W_{ab} = - \int_{V_a}^{V_b} P dV$

$$P = mV + P_0$$

$$m : \frac{(500 - 300) \times 10^3}{2 - 0.5} = 1.33 \times 10^5 \text{ Pa/m}^3$$

$$\frac{500 \times 10^3 - P_0}{2 - 0} = 1.33 \times 10^5$$

$$\Rightarrow P_0 = 2.33 \times 10^5 \text{ Pa}$$

$$P = 1.33 \times 10^5 V + 2.33 \times 10^5$$

$$W_{ab} = - \int_{V_a}^{V_b} [1.33 \times 10^5 V + 2.33 \times 10^5] dV$$

$$= - \left[\frac{1.33 \times 10^5}{2} (V_b^2 - V_a^2) + 2.33 \times 10^5 (V_b - V_a) \right]$$

$$= - \frac{1.33 \times 10^5}{2} (4 - 0.25) - 2.33 \times 10^5 (2 - 0.5)$$

$$= -598 \text{ kJ}$$

Fig. 3.5. : $V_a = 3 \text{ m}^3$ $V_b = 1 \text{ m}^3$

$$\begin{aligned} W_{ab} &= \text{Area under Curve} \\ &= P \Delta V + \frac{1}{2} \pi r^2 \\ &= 2 \times 10^5 (2) + \frac{1}{2} \pi (100 \times 10^3) (1) \\ &= 5.57 \times 10^5 \text{ J} \end{aligned}$$

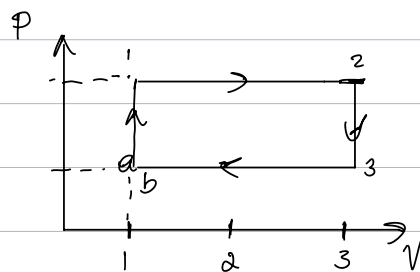
Fig 3.6. $PV^2 = \text{Const} = K$

$$\begin{aligned} P &= \frac{K}{V^2} \\ W_{ab} &= -K \int_a^b \frac{1}{V^2} dV \\ &= K \left(\frac{1}{V_b} - \frac{1}{V_a} \right) \end{aligned}$$

$$\begin{aligned} P_a V_a^2 &= K = (50 \times 10^3 \text{ Pa}) (2 \text{ m}^3)^2 \\ &= 200 \times 10^3 \text{ Pa m}^6 \end{aligned}$$

$$\begin{aligned} W_{ab} &= 200 \times 10^3 \text{ Pa m}^6 \left(\frac{1}{1 \text{ m}^3} - \frac{1}{2 \text{ m}^3} \right) \\ &= + 1 \times 10^5 \text{ J} \end{aligned}$$

Fig 3.7 $W_{ab} = - \text{area of rectangle}$
best way to calculate this.



$$\begin{aligned} W_{ab} &= W_{a1} + W_{12} + W_{23} \\ &\quad + W_{3b} \end{aligned}$$

$$W_{a1} = - \int_a P dV \quad dV = 0$$

$$\begin{aligned} W_{12} &= - \int_1^2 P dV = - P \Delta V \\ &= - (400 \times 10^3)(3 - 1) \\ &= - 800 \times 10^3 \text{ J} \end{aligned}$$

$$W_{23} = 0$$

$$\begin{aligned} W_{3b} &= - P \Delta V \\ &= - (200 \times 10^3)(1 - 3) \\ &= 400 \times 10^3 \text{ J} \end{aligned}$$

$$\begin{aligned} W_{ab} &= (-800 + 400) \times 10^3 \\ &= -400 \times 10^3 \text{ J} \end{aligned}$$

Fig 3.8 : $W_{ab} = - \int_a^b P dV$

$$P = \frac{NRT}{V}$$

$$T = mV + T_0$$

$$m = \frac{300 - 400}{1 - 0.2} = -200$$

$$\frac{300 - T_0}{1 - 0} = -200 \quad \Rightarrow \quad T_0 = 500$$

$$T = -200V + 500$$

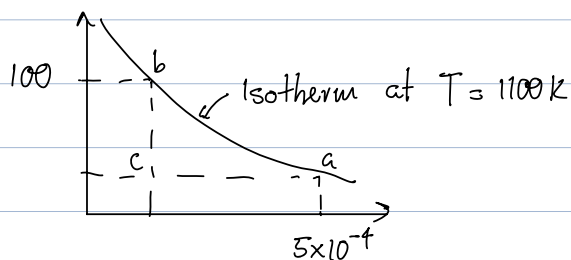
$$P = NR \left[-200 + \frac{500}{V} \right]$$

$$W_{ab} = -NR \int_{V_a}^{V_b} \left(-200 + \frac{500}{V} \right) dV$$

$$= -8.314 \left[-200(0.2 - 1) + 500 \ln \left(\frac{0.2}{1.0} \right) \right] \quad N=1$$

$$= 5.36 \times 10^3 \text{ J}$$

6.



$$T_c = 300 \text{ K}$$

$$V_a = 5 \times 10^{-4} \text{ m}^3$$

$$P_b = 100 \text{ kPa}$$

a) W_{ab} , W_{bc} , W_{ca} assuming quasistatic processes

$$W_{ab} = - \int_a^b P dV$$

$$= - \int_a^b \frac{NRT}{V} dV$$

$$= NRT \ln \left(\frac{V_a}{V_b} \right)$$

from problem 2.1.6 $m_{He} = 6 \text{ mg}$

$$N = 6 \times 10^{-3} \text{ g} / 4 \text{ g/mol}$$

$$= 1.5 \times 10^{-3} \text{ mol}$$

$$V_b = \frac{NRT}{P_b} = \frac{1.5 \times 10^{-3} \times 8.314 \times 1100}{10^5}$$

$$= 1.37 \times 10^{-4} \text{ m}^3$$

$$W_{ab} = 1.5 \times 10^{-3} (8.314) (1100) \ln \left(\frac{5 \times 10^{-4}}{1.37 \times 10^{-4}} \right)$$

$$\approx 17.76 \text{ J}$$

$$W_{bc} = 0 \quad \text{since} \quad dV = 0$$

$$P_a = \frac{NRT}{V_a} = 2.74 \times 10^4 \text{ Pa}$$

$$W_{ca} = - \int_c^a P dV$$

$$= -2.74 \times 10^4 (5 \times 10^{-4} - 1.37 \times 10^{-4})$$

$$= -9.95 \text{ J}$$

$$b) \quad U_{ab} = U_b - U_a$$

$$= \frac{3}{2} NRT$$

$$= 0$$

$$U_{bc} = \frac{3}{2} NR(T_c - T_b)$$

$$= \frac{3}{2} (P_c V_c - P_b V_b)$$

$$= -\frac{3}{2} (2.74 \times 10^4 \times 1.37 \times 10^{-4} - 10^5 \times 1.37 \times 10^{-4})$$

$$= -14.9 \text{ J}$$

$$U_{ca} = \frac{3}{2} P_a (V_a - V_c)$$

$$= 14.9 \text{ J}$$

$$ab : W_{ab} > U_{ab}$$

$$bc : W_{bc} > U_{bc}$$

$$ca : W_{ca} < U_{ca}. \quad \text{Not possible, there must be some other}$$

energy exchange process.

$$\begin{aligned}\text{Total work input } W_{ab} + W_{bc} + W_{ca} &= 17.76 - 9.95 \\ &= 7.81 \text{ J}\end{aligned}$$

$$\text{Total energy change } U_{ab} + U_{bc} + U_{ca} = 0$$