FUEL PIPING Table 12-35

TABLE 12-35 Corrugated Stainless Steel Tubing (CSST) [NFPA 54: Table 6.3(h)]

| | | | | | | | | | | | Gas: | Undiluted Propane 279mm w.c. 12.7mm w.c. | | | |
|-------------------|----------------|------------------|---------|----------|----------|---------|---------|---------|-------------------|-----------|----------|--|-----------|---------|--|
| | | | | | | | | | | Inlet Pr | essure: | | | | |
| | | | | | | | | | | Pressur | e Drop: | | | | |
| | | | | | | | | | Specific Gravity: | | | 1.50 | | | |
| INTENDED U | SE: CS | ST Sizin | g Betwe | en Singl | e or Sec | ond Sta | ge (Low | Pressur | re) Regu | lator and | d Applia | nce Shu | toff Valv | re e | |
| | | Tube Size (EHD)* | | | | | | | | | | | | | |
| Flow Designation: | 13 | 15 | 18 | 19 | 23 | 25 | 30 | 31 | 37 | 39 | 46 | 48 | 60 | 62 | |
| Length (m) | Capacity in kW | | | | | | | | | | | | | | |
| 1.6 | 21.1 | 29.0 | 53.0 | 61.8 | 104.0 | 124.8 | 218.0 | 252.9 | 416.1 | 479.9 | 829.2 | 958.1 | 1,693.5 | 1,919.2 | |
| 3 | 14.7 | 20.2 | 37.8 | 44.0 | 74.4 | 88.8 | 152.7 | 177.3 | 284.5 | 345.4 | 583.1 | 679.8 | 1,204.2 | 1,359.5 | |
| 4.5 | 11.4 | 16.1 | 30.5 | 35.5 | 60.9 | 72.7 | 123.6 | 143.6 | 227.1 | 284.8 | 474.7 | 556.7 | 987.4 | 1,110.5 | |
| 6 | 10.0 | 14.4 | 26.7 | 31.1 | 53.6 | 63.3 | 106.9 | 124.5 | 193.7 | 248.2 | 410.2 | 483.5 | 858.5 | 964.0 | |
| 7.5 | 8.8 | 12.3 | 24.0 | 27.5 | 48.1 | 56.3 | 95.2 | 111.0 | 170.8 | 223.3 | 366.3 | 433.6 | 770.6 | 861.4 | |
| 9 | 8.2 | 11.4 | 21.7 | 25.5 | 44.2 | 51.9 | 87.0 | 100.8 | 154.7 | 204.5 | 334.0 | 395.6 | 703.2 | 785.2 | |
| 12 | 6.7 | 9.7 | 18.8 | 21.7 | 38.4 | 44.8 | 75.0 | 87.0 | 131.6 | 178.7 | 289.5 | 342.8 | 612.4 | 682.7 | |
| 15 | 5.9 | 8.8 | 17.0 | 19.3 | 34.6 | 40.1 | 66.5 | 77.6 | 116.3 | 160.6 | 259.0 | 307.7 | 547.9 | 609.4 | |
| 18 | 5.6 | 7.6 | 15.5 | 17.6 | 31.4 | 36.9 | 60.7 | 70.6 | 105.2 | 147.1 | 235.9 | 281.6 | 501.0 | 556.7 | |
| 21 | 5.0 | 7.3 | 14.4 | 16.7 | 29.0 | 34.3 | 56.0 | 65.0 | 96.7 | 136.5 | 218.3 | 260.8 | 465.9 | 515.7 | |
| 24 | 4.4 | 6.7 | 13.2 | 15.2 | 27.5 | 31.9 | 52.2 | 60.9 | 90.0 | 128.3 | 203.9 | 244.1 | 436.6 | 483.5 | |
| 27 | 4.4 | 6.4 | 12.9 | 14.7 | 26.4 | 29.9 | 49.5 | 57.7 | 83.8 | 121.3 | 192.2 | 230.6 | 410.2 | 454.2 | |
| 30 | 4.1 | 5.9 | 12.0 | 13.8 | 24.9 | 28.7 | 46.6 | 54.5 | 79.1 | 115.1 | 182.0 | 218.6 | 389.7 | 433.6 | |
| 45 | 3.2 | 4.4 | 9.1 | 10.5 | 19.3 | 22.0 | 36.0 | 41.9 | 63.6 | 94.9 | 148.3 | 179.0 | 319.4 | 354.5 | |
| 60 | 2.6 | 4.1 | 8.2 | 9.7 | 17.6 | 20.2 | 32.8 | 37.8 | 53.6 | 82.9 | 128.3 | 155.6 | 277.8 | 307.7 | |
| 75 | 2.3 | 3.5 | 7.3 | 8.8 | 15.5 | 17.9 | 29.0 | 34.3 | 47.8 | 74.4 | 114.3 | 139.5 | 249.1 | 273.7 | |
| 90 | 2.3 | 3.2 | 6.7 | 7.6 | 14.7 | 16.7 | 26.4 | 31.4 | 43.1 | 68.6 | 104.6 | 127.2 | 227.7 | 250.2 | |

^{*}EHD = Equivalent Hydraulic Diameter, which is a measure of the relative hydraulic efficiency between different tubing sizes. The greater the value of EHD, the greater the gas capacity of the tubing.

⁽¹⁾ Table includes losses for four 90 degree bends and two end fittings. Tubing runs with larger numbers of bends and/or fittings shall be increased by an equivalent length of tubing to the following equation: L= 1.3n, where L is additional length (ft) of tubing and n is the number of additional fittings and/or bends.

(2) All table entries are rounded to 3 significant digits.

SI: 1m = 3.3 ft.; 1mm = 0.04 in.; 1m³ = 33.3 ft.³; 1bar = 14.5 psi