$\begin{array}{c} \text{MECH0011 Topic Notes} \\ \text{UCL} \end{array}$

HD

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Part I

Fluids

Chapter 1

Differential equations of mass, momentum and energy

1.1 Differential analysis of fluid flow

What do we want to know? The velocity field, pressures, densities and temperature everywhere and anytime. Hence, these will be a function of (x, y, z, t).

List of variables

	Variable	Type	Units
$\overrightarrow{\overrightarrow{U}} = \overrightarrow{U} = u$	$ \hat{u}_{1} + v\hat{j} + w\hat{k} $ $\hat{u}_{1} + u_{2}\hat{i}_{2} + u_{3}\hat{i}_{3} $	Velocity/Vector	${ m ms^{-1}}$
	p	Pressure/Scalar	${ m Nm^{-2}}$
	T	Temperature/Scalar	$^{\circ}\mathrm{C}$
	ρ	Density/Scalar	${\rm kgm^{-3}}$
T =	$\begin{bmatrix} \tau_{xx} & \tau_{xy} & \tau_{xz} \\ \tau_{yx} & \tau_{yy} & \tau_{yz} \\ \tau_{zx} & \tau_{zy} & \tau_{zz} \end{bmatrix}$	Stress Tensor	${ m Nm^{-2}}$

Since we have 12 variables, we need 12 equations to describe the fluid!

From last year, we have our conservation of mass equation

$$\frac{\partial}{\partial t} \int_{V} \rho \, dV + \oint_{S} (\rho \overrightarrow{V} \cdot \hat{n}) \, dS = 0$$

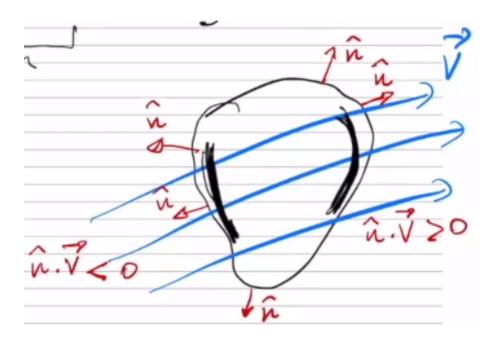


Figure 1.1: Consider \hat{n} to be a vector coming out of the control volume. Depending on where \hat{n} is, our dot product will either be greater than or less than 0.

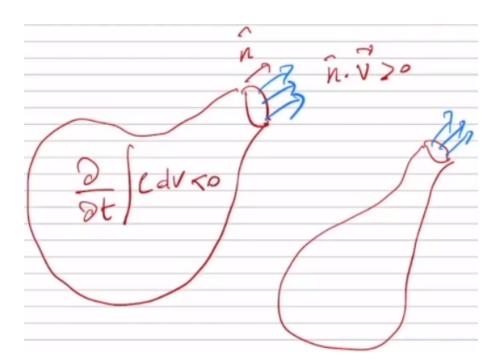
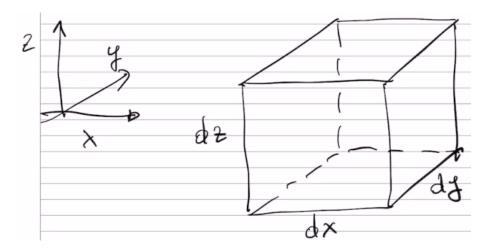


Figure 1.2: There is a velocity exiting the balloon. The amount of mass inside will decrease with time. The volume of the balloon will become smaller. This will be equal to the amount of mass which came out of the control volume (the balloon). If the second term of the continuity equation is positive, the first term must be negative.

1.2 Conservation of mass

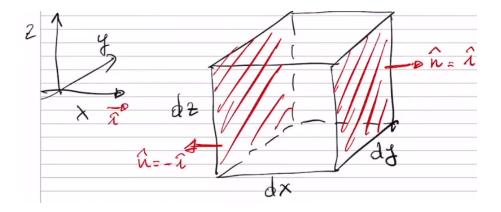
Let us consider an infinitesimally small cube:



Consider term 1 in our continuity equation - the mass variation inside the control volume.

$$\frac{\partial \rho}{\partial t} \cdot dV = \frac{\partial \rho}{\partial t} \cdot dx \cdot dy \cdot dz$$

Consider term 2 - the contribution of mass from the sides of the cube, which are orthogonal to x, shown below.



Left side:

$$\rho \overrightarrow{V} \cdot \hat{n} \, dS = \rho \overrightarrow{V} \cdot (-\hat{i}) \, dz \, dy \tag{1.1}$$

$$= -\rho u \, \mathrm{d}z \, \mathrm{d}y \tag{1.2}$$

Looking from the right side, we will not have a negative (which is coming from the fact that the normal vector is going in the opposite direction to i)

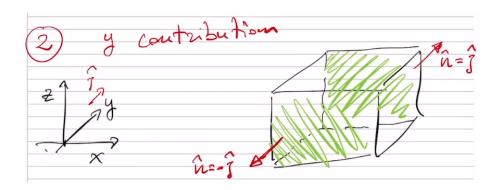
$$(\rho u + \frac{\partial \rho u}{\partial x} \cdot dx) dz dy \tag{1.3}$$

The net contribution from the orthogonal x direction is

$$= (\rho u + \frac{\partial \rho u}{\partial x} \cdot dx) dz \cdot dy - \rho u dz dy$$
 (1.4)

$$= \frac{\partial \rho u}{\partial x} \, \mathrm{d}x \, \mathrm{d}z \, \mathrm{d}y \tag{1.5}$$

y orthogonal contribution



Front side

$$\rho \overrightarrow{V} \cdot \hat{n} \, dS = \rho \overrightarrow{V} \cdot (-\hat{j}) \, dx \, dz$$

$$= -\rho v \, dx \, dz$$
(1.6)

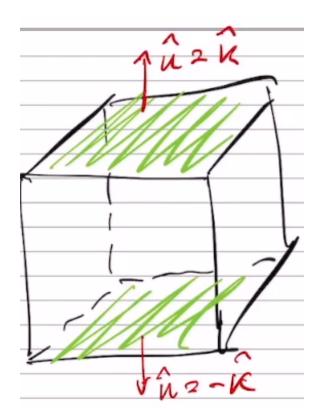
Back side

$$\left(\rho v + \frac{\partial \rho v}{\partial y} \cdot dy\right) dz dx \tag{1.8}$$

Final contribution

$$\frac{\partial \rho v}{\partial y} \, \mathrm{d}y \, \mathrm{d}z \, \mathrm{d}x \tag{1.9}$$

z orthogonal contribution



Bottom side

$$\rho \overrightarrow{V} \cdot \hat{n} \, dS = \rho \overrightarrow{V} \cdot (-\hat{k}) \, dx \, dy \tag{1.10}$$

$$= -\rho w \, \mathrm{d}x \, \mathrm{d}y \tag{1.11}$$

Top side

$$\left(\rho w + \frac{\partial \rho w}{\partial z} \cdot dz\right) dx dy \tag{1.12}$$

Final contribution

$$\frac{\partial \rho w}{\partial z} \, \mathrm{d}z \, \mathrm{d}x \, \mathrm{d}y \tag{1.13}$$

If we add up all of the contributions above, we get the conservation of mass for an infinitesimal volume.

$$\frac{\partial \rho}{\partial t} \cdot dx \cdot dy \cdot dz + \frac{\partial \rho u}{\partial x} dx dz dy + \frac{\partial \rho v}{\partial y} dy dz dx + \frac{\partial \rho w}{\partial z} dz dx dy = 0$$
 (1.14)

This simplifies to:

$$\frac{\partial \rho}{\partial t} + \frac{\partial \rho u}{\partial x} + \frac{\partial \rho v}{\partial y} + \frac{\partial \rho w}{\partial z} = 0 \tag{1.15}$$

We can simplify this a bit more by introducing a term called the divergence.

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \overrightarrow{V}) = 0 \tag{1.16}$$

Where $\nabla \cdot (\rho \overrightarrow{V})$ is the divergence of the vector $\rho \overrightarrow{V}$. It is a scalar.

$$\frac{\partial \rho}{\partial t} + \overrightarrow{V} \cdot \nabla \rho + \rho \nabla \cdot \overrightarrow{V} = 0 \tag{1.17}$$

 $\nabla \cdot \overrightarrow{V}$ is the divergence of the vector \overrightarrow{V} and it is a scalar. $\nabla \rho$ is the gradient of the density ρ and is a vector. It can be expanded as:

$$\frac{\partial \rho}{\partial x}\hat{i} + \frac{\partial \rho}{\partial y}\hat{j} + \frac{\partial \rho}{\partial z}\hat{k} \tag{1.18}$$

$$\overrightarrow{V} \cdot \rho \nabla = (u\hat{i} + v\hat{j} + w\hat{k}) \cdot \left(\frac{\partial \rho}{\partial x}\hat{i} + \frac{\partial \rho}{\partial y}\hat{j} + \frac{\partial \rho}{\partial z}\hat{k}\right) = u\frac{\partial \rho}{\partial x} + v\frac{\partial \rho}{\partial y} + w\frac{\partial \rho}{\partial z}$$
(1.19)

$$\rho \nabla \cdot \overrightarrow{V} = \rho \left(\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} \right) \tag{1.20}$$

For steady flow:

$$\frac{\partial \rho}{\partial t} = 0 \to \nabla \cdot (\rho \overrightarrow{V}) = 0 \tag{1.21}$$

[H] For incompressible flow, the density is constant. This means all derivatives of ρ are 0. Hence, our equation reduces to:

$$\rho = \text{const} \to \nabla \cdot \overrightarrow{V} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$
(1.22)

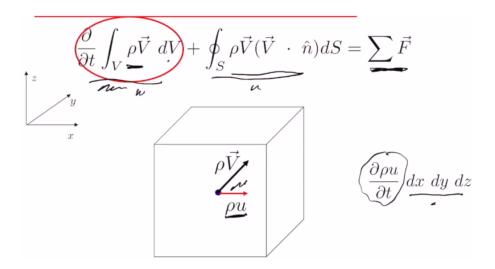
Each of these derivatives represent the stretch or compression of the fluid particle in the orthogonal direction. When these are all added up, it gives the variation in volume. If this is positive, it shows that the volume has increased with time. If ρ is constant, then the volume cannot change. Which is why equation (1.22) must equal 0.

1.3 Conservation of momentum

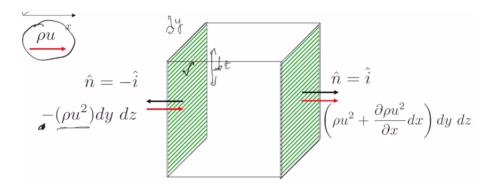
$$\frac{\partial}{\partial t} \int_{V} \rho \overrightarrow{V} \, dV + \oint_{S} \rho \overrightarrow{V} (\overrightarrow{V} \cdot \hat{n}) \, dS = \sum \overrightarrow{F}$$
 (1.23)

We have two types of external force that can act on our infinitesimal fluid element, volumetric forces (e.g. gravity) and surface forces (shear, pressure).

Momentum is a vector as we have to take into account momentum in 3D (first term). We want to know how these change with time. The second term looks at the flux of momentum through the sides of the control volume. In this example, we are only looking at the momentum in the x direction.

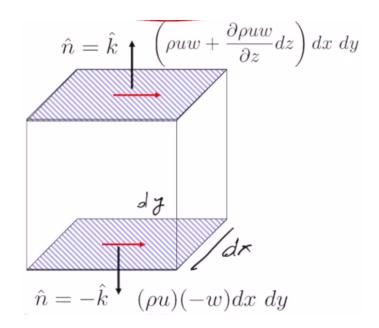


Where $\frac{\partial \rho u}{\partial t} dx dy dz$ is the momentum in x.



Adding the left and the right sides, we get

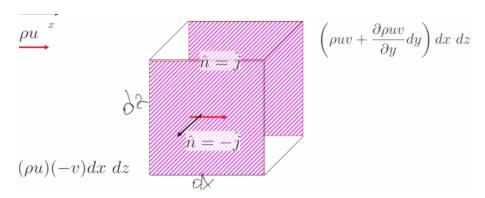
$$\rho u(\overrightarrow{V} \cdot \hat{n}) dS = \frac{\partial (pu^2)}{\partial x} dx dy dz$$
(1.24)



Adding the net contribution to our equation:

$$\rho u(\overrightarrow{V} \cdot \hat{n}) dS = \frac{\partial(\rho u^2)}{\partial x} dx dy dz + \frac{\partial(\rho u w)}{\partial z} dx dy dz$$
 (1.25)

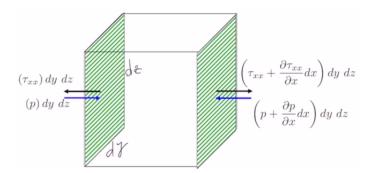
y orthogonal



Adding the net contribution to our equation:

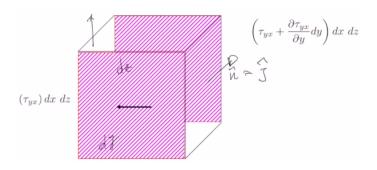
$$\rho u(\overrightarrow{V} \cdot \hat{n}) dS = \frac{\partial(\rho u^2)}{\partial x} dx dy dz + \frac{\partial(\rho u w)}{\partial z} dx dy dz + \frac{\partial\rho u v}{\partial y} dx dy dz \qquad (1.26)$$

Let us look at the $\sum \overrightarrow{F}$ term. Pressure is always exerted orthogonal to a face. We also have our τ stresses acting orthogonally



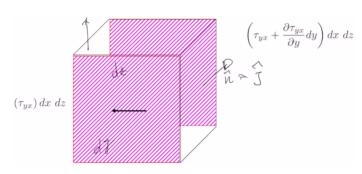
$$\sum F_x = -\left(\frac{\partial p}{\partial x}\right) dx dy dz + \left(\frac{\partial \tau_{xx}}{\partial x}\right) dx dy dz \qquad (1.27)$$

z orthogonal shear force.



$$\sum F_x = -\left(\frac{\partial p}{\partial x}\right) dx dy dz + \left(\frac{\partial \tau_{xx}}{\partial x}\right) dx dy dz + \left(\frac{\partial \tau_{zx}}{\partial z}\right) dx dy dz \qquad (1.28)$$

y orthogonal shear force z orthogonal shear force.



$$\sum F_x = -\left(\frac{\partial p}{\partial x}\right) dx dy dz + \left(\frac{\partial \tau_{xx}}{\partial x}\right) dx dy dz + \left(\frac{\partial \tau_{zx}}{\partial z}\right) dx dy dz + \left(\frac{\partial \tau_{yx}}{\partial y}\right) dx dy dz \quad (1.29)$$

Substituting this back into our original equation, the conservation of momentum in the x direction is:

$$\frac{\partial}{\partial t}(\rho u) + \frac{\partial}{\partial x}(\rho u u) + \frac{\partial}{\partial y}(\rho u v) + \frac{\partial}{\partial z}(\rho u w) = -\frac{\partial p}{\partial x} + \frac{\partial \tau_{xx}}{\partial x} + \frac{\partial \tau_{yx}}{\partial y} + \frac{\partial \tau_{zx}}{\partial z} \quad (1.30)$$

v direction:

$$\frac{\partial}{\partial t}(\rho v) + \frac{\partial}{\partial x}(\rho v u) + \frac{\partial}{\partial y}(\rho v v) + \frac{\partial}{\partial z}(\rho v w) = -\frac{\partial p}{\partial x} + \frac{\partial \tau_{xy}}{\partial x} + \frac{\partial \tau_{yy}}{\partial y} + \frac{\partial \tau_{zy}}{\partial z}$$
(1.31)

z direction (we add ρg here due to the gravitational force acting downwards).

$$\frac{\partial}{\partial t}(\rho w) + \frac{\partial}{\partial x}(\rho w u) + \frac{\partial}{\partial y}(\rho w v) + \frac{\partial}{\partial z}(\rho w w) = -\frac{\partial p}{\partial x} - \rho g + \frac{\partial \tau_{xz}}{\partial x} + \frac{\partial \tau_{yz}}{\partial y} + \frac{\partial \tau_{zz}}{\partial z} \quad (1.32)$$

These can be added to find that we arrive with two terms, one being the continuity equation, which must equal 0. To summarise, we have our continuity equation and momentum equations below.

Conservation of mass

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \overrightarrow{V}) = \frac{\partial \rho}{\partial t} + \frac{\partial \rho u}{\partial x} + \frac{\partial \rho v}{\partial y} + \frac{\partial \rho w}{\partial z} = 0 \tag{1.33}$$

x direction momentum

$$\rho \left(\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} \right) = -\frac{\partial p}{\partial x} + \frac{\partial \tau_{xx}}{\partial x} + \frac{\partial \tau_{yx}}{\partial y} + \frac{\partial \tau_{zx}}{\partial z}$$
(1.34)

y direction momentum

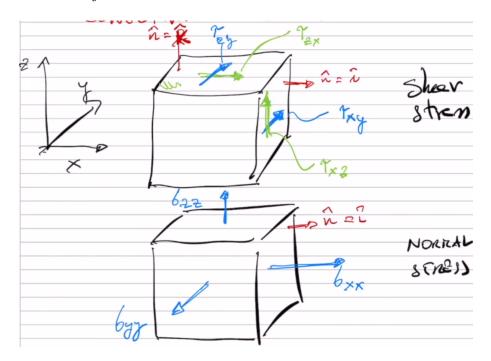
$$\rho \left(\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} \right) = -\frac{\partial p}{\partial y} + \frac{\partial \tau_{xy}}{\partial x} + \frac{\partial \tau_{yy}}{\partial y} + \frac{\partial \tau_{zy}}{\partial z}$$
(1.35)

z direction momentum

$$\rho \left(\frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} \right) = -\frac{\partial p}{\partial z} - \rho g + \frac{\partial \tau_{xz}}{\partial x} + \frac{\partial \tau_{yz}}{\partial y} + \frac{\partial \tau_{zz}}{\partial z}$$
(1.36)

1.4 Stress tensor notation

To identify a stress component we use a double subscript notation (tensor notation). The first subscript indicates the direction of the normal to the plane on which stress acts. Second subscript indicates the direction of the stress. Thus, the symbol τ_{ij} denotes a stress in j direction on a face normal to the i-axis.



The normal stresses two contributions are pressure p and viscous stress τ . Pressure is always negative due to it acting against the surface (if we take the arrow coming out of the surface as positive). τ accounts for the extra stress coming from viscosity.

$$\sigma_{xx} = -p + \tau_{xx} \tag{1.37}$$

$$\sigma_{yy} = -p + \tau_{yy} \tag{1.38}$$

$$\sigma_{zz} = -p + \tau_{zz} \tag{1.39}$$

Parts on the opposite sides of a stress tensor are equal.

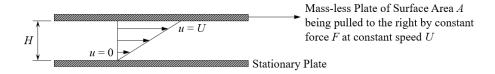
$$\tau_{xy} = \tau_{yx}, \ \tau_{xz} = \tau_{zx}, \ \tau_{yz} = \tau_{zy}$$

Chapter 2

Navier-Stokes Equation

2.1 Constitutive equations

We want to find a way to link the stress tensor τ with the velocity field i.e. $\tau = f(u, v, w)$.



The angle of deformation $\Delta\theta$ can be used to derive the following:

$$\tan \Delta \theta = \frac{u \cdot \Delta T}{H} \tag{2.1}$$

$$\tan \Delta\theta = d\theta = \frac{u \cdot t}{H} \to \frac{d\theta}{dt} = \frac{u}{H}$$
(2.2)

$$\tau = \frac{F}{A} \propto \frac{\mathrm{d}\theta}{\mathrm{d}t} = \frac{u}{H} \tag{2.3}$$

$$\tau = \mu \frac{\mathrm{d}\theta}{\mathrm{d}t} = \mu \frac{u}{H} \tag{2.4}$$

$$\tau = \mu \frac{\mathrm{d}u}{\mathrm{d}y} \tag{2.5}$$

- \bullet τ is the shear stress
- $\frac{\mathrm{d}u}{\mathrm{d}y}$ is the shear rate
- μ is the dynamic viscosity and has units N s m⁻²
- $\nu = \frac{\mu}{\rho}$ is the kinematic viscosity and has units m² s⁻¹

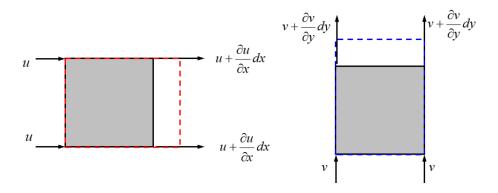
For Newtonian fluids, μ is constant. In the case above, our stress tensor is τ_{yx} , hence:

$$\tau_{yx} = \mu \frac{\partial u}{\partial y} \tag{2.6}$$

Our velocity gradient can be defined as:

$$\nabla \vec{V} = \begin{bmatrix} \frac{\partial u}{\partial x} & \frac{\partial v}{\partial x} & \frac{\partial w}{\partial x} \\ \frac{\partial u}{\partial x} & \frac{\partial v}{\partial y} & \frac{\partial w}{\partial y} \\ \frac{\partial u}{\partial z} & \frac{\partial v}{\partial z} & \frac{\partial w}{\partial z} \end{bmatrix}$$
(2.7)

The left diagonal components are the normal deformation, orthogonal to the surface.



A simplified way of writing these left diagonal terms is

$$\nabla \cdot \vec{V} = \frac{\partial u_i}{\partial x_i} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z}$$
 (2.8)

The repeated index i means sum in the x, y and z directions.

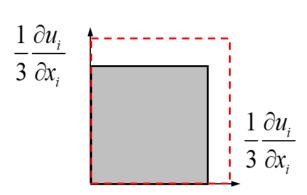
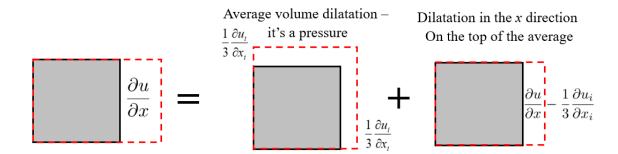


Figure 2.1: 1/3 symbolises the average deformation in x, y and z.

To find $\frac{\partial u}{\partial x}$, we can do the following

$$\frac{\partial u}{\partial x} = \frac{1}{3} \frac{\partial u_i}{\partial x_i} + \left(\frac{\partial u}{\partial x} - \frac{1}{3} \frac{\partial u_i}{\partial x_i} \right) \tag{2.9}$$

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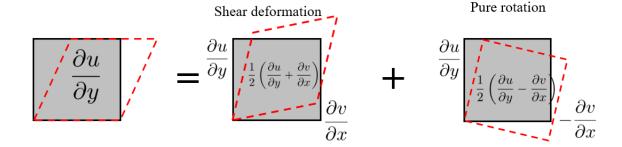
This can be also done for the other two orthogonal directions

$$\frac{\partial v}{\partial y} = \frac{1}{3} \frac{\partial u_i}{\partial x_i} + \left(\frac{\partial v}{\partial y} - \frac{1}{3} \frac{\partial u_i}{\partial x_i} \right) \tag{2.10}$$

$$\frac{\partial w}{\partial z} = \frac{1}{3} \frac{\partial u_i}{\partial x_i} + \left(\frac{\partial w}{\partial z} - \frac{1}{3} \frac{\partial u_i}{\partial x_i} \right) \tag{2.11}$$

Let us consider another term, such as $\frac{\partial u}{\partial y}$. We can define this as a component of deformation and rotation of the fluid particle.

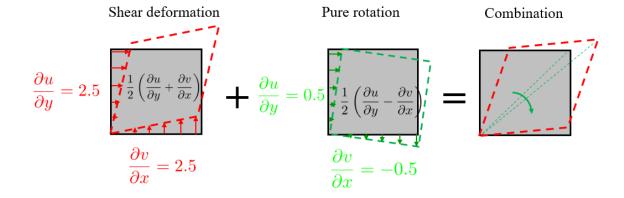
$$\frac{\partial u}{\partial y} = \frac{1}{2} \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) + \left(\frac{\partial u}{\partial y} - \frac{\partial v}{\partial x} \right) \tag{2.12}$$

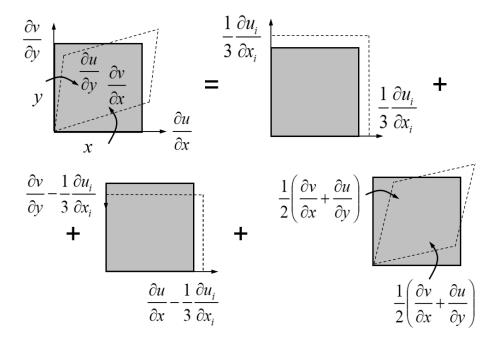


Example

$$\frac{\partial u}{\partial y} = 3 = \frac{1}{2} \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) + \left(\frac{\partial u}{\partial y} - \frac{\partial v}{\partial x} \right) = 2.5 + 0.5 \tag{2.13}$$

$$\frac{\partial v}{\partial x} = 2 = \frac{1}{2} \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) + \left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right) = 2.5 - 0.5 \tag{2.14}$$





2.1.1 Strain rate tensor

$$s = \begin{bmatrix} \frac{\partial u}{\partial x} & \frac{1}{2} \left[\frac{\partial u}{\partial y} + \frac{1}{2} \frac{\partial v}{\partial x} \right] & \left[\frac{\partial u}{\partial z} + \frac{\partial w}{\partial x} \right] \\ \frac{1}{2} \left[\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right] & \frac{\partial v}{\partial y} & \frac{1}{2} \left[\frac{\partial v}{\partial z} + \frac{\partial w}{\partial y} \right] \\ \frac{1}{2} \left[\frac{\partial u}{\partial z} + \frac{\partial w}{\partial x} \right] & \frac{1}{2} \left[\frac{\partial v}{\partial z} + \frac{\partial w}{\partial y} \right] & \frac{\partial w}{\partial z} \end{bmatrix} = (2.15)$$

$$\begin{bmatrix}
\frac{1}{3}\nabla \cdot \vec{V} & 0 & 0 \\
0 & \frac{1}{3}\nabla \cdot \vec{V} & 0 \\
0 & 0 & \frac{1}{3}\nabla \cdot \vec{V}
\end{bmatrix} + \\
\begin{bmatrix}
\left[\frac{\partial u}{\partial x} - \frac{1}{3}\nabla \cdot \vec{V}\right] & \frac{1}{2}\left[\frac{\partial u}{\partial y} + \frac{1}{2}\frac{\partial v}{\partial x}\right] & \frac{1}{2}\left[\frac{\partial u}{\partial z} + \frac{\partial w}{\partial x}\right] \\
\frac{1}{2}\left[\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x}\right] & \left[\frac{\partial v}{\partial y} - \frac{1}{3}\nabla \cdot \vec{V}\right] & \frac{1}{2}\left[\frac{\partial v}{\partial z} + \frac{\partial w}{\partial y}\right] \\
\frac{1}{2}\left[\frac{\partial u}{\partial z} + \frac{\partial w}{\partial x}\right] & \frac{1}{2}\left[\frac{\partial v}{\partial z} + \frac{\partial w}{\partial y}\right] & \left[\frac{\partial w}{\partial z} - \frac{1}{3}\nabla \cdot \vec{V}\right]
\end{bmatrix} (2.16)$$

Deformation part which goes in pressure ρ +

Deformation part which goes in the stress tensor T (2.17)

Compact notation of the strain rate tensor, indices i, j = 1, 2, 3

$$s_{ij} = \frac{1}{2} \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \tag{2.18}$$

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2.1.2 Stress tensor

$$T = \begin{bmatrix} \tau_x x & \tau_y x & \tau_z x \\ \tau_x y & \tau_y y & \tau_z y \\ \tau_x z & \tau_y z & \tau_z z \end{bmatrix} = (2.19)$$

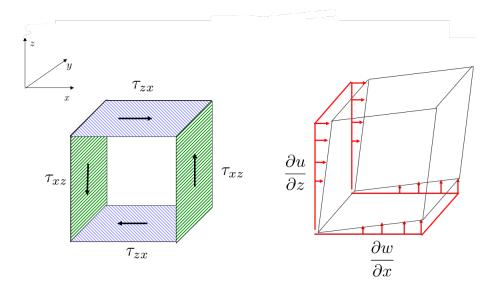
$$\begin{bmatrix}
\mu \left[2\frac{\partial u}{\partial x} - \frac{2}{3}\nabla \cdot \vec{V} \right] & \mu \left[\frac{\partial u}{\partial y} + \frac{1}{2}\frac{\partial v}{\partial x} \right] & \mu \left[\frac{\partial u}{\partial z} + \frac{\partial w}{\partial x} \right] \\
\mu \left[\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right] & \mu \left[2\frac{\partial v}{\partial y} - \frac{2}{3}\nabla \cdot \vec{V} \right] & \mu \left[\frac{\partial v}{\partial z} + \frac{\partial w}{\partial y} \right] \\
\mu \left[\frac{\partial u}{\partial z} + \frac{\partial w}{\partial x} \right] & \mu \left[\frac{\partial v}{\partial z} + \frac{\partial w}{\partial y} \right] & \mu \left[2\frac{\partial w}{\partial z} - \frac{2}{3}\nabla \cdot \vec{V} \right]
\end{bmatrix}$$
(2.20)

Compact notation for constitutive equation:

$$\tau_{ij} = 2\mu \left[s_{ij} - \frac{1}{3} (\nabla \cdot \vec{V}) \delta_{ij} \right] = \mu \left[\left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) - \frac{2}{3} (\nabla \cdot \vec{V}) \delta_{ij} \right]$$
(2.21)

$$\delta_{ij} = \begin{cases} 1 & \text{if } i = j \\ 0 & \text{if } i \neq j \end{cases}$$
 (2.22)

The stress tensor is always symmetric along the left diagonal.



We now have 10/12 equations to describe the fluid. The final two relate to the temperature and the energy of the fluid. We will not be considering the energies of the fluid in this course. Our state equation can be $p = \rho RT$, when the fluid is compressible and if our fluid is incompressible we take ρ as constant. All in all, 11 variables and 11 equations to describe the fluid

2.2 Navier-Stokes Equations

Navier-Stokes equations are a system of equations that can be used to describe the behaviour of a fluid. They can be obtained through inserting the Constitutive Equa-

tions into the Conservation of Momentum Equations, rearranging, and simplifying them. The Navier-Stokes Equations for an incompressible fluid in 3D are as follows:

Conservation of Mass:

$$\nabla \cdot \vec{V} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$
 (2.23)

Conservation of Momentum (x, y, z):

$$\rho \left(\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} \right) = -\frac{\partial p}{\partial x} + \mu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right) \tag{2.24}$$

$$\rho \left(\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} \right) = -\frac{\partial p}{\partial y} + \mu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right)$$
(2.25)

$$\rho \left(\frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} \right) = -\frac{\partial p}{\partial z} + \mu \left(\frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right) - \rho g \quad (2.26)$$

The Navier-Stokes Equations can be further simplified if the following occur:

- Constant Density
- Assume Steady Flow (No Time-Dependent Terms)
- Assume No External Forces
- Assume Fluid is Incompressible

The Navier-Stokes Equations in 2D, with the above assumptions applied are below:

Conservation of Mass (2D):

$$\nabla \cdot \vec{V} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \tag{2.27}$$

Conservation of Momentum (x, y):

$$\rho\left(u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y}\right) = -\frac{\partial p}{\partial x} + \mu\left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2}\right) \tag{2.28}$$

$$\rho \left(u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) = -\frac{\partial p}{\partial y} + \mu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right)$$
 (2.29)

2.3 Lagrangian vs. Eulerian

$$\frac{\mathbf{D}}{\mathbf{D}t} = \frac{\partial}{\partial t} + \left(u \frac{\partial}{\partial x} + v \frac{\partial}{\partial y} + w \frac{\partial}{\partial z} \right) \tag{2.30}$$

- $\frac{D}{Dt}$ Lagrangian/Material Derivative: Variation in time of a property (for example temperature, density or velocity component) of a fluid particle. The reference system is moving with the fluid particle.
- $\frac{\partial}{\partial t}$ Eulerian Derivative: Variation in time of a property (for example temperature, density etc..) in a fixed point in space (x, y, z). Reference system fixed in space.
- $u\frac{\partial}{\partial x} + v\frac{\partial}{\partial y} + w\frac{\partial}{\partial z}$ Convection Terms in the x, y and z: Variation of a property due to how the particle is moving in space.

Chapter 3

Flow in Pipe

Chapter 4

Boundary-Layer Theory

Part II

Thermodynamics