1) Comparing the water at the outlet to the top of the tanks

$$\frac{P_1}{lg} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{lg} + \frac{V_2^2}{2g} + z_2$$

$$0 + 0 + h = 0 + \frac{V_2^2}{2g} + 0$$

$$V_2^2 = 2gh$$

$$V_2 = \sqrt{2gh}$$

: the relocity of the water at all outlets is  $\sqrt{2gh}$ .

At Wil

$$\frac{P_1}{rg} + \frac{V_1^2}{2g} + h_1 = \frac{P_0}{rg} + \frac{V_0^2}{2g} + \frac{1}{20}$$

$$0 + 0 + h_1 = 0 + \frac{\sqrt{2gh^2}}{2g} + 0$$

h, = h

$$\frac{p_{2}}{p_{3}} + \frac{V_{2}^{2}}{2g} + h_{2} = \frac{p_{0}}{p_{3}} + \frac{V_{0}^{2}}{2g} + \frac{7}{2g}$$

$$0 + 0 + h_2 = 0 + \sqrt{29h} + 0$$

$$\frac{p_3}{p_9} + \frac{v_3^2}{2g} + h_3 = \frac{p_0}{p_9} + \frac{v_0^2}{2g} + \frac{y}{2g}$$

$$\frac{1}{0} + \frac{1}{0} + \frac{1}$$

2) Comparing the surface of the vil to the exit nozzle,

$$\rho_1 + \frac{1}{2}V_1^2 \rho_{0il} + 2\rho_{0il} g = \rho_2 + \frac{1}{2}V_2^2 \rho + 2\rho_g$$
 $0 + 0 + 4\rho_{0il} g = 0 + \frac{1}{2}V_2^2 \rho + 0$ 
 $V_2^2 = 8\rho_{0il} g$ 

V2 = 58569

$$\frac{P_{1}}{p_{9}} + \frac{V_{1}^{2}}{2g} + h = \frac{P_{2}}{p_{9}} + \frac{V_{2}^{2}}{2g} + Z_{2}$$

$$0 + 0 + h = 0 + \frac{\sqrt{856g}}{2g} + 0$$

2) 
$$A_1V_1 = A_2V_2$$

$$\pi(0.2)^2 V_1 = \pi(0.1)^2 V_2$$

$$V_1 = \frac{1}{4}V_2$$

.. Velocity of the water in the pipe is

Upipe = 4 J8569

Comparing the worker at the exit nozzle and at the pipe

$$\frac{p_{1}}{p_{9}} + \frac{v_{1}^{2}}{2g} + z_{1} = \frac{p_{2}}{p_{9}} + \frac{v_{1}^{2}}{2g} + z_{2}$$

$$0 + \frac{\sqrt{8s6g^2}}{2g} + 1 - \frac{\rho_2}{\rho_g} + (\frac{1}{4}\sqrt{8s6g})^2 + 0$$

$$456 + 1 - \frac{1}{4}56 - \frac{\rho_2}{\rho_g}$$

$$P_{2} = (\frac{15}{4} 56 + 1)$$

$$\frac{\rho_{1}}{\rho g} + \frac{v_{1}^{2}}{2g} + \frac{2}{2g} + \frac{\rho_{2}}{\rho g} + \frac{v_{2}^{2}}{2g} + \frac{2}{2g}$$

$$0 + 0 + 4 = 0 + \frac{V_2^2}{2g} + 0$$

$$V_2 = \sqrt{8q}$$

Volumetric flowrate = AV

$$= \pi \left( \frac{5 \times 10^{-2}}{2} \right)^2 \times \sqrt{8 \times 9.81}$$

b) Comparing the water at the highest point with the water exiting the tube

$$0 + 0 = \frac{P_2}{rg} + 4 + H$$

$$H = -4 - \frac{(1.8 - 101.3) \times 10^3}{1000 \times 9.81}$$

4) Volumetric flow rate 
$$Q = A_1V_1 = A_2V_2$$

$$\mathcal{K}\left(\frac{d_1}{2}\right)^2 V_1 = \mathcal{K}\left(\frac{d_2}{2}\right)^2 V_2$$

$$V_1 = \frac{d_2^2}{d_1^2} V_2$$

lomparing the oil at the narrower section of the pipe to the wider section of the pipe

$$\frac{P_{1}}{\rho g} + \frac{V_{1}^{2}}{2g} + Z_{1} = \frac{P_{2}}{\rho g} + \frac{V_{2}^{2}}{2g} + Z_{2}$$

$$\frac{P_{1}-P_{2}}{P_{g}}=\frac{1}{2g}(V_{2}^{2}-V_{1}^{2})+z_{2}-z_{1}$$

$$Sub V_1 = \frac{d_2^2}{d_1^2} V_2$$

$$\frac{P_1 - P_2}{P_9} = \frac{1}{29} \left( V_2^2 - \frac{d_2^4}{d_1^4} V_2^2 \right) + z_2 - z_1$$

$$\frac{P_{1}-P_{2}}{P_{9}}=\frac{V_{2}^{2}}{2g}\left(1-\left(\frac{J_{2}}{J_{1}}\right)^{4}\right)+Z_{2}-Z_{1}$$

$$\frac{V_2^2}{2g}\left(1-\left(\frac{d_2}{d_1}\right)^4\right) = \frac{p_1-p_2}{p_9} + z_1-z_2-(1)$$

4) Finding the pressure difference between 
$$p$$
, and  $p_2$ 

$$p_1 + \frac{56_{Hq}}{56_{0i}} pgh - pg(z_2-z_1+h) = p_2$$

$$p_2 + \frac{56_{Hq}}{56_{0i}} pgh - pgh + pg(z_1-z_2) = p_2$$

$$p_3 + pgh \left(\frac{56_{Hq}}{56_{0i}} - 1\right) + pg(z_1-z_2) = p_2$$

$$p_4 - p_2 = -pgh \left(\frac{56_{Hq}}{56_{0i}} - 1\right) - pg(z_1-z_2)$$

$$\frac{p_1 - p_2}{pg} = z_2 - z_1 - h\left(\frac{56_{Hq}}{56_{0i}} - 1\right) - (z)$$
Sub (2) into (1)

$$\frac{V_{1}^{2}}{2g}\left(1-\left(\frac{d_{1}}{d_{1}}\right)^{4}\right)=\frac{3}{2}\left(1-h\left(\frac{56}{56}\right)+\frac{1}{56}\right)+\frac{1}{2}\left(1-\frac{1}{2}\right)$$

$$V_{2} = \frac{-2(9.81)(100\times10^{-3})(\frac{13.6}{0.9}-1)}{1-(\frac{300\times10^{-3}}{100\times10^{-3}})^{4}}$$

= 0.5882813953 ms-1

$$Q = A_2 V_2 = \pi \left( \frac{300 \times 10^{-3}}{2} \right)^2 (0.5882813953)$$

$$= 0.04158316147 \approx 0.042 \text{m}^3 \text{s}^{-1}$$