# **Project Chemical Species Transport**

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#### **Outline**

#### Discretization of the concentration convection-diffusion equation

Fundamental equation

Boundary conditions

Discretization

**Timestep Control** 

Implementation

Results



## Discretization of the concentration convectiondiffusion equation







## Fundamental equation I

$$\frac{\partial c}{\partial t} + \vec{u} \cdot \nabla c = \lambda \Delta c + Q(t, x, y, \vec{u}, c) \tag{1}$$

- $\bullet$   $\lambda$  diffusion coefficient
- Q source term (location, time, velocity, concentration), multi-species-systems are modeled here
- the chemical processes under consideration have no effect on the density and hence produce no buoyancy forces ⇒ no coupling with the momentum equations
- convective transport:  $\vec{u} \cdot \nabla c$
- diffusive spreading:  $\lambda \Delta c$





## Fundamental equation II

- time step control necessary
- for very stiff equations, implicit procedures might be necessary, we do an explicit time stepping





## **Boundary conditions**

- Dirichlet BC when injecting concentration
- Neumann BC for impermeable walls





#### Discretization I

$$\left[\frac{\partial c}{\partial t}\right]_{ij}^{n+1} + \left[\frac{\partial uc}{\partial x}\right]_{ij} + \left[\frac{\partial vc}{\partial y}\right]_{ij} = \lambda \left[\frac{\partial^2 c}{\partial x^2} + \frac{\partial^2 c}{\partial y^2}\right]_{ij} + Q_{ij}$$
 (2)

$$\left[\frac{\partial c}{\partial t}\right]_{ij}^{n+1} = \frac{1}{dt} \left(c_{ij}^{n+1} - c_{ij}^{n}\right) \tag{3}$$

$$\left[\frac{\partial uc}{\partial x}\right]_{ij} = \frac{1}{dx} \left( u_{ij} \frac{c_{ij} + c_{i+1,j}}{2} - u_{i-1,j} \frac{c_{i-1,j} + c_{ij}}{2} \right) + \frac{\gamma}{dx} \left( |u_{ij}| \frac{c_{ij} - c_{i+1,j}}{2} - |u_{i-1,j}| \frac{c_{i-1,j} - c_{ij}}{2} \right)$$
(4)





#### Discretization II

$$\left[\frac{\partial vc}{\partial y}\right]_{ij} = \frac{1}{dy} \left(v_{ij} \frac{c_{ij} + c_{i,j+1}}{2} - v_{i,j-1} \frac{c_{i,j-1} + c_{ij}}{2}\right) + \frac{\gamma}{dy} \left(|v_{ij}| \frac{c_{ij} - c_{i,j+1}}{2} - |v_{i,j-1}| \frac{c_{i,j-1} - c_{ij}}{2}\right) \tag{5}$$

$$\left[\frac{\partial^2 c}{\partial x^2}\right]_{ij} = \frac{c_{i+1,j} - 2c_{ij} + c_{i-1,j}}{(dx)^2} \tag{6}$$

$$\left[\frac{\partial^2 c}{\partial y^2}\right]_{ij} = \frac{c_{i,j+1} - 2c_{ij} + c_{i,j-1}}{(dy)^2} \tag{7}$$

- concentration c lies on the center of the staggered grid cell
- standard central differences of the Laplacian
- add timestep control





### **Timestep Control**

$$dt < \frac{1}{2\lambda_i} \left( \frac{1}{(dx)^2} + \frac{1}{(dy)^2} \right)^{-1}$$
 (8)

- has to be added for every new species
- depends on the diffusion constant





## Implementation I

- array of Arrays for multiple concentrations
- array of reals for the lambdas
- extended parameter reader
- extended initialization





## Implementation II

#### Main loop:

- determineNextDT: added support for the concentration convection diffusion equation
- refreshBoundaries: Dirichlet and Neumann BC according to input for every species (e.g. iterate over all Arrays)
- computeFG: no change
- composeRHS: no change
- calculateConcentrations: explicit concentration update
- updateVelocities: no change
- vtk: support for multiple concentrations





#### Results

- two species
- annihilate with each other
- in a complicated grid setup